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First computer mouse



Created "Siri" for i-phone



Engineering-Scale Demonstration of the Mixed-Salt Process (MSP) for CO₂ Capture

DOE Contract: DE-FE0031588

Presented by: Indira Jayaweera, Sr. Staff Scientist and Sr. Program Manager

SRI International

333 Ravenswood Ave.

Menlo Park CA 94025



August 26-30, 2019 • Convention Center • Pittsburgh, Pennsylvania

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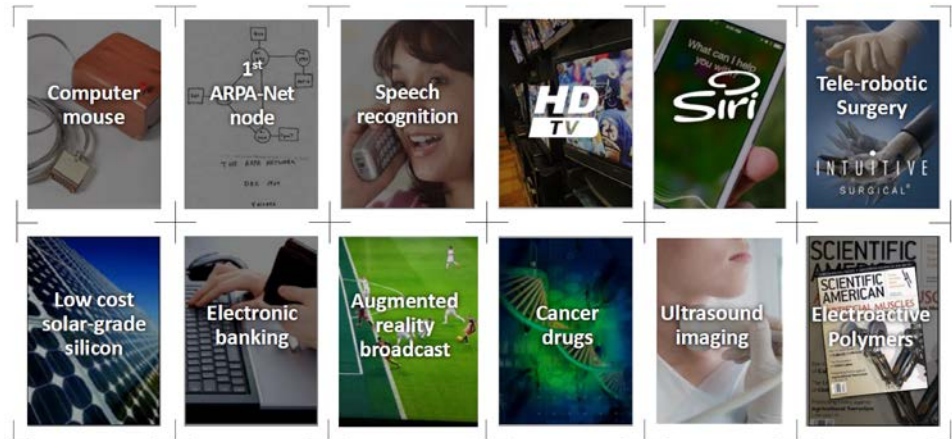
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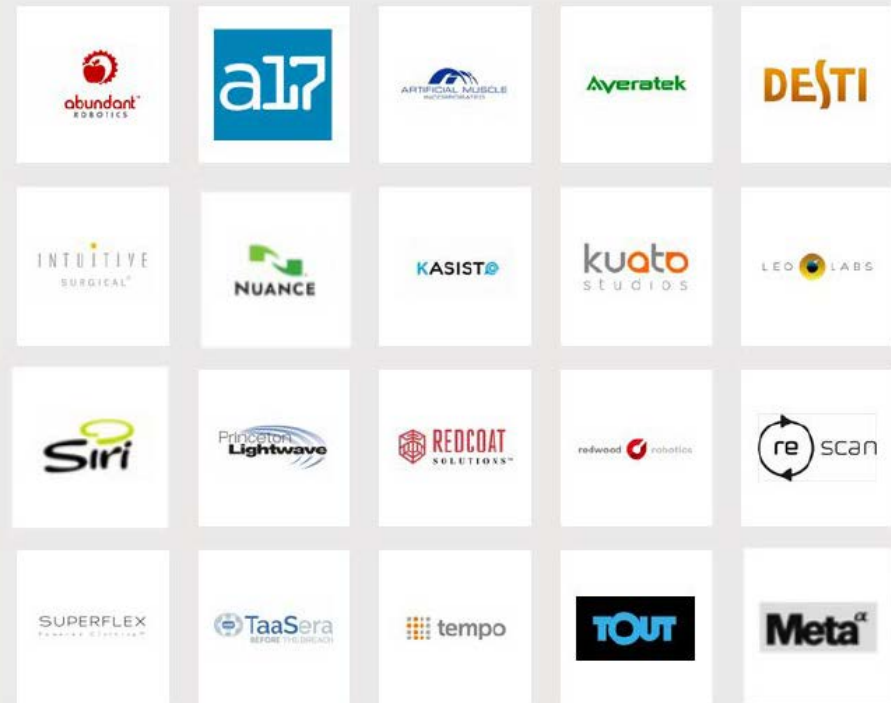
In 2017, we launched 7 startups and they raised **over \$60 million**.

In 2018, we launched 7 successfully-funded startups

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Portfolio Companies





Project Background and Technology

CAP Plant at Technology Center Mongstad (TCM)



MSP engineering demonstration at TCM is a critical step in the road map to scale-up

Source: https://www.norskipetroleum.no/wp-content/uploads/TCM_Mongstad_foto_Helge_Hansen_Statoil_1440_480-1440x480-c-default.jpg

Project Objectives

(DOE Contract: FE0031588)

- Perform integrated MSP testing at engineering scale for long-term periods under dynamic and continuous steady-state conditions with a real flue gas stream to address concerns relating to scale-up and integration of the technology to coal-based power plants;
- Operate the MSP with advanced heat integration to improve the process efficiencies;
- Study the solvent and water management strategies; and
- Collect critically important data for a detailed techno-economic analysis (TEA) and for further process advancements to reach the DOE's goal of \$30/tonne of CO₂ by 2030.

Key Focus:

- (1) Process optimization, energy efficiency, chemical consumption and low emissions
- (2) Dynamic and steady-state operations

Project Team

DOE Project Manager: Andrew Jones

Prime Contractor: SRI International

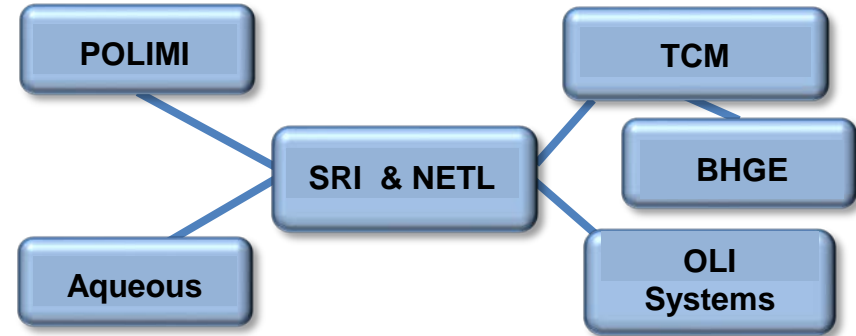
Project Team: US and International Partners

