

Low-Cost and Recyclable Oxygen Carrier and Novel Process for Chemical Looping Combustion DE-FE0031534



By

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12/01/2017 to 11/30/2020







Presentation Overview

- Project Overview
- Background on existing CLC projects at UND/Envergex LLC
- Project Objectives
- Technical Approach
- Scope of Work
- Questions/Discussion

Project Overview

Overall Goal: Demonstrate transformational technology that overcomes two key CLC technology gaps:

- high cost of OC replacement/loss
- incomplete fuel conversion, resulting in reduced CO₂ capture efficiency and an oxygen demand downstream of the CLC reducer reactor.

Funding: Department of Energy \$1,500,000; Cost-share - \$375,000

Project Participants:

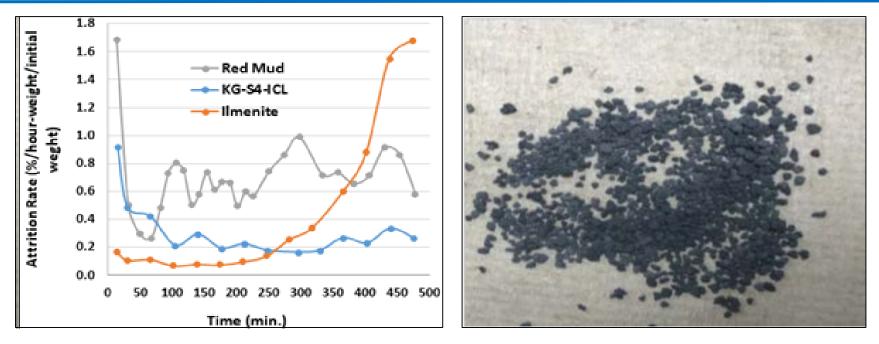
- 1. University of North Dakota Institute for Energy Studies (Lead)
- 2. Envergex LLC
- 3. Barr Engineering
- 4. Microbeam Technologies, Inc. (pending)
- 5. Carbontec Energy Corporation

Existing Projects

- **1. Attrition Evaluation**
- 2. Char Stripping

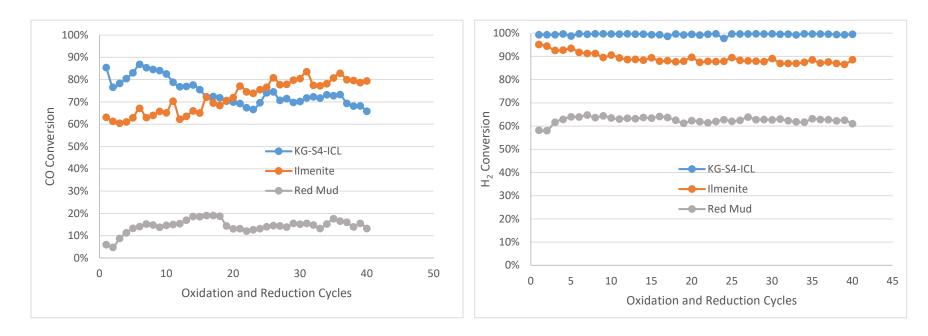
3. Spout – Fluid Bed Development

- Developing a novel reactor geometry to be used for chemical looping combustion
- Developing a modeling tool co-currently with the reactor geometry to facilitate scale up



Unique oxygen carrier composition and manufacturing platform:

- Main component enriched iron oxide powder: abundant and low-cost domestic production
- Blending in a small proportion of low-cost additives to avoid agglomeration tendency of pure iron oxide
- Preliminary attrition results promising

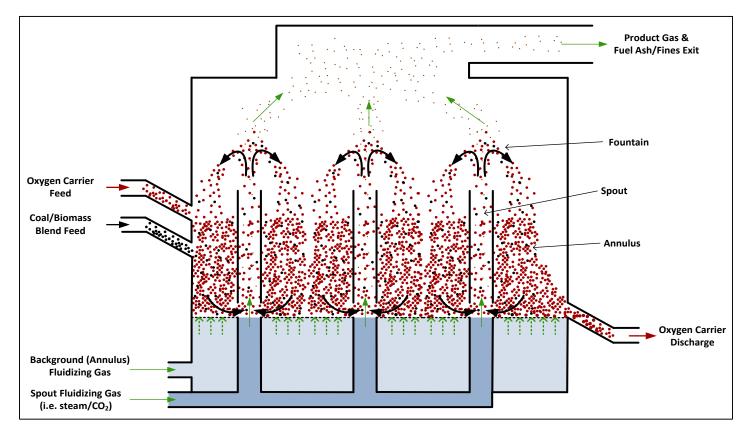


Tested in laboratory scale reactor (High Temperature Redox Attrition Test Unit):

