

# Ammonia Combustion at Purdue

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Zander Hodge

Tristan Shahin

Rohan Gejji

Prof. Carson Slabaugh

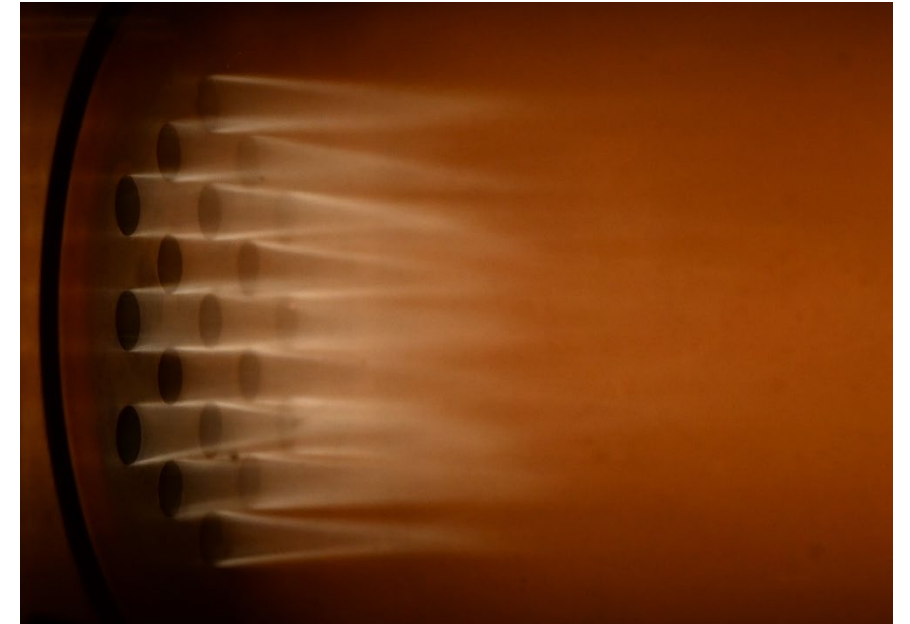
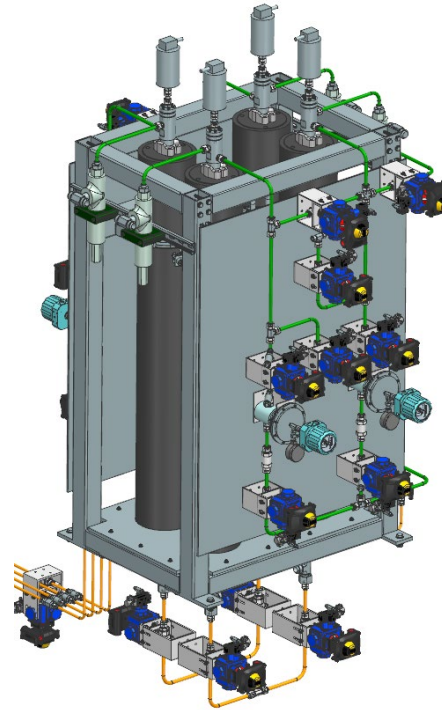
Prof. Robert Lucht

School of Aeronautics and Astronautics

School of Mechanical Engineering

Purdue University

West Lafayette, IN



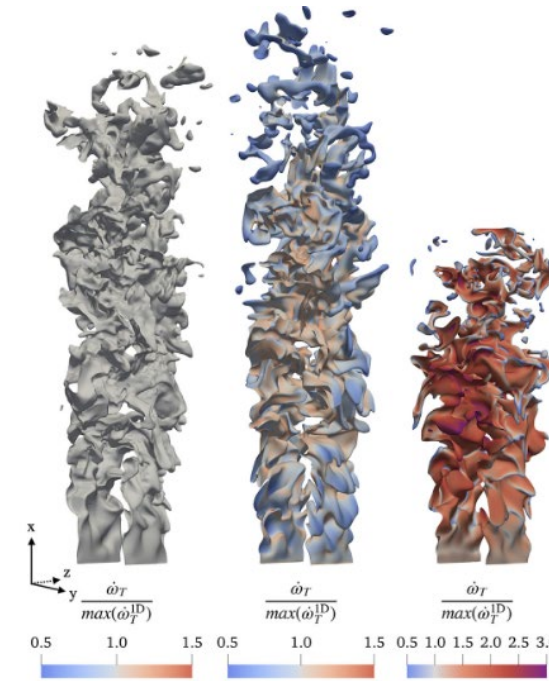
# Ammonia Combustion at Purdue

## Background

- Challenges with ammonia combustion (kinetics, emissions, etc.) motivates blending with other fuels like  $H_2$  or  $CH_4$
- Limited combustion investigations of these blended fuels at high pressure,  $Re$ , and  $P_{thermal}$

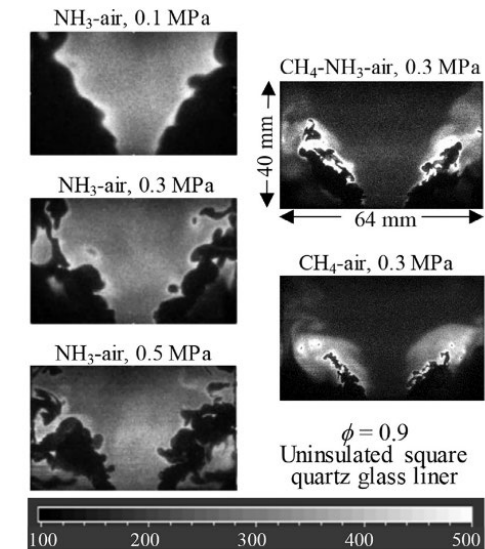
## Goals

- Develop a high-pressure ammonia storage system
  - Capable of liquid or gaseous injection
  - Large-scale storage capable of steady-state operation
- Conduct  $NH_3$ -blended combustion experiments at engine relevant conditions ( $P_4 \geq 10$  bar,  $T_3 \approx 750$  K)
  - Investigate impacts of fuel composition on combustion dynamics and emissions
  - Study flame structure and coupled behaviors under high turbulence



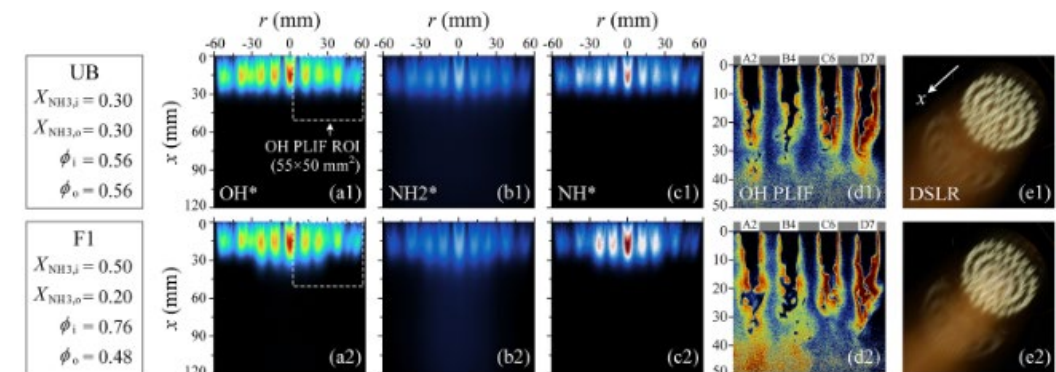
**Fig. 3.** Isosurfaces of  $c=c^*$ , retrieved at  $t=2\tau$  and colored by HRR normalized by the maximum value in the corresponding 1D unstretched laminar flame for all cases.  $CH_4$  case at  $c_{CH_4}^* = 0.72$  (left),  $NH_3-H_2$  case at  $c_{H_2O}^* = 0.78$  (center),  $H_2$  case at  $c_{H_2}^* = 0.85$  (right). (For interpretation of the references to color in this figure, the reader is referred to the web version of this article.)

[Coulon et al. 2023](#)