Project Value: ~ \$22 M

(DOE funding: \$13 M and TCM in-kind cost-share: \$9 M)

Period of Performance: 7/1/18 to 7/31/21

- TASK 1.0 (BP1, BP2 & BP3) - Project Management and Execution
- Task 2 (BP1) - Detailed investigation of required changes to the TCM CAP Plant to run MSP
- TASK 3.0 (BP2) - Re-commissioning of the CAP Pilot at TCM
- TASK 4.0 (BP2) - System Modification, Modeling and Initial Testing
- TASK 5.0 (BP3) - Dynamic and Steady-state Testing of MSP
- TASK 6.0 (BP3) - Process Economics, Technology Gaps and Technology Maturation
- TASK 7.0 (BP3) - Environmental, Health and Safety (EH&S) Assessment
- TASK 8.0 (BP3) - Pilot plant shutdown and Project Closure



Work Organization

SRI International

- Technology provider

Technology Center Mongstad (TCM), Norway

- Host site and cost-share partner

Baker Hughes, a GE company (BHGE), Norway

- Process HAZOP

OLI Systems, USA

- Process modeling

Aqueous Systems Aps, Denmark

- Thermodynamic modeling

POLIMI, Italy

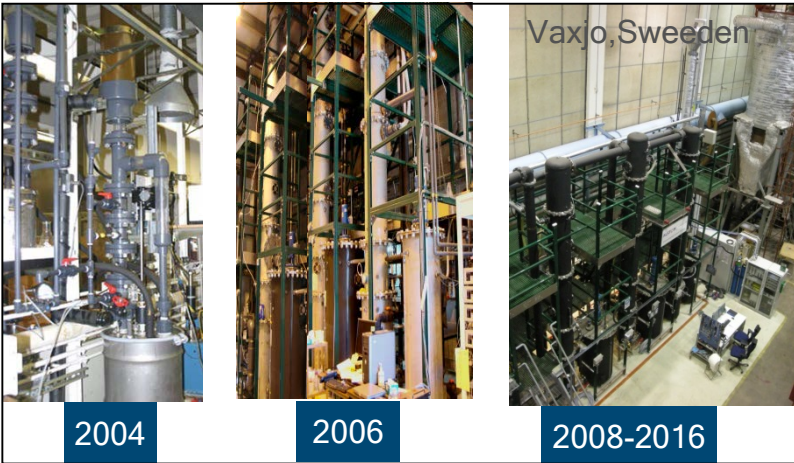
- Techno-economic analysis

MSP Developments

Small bench to mini-pilot to large pilot

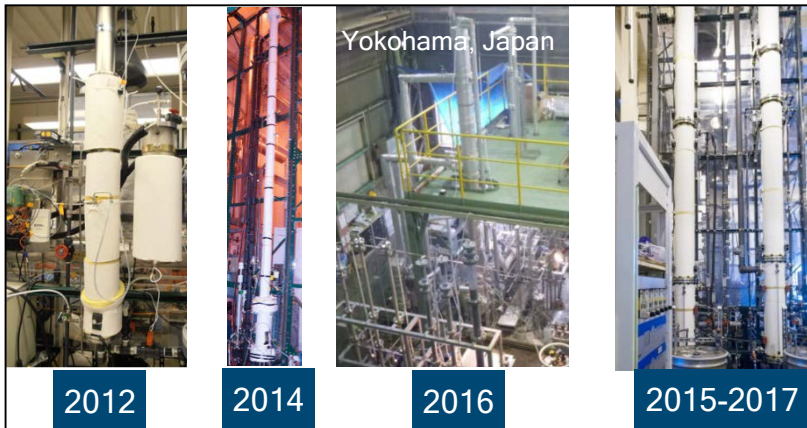
Ammonia technology development started at SRI in 2004

Chilled Ammonia Process (CAP)



CAP Validation at TCM

Mixed-Salt Process (MSP)



MSP Testing at TCM
DE-FE0031588

Step change



MSP scale-up development was funded by DOE under DE-FE0012959
MSP proof of concept development was funded by IHI, Japan

Mixed-Salt Process (MSP)

How it works:

Selected composition of potassium carbonate and ammonium salts

- Overall heat of reaction 35 to 60 kJ/mol (tunable)
- Excellent solvent physical properties

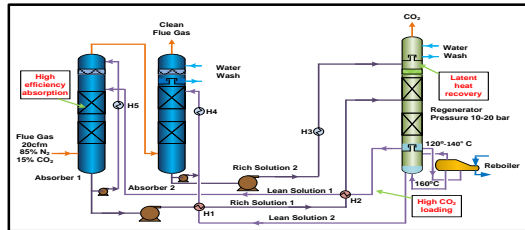
Absorber operation at 20° - 40° C at 1 atm with 30-40 wt.% mixture of salts

Regenerator operation at 120° - 160° C at 10-15 atm

- Produce high-pressure CO₂ stream

K₂CO₃-NH₃-CO₂-H₂O system

High CO₂ cycling capacity



Process Highlights:

- Reduced ammonia emissions
- Enhanced efficiency
- Reduced reboiler duty
- Reduced CO₂ compression energy

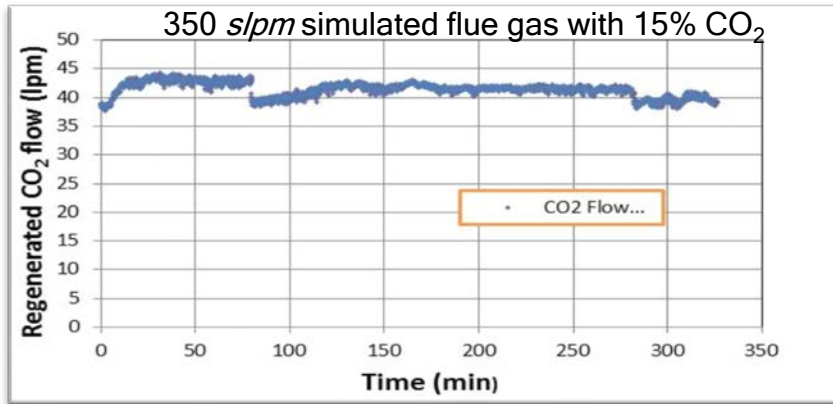
**A SIGNIFICANT PARASITIC POWER REDUCTION
COMPARED TO MEA !**