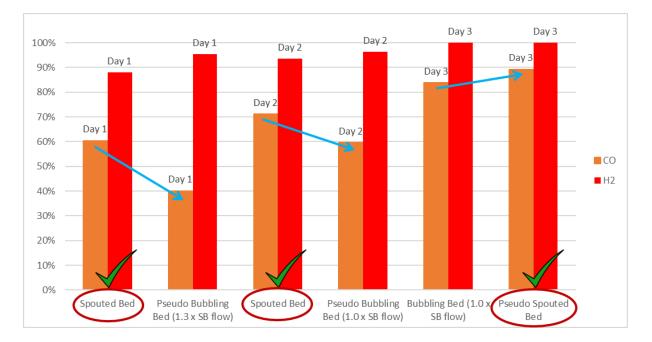
- Hydrogen conversion very good
- CO conversion also promising

SPOUT FLUID-BED REDUCER DESIGN:

- High velocity in draft tube (turbulent to transport regime)
- Low velocity in annulus (low to minimum fluidization velocity)
 - Annulus operates like a "moving bed"
 - Better solid-gas interactions

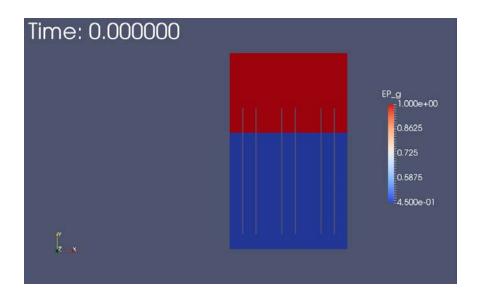


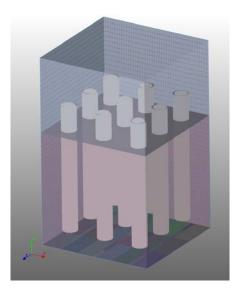


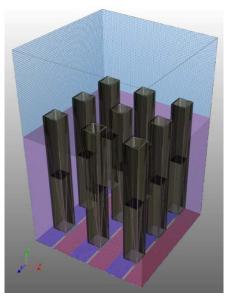


> 3-D MFiX Models – Hydrodynamics

- Cylindrical draft tubes replaced with rectangular → Simplifies modeling
- Use to investigate flow patterns of OC
- 3-D isothermal case with variable material inlet and outlet mass flows
- Implementing custom solver to run simulations more robustly

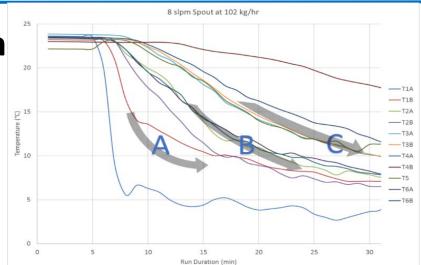


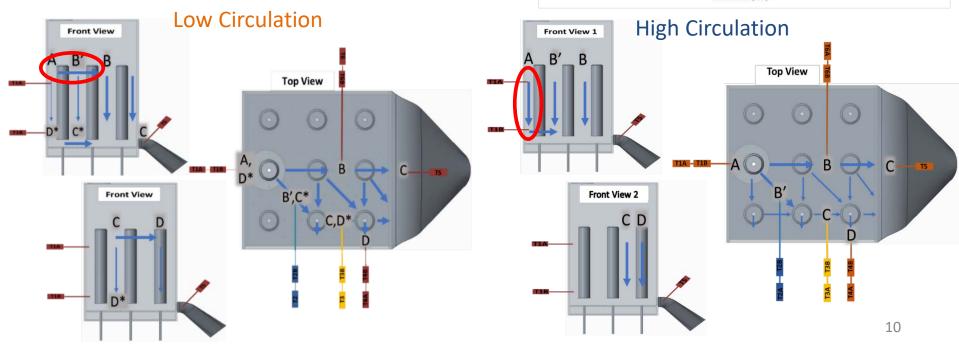




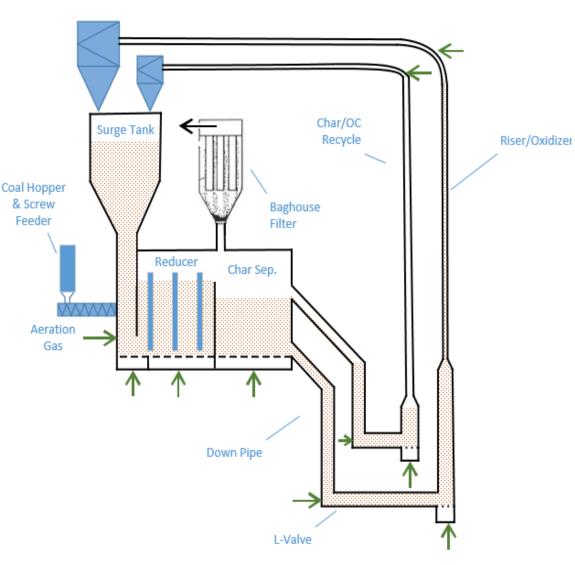
Residence Time and Circulation

- OC cooled to < 5°C
- Thermocouples used to monitor effect of circulation and feed rate
- High Circulation vs Low Circulation
- Compare experimental and simulation data





