

# Advanced Manufactured Carbonate Materials for Algal Biomass Production: Joint LLNL-SNL Program

NETL CO<sub>2</sub> Capture Technology Project Review Meeting

August 30, 2019

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SNL: Todd Lane, Mary Tran-Gyamfi

DOE NETL Project Manager: Andrew Jones



# Project Overview

**Project:** FWP-FEW0223

**Project Period:** 10/01/2017-12/31/2019

**Funding:**

	<b>Government Share FY18</b>	<b>Government Share FY19</b>
Lawrence Livermore National Laboratory	\$390,000	\$375,000
Sandia National Laboratory	\$360,000	\$350,000
<b>Total</b>	<b>\$750,000</b>	<b>\$725,000</b>

**Objective:** Develop and evaluate advanced manufactured carbonate materials for carbon capture, storage, and algal biomass production.

# Project Tasks

FY18	Task 1	Project planning and management
	Task 2	Select the most promising material and geometry
	Task 3	Demonstrate CO <sub>2</sub> storage and delivery to support algal culture
	Task 4	Evaluate the economics and gate-to-gate GHG emissions
FY19	Task 5	Refine the material formulation
	Task 6	Scale-up synthesis, CO <sub>2</sub> loading, and delivery processes
	Task 7	Demonstrate scalability of material to sustain algal growth
	Task 8	Refine TEA and LCA of the system

# Success Criteria FY19



July 1, 2019

Achieve a material loading capacity of at least 10 wt% CO<sub>2</sub>



Sept. 30, 2019

Carbonate materials can be reloaded with CO<sub>2</sub> after use in algal cultures with less than 10% loss of CO<sub>2</sub> capacity over 10 cycles



Oct. 31, 2019

Carbonate materials can support algal growth in indoor and outdoor conditions up to 20L scale for >24 hr



Dec. 31, 2019

At 100-1000 L scale, carbonate materials can support the growth of algae at 80% productivity for one day-night cycle (24 hours)

# CO<sub>2</sub>-loaded materials can be used for algae production

## Challenges to CO<sub>2</sub> Capture & Utilization:

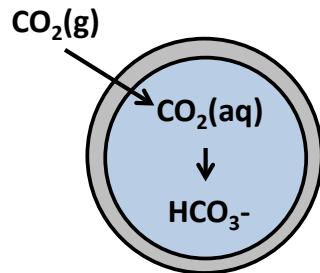
Corrosivity, evaporative losses, and fouling



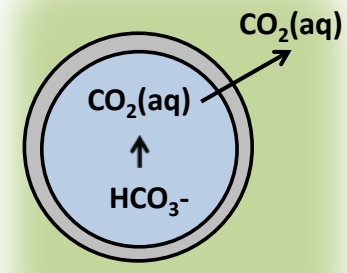
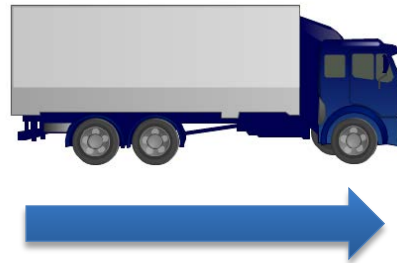
Transportation



CO<sub>2</sub> is at least 20% of cost of algae cultivation



Absorption

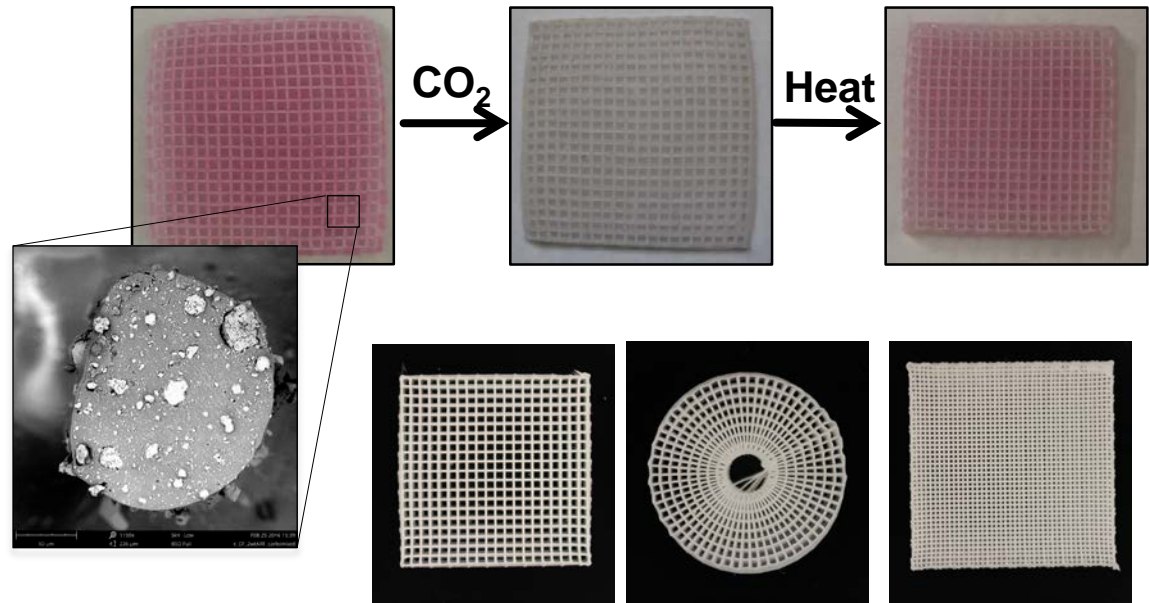
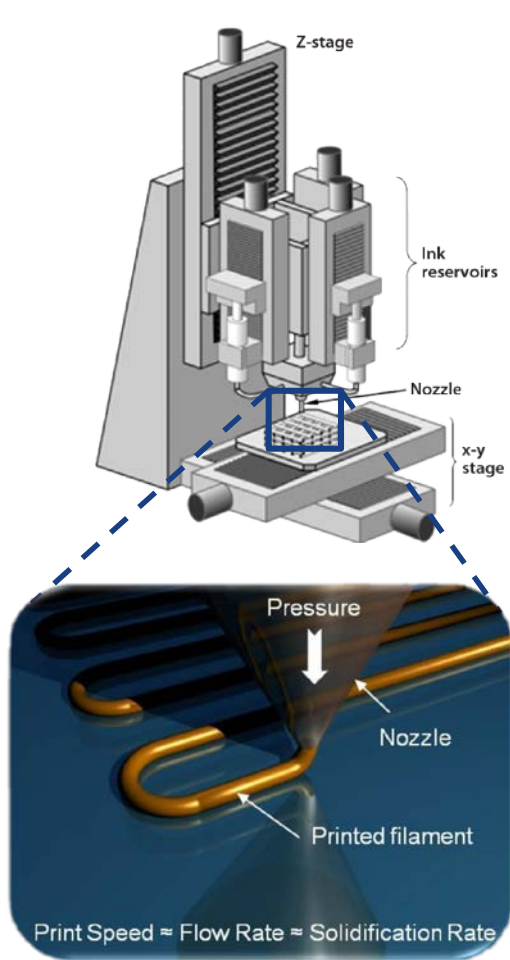