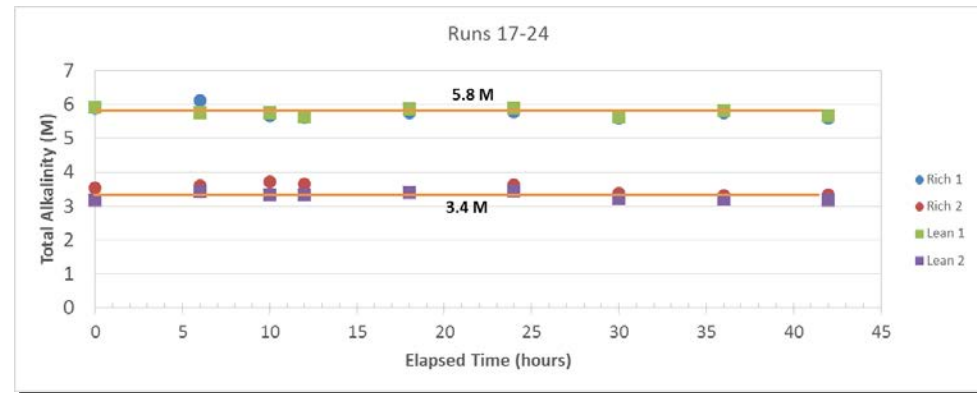
MSP Mini-pilot at SRI

Examples of Steady-State and Dynamic Testing of the Large Bench (mini-pilot)

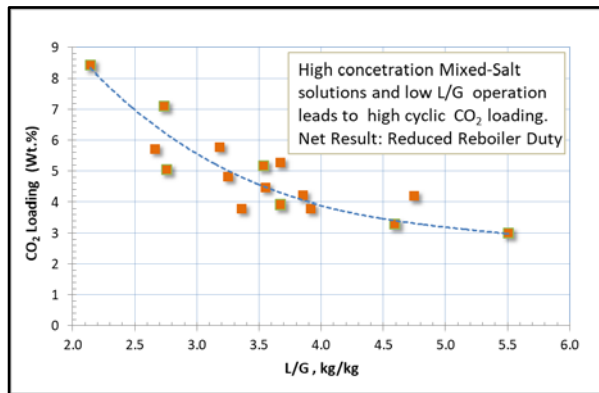
Results from FE0012959



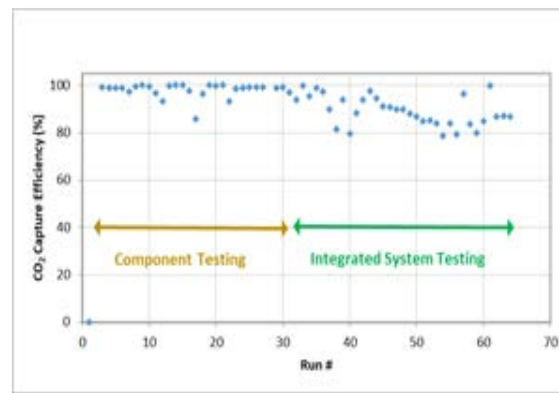
Observed 90% capture efficiency and regeneration with cyclic loading of ~0.7 mole of CO₂/mole of ammonia



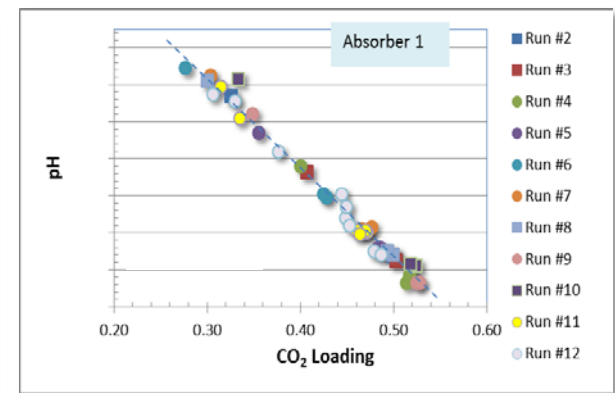
Alkalinity of rich and lean solutions circulating in the integrated system



Observed CO₂ loading as a function of L/G



CO₂ capture efficiency in parametric test runs



Observed pH as a function of CO₂ loading

Absorber: 20-35°C; Regenerator : 140°C; Reboiler: 160°C; L/G = 2 to 6 (kg/kg); Solvent composition: 5 to 8 m

MSP Summary and Benefits

Process Summary

- Uses inexpensive, industrially available material (potassium and ammonium salts)
- No chemical degradation
- Has the potential for easy permitting in many localities
- Uses known process engineering
- Accelerated development possible

