



Flame Speed Measurements of Ammonia-Hydrogen Mixtures

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- Motivation
- Experimental setup
- Theoretical background
- Results and discussion
- Future works

- CO₂ emission
 - Need to decrease
- Ammonia (NH₃)
 - NH₃ has higher volumetric energy density than H₂ and natural gas

Properties	Ammonia	Hydrogen	Natural Gas
Density, g/cm ³	0.77 (liq.)	0.071	0.187
Ignition point, °C	800	400	650
Low calorific value, kJ/kg	18,610	120,000	38,100
Octane number	110	130	107
Explosion limit (volume ratio)%	16~28	4.5~75	5~15
Energy Density, MJ/m ³	11.3	3.75	7.134
Minimum Ignition Energy, mJ	680	0.02	0.32

Yu, et al., 2022

- CO₂ emission
 - Need to decrease
- **Ammonia (NH₃)**
 - NH₃ has higher volumetric energy density than H₂ and natural gas
 - **Cheaper than H₂**



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 - **Production, storage, transportation, and distribution**

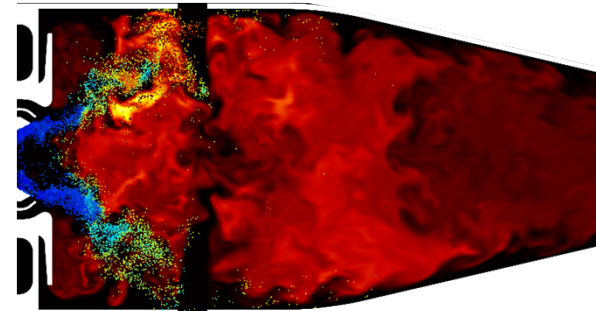


<https://www.dreamstime.com>

- CO₂ emission
 - Need to decrease
- **Ammonia (NH₃)**
 - NH₃ has higher volumetric energy density than H₂ and natural gas
 - Cheaper than H₂
 - Production, storage, transportation, and distribution
 - **Toxic, but easy to detect by the distinctive smell**
 - **Strong fuel candidate for gas turbines, and engines**

□ Laminar burning speed

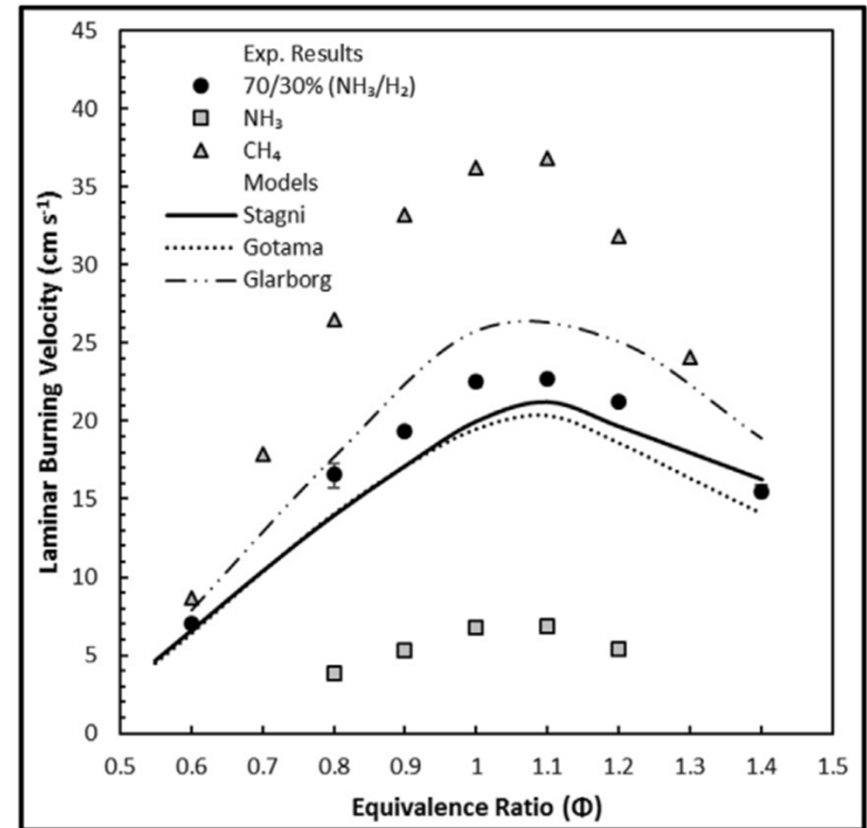
- Design internal combustion engine.
- Modeling turbulent combustion
- Validation of chemical kinetic mechanism



The current state of $\text{NH}_3\text{-H}_2$ combustion research is insufficient to accurately predict its explosion characteristics

Inaccuracies exist in both the lean and rich regions for various mechanisms, necessitating reaction reduction for positively/negatively sensitive reactions

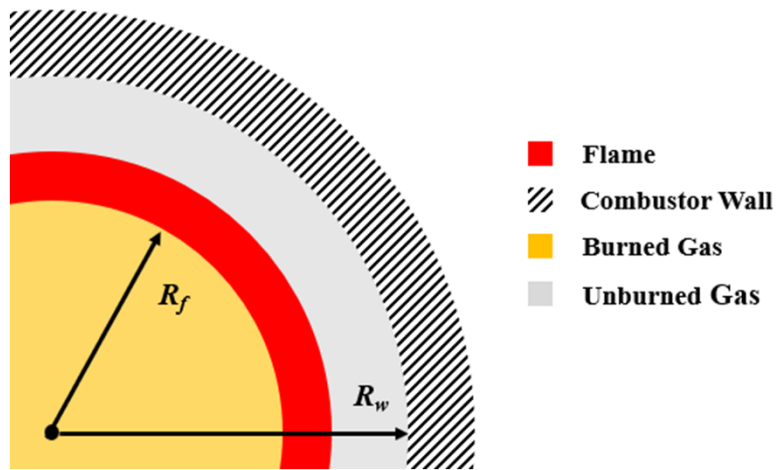
Greater knowledge of $\text{NH}_3\text{-H}_2$ combustion at higher pressures is needed to reach the design stage for turbine development



Source: S. Mashruk *et al*, 2022

- The preliminary model developed by UCF has been updated.
 - **256** Reactions *currently under development*
- Reactions for ammonia pyrolysis have been included from literature (Baker et al. and Alturaifi et al.)
- Reactions added for NH₂, NH, NNH, N₂H₂, N₂H₃, N₂H₄ and H₂NN relevant to pyrolysis.

