

# *Improving the Economic Viability of Biological CO<sub>2</sub> Utilization by Improved Algae Productivity & Integration with Wastewater Treatment*

Cooperative Agreement No: DE-FE0030822

CO<sub>2</sub> Capture Technology  
Project Review Meeting  
August 2019

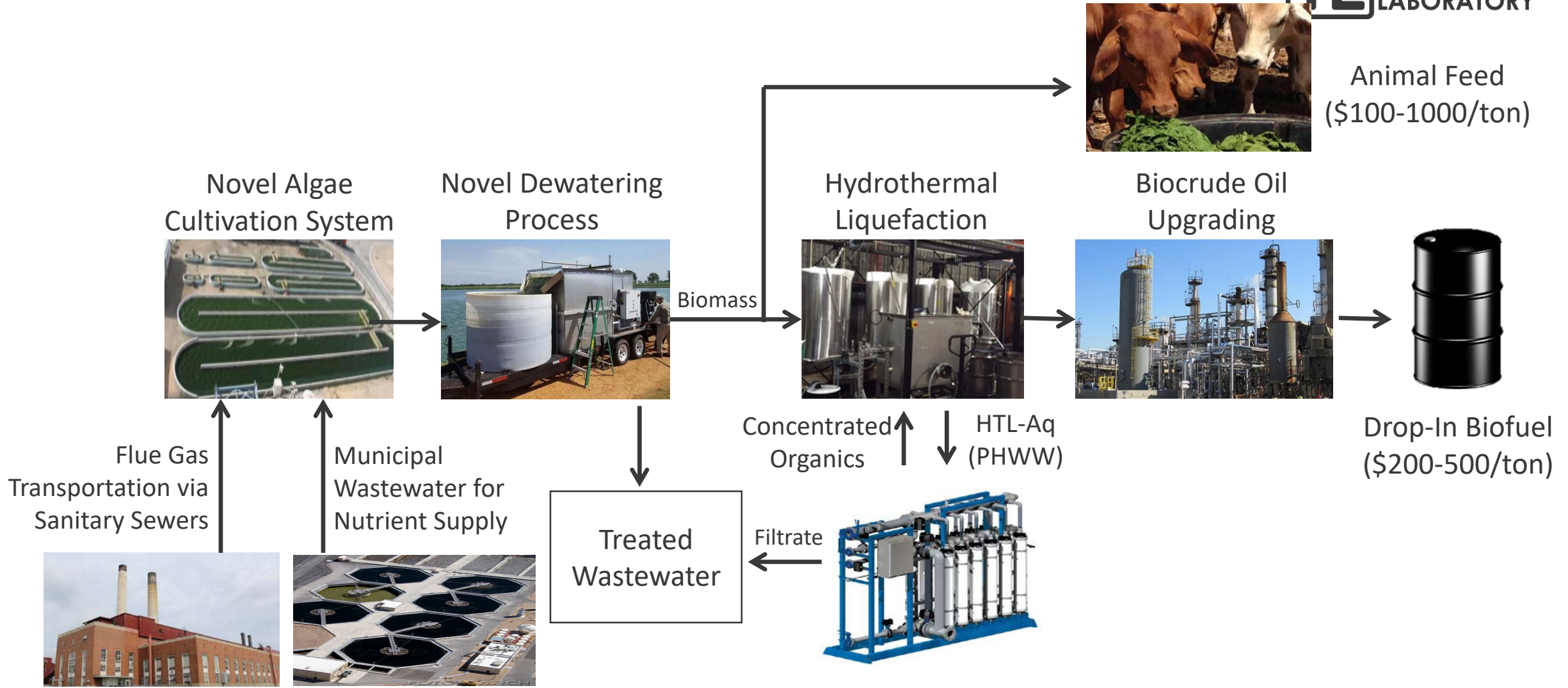


# Basic Project Information for DE-FE0030822



- **Title:** *Improving the Economic Viability of Biological Utilization of Coal Power Plant CO<sub>2</sub> by Improved Algae Productivity & Integration w/ Wastewater Treatment*
  - DOE Program Manager: Andy Aurelio
  - Lead Organization: University of Illinois- Illinois Sustainable Technology Center
  - Primary Collaborating Organization: Helios-NRG
    - CO-Pi: Ravi Prasad, Fred Harrington
- **DOE Funding Program DE-FOA-0001622:** *Applications for Technologies Directed at Utilizing Carbon Dioxide from Coal Fired Power Plants*
  - Total Project Value: \$ 1,249,873      Government : \$999,536      Cost Share: \$250,337
  - Currently in Budget Period 2 (BP2)- October 1, 2018 – September 30, 2019
- **Major Project Objectives & Goals**
  - End of project performance goals
    - 35 g/m<sup>2</sup>day biomass productivity (vs 8.5 g/m<sup>2</sup> day DOE Baseline- 2015 State of Technology)
    - 70% CO<sub>2</sub> capture efficiency
    - \$470/ton algal biomass projected n<sup>th</sup> plant (vs \$1,641/ton current DOE Baseline)

# BP2 Project Tasks in Context of Process Flow Diagram





# BP2 Project Tasks in Context of Process Flow Diagram

*Task 4. Improve Algae Productivity & CO<sub>2</sub> Capture by Improved Bioreactors & Acclimation*

Novel Algae Cultivation System

*Task 5. Reduce Dewatering Energy Using Forward Osmosis*

Novel Dewatering Process

*Task 6. Increase Algal Biomass Value by Developing Animal Feed Products*

Animal Feed (\$100-1000/ton)

Hydrothermal Liquefaction

Biocrude Oil Upgrading



Drop-In Biofuel (\$200-500/ton)

Flue Gas Transportation via Sanitary Sewers

Municipal Wastewater for Nutrient Supply

Treated Wastewater

Concentrated Organics ↑ HTL-Aq (PHWW) ↓

Filtrate

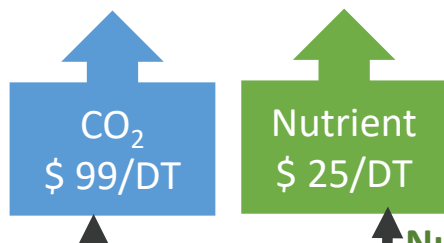
*Task 7. Reduce Cost of HTL Aq. Product Treatment via Membrane Conc. & Recycling*

# Techno-Economic Rationale: Integrating wastewater (WW) treatment can make algal animal feed cost-effective

Ponds/Inoculum:  
 2015 DOE Case \$1,359/DT  
 Proposed Case \$331/DT

Harvest & Dewater  
 \$82/DT  
 \$50/DT

Total Biomass Cost  
 \$1641 /DT  
 \$ 537 /DT



CO<sub>2</sub> credits

Nutrient removal credits



Cost Categories	2015 SOT DOE Baseline 8.5 g/m <sup>2</sup> /day	Proposed Case for BP2 25 g/m <sup>2</sup> /day
Ponds & Inoculum	\$ 1,359	\$ 331
CO <sub>2</sub> Supply	\$ 99	\$ 99
Dewatering Operations	\$ 82	\$ 50
Nutrient Supply	\$ 25	\$ 25
Other Costs	\$ 76	\$ 32
<b>TOTAL Algae Biomass Prod</b>	<b>\$ 1,641 /DT</b>	<b>\$ 537 /DT</b>

## Revenue for Algal Biomass

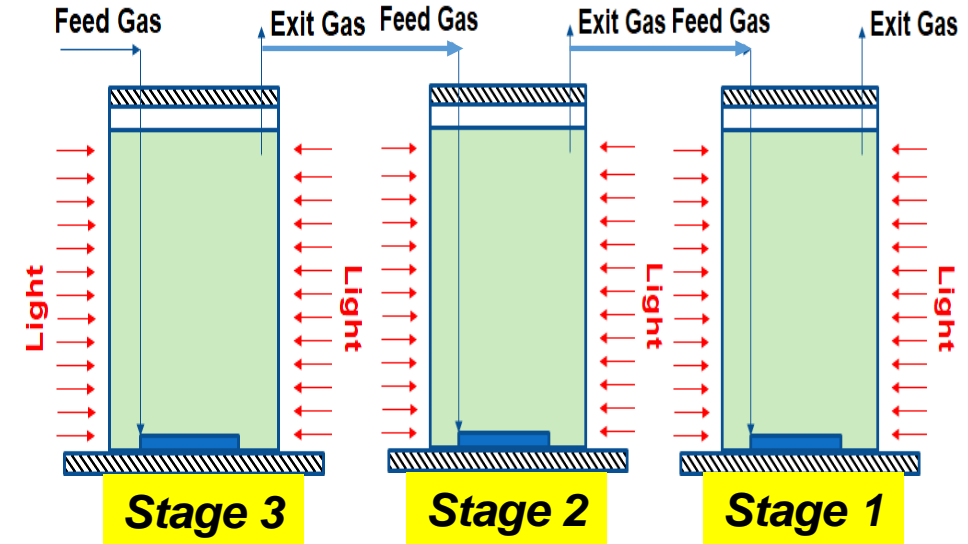
CO<sub>2</sub> Removal: \$ 0 - \$ 60 /DT  
 Nutrient Removal: \$ 380 - \$ 680 /DT  
 Wet Animal Feed: \$ 100 - \$ 300 /DT  
**\$ 480 - \$1,040 /DT**

