

2018 NETL CO₂ Capture Technology Project Review Meeting Pittsburgh, PA August 13 – 17, 2018

Advanced CO₂ Compression with Supersonic Technology (FE0026727)

dresser-rand.com

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The Dresser-Rand business

Well positioned to compete and bring value to our clients



• Enhanced client relationships & agreements

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The Dresser-Rand business at a glance



Services now part of Siemens Power Generation Services Distributed Generation and Oil & Gas

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History of Innovation and Technology Leadership





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Partnership with U.S. DOE

In 2008, The U.S. Department of Energy partnered with Ramgen Power Systems and the Dresser-Rand business by co-funding the adaption of flightbased supersonic compression to carbon capture and sequestration (CCS) applications requiring "100:1" total CO_2 compression ratios.

The DOE identified two key objectives:

- Reduce cost
- Improve efficiency

Supersonic compressors offer the potential of lower capital costs, smaller footprints, competitive efficiencies, and waste heat energy recovery.

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History and Testing Milestones

2008 Dresser-Rand and Ramgen Power Systems entered into an exclusive arrangement to further develop supersonic compression technology Construction of the world's first supersonic CO₂ compression test facility 2011 2013 First HP compressor test phase concluded with successful demonstration of CO₂ shockwave compression Second HP CO₂ compressor test phase concluded; achieved 9:1 2014 pressure ratio Dresser-Rand acquired assets of Ramgen Power Systems and established Seattle Technology Center in Bellevue, WA, USA Third HP CO₂ compressor test phase (DATUM S) concluded; achieved 2015 11.5:1 pressure ratio 2016 Award signed (DE-FE-0026727) Design of LP CO₂ compressor completed and manufactured. Assembly 2017 began in fall 2017 2018 First LP CO₂ compressor test phase (DATUM S) concluded; achieved 12.0:1 pressure ratio LP/HP 100:1 compressor train is sized at ~ 182 MWe , 90% capture 1.5 MTPA of CO₂ Unrestricted



DATUM-S Compressor Program – DOE Partnership

- Selection notification announced Aug 13, 2015: DE-FOA-0001190
- Award signed (DE-FE-0026727) March 16, 2016
- Program kick-off meeting held April 8, 2016
- Scope included:
 - Additional HP unit testing
 - Design / build / test the high flow coefficient LP stage to complete the 100:1 total pressure ratio demonstration
 - TEA including heat integration into Case B12B

DOE partnership and support is critical to the success of this program.

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DATUM-S HP and LP Compressors







DATUM-S Compressor Benefits

When compared to traditional subsonic compression solutions

- Smaller footprint, less equipment, less piping, fewer coolers
- Higher compression ratios
- Reduced need for gas intercooling
- Discharge temperatures exceeding 550°F (290°C)
- Waste heat recovery enables unmatched overall system efficiency



Improved availability, integration of waste heat and smaller footprint all underscore the merits of employing the DATUM-S compressor for the lowest total cost of ownership.

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Waste Heat Integration



Heat integrated back into the system 5% Waste

In a traditional system that is 85% efficient, 15% of the total energy input is lost and manifests itself mostly as low-grade heat.

In a DATUM-S compression system that is 80% efficient, 20% of the total energy input manifests itself as midgrade heat.

If 75% of the mid-grade heat can be put to work, waste energy stream is reduced to 5%.

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Multiple Opportunities for Waste Heat Integration

- Regenerate sorbent / amine Transfer heat from the compressed CO₂ and reduce steam diversion from the power cycle
- Sorbent drying Utilize waste heat to dry sorbent after steam regeneration
- Amine reboiler Utilize waste heat in the amine reboiler
- Boiler feed water heater Utilize waste heat to heat boiler feed water and reduce steam diversion from power cycle

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Schedule Summary (Fiscal Years Shown)



Program executed in 34 months (vs 31 month initial plan)

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Olean: Dedicated High Pressure CO₂ Test Facility





In parallel with the compressor design efforts, a new 10 MW test facility was designed and built on the Olean, NY campus

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10MW HP CO₂ Compressor on Test Stand





