

R&D Experiences for NH₃ combustion in KIER

- Fundamental staging-combustion behavior
- Co-firing with pulverized coal particles

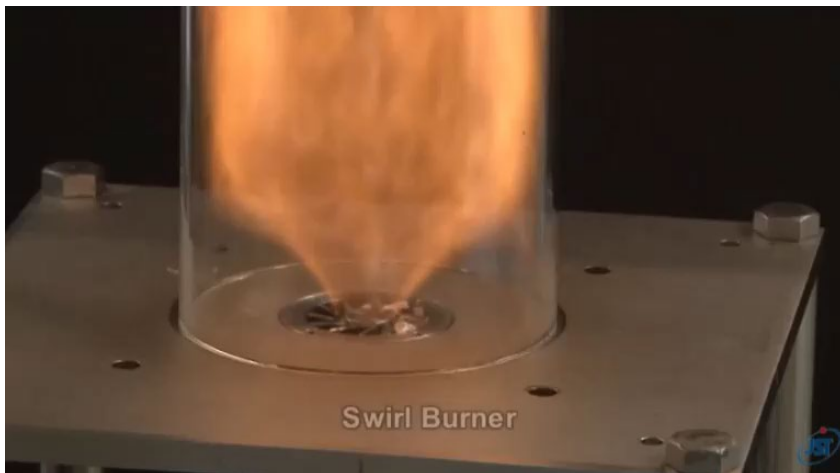
Hookyung LEE (Ph.D.)

Combustion Group in Energy Efficiency Research Division

Most Known Facts about NH₃ Combustion

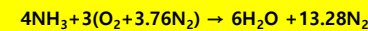
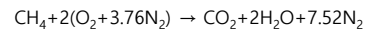
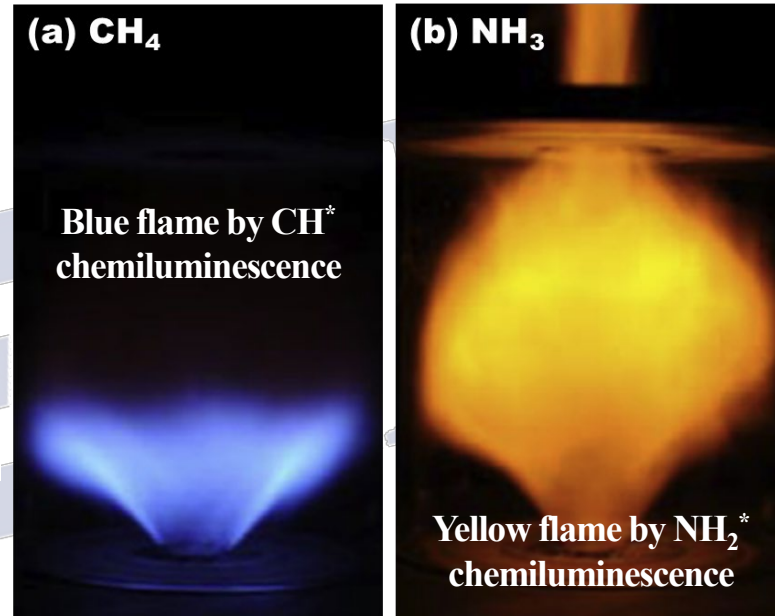
➤ Difficult ignition and flame stability conditions due to very low burning rates

Apparent flame images

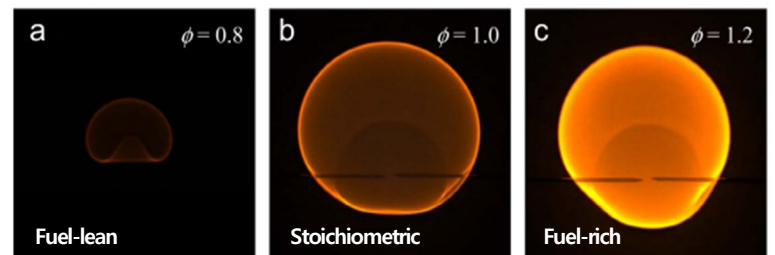


[SIP Energy Carriers PJT, Japan]

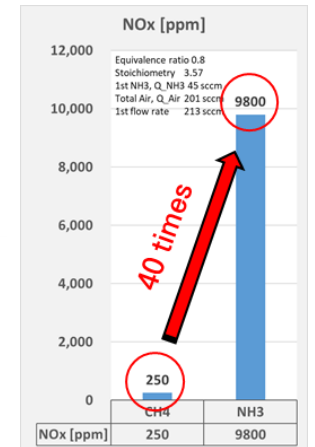
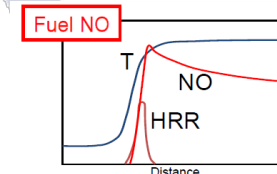
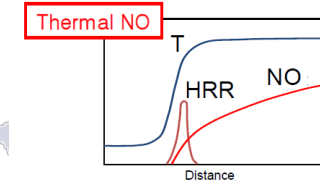
Stabilized premixed flame under the same flow rate and equivalent ratio conditions (swirl flow condition)



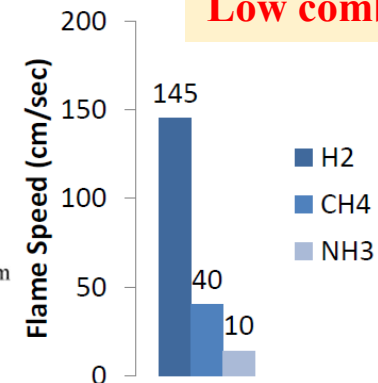
Spherical propagation flame according to equivalence ratio



Excessive NO_x emission



Low combustion rate



Burning velocity

1/4 level compared to LNG (CH₄)

1/15 level compared to Hydrogen (H₂)

Key Policy for NH₃ Use in Co-generation in Korea

➤ National Power Supply Plan : Advanced recognition of carbon emission reduction by using H₂ and NH₃

[2030 NDC goal '21.10] <2030 Energy mix plan>

(unit: TWh)

	Nuclear	Coal	LNG	Renewable	NH ₃	Others	Total
Gen. amount	1464	1332	1195	1852	221	60	6124
Share	23.9%	21.8%	19.5%	30.2%	3.6%	1.0%	100.0%

[10th National power supply plan '23.1]

Forecast of gen. amount and share by power source (unit: TWh)

YEAR		Nuclear	Coal	LNG	Renewable	H ₂ NH ₃	Others	Total
'30년	Gen. amount	201.7	122.5	142.4	134.1	13.0	8.1	621.8
	Share	32.4%	19.7%	22.9%	21.6%	2.1%	1.3%	100%
'36년	Gen. amount	230.7	95.9	62.3	204.4	47.4	26.6	667.3
	Share	34.6%	14.4%	9.3%	30.6%	7.1%	4.0%	100%

Forecast of H₂ and NH₃ power generation in 2030

	Fuel amount	Gen. amount	Target Power
Hydrogen	0.3 million-tons	6.1TWh	LNG
Ammonia	2.96 million-tons	6.9TWh	Coal

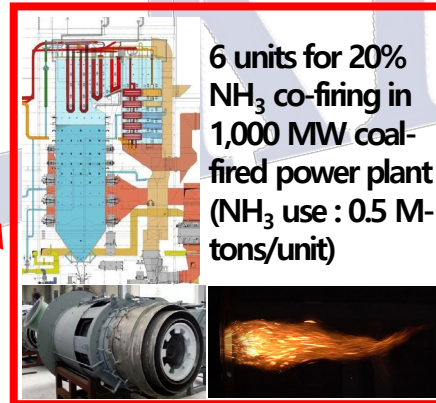
	'30년	'36년
Hydrogen Gen. amount (TWh)	6.1	26.5
Ammonia Gen. amount (TWh)	6.9	20.9

**[Ammonia receiving base
(for power generation)]**

Eastern Sea Area

Western Sea Area

Southern Sea Area



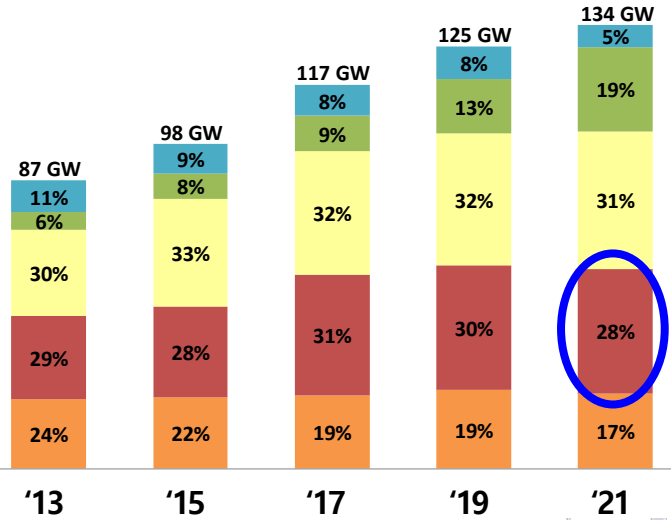
- Ammonia hub terminal
- Ammonia co-firing power generation
- Back industrial complex



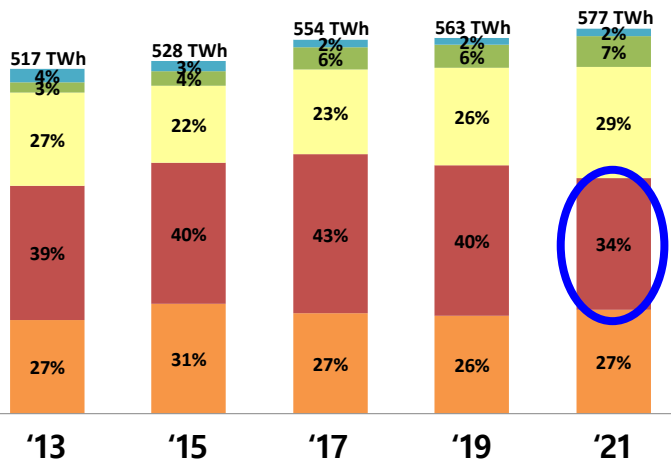
Demonstration Plants for Fuel Conversion to NH₃ (first-step with coal)