*Animal feed revenue potential of >\$ 1000 / DT, but will likely require extra drying cost (\$330/DT)*

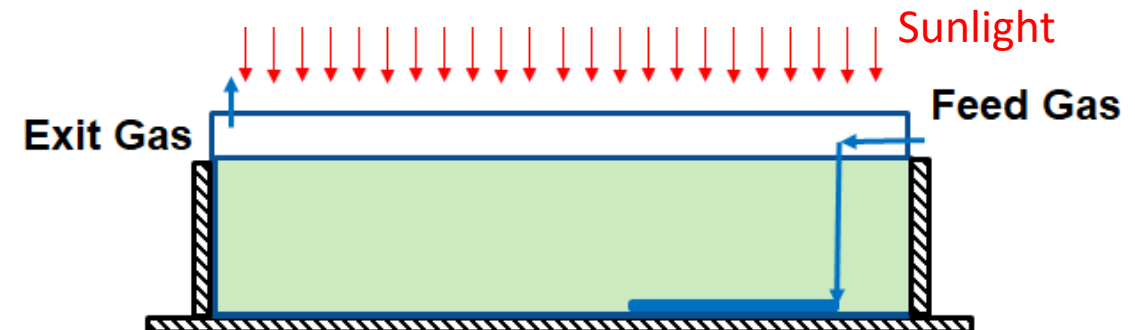
# Task 4- BP2 Algae Testing Plan Overview

- Transition from lab batch to continuous (w/liquid transfer)
- Transition from artificial lighting to sunlight (Greenhouse)
  - Quantify sunlight variations and impact on performance
- Greenhouse tests w/ simulated flue gas
  - 12% CO<sub>2</sub> + SO<sub>x</sub>, NO<sub>x</sub> & 5 heavy metals (Cu, Cr, Hg, As, Se)
- Investigate and optimize greenhouse cultivation operations
  - Algae concentration effects on productivity
  - Gas/liquid flow rates effect on CO<sub>2</sub> capture & productivity
  - Long term stability & performance in greenhouse
- Demonstrate weekly average productivity of 25 g/m<sup>2</sup>/day with 70% CO<sub>2</sub> capture simultaneously for a simulated Multi-Stage Continuous (MSC) reactor system

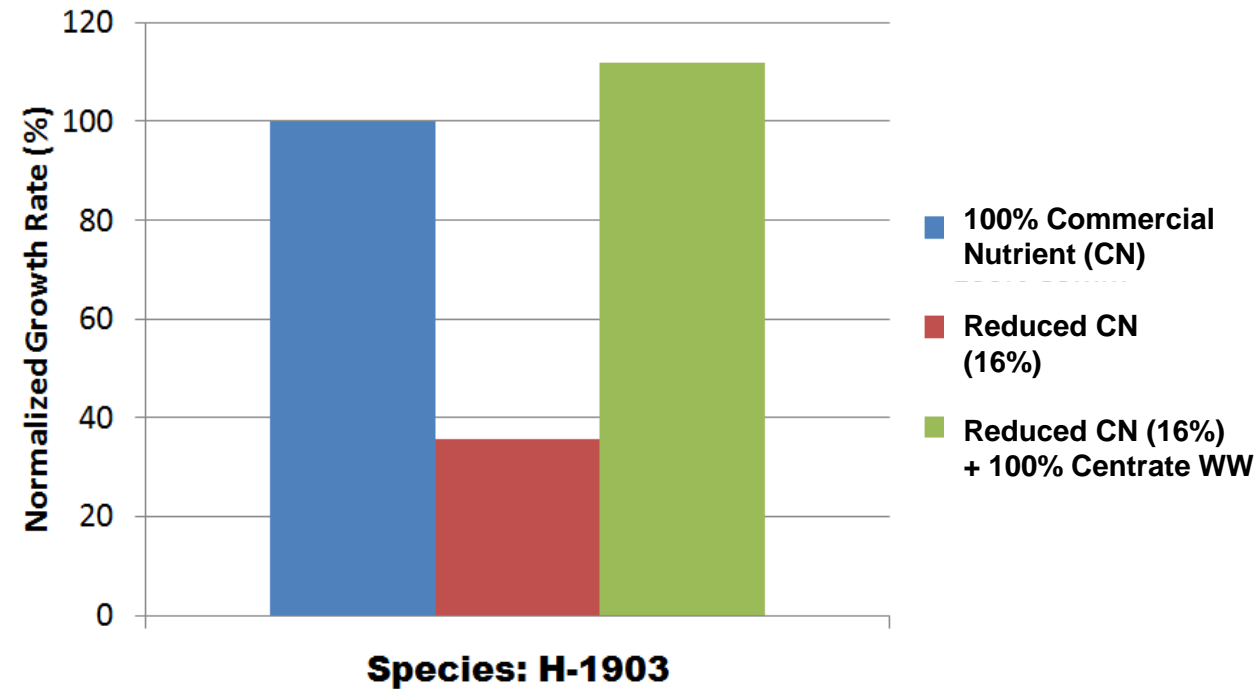
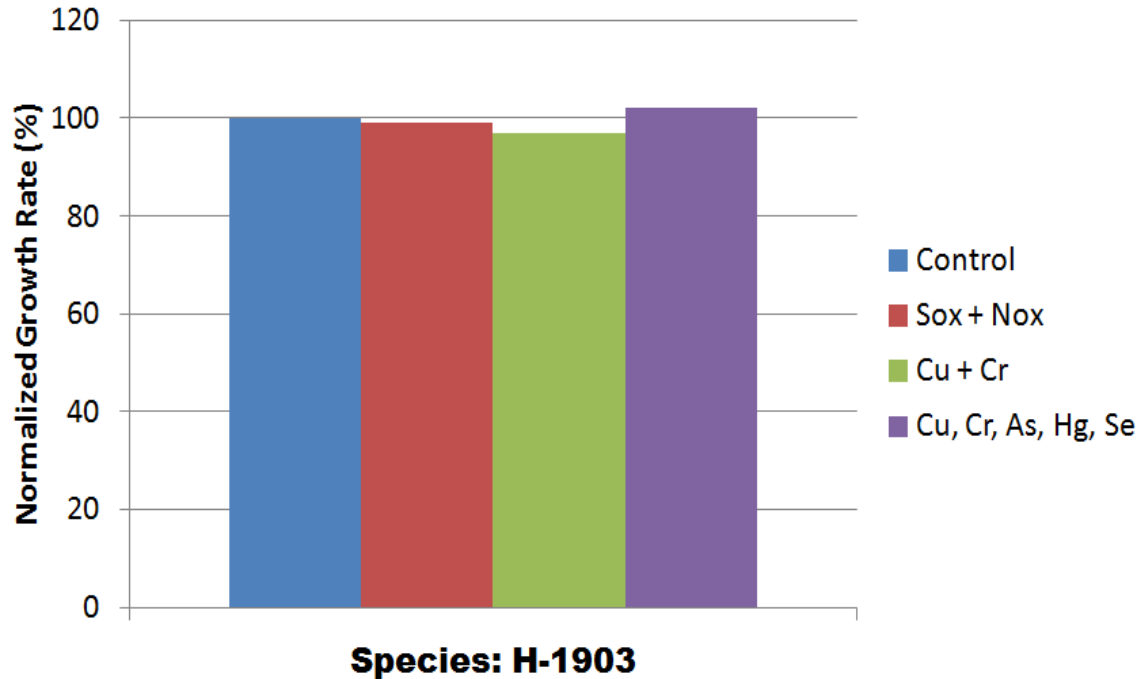
## Lab Side-Lit & Multi-Stage Continuous System