Rxn.no	Reaction	A	n	Ea
1	NH ₂ +M=NH+H+M	1.20E+15	0	75950
2	NH ₂ +H=NH+H ₂	6.92E+13	0	3650
3	NH ₂ +NH=NH ₃ +N	9.57E+03	2.46	107
4	NH ₂ +NH ₂ =NH ₃ +NH	5.64E+00	3.53	522
5	NH ₂ +NH ₂ =N ₂ H ₂ +H ₂	1.74E+08	1.02	11783
6	NH ₂ +NH ₂ =H ₂ NN+H ₂	7.17E+04	1.88	8802
7	NH+M=H+N+M	1.80E+14	0	74760
8	NH+H=H ₂ +N	1.00E+14	0	0
9	NH+N=N ₂ +H	3.00E+13	0	0
10	NH+NH=N ₂ +H+H	2.50E+13	0	0
11	NH+NH=NH ₂ +N	5.66E-01	3.88	342
12	NNH+NH=N ₂ +NH ₂	5.00E+13	0	0
13	NNH+NH ₂ =N ₂ +NH ₃	5.00E+13	0	0
14	N ₂ H ₂ =H ₂ NN	9.20E+38	-9.01	67727
	PLOG / 0.1	9.20E+38	-9.01	67727
	PLOG / 1.0	2.00E+41	-9.38	68452
	PLOG / 10.0	1.30E+45	-10.13	70757
15	N ₂ H ₃ +H=N ₂ H ₂ +H ₂	2.40E+08	1.5	0
16	N ₂ H ₃ +NH ₂ =N ₂ H ₂ +NH ₃	9.20E+05	1.94	-1152
17	N ₂ H ₃ +NH ₂ =H ₂ NN+NH ₃	3.00E+13	0	0
18	NH ₂ +NH ₂ (+M)=N ₂ H ₄ (+M)	5.60E+14	-0.414	66
	LOW / 1.60E+34 -5.49 1987/			
	TROE / 0.31 1E-30 1E30 1E30/			
19	N ₂ H ₄ =H ₂ NN+H ₂	4.00E+44	-9.85	71353
	PLOG / 0.1	4.00E+44	-9.85	71353
	PLOG / 1.0	5.30E+39	-8.35	69307
	PLOG / 10.0	2.50E+39	-8.19	69664
21	N ₂ H ₄ +NH ₂ =N ₂ H ₃ +NH ₃	3.90E+12	0	1500
22	H ₂ NN=NNH+H	3.40E+26	-4.83	46228
	PLOG / 0.1	5.90E+32	-6.99	51791
	PLOG / 1.0	9.60E+35	-7.57	54841
	PLOG / 10.0	5.00E+36	-7.43	57295



Mutlizonne Combustion Model

Definition of laminar burning speed

$$\rho_u S_u = \frac{1}{A_f} \frac{dm_b}{dt}$$

Bradley & O'Donovan et al. flame radius derivation

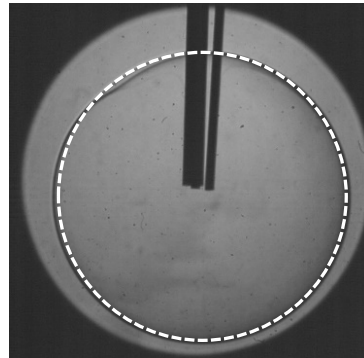
$$R_f = R_0 \left(1 - (1 - X) \left(\frac{P_i}{P} \right)^{\frac{1}{\gamma}} \right)^{\frac{1}{3}}$$

Generalized combustion model using flame radius and pressure data

$$S_u = \frac{R_0^3}{3R_f^2} \left(\frac{P_i}{P} \right)^{\frac{1}{\gamma}} \frac{dX}{dt}$$

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Single Layer

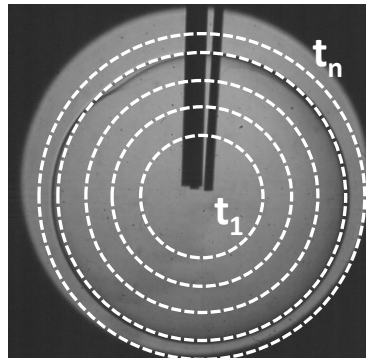
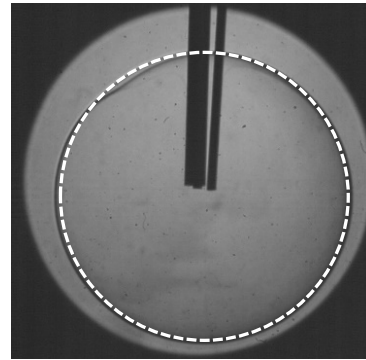
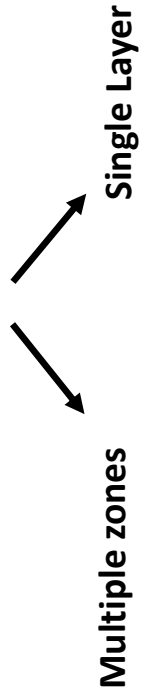


Linear model

$$X = \frac{P - P_i}{P_e - P_i}$$

- P_i : Initial pressure
- P : Instantaneous pressure
- P_e : Estimated peak pressure

$$S_u = \frac{R_0^3}{3R_f^2} \left(\frac{P_i}{P} \right)^{\frac{1}{\gamma}} \frac{dX}{dt}$$



Linear model

$$X = \frac{P - P_i}{P_e - P_i}$$

P_i : Initial pressure
 P : Instantaneous pressure
 P_e : Estimated peak pressure