■ Nuclear
 ■ Coal
 ■ LNG
 ■ Renew.
 ■ Etc

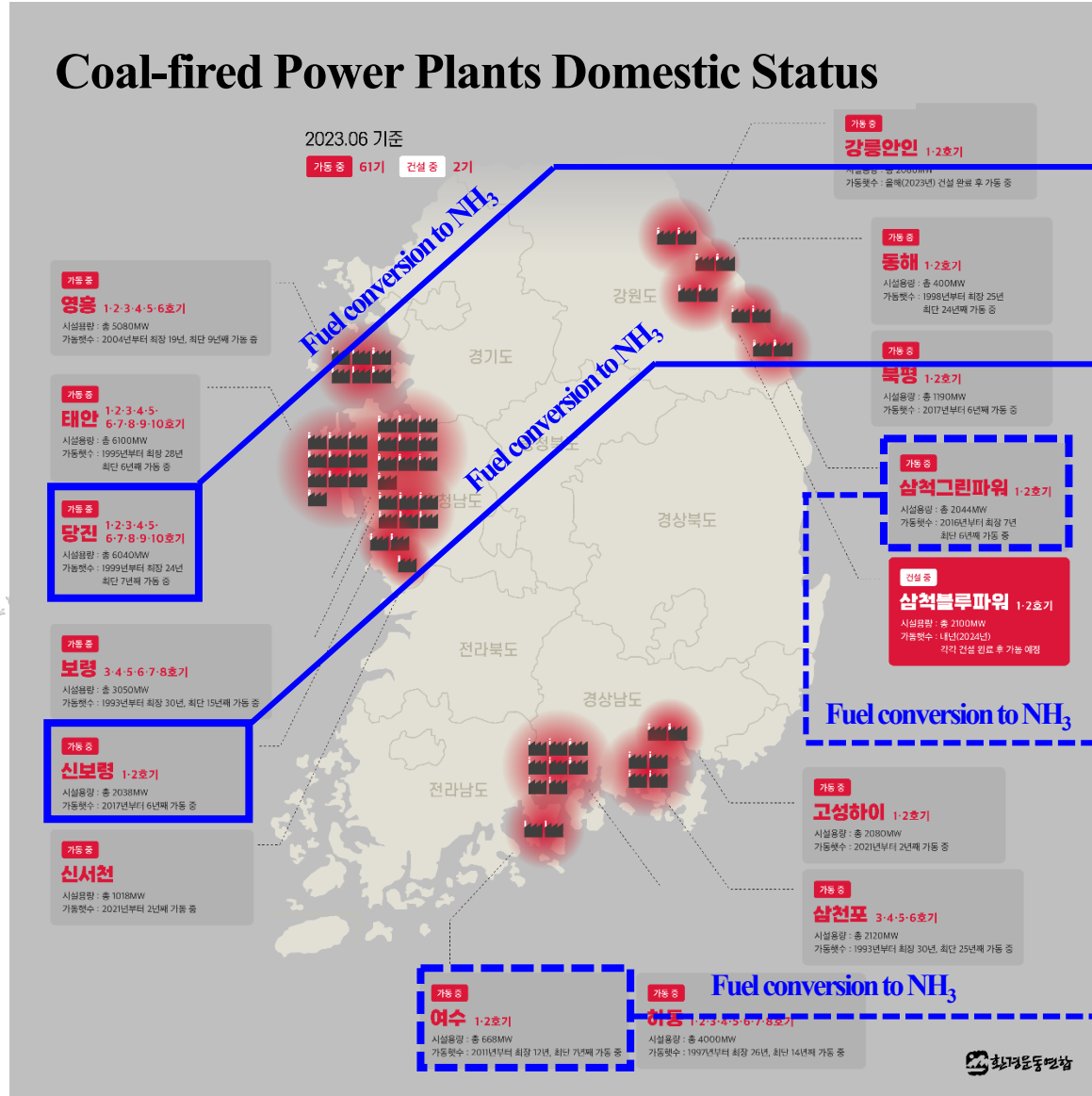
➤ Facility capacity in power sources [GW]



➤ Power gen. amount in power sources [TWh]



Coal-fired Power Plants Domestic Status



Pulverized coal - 20% NH₃ co-firing

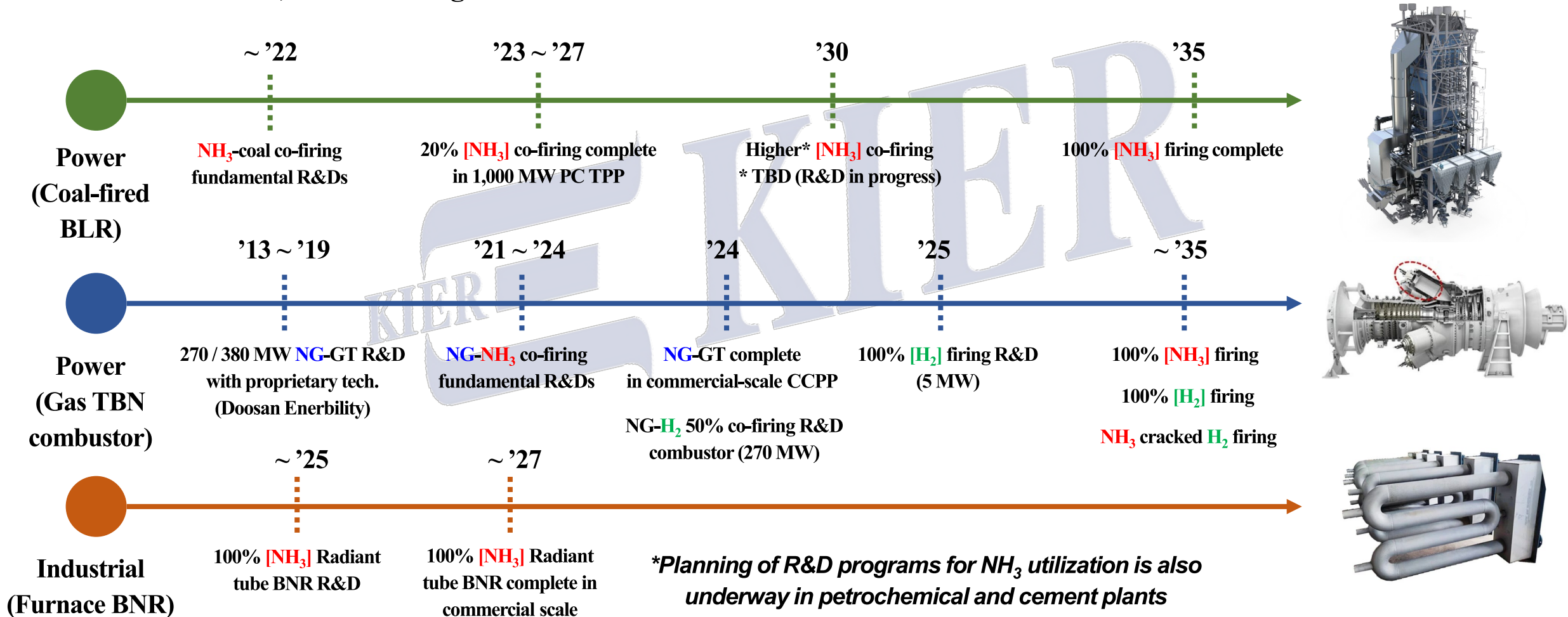


CFBC - 20% NH₃ co-firing



Current Status of NH₃ Combustion Research in Korea

- National R&D is underway in the power generation sector, such as coal-fired boilers and gas turbines (marine engine), and in the steel sector, such as heating furnace burners



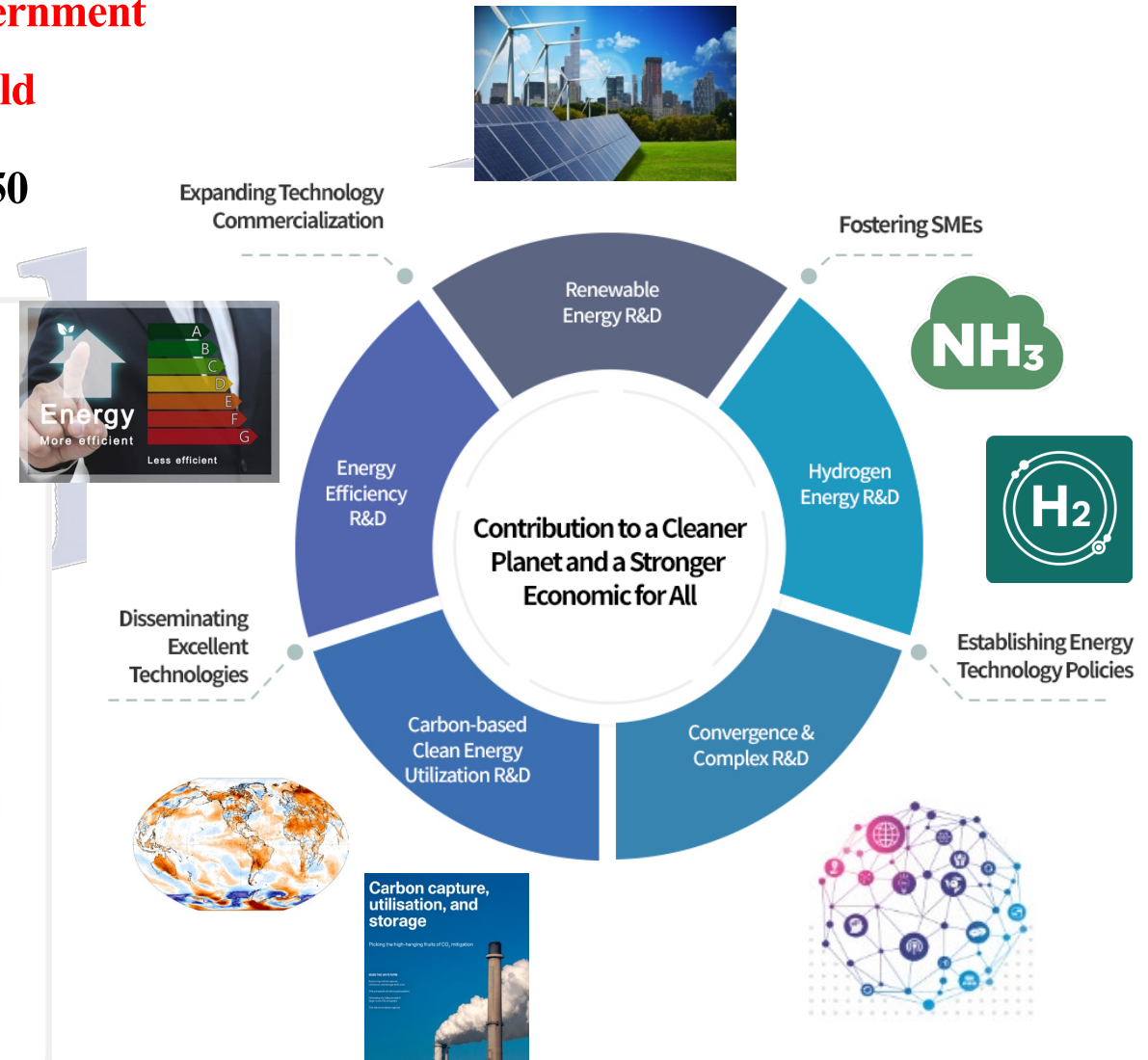
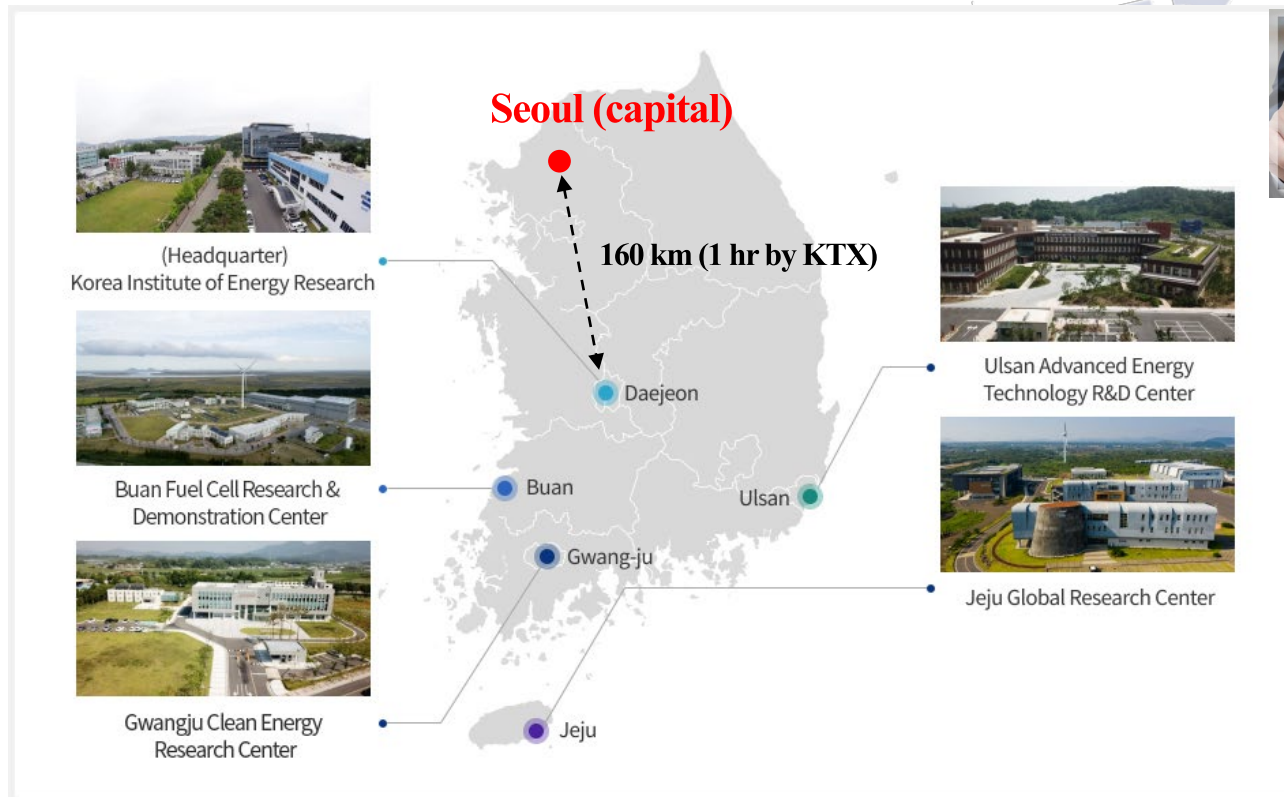
Korea Institute of Energy Research (KIER)