## Greenhouse Top-Lit (Sun) System



# Lab- Algae cultivation w/ simulated flue gas & WW nutrients

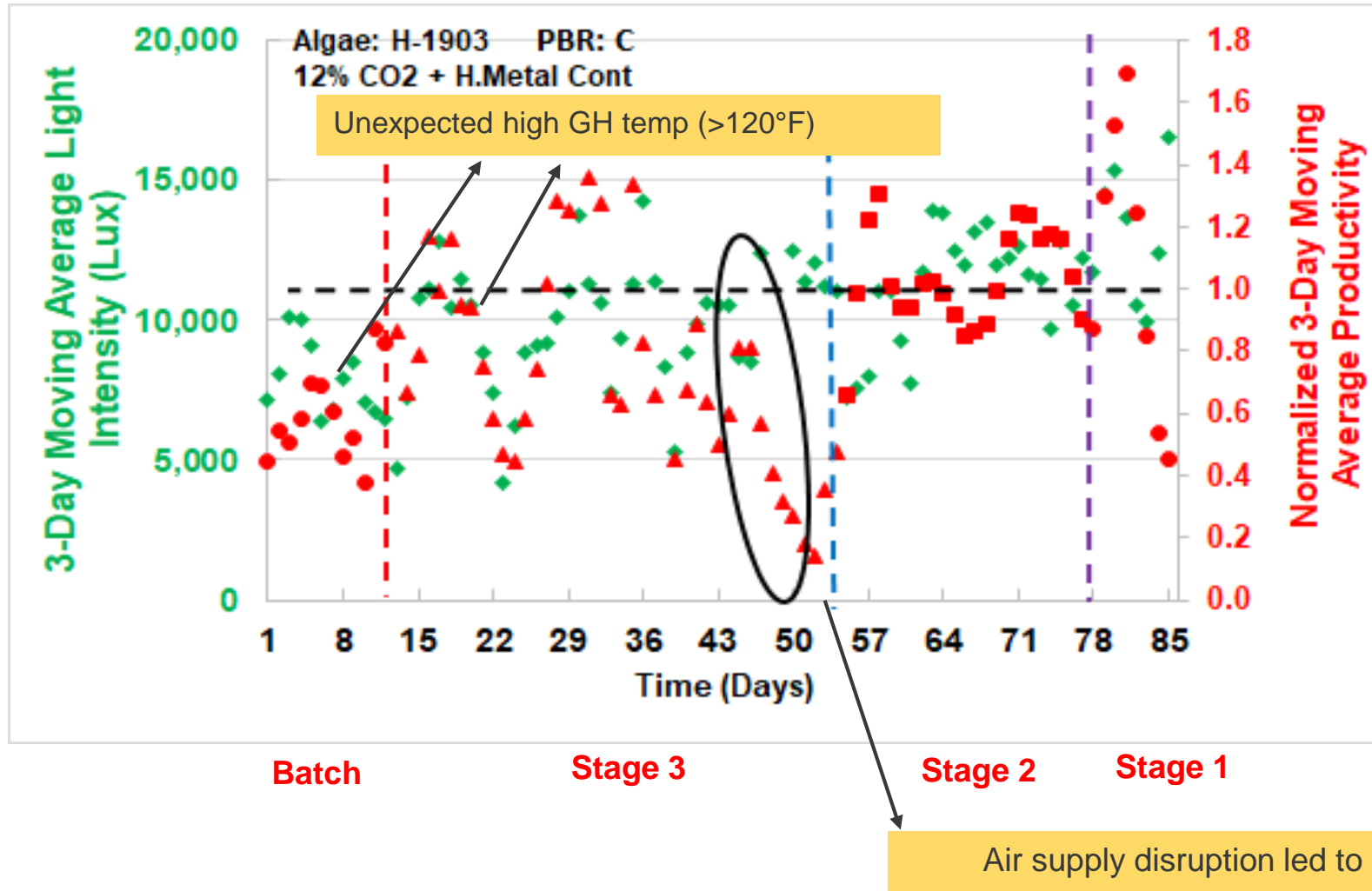


- **Algae tolerance to key post-FGD flue gas contaminants demonstrated**

- **Wastewater can beneficially replace purchased nutrients to reduce costs**



# Optimizing Long-term Greenhouse Operations

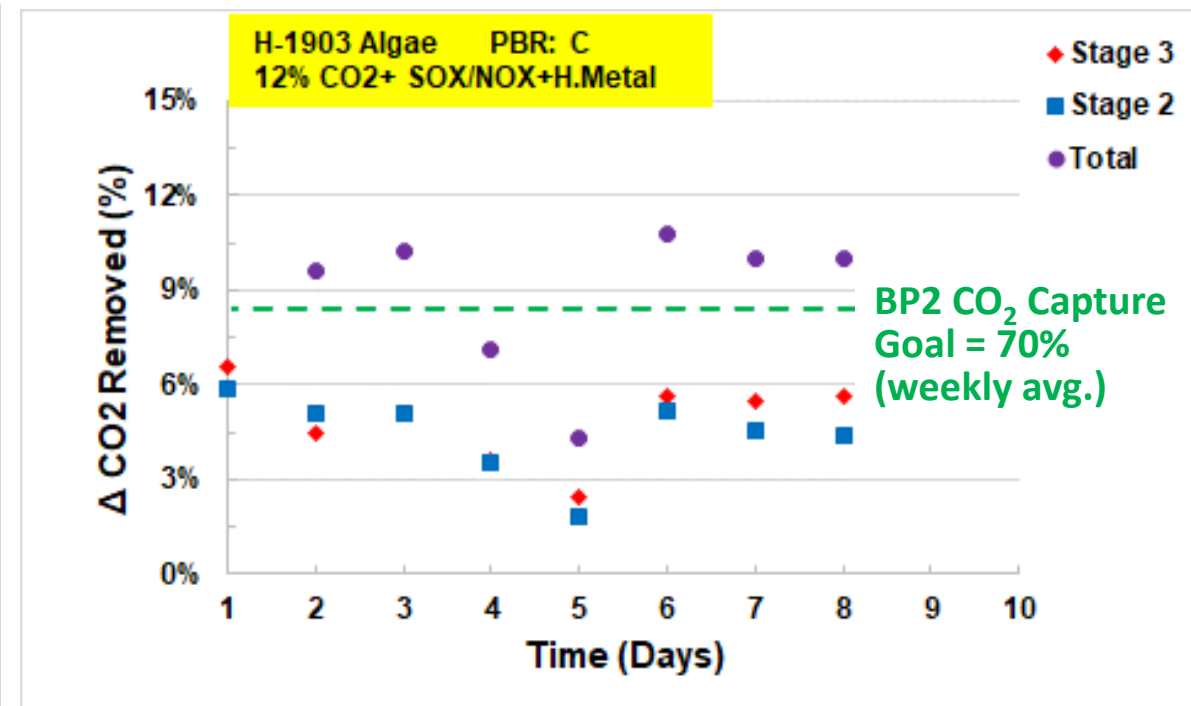
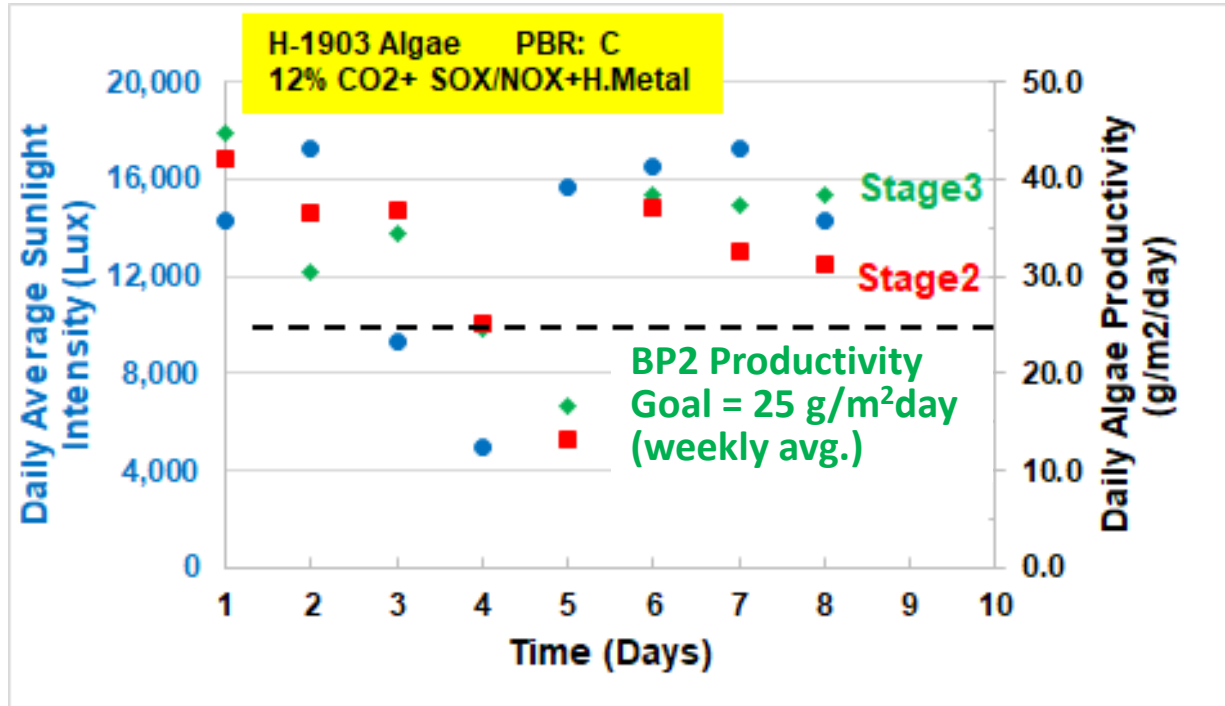