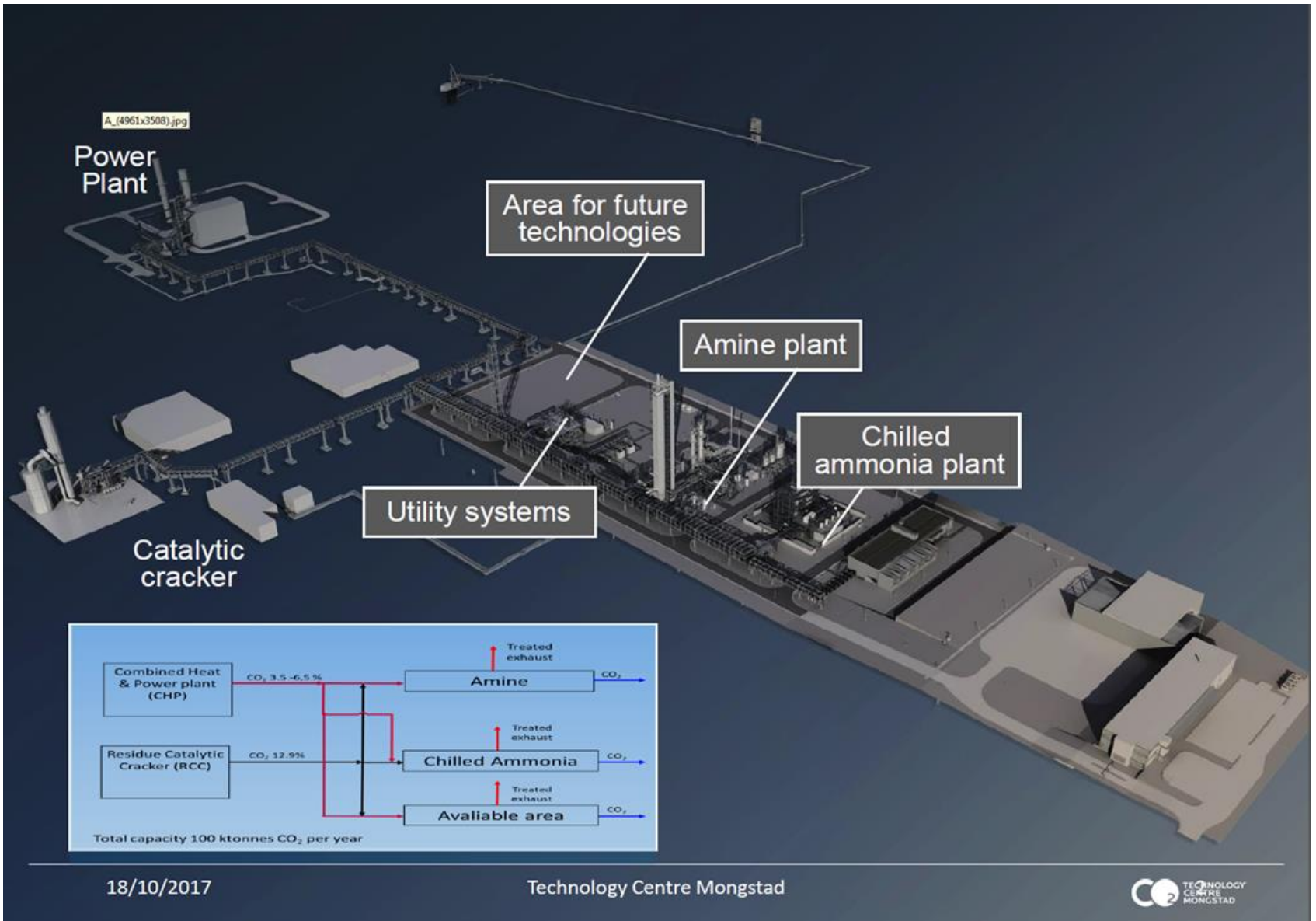


Demonstrated Benefits (By testing and modeling)

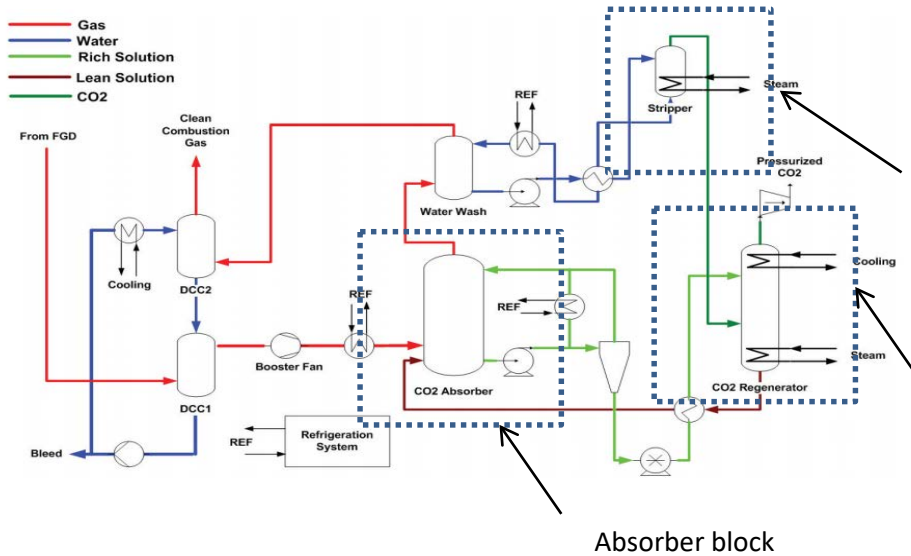
- Enhanced CO₂ capture efficiency
- High CO₂-loading capacity
- High-pressure release of CO₂ (10-15 bar)
- Reduced energy consumption (~ 2 MJ/kg-CO₂)
- Reduced auxiliary electricity loads