**Fig. 2.** OH-PLIF images of the swirl stabilized premixed flames in the uninsulated square-shaped liner.

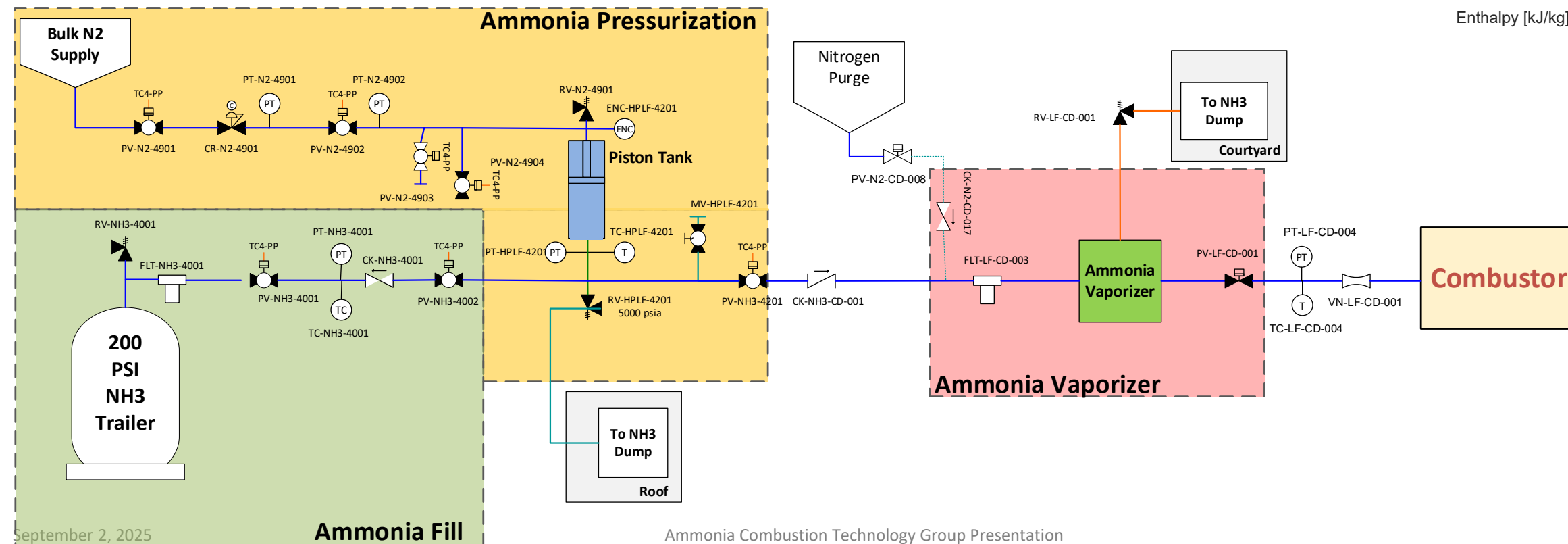
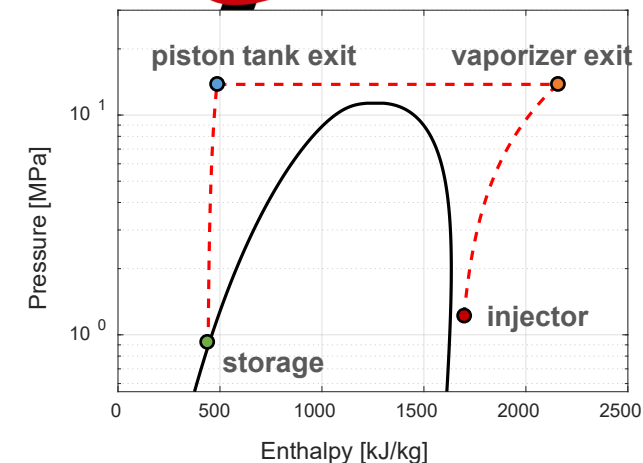
[Okafor et al. 2021](#)



[Jin and Kim 2024](#)

# Ammonia System Overview

- Ammonia filled into piston tank as saturated liquid
- Liquid ammonia delivered from piston tank to vaporizer
  - Linear encoder provides position feedback from piston
- Gaseous ammonia flowrate metered using critical flow venturi nozzle

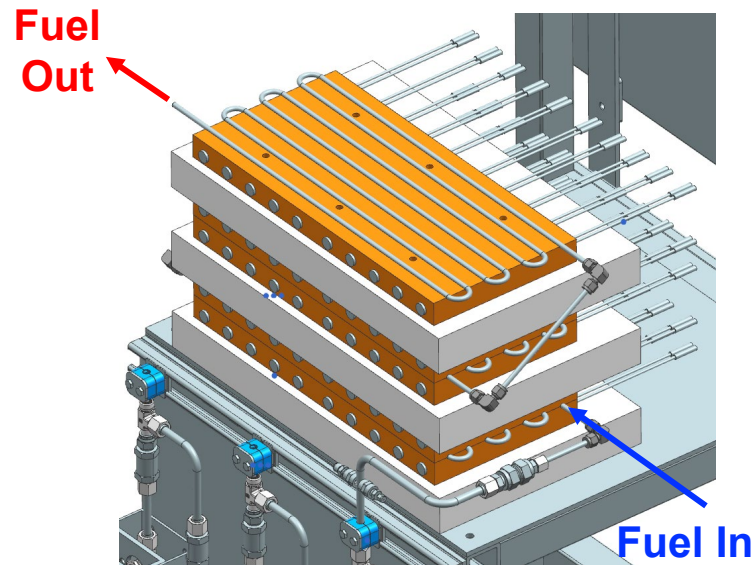




# Ammonia System Specifications



- 4 piston tanks, total of 115 liter storage up to 350 bar
- Accumulators capable of running individually or in parallel
- Ethylene propylene rubber (EDPM) or PTFE used for all elastomeric sealing
- Dump barrels filled with water + antifreeze
- 54 kW electrically heated ammonia vaporizer
- Lines from vaporizer outlet to experiment wrapped in heat tape



Linear encoders

NH<sub>3</sub> tanks

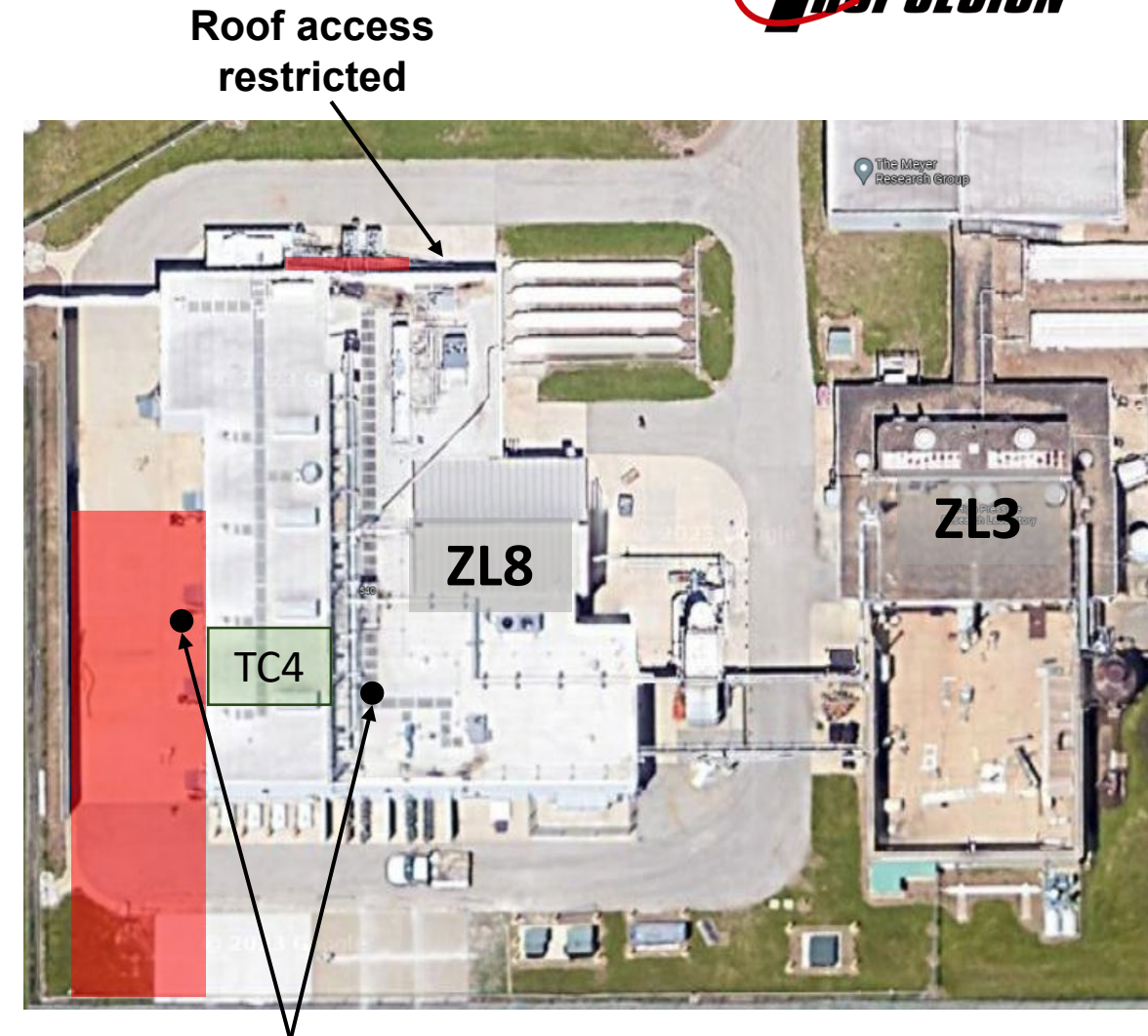
N<sub>2</sub> relief valves

N<sub>2</sub> supply circuit

NH<sub>3</sub> supply & relief valves (below)

# Safety and Detection

- All filling operations performed remotely
- 4 x ammonia gas sensors (0 – 75 PPM full-scale) located throughout test cell
- Restricted areas prevent access up to 20 ft minimum
- Full PPE required for all handling of ammonia



