

# Universal Solvent Viscosity Reduction via Hydrogen Bonding Disruptors

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DOE Program Manager: Andrew Jones

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# Project Overview

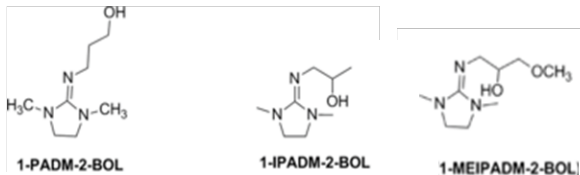
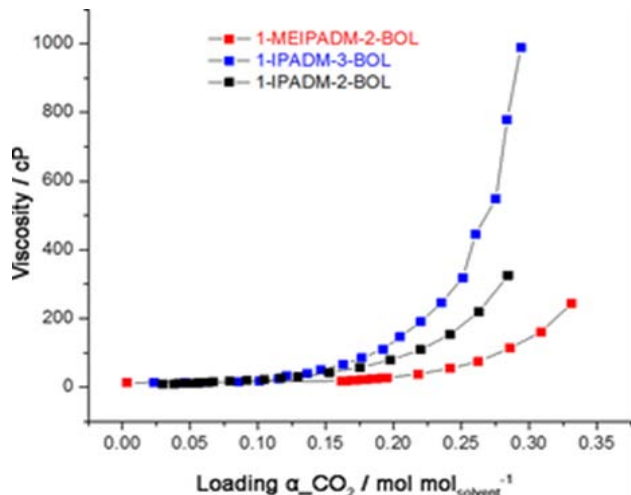
- Funding: \$2,304,612
  - DOE: \$1,843,690
  - Cost Share: \$460,922
- Overall Project Performance Dates:
  - 10/01/2018 – 9/30/2021
- Project Participants:
  - Liquid Ion Solutions (LIS)
  - Carnegie Mellon University (CMU)
  - Carbon Capture Scientific (CCS)



# Project Objectives

- Computer simulation to understand the molecular interactions in non-aqueous CO<sub>2</sub> capture solvents.
- Synthesis and characterization of hydrogen bonding disrupter molecules with the specific goal of significantly reducing the viscosity of non-aqueous carbon capture solvents in the presence of CO<sub>2</sub>.
- Proof-of-concept performance testing to demonstrate the effectiveness of hydrogen bonding disrupters in lowering viscosity.
- Optimization of hydrogen bonding disruptor chemical structure based on insights gained from computational modeling and experimental proof-of-concept studies.
- Demonstration of the effectiveness of the optimized hydrogen bonding disrupters in the presence of synthetic flue gas.

# Technical Background - The Problem



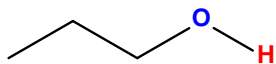
## Aqueous amine drawbacks:

- High energy cost for solvent regeneration
- Solvent loss due to evaporation
- Oxidative and thermal degradation in the adsorption-desorption cycles
- Corrosion problems

## Non-aqueous amine drawbacks:

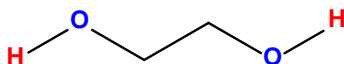
- High viscosity
  - Slower CO<sub>2</sub> uptake
  - Need more surface area (Larger equipment\$)\$