- One of the **National Research Institute Funded by Korean Government**
- Representative R&D Institute in the **Combustion & Energy Field**

Personnel : 550 (full-time) / Ph.D. 350

Budget : \$ 160 M/yr (USD)

H/Q Location : Daejeon



Combustion Group in KIER

- A group of combustion experts (15) who have been conducting combustion research for over 40 years in a KIER lab.
- Application to power generation, steel treatment and petrochemical processes

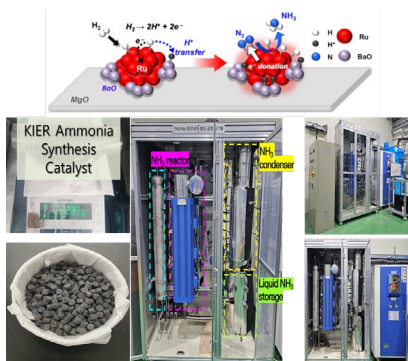
	1990s	2000s	2010s	2020s
Body system	Rolling heating furnace design Al melting furnace	Roller kiln Forging furnace	Shuttle kiln Shuttle kiln Oxy-fuel heating furnace Smart EAF	Smart furnace design platform CAL system
Comb. device	Low P pneumatic oil BNR Flat BNR	Hot air BNR High V BNR Low NOx BNR	Heat storage BNR Oxy-fuel BNR	sCO2 combustor Porous media BNR Semi-conductor process BNR H ₂ /NH ₃ firing BNRs NH ₃ co-firing BNRs & system NH ₃ firing BNRs & system
Waste heat recovery	Waste heat recovery BNR	Channel recuperator Radiation recuperator	Ceramic recuperator	
Furnace control	Furnace control / PLC design		Furnace combustion optimization	
etc		Gas torch Plasma	Oxy-fuel boiler	Electrification

Ammonia Research Flows in KIER

➤ Full-cycle research is being conducted from NH₃ production, utilization (combustion, fuel cell) and post-treatment technology