Release (Algae Pond)

- 1) Provide tunable transport, storage, and delivery
- 2) Eliminate need to co-localize
- 3) Reduce capture costs up to 75%



# Sorbent-polymer composites printed with Direct Ink Write (DIW)

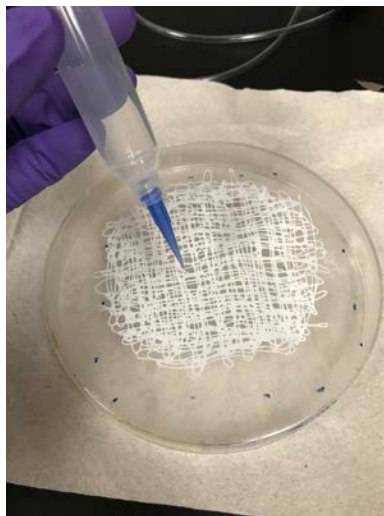


- Ink can be loaded with as much as ~60 wt% carbonate
- Particulate sizes sieved as small as possible for best performing ink

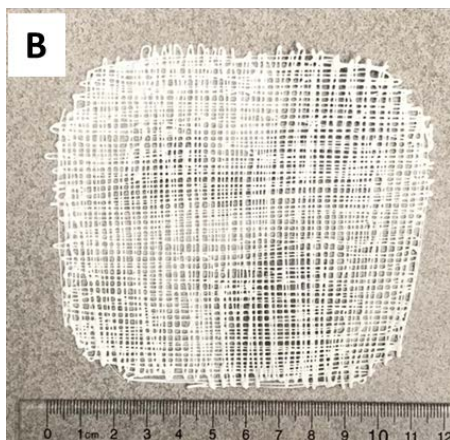
# Scale up materials synthesis from grams



