

A wide-angle photograph of an industrial facility, likely a power plant or refinery, with several tall smokestacks emitting white plumes of smoke. The facility is situated behind a large, green agricultural field with distinct rows of crops. The sky is blue with scattered white clouds.

## AMMONIA GAS TURBINE COMBUSTOR

**UTSR Meeting 2024**

DE-SC-002093

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Irvine, CA

09/25/2024

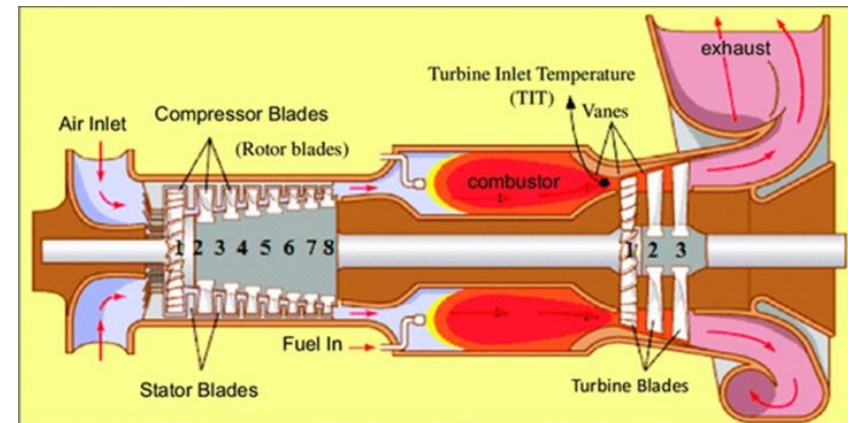
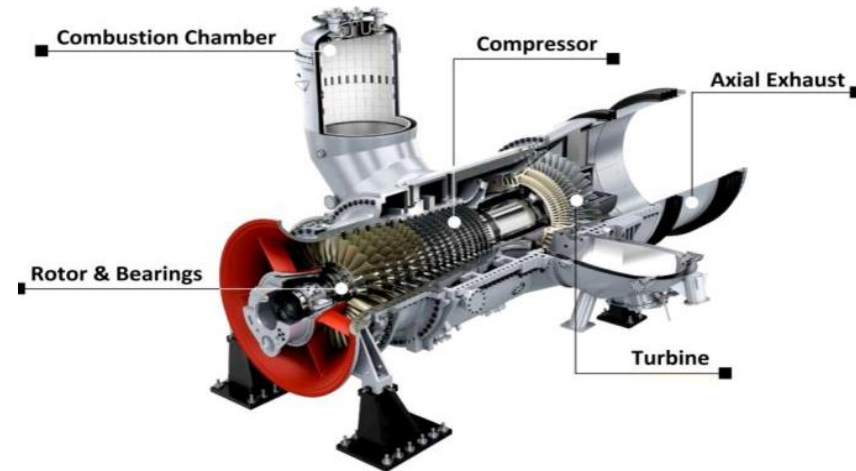


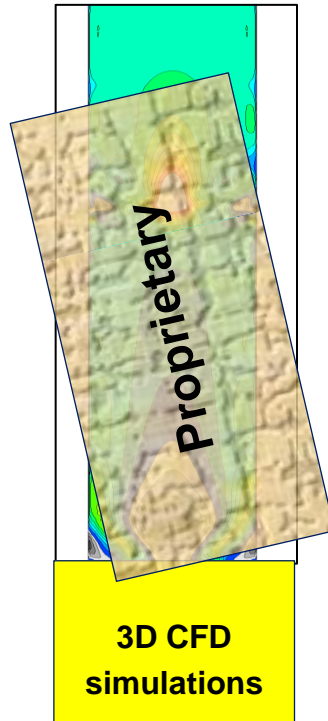
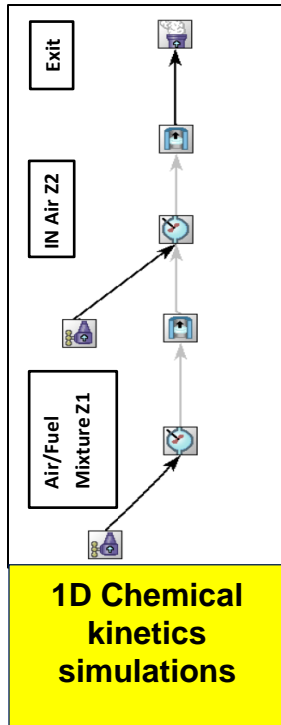
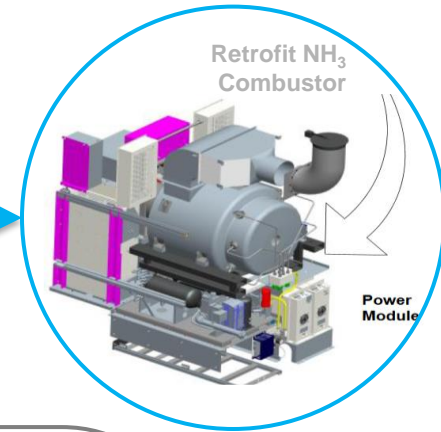
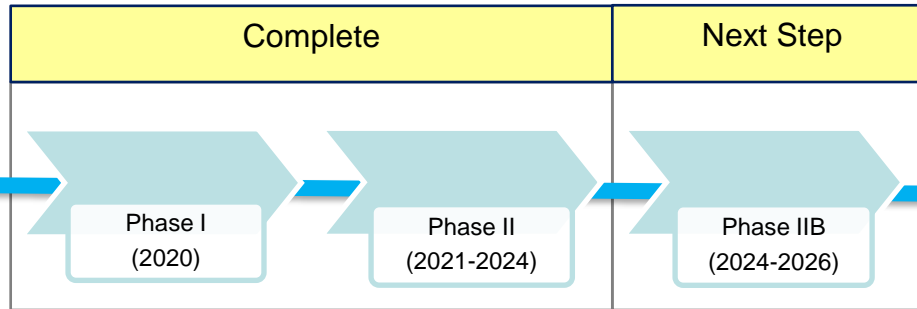
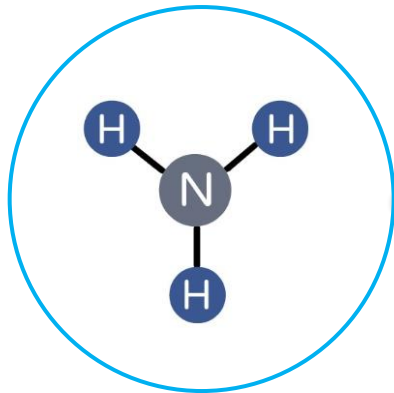
**UCI Combustion  
Laboratory**