Multizone model

$$X = \sum_{i=1}^n x_i$$

- Cantera

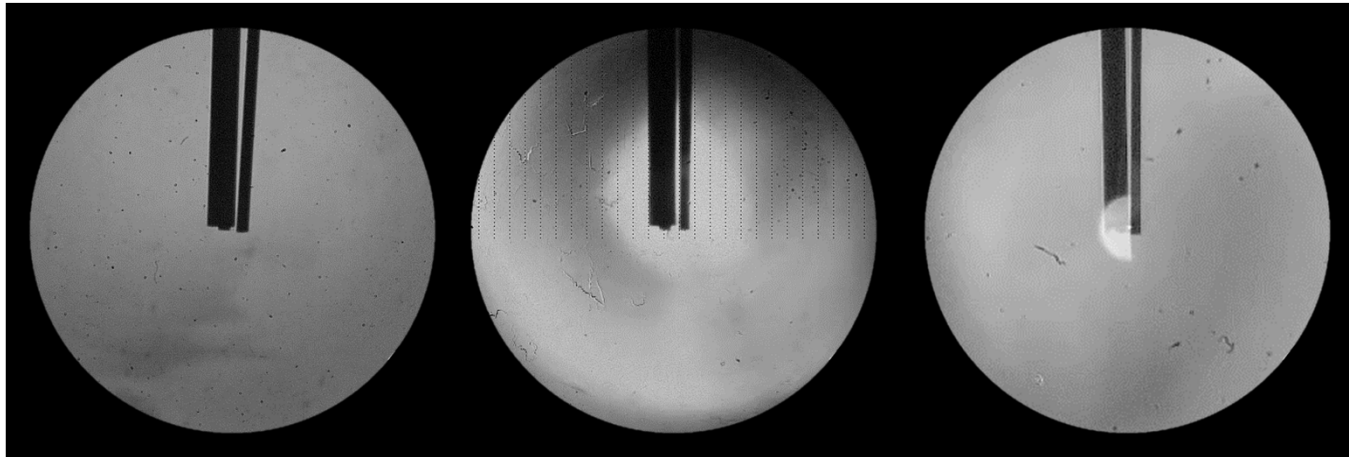
- Experimental conditions

Synthetic air		Initial conditions		Fuel
Oxidizer	Diluent	Temperature	Pressure	NH ₃ /H ₂
O ₂	He/Ar/N ₂	296 K	5 atm	
1	variety			

- Synthetic air details

		Fuel		
Ratio of NH ₃ /H ₂		1/0	0.5/0.5	0.7/0.3
Ratio of	O ₂	1.0		
	N ₂	1.0		
	Ar	1.5	0	0
	He	0	1.5	3