Project Update

Plant View of TCM

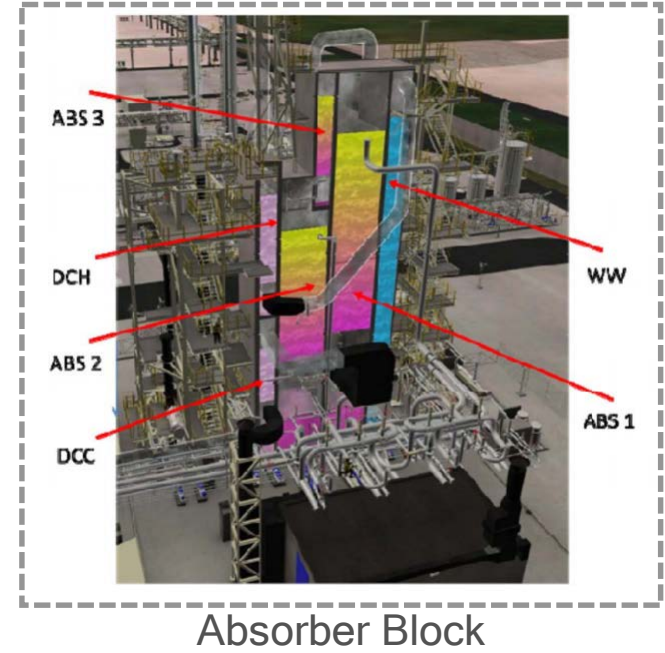


Existing CAP Infrastructure at TCM



Ammonia recovery block

Regenerator block



Process flow diagram of the as-built CAP system

Source: Energy Procedia 114 (2017) 5593 – 5615

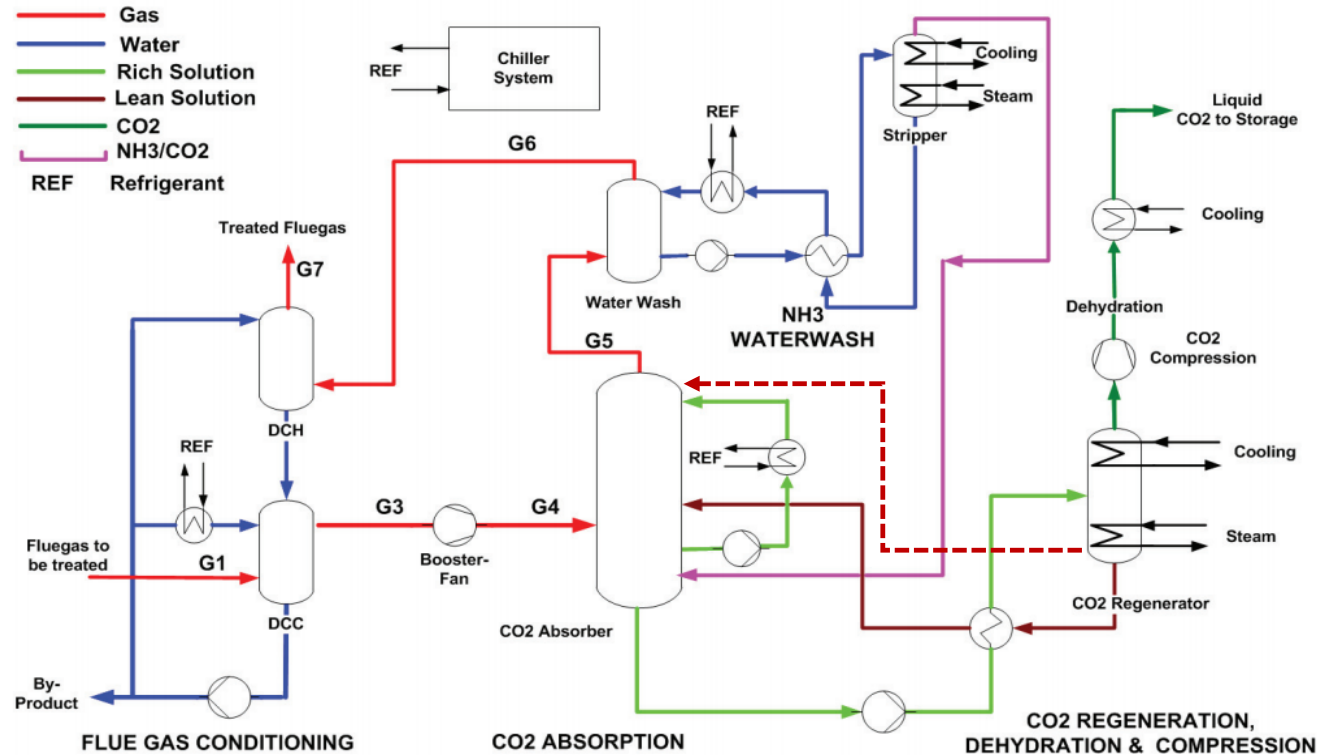


Regenerator and Ammonia Recovery Blocks

Source: Energy Procedia 51 (2014) 31 – 39

CAP System Modification

MSP testing will be in non-solid mode



----- New Piping to Demonstrate MSP

Non-Solid Mode Operation Flow Scheme

Key Modifications:

Absorber rearrangement (piping, valves etc.)

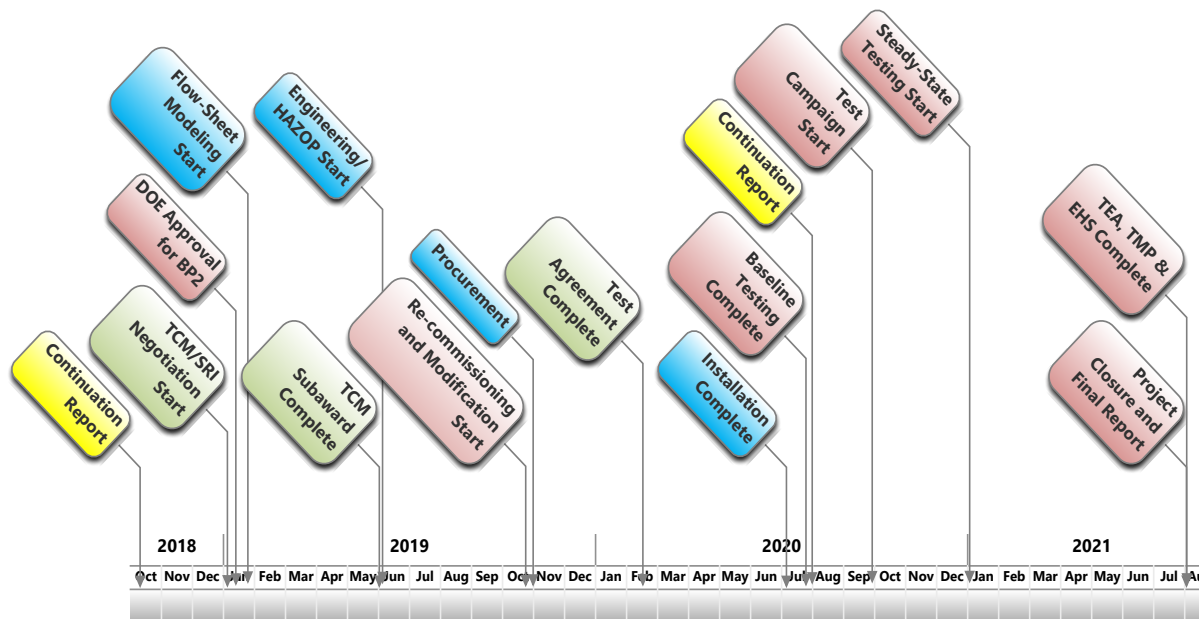
New lean transfer line from regenerator to absorber (piping, valves etc.)