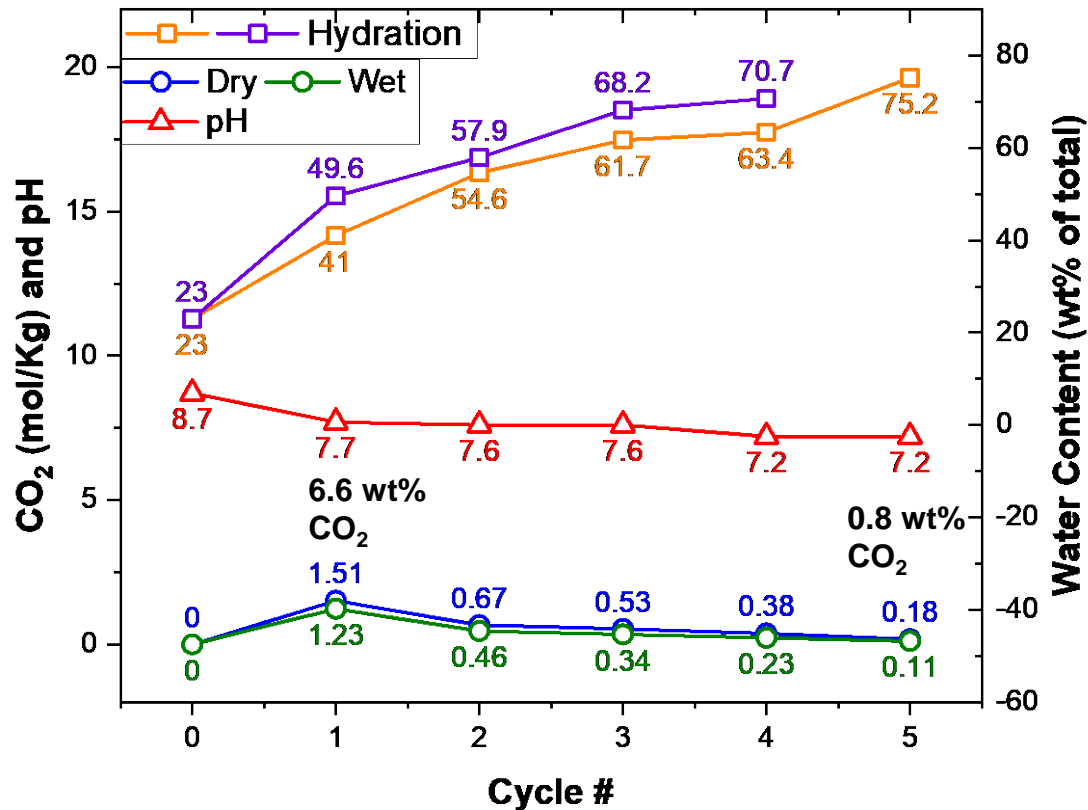
Hand extrusion  
~10s grams



Power extrusion  
kilograms



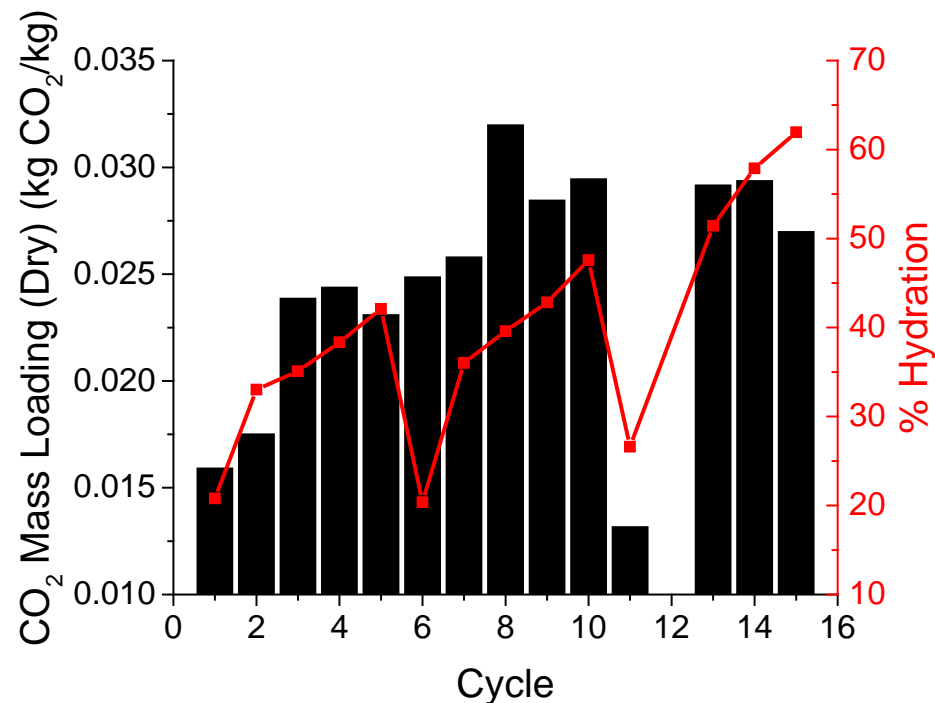
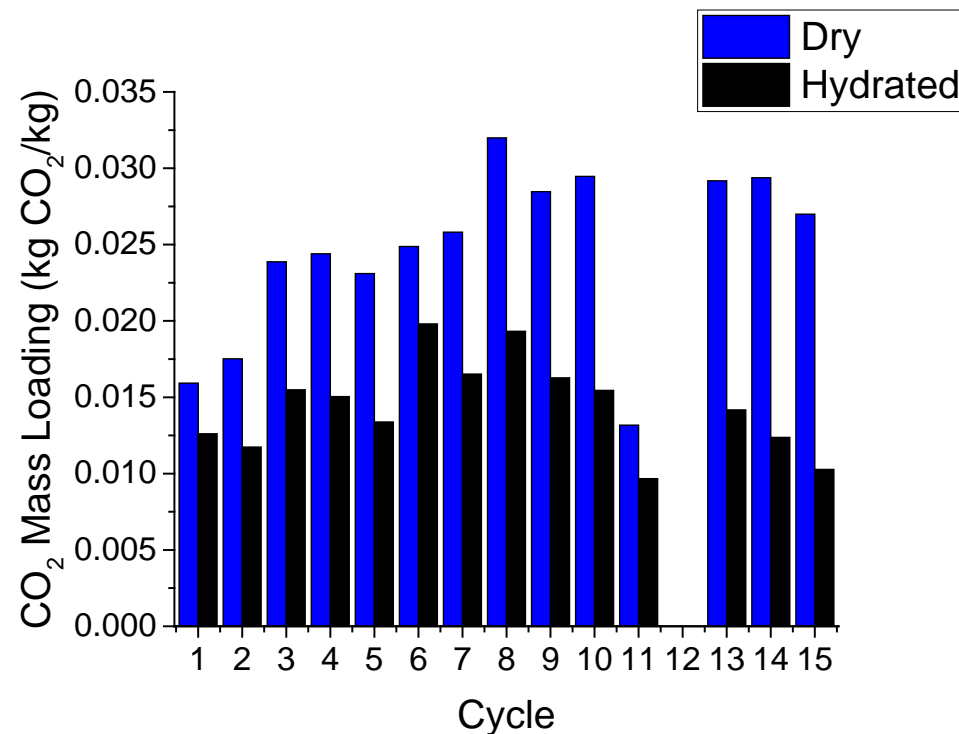
# CO<sub>2</sub> capacity decreases across 5 cycles *without* algae



- 25% sodium carbonate, 52% SE-1700 + 23% Sylgard formulation
- Samples loaded in 100% CO<sub>2</sub>
- Samples “regenerated” by soaking in media **without** algae
- **Samples were not adequately regenerated**



# Constant CO<sub>2</sub> capacity across 15 cycles *with* algae



- 25% sodium carbonate, 52% SE-1700 + 23% Sylgard formulation
- Material loaded with 10% CO<sub>2</sub> in N<sub>2</sub> for 1.5 hours
- Material regenerated in algal culture for 2 hours

**CO<sub>2</sub> loading dependent on hydration and does not decrease over cycling**

# Process configuration for preliminary TEA of transport and delivery

CO<sub>2</sub>  
Absorption

Loading

Truck  
Transport

Unloading &  
Temporary  
Storage

Dosing,  
Regeneration  
& Separation

Unloading

Truck  
Transport

Temporary  
Storage &  
Loading

Drying

Flow diagram of CO<sub>2</sub> delivery to algal farm

# TEA model assumptions & results for transport and delivery

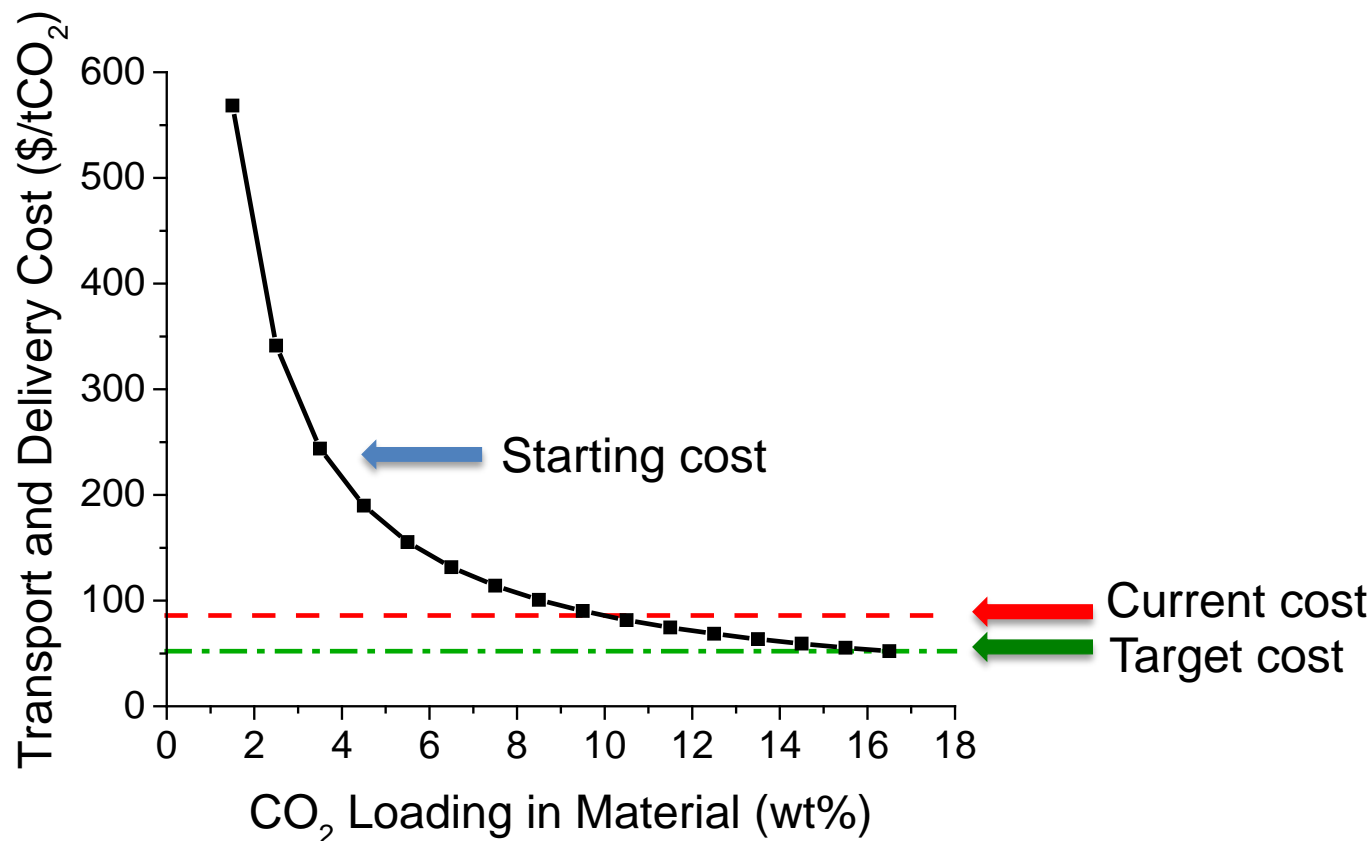
## Assumptions:

- 5000 ac pond area
- 1,112 tons CO<sub>2</sub>/daily
- **16.5 wt%** CO<sub>2</sub> loading in material
- Transported via motor transport 60 mi (one-way)

Stage	Cost (\$/ton of CO <sub>2</sub> delivered)
<b>Non-Fuel Transportation Cost</b>	21
<b>Fuel Transportation Cost</b>	19
<b>Storage Units Cost</b>	0.19
<b>Conveyors Cost</b>	12
<b>Total</b>	\$52/ton CO <sub>2</sub>

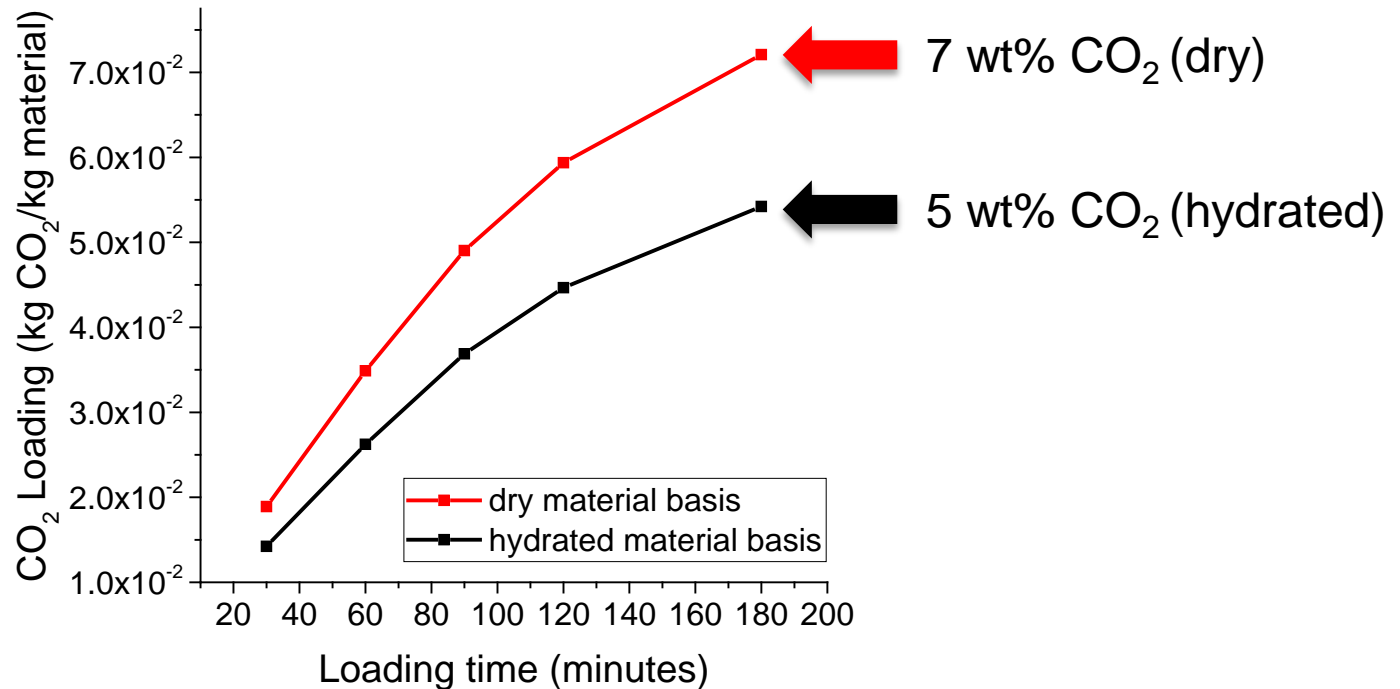
**Target cost for transportation & delivery is \$52/ton CO<sub>2</sub>**