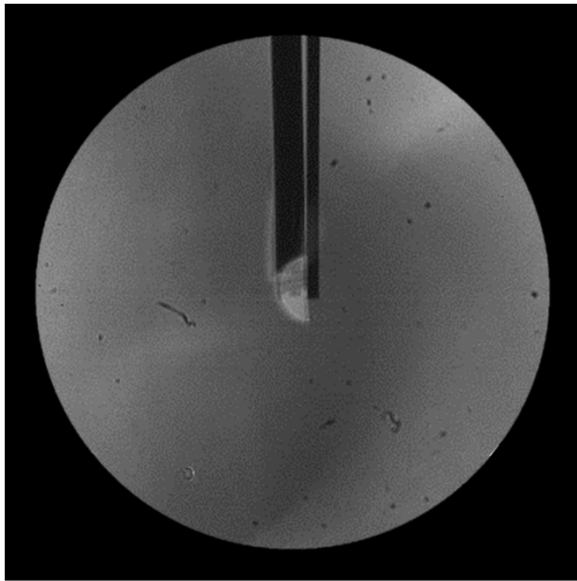
428K and Equivalence ratio of 1.3



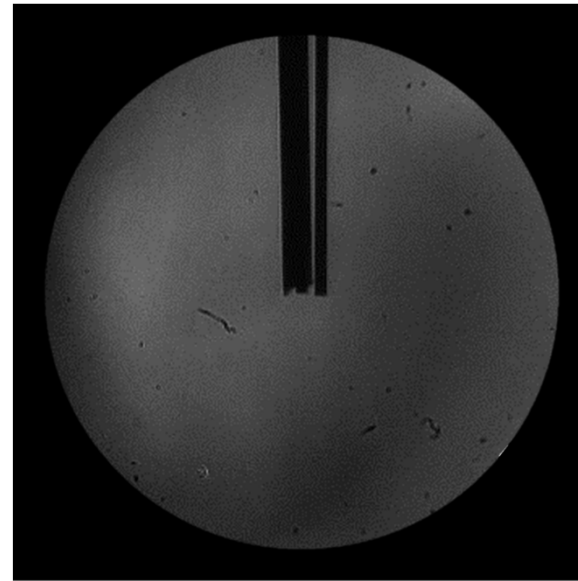
1 atm

2 atm

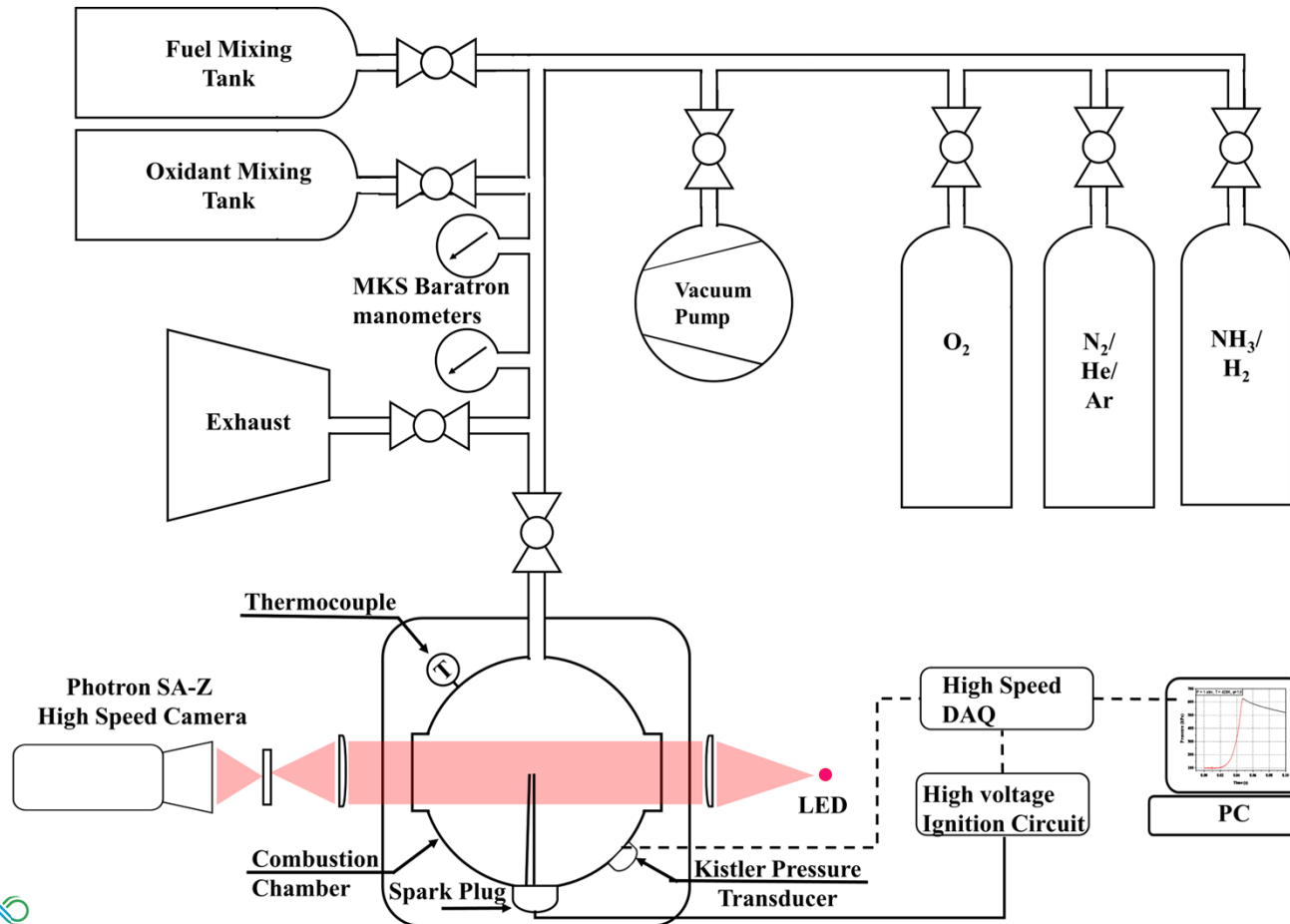
10 atm



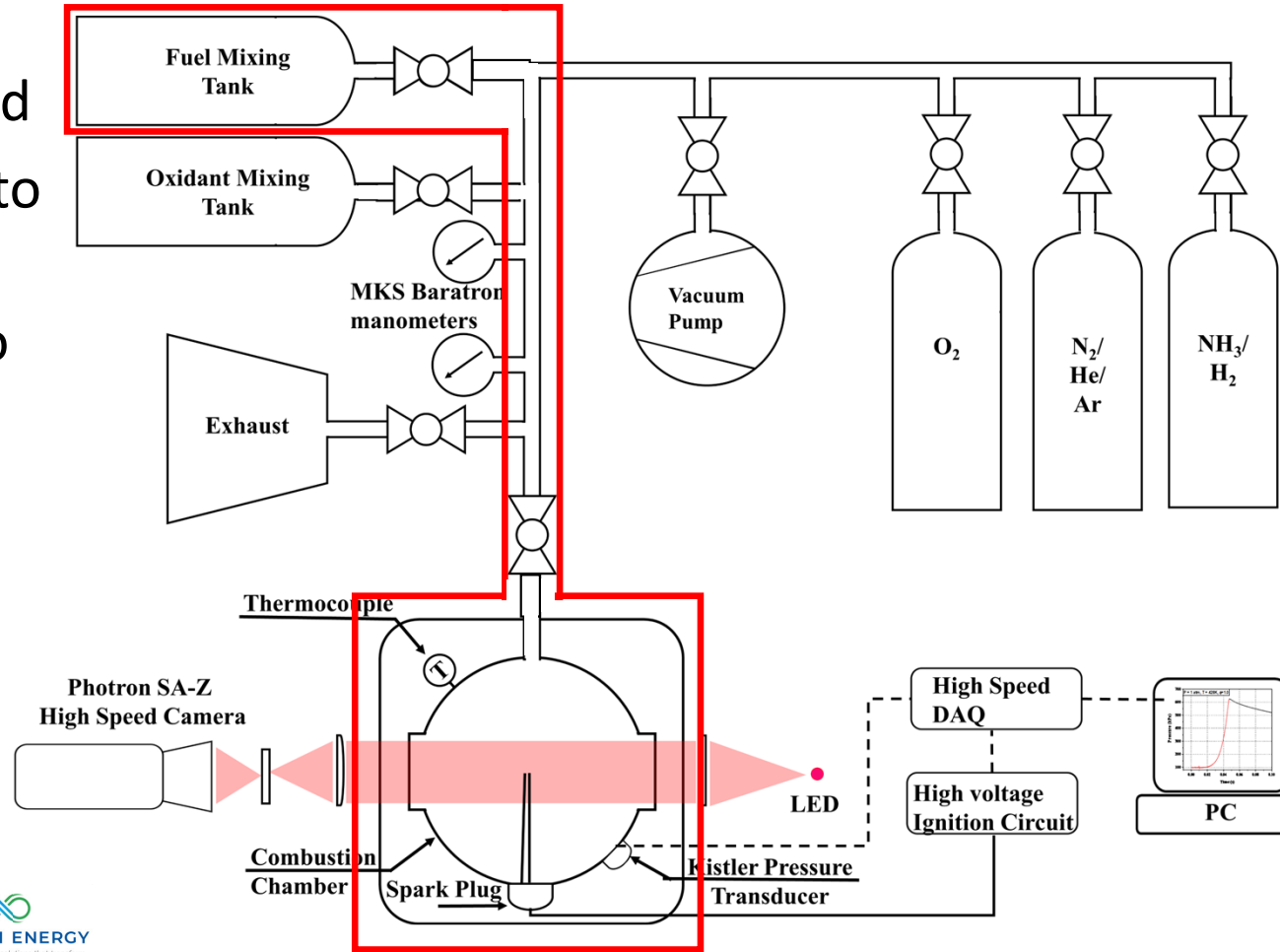
$\phi = 1.3$ with N_2 and He



$\phi = 1.3$ with N_2



- Setup are in the fume hood
- Exhaust line is connected to exhaust valve of building
- Schlieren image setup also is in the fume hood
- High speed camera is at outside the fume hood.

