

# Amine-Appended Metal-Organic Frameworks as Switch-Like Adsorbents for Energy-Efficient Carbon Capture

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# Project Overview

## Funding

- Total project funding
  - DoE share: \$7.4M
  - Cost share: \$755k

## Overall Project Performance Dates

- Project start date: 8/1/2017
- Industrial partners start date: 8/1/2018
- Project end date: 7/31/2021

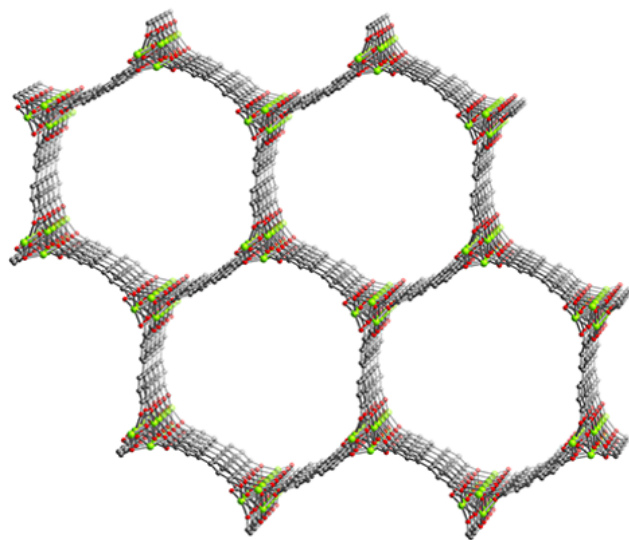
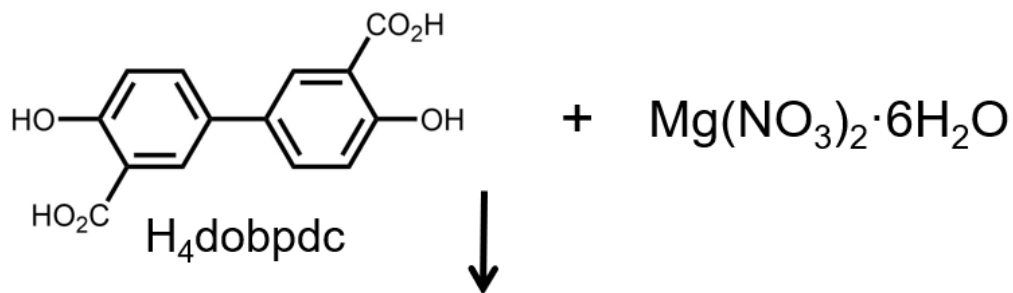
## Project Participants

- PI: Jeffrey Neaton (LBNL)
- Co-PI: Jeffrey Long (LBNL)
- Co-PI: Maciej Haranczyk (LBNL)
- Mosaic Materials (MOF production)
- Inventys (System development)
- Electricore (System development)
- CCSI<sup>2</sup> (Process modeling – unfunded)

## Overall Project Objectives

Development of a transformational technology based upon a diamine-appended MOF for post-combustion CO<sub>2</sub> capture at a coal power plant

# Technology Background: MOFs for CO<sub>2</sub> Capture

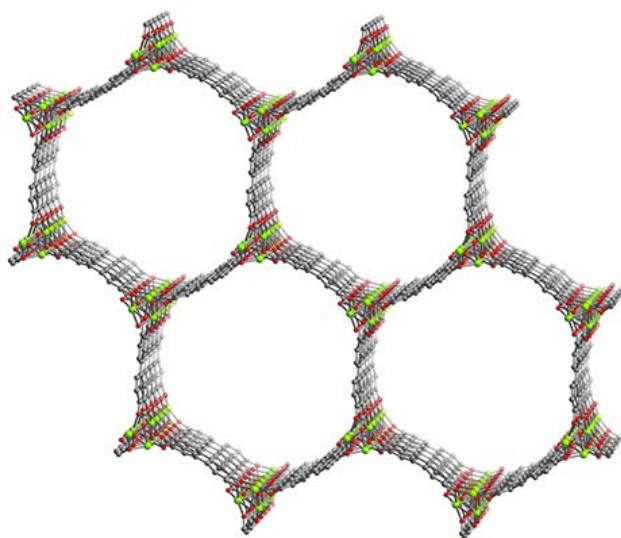
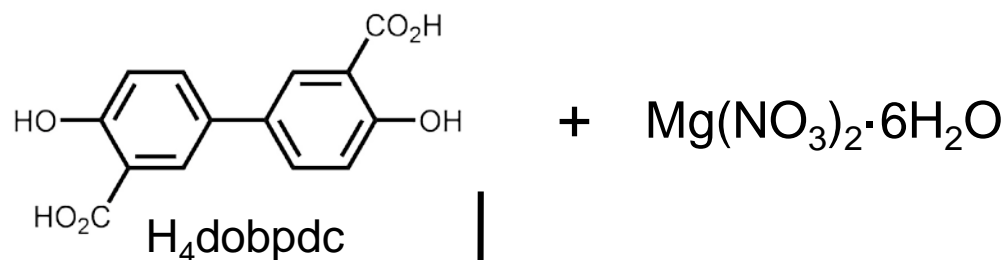


**Mg<sub>2</sub>(dobpdc)**

- MOF channels have a diameter of 18 Å and are lined with open Mg<sup>2+</sup> sites
- Dangling amines coat periphery of the channel leaving space for rapid CO<sub>2</sub> diffusion

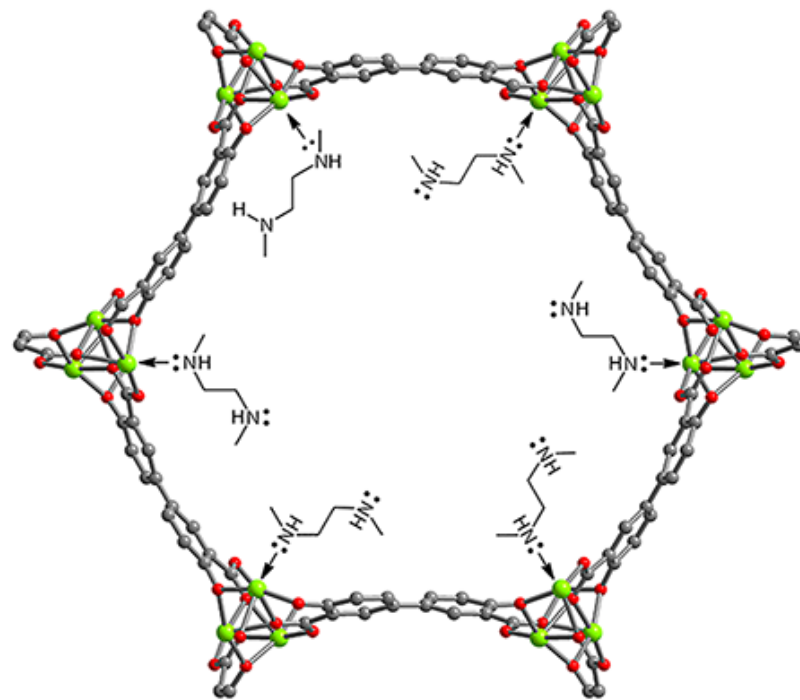
McDonald, Lee, Mason, Wiers, Hong, Long *J. Am. Chem. Soc.* **2012**, 134, 7056