# Target cost of transport and delivery based on TEA



Transportation cost & delivery has been reduced by 60%

# CO<sub>2</sub> loading in process-relevant conditions

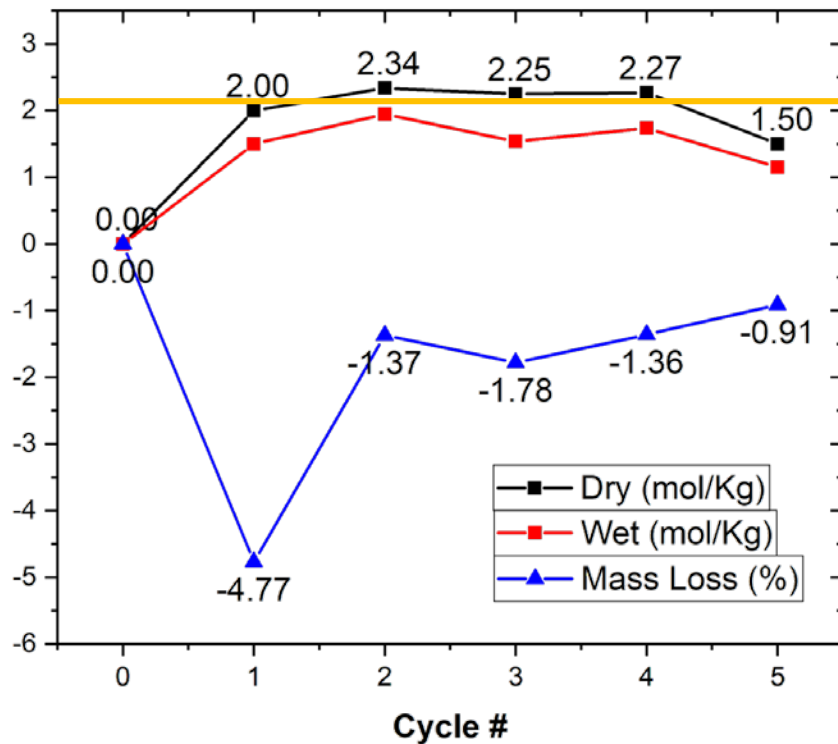


- **25% sodium carbonate**, 23% Sylgard, and 52% SE-1700
- 10% CO<sub>2</sub> with 87% relative humidity at 23°C

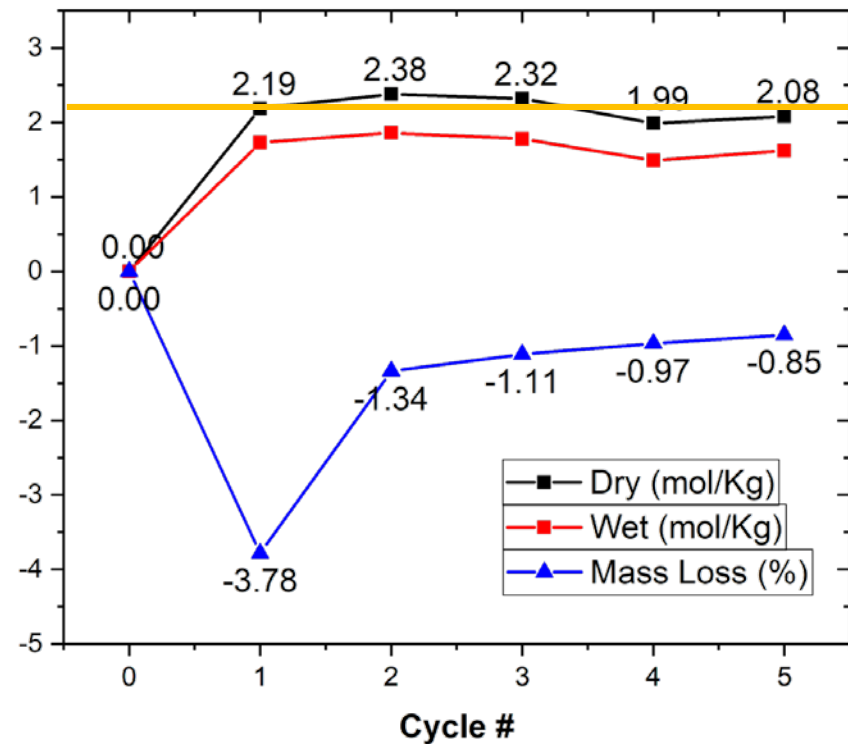
Loading rate slower than expected – can be tuned with filament size



# Tune material formulation to increase CO<sub>2</sub> loading



40% Na<sub>2</sub>CO<sub>3</sub> + 25% SE-1700 + 35% Sylgard



40% Na<sub>2</sub>CO<sub>3</sub> + 35% SE-1700 + 25% Sylgard

Orange line meets 10 wt% CO<sub>2</sub> loading

# Stability of CO<sub>2</sub>-loaded material

CO<sub>2</sub> loading and hydration of samples stored in **2L** containers for 20 days

Condition	% CO <sub>2</sub> “lost”	% Hydration after incubation
35C with media	32.72	40.13
35C with media	55.30	52.72
RT with media	12.58	31.59
RT with media	13.29	29.55
RT	6.50	11.40
RT	3.05	12.12
35C	55.90	21.59
35C	53.37	14.63

**Samples stored at room temperature lost <10% of the loaded CO<sub>2</sub>**

# Stability of CO<sub>2</sub>-loaded material

CO<sub>2</sub> loading and hydration of samples stored in **50 ml** containers for 14 days

Condition	% CO <sub>2</sub> “lost”	% Hydration after incubation
RT	8.3	15.7
RT	9.2	15.1
RT	5.3	11.9
RT	11.9	17.9
35C	10.5	24.58