# Effect of Hydrogen Bonding (HB) and Electrostatic (ES) on Viscosity



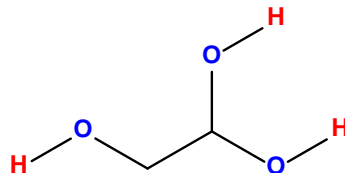
Molecular Weight: **60.10**

**2 Cp @25°C**



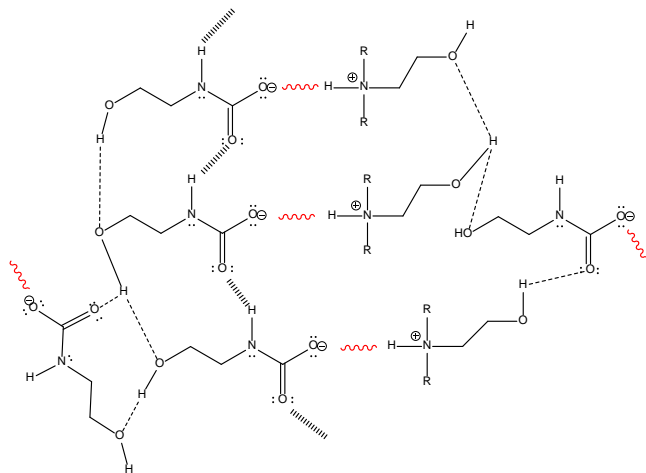
Molecular Weight: **62.07**

**37 Cp @25°C**



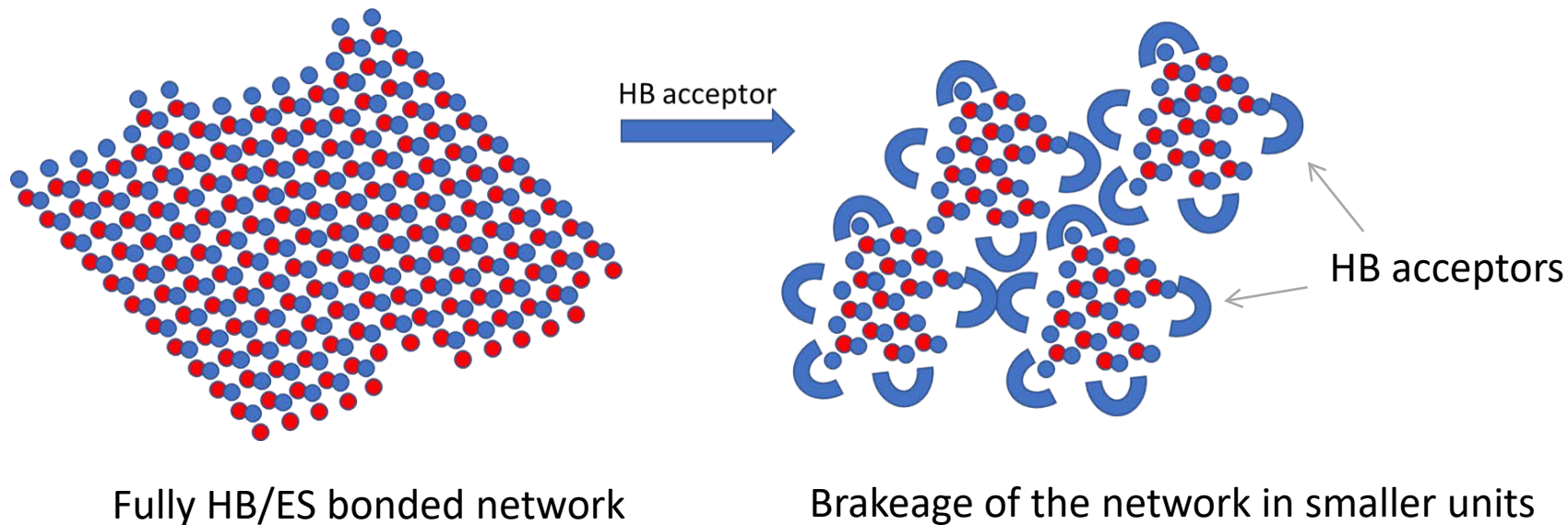
Molecular Weight: **78.07**

**934 Cp @25°C**

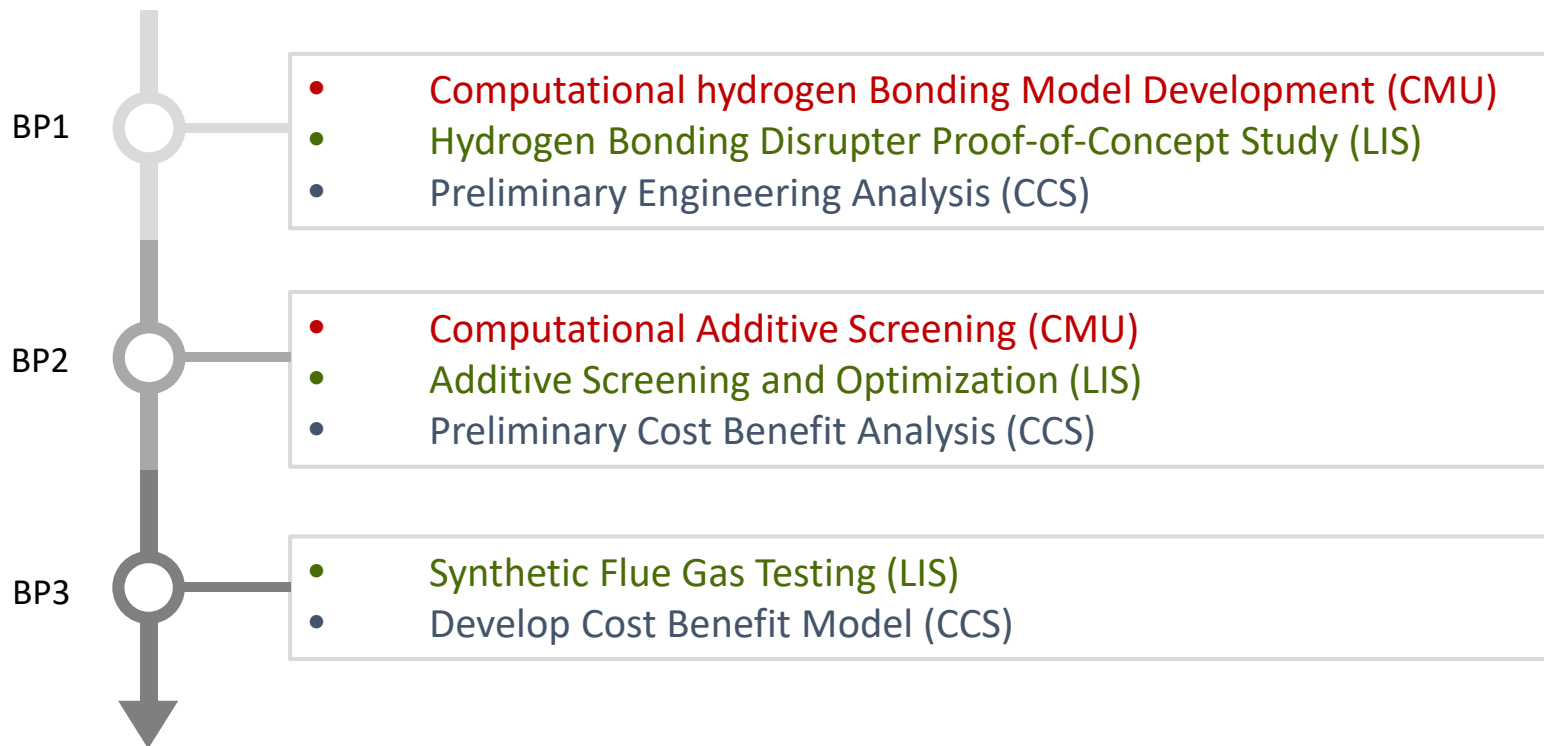


Hydrogen bonding and ionic bonding in a monoethanolamine based solvent

# The Solution –Segmentation



# Project Schedule

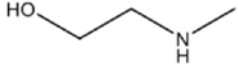
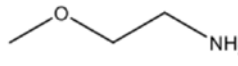
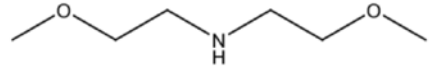