# Technology Background: MOFs for CO<sub>2</sub> Capture



**Mg<sub>2</sub>(dobpdc)**

mmen

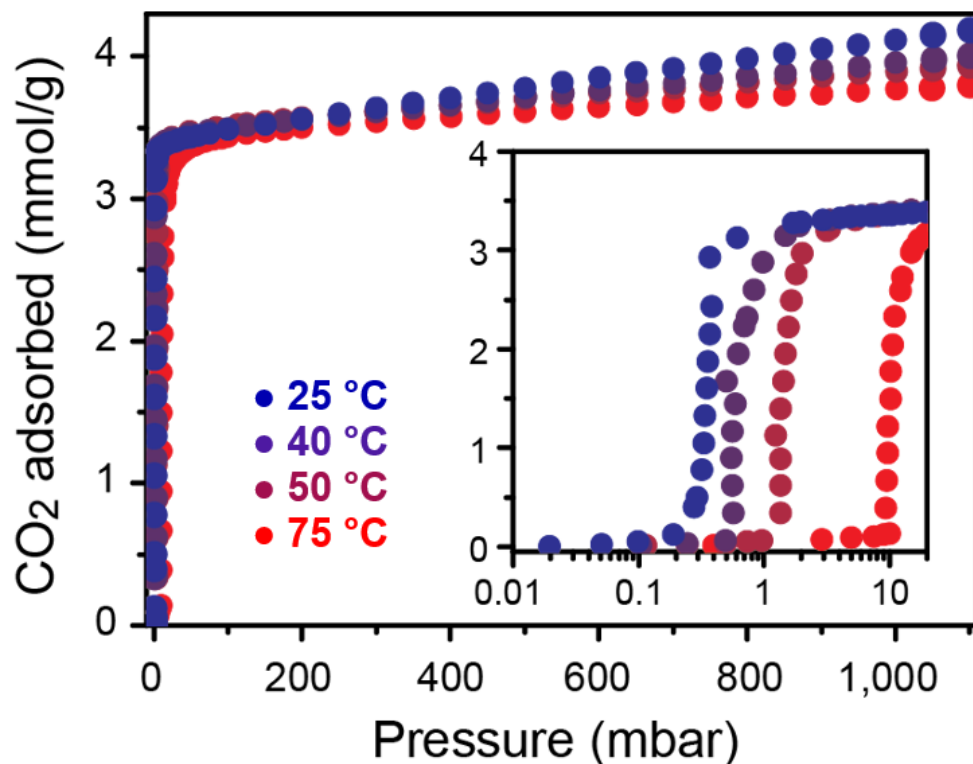


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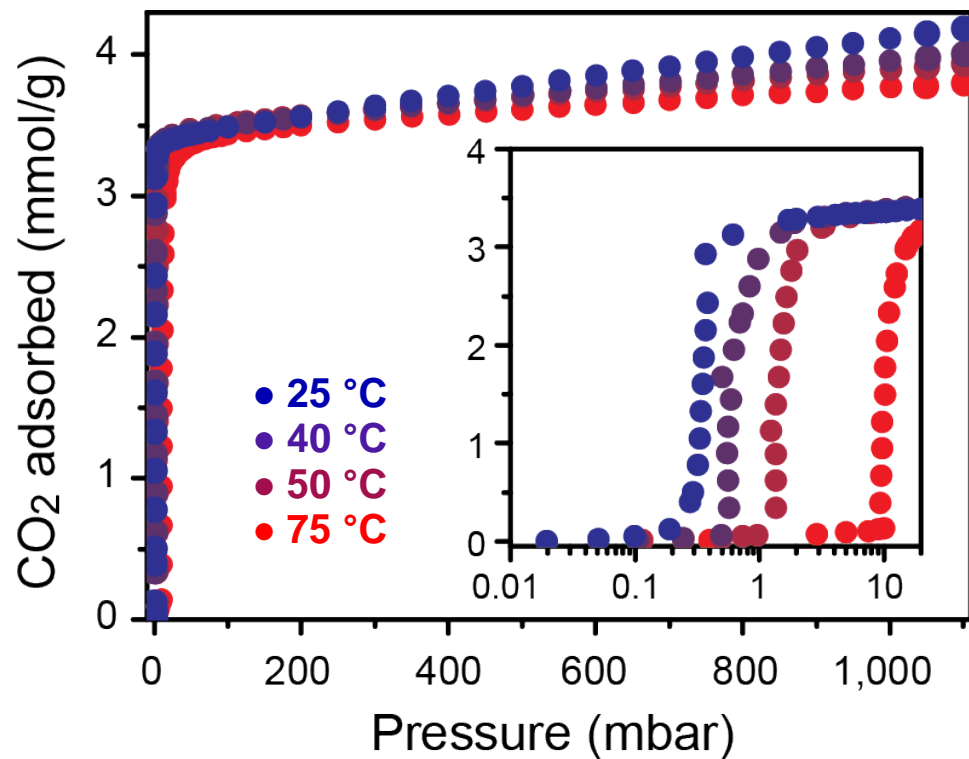
# Step-Shaped Isotherms via Cooperative CO<sub>2</sub> Binding



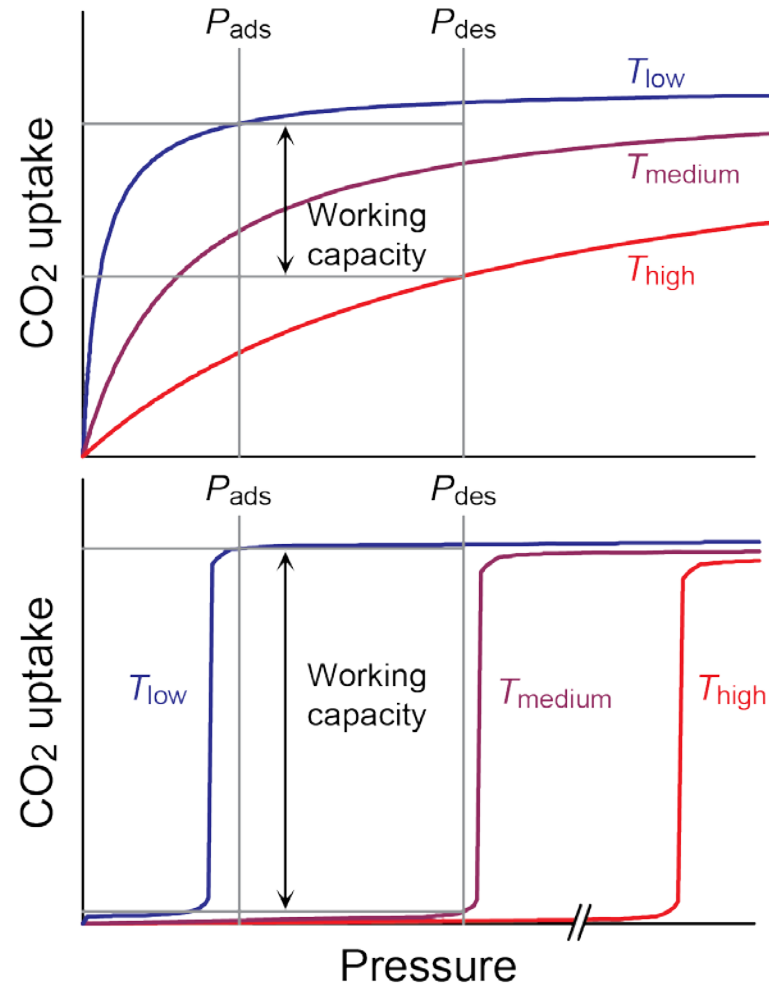
- Very little hysteresis upon desorption of CO<sub>2</sub>
- Step shifts rapidly to higher pressure with increasing temperature

McDonald, Mason, Kong, Bloch, Gygi, Dani, Crocellà, Giordano, Odoh, Drisdell, Vlasisavljevich, Dzubak, Poloni, Schnell, Planas, Lee, Pascal, Prendergast, Neaton, Smit, Kortright, Gagliardi, Bordiga, Reimer, Long *Nature* **2015**, 519, 303