Project Timeline

For system recommission, modification and testing

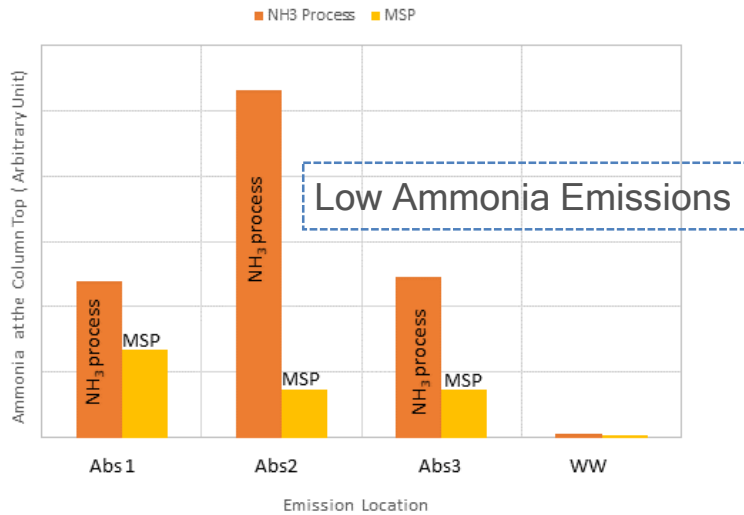
Completed or Ongoing Activities:

- Contract Negotiation Phase 1 ✓
- Prep work for recommission - system investigation ✓
- Contract Negotiation Phase 2 ✓
- Prep Work and Engineering for Modification (in progress)
- Flow-sheet modeling ✓
- HAZOP (in preparation)