UCIrvine | UNIVERSITY  
OF CALIFORNIA

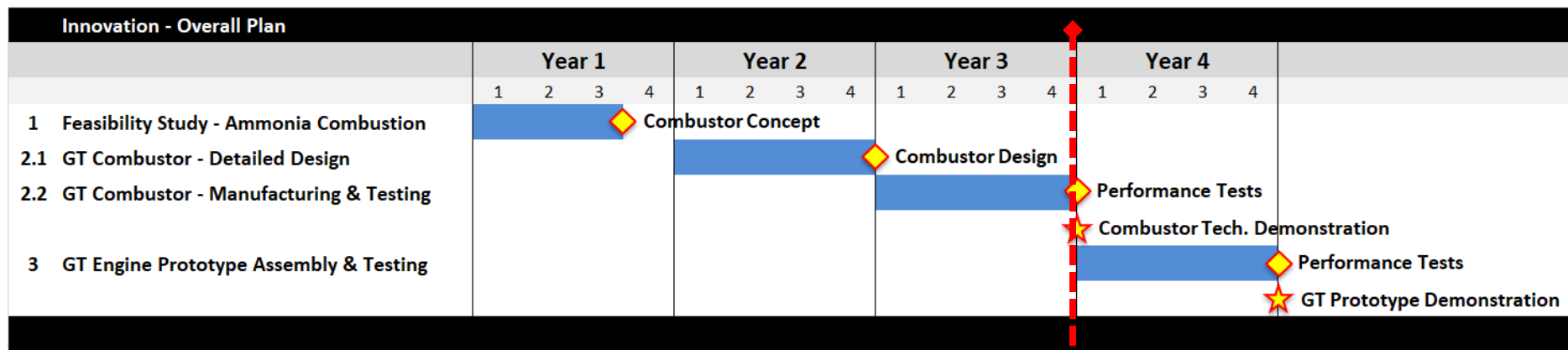
# Introduction

- Objective – Develop an ammonia combustor that will be retrofitted into a gas turbine and operate the engine across all load levels.
  
- Design goals and criteria
  - Complete burnout of fuel
  - Minimize NO<sub>x</sub> emissions at engine exit at all loads
  - Stable conditions – Low thermoacoustic vibrations
  - Reduced cost (capital cost, operating costs, maintenance, etc..)





- Stable ammonia flames 
  - Reactants' ignition method
  - Flame equivalence ratios
  - Hydrogen mass fraction if any?
- Burner and Combustor Concept 
  - One or two combustor zones
  - Aero concept designs
  - Fuel and air flows
- Pollutants' emission levels at combustor exit 
  - $\text{NH}_3 < 1 \text{ ppm}$
  - $\text{NO}_x < 100 \text{ ppm}$  (15% Excess  $\text{O}_2$ )
- Combustor outlet conditions (mass flow and temperatures) to drive GT cycle 
- Down-selection industrial Gas Turbine 



Current Status

## Challenges for Ammonia Combustor

- Ignition on 100% NH<sub>3</sub>
- Flame Stability
- Low Emissions across all engine load levels
- Translation to physical design

## Parameters analyzed to address challenges

- Burner Stabilization Method
- Equivalence Ratio
- Air Inlet Temperature
- Pressure
- Residence Time

- Microturbine Engine Selection criteria:
  - Relatively small engine size with a recuperative capability (Advantageous for Decentralized Power).
  - Combustor inlet air temperature should be as high as possible to facilitate ammonia ignition and flame stability.
  - Easy modification of the combustor section

All state-of-the-art gas turbines natural gas combustion systems are characterized by the following:

- They are based on **premix combustion** concept at full engine loads
- **Combustion temperatures** are maintained below the threshold of high rates of formation of thermal NO
- The burners rely primary on **swirling flows** that maintain internal recirculation zone close to burner exit to stabilize the combustion process.
- The burners operate under **mixed operation conditions** (premix/diffusion) at engine medium load levels.
- The burners operate under **diffusion combustion conditions at low loads.**
- Burner startup is managed under diffusion mode of operation.

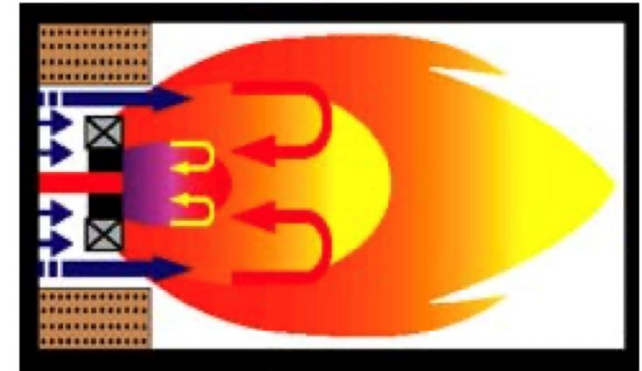


Fig. 1. Non -TVC Swirl Stabilized Combustion (Courtesy of National Combustion Equipment, Inc.)