Production

➤ NH₃ synthesis in low T and low P



Utilization

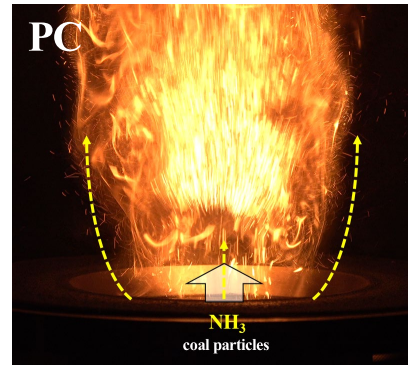
➤ NH₃ -only combustion



➤ H₂ prod. with NH₃ decomposition



➤ NH₃ combustion with other fuels

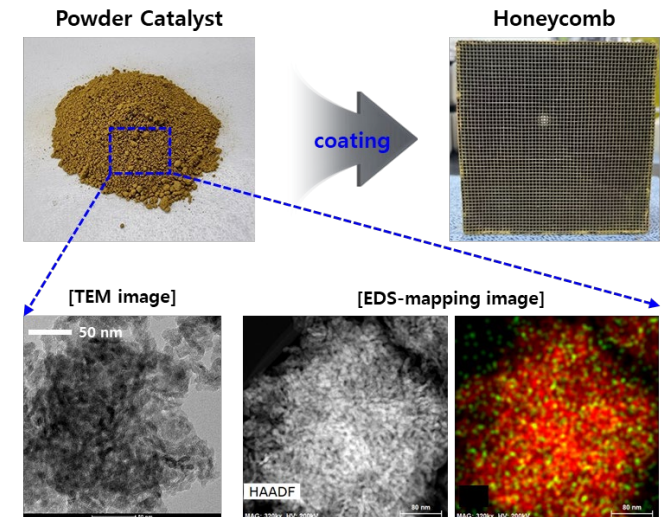


Post-treatment

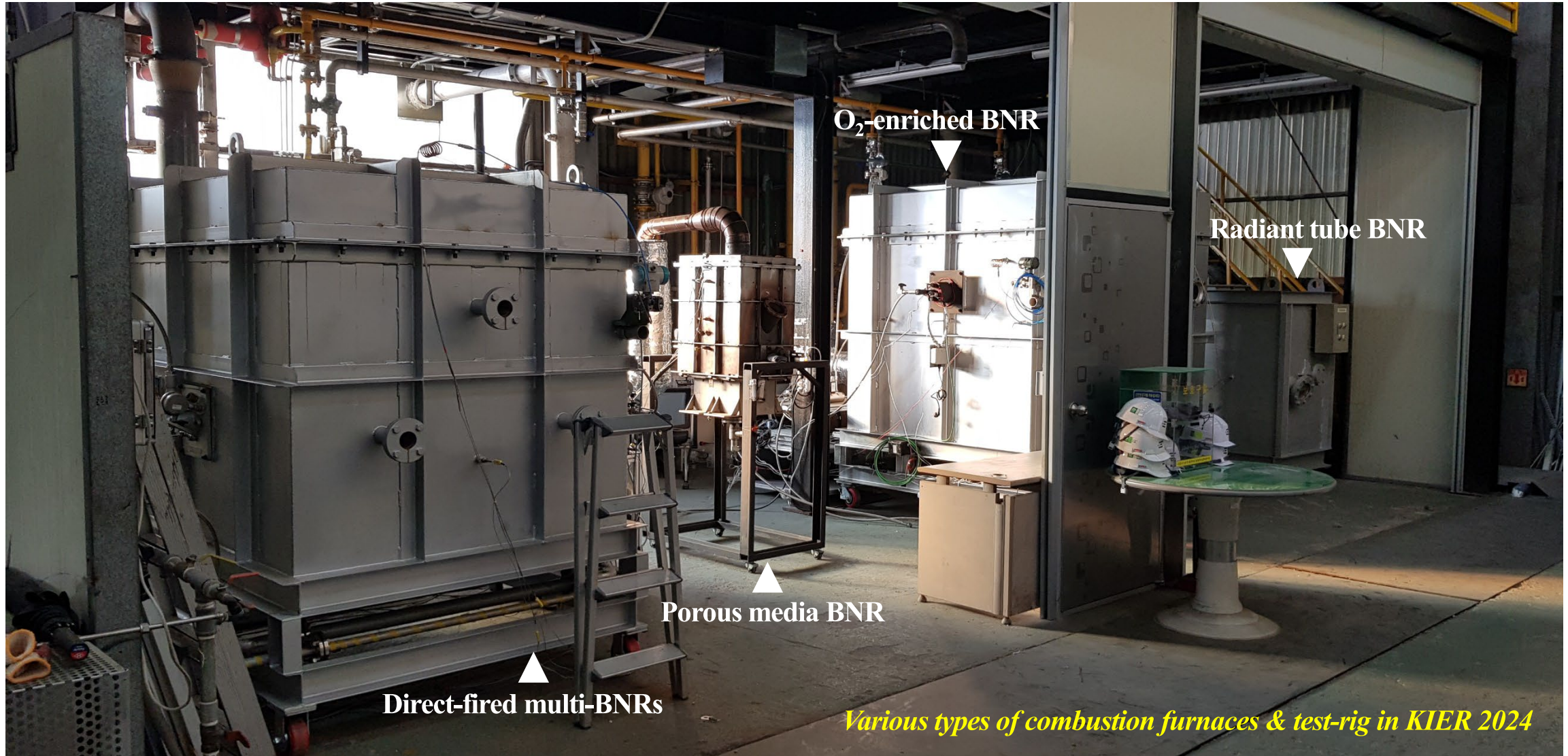
➤ N-complex species

- NO, NO₂, N₂O, (slipped) NH₃
- Simultaneous reduction

KIER SCR Catalyst



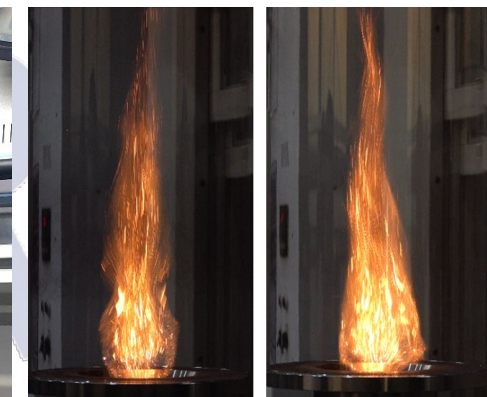
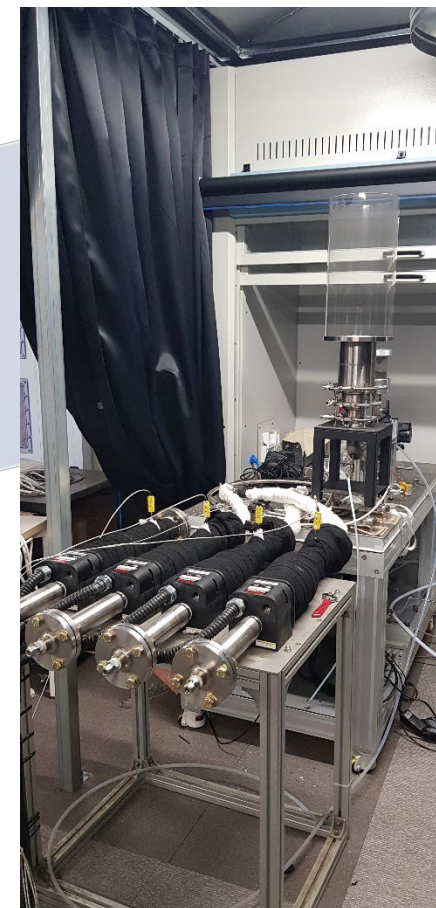
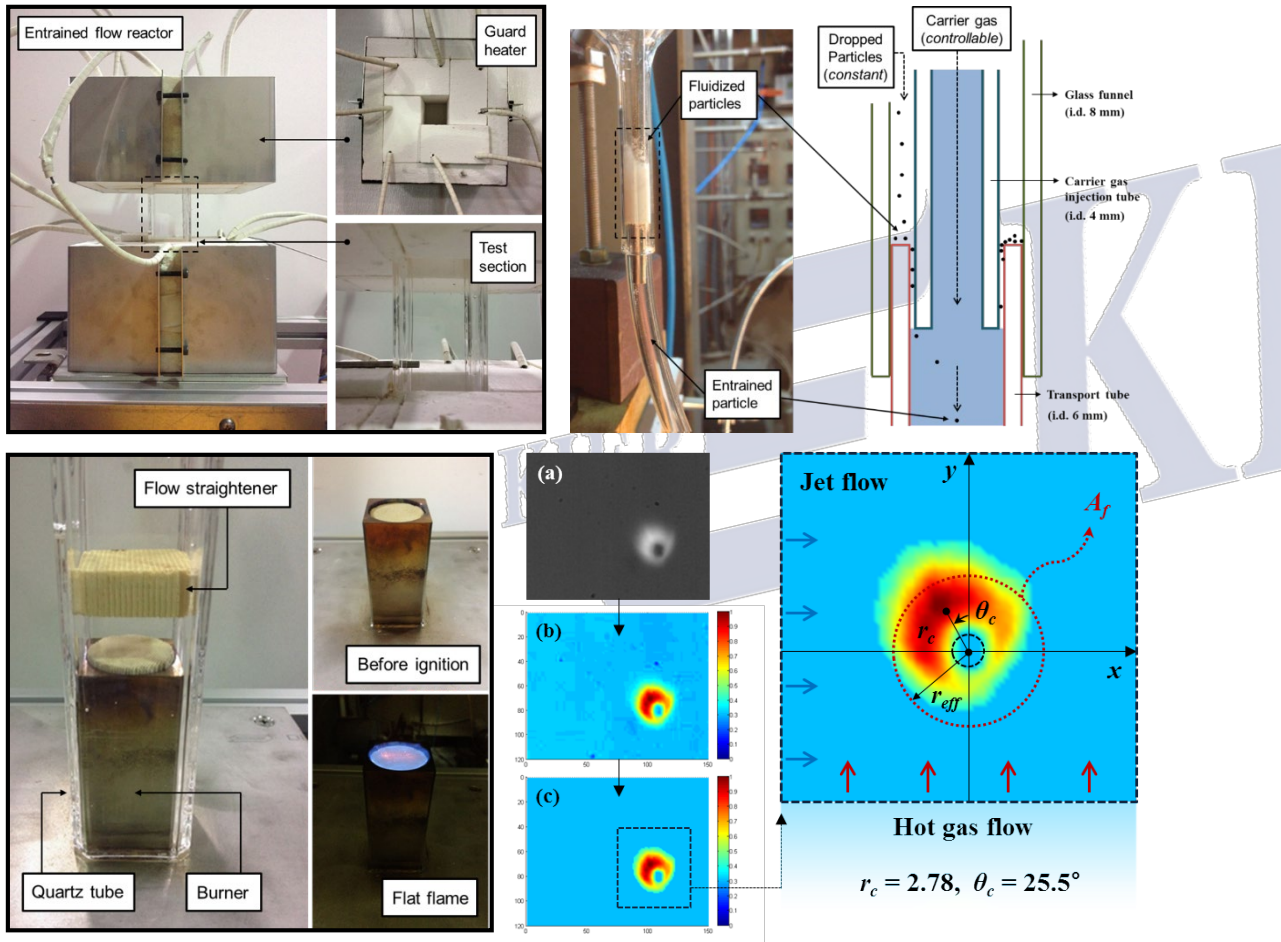
NG-NH₃ Co-firing Facility at KIER



Pulverized Coal-NH₃ Co-firing Facility at KIER

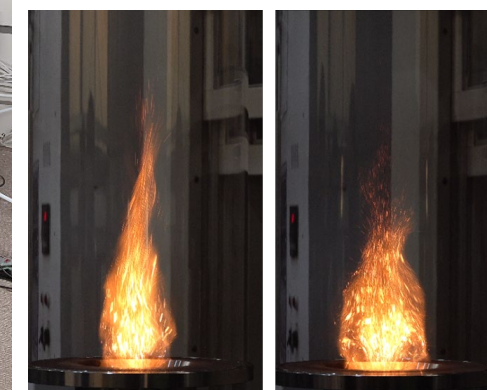
「 Single coal particle combustion system 」

「 30 kW PC & NH₃ Co-firing Flame-Emission Measurement 」



Coal 100%

80:20 (PA)



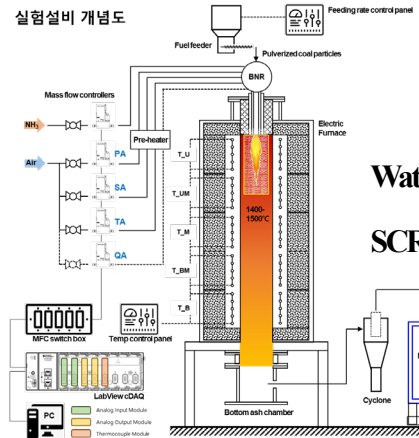
80:20 (TA)

80:20 (QA)

Pulverized Coal-NH₃ Co-firing Facility at KIER (cont'd)

「 30 kW PC-NH₃ co-firing system (single BNR) 」

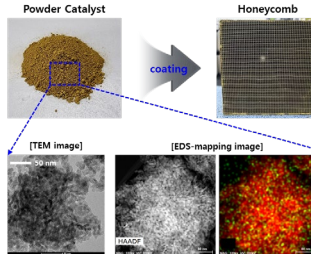
「 1.0 MW PC & Gas fuel co-firing combustor (single BNR) 」



KIER Absorbent

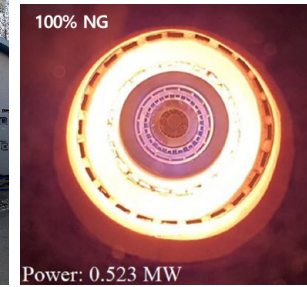
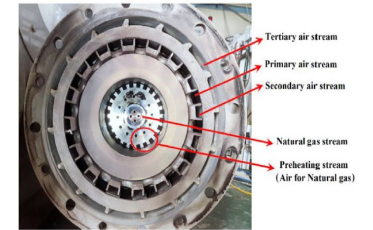
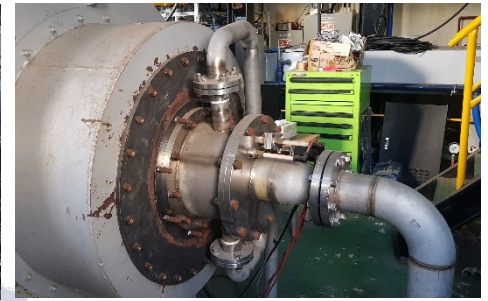
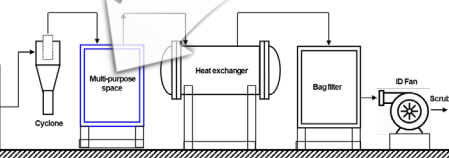


KIER SCR Catalyst



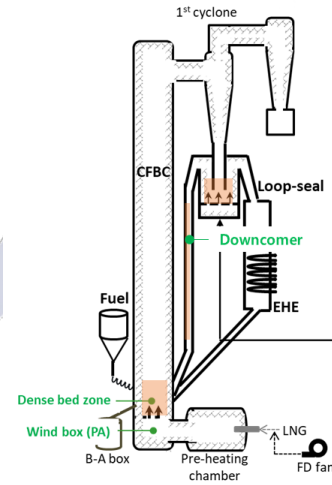
Water tube corrosion properties

SCR catalyst performance

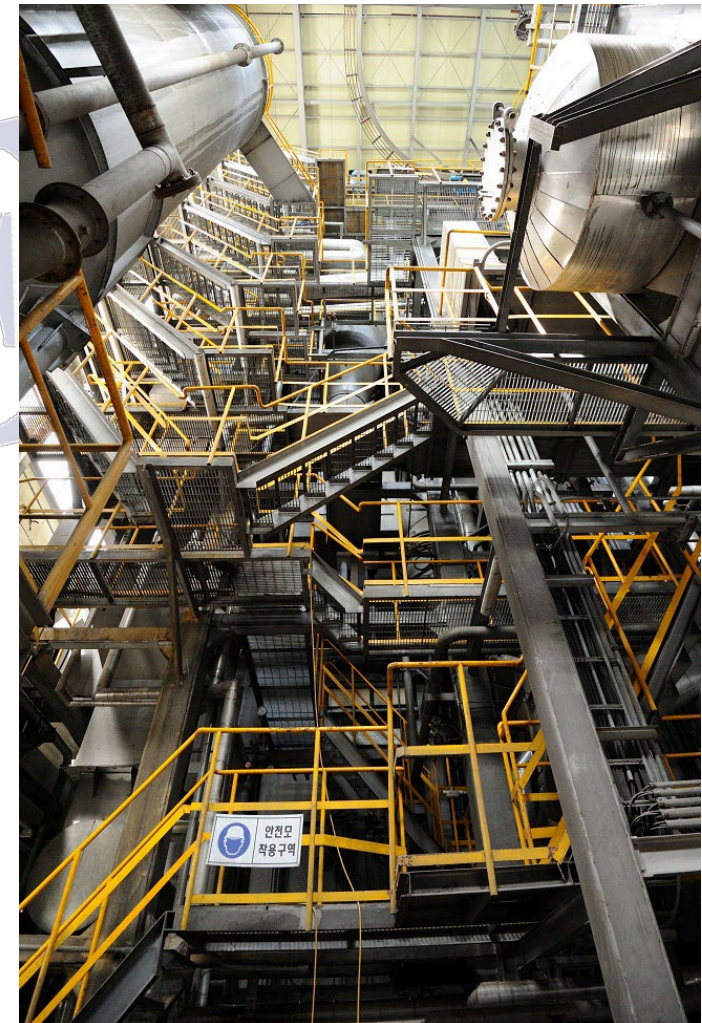


NH₃ Co-firing (coal/biomass/waste) Facility in CFB at KIER

「 100 kW NH₃ co-firing CFB system 」



「 10 MW NH₃ co-firing CFB system with steam TBN (2 MWe) 」



에너지기술연구원, 국내 최초 암모니아 혼소기술 개발

100 kW급 순환유동층 시스템
암모니아 혼소 운전 기술 확보
기존 발전소에서 정량발전 가능



【뉴스인포】 안전을 지향한 전력수급의 안정성을 확보하면서 석탄발전용 청정발전으로 전환시킬 '암모니아 혼소' 기술이 국내 최초로 개발됐다.