# Step-Shaped Isotherms via Cooperative CO<sub>2</sub> Binding

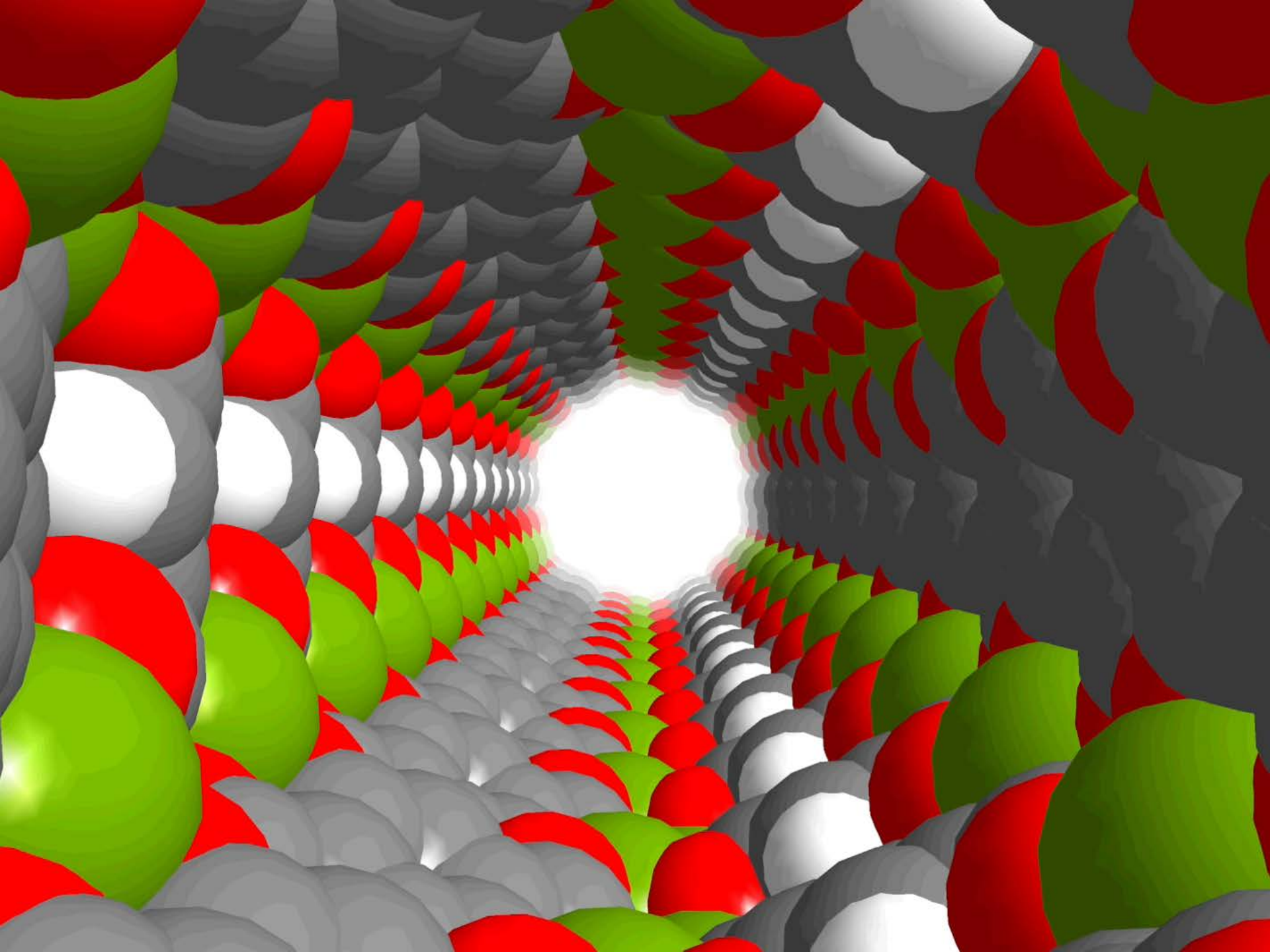


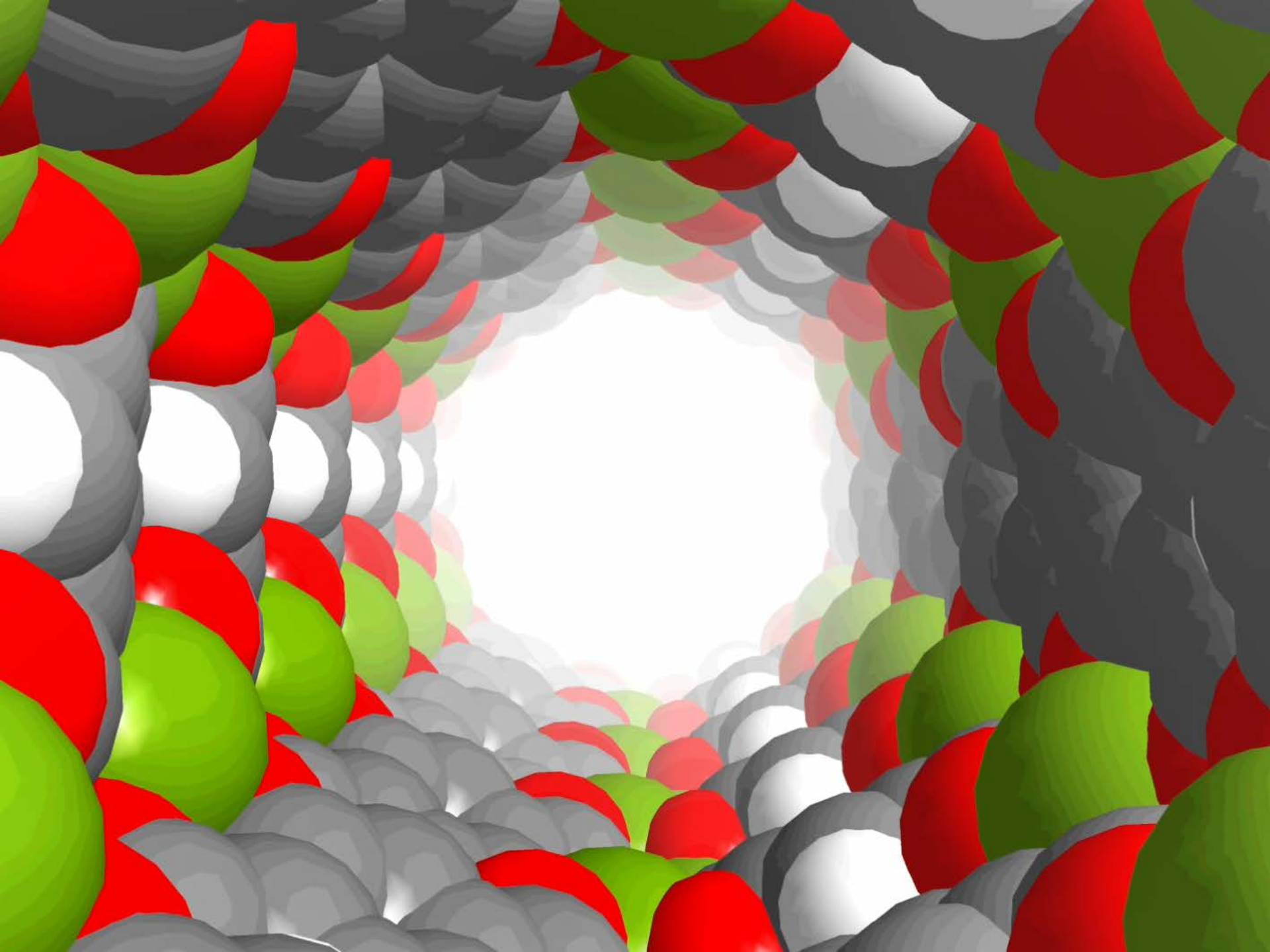
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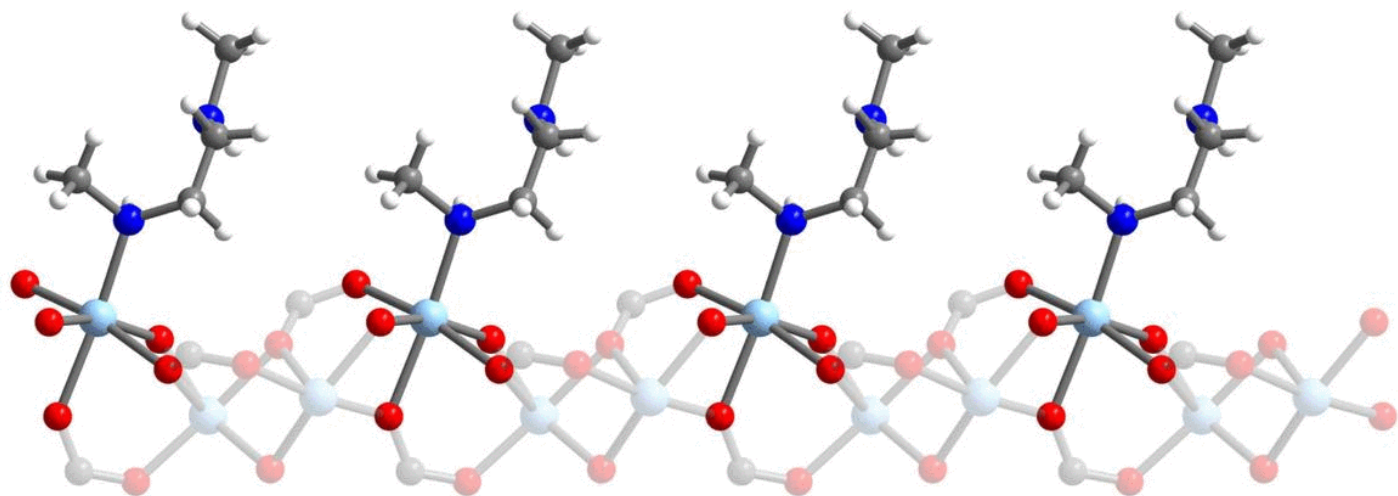
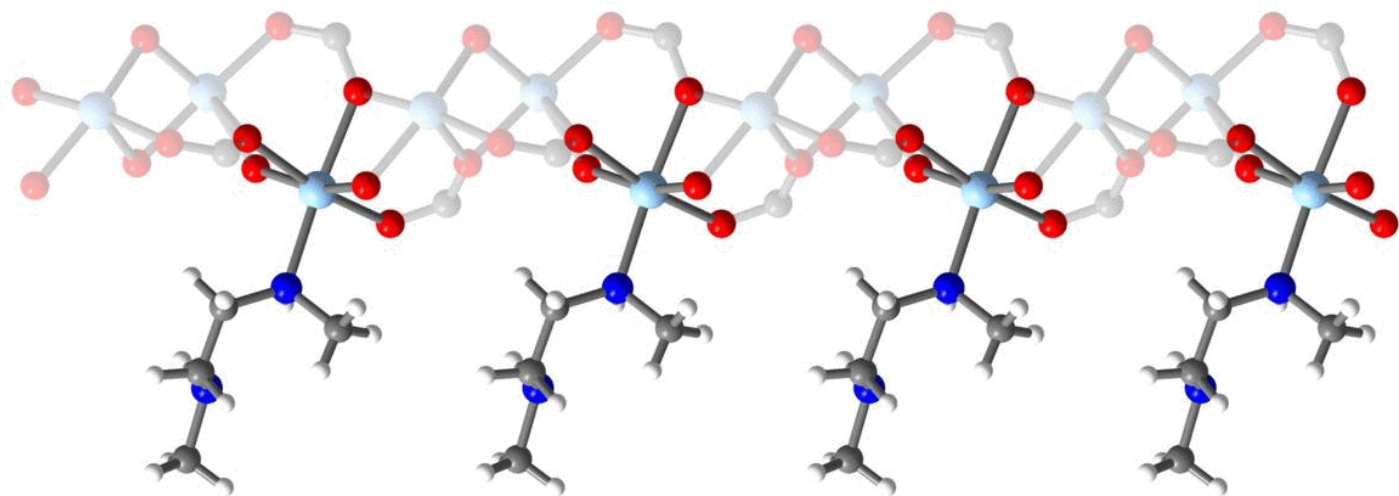
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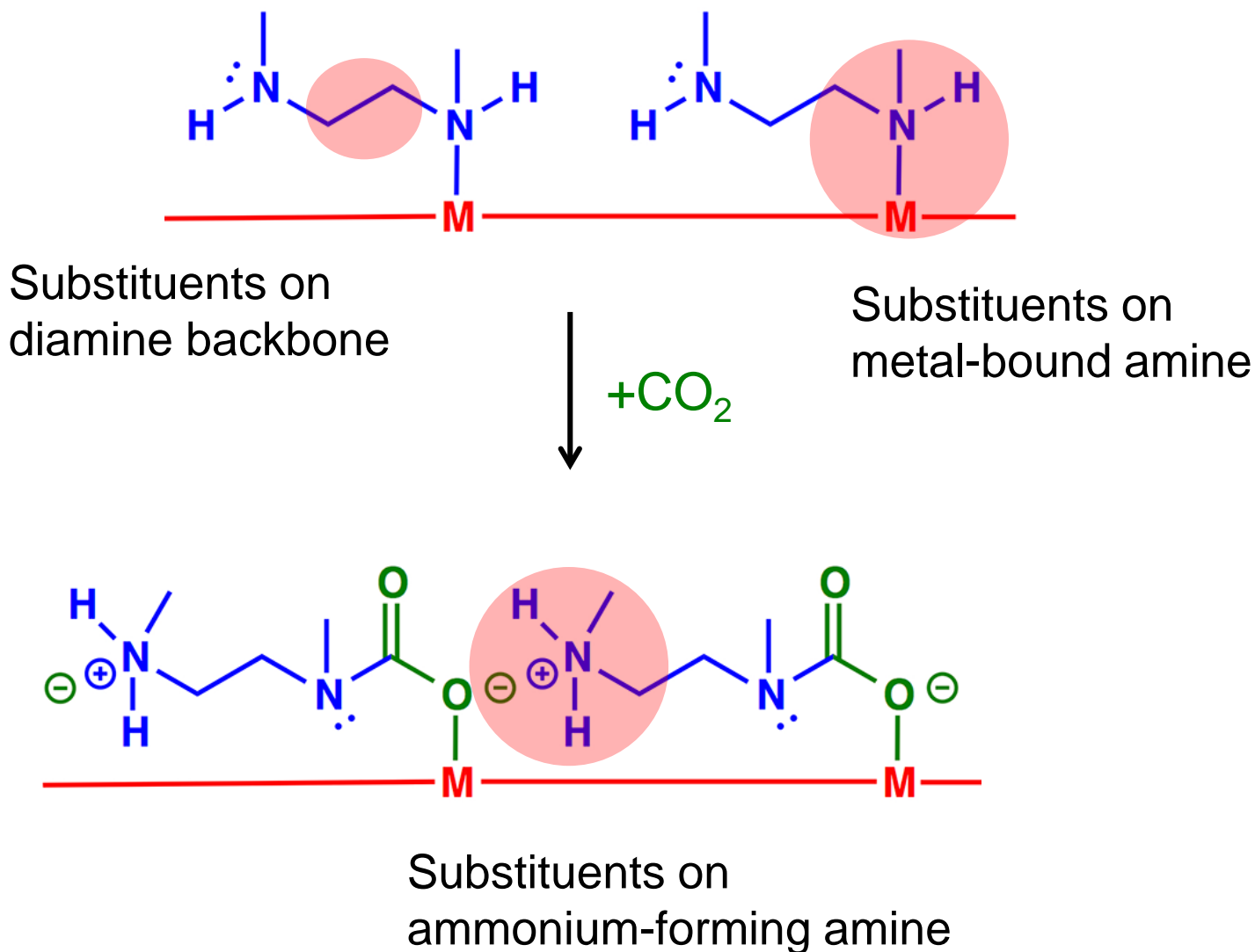