Limitation of current technologies:

- Management of thermoacoustic vibrations due to flame instabilities
- High emissions at medium and low load levels,  $NO_x$ , CO
- No possibility to startup the burners under premix mode of operation
- Combustor outlet temperature Spread (TAT spread); overheating of combustor liners and stage 1 vanes

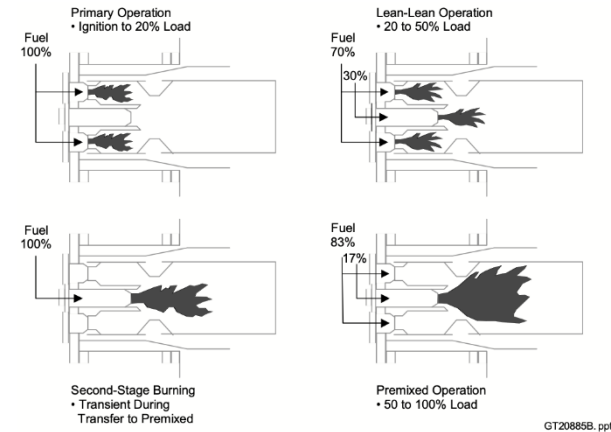
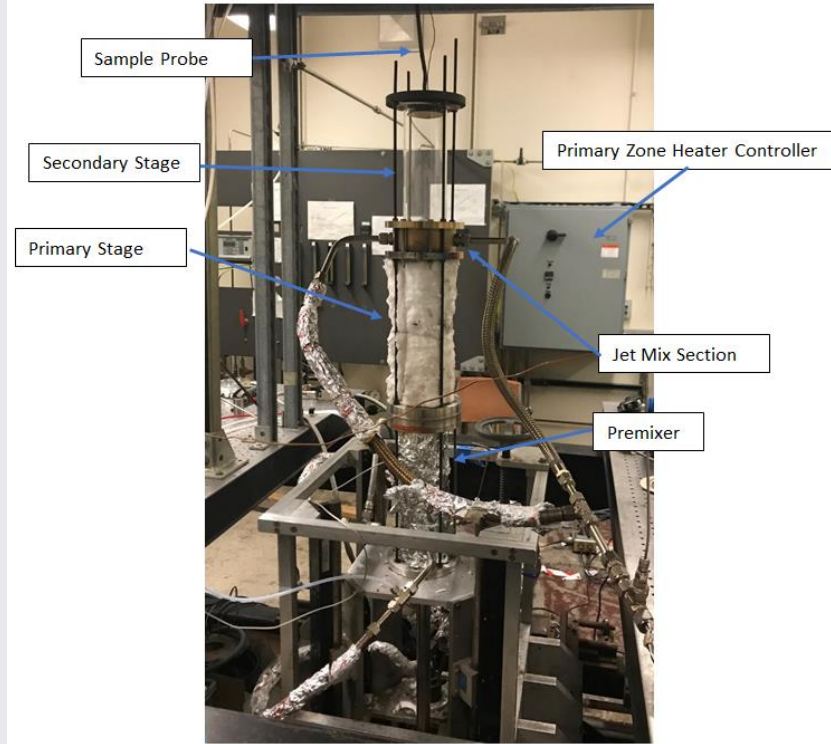
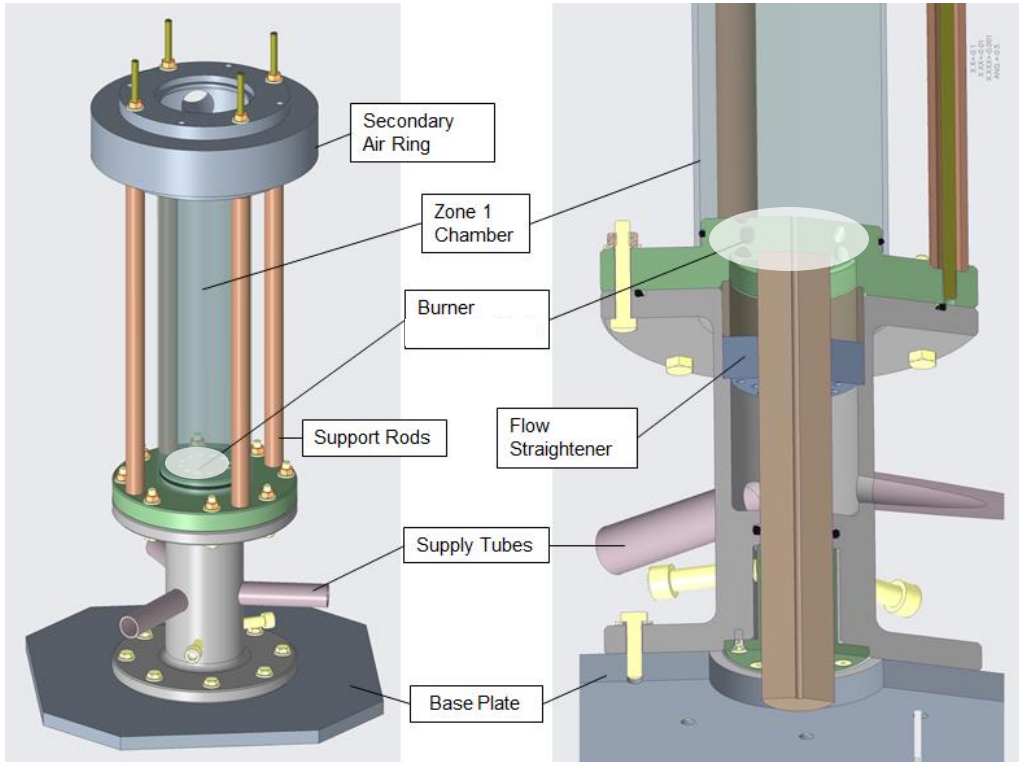