- Fluctuating light intensity results in large variations in algae growth (productivity) and CO<sub>2</sub> uptake
- Resilience of system demonstrated despite natural and abnormal fluctuations in greenhouse conditions



# Demonstration of CO<sub>2</sub> Capture and Productivity Goals

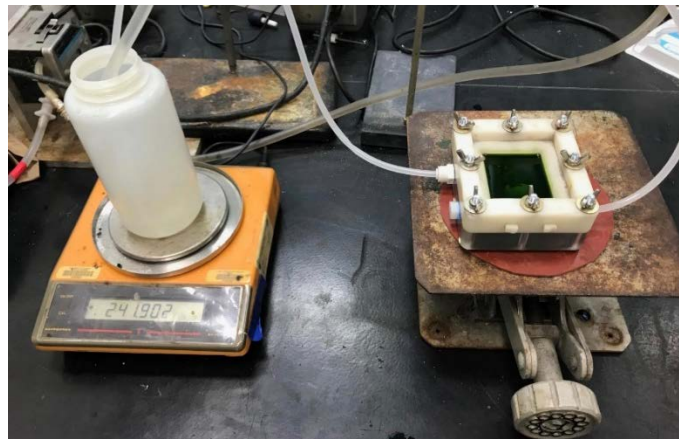
## Greenhouse Operation



BP2 algae cultivation targets met → Weekly average of 30 g/m<sup>2</sup>/day productivity achieved simultaneous with 74% CO<sub>2</sub> capture demonstrated for a 2-stage MSC system

# Task 5. Evaluate novel forward osmosis algae dewatering process

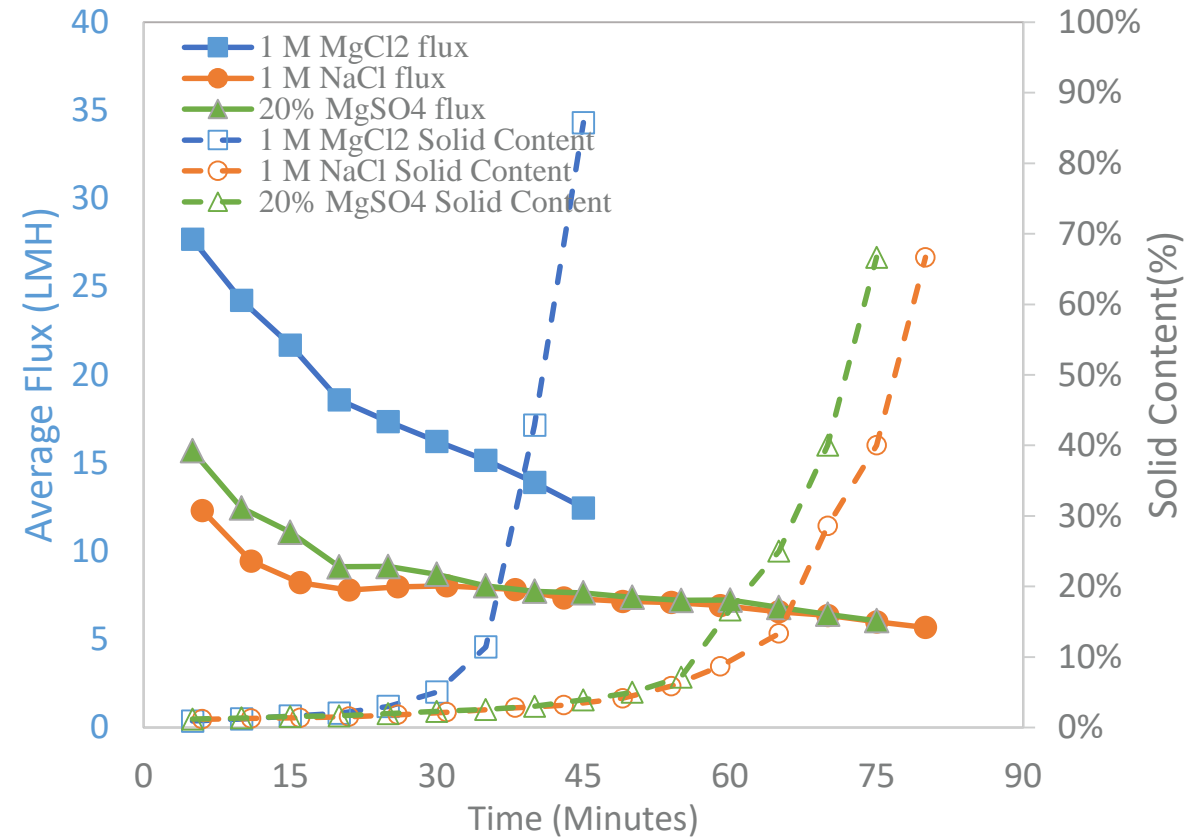
Forward osmosis open cell experiments with different draw solutions



Open Cell FO System



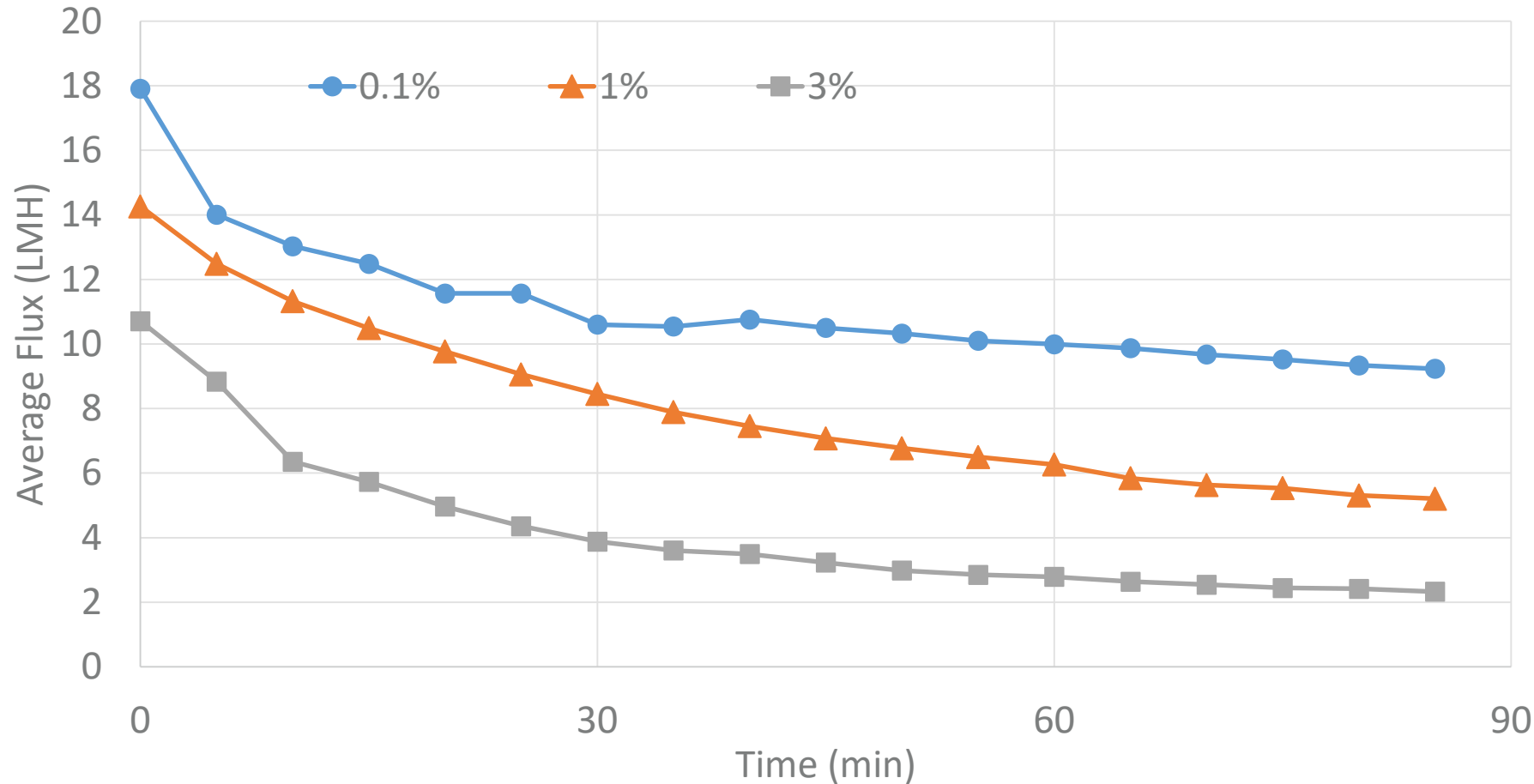
Dewatered Biomass  
(40% Solid Content)