# Manipulating the Adsorption Step Position



# Technical and Economic Advantages/Challenges

## Advantages

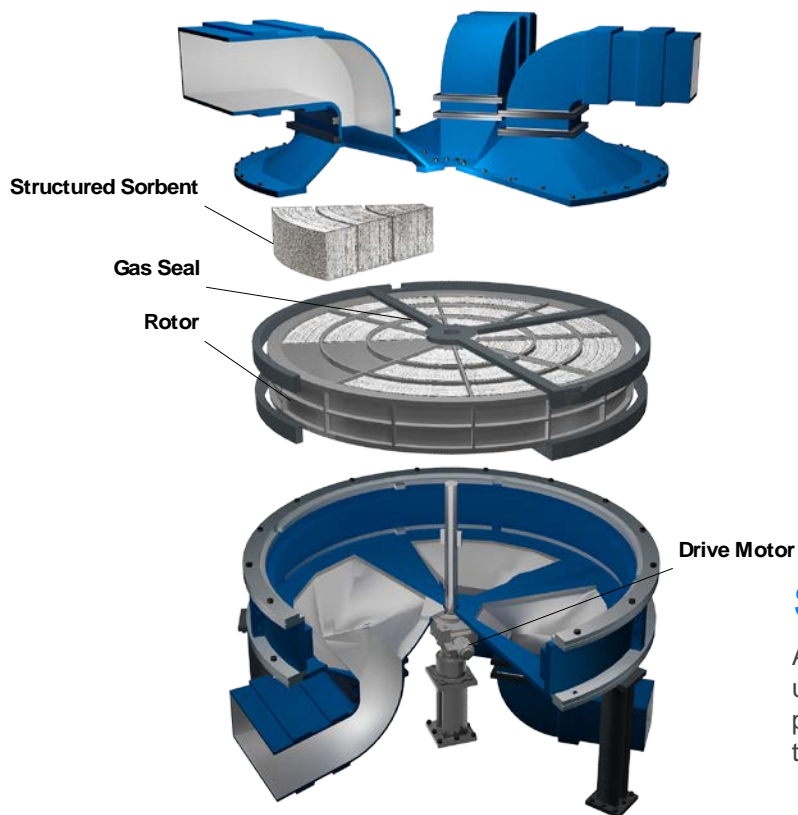
- High tunability of amine-appended framework materials
- Large working capacity due to stepped CO<sub>2</sub> adsorption
- High CO<sub>2</sub> selectivity over N<sub>2</sub>, O<sub>2</sub>, and H<sub>2</sub>O
- Molecular level characterization is possible

## Challenges

- Large scale and economical production of materials
- Durability and chemical stability is unknown
- Reduction of regeneration cost (temperature swing)

# Objective: Implement Adsorbents in RTSA Process

## THREE SIMPLE STEPS



### Step 1: Adsorption

As flue gas passes through the VeloxoTherm™ Adsorbent Structure, CO<sub>2</sub> clings to the adsorbent while the other gases pass through.

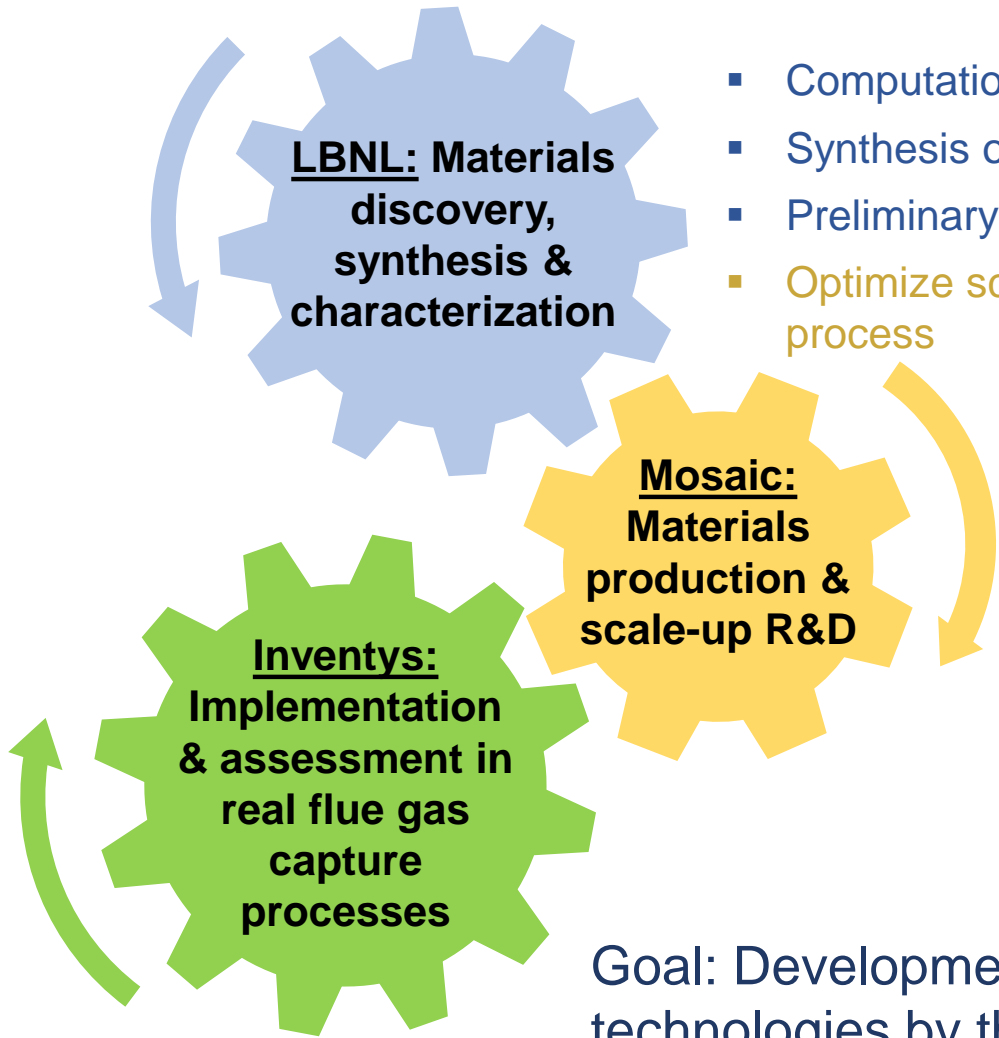
### Step 2: Regeneration

After the structured adsorbent becomes saturated with CO<sub>2</sub>, it is regenerated. Low pressure steam is used to release the CO<sub>2</sub> from the adsorbent.

### Step 3: Cooling

After the CO<sub>2</sub> has been released, air is used to cool the structured adsorbent, preparing it for the adsorption step and the process is started over again.