# Research Progress



## Task 2. Computational Hydrogen Bonding Model Development

### Construction of Ab Initio Molecular Model

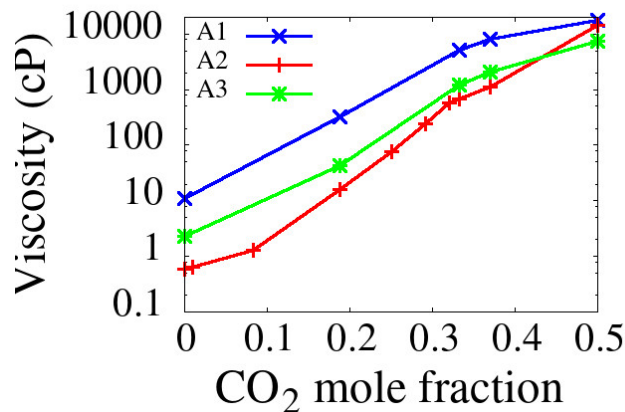
Chemical structure	Abbr.
	A1
	A2
	A3

Force field parameterization based on OPLS-AA force field with the aid of ab-initio calculations:

- Ab-initio calculations for amines and cations at MP2/6-31G(d,p) level, while those for anions were at MP2/6-31G++(d,p) level.
- Partial charges were fitted using CHELPG method.

Solvent	MD	Viscosity at 300K lit.	Viscosity at 298.15K exp.
A1	11.15	10.51	13.8
A2	0.59	0.66	0.6
A3	2.28	--	1.3

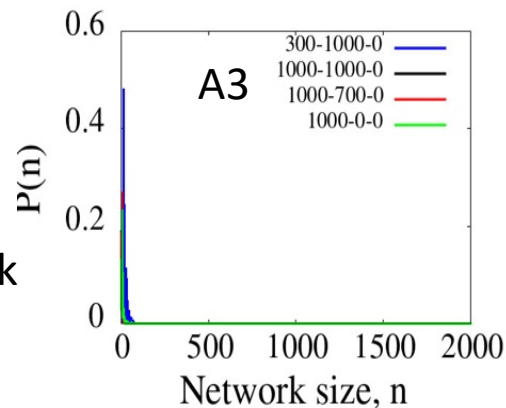
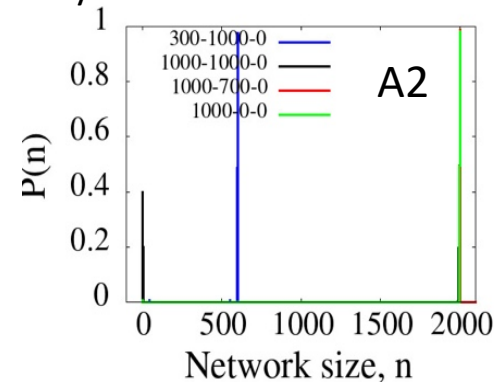
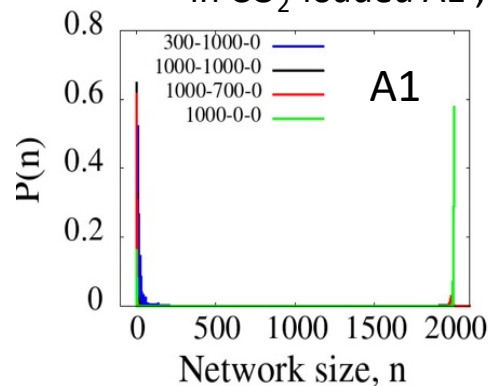
# Simulation of Relationship between Hydrogen Bonding and Viscosity