- Bench-scale open cell forward osmosis system was developed to test algae dewatering
- Biomass dewatered to above 20% solid content without pre-treatment in reasonable time
- Dewatering efficiency: 1 M MgCl<sub>2</sub> > 20% MgSO<sub>4</sub> ~ 1 M NaCl

# Improving F.O. dewatering process for cost and energy inputs

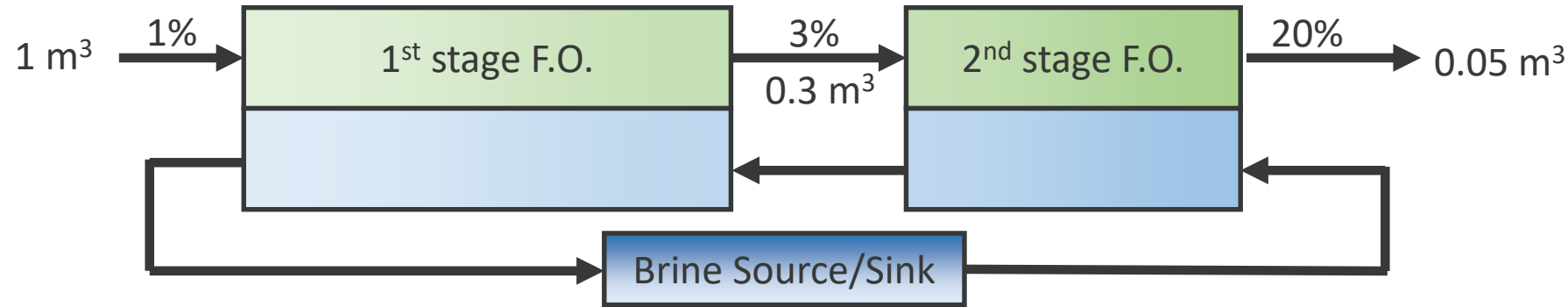
Effect of Feedstock Solids Content on Flux



- Forward osmosis dewatering efficiency drops as culture concentration increases



# Improving F.O. dewatering process energy inputs



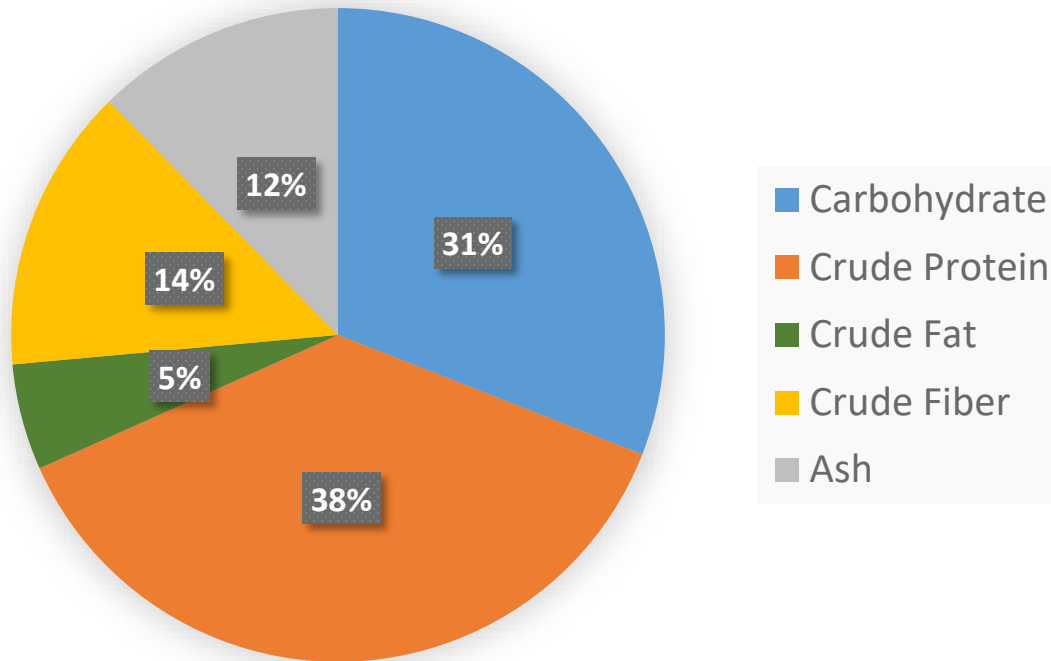
	Starting Solid (%)	Ending Solid (%)	Energy consumption (kWh/m3)
Settling Pond	0.1	1	-
Membrane	1	13	0.04
Centrifuge	13	20	1.35
Forward Osmosis 1 <sup>st</sup> Stage	1	3	0.26
Forward Osmosis 2 <sup>nd</sup> Stage	3	20	0.57

\* 2-stage F.O. process using natural brines or sea water can greatly reduce dewatering energy inputs

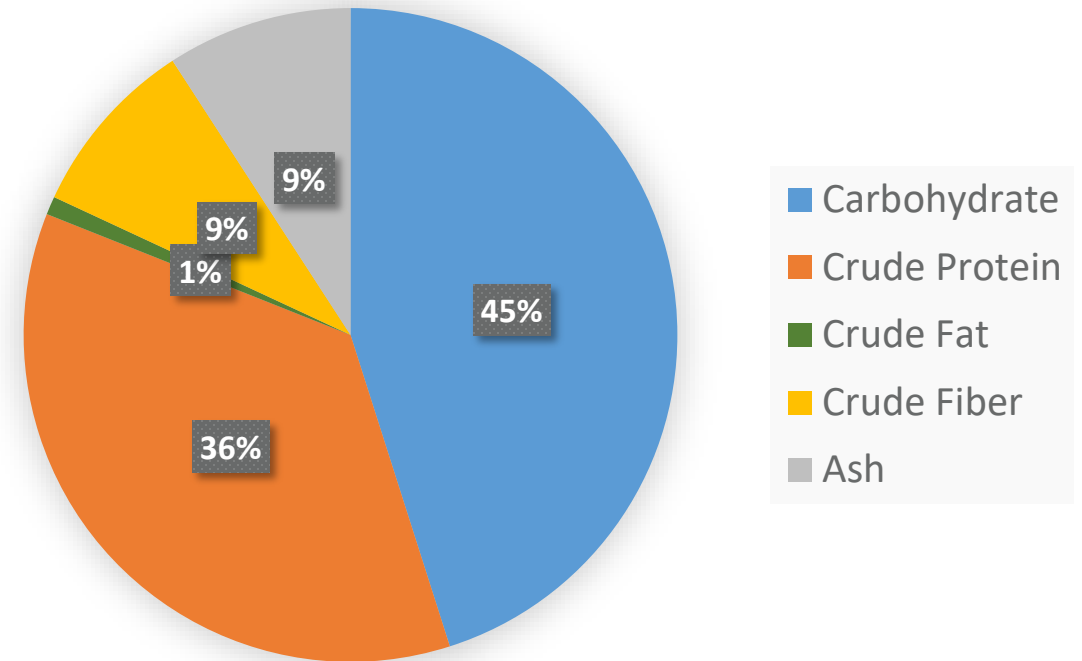
# Task 6. Characterize algal biomass for HTL & animal feed