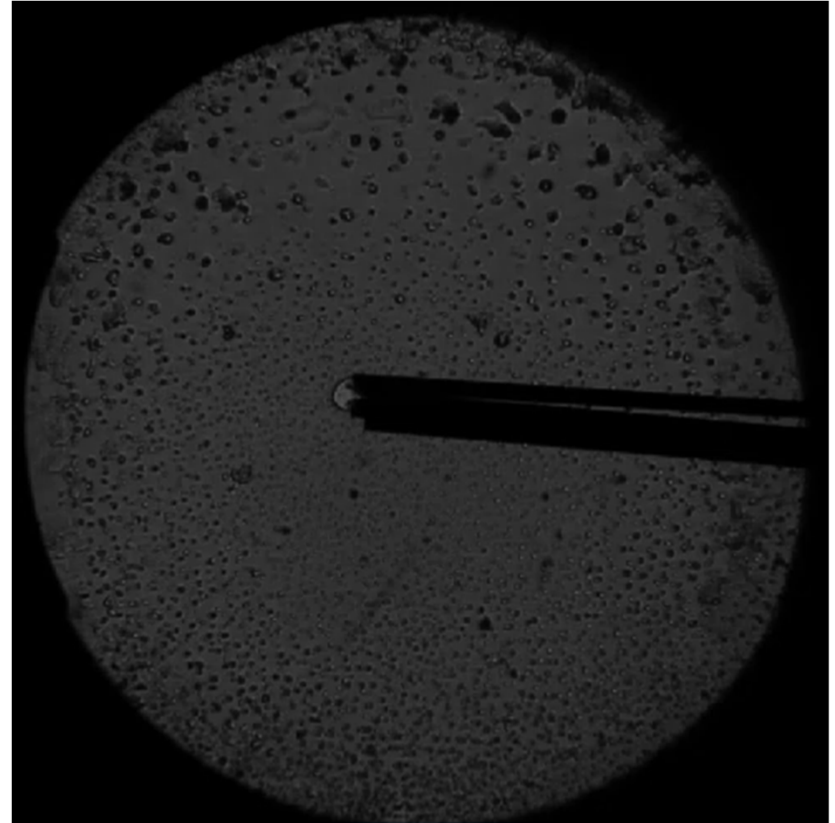


Experimental Validation:

Schlieren imaging was used to visualize the flame surface during kernel development and validate optimum oxidant conditions

The Schlieren images validate the following assumptions in our combustion model:

- 🔥 Flame is smooth and thin
- 🔥 No buoyancy forces present
- 🔥 The flame is spherical in nature

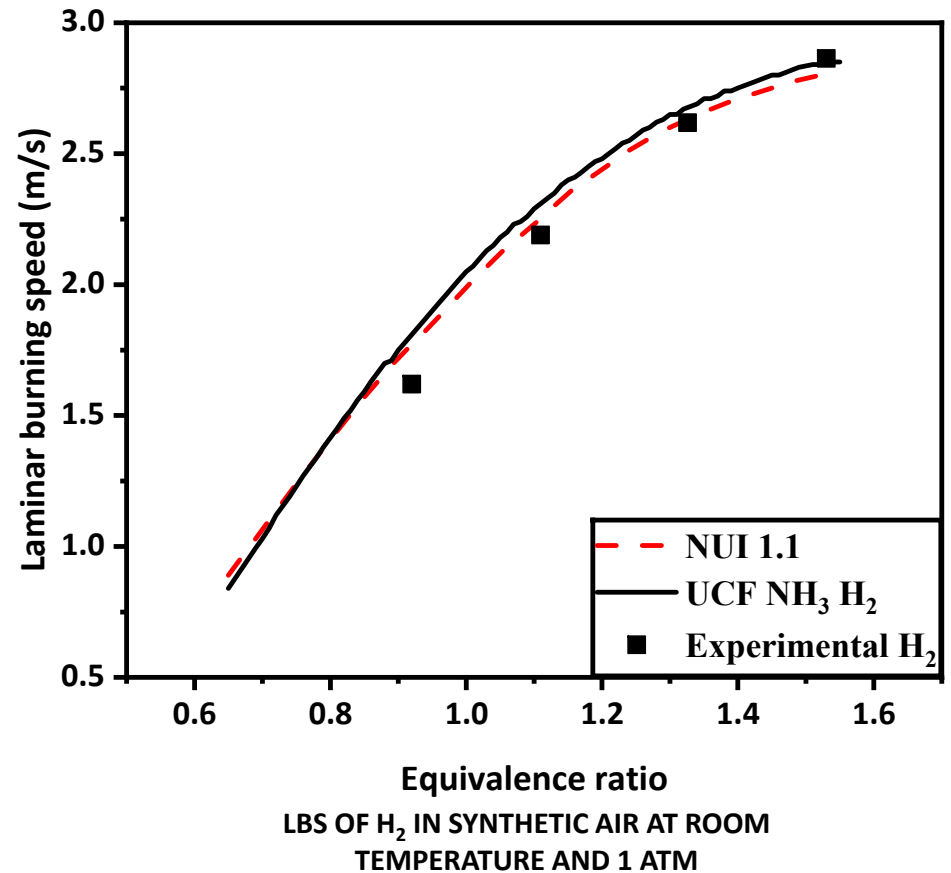


FLAME PROPAGATION VIDEO FOR H₂-ENHANCED NH₃ USING CUSTOMIZED OXIDANT MIXTURE

Experimental Validation:

Pure H₂ was ignited in air at room temperature and 1 atm to validate the experimental setup and combustion model

- 🔥 The UCF NH₃-H₂ mechanism accurately predicted experimental LBS values for pure H₂ ignition

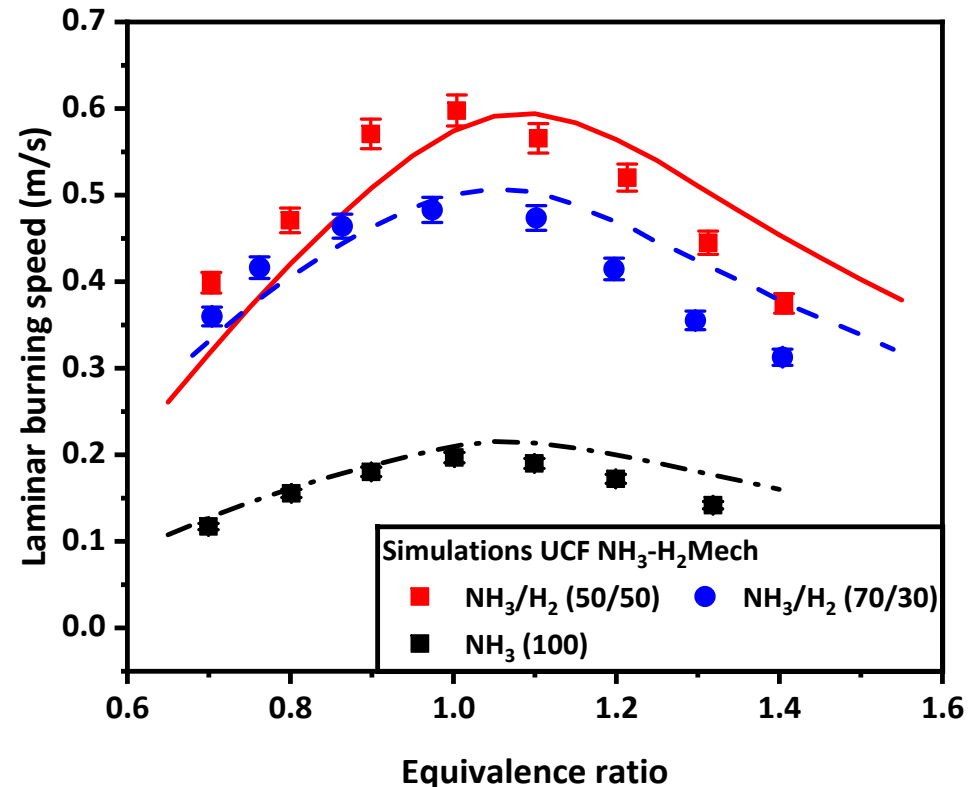


Effect of H₂ Addition to NH₃:

The flame speed was increased significantly with H₂ addition. Laminar flames were achieved using the customized oxidant prepared prior to experimentation

Chemical-Kinetic Mechanism:

The UCF NH₃-H₂ mechanism shows increased underprediction of the LBS in the lean region with increased H₂ concentration



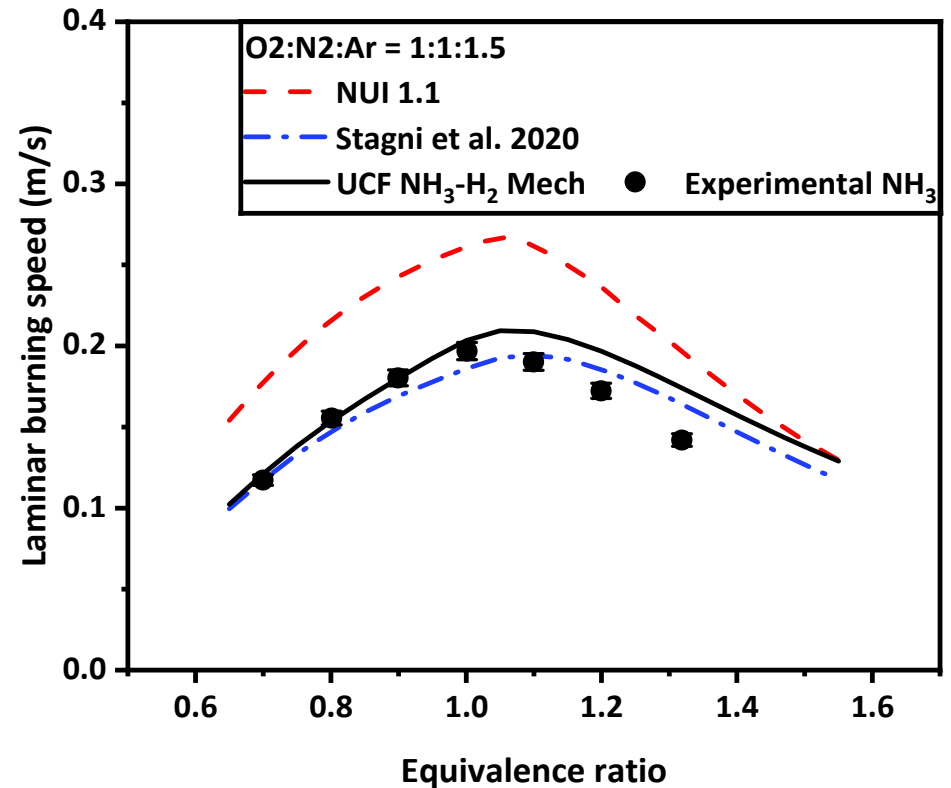
LBS OF ALL NH₃ IGNITIONS AT 296 K AND 5 ATM

Pure NH₃ Flames:

The maximum laminar burning speed (LBS) for pure NH₃ ignitions was determined to be 0.2 m/s at stoichiometric conditions ($\phi = 1.0$)

Chemical-Kinetic Mechanism:

The UCF NH₃-H₂ mechanism accurately predicted LBS values for pure NH₃ flames. The model overestimates the LBS values in the fuel-rich region