# Technical Approach and Project Scope



**LBNL: Materials discovery, synthesis & characterization**

- Computational prediction of materials
- Synthesis of amine-appended MOFs (Gen1–Gen3)
- Preliminary stability testing
- Optimize scalable diamine-appended MOF production process

**Mosaic: Materials production & scale-up R&D**

- Interface between LBNL and Inventys for process improvements
- Deliver kg-scale batches of material for preliminary testing and demo at NCCC
- Formation of structured adsorbent beds
- Process development and testing: powders → VTS → PDU → RPV-RAM
- Process modeling and validation

**Inventys: Implementation & assessment in real flue gas capture processes**

Goal: Development of transformative carbon capture technologies by the cooperative insertion of CO<sub>2</sub> in amine-appended frameworks



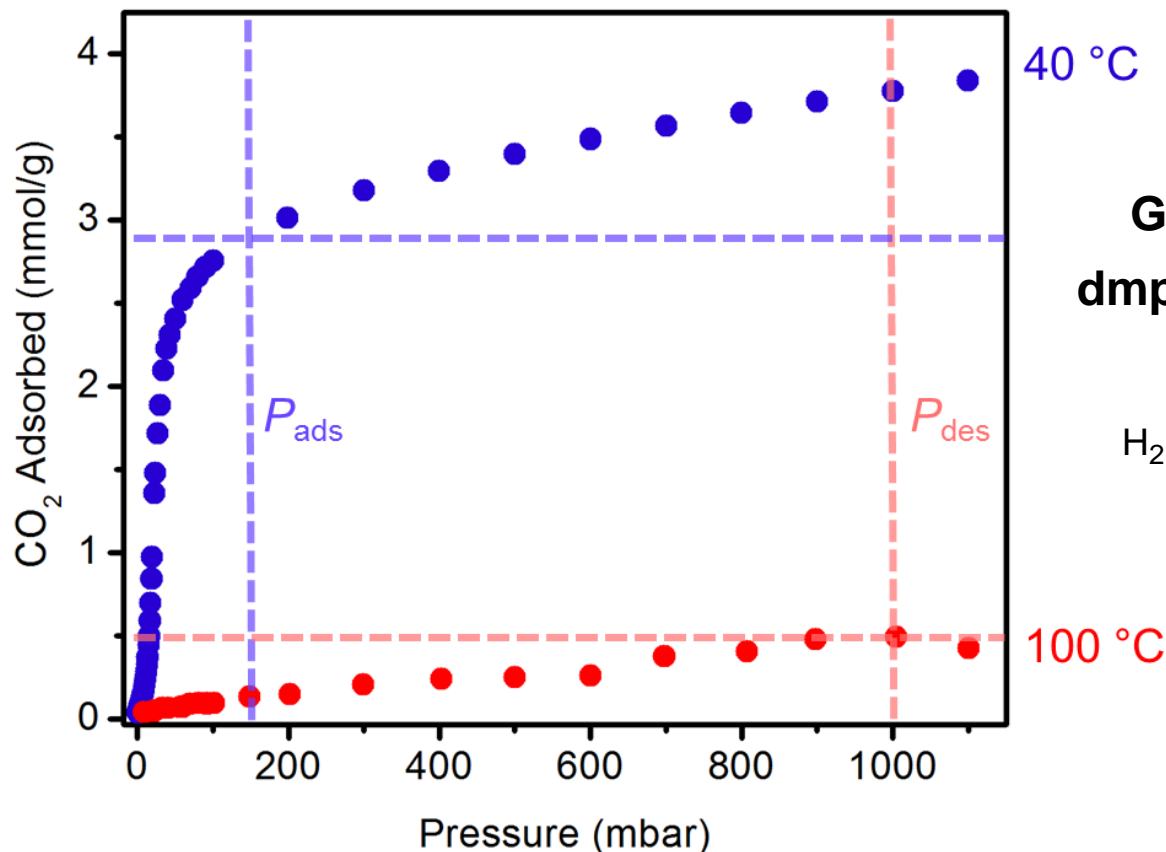
# Project Schedule & Key Milestones (Year 2)

	Tasks
<b>Materials Synthesis</b>	Synthesis of new diamine-appended MOFs (Gen2 materials)
	Characterization of the effects of water, O <sub>2</sub> , SO <sub>x</sub> , and NO <sub>x</sub> on CO <sub>2</sub> adsorption properties of Gen1 and Gen2 materials
<b>Computation</b>	Search optimal amine-appended MOFs within databases of reported materials
	Prediction of CO <sub>2</sub> binding energies and relative isotherm step position for amine-appended MOFs
<b>System Testing</b>	Gen1 materials production and process cost model development
	Concept development modeling and testing
	Process and cycle design simulations

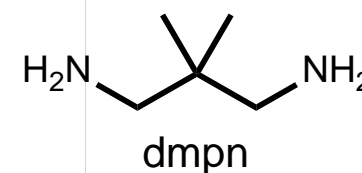
# Project Schedule & Key Milestones (Year 2)

Key Milestones	Status
Gen1 material successfully synthesized at kg-scale and meets CO <sub>2</sub> performance metrics	Complete
Select initial material for VTS-scale single bed testing that demonstrates <5% loss in CO <sub>2</sub> working capacity under cyclic conditions over 5 hours	Complete
Delivery of Gen1 material to Inventys for dynamic VTS testing	Ongoing (2 kg to date)
Create a new material with a working capacity of >3.0 mmol/g (temperature swing <80 °C)	Complete (3.6 mmol/g)

# Year 1 Recap: Gen1 Material Identified



**Gen1 material:**  
**dmpn-Mg<sub>2</sub>(dobpdc)**



- 2.4 mmol/g (9.1 wt %) working capacity with only a 60 °C temperature swing
- Approximate regeneration energy: 2.4 MJ/kg CO<sub>2</sub>

Milner, Siegelman, Forse, Gonzalez, Runčevski, Martell, Reimer, Long *J. Am. Chem. Soc.* **2017**, 139, 13541

# Year 2: Large Scale Synthesis of Gen1 Material

## Objectives

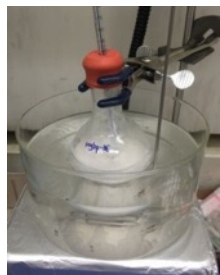
- Research gram to kilogram scale-up method
- Produce MOF at the gram to kilogram scale for use by Inventys
- Identify improvements at kilogram scale

## Scale-up involves four distinct steps

- MOF synthesis  
Batch reaction of metal salt and organic ligand in solvent
- MOF purification  
Product is washed and dried to remove impurities and excess solvents
- Amination  
Purified MOF product is impregnated with amines
- Activation  
Solvent is removed

Steps are dependent on each other, and changes to one procedure often effects the others

# Increasing Scales of Synthesis Equipment



LBNL Gen1  
synthesis



150 mL  
reaction



1.5 L reaction



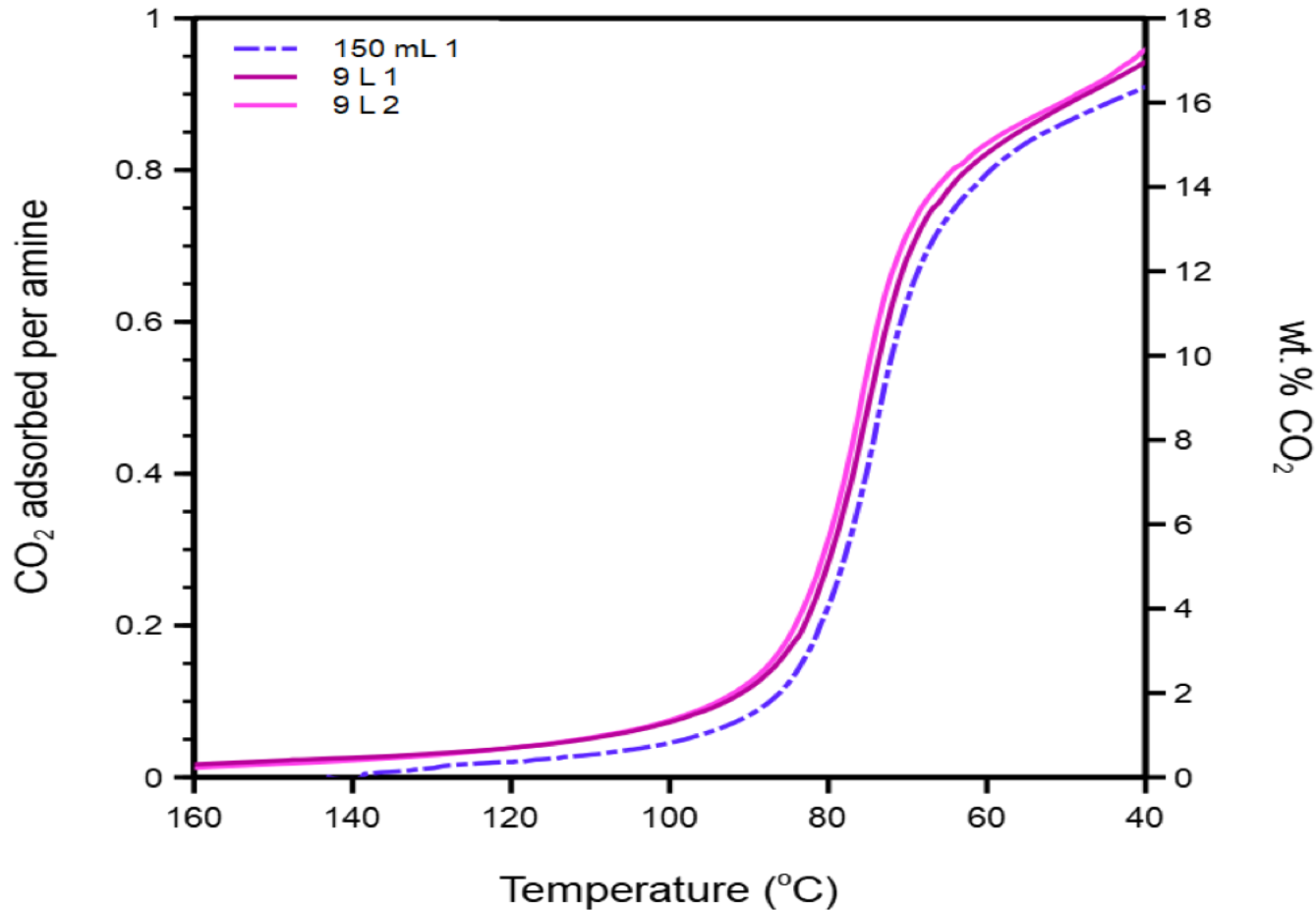
10 L reaction



# Scale-Up Research & Optimization

- Stage 1: Standardized synthesis of 150 mL reaction volume → success  
All QC metrics met: PXRD after synthesis, N<sub>2</sub> surface area after purification, CO<sub>2</sub> capacity (TGA) after amination, amine content (NMR) after activation
- Stage 2: Scale-up to 1.5 L (100 g theoretical yield) → success  
All QC metrics met: PXRD after synthesis, N<sub>2</sub> surface area after purification, CO<sub>2</sub> capacity (TGA) after amination, amine content (NMR) after activation
- Stage 3A: Scale-up MOF to 10 L scale → success  
All QC metrics met: PXRD after synthesis, N<sub>2</sub> surface area
- Stage 3B: Amination and purification combined at 10 L scale → fail  
Amine content and CO<sub>2</sub> adsorption capacity standards not met  
Separating these steps at 10 L scale → success