- Use unique hydrodynamics available with the SFB reducer design
 - Thermodynamics limits combination of fuel gas conversion and deep OC reduction
 - Counter-current operation of the annulus in the SFB can help to improve on this limit
- Incorporate the PCS carbon stripper technology
- Goal: 90% CCR with no/minimal reducer exhaust oxygen demand



Project Objectives

Specific Objectives:

- 1. Demonstrate novel OC manufacturing platform: high performance of "engineered" OCs, but with cost structure of natural ores
- 2. Identify OC phase transformations and interactions with coal impurities that could impact OC/process performance and OC recyclability; identify mitigation strategies
- 3. Test a novel combination of CLC components at the 10 kW_{th} -scale using existing projects at UND and Envergex LLC.
- 4. Perform economic assessment to demonstrate progress towards DOE cost of CO_2 capture and cost of electricity targets

Scope of Work

- Task 1 Project Management and Planning
- Task 2 Laboratory-scale OC Manufacturing & Assessment
- Task 3 Modeling and Laboratory-scale Evaluation of OC Performance with Coal
- Task 4 10 kW_{th} Integrated System Installation
- Task 5 Scaled-up OC Manufacturing
- Task 6 10 kW_{th} Testing
- Task 7 Process Design and Techno-Economic Analysis



Subtask 2.1 – OC Manufacturing

- ~40 unique OC formulations
- Composition, binder loading, particle size, granulation method, curing

Subtask 2.2 – OC Characterization and Performance Testing

- Determine physical/chemical characteristics before/after exposure to CLC tests
- Perform CLC testing: reducing gas conversions, impact of sulfur, attrition, agglomeration
- Parameters to include: temperature, gas/solid contact time, reducing gas composition, jet velocity
- Down-select to 2 OCs based on testing

Subtask 2.3 – Longer-term Operation and Recyclability Evaluation

- **~500 redox cycles**; Evaluate long term performance
- Collect fines generated and evaluate CLC performance/characteristics of reformulated fines compared to fresh OC

Task 3 Overview

Subtask 3.1 – Fluidized Bed Testing with Coal

- Use coal as reductant instead of reducing gases
- Parametric and longer-term testing
- Down-select to 1 OC formulation

Subtask 3.2 – Experimental Evaluation of OC/Coal Ash Interactions

- TGA-DSC: Identify zones of phase transformations/reactions of OC/coal ash; characterization to determine OC transformations
- Temperature, contact time, gas phase composition, ash type/composition

Subtask 3.3 – Thermochemical Equilibrium Modeling

- HSC Chemistry 9.0: model reactions of OC with coal ash
- Investigate agglomeration potential using viscosity models
- Develop mitigation strategies to minimize detrimental impacts

Subtask 3.4 – OC Fines Separation and Recyclability

• Tests to identify impact of coal impurities on OC recyclability

Tasks 4-6 Overview

Task 4 – 10 kW_{th} System Installation

- Leverage existing and to-be-constructed equipment from existing projects
- SFB reducer, PCS carbon stripper, Novel process configuration
- Circulating CLC system

Task 5 – Scaled-up OC Manufacturing

- ~1000 kg of down-selected OC formulation
- Evaluate physical/chemical characteristics to compare to lab quantities

Task 6 – 10 kW_{th} Testing

- Reducer/oxidizer temperature, OC residence time
- Reducer coal/char residence time
- OC/Coal ratio
- ~100 hours of testing at optimized conditions for two coal types

Task 7 Overview

Task 7 – Process Design and Techno-Economic Assessment

- Benchmark: NETL's Reference Plant Designs and Sensitivity Studies (Stevens et al 2014)
- Process modeling using Aspen Plus®
- Determine economic metrics
- Led by qualified 3rd party A&E Firm Barr Engineering Company

Stevens, R. et al., 2014: "Guidance for NETL's Oxy-combustion R&D Program: Chemical Looping Combustion Reference Plant Designs and Sensitivity Studies," DOE-NETL Report 2014/1643

Project Schedule

			2017	2017 2018										2019						2020							
Task/Subtask/Milestone Description	Start	End	11 12	1 2	2 3	4	5 6		89	10	11 1	12	1 2	3	4 5	1 1	7 8	91	10 11	1 12	1	2 3		5 6		78	9 10
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Subtask 2.2 - OC Characterization and Testing		7 05/31/18					_				1																
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Task 3 - Modeling and Laboratory-scale Evaluation of OC Performance with Coal	09/01/18	8 07/31/19																	T								
Subtask 3.1 - Fluidized Bed Testing	09/01/18	3 01/31/19	1																								
Subtask 3.2 - TGA Testing	01/01/19	9 03/31/19	1							ļ	1																
Subtask 3.3 - Thermodynamic Modeling	03/01/19	9 04/30/19	1								1																
Subtask 3.4 - OC Fines Separation and Recylability	04/01/19	9 07/31/19	1							ļ	1																
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Task 7 - Process Design and Technical and Economic Analysis	07/01/20	0 10/31/20								Т									Τ								
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Note: Actual Start date January 18, 2018

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Questions/Discussions

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