Fig 2. GE's DLN Burner System

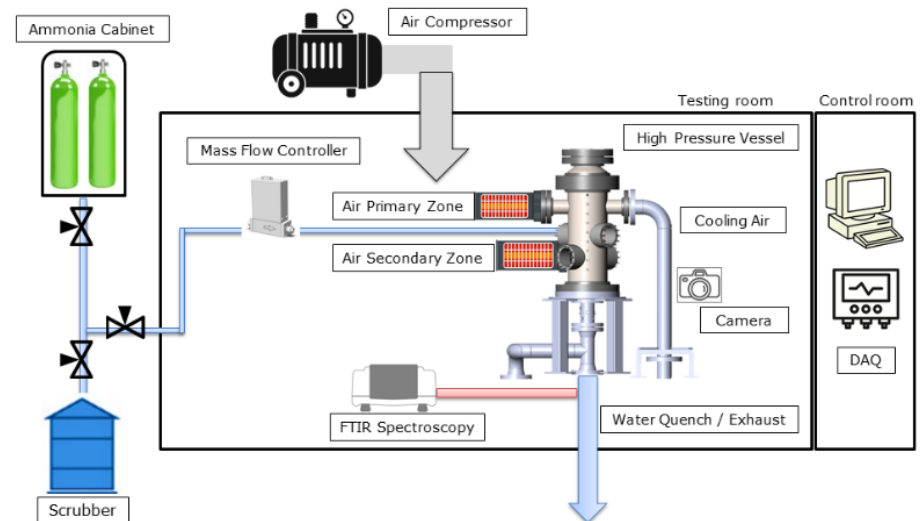
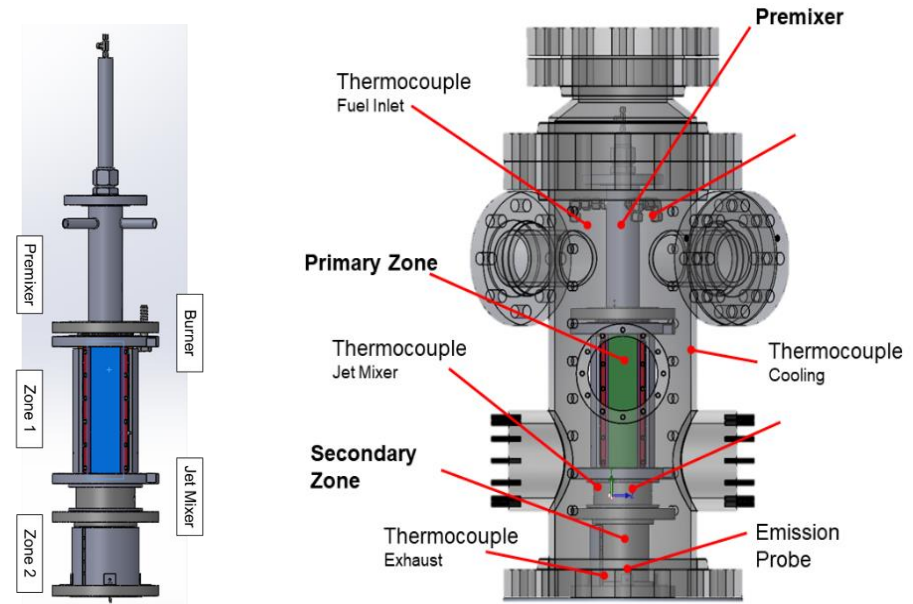
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# **Atmospheric and High-Pressure Experimental Set-up at UCICL**





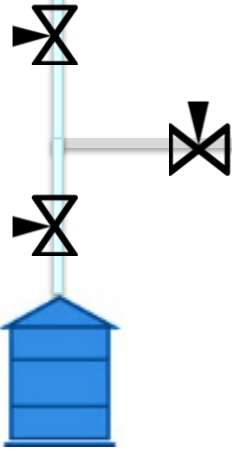
- Rig Designed to simulate ~1/2 engine cycle conditions:
  - 100 kW steady-state thermal power
  - 4 bar
  - 1200 K
  - Emissions sampling
- Concept built around standard 150 lb schedule 40 pipe and flanges
  - Optical access to the flame zone (zone 1)
  - Zone 2 is customizable modified for standard flanges
  - Exit/Cooling sleeve allows rig preheating and partial quench
- Modular Sections
  - Changeable burner plate
  - Changeable jet ring
  - Separate feed for zone 1 and zone 2
  - Separate heat for zone 1 and zone 2