Proximate analysis of flue gas fed algal biomass

H1903



H0322



- Both species are rich in protein and carbohydrates, low in fat, which is suitable for animal feeds

# Heavy metals in algae grown w/ flue gas contaminants

Compare with animal feed maximum tolerable level (MTL)

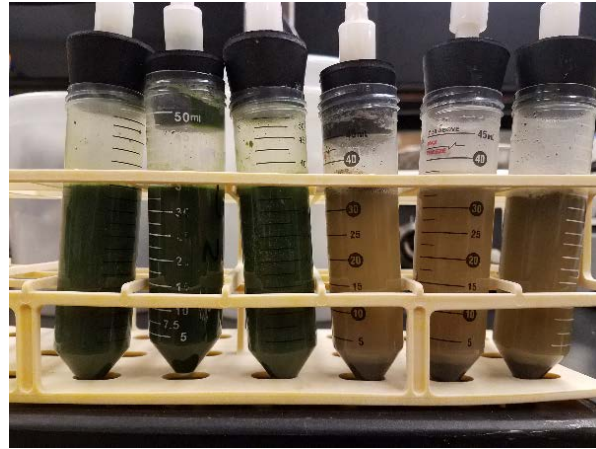
Minerals	H-1903 Cu, Cr, As, Hg, Se (ppm)	Poultry Feed MTL (ppm)	Swine Feed MTL (ppm)	Cattle Feed MTL (ppm)	Fish Feed MTL (ppm)
As	2.18	30	30	30	5
Cd	<1	10	10	10	10
Cr	1.16	100	100	100	3,000* as CrO
Co	<2	25	100	25	
Cu	46.6	250	250	40	100
Hg	0.5	1	2	2	1
Pb	<5	10	10	100	10
Ni	<5	250	250	100	50
Se	0.54	3	4	5	2
Zn	11.3	500	1000	500	250

- Algal biomass grown with flue gas contaminant meets most animal feed limits for metals and it can be blended with other feeds to mitigate any heavy metal concerns



# Cattle digestibility test with algal biomass

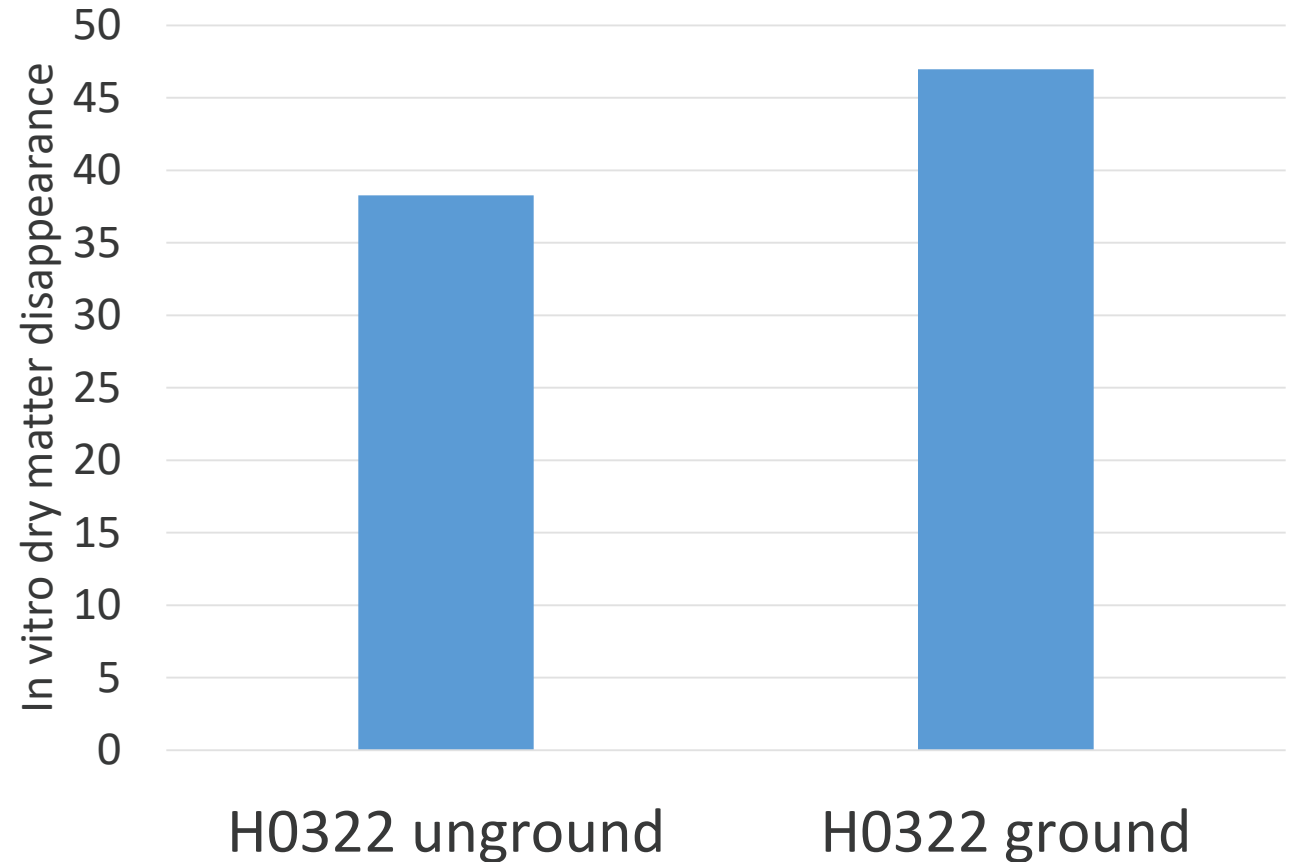
- **In vitro fermentation assay**
  - Rumen fluid from cannulated steer
  - Incubate samples for 24 hours



- **Results**

- Grinding with mortar and pestle increased In-vitro dry matter digestability (IVDMD)
- Looking into other biomass treatments to increase digestability
- Working to reduce run to run variations