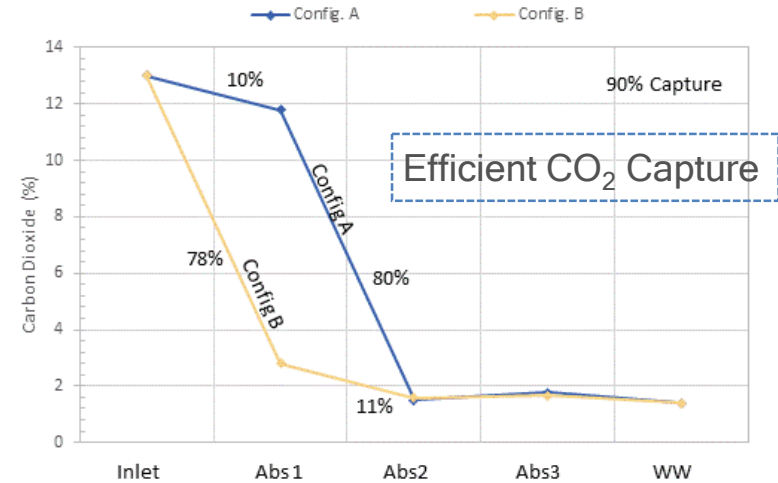


Selected Results from Flowsheet Modeling

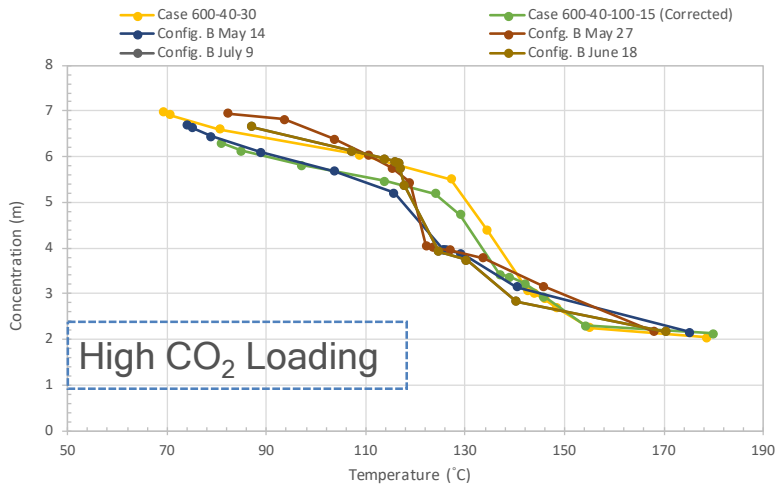
Comparison of Ammonia Emissions



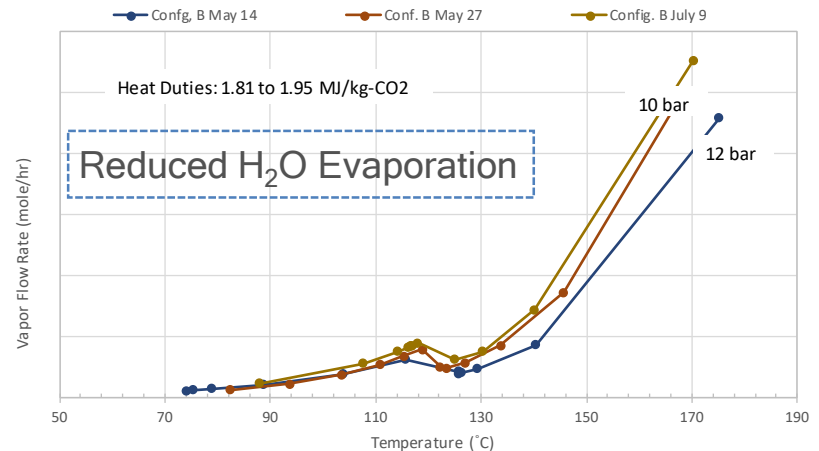
Comparison of CO₂ Removal Efficiencies



Regenerator Dissolved CO₂ Concentrations

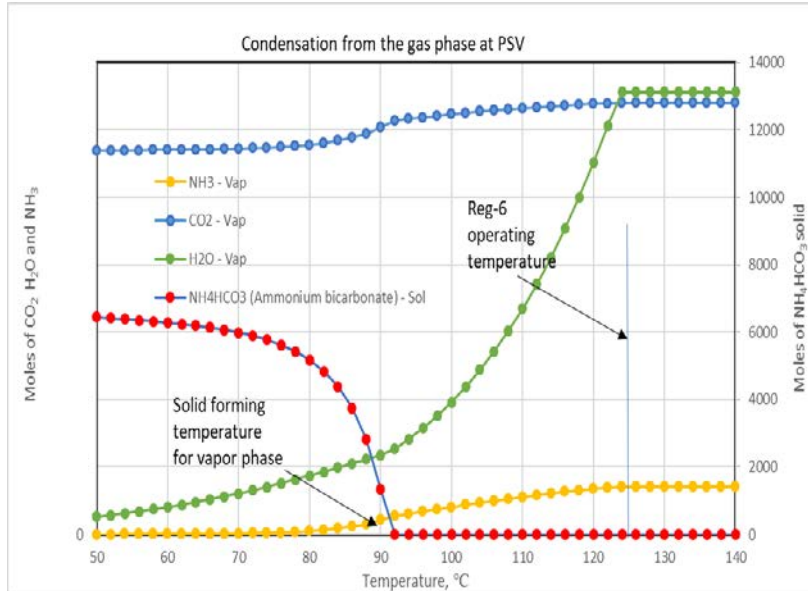


Regenerator H₂O Vapor Emissions

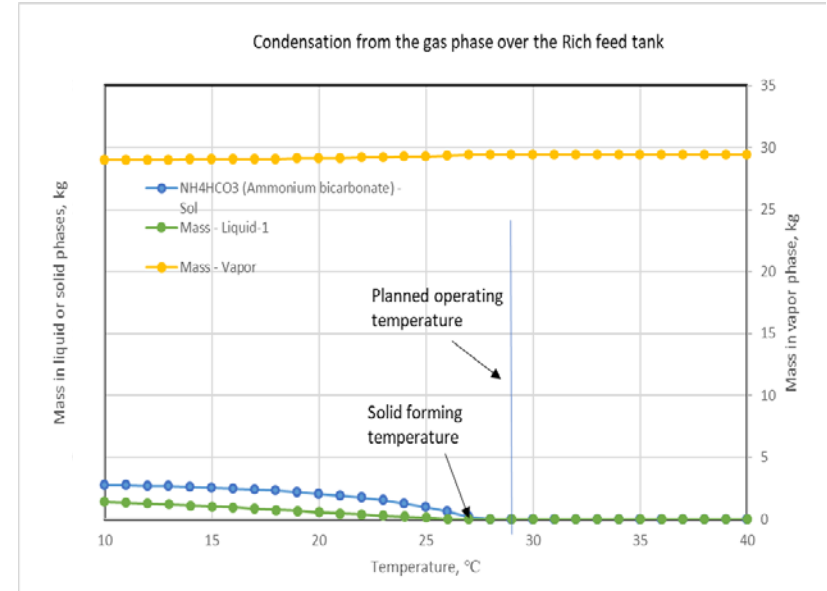


Selected Results from VLE Modeling

E.g., Crystallization risk avoidance by modeling the speciation of the vapor condensation



Solid formation behavior rich solution stream assuming a N_2 headspace such as in a PSV

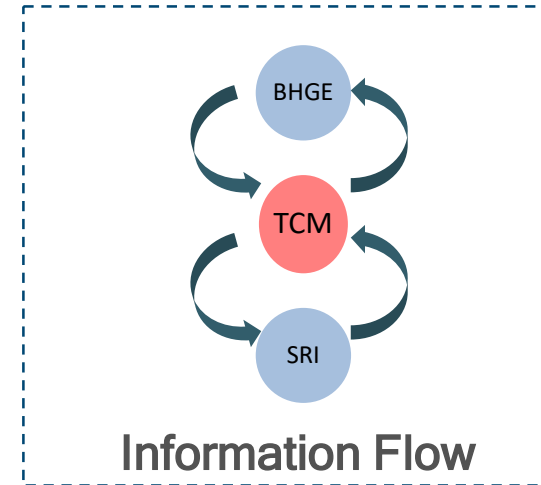


Solid formation temperature for the headspace gas in the Rich Feed tank

Current Tasks (HAZOP related)

Subtasks 3.2 & 4.1

- Document exchange and skype meetings
- Document review
- 2 Day HAZOP (starting 9/10/2019)
- Definitize the modification
- TCM board approval