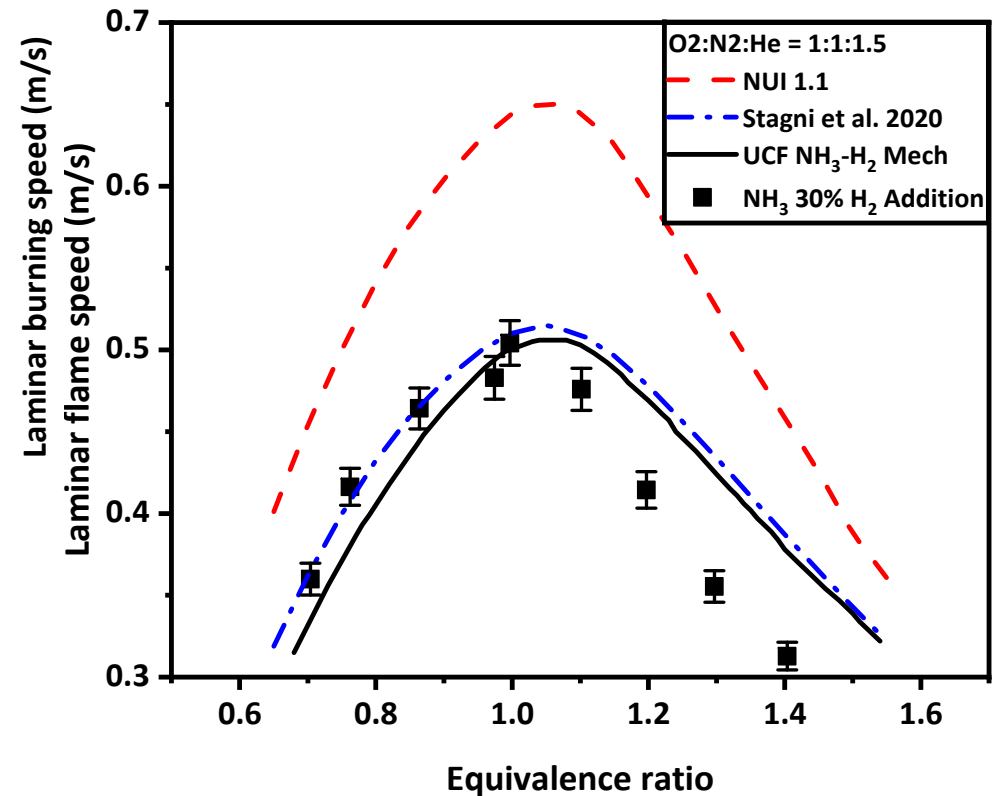
LBS OF PURE NH₃ IN SYNTHETIC AIR AT 296 K AND 5 ATM

H₂-Enhanced NH₃ Flames (70/30):

The maximum laminar burning speed (LBS) for 70% NH₃ + 30% H₂ ignitions was found to be 0.5 m/s at stoichiometric conditions ($\phi = 1.0$)

Chemical-Kinetic Mechanism:

The UCF mechanism developed for this investigation accurately predicted experimental LBS values for those in the fuel-lean region



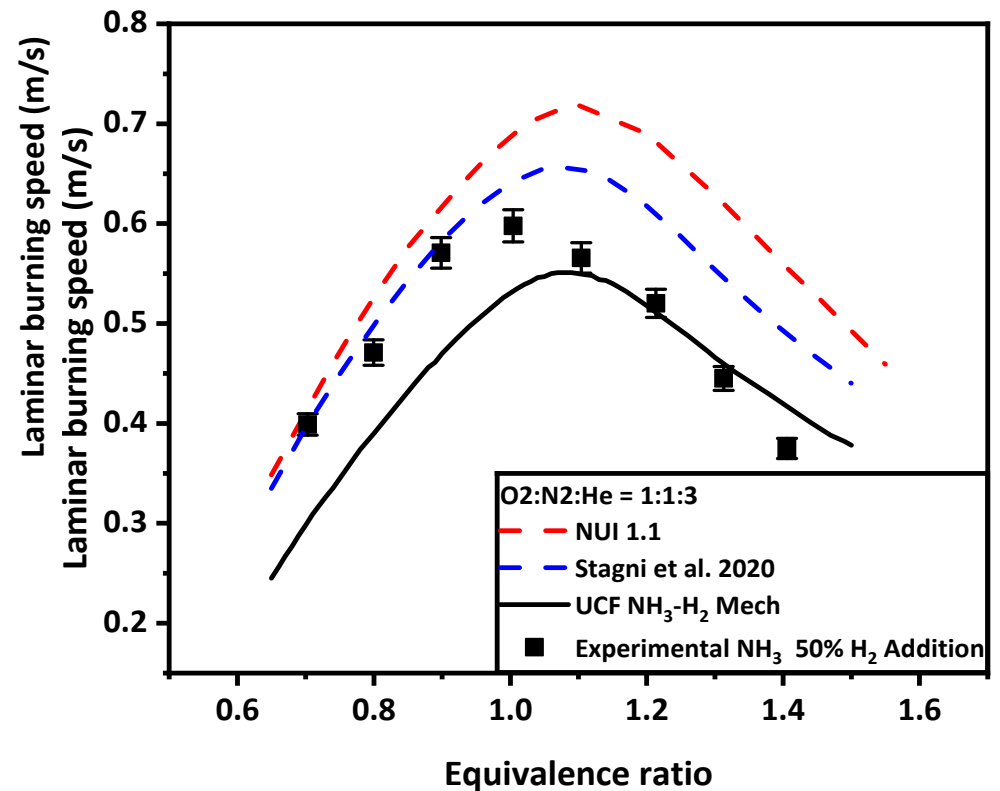
LBS OF 70% NH₃ + 30% H₂ IN SYNTHETIC AIR AT 296 K AND 5 ATM

H₂-Enhanced NH₃ Flames (50/50):

The maximum laminar burning speed (LBS) for 50% NH₃ + 50% H₂ ignitions was found to be 0.6 m/s at stoichiometric conditions ($\phi = 1.0$)