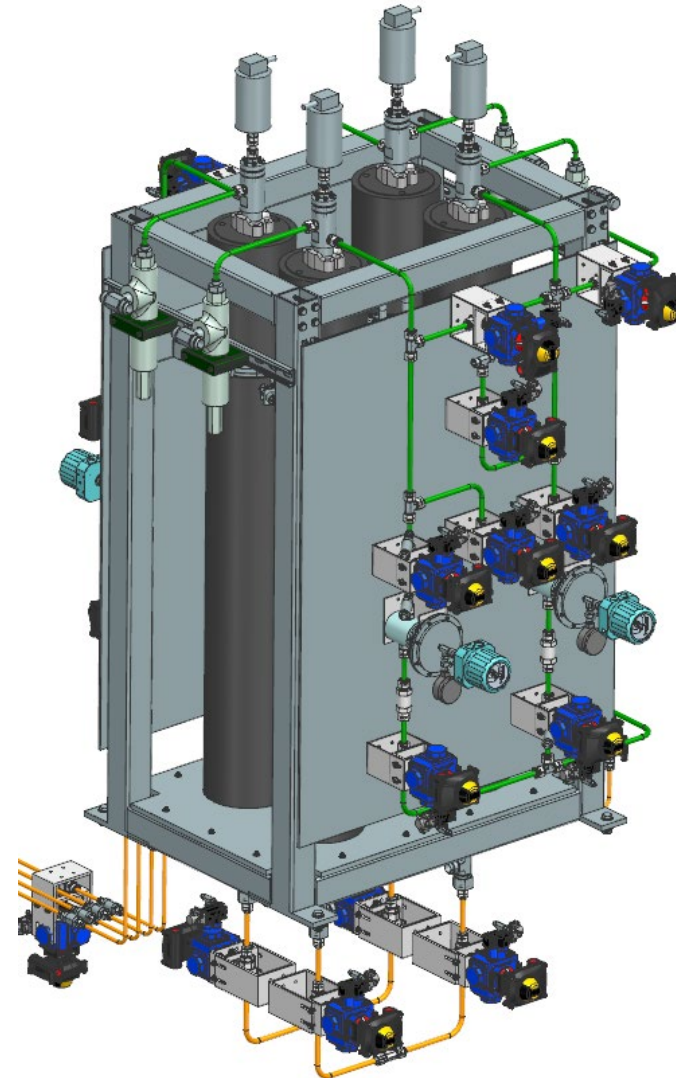
**Ammonia Release  
Barrel Locations**



# Ammonia System Lessons Learned



- Filling behavior dependent on ambient conditions
  - Lower temperature means less  $\Delta P$  for filling
- Significant heating required to vaporize ammonia
  - High latent enthalpy of vaporization
  - Joule Thompson cooling during expansion
- Careful consideration of trapped liquid volumes
  - $\frac{dP_{vap}}{dT}$  is large near ambient conditions
  - Thermal expansion
- Lab goggles or full-mask respirators recommended for ammonia handling
- Human detection limit often lower than sensors
  - Easy to tell if concentration is rising well before it becomes dangerous



# Experiment Methodology

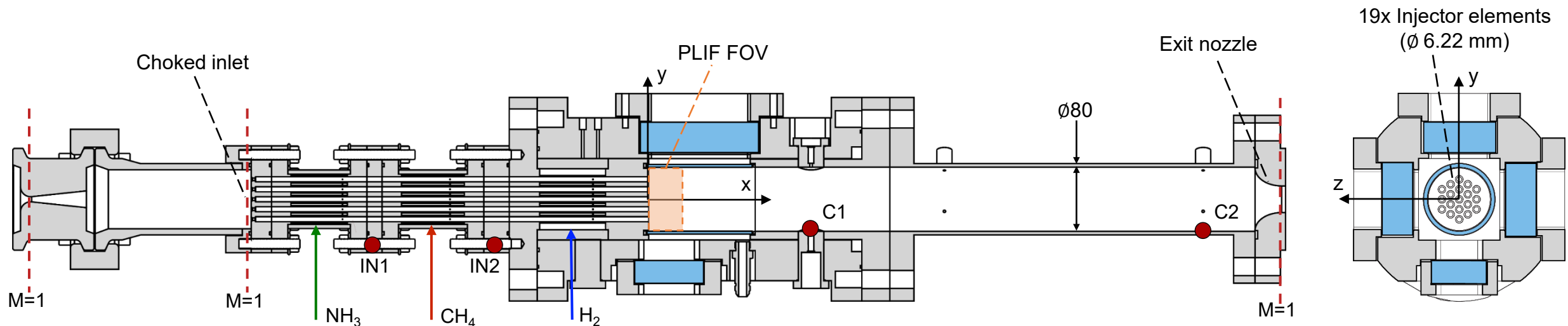
- 0.7 MW high pressure (~10 bar) optically accessible combustion chamber
- Canonical combustor configuration with well defined acoustic boundaries suitable for model validation
- Explore flame structure and dynamics with hydrogen, ammonia, and mixtures of these fuels with methane
- Premixed multi-stage, multi-tube, micromix ( $M^3$ ) injector
  - $Re_{inj} \approx 150000$

## Fuel Composition

$$x \left[ \eta \left( \frac{3}{2} H_2 + \frac{1}{2} N_2 \right) + (1 - \eta) NH_3 \right] + (1 - x) CH_4$$

$x$  = hydrogen fraction

$\eta$  = ammonia decomposition efficiency



# Micromixer Flame Structure

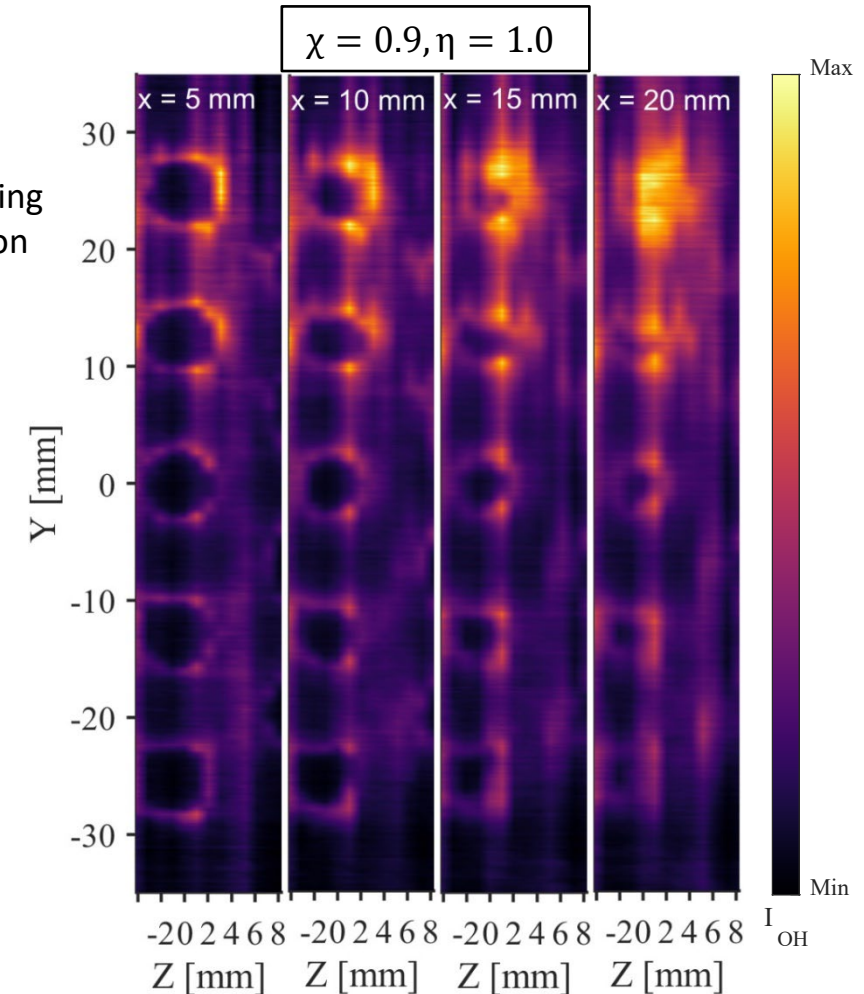
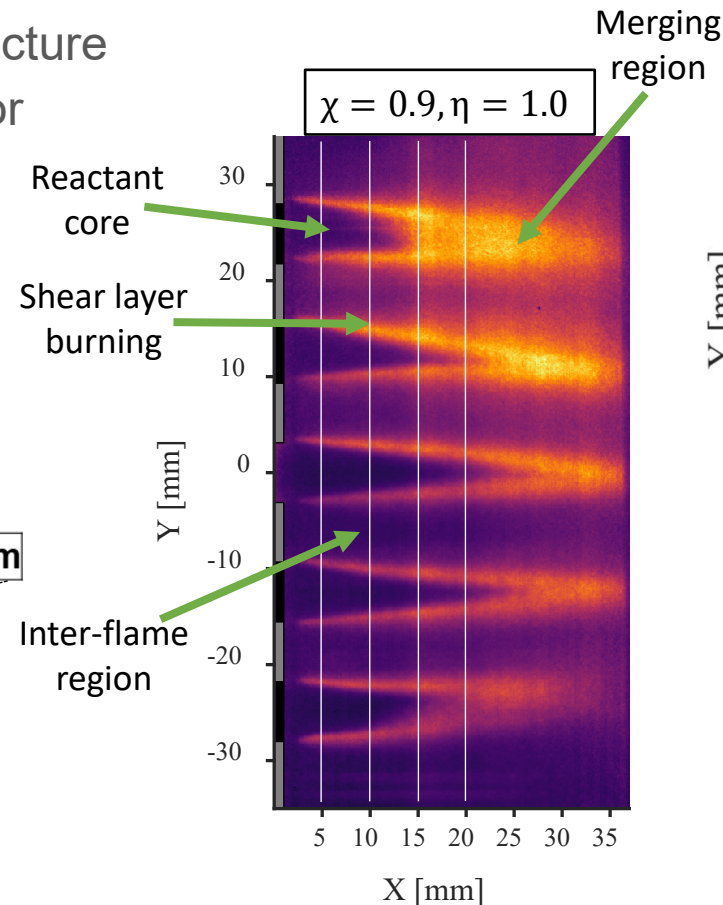
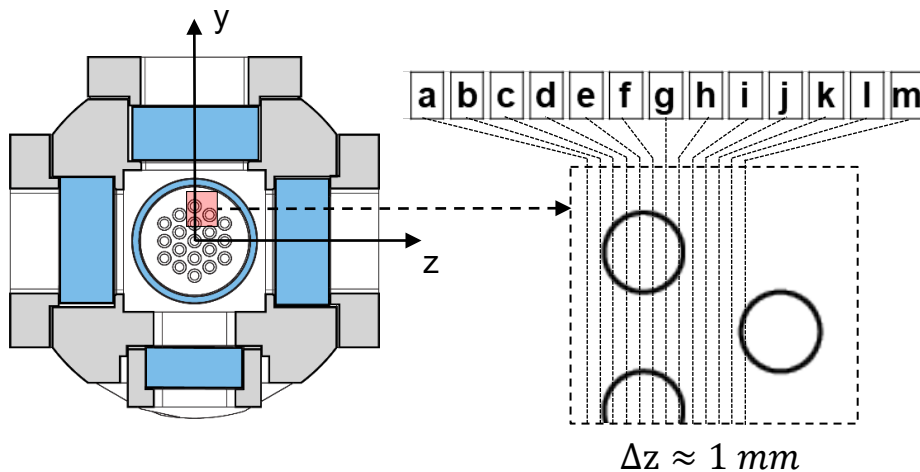
- 100 kHz planar laser-induced fluorescence of OH performed using burst mode laser
  - Time-resolved flame structure imaging
  - Time-average shows prominent features
- Multi-plane imaging reveals 3D flame structure
  - Reactions occur through entire injector circumference on average