**Pneumatic Valve**

**Emergency Shutdown Controller**



**Scrubber**  
• 280 gallons of water



**Anhydrous ammonia**  
• Highly irritating gas  
• Colorless  
• Suffocating odor

**Scrubber Water tanks**

**Ammonia Tank**

**Heater Blanket**  
2 kW



**Sensor #1**

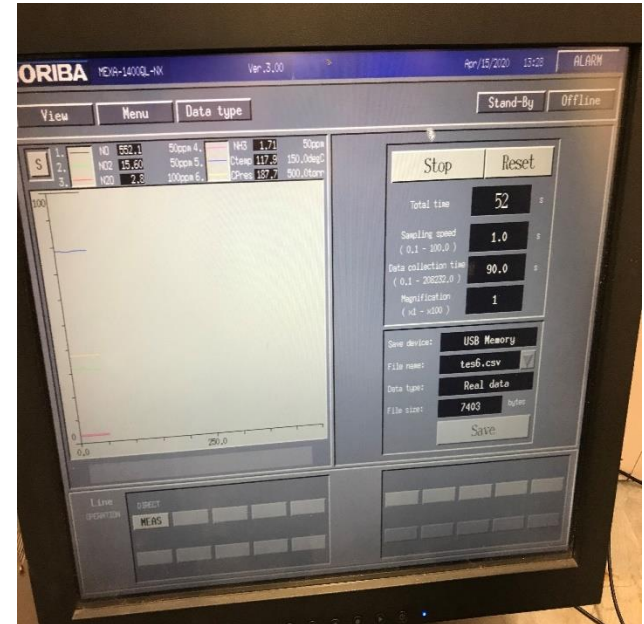
**Air Blower**

**Nitrogen Tank For Purging**

**Ammonia resistant Materials**

- Stainless Steel
- Kalrez
- EDPM
- Teflon
- Viten

- Horiba PG-250/PG-235
  - Primarily for O<sub>2</sub> measurement
- Horiba MEXA QCL-1400-NX
  - NO, NO<sub>2</sub>, N<sub>2</sub>O, NH<sub>3</sub>
- Phase II: AVL FTIR DEMO SESAM SN 3853
  - NO, NO<sub>2</sub>, N<sub>2</sub>O, NH<sub>3</sub>, H<sub>2</sub>O
- Water cooled 0.25" extractive probe located at exit of the 2nd stage
  - Corrected to 15% O<sub>2</sub> (measured O<sub>2</sub> levels)



# Ammonia Atmospheric Combustion

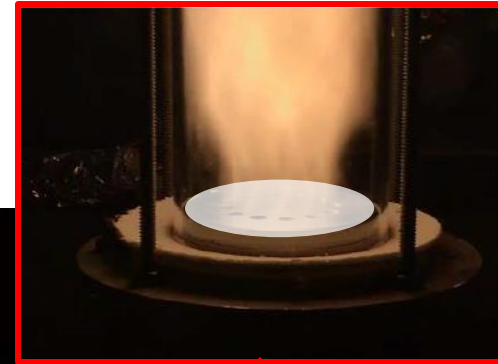
➤ Observed Stable Combustion Flames



Lean PZ

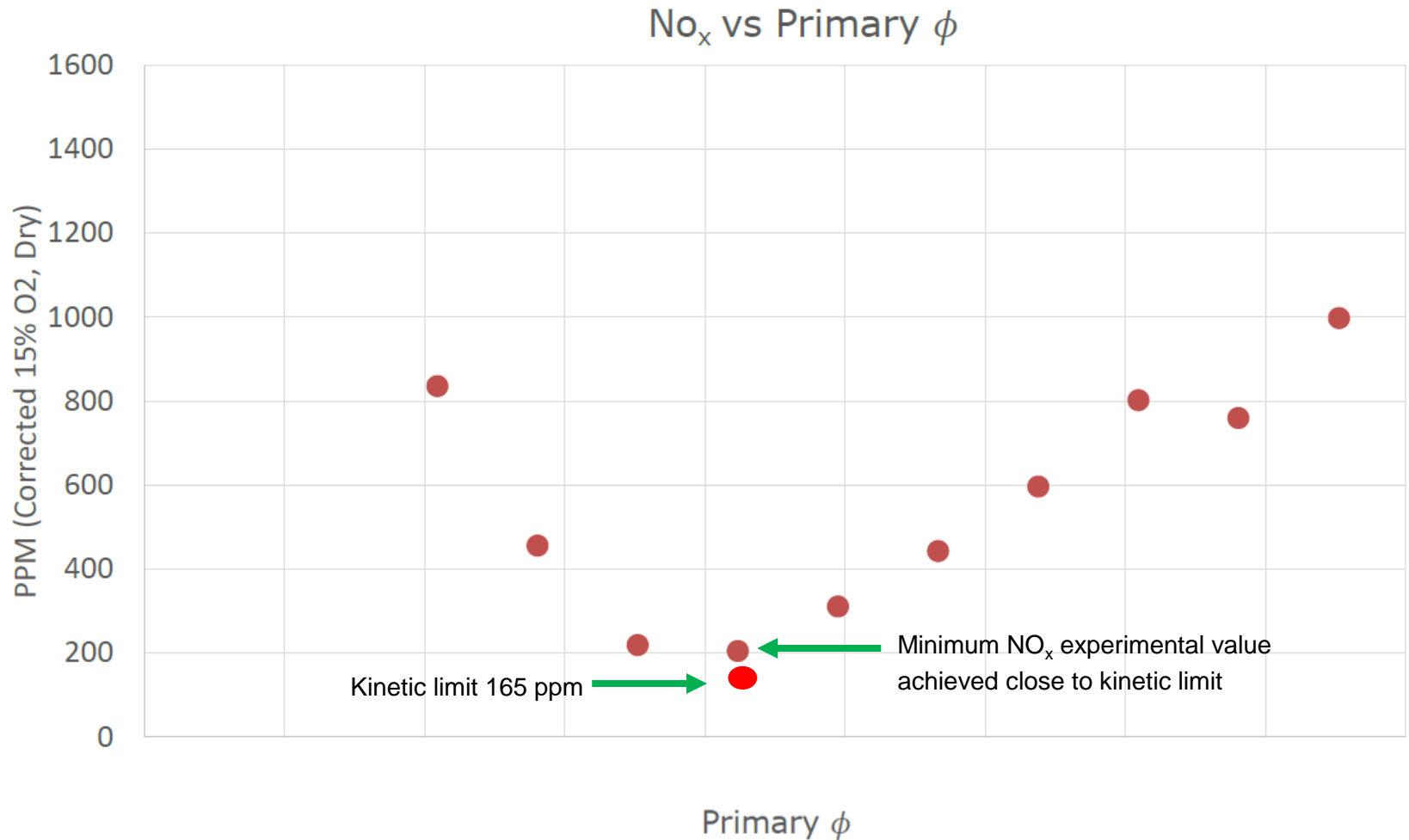


~ Stoichiometric PZ



Stable Operation attained approaching LFL for NH<sub>3</sub>/Air  
Allowed focus on 100% NH<sub>3</sub> rather than NH<sub>3</sub>/H<sub>2</sub> mixtures