- 10MW electric drive
- Closed loop CO₂
- P1 = 210 psia
- P2 = 2,100 psia

HP and LP unit is sized at ~ 182 MWe , 90% capture 1.5 MTPA of CO_2

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DATUM-S LP CO₂ Compressor Design

- LP CO₂ compressor design evolved through the following process
 - System requirements
 - Conceptual design
 - Preliminary design
 - Final design
 - Production readiness and release •
- Design decisions were based on extensive analysis of system components
 - Aero : 1D meanline, 3D CFD and flow path optimization
 - Mechanical: structural, modal, thermal and • rotor dynamic

Rigorous design process executed to ensure compressor satisfies requirements

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DATUM-S Optimization on OLCF's Titan Supercomputer





- Intelligently driven optimization is used to maximize compressor performance
- Database generation requires 17,000 simulations, 34 hrs on 128,000 cores
- Each optimization cycle requires evaluation of 600 simulations, 2 hrs on 76,800 cores
- Access to the DOE OLCF Titan supercomputer has been invaluable to optimize DATUM-S aerodynamic designs
- DATUM-S development greatly accelerated by the ORNL Supercomputers

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LP CO₂ Assembly Tooling



Tooling assemblies for bundle insertion into pressure case

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10 MW LP CO₂ Test Configuration

(Typical test arrangement shown for reference)



Selected test configuration leverages existing D-R production components to reduce overall program costs

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Test Results: Pressure Ratio



Normalized Flow

- Compressor achieved program performance target at design operating speed
- At 104% speed compressor achieved a pressure ratio in excess of 12:1
- Use of MIGVs significantly increases the compressor turndown capability
- Good agreement between CFD pre-test prediction and experimental data is observed

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Test Results: Efficiency



- Compressor achieved program efficiency target at design operating speed
- At 104% speed a slight decrease in efficiency is observed
- Lessons learned from HP testing were incorporated in the design of the LP unit
- Good agreement between CFD pre-test prediction and experimental data is observed Unrestricted

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Test Results: IGV Actuation at 104% Speed



Normalized Flow

- Compressor IGV actuation at constant speed provided an increase in compressor operating range while achieving a total pressure ratio in excess of the program goal
- Further compressor testing for larger IGV operating angles planned as part of Dresser-Rand internal R&D efforts

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Tasks 3.0 - Initial Techno-Economic Analysis

- The Dresser-Rand business performed an initial Techno-Economic Analysis (TEA) to evaluate the benefit of integrating the DATUM-S compressor for a CCS application
- NETL Baseline Case B12B from Cost and Performance Baseline for Fossil Energy Plants, Volume 1a, Revision 3 was used as a benchmark and baseline
- A thermodynamic tool was created to model the CO₂ compressors, heat exchangers, and changes to the plant steam cycle
- Compressor selection and staging were configured to provide the TEG dryer inlet pressure at 439 psia
- For the initial TEA, a hybrid approach that provides heat to both the amine reboiler and boiler feed water heater was selected
 - CO₂ is routed to amine reboiler and waste heat is recuperated to around 300 °F (149 °C)
 - Remaining heat energy is used in the feed water heater

Selected approach increases both plant net output power and efficiency, and reduces plant capital cost.

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Task 3.0 - Initial Techno-Economic Analysis

- Existing Case B12B dehydration pressure level constrained DATUM-S compressor ratios, but value of heat integration was still apparent
 - Displaced steam generated 15.8 MWe additional power, for a net gain of 3 MWe electricity (turbine - compressor power) from B12B Baseline
 - Plant CAPEX reduced \$15M; COE reduced by \$1.17/MWh
 - Circulating cooling water flow reduced by 21,000 gallons per hour
- Case B12B baseline CO₂ compressor underestimated actual power requirement
 - Commercial selection of comparable integrally-geared compressor indicated Case B12B compressor would consume 42.7 MW, a 7 MW increase from the baseline
 - Compared to updated selection, DATUM-S enables a net gain of 10 MWe (turbine compressor) above the proposed / modified B12B baseline

Initial TEA showed strong benefit from DATUM-S with heat integration

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Task 9.0 - Final Techno-Economic Analysis