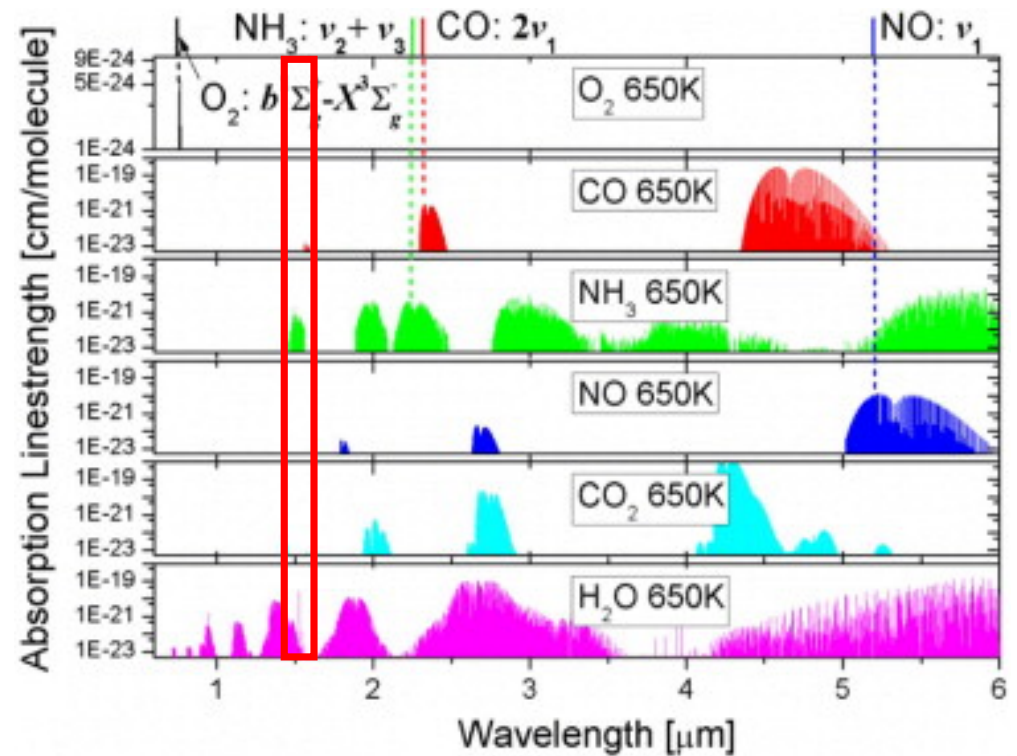
Chemical-Kinetic Mechanism:

The NH₃-H₂ mechanism developed for this study underestimated LBS values for the fuel-lean region.



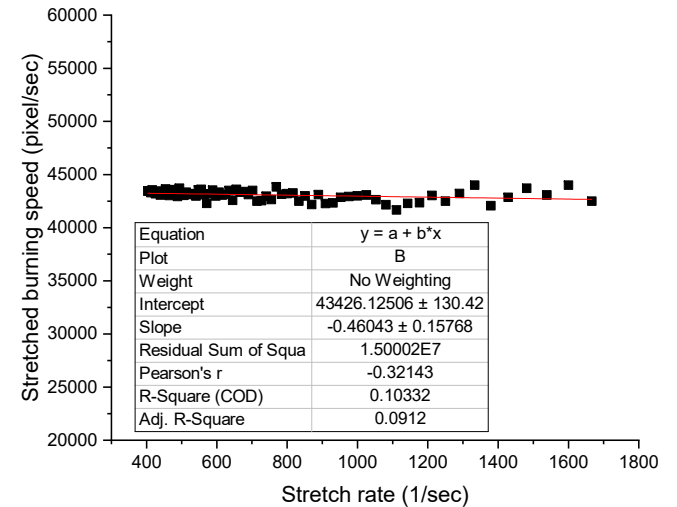
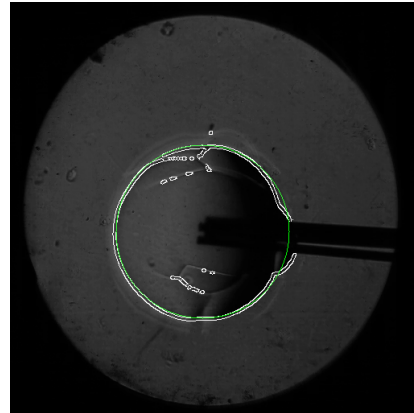
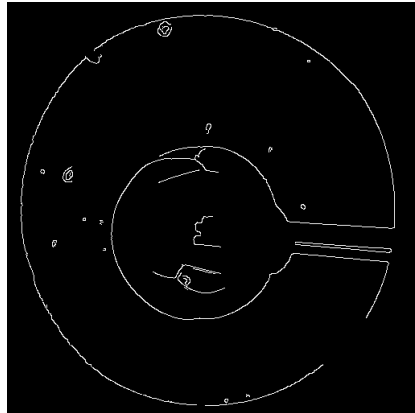
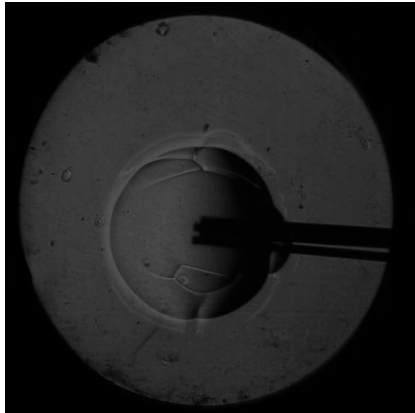
LBS OF 50% NH₃ + 50% H₂ IN SYNTHETIC AIR AT 296 K AND 5 ATM

- Need to check condensation of NH₃
- NH₃ wavelength w/o interference
 - 1.55 μm



- Constant Pressure method
 - Extraction image from video
 - Find edges with Edge Detector
 - Find flame and calculate radius
 - Calculate unstretched burning speed with radius
 - Convert to Laminar burning speed ($S_u = \rho_b / \rho_u \cdot S_0$)

phi	CVM (m/s)	CPM (m/s)	Difference (%)
0.70	0.350	0.345	1.61
0.91	0.576	0.563	2.29



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