Next Tasks

Subtasks 3.1 & 4.2

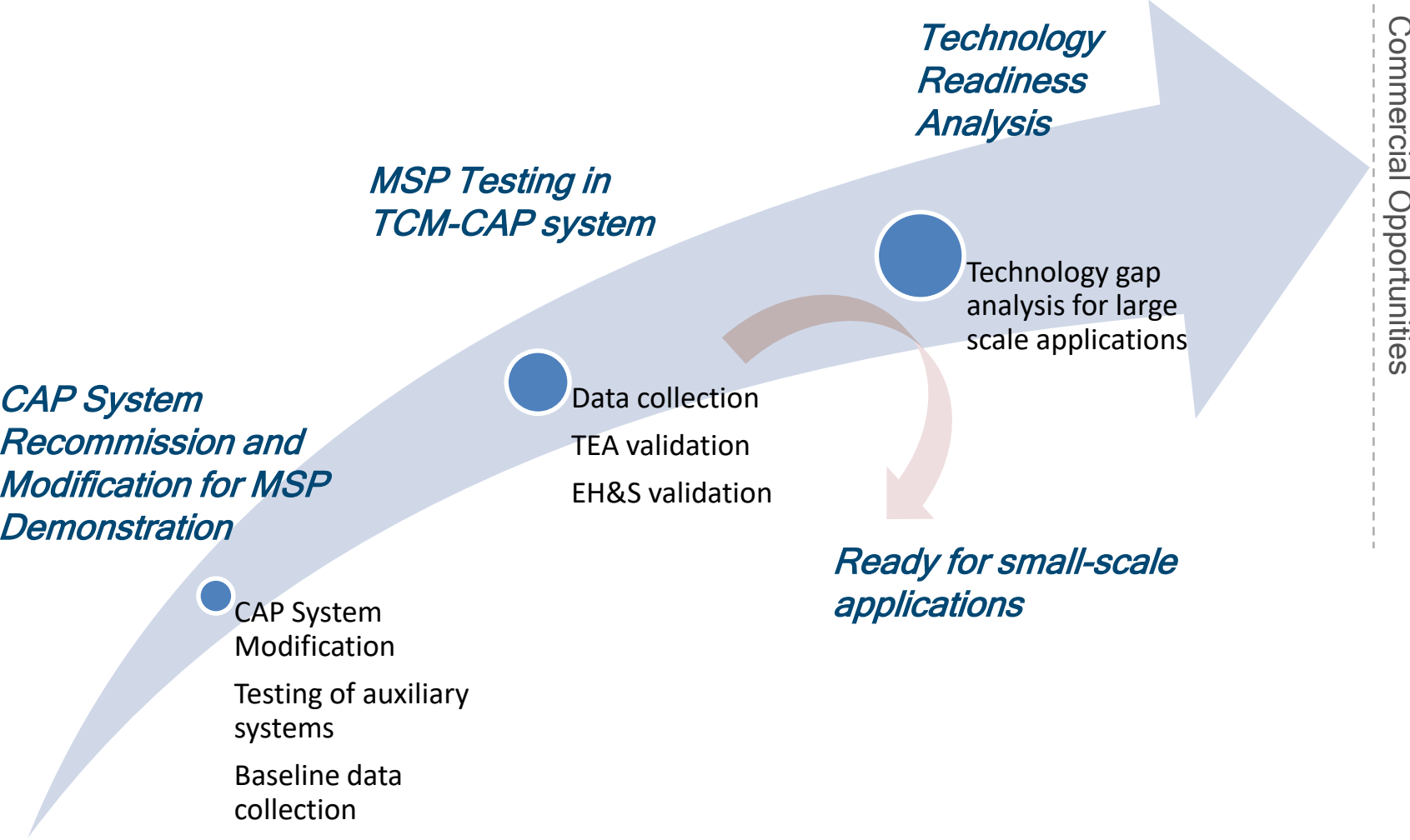
- CAP system recommissioning
- CAP system modification (procurement and fabrication)

Selected Project Milestones

BP	Task/ Subtask No.	Milestone Description	Planned Completion	Actual Completion	Verification Method
1	1	a. Updated PMP submitted	8/3/2018	8/3/2018	PMP file
1	1	b. Kickoff / BP1 Review Meeting convened	10/3/2018	10/2/2018	Presentation file
1	2	c. Work scope and firm cost estimate for the Chilled Ammonia Plant (CAP) recommissioning submitted	9/30/2018	10/12/2018	BP2 Continuation Application
1	1	e. Technology Maturation Plan	9/30/2018	9/26/2018	Topical Report
2	1	f. Updated PMP submitted	12/31/2018	12/18/2018	PMP file
2	3.1	g. Completion of CAP system recommissioning.	11/27/2019		RPPR quarterly
2	1	h. Test Site Agreement with TCM	11/27/2019		Agreement documents
2	4.5	i. Completion and submission of the test plans for both dynamic and steady state testing.	5/30/2020		RPPR quarterly
2	4.4	j-ii. Completion of CAP system modification.	5/30/2020		RPPR quarterly
2	4.4	j-iii. Completion of initial testing. Systems operability with regenerator at 10 bar and ammonia recovery [from the sour stripper] at >50% demonstrated.	5/30/2020		RPPR quarterly
3	5.1-5.2	l. Completion of dynamic testing and data analysis.	12/31/2020		RPPR quarterly
3	5.4-5.5	m. Completion of the steady-state testing and data analysis.	5/30/2021		RPPR quarterly
3	6.1	n. Techno-Economic Analysis topical report submitted	7/31/2021		Topical Report and summary in Final Report

Note: Project milestones g to m will be updated after the HAZOP

Pathway Toward Testing MSP at TCM and Beyond



SRI has the patent coverage for MSP in US, Japan and Europe



Acknowledgements

Teams for Mixed-Salt Related Activities

NETL (DOE)

- Andrew Jones, Steven Mascaro, Jose Figueroa, Lynn Brickett, John Litynski and other NETL staff members

SRI Team

- Indira Jayaweera, Palitha Jayaweera, Elisabeth Perea, Regina Elmore, William Olsen, Chris Lantman, Kelli Connolly, Lisa Wottrich and Rene Harmount

Host Site

- TCM (Bjørn-Erik Haugan, Jorunn Brigsten, Kjetil Hantveit, Gerard Lombardo, Muhammad Ismail Shah, Stien Olav Nesse, Ronny Andvik and others)

HAZOP Team Partner

- BHGE (Gianluca Difederico, Olaf Stallmann, Erik Ullrich, Chris Schneider, Peter Strunz, Karsten Woitasky, and Michael Balfe)

Other Collaborators and Contributors

- OLI Systems (Ron Springer, Prodip Kondu and Andre Anderko)
- POLIMI (Davide Bonalumi, Stefano Lillia and Gianluca Valenti)
- Stanford University (Adam Brant and Charles Kang)
- Aqueous (Kaj Thomsen)
- IHI Corporation (Shiko Nakamura, Okuno Shinya, Kubota Nabuhiko, and others)

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Thank You!

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