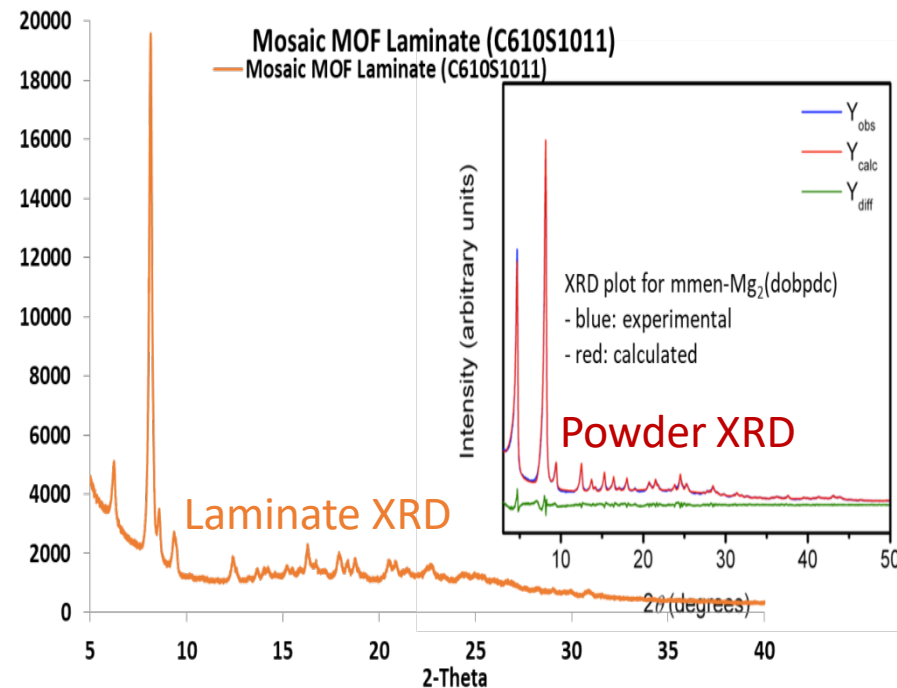
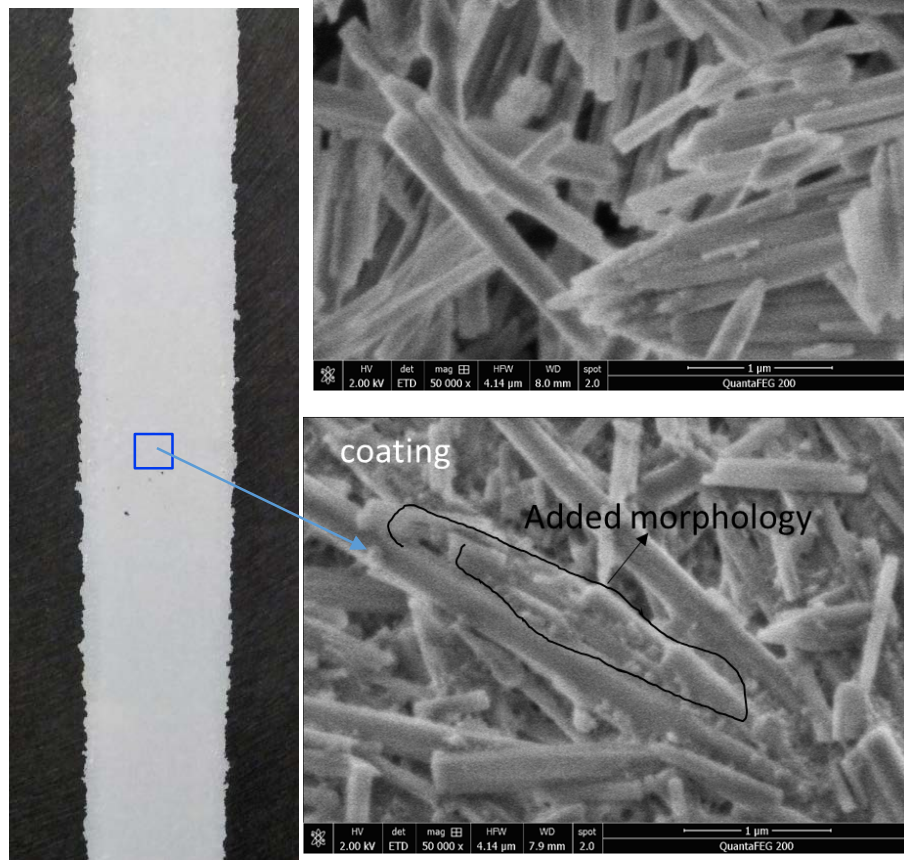
# Modified Purification and Amination Procedure



- New procedure separates purification and amination → successful procedure with all quality control metrics met

# Gen1 MOF Laminate Formulation

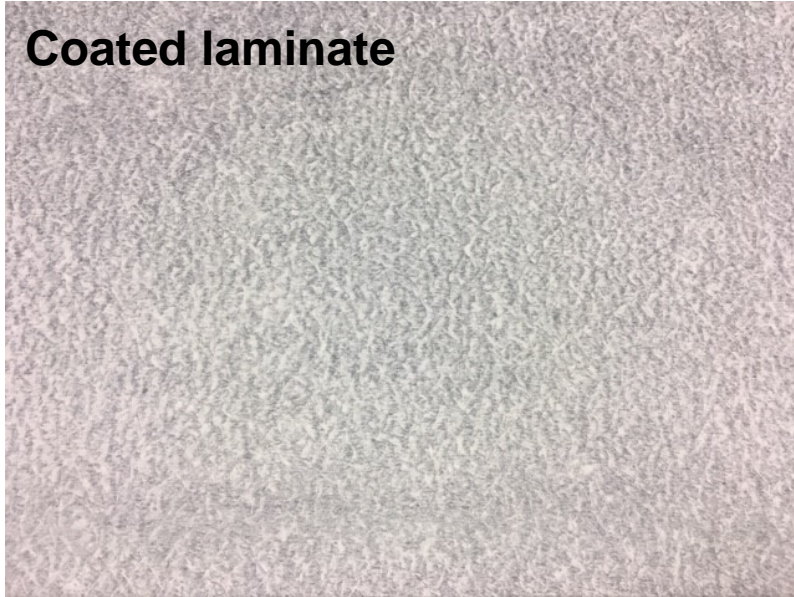
Coating (1")



- XRD and SEM morphology demonstrate equivalent structure between the powder and laminate. Added morphology found at the laminate surface could be the result of pulverization of the rod-shaped crystals and/or binder addition