Viscosity vs CO<sub>2</sub> mole fraction  
(= mol CO<sub>2</sub>/mol total amine)  
for A1, A2, and A3

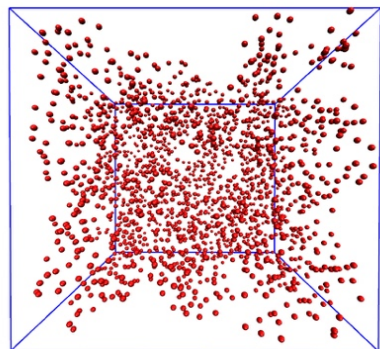
Ions in A1 and A2 form essentially a single network  
A3 forms many small networks.

Size distribution of “hydrogen-bonded” ion networks  
in CO<sub>2</sub>-loaded A1, A2 and A3 systems

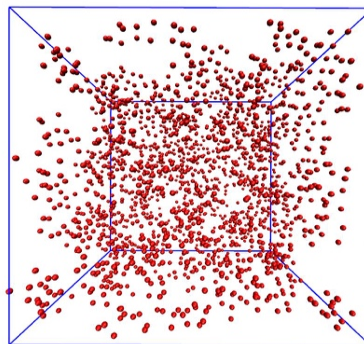


# Quantitative Analysis of Co-solvent and Mixture Effects

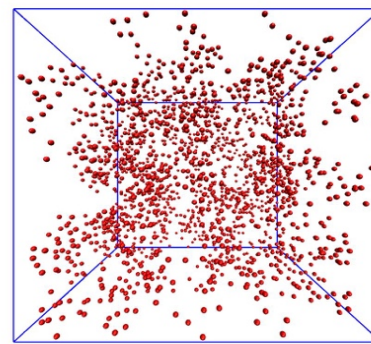
1000 A2 + 1000 ion pairs ( $\text{CO}_2$  mole fraction = 0.333) + additives (DMSO)



No DMSO



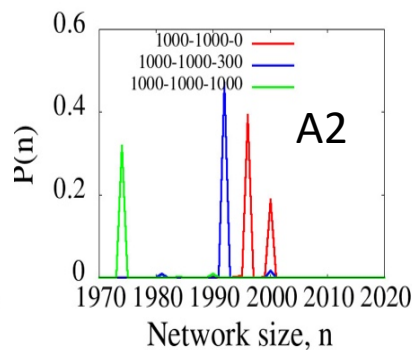
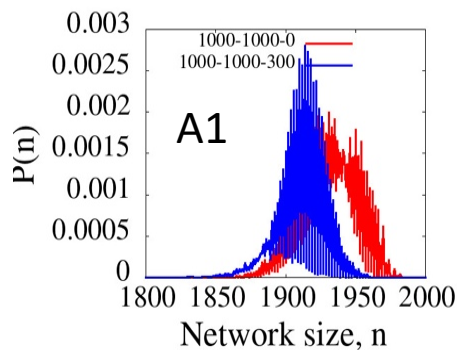
300 DMSO



1000 DMSO

Only nitrogen atoms of ions are shown.

Size distribution of “hydrogen-bonded” ion networks in  $\text{CO}_2$ -loaded A1 and A2 systems



As DMSO are added, hydrogen-bonded ion network becomes “looser” and somewhat smaller