## Fuel Composition

$$\chi \left[ \eta \left( \frac{3}{2} \text{H}_2 + \frac{1}{2} \text{N}_2 \right) + (1 - \eta) \text{NH}_3 \right] + (1 - \chi) \text{CH}_4$$

$\chi$  = hydrogen fraction

$\eta$  = ammonia decomposition efficiency



Hodge et al., "Time-Resolved Structure of H<sub>2</sub>-NH<sub>3</sub> and H<sub>2</sub>-CH<sub>4</sub> Flames in a High-Pressure Micromix Combustor," *International Journal of Hydrogen Energy*, Vol. 163, 2025, p. 150596. <https://doi.org/10.1016/j.ijhydene.2025.150596>



# Effect of CH<sub>4</sub> Addition

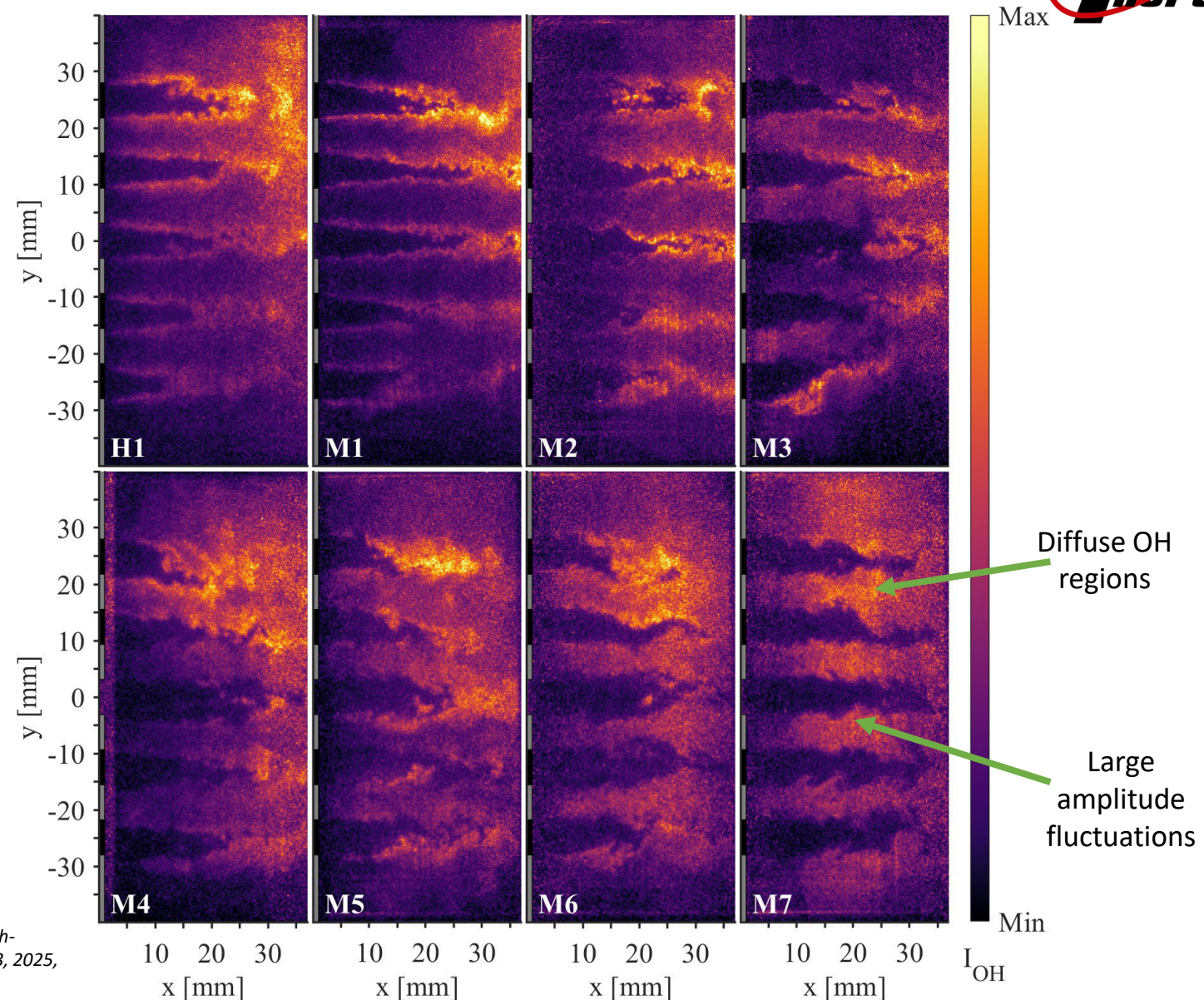
- H<sub>2</sub> flame has a compact, highly curved flame front
- Reactivity and flame speed decreases with CH<sub>4</sub>
- Distribution of OH is more diffuse
- Reactant core angle increases
- Flame wrinkling length scale increases
- OH broadens out to inter-flame region

## Fuel Composition

$$\chi \left[ \eta \left( \frac{3}{2} \text{H}_2 + \frac{1}{2} \text{N}_2 \right) + (1 - \eta) \text{NH}_3 \right] + (1 - \chi) \text{CH}_4$$

$\chi$  = hydrogen fraction

$\eta$  = ammonia decomposition efficiency



Hodge et al., "Time-Resolved Structure of H<sub>2</sub>-NH<sub>3</sub> and H<sub>2</sub>-CH<sub>4</sub> Flames in a High-Pressure Micromix Combustor," *International Journal of Hydrogen Energy*, Vol. 163, 2025, p. 150596. <https://doi.org/10.1016/j.ijhydene.2025.150596>



# Effect of NH<sub>3</sub> Addition

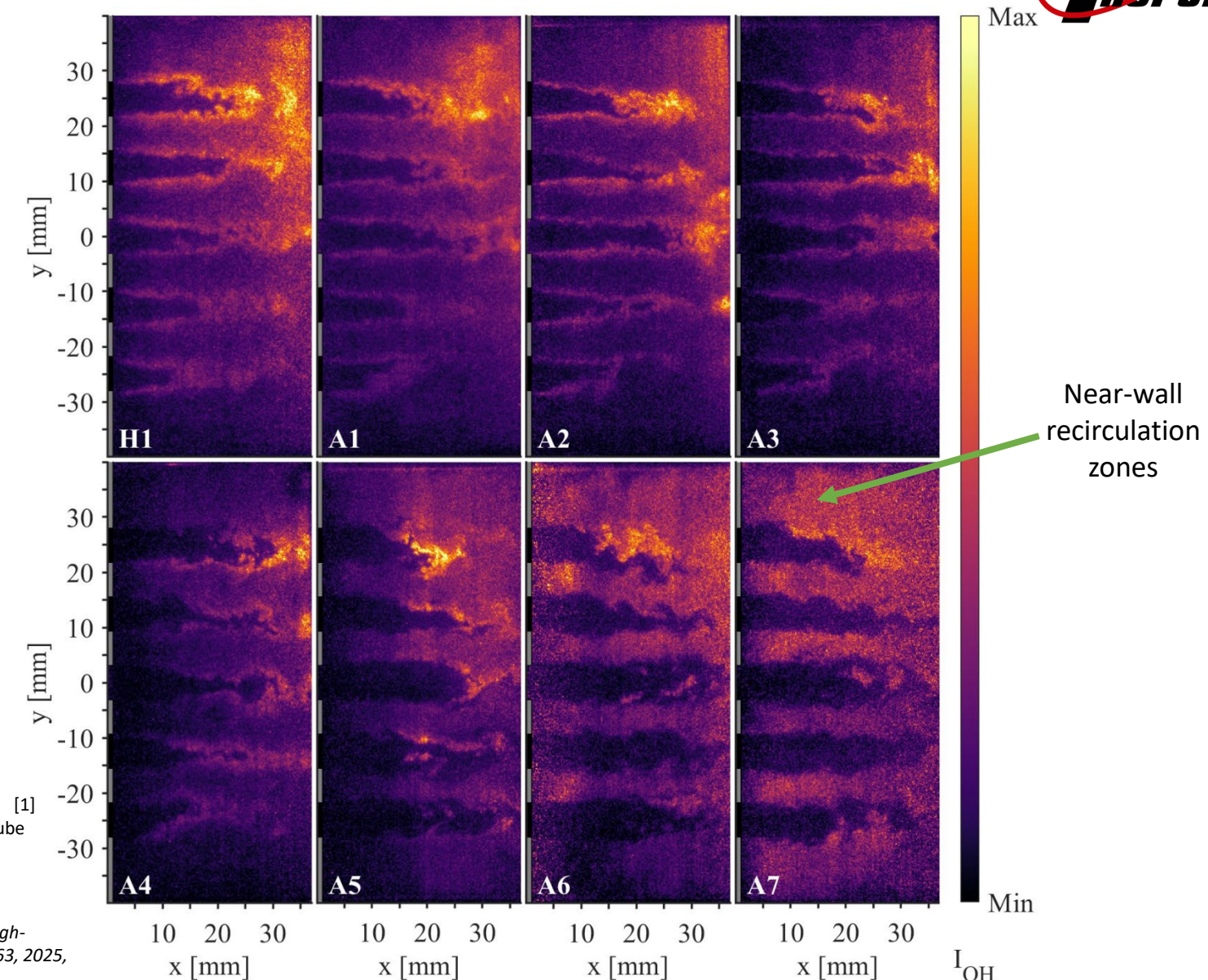
- OH regions are more diffuse compared to CH<sub>4</sub> addition
- Reactant core length increases significantly
- Global decrease in OH
- Significant disparity in reactant core length
  - Highlights presence of near-wall recirculation zones<sup>1</sup>

## Fuel Composition

$$\chi \left[ \eta \left( \frac{3}{2} \text{H}_2 + \frac{1}{2} \text{N}_2 \right) + (1 - \eta) \text{NH}_3 \right] + (1 - \chi) \text{CH}_4$$

$\chi$  = hydrogen fraction

$\eta$  = ammonia decomposition efficiency



[1]

[1] Zhang et al., "Three-Dimensional Analysis of Hydrogen Fuel Effects in Multi-Tube Combustor," *Proceedings of the Combustion Institute*, Vol. 41, 2025, p. 105790.