# Gen1 Preliminary VTS Bed Produced

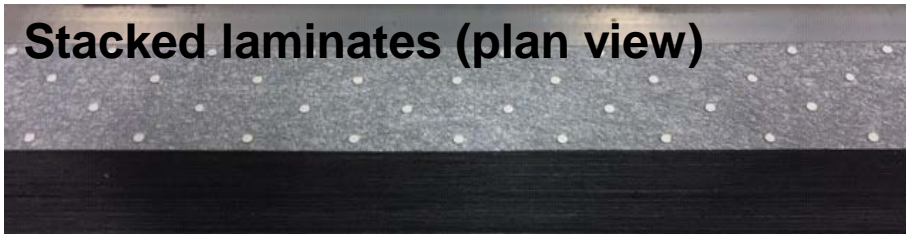
**Coated laminate**



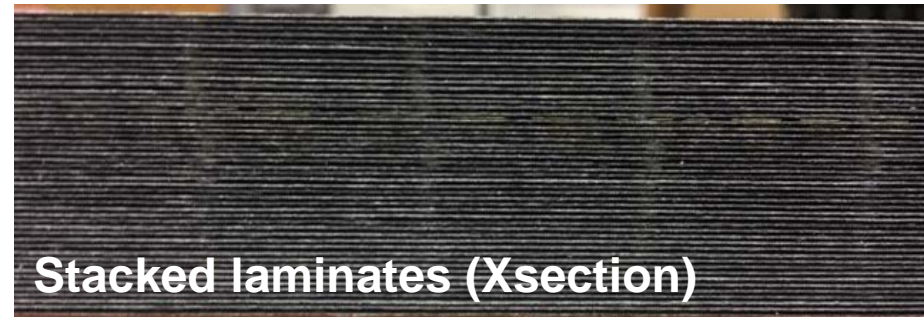
**Coated laminate with spacer**



**Stacked laminates (plan view)**



**Stacked laminates (Xsection)**



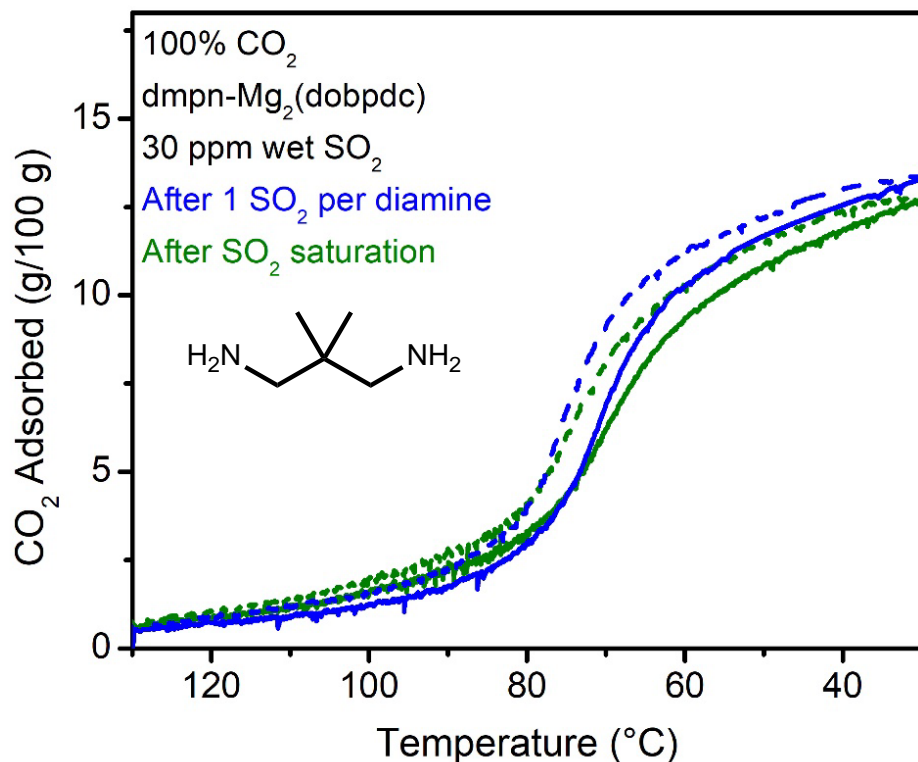


# Gen1 MOF VTS Bed Formulation

- Using a new coating technique, Inventys was able to produce enough laminate to build a VTS bed
  - Water based solvent with added diamine was used
    - CO<sub>2</sub> capacity at 50 °C, 15% CO<sub>2</sub> for the laminate >41 cc/g<sub>MOF</sub> (1.84 mmol/g); working capacity >34.5 cc/g<sub>MOF</sub> (1.55 mmol/g) for 50 °C/90 °C swing
    - Coating density is 30% of the desired capacity → laminate formulation at full MOF coating density in progress, streamlining material processing between Mosaic and Inventys
- Preliminary VTS bed is a very important milestone which permits testing the full performance of the Gen1 material to rapid-cycling TSA with standard flue-gas concentration and moisture
  - Preliminary kinetics and cycle parameters can be determined
  - Both hot CO<sub>2</sub> and steam will be tested as regeneration gas



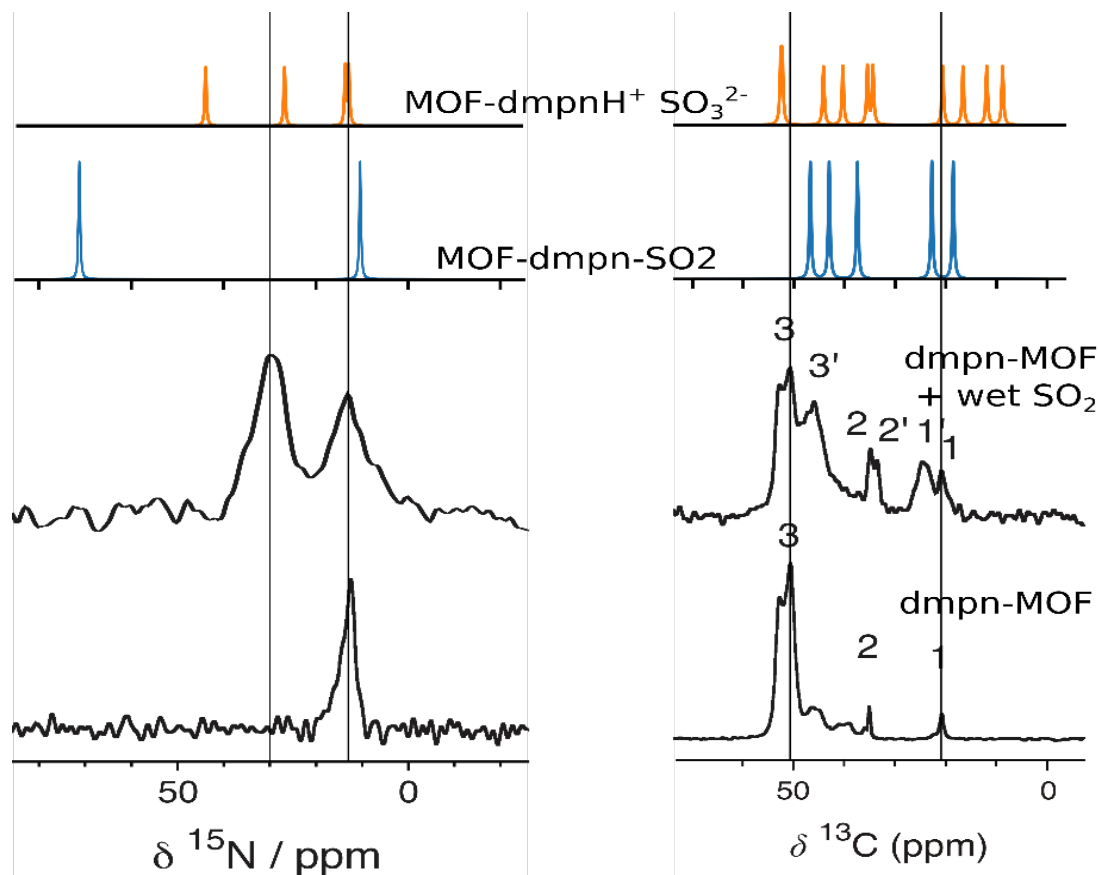
# Year 2 R&D: SO<sub>2</sub> Stability and Regeneration



conditions	Gen1 CO <sub>2</sub> capacity retained
1 SO <sub>2</sub> per diamine	79
full SO <sub>2</sub> saturation	77
3 days past SO <sub>2</sub> saturation	77
SO <sub>2</sub> saturation with 14% CO <sub>2</sub>	90

- Capacity of 1 SO<sub>2</sub> per diamine obtained from both elemental analysis and SO<sub>2</sub> breakthrough data
- CO<sub>2</sub> capacity does not continually degrade with increased SO<sub>2</sub> exposure time

# Understanding SO<sub>2</sub> Adsorption in Gen1 Material



- Solid-state NMR and DFT calculations suggest formation of ammonium sulfites
- Mass spectrometry data also indicates the presence of sulfites

# Characterization of SO<sub>2</sub> Adsorption in Gen1 Material

Gen1 initial diamine loading	after humid SO <sub>2</sub> exposure	after collecting CO <sub>2</sub> isobar
98%	98%	89%

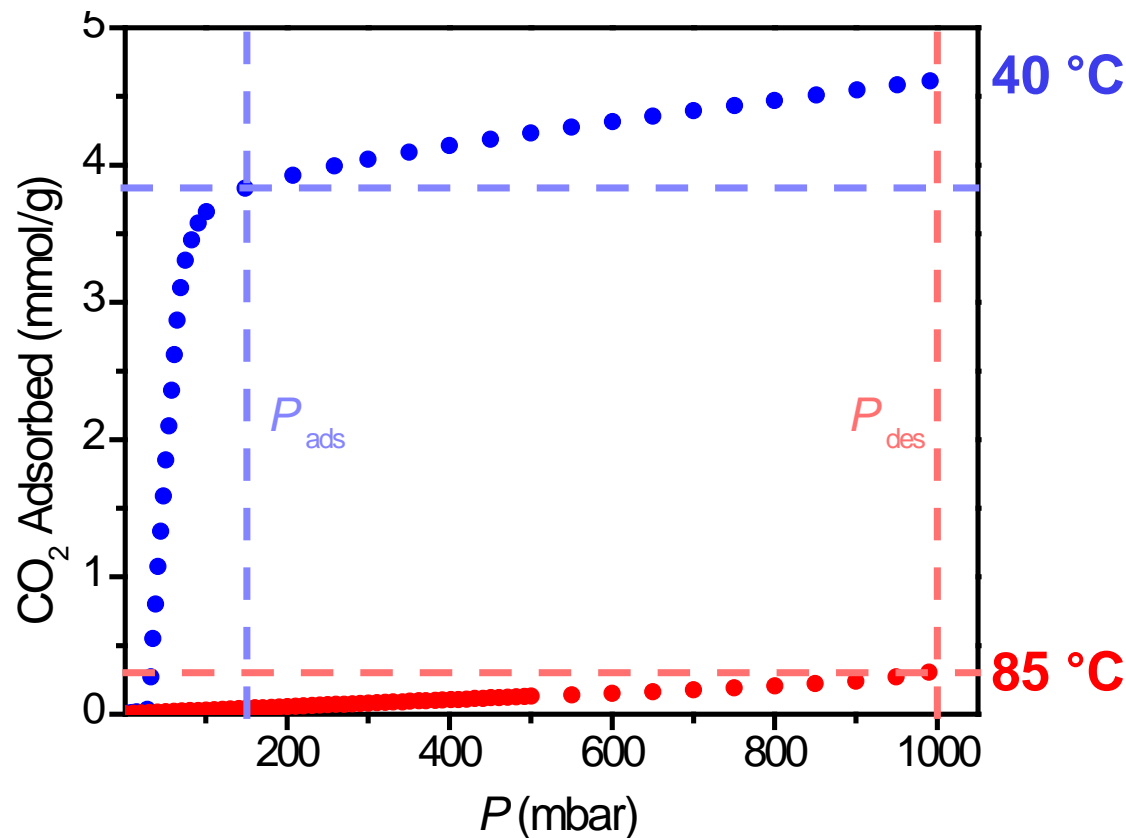
## Mechanism of degradation

- Diamine loading shows that diamines are lost during re-activation instead of during exposure