## Effects of Additives on System Viscosity

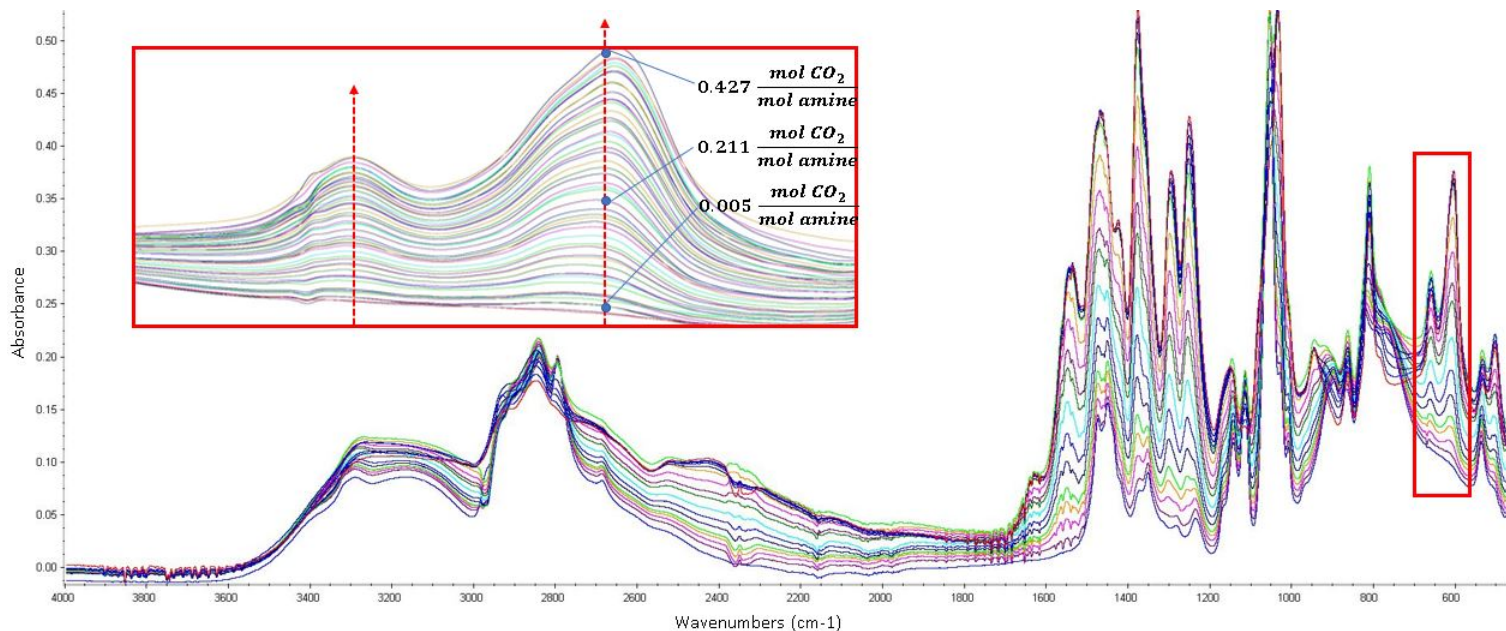
Type of amine	Mole fraction of adsorbed CO <sub>2</sub> vs total amine	Viscosity (cP)	Number of DMSO molecules	Number of water molecules	Viscosity with DMSO or water (cP)
A1	0.333	5148	300	0	3024
	0.370	8182	300	0	5278
	0.500	17641	300	0	8158
A2	0.188	16	300	0	14
	0.250	78	300	0	44
	0.291	244	300	0	154
	0.333	684	300	0	377
	0.333	684	1000	0	175
	0.333	684	0	1300	742
	0.333	684	0	4000	207
	0.370	1134	300	0	957
	0.500	14370	300	0	6576
	0.500	14370	600	0	3309
A3	0.333	1197	300	0	568
	0.370	2029	300	0	1017
	0.500	7490	300	0	4010

- Viscosity increases as CO<sub>2</sub>/amine ratio increases
- Both DMSO and water have similar effect on viscosity reduction
- The higher the additive %, the more viscosity reduction

# Task 3. Hydrogen Bonding Disruptor Proof-of-Concept Study

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## Baseline Solvent Testing



- Obtained quantitative correlation between CO<sub>2</sub> uptake and FT-IR spectra

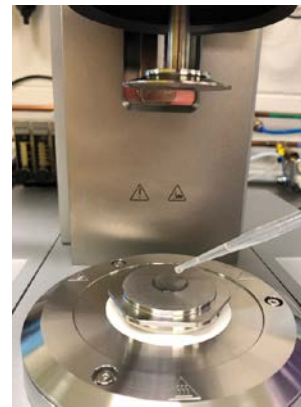
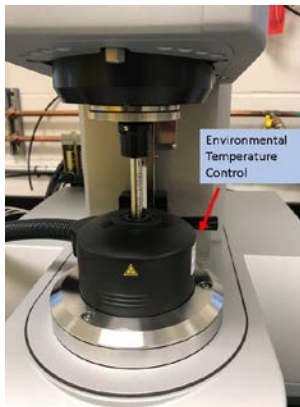
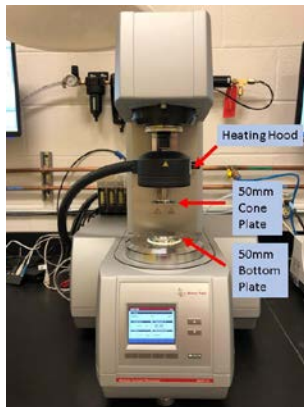
# Task 3. Hydrogen Bonding Disruptor Proof-of-Concept Study cont'd

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## Initial Hydrogen Bonding Disruptor Synthesis

- Designed several classes of compounds with various molecular architectures and functionalities
- Prepared five promising candidates for viscosity testing.