	Case B12B	Case B12B alternate	DATUM S w/ heat integration		
	Baseline	Lower IG comp. perf.	Case DR1	Deltato baseline	Deltato alternate
Gross Power, MWe	641.5	641.5	656.3	14.8	14.8
Aux Load, MWe	91.3	99.7	104.7	13.4	5.0
Net Power, MWe	550.2	541.8	551.6	1.4	9.8
HHV Net Plant Eff., %	32.5%	32.0%	32.6%	0.1%	0.6%
HHV Net Plant Heat Rate, Btu/kWh	10,508	10,672	10,482	-26	-190
COE w/o T&S, \$/MWh	133.17	135.40	132.13	-1.04	-3.27
ΔĊOE/ĊOE _{comp} , %	-	_	_	-10%	-27%

Significant CAPEX and COE reduction achieved with DATUM-S and heat integration

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Task 9.0 - Final Techno-Economic Analysis

	Case B12B	DATUM S w/ heat		DATUMS w/ improved heat	
	alternate LowerIG comp. perf.	Case DR1	ration Delta to alternate	Case DR2	ration Delta to alternate
Gross Power, MWe	641.5	656.3	14.8	657.0	15.5
Aux Load, MWe	99.7	104.7	5.0	104.3	4.6
Net Power, MWe	541.8	551.6	9.8	552.7	10.9
HHV Net Plant Eff., %	32.0%	32.6%	0.6%	32.6%	0.6%
HHV Net Plant Heat Rate, Btu/kWh	10,672	10,482	-190	10,460	-212
COE w/o T&S, \$/MWh	135.40	132.13	-3.27	131.95	-3.45
ΔCOE/COE _{comp} , %	_	_	-27%	_	-28%

Sensitivity study (closer HX approach, better utilization of heat) shows even larger benefit

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Task 9.0 - Final Techno-Economic Analysis

- For the final Techno-Economic Analysis, the plant architecture remained the same as for the initial TEA, with the heat of compression displacing steam used in the amine reboiler and boiler feedwater heaters.
- Case B12B dehydration pressure level was not altered (439 PSIA). This constrained DATUM-S compressor ratios as in the initial TEA.
 - Co-optimization of the TEG dehydration pressure and DATUM-S pressures represents an opportunity to further improve TEA results.
- Thermodynamic model was updated for the final TEA:
 - Excel model was replaced with one in Thermoflex
- Heat integration from the DATUM-S results in significant improvement
 - Displaced steam generated 14.8 MWe additional power, for a net gain of 1.4 MWe electricity from B12B Baseline
 - Plant CAPEX reduced \$16M; COE reduced by \$1.04/MWh
 - Circulating cooling water flow reduced by 21,500 gallons per hour
- Case B12B baseline CO₂ compressor underestimated actual power requirement
 - Commercial selection of comparable integrally-geared compressor indicated Case B12B compressor would consume 44.0 MW, an 8.3 MW increase from the baseline
 - Compared to updated selection, DATUM-S enables a net gain of almost 10 MWe above the proposed/modified B12B baseline

Final TEA shows strong benefit from DATUM-S with heat integration

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Summary

- Completed HP and LP compressor testing
 - 11.5:1 pressure ratio in HP
 - 12.0:1 pressure ratio in LP
 - Discharge temperature is approximately ~550F
- Completed final TEA for integration of waste heat shows benefit for Carbon Capture and Sequestration applications
 - 28% reduction in COE for the cost of compression duty
 - 21,000 gallon reduction in cooling water
- Program was executed in 34 months compared to 31 month original schedule
- Program was executed within 1.6% of total initial budget, \$8.13M vs \$8.00M

Dresser-Rand business continues to develop and commercialize supersonic compression technology to reduce cost and improve efficiency of compression for CCS applications.

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Contact



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Mark J Kuzdzal Director, Business Development Strategic Business Development and Commercialization Unit 500 Paul Clark Drive, Olean, New York, 14760, USA Tel: +1 (716) 375-3573 Mobile: +1 (716) 378-5483 Mark.Kuzdzal@siemens.com

Ravi Srinivasan Aero/Thermodynamic Engineer R&D Seattle Technology Center 11808 Northup Way Suite W-190 Bellevue, WA 98005 Phone: +1 (425) 828-4919 ext 247 Fax: +1 (425) 828-7756 ravichandra.srinivasan@siemens.com

dresser-rand.com

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