<https://doi.org/10.1016/j.proci.2025.105790>

Hodge et al., "Time-Resolved Structure of H<sub>2</sub>-NH<sub>3</sub> and H<sub>2</sub>-CH<sub>4</sub> Flames in a High-Pressure Micromix Combustor," *International Journal of Hydrogen Energy*, Vol. 163, 2025, p. 150596. <https://doi.org/10.1016/j.ijhydene.2025.150596>

September 2, 2025

Ammonia Combustion Technology Group Presentation

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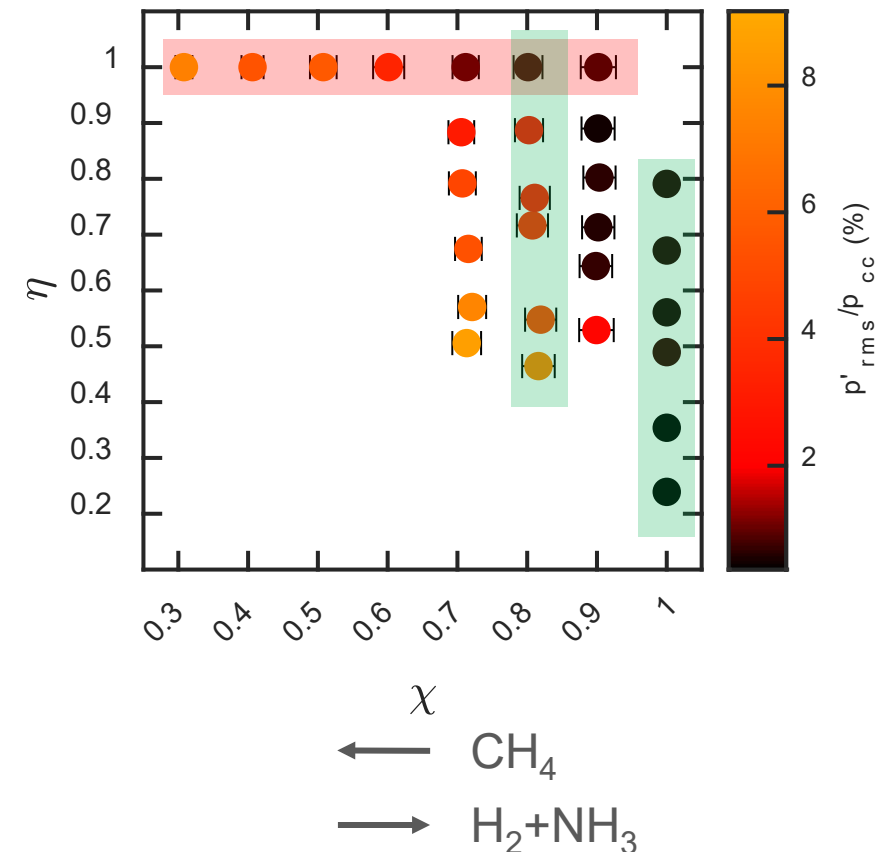
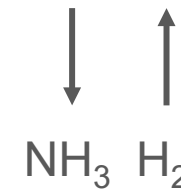
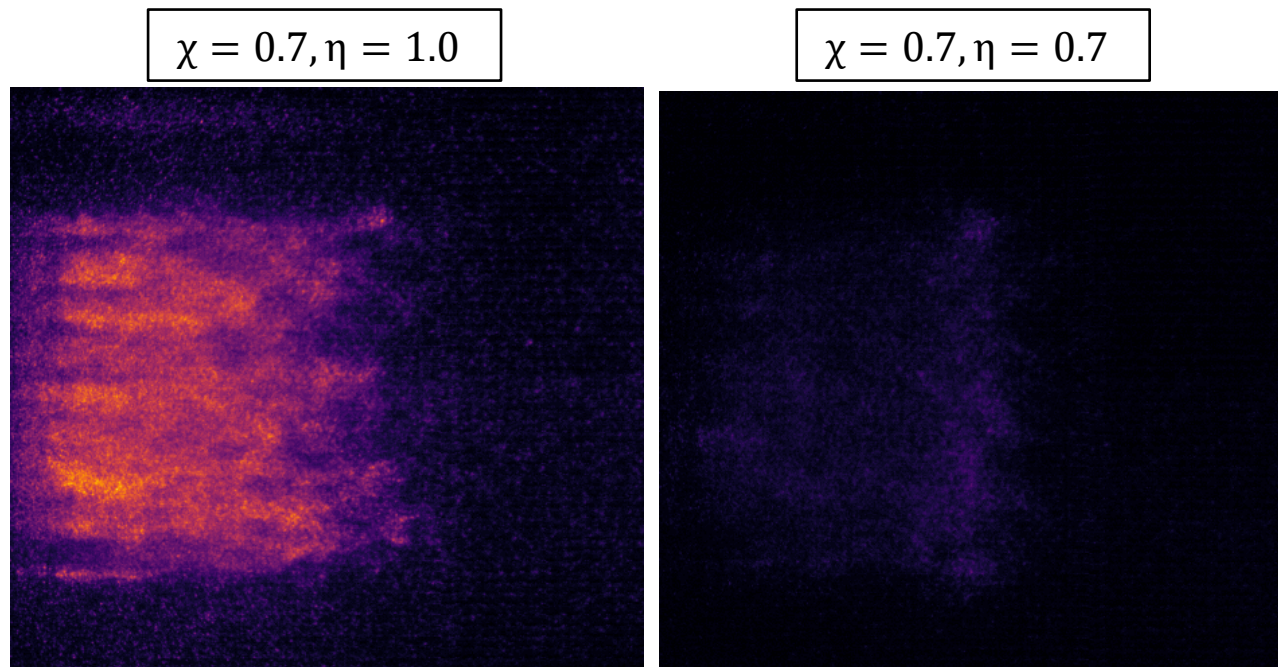
# Parametric Survey of Dynamics

- High amplitude pressure fluctuations ( $p'$ ) observed
  - Methane addition observed to promote combustion instabilities
  - Combustion instability amplitude is largely invariant to the addition of ammonia in absence of methane
  - As hydrogen content is decreased, ammonia addition increases combustion instability amplitudes

**Fuel Composition**

$$\chi \left[ \eta \left( \frac{3}{2} \text{H}_2 + \frac{1}{2} \text{N}_2 \right) + (1 - \eta) \text{NH}_3 \right] + (1 - \chi) \text{CH}_4$$