**Samples stored at room temperature lost <10% of the loaded CO<sub>2</sub>**

# Scale up CO<sub>2</sub> loading from column to 2L reactor

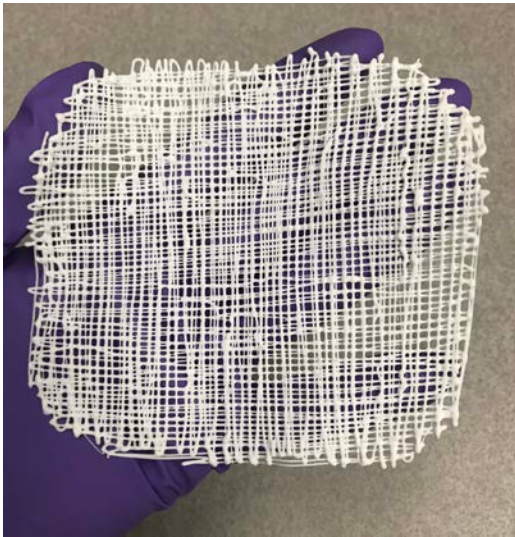


Small absorption column  
~50 g material



Larger, automated absorption column  
~300 g material

# Measure CO<sub>2</sub> delivery to algal cultures



Measure pH of culture every 30 minutes

Dose the culture with CO<sub>2</sub> loaded material every 2 hours



# Scale up cultures from 500 mL to 4L

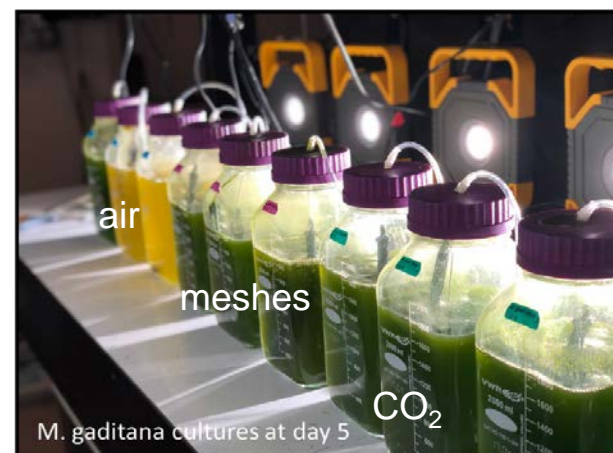
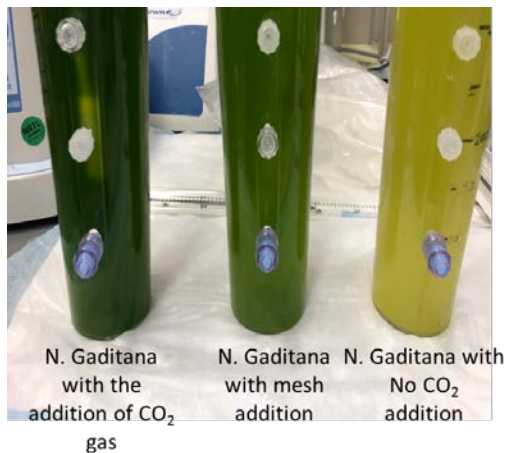
500 mL



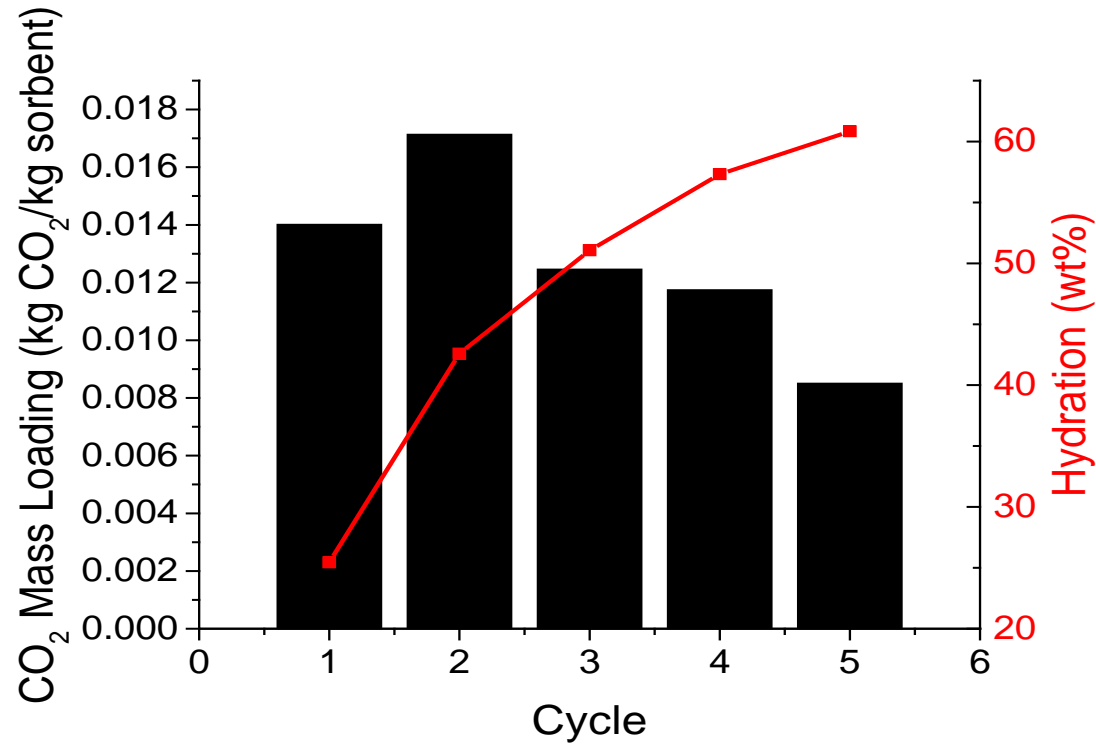
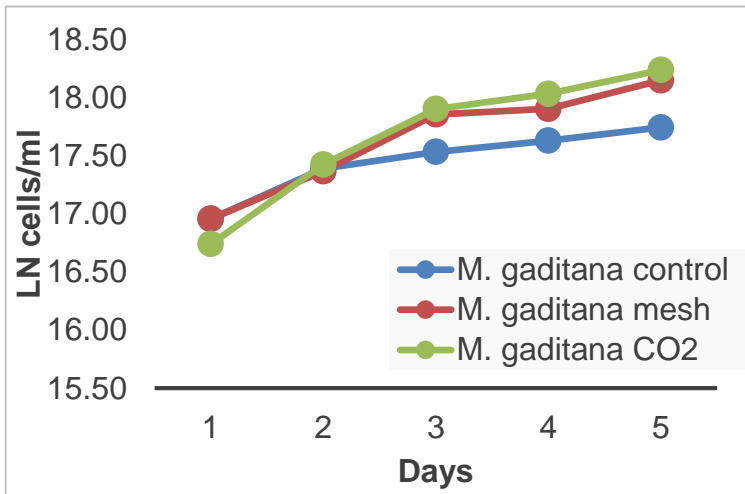
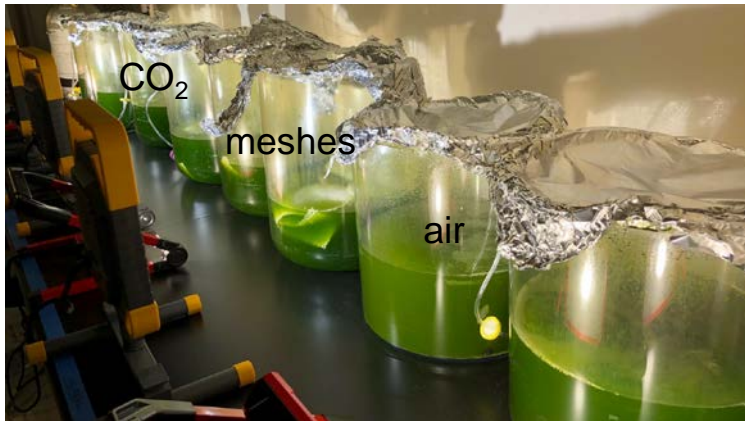
2L