한국에너지기술연구원(원장 김홍진) 청정연료연구실 운영팀 박지 연구진은 국내 최초로 순환유동층 연소시스템에서 이산화탄소 발생을 감축시키는 암모니아 혼소 기술을 개발했다.

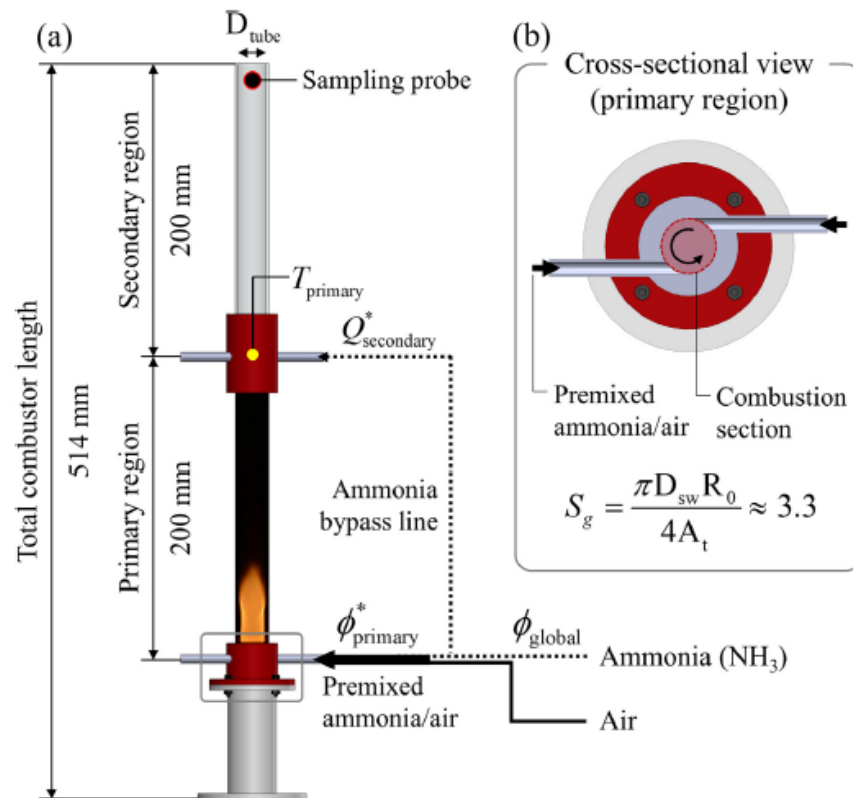
석탄화력발전소 열병합발전소에서 암모니아 혼소 기술은 기존 발전 플랜트 및 송배전선로 등 전력 인프라를 그대로 활용(해조)할 수 있다는 장점이 있다. 또한 재래에너지 건설비용 차감 수급 불균형 해소는 물론 더 나아가 탄소중립 선진국목, 1000kw급 및 탄소중립발전소 등에 대응이 가능하다.

그러나 세계적으로 순환유동층 암모니아 혼소 분야에 대한 기술이 전무한 상태. 발전분야에서 암모니아를 연료로 이용하기 위한 국산 기술 확보가 시급하다.

Fundamental Researches for 100% NH₃ Combustion

➤ Study on stability and emission characteristics of ammonia-air flames in globally lean - locally lean two-stage combustion condition

- Tangential injection combustor
 - : Intense angular momentum
 - : Remarkable mixing performance



Measurement techniques

- Flame stability limit
- Recorded flame detachment/blowoff conditions
- Emission measurement
- FTIR (Fourier Transform Infra-Red) system
- NO (corrected) and N₂O concentration in ppmvd
- NO was adjusted by the theoretical O₂ concentration
- Secondary ammonia injection
- To reduce massive fuel NOx emissions by using SNCR reaction (Thermal DeNOx process)
- Ammonia feeding lines were distributed into primary and secondary injection ports

Test conditions

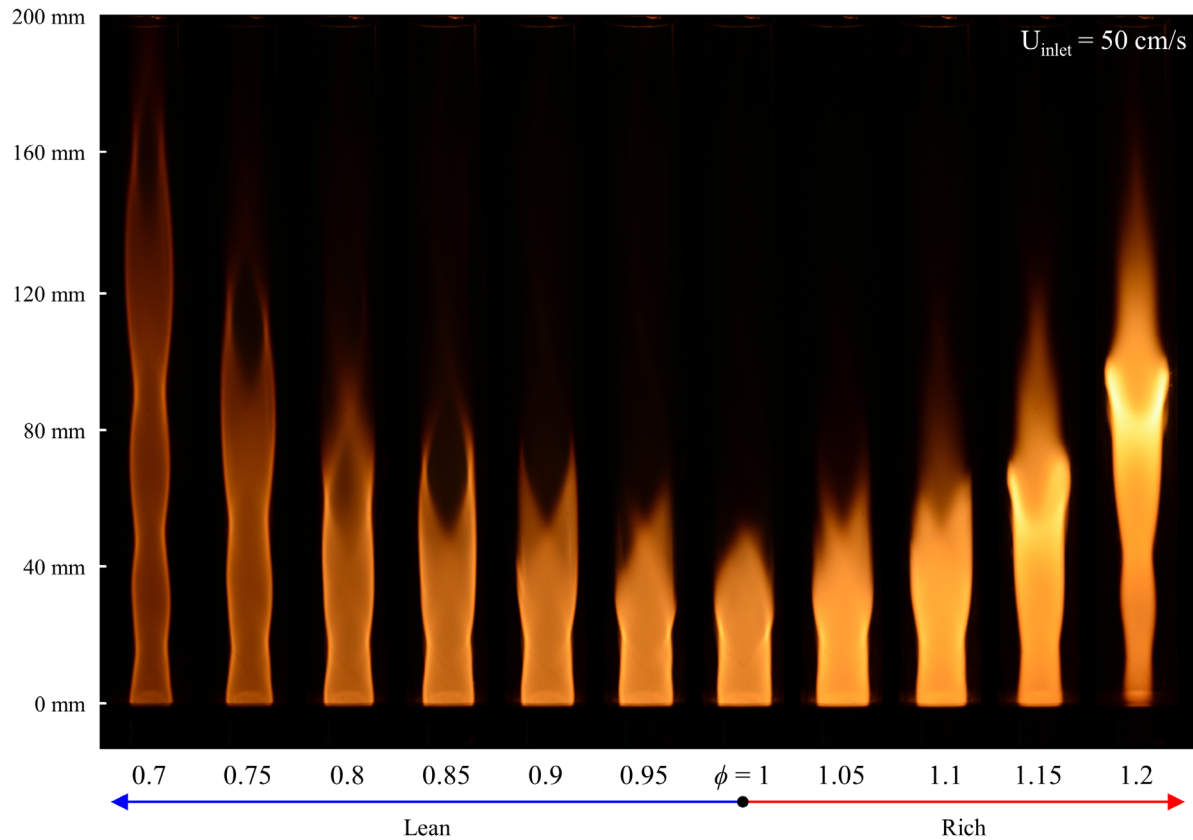
- $U_{\text{inlet}} = 10 \sim 200$ cm/s
- $\phi_{\text{global}} = 0.60 \sim 1.3$
- $\phi_{\text{primary}}^* = 0.75 \sim 0.95$ ($Q_{\text{secondary}}^* = 0.1 \sim 0.4$ SLPM)

Fig. 1. (a) Schematic of a fuel-staged, tangential injection combustor with an emission measurement system, (b) Cross-sectional view of a primary combustion zone.

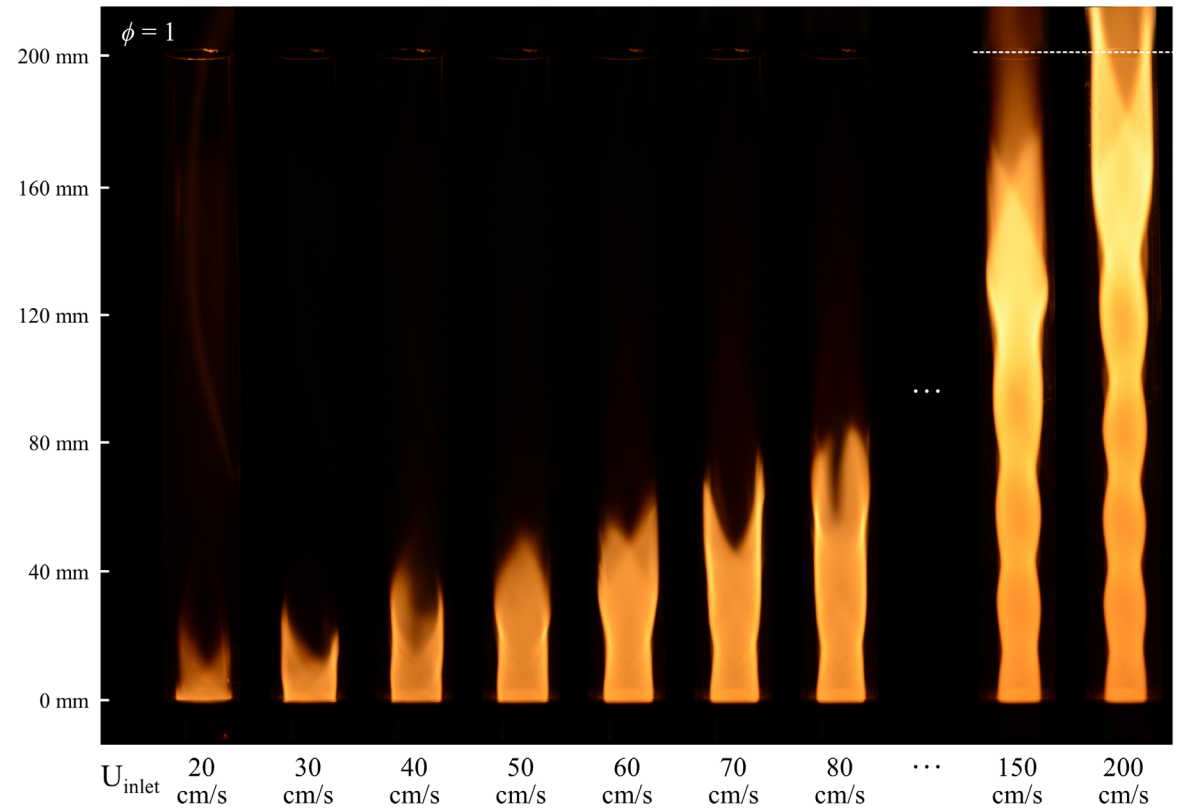
Apparent Flame Structures

➤ Effects of equivalence ratio (ϕ) and inlet velocity (U_{bulk}) on flame structures