$\chi$  = hydrogen fraction  
 $\eta$  = ammonia decomposition efficiency

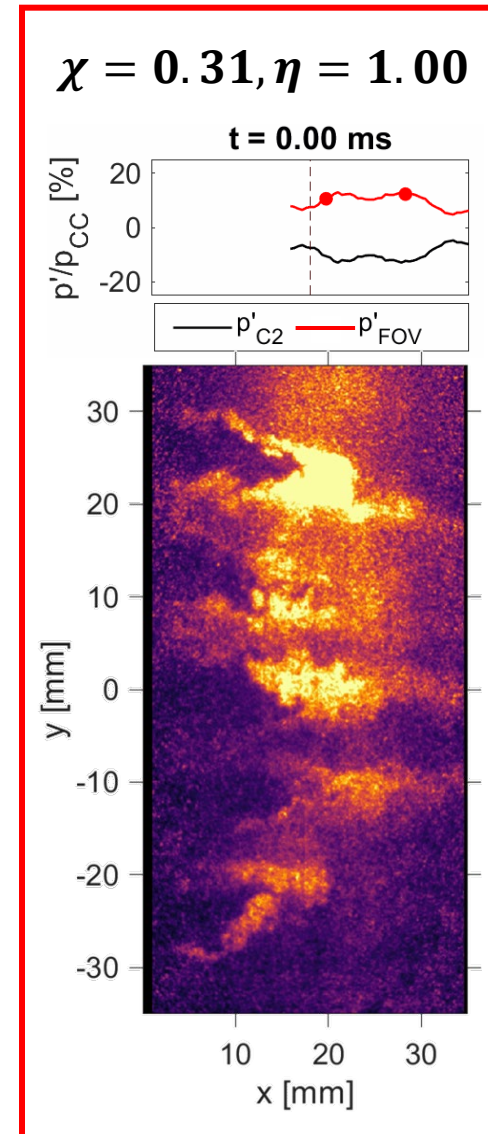
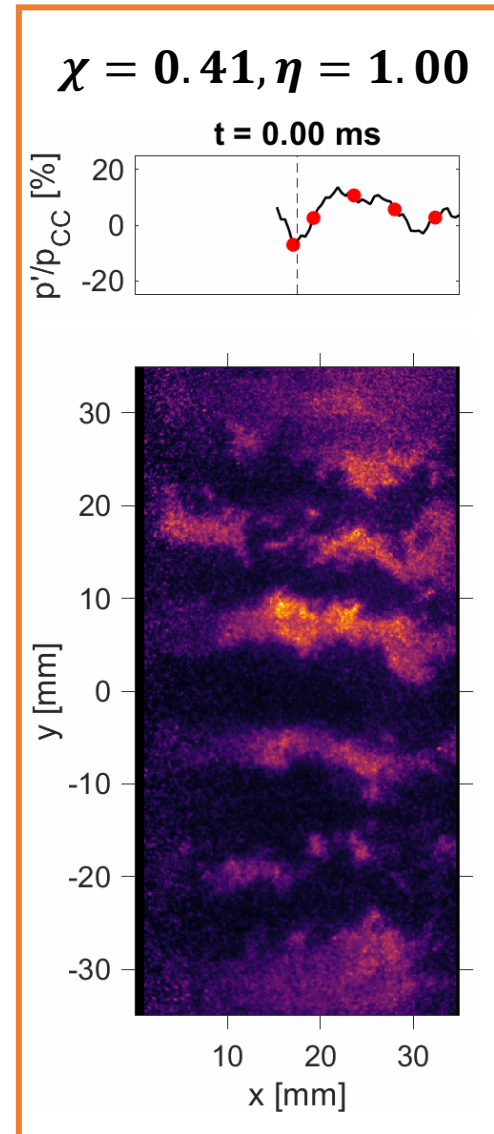
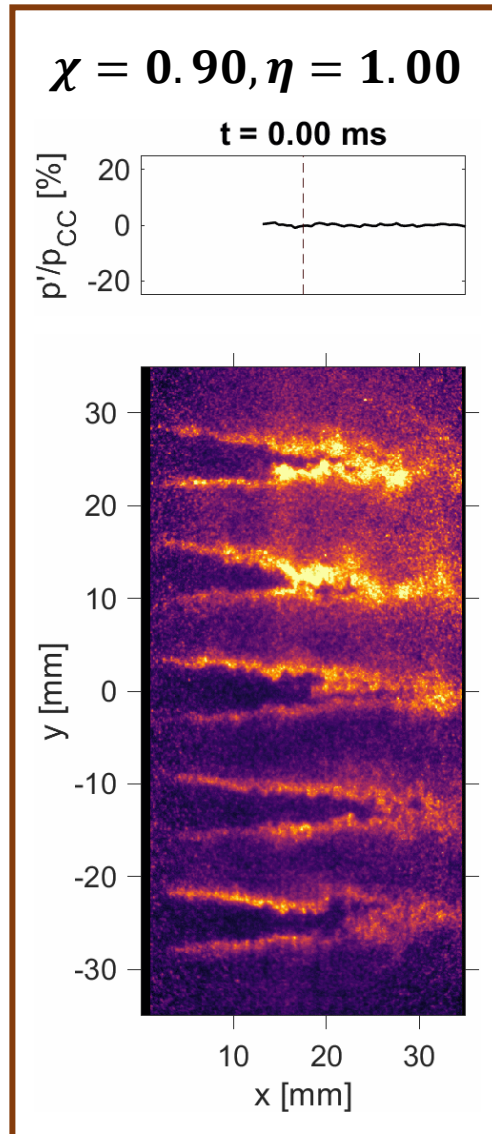


Shahin et al., "Dynamics of Hydrogen–Ammonia–Natural Gas Lean-Premixed High-Pressure Flames," *Fuel*, Vol. 385, 2025, p. 134016. <https://doi.org/10.1016/j.fuel.2024.134016>



# Dynamics Sensitivity to Methane Addition

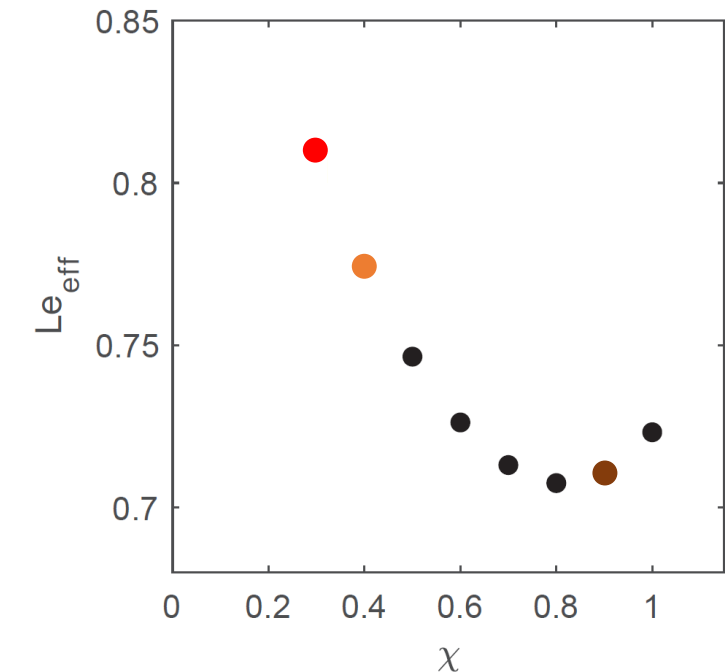
- Time-resolved OH PLIF shows flame response during instability cycle



**Fuel Composition**

$$\chi \left[ \eta \left( \frac{3}{2} \text{H}_2 + \frac{1}{2} \text{N}_2 \right) + (1 - \eta) \text{NH}_3 \right] + (1 - \chi) \text{CH}_4$$

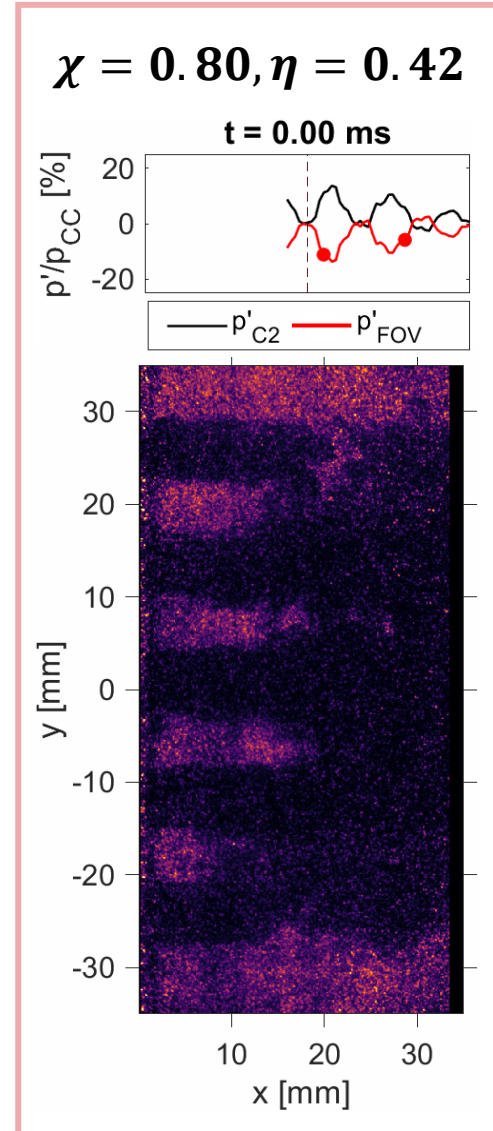
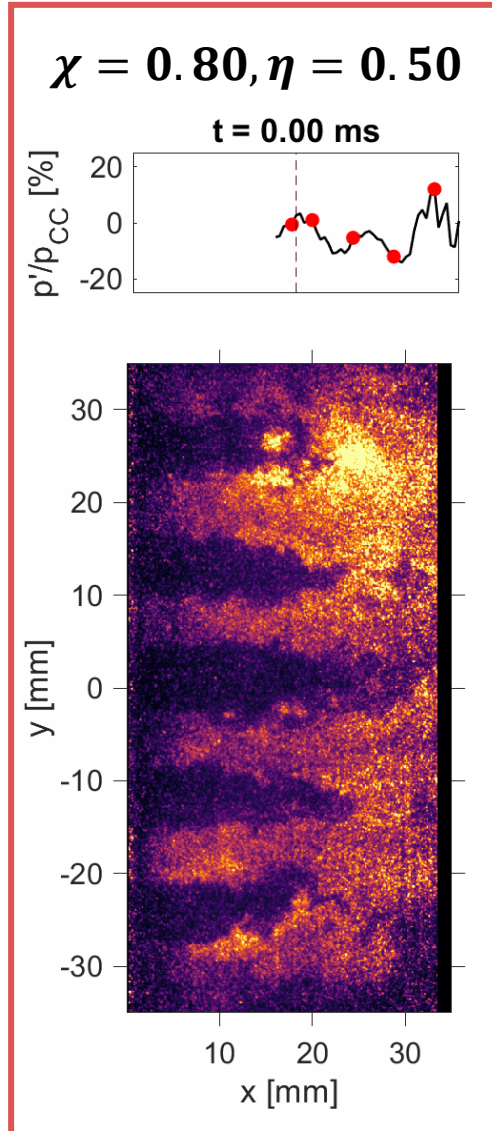
$\chi$  = hydrogen fraction  
 $\eta$  = ammonia decomposition efficiency