4L



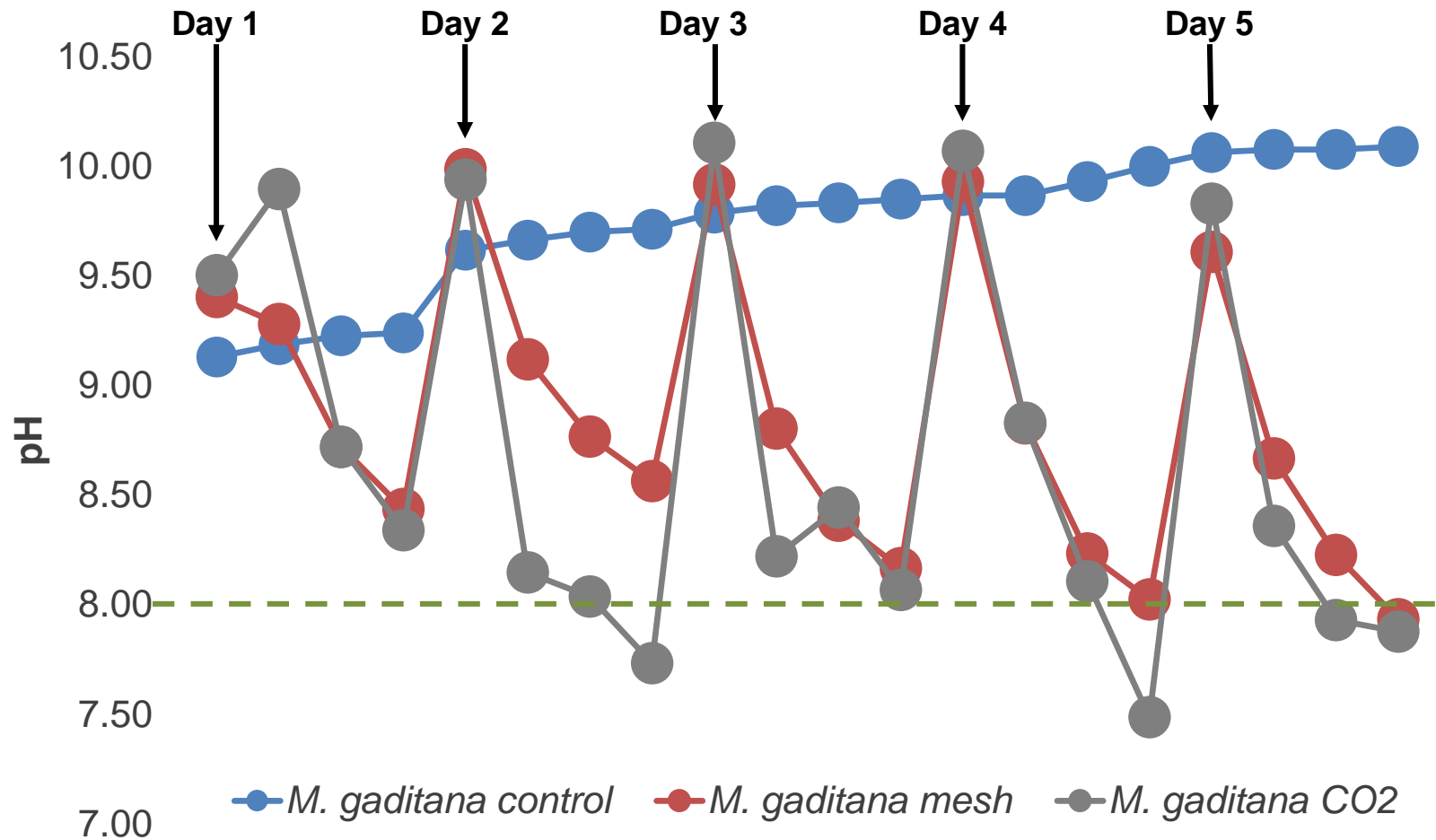
# 8 L algal cultures



~1.2 wt% CO<sub>2</sub> loading, 30-60 wt% hydration

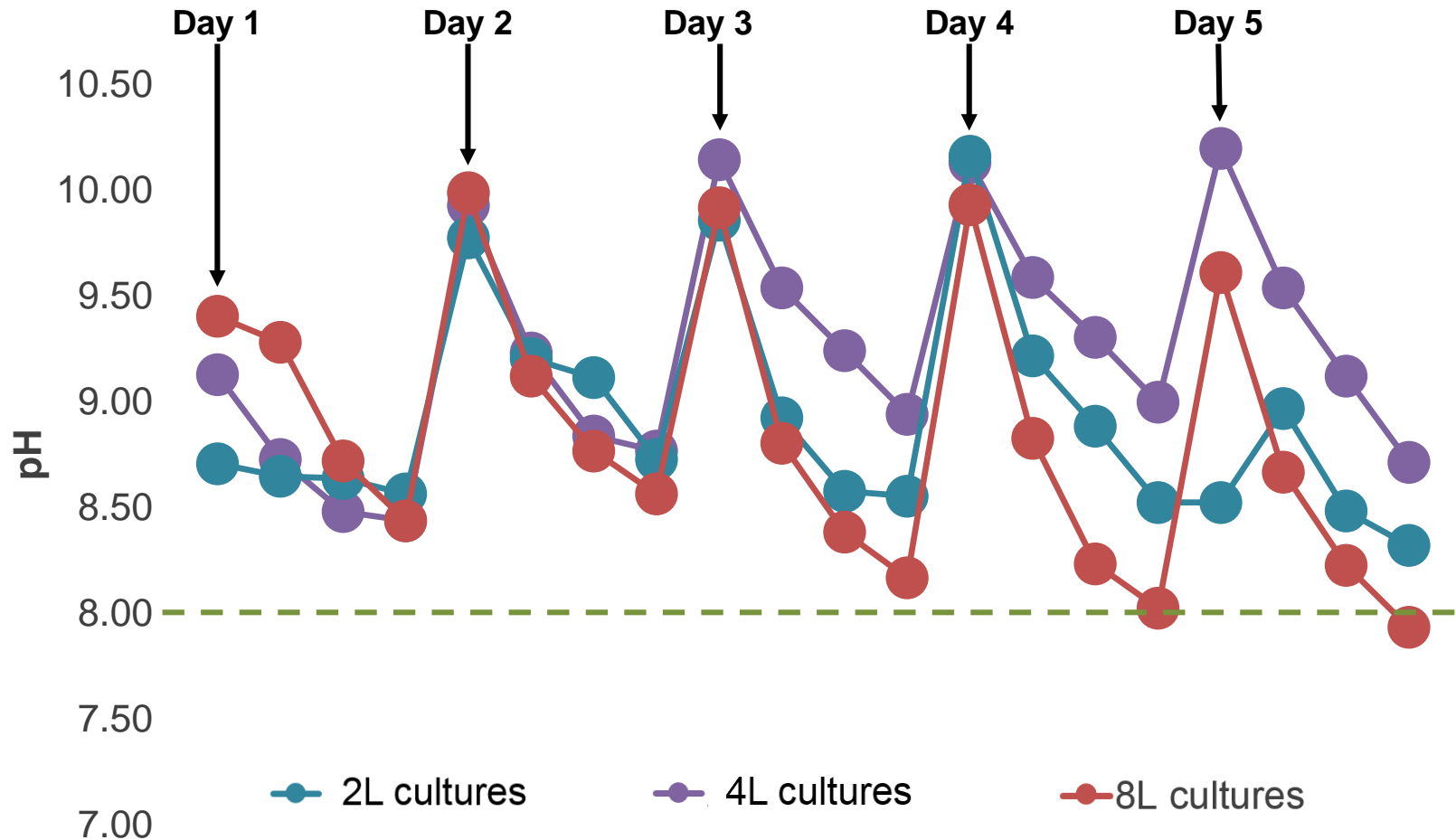
Hydration increases over 5 cycles, but mass of CO<sub>2</sub> loaded is constant