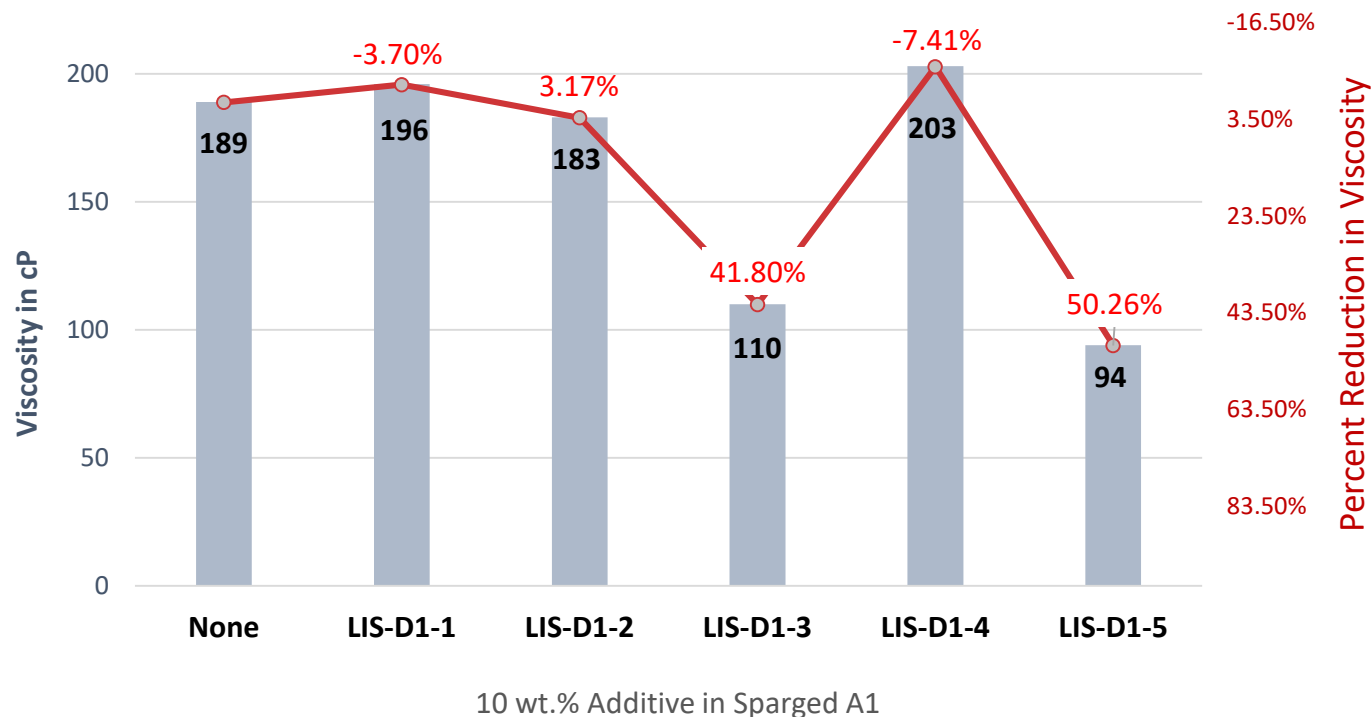
## Proof-of-Concept Viscosity Testing – Rheometer Setup



# Task 3. Hydrogen Bonding Disruptor Proof-of-Concept Study cont'd

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Effect of 10 wt.% additives on sparged A1



# Task 3. Hydrogen Bonding Disruptor Proof-of-Concept Study cont'd

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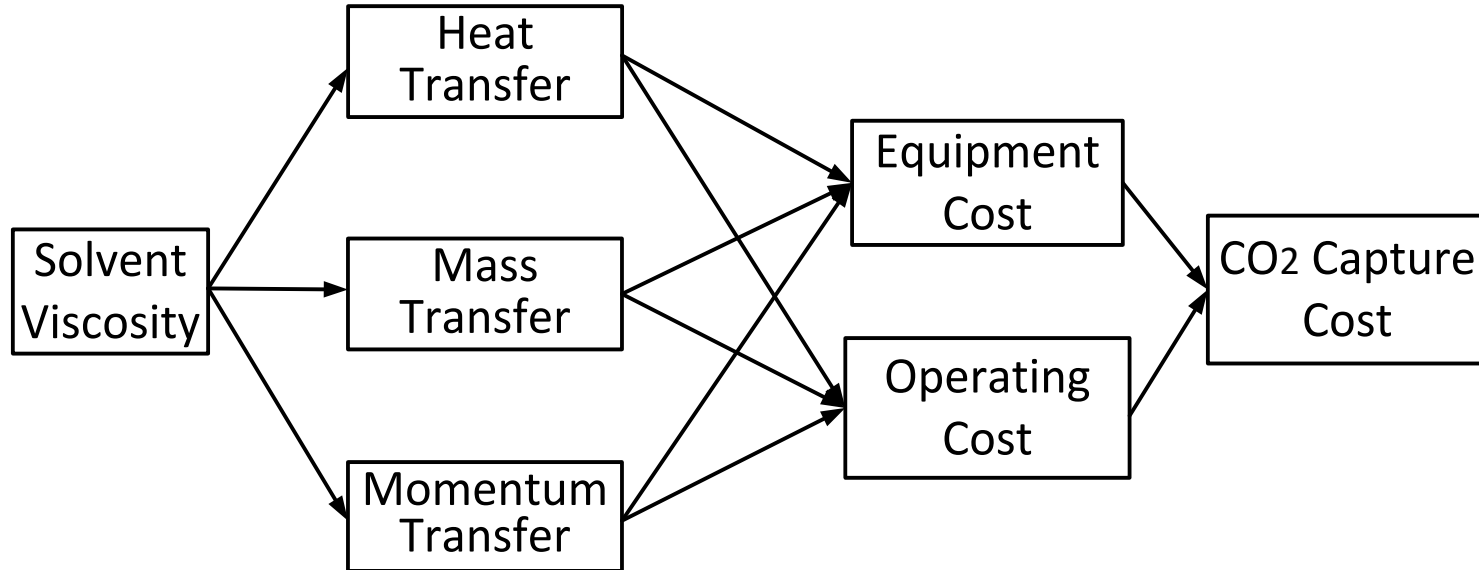
Effect of 10 wt.% LIS-D1-3 on sparged amines