Shahin et al., "Structure of High-Pressure Premixed Ammonia, Hydrogen, and Methane Flames with 100 kHz OH-PLIF Measurements," *Journal of Engineering for Gas Turbines and Power*, 2025, pp. 1–14. <https://doi.org/10.1115/1.4069450>

# Dynamics Sensitivity to Ammonia Addition

- Time-resolved OH PLIF shows flame response during instability cycle



## Fuel Composition

$$\chi \left[ \eta \left( \frac{3}{2} \text{H}_2 + \frac{1}{2} \text{N}_2 \right) + (1 - \eta) \text{NH}_3 \right] + (1 - \chi) \text{CH}_4$$

$\chi$  = methane fuel fraction

$\eta$  = hydrogen decomposition efficiency

# Dynamics Sensitivity to Ammonia Addition

- Image binarization achieved using semantic segmentation
  - Employs convolutional neural network
  - Model identifies the reactant jet
- Noticeable improvement over gradient-based edge tracking
- Allows for time-resolved tracking of reactant area and flame front
- Instability mode switch can be tied to the duration of reactant area consumption
  - 27 frames ( $270 \mu s$ ) to consume reactants in 2L case (longer than 2L methane case)
  - 60 frames ( $600 \mu s$ ) to consume reactants in 1L case

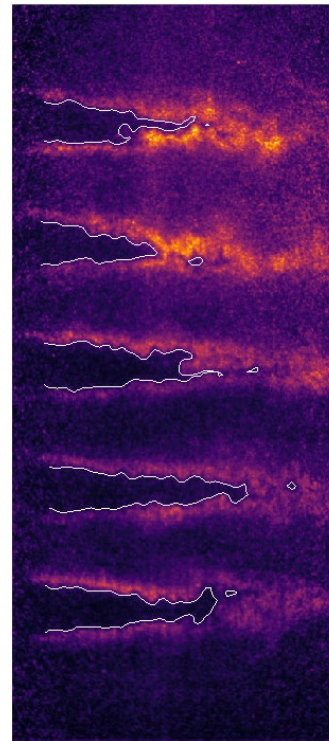
## Fuel Composition

$$\chi \left[ \eta \left( \frac{3}{2} \text{H}_2 + \frac{1}{2} \text{N}_2 \right) + (1 - \eta) \text{NH}_3 \right] + (1 - \chi) \text{CH}_4$$

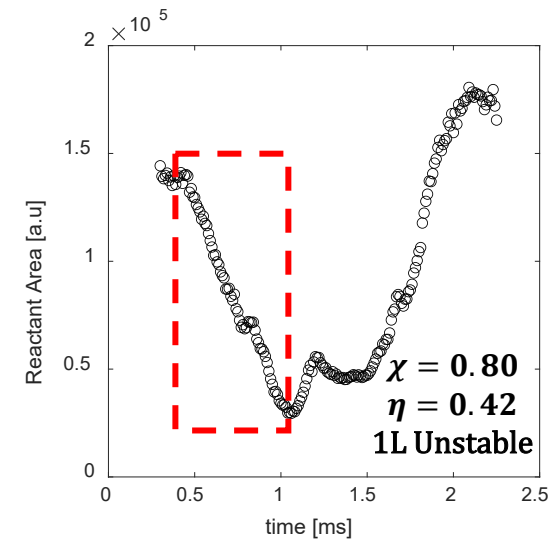
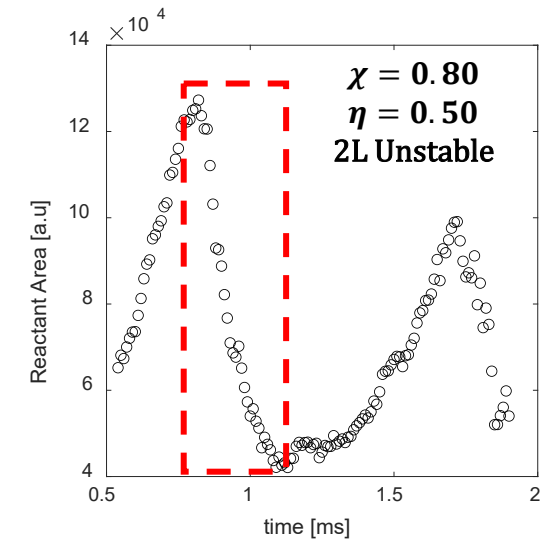
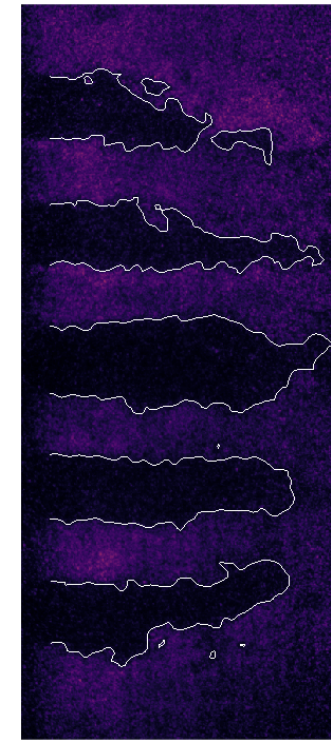
$\chi$  = methane fuel fraction

$\eta$  = hydrogen decomposition efficiency

$\chi = 0.90 \quad \eta = 1.00$



$\chi = 1.00 \quad \eta = 0.32$





# Effect of Ammonia Addition on Flame Structure

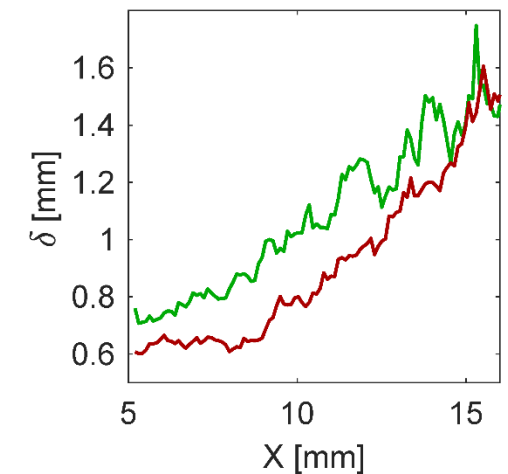
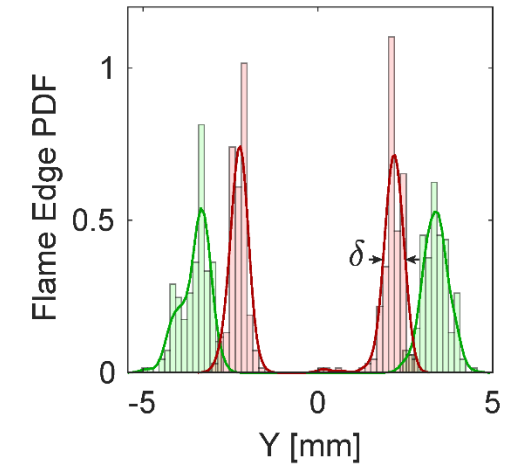
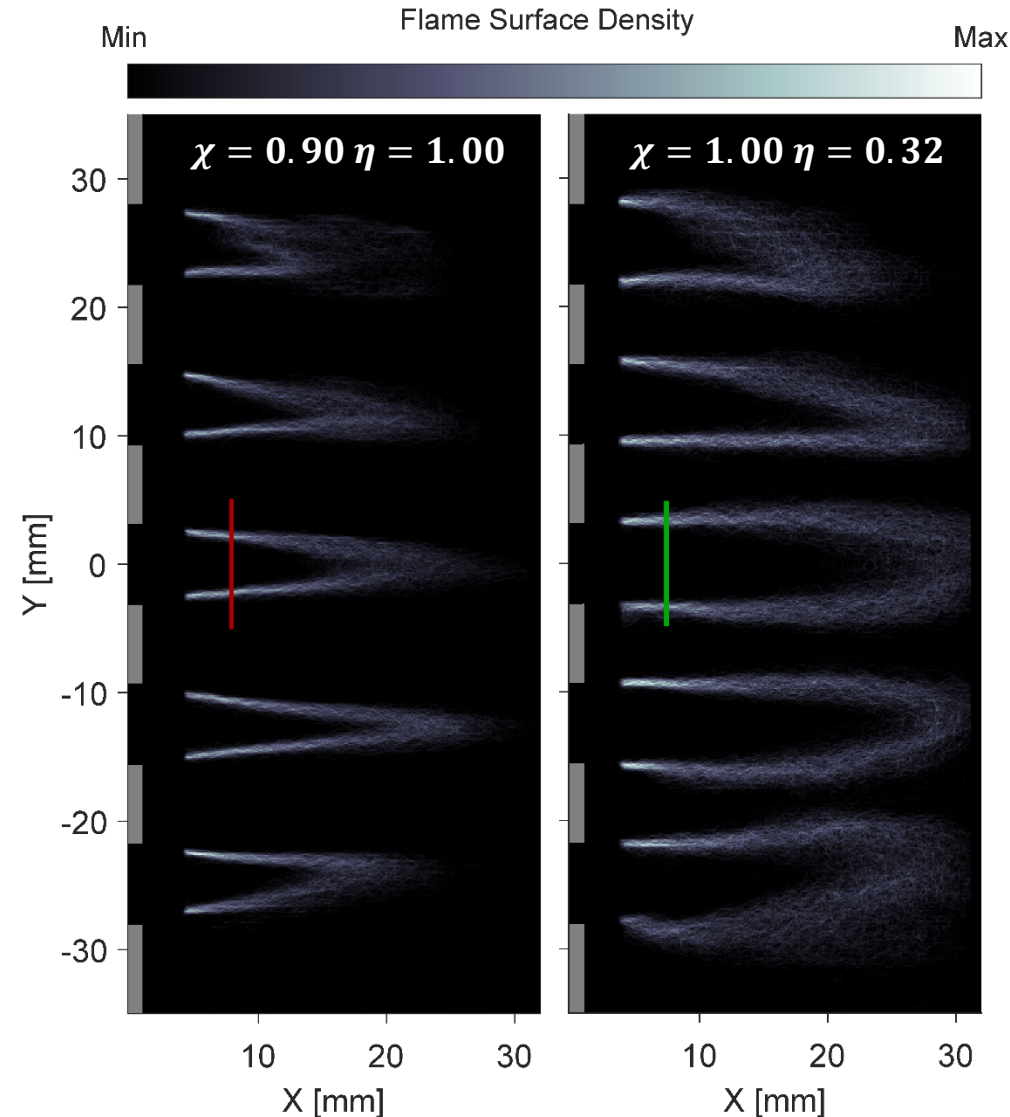
- Flame surface density (FSD) generated from flame fronts of all frames
- Upstream FSD width larger with more ammonia, indicating slower kinetics
- Downstream FSD width also larger with more ammonia, indicating larger amplitude flame front fluctuations