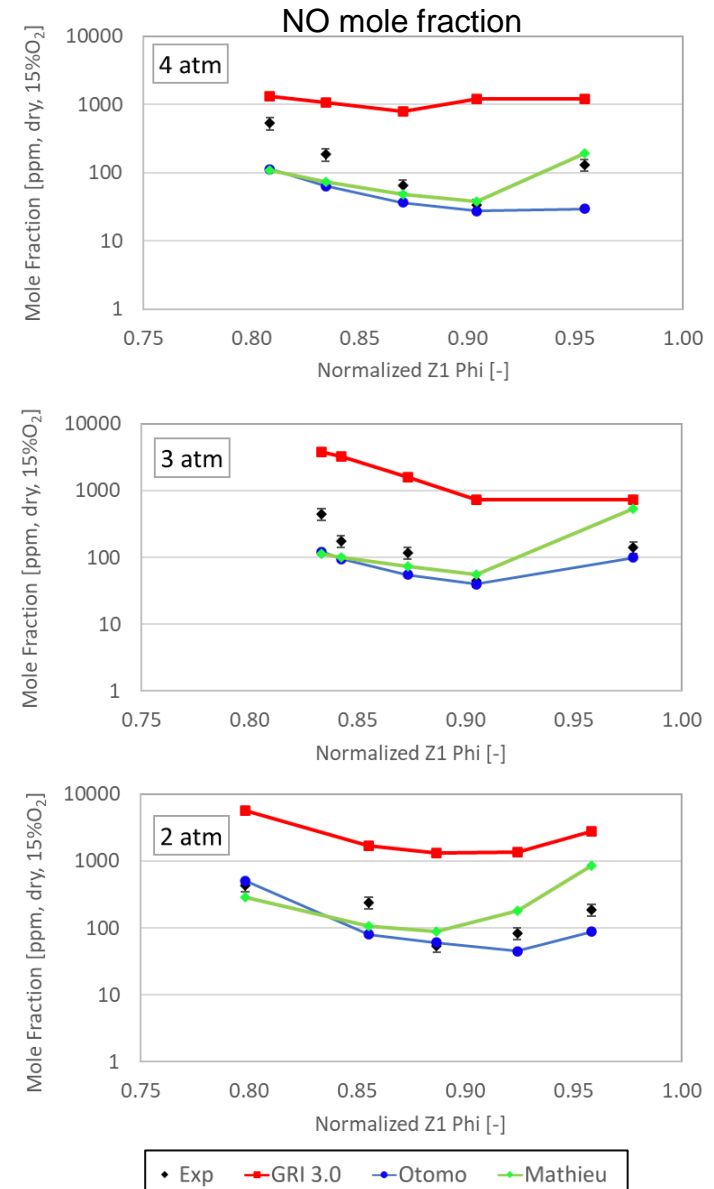
Measured NO<sub>x</sub> emissions from the atmospheric laboratory scale experiment



**High Pressure  
Ammonia  
Combustion Tests at  
UCICL**



- Chemical kinetics calculations validated against experimental measurements.
  - Optimum equivalence ratio shifts to richer conditions with increasing pressure.
  - NOx emissions significantly reduced with increasing pressure conditions:
    - TBN\_4atm = 36ppm
    - TBN\_3atm = 50 ppm
    - TBN\_2atm = 90 ppm
- (Total Bound Nitrogen (TBN): is the sum of NO+NO<sub>2</sub>+N<sub>2</sub>O+NH<sub>3</sub>)

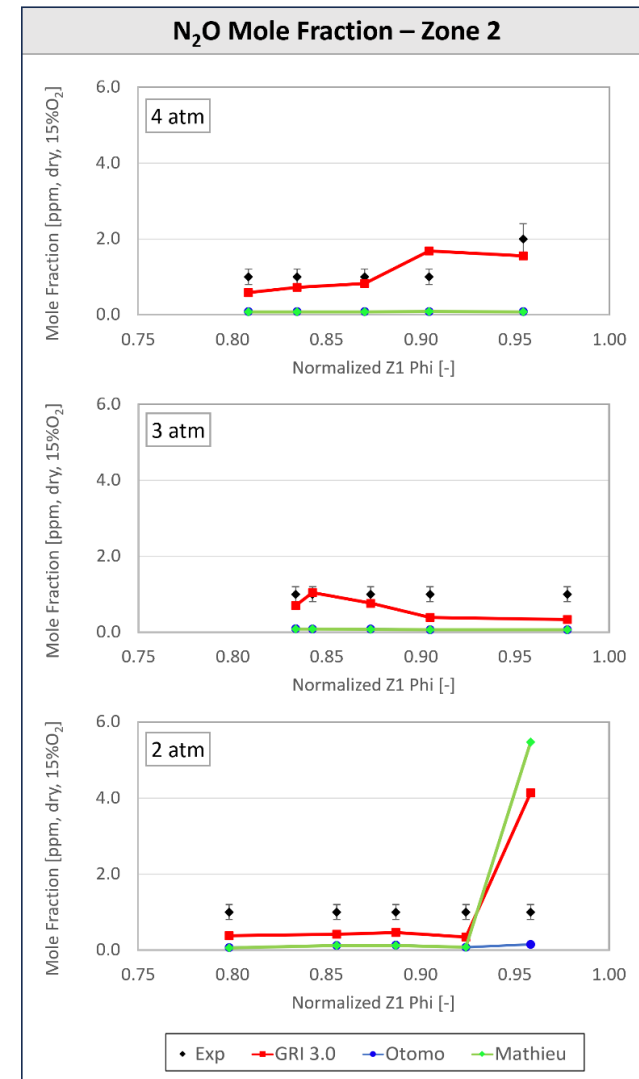
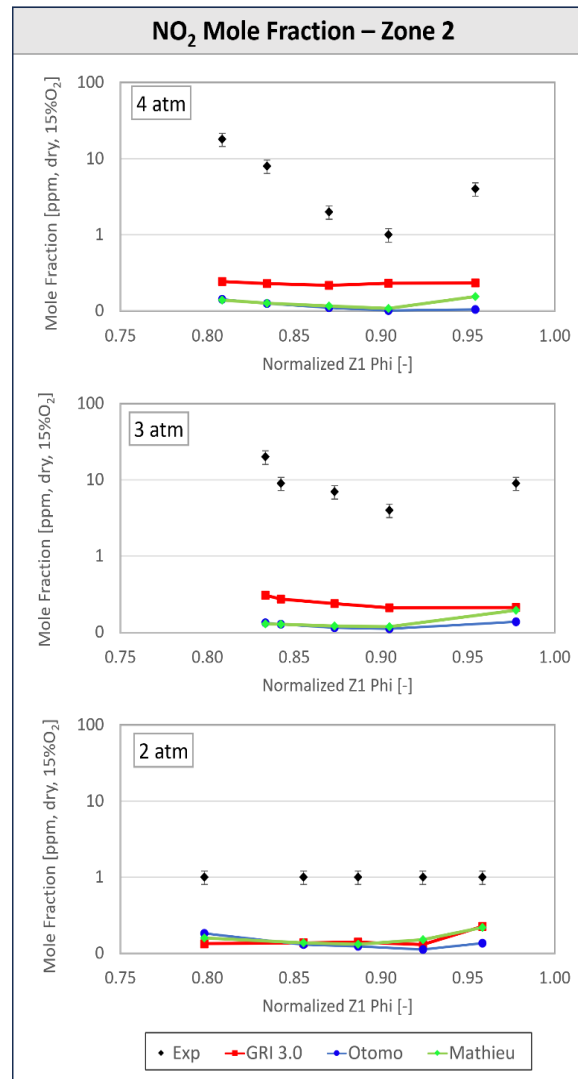