「 Equivalence ratio effect 」



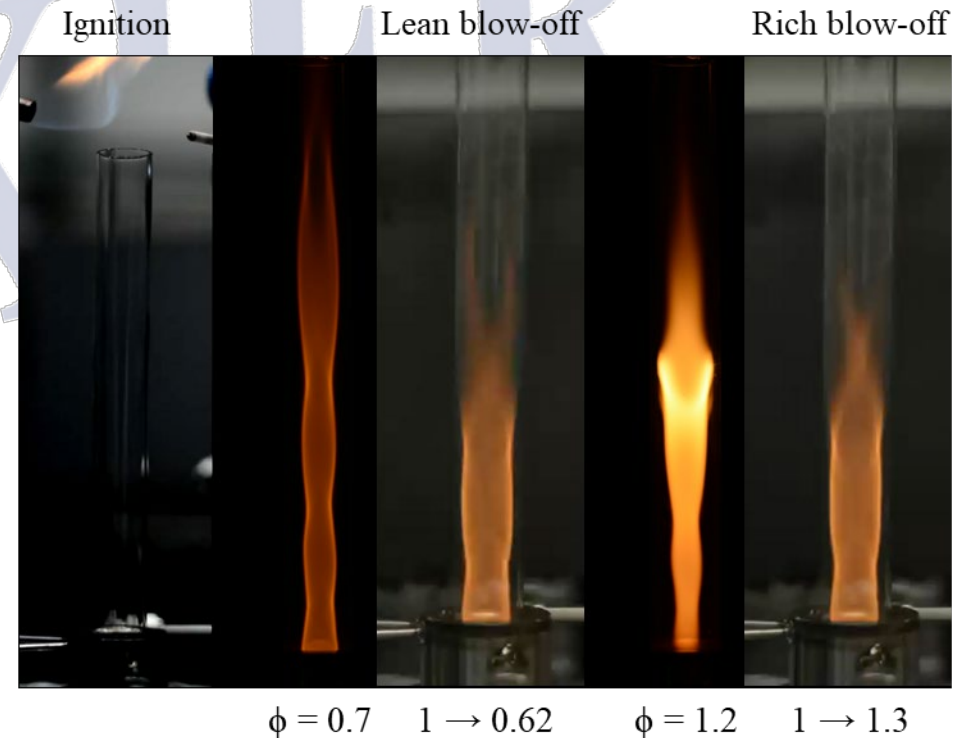
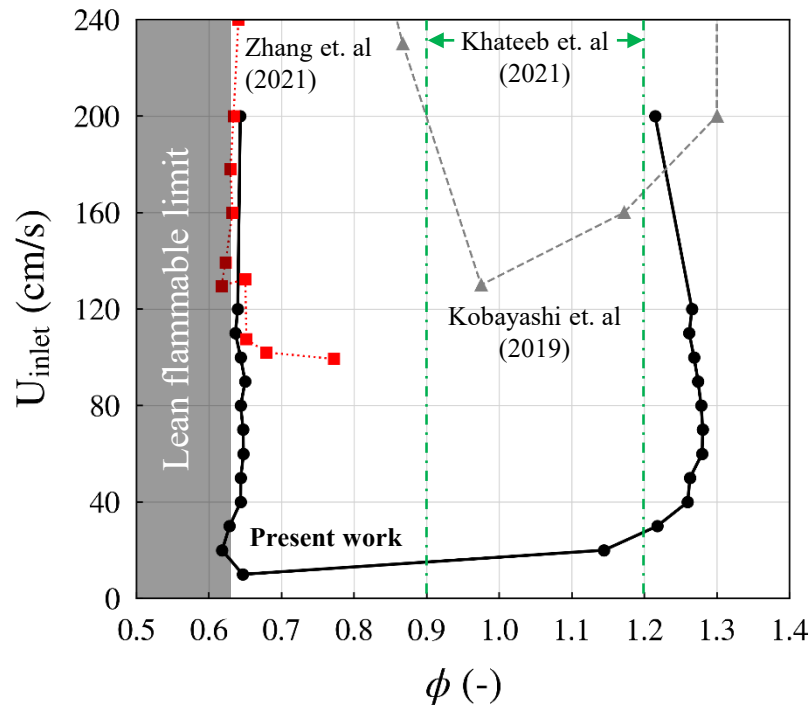
「 Inlet velocity effect 」



Flame Stability Characteristics

➤ Stability map of the premixed NH₃ flame and varying flame structures with respect to the global equivalence ratio

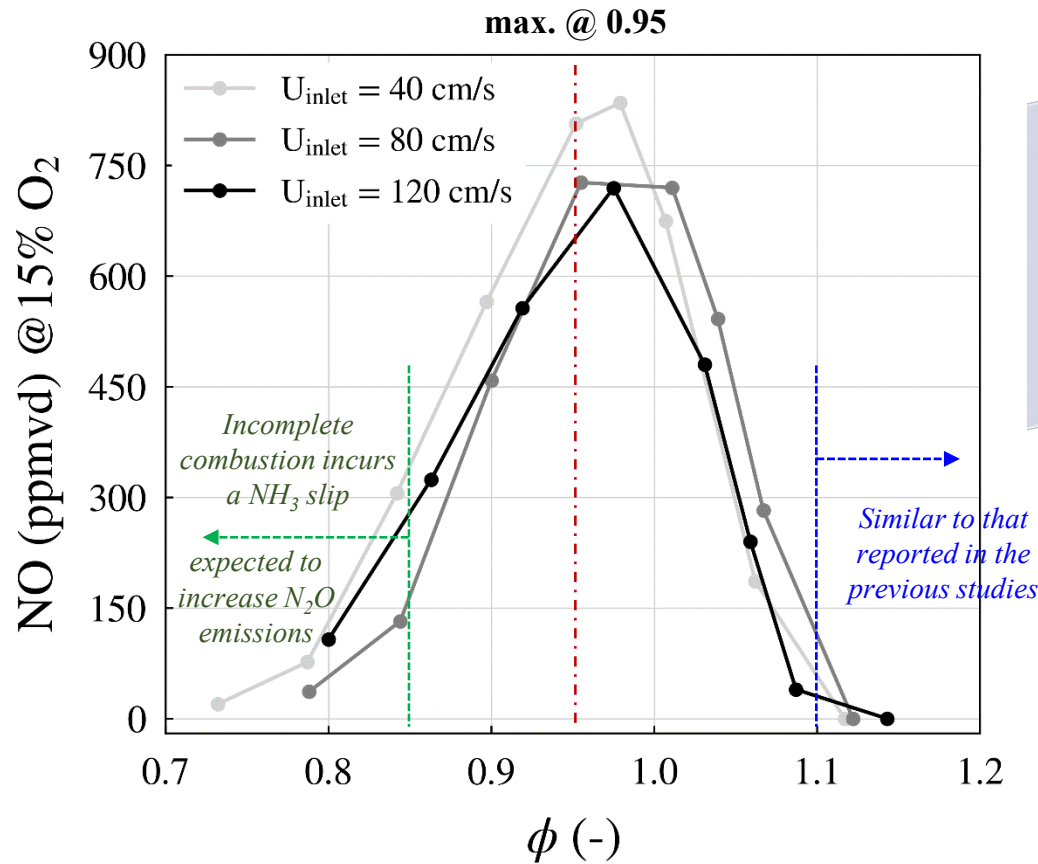
- Premixed ammonia flames in the high-swirl combustor are stabilized even in the vicinity of lean flammable limit and at low velocity condition of 10 cm/s, and have a relatively wide range of operation window.
- Lean and rich blow-off processes are markedly different, especially for the initial point of flame extinction.



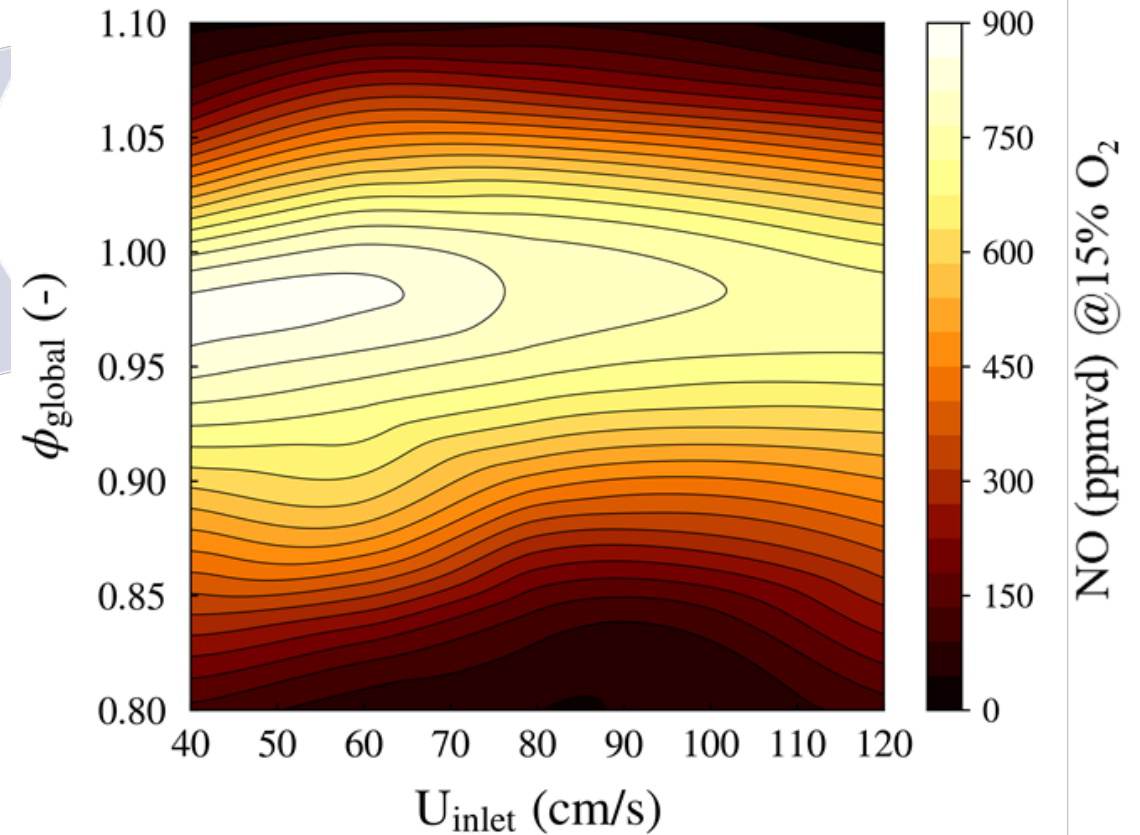
Emission Characteristics

➤ **Exceptional NO emission trend under lean conditions, the abrupt decrease in [NO] in the rich-burn regime is similar to that reported**

- Salient feature of low [NO] is observed but it is associated with heat loss through the wall and ambient inlet mixture temperature
- Increasing U_{bulk} give rise to a gradual increase in the NO mole fraction due to the elevated T_{primary} → Improved combustion efficiency