## Fuel Composition

$$\chi \left[ \eta \left( \frac{3}{2} \text{H}_2 + \frac{1}{2} \text{N}_2 \right) + (1 - \eta) \text{NH}_3 \right] + (1 - \chi) \text{CH}_4$$

$\chi$  = methane fuel fraction

$\eta$  = hydrogen decomposition efficiency



# Effect of Ammonia Addition on Flame Structure

- Probability density functions (PDF) for radius of curvature ( $r$ ) show the impact of  $\text{NH}_3$  on flame structure
- Over entire FOV, slight bias towards negative curvature due geometry of the jet flames
- In upstream region, curvature more uniform with more  $\text{H}_2$ 
  - $\text{H}_2$  induces thermo-diffusive instabilities that balance flame surface production from turbulent flow strain<sup>1</sup>
- In downstream region, this trend is reversed
  - Rapid surface annihilation near reactant core tip enhanced with more  $\text{H}_2$ , causing negative curvature bias

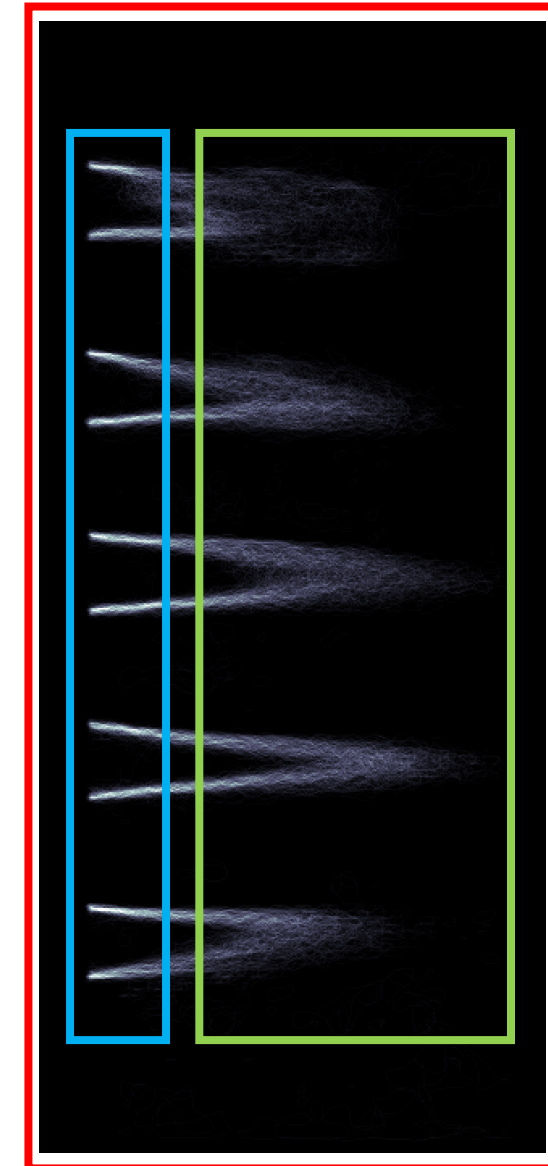
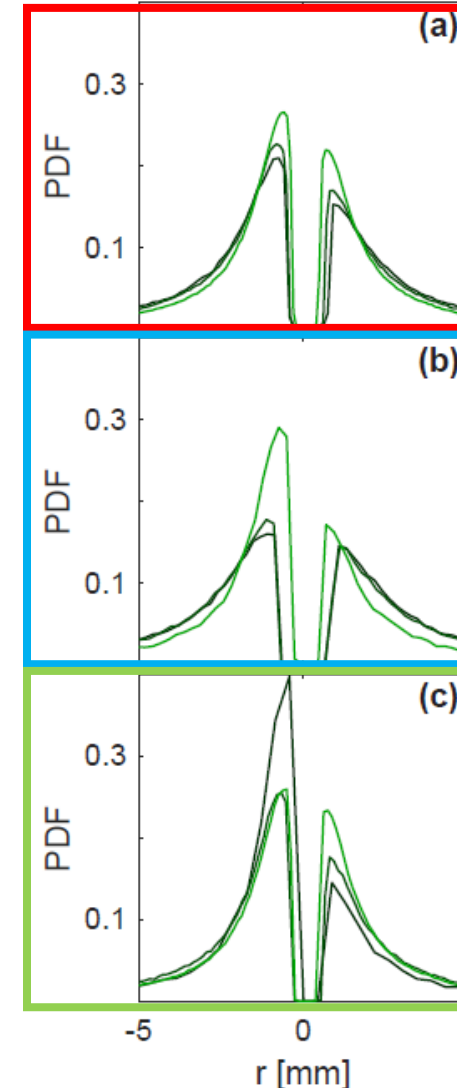
## Fuel Composition

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$\chi$  = methane fuel fraction

$\eta$  = hydrogen decomposition efficiency

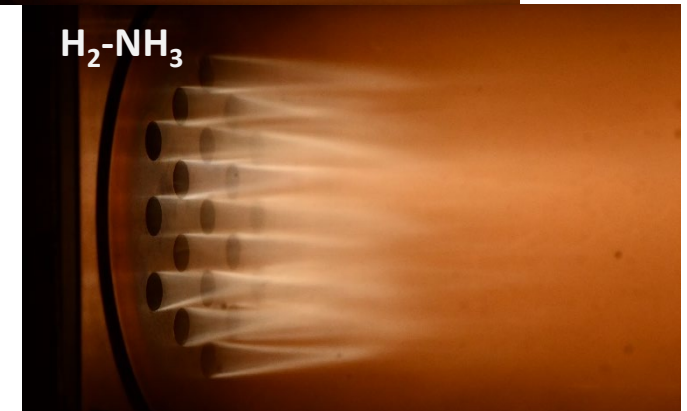
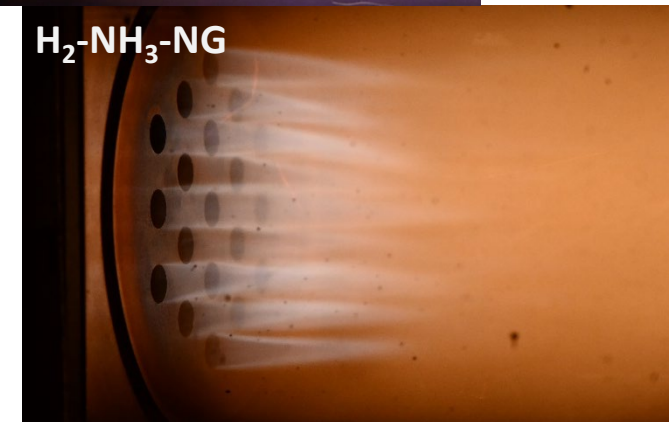
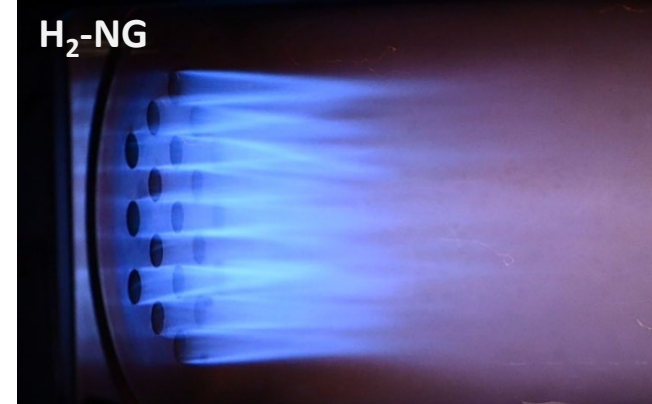
- $\chi = 1.00 \quad \eta = 0.89$
- $\chi = 1.00 \quad \eta = 0.70$
- $\chi = 1.00 \quad \eta = 0.32$



[1] Coulon, V., Gaucherand, J., Xing, V., Laera, D., Lapeyre, C., and Poinso, T., "Direct Numerical Simulations of Methane, Ammonia-Hydrogen and Hydrogen Turbulent Premixed Flames," *Combustion and Flame*, Vol. 256, 2023, p. 112933.  
<https://doi.org/10.1016/j.combustflame.2023.112933>

# Summary

- High pressure ammonia storage systems present novel challenges for safe and efficient use
- The addition of  $\text{NH}_3$  and  $\text{CH}_4$  alters the flame shape and distribution of reactions
- Combustion stability map shows sensitivity of thermoacoustics to  $\text{NH}_3$  and  $\text{CH}_4$  addition
- Time-resolved OH PLIF reveals how local flame behaviors affect the global dynamics
- Flame front tracking shows how fuel composition affects the turbulent flow-flame processes, leading to changes in combustion dynamics





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