## Preprocessing Effects on Digestability

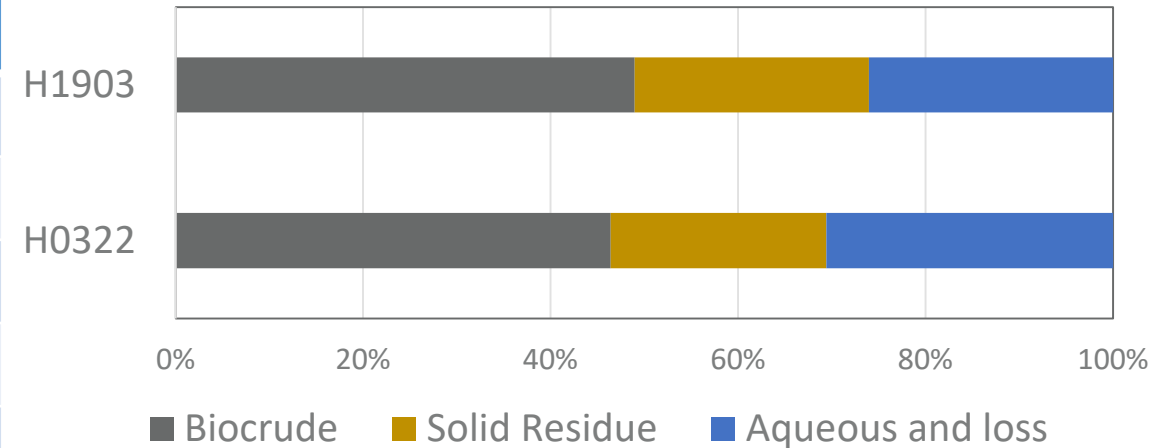


# Biomass elemental analysis and HTL Performance

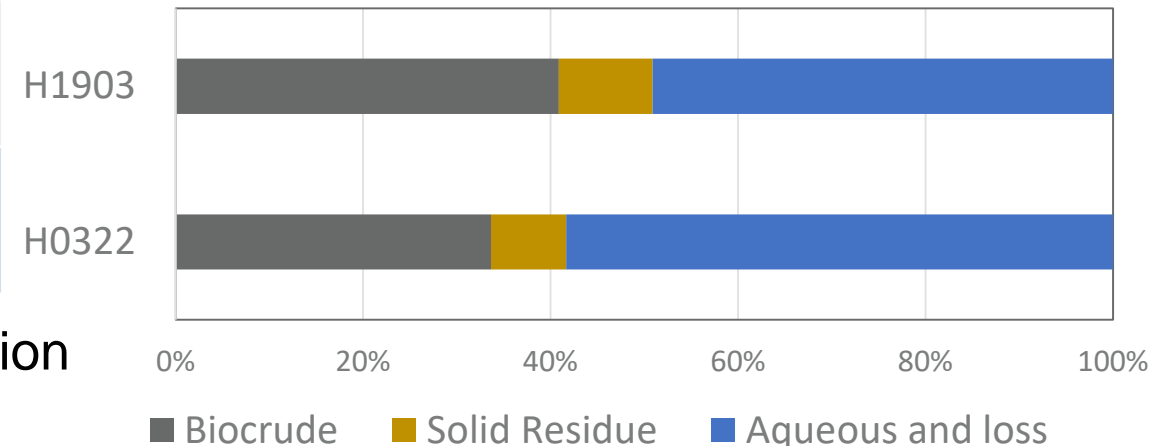
	H1903	H0322
C (% dw)	52.44	46.83
H (% dw)	7.54	7.11
O (% dw)	35.52	40.98
N (% dw)	4.50	5.10
Biomass Heating Value (MJ/kg)	22.15	18.66
HTL Biocrude oil Fraction	0.347	0.312
HTL Biocrude oil HHV (MJ/kg)	35.1	34.8

- H1903 biomass was preferable for biocrude production
- Most of N is distributed to HTL aqueous product

Carbon Distribution in HTL Products

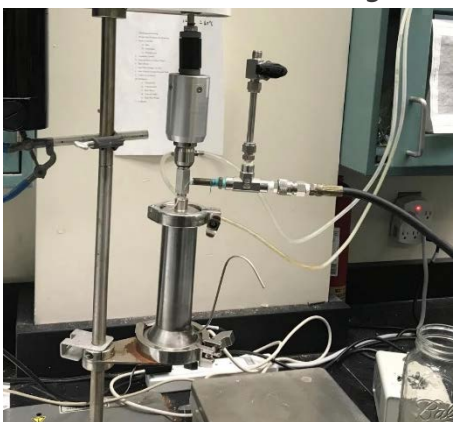
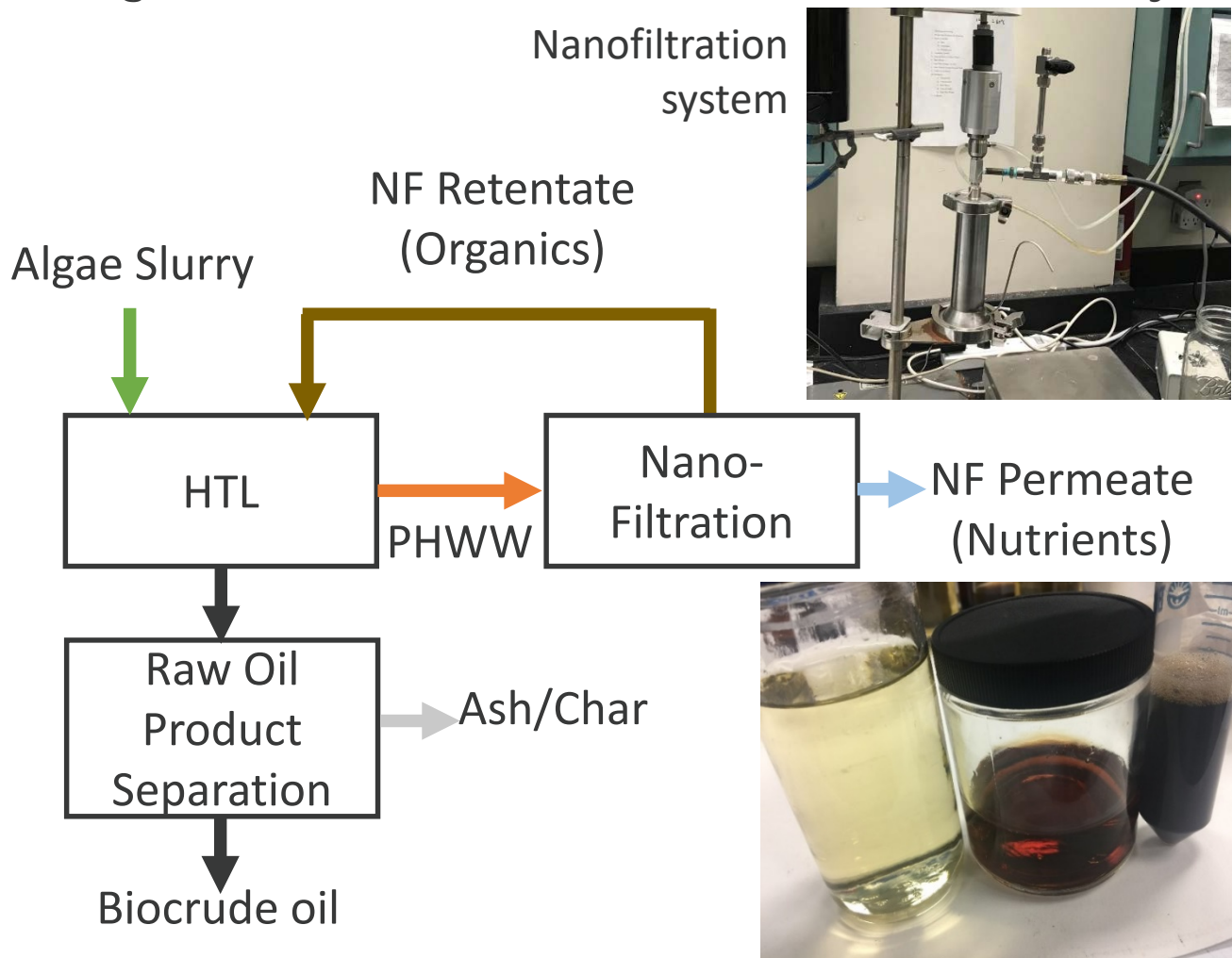