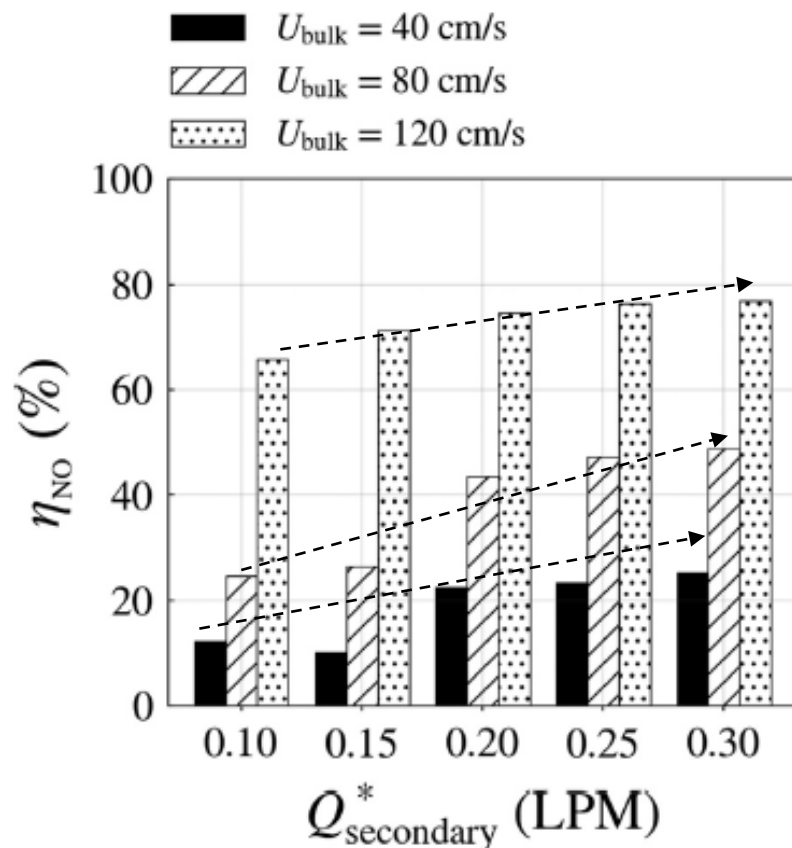


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Emission Characteristics with Fuel Staging

➤ To maximize the NO reduction rate, delicate control of the temperature distribution by the U_{bulk} and Φ is pivotal in this strategy



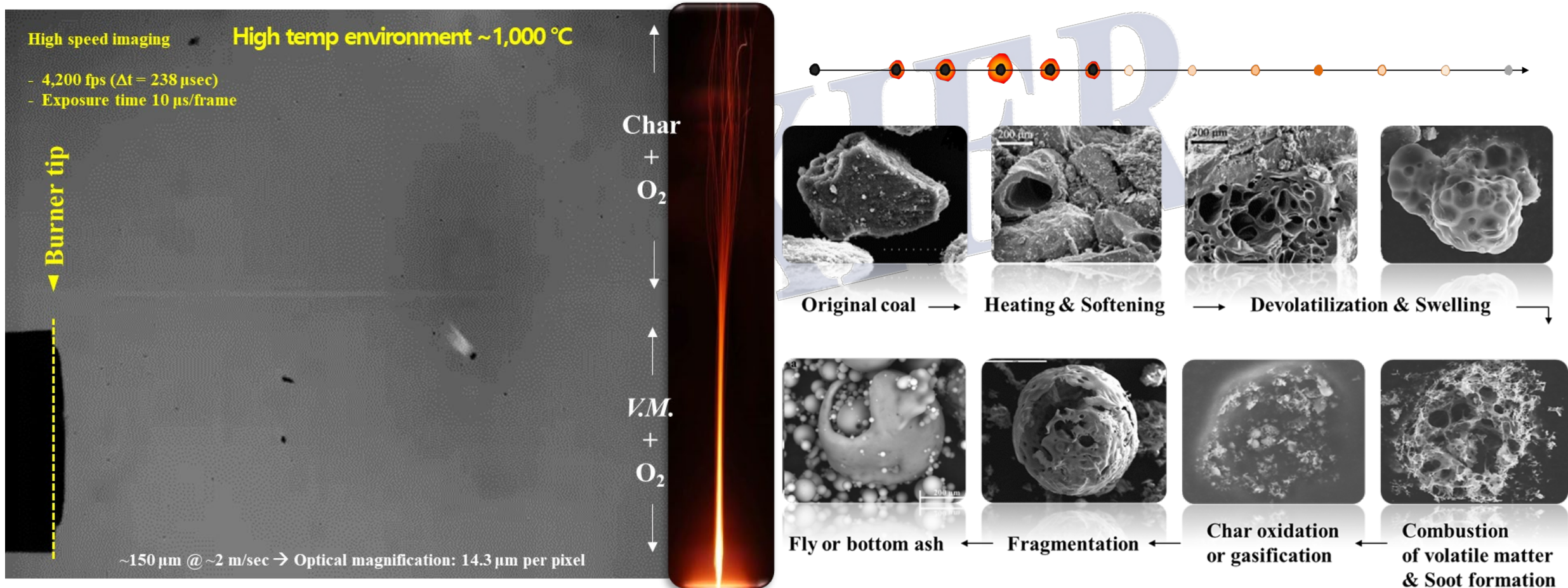
$$\eta_{\text{NO}}(\%) = \left\{ 1 - \frac{[\text{NO}]_{\text{staging}} | \phi_{\text{primary}}^*}{[\text{NO}]_{\text{baseline}} | \phi_{\text{global}} = \phi_{\text{primary}}^*} \right\} \times 100$$

NO reduction rate dramatically increased with increasing bulk velocity as a result of the elevated temperature

- $U_{\text{bulk}} = 40$ cm/s
 - NO emissions decreased by up to 25% when $Q_{\text{secondary}}^*$ is 0.3 LPM ($\phi_{\text{primary}}^* = 0.77$)
- $U_{\text{bulk}} = 120$ cm/s
 - $T_{\text{primary}} = 680$ °C promotes a substantial NO reduction of up to 77% despite the small addition of the bypassed NH_3 , which corresponds to 8% of the total fuel flow rate
 - Nevertheless, it could not reduce the [NO] below 160 ppmv
- Over $U_{\text{bulk}} = 120$ cm/s
 - Elongated flame structure went beyond the primary region
 - Then, NH_3 is directly burned ammonia instead of facilitating the SNCR process.

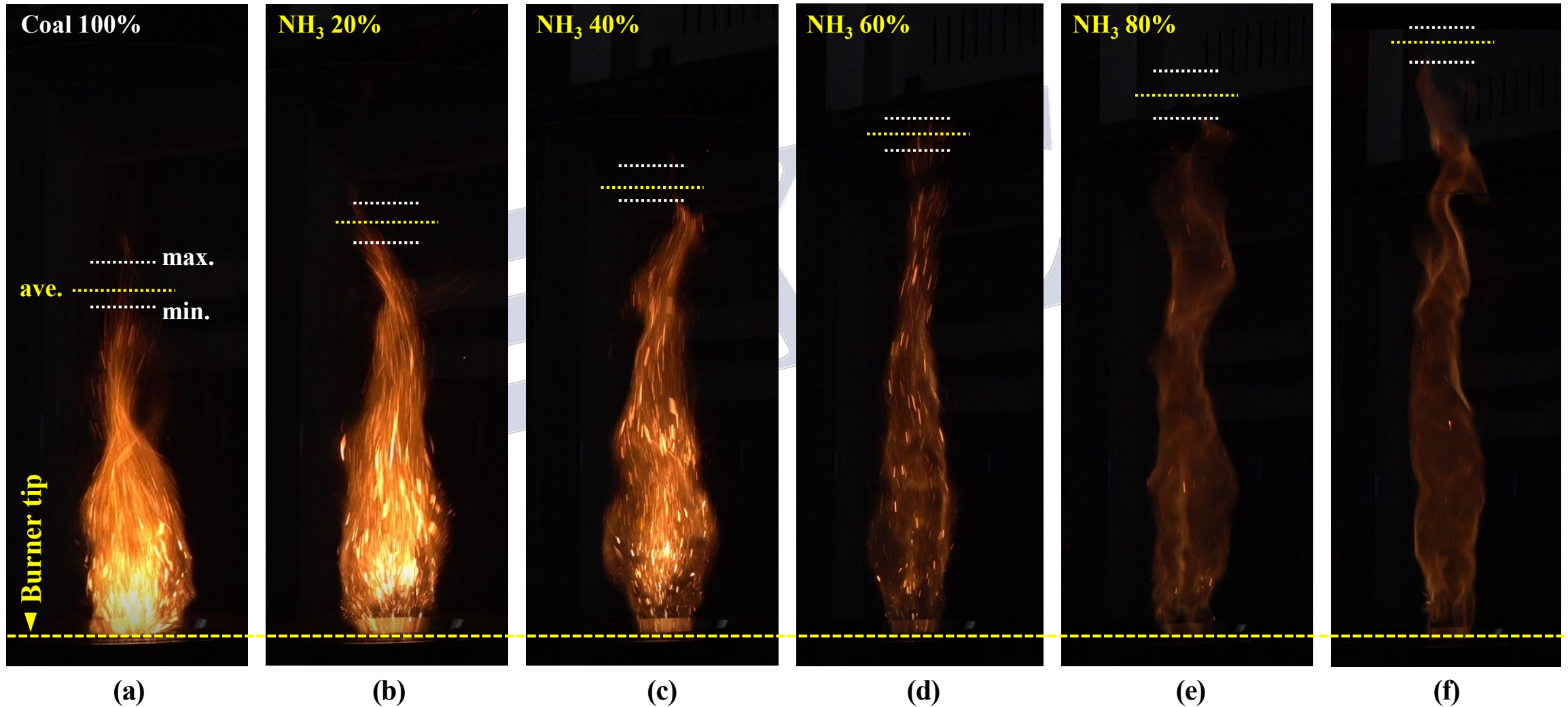
Phenomenological Characteristics of PC Combustion

- For approach to detailed observation : $d_p \sim 100 \mu\text{m}$ moving at $\sim 3 \text{ m/s}$, Time resolution (Δt) $\sim 100 \mu\text{s}$, Size resolution (pixel) $\sim 10 \mu\text{m}$
- Extremely heterogeneous behavior : Unable to expect uniform data when using gaseous fuel



Apparent Flame Behavior in PC-NH₃ Co-firing Conditions

➤ Flame shape according to ammonia co-firing rate, when ammonia is injected into PA flow (30 kW_{th})

