# Transformational Membranes for Pre-combustion Carbon Capture – DE-FE0031635

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# Membranes for CO<sub>2</sub>/H<sub>2</sub> Separation



## **Facilitated Transport Membrane**



 Facilitated transport of CO<sub>2</sub> via reversible reaction with amin CO<sub>2</sub> + R-NH<sub>2</sub> + H<sub>2</sub>O → R-NH<sub>3</sub><sup>+</sup> + HCO<sub>3</sub><sup>-</sup>
 Facilitated transport = flux augmentation via reaction



#### **Techno-economic Analysis** CO<sub>2</sub> Partial Pressure Change and Membrane Allocation CO; partial pres - - - CO<sub>2</sub> permeance -- CO./H. selectivit Membrane 3 Membrane 2 Feed inle Hudropen recover 0.6 20 30 40 50 60 70 80 0.2 0.4 0.8 Percentage of Membrane 3 (%) Effect of Feed Pressure Effect of CO<sub>2</sub> Permeance --- COE increase 20 Membrane are: 17 COE increase of current branes 2 and 3 20 150 200 250 300 350 400 Feed pressure (bar) CO<sub>2</sub> permeance (GPU) Effect of H<sub>2</sub>S/CO<sub>2</sub> Selectivity Effect of Membrane Cost 4 vnaas H<sub>2</sub>S for curr Membranes 2 and 3 40 60 80 H<sub>2</sub>S/CO<sub>2</sub> selectivity Membrane element cost (\$/m2 Techno-economic Analysis Based on Cases B5A and B5B in NETL baseline • Feasible separation performance at >30-bar feed pressure · Considerable reduction in gas cooling requirement compared to Selexol 15.7% COE increase for current compositions, >50% less than Selexol

- >99.4%  $H_2$  recovery achieved by high  $CO_2/H_2$  selectivity
- <6 ppm  $H_2S$  in sweet syngas, promising for use in chemical synthesis

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