Amine	CO <sub>2</sub> wt.%	Molar Ratio [CO <sub>2</sub> /Amine]	Viscosity of Amine, cP	Viscosity of Amine + Additive, cP	% Reduction in Viscosity
A1	17.7	0.3021	189 ± 8	110 ± 1	41.8
A2	17.65	0.3012	22 ± 2	16 ± 1	27.3
A3	9.14	0.3021	4.8 ± 0.7	<b>1.8 ± 0.04</b>	62.5



# Task 4. Investigation of Impacts of Viscosity on Solvent Based CO<sub>2</sub> Capture Processes 17

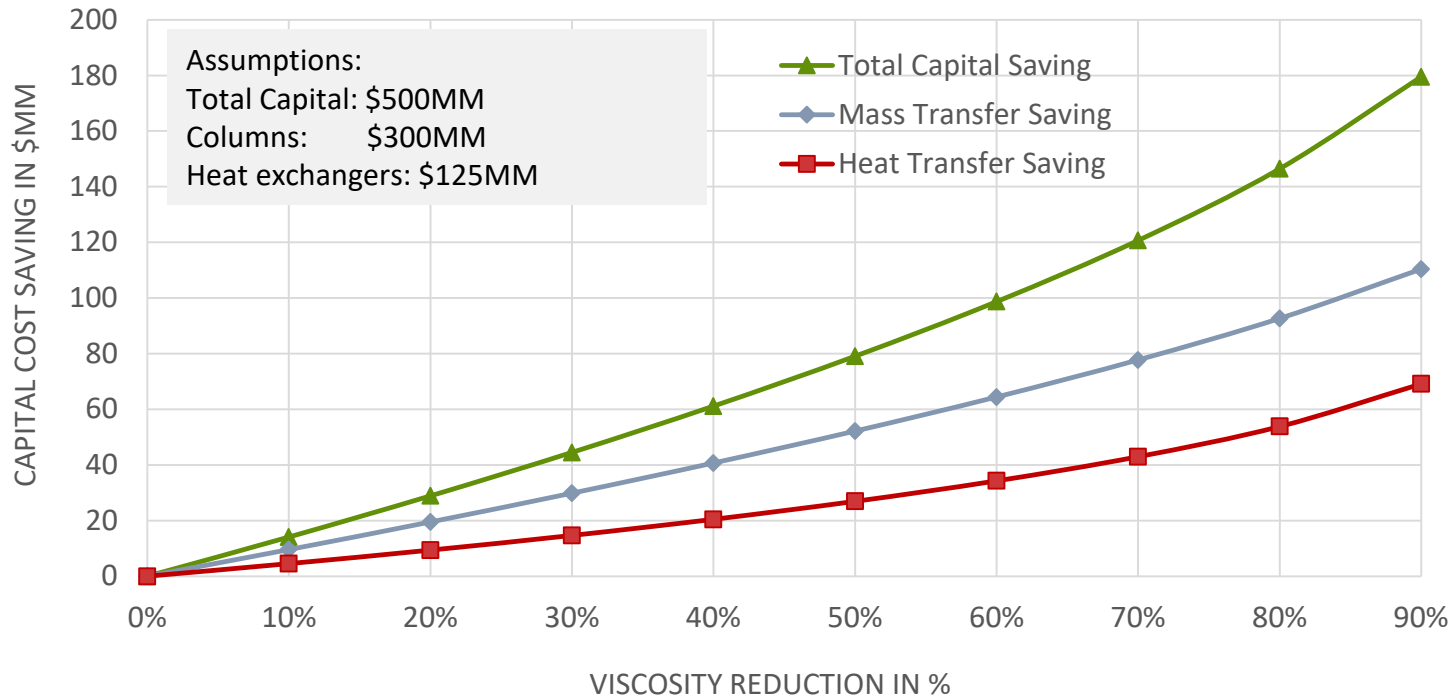
## Overall Approach



# Task 4. Investigation of Impacts of Viscosity on Solvent Based CO<sub>2</sub> Capture Processes cont'd

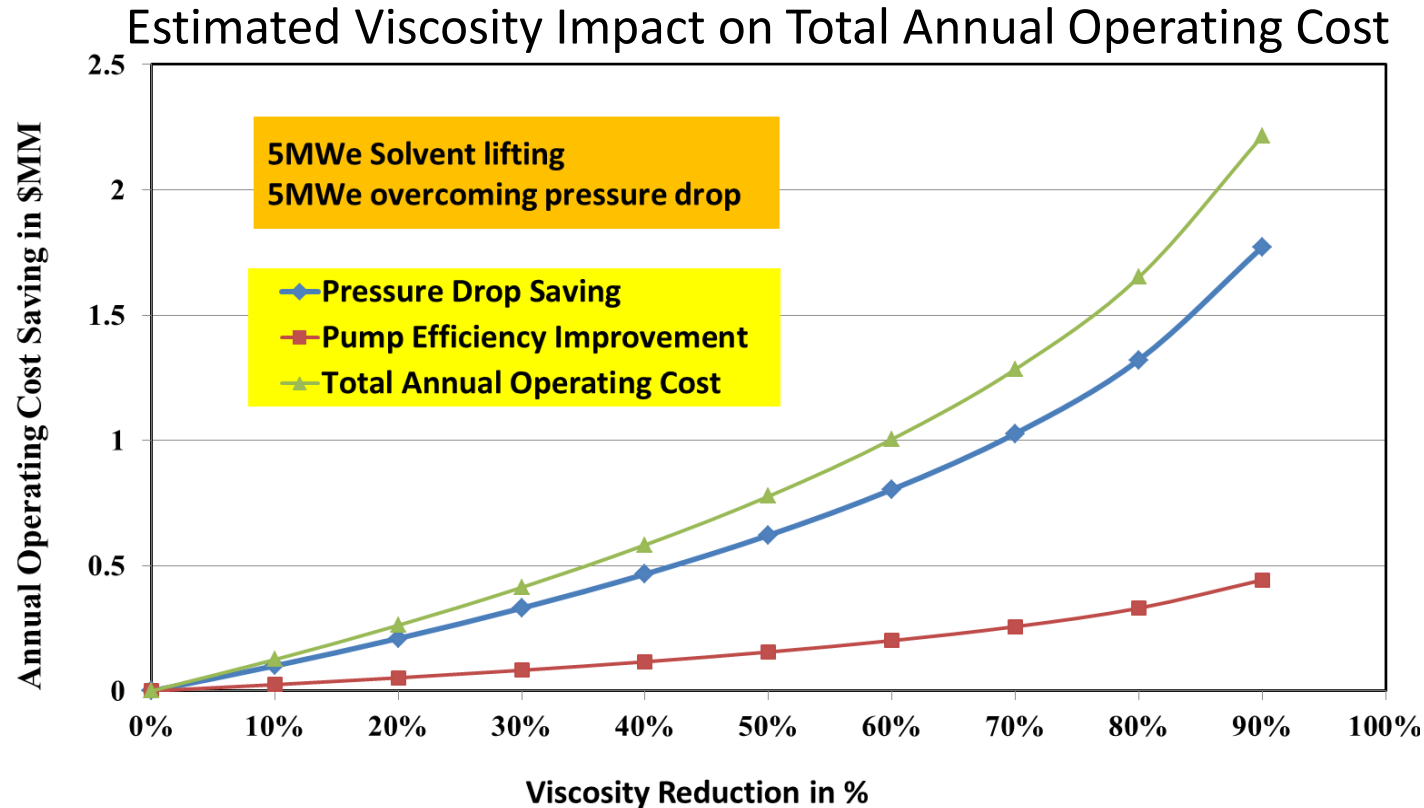
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## Obtained Viscosity Impact on Total Equipment Cost



# Task 4. Investigation of Impacts of Viscosity on Solvent Based CO<sub>2</sub> Capture Processes cont'd

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# Conclusions and Future Plan

- Computational study gave insights on hydrogen bonding in the model solvents, viscosity at various CO<sub>2</sub> level, and additive effect on viscosity reduction.
- Additives LIS-D1-3 and LIS-D1-5 showed 40-50 % viscosity reduction on all model amines.
- LIS-D1-3/A3 system showed viscosity around 2 cP, demonstrating the potential feasibility of the additive approach.
- Preliminary engineering analysis revealed that a 50% reduction in solvent viscosity will reduce total equipment cost of an absorption/stripping based process by 15%.
- In the process of designing and preparing Gen2 additives based on the insights gained from BP1 research.

# Acknowledgement and Disclaimer

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# Thank you!

Any Questions?