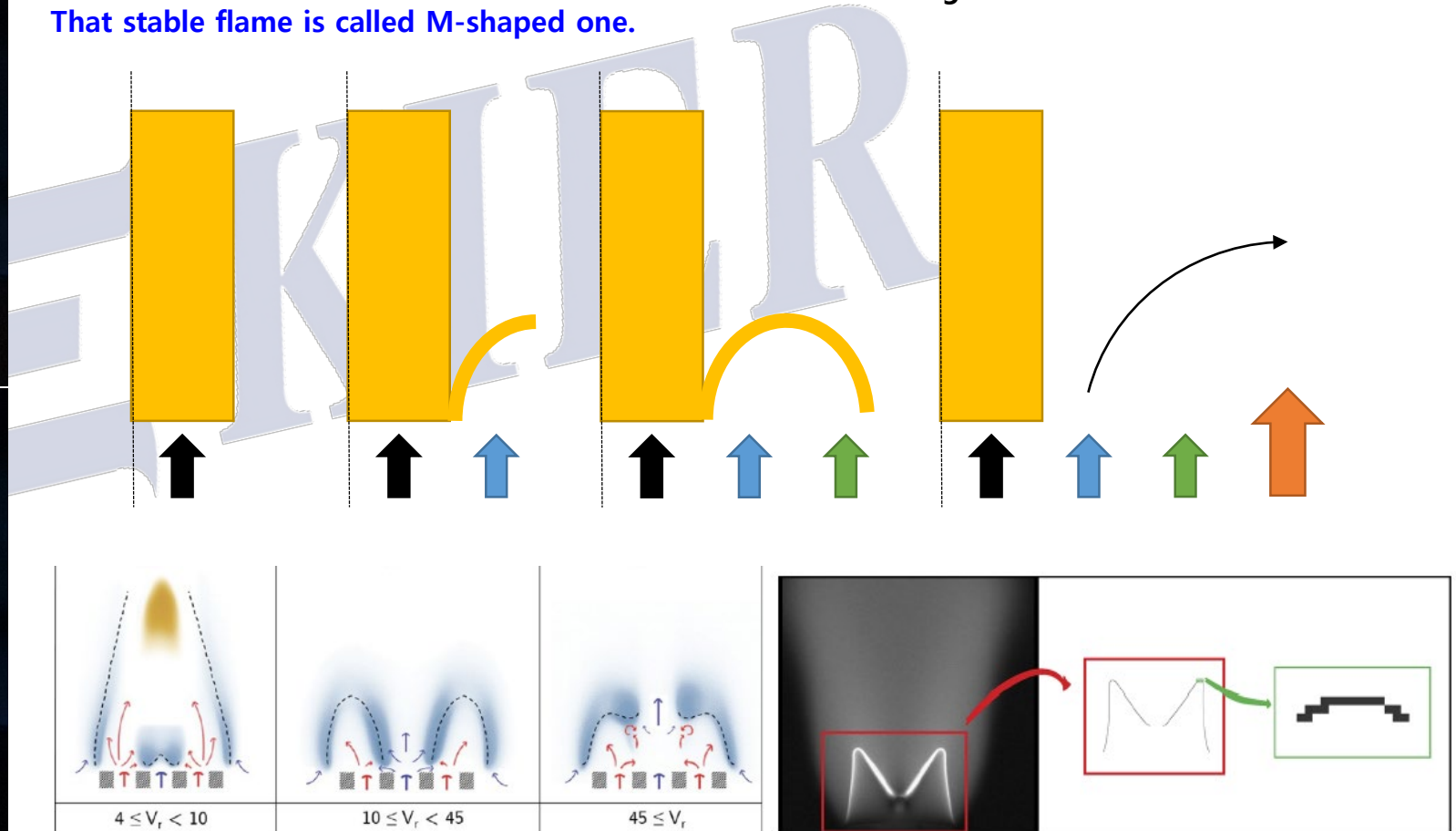


Relation between Fuel-staging and Flame Stability

- If the swirl intensity of the outermost flow is strong, it adversely affects the flame stability

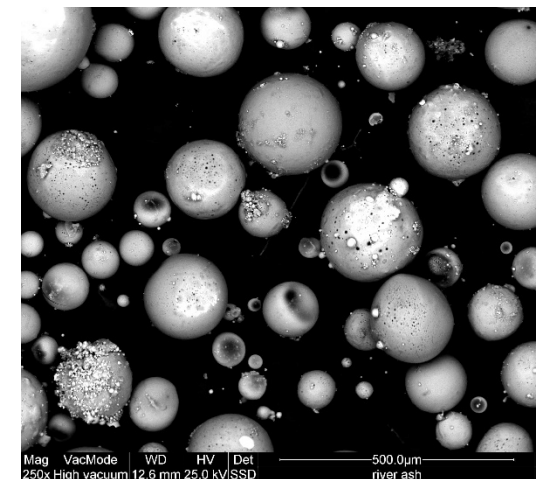
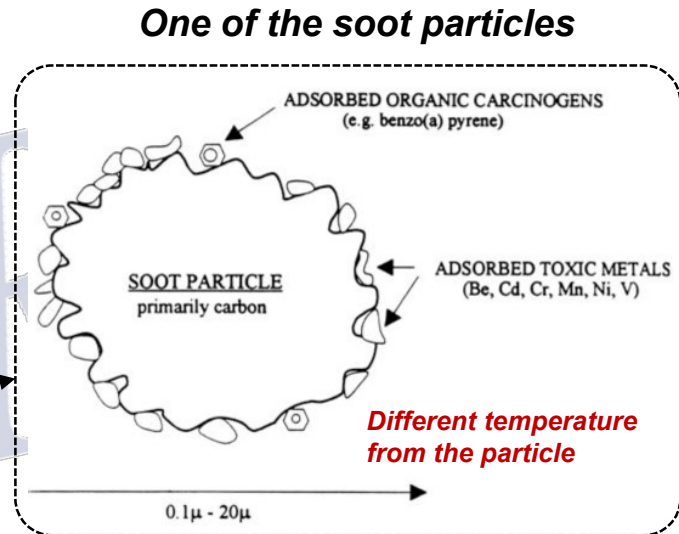
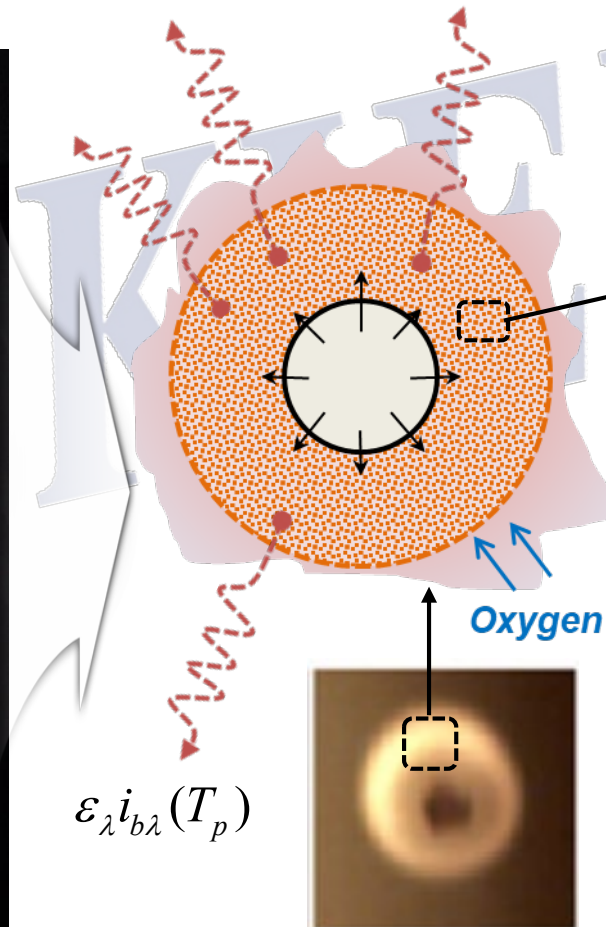
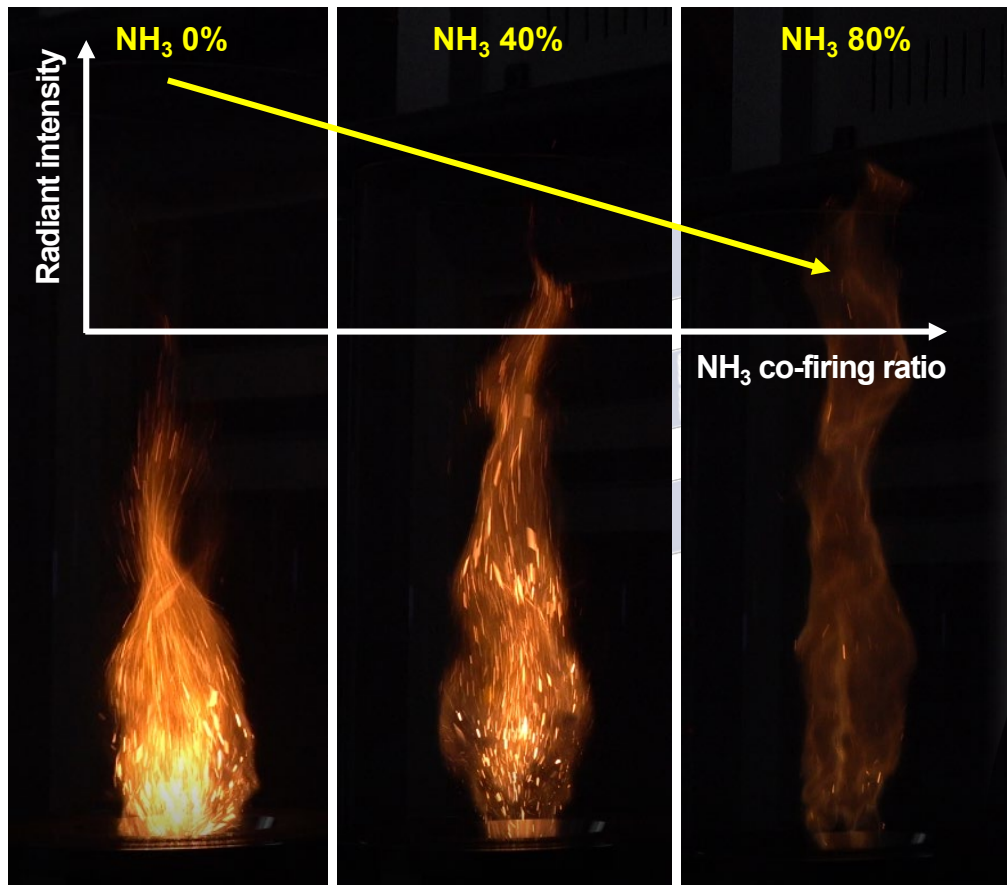


One of the stable forms of such a flame configuration is the stabilization of the front in the vortex zone behind the stabilizer and in the vortex zone at the thin edge of the nozzle. That stable flame is called M-shaped one.



PC-NH₃ Co-firing Flame Radiant Intensity

- Most radiative heat transfer is caused by the radiation of soot particles in a coal flame
- Lower coal flow (Higher NH₃ co-firing ratio) → Lower radiant intensity



Y.A. Levendis (2013)

North Carolina Health News

Proper NH₃ staging induces the SNCR (selective non-catalytic reduction) effect

- Excessive staging causes NH₃ slip
- A small amount (~ 10 ppm) of N₂O is also generated from pulverized coal co-firing conditions

PC- 20% NH₃ co-firing can be overcome with well-controlled combustion techniques

High co-firing rate or NH₃ combustion requires new nozzle design

- Will it create a stable flame? Would you be satisfied with adding NH₃?

NH₃-ready burner design is required considering NH₃ supply (commercial)

- Global R&D trends indicate that no facilities can use only one fuel

Please e-mail any questions to :

Dr. Hookyung Lee (hk.lee@kier.re.kr)



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