➤ Mole Fraction of NO<sub>2</sub>:

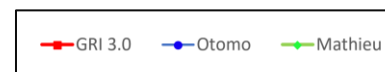
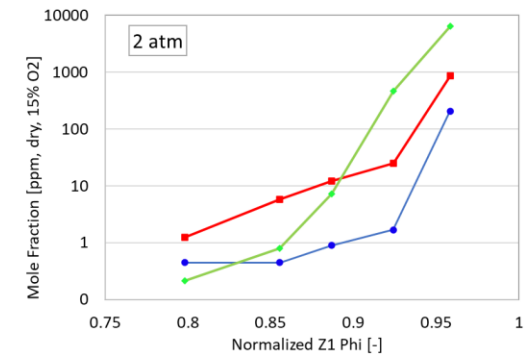
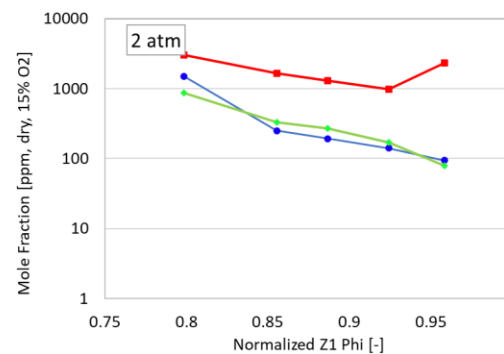
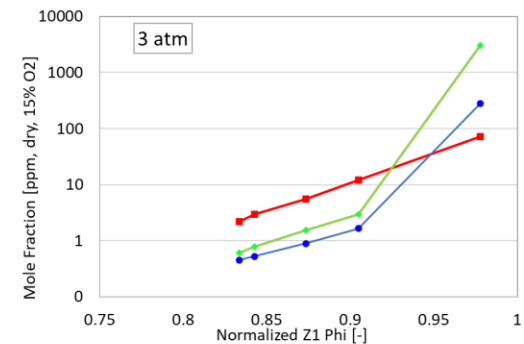
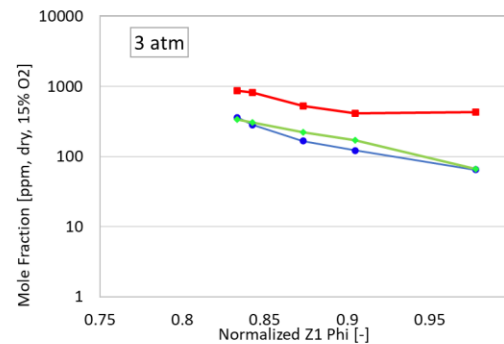
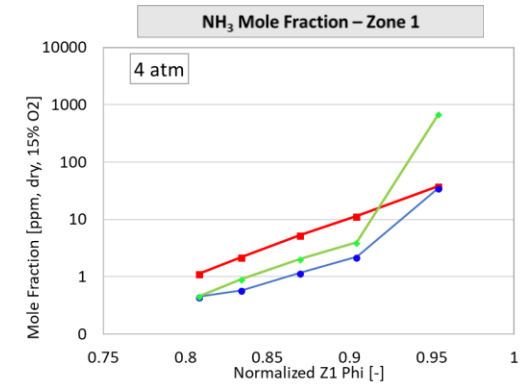
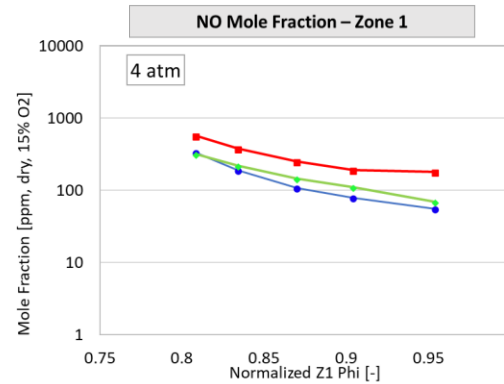
- Experimental data shows that NO<sub>2</sub> follows a similar trend as NO.
- Chemical mechanisms employed underpredicted NO<sub>2</sub> concentrations at the end of the secondary zone.