Nitrogen Distribution in HTL Products

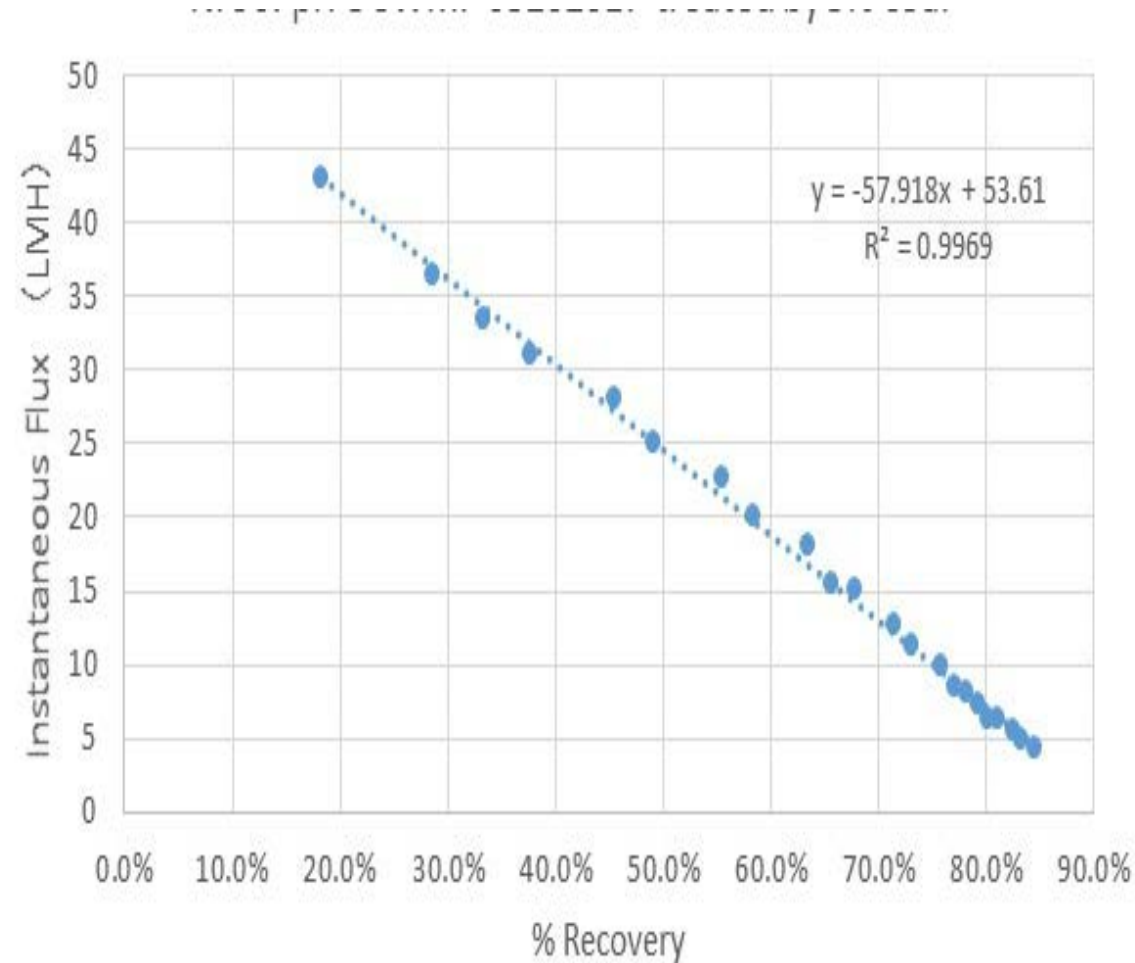


# Task 7. Demonstrate ability to concentrate & recycle HTL aqueous phase (PHWW)

Integration of HTL with nanofiltration for carbon recycle



Permeate PHWW Retentate



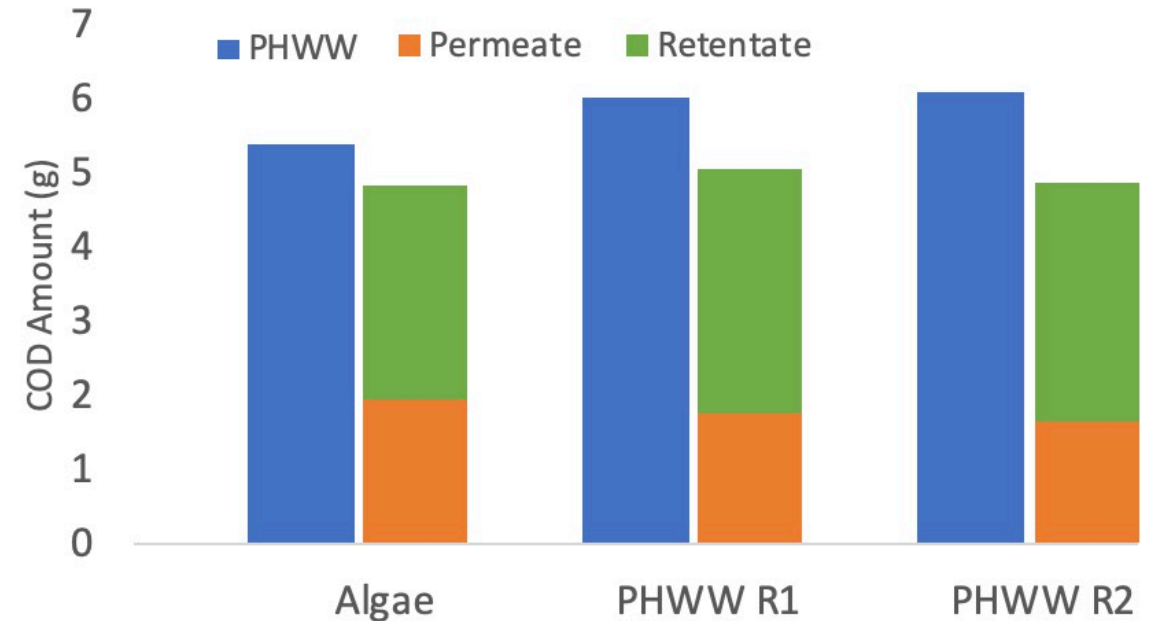


# Effect of recycling PHWW on biocrude yield & quality

	Algae Only	Algae + Run 1 Retentate (20%)	Algae + Run 2 Retentate (20%)
Biocrude Oil Yield Fraction	0.349	0.368	0.371
C (%)	70.64	73.74	73.42
H (%)	8.78	9.38	9.12
N (%)	5.63	5.59	5.72
O (%)	14.95	11.29	11.74
HHV (MJ/kg oil)	33.7	36.3	35.7

- 6% increase in biocrude yield w/ PHWW recycle
- Small N increase in the biocrude oil

**Organics Distribution (Measured as COD)**



- ~60% of PHWW organics captured in NF retentate
- Significant N also captured in NF retentate (~50%)
  - May not be desirable → Zeolite treatment can mitigate

# TEA: Integrating WW treatment can make algal biofuels cost-effective

Algal biomass for fuel

Algal Biomass Supply Cost:  
\$15.15/gge (\$1,641/DT)

Algal Biomass Supply Cost:  
\$5.25/gge (\$537/DT)



Hydrothermal Liquefaction  
\$1.18/gge



Bio-oil Upgrade  
\$0.44/gge



Aqueous Product Treatment  
**Catalytic Hydrothermal Gasification**  
\$1.54/gge  
**Nanofiltration**  
\$0.28/gge



Biofuel Production Cost	DOE Baseline (2015 case)	Proposed case for BP2
Algal Biomass	\$15.15 /gge	\$ 5.25/gge
Hydrothermal Liquefaction	\$ 1.18/gge	\$ 1.18/gge
Bio-oil Upgrade	\$ 0.44/gge	\$ 0.44/gge
Aqueous post treatment	\$ 1.54/gge	\$ 0.28/gge
Balance of plant	\$ 0.29/gge	\$ 0.29/gge
<b>TOTAL Biofuel Cost</b>	<b>\$ 18.60/gge</b>	<b>\$ 7.44/gge</b>

### Revenue for Algal Biofuels

CO<sub>2</sub> Removal: \$ 0 - \$ 0.6 /gge  
 Nutrient Removal: \$ 3.7 - \$ 7.2 /gge  
 Fuel Selling Price: \$ 2.0 - \$ 3.5 /gge  


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**\$ 5.7 - \$ 11.3/gge**

# Project Milestones for Budget Period 2



Budget Period	Task #	Milestone #	Milestone Description	Planned Completion Date	Actual Completion Date	Comments
2	4	T4.1	Single stage test of MSC representation with >70% CO <sub>2</sub> capture and >25 g/m <sup>2</sup> /d	9/30/2019	7/30/2019	Simulated Multi-stage CO <sub>2</sub> capture demonstrated >70% w/ single-stage tests
2	5	T5.1	Dewater algal biomass >15% solid content through forward osmosis using <1.35 kwh/m <sup>3</sup>	9/30/2019		In-Progress- >20% solids content shown w/ min. energy input of 0.83 kWh/m <sup>3</sup> when seawater available
2	6	T6.1	Characterize algal species that biomass heating value > 18MJ/kg and protein content > 30%	3/31/2019	3/20/2019	Completed- 2 species sample analyzed
2	6	T6.2	Demonstrate a minimum in vitro dry matter disappearance of 40% for algal strains digested in rumen fluid	9/30/2019		In-Progress- H0322 ground sample had >45% dry matter disappearance, but the result was not yet repeated
2	7	T7.1	Recycle >50% of carbon from HTL aqueous and increase biocrude oil yield by > 5%	9/30/2019	6/30/2019	Completed- ~60% of carbon from HTL-aq recycled to enhance oil by 5%

# Project Success Criteria for Each Budget Period



Decision Point	Date	Success Criteria
G/N-1 Go/No-Go Budget Period 1	9/30/2018	Algal Productivity > 25 g/m <sup>2</sup> /d (weekly average) with Simulated Flue gas containing 12% CO <sub>2</sub> , SOX, NOX and representative levels of heavy metals Hg, Se, As, Cu and Cr
G/N-2 Go/No-Go Budget Period 2	9/30/2019	Algal Productivity > 25 g/m <sup>2</sup> /d (weekly average) and >70% CO <sub>2</sub> capture with Simulated Flue gas containing 12% CO <sub>2</sub> , SOX, NOX and representative levels of heavy metals Hg, Se, As, Cu and Cr
G/N-3 Go/No-Go Budget Period 3	9/30/2020	Integrated Application of Project Technologies w/ Projected Cost of Algal Biomass < \$470 /dry ton



# Questions and Comments...

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