# pH response of 8L cultures



pH profile of cultures with meshes matches that of positive control

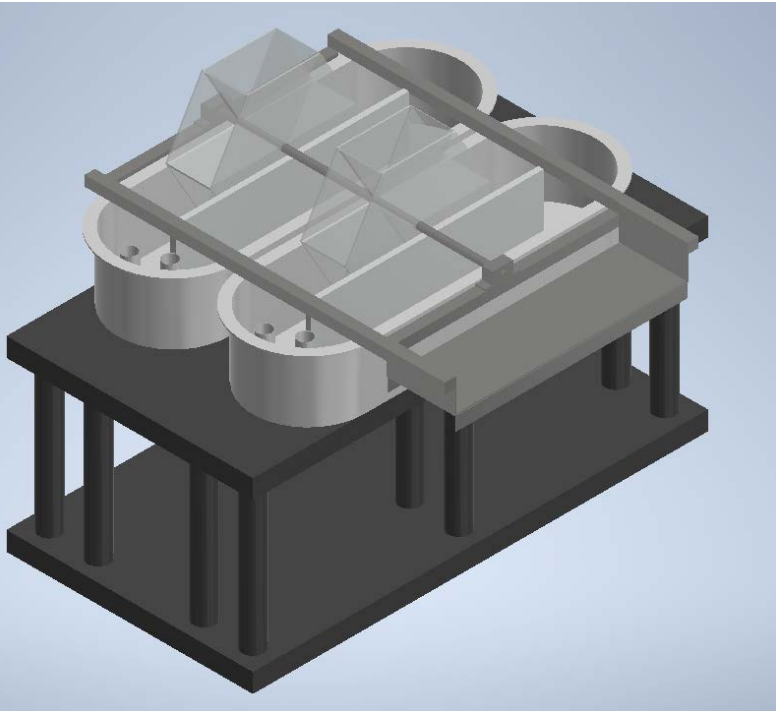
# pH response from 2-8 L scale up



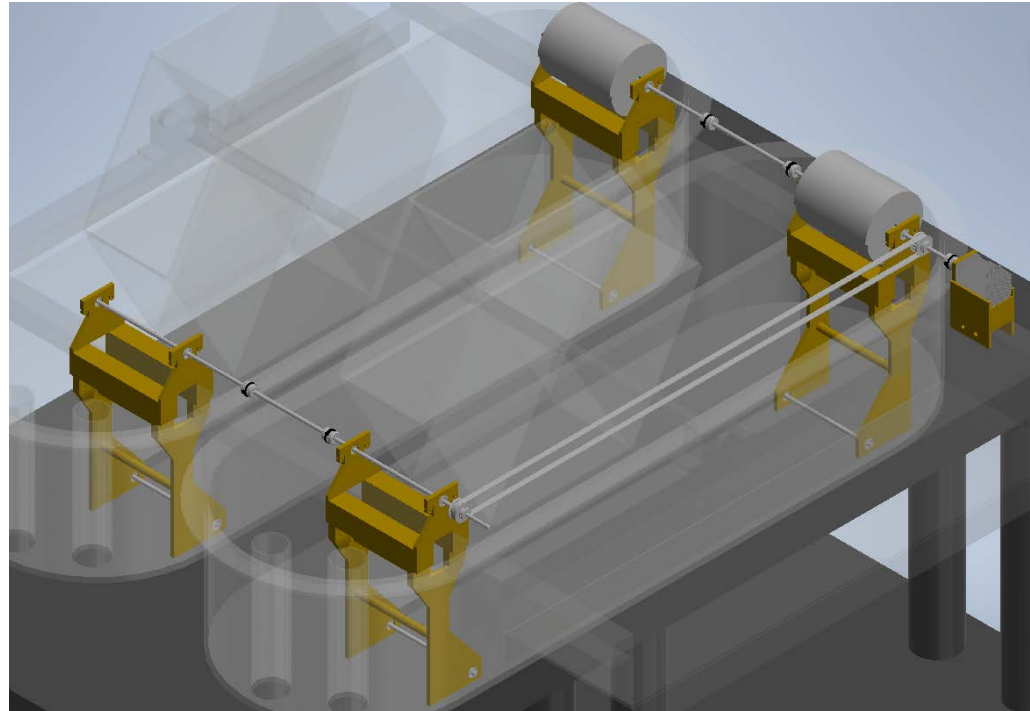
**Dosing of cultures did not scale linearly with culture volume**



# Develop scalable delivery method to raceways



Drawing of 100L raceways



Design for roll-to-roll automated delivery system

**Design for delivery system is being finalized**



# Remaining tasks

- Install power extruder to scale production to kilograms
- Scale algal cultures to 20L and 100L
- Build an automated material delivery system for 100L raceways
- Complete TEA/LCA based on experimental data from scale up studies

# Summary

- Synthesis was scaled up to 100s of grams
- Formulation was tuned to achieve 10 wt% CO<sub>2</sub> loading
- CO<sub>2</sub>-loaded material loses <10% of CO<sub>2</sub> over 2 weeks at room temperature
- CO<sub>2</sub>-loaded material controls pH of algal cultures and retains loading capacity over cycling
- We have scaled our benchtop algal cultures from 0.5L to 8L and tested ability of the material to deliver CO<sub>2</sub> and control pH

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