## Attempts at regeneration

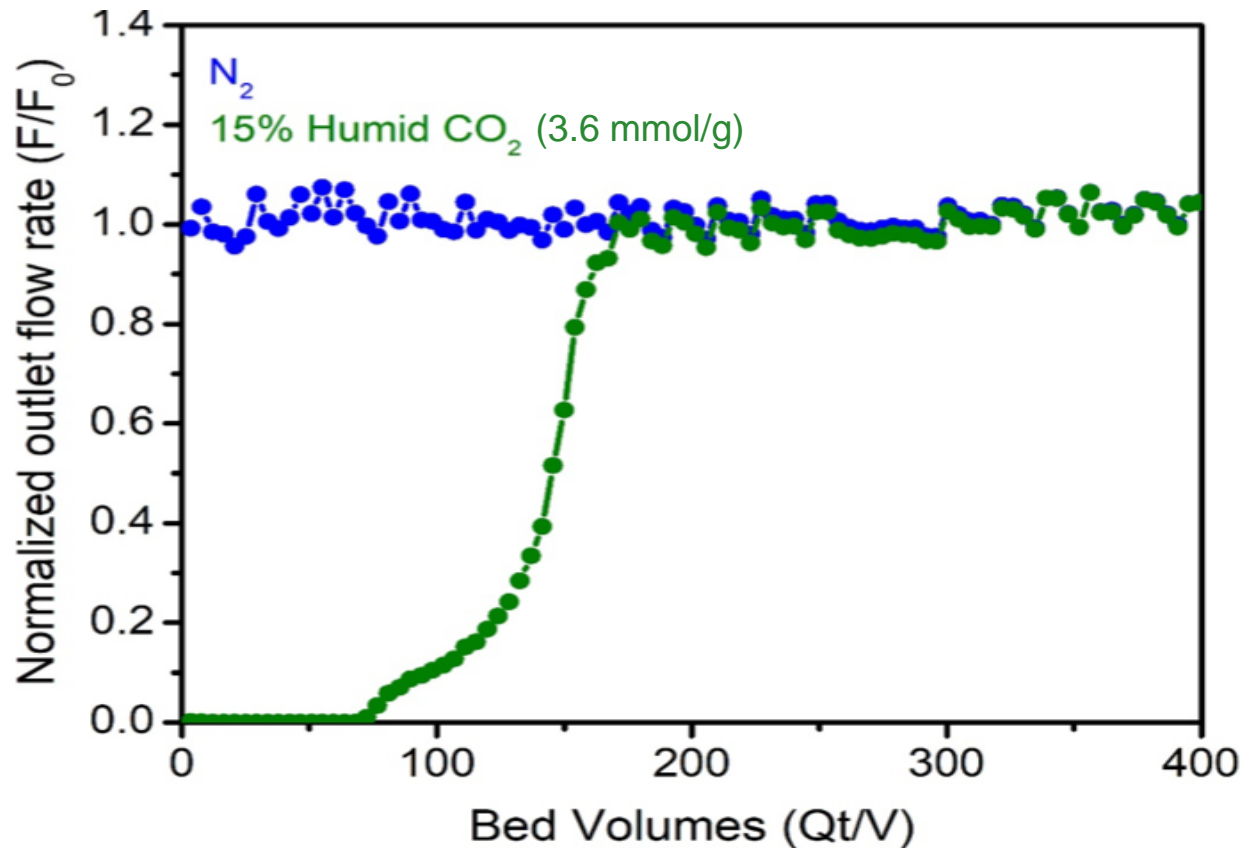
- Ethanol soak, room temperature: removed diamines
- Acetonitrile soak, room temperature: no change
- Acetonitrile soak, 60 °C: removed diamines
- Flowing humid N<sub>2</sub>, 4 h at 55 °C: no change
- Flowing humid CO<sub>2</sub>, 4 h at 50 °C: no change

# Year 2 R&D: Gen2 Material Identified



- 3.6 mmol/g (16 wt %) working capacity with only a 45 °C temperature swing
- Approximate regeneration energy: 2.2 MJ/kg CO<sub>2</sub>

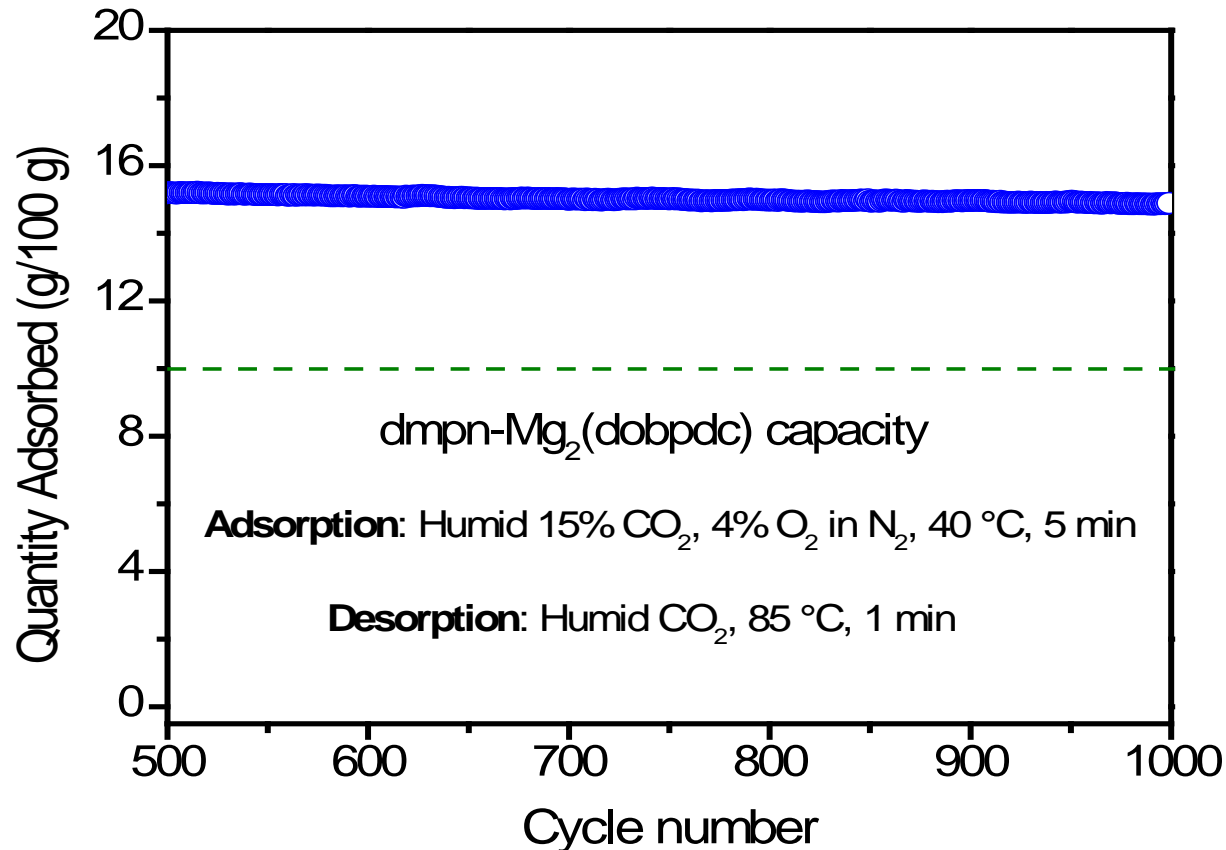
# Gen2: Humid Breakthrough Experiments



- Breakthrough experiments with pre-humidified column and gas stream show sharp  $CO_2$  breakthrough and the expected high capacity



# Gen2: 1000 Adsorption/Desorption Cycles



- Stable to 1000 humid adsorption/desorption cycles under simulated coal flue gas conditions (diamine loading after experiment: 99%)
- Gen2 cycling capacity is 50% greater than Gen1 material

# Plans for Future Testing and Development

## Preliminary system testing of Gen1 material

- Process improvements to large scale manufacturing procedure to better integrate with laminate formulation process
- RTSA testing with VTS bed: steam and hot CO<sub>2</sub>
- In house multi-bed PDU performance testing → optimize cycle parameters
- Planning and refinements to design of testing skid at NCCC

## Synthesis of improved diamine-appended MOFs (Gen2/Gen3 materials)

- Long term stability assessments of Gen2 material and scale-up evaluation
- Evaluate new diamine-appended MOFs with similar properties of Gen1/Gen2 materials

## Further materials improvements

- Use screening database to search for new diamine-appended MOF candidates
- Structure-stability studies of materials (H<sub>2</sub>O, SO<sub>x</sub>, NO<sub>x</sub>) and evaluation of alternate regeneration strategies to recover greater CO<sub>2</sub> capacity

# Acknowledgements

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