➤ Mole fraction of N<sub>2</sub>O:

- Experimental data shows that higher pressures has no significant impact on N<sub>2</sub>O concentrations.
- Chemical mechanisms employed slightly underpredicted NO<sub>2</sub> concentrations.



- Mole Fraction of NO:
  - Modeling predictions at the end of Zone 1 show that higher pressure leads to lower NO.
  
- Mole fraction of NH<sub>3</sub>:
  - The NH<sub>3</sub> plots confirm that unburned NH<sub>3</sub> quickly rises at higher equivalence ratios.
  - With an increase in pressure, unburned NH<sub>3</sub> levels decrease.
  
- Other comments:
  - Predictions of species concentrations are generally within the same range across the three chemical mechanisms used. However, under high fuel-rich conditions, the models' predictions become less consistent. The GRI mechanism shows maximum deviations from the other two.

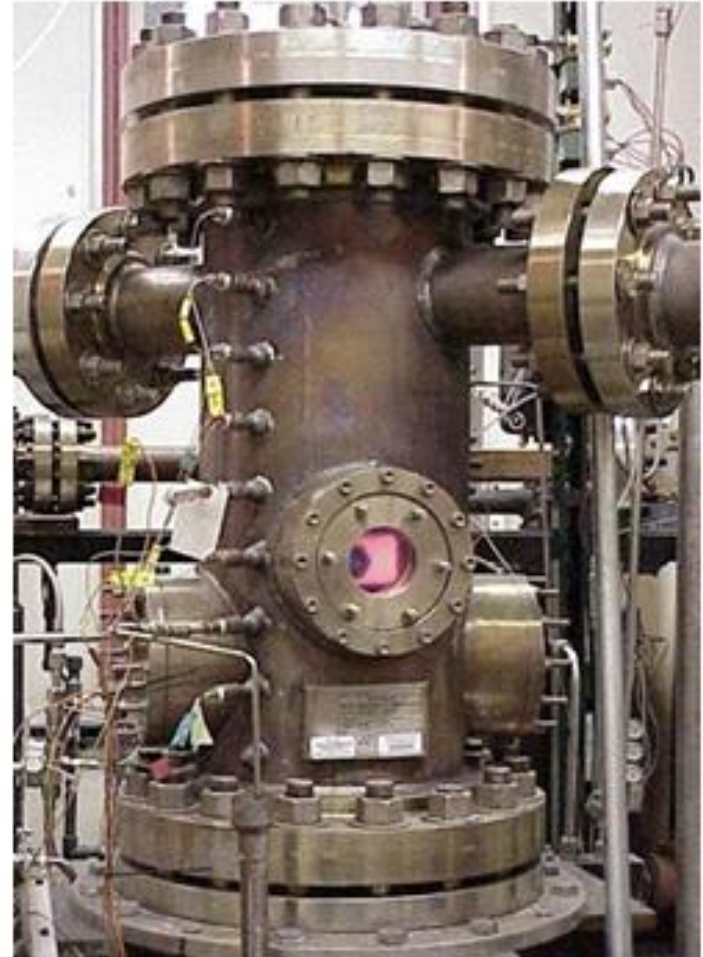


- Modeling results show that minimum NO<sub>x</sub> emission levels rest within a narrow temperature band.
- Experimental results compare well with modelling predictions. Variations could be attributed to the non-ideal rig conditions (Heat Losses) as well as gas analyzer measurement uncertainties.

Proprietary

**Natural Gas  
Validation Testing at  
UCICL**

- To establish a frame of reference, CPS tested the new burner using natural gas as a fuel in the high-pressure combustion facility at UCICL.
- Pressure was varied between 1-4 bars within the rig.
- Combustion air was preheated to 170 C.
- Combustion tests were carried out using natural gas as a fuel.
- Residence time in the reactor was varied to investigate the impact of short residence time on CO and NO<sub>x</sub> emission levels.
- Burner stability was tested under a wide range of relatively low to high combustion temperatures to determine the lean blowoff limit of the new combustion system.



- Results demonstrate very low NO<sub>x</sub> emissions achieved under a wide range of combustion conditions. NO<sub>x</sub> emission levels hovered between 2 - 4 ppm.
- Moreover, the new design achieved very low CO emissions, 4 - 34 ppm, under a wide range of temperatures demonstrating the superiority of the new design over existing ones.
- The lean blowoff limit of the new combustion system is extended drastically relative to state-of-the art commercial combustion systems.
- It is noteworthy to mention that heating the combustion air to temperatures typical for gas turbines (400 °C or higher), in comparison to what was done in this program (170 °C), would lead to higher stability making this technology a big disruptor once it is commercially rolled out.
- Moreover, ignition of the burner for ammonia and natural gas cases was achieved in a premix mode of operation.

Proprietary

- The new combustion system demonstrates very weak correlation between residence time and CO and NO<sub>x</sub> emission levels for the natural gas case across all tested pressures.
- NO<sub>x</sub> emission levels increase from 2 ppm for short residence times to 6 ppm for long residence times.
- CO emissions increase from 4 ppm to 34 ppm when the residence time is reduced to 5 millisecond.
- This demonstrates that the combustion process is completed quickly.
- The experimental results support the conclusion of our modelling studies that the new design complete the combustion process in a very short time.
- These results demonstrate the new combustor is superior to current commercial ones.

Proprietary



The experimental program results also show that our kinetic model can provide accurate predictions of the performance of the new combustion system.

Proprietary

Our kinetic model exhibits very weak functionality between  $\text{NO}_x$  and CO emissions and residence time like what was observed experimentally

Proprietary

Testing the burner using ammonia and natural gas as fuels provided us with the following conclusions:

- Fast combustion achieved in the natural gas case indicating that the new design would achieve similar results for the ammonia case.
- Very low emissions achieved in both cases.
  - Natural Gas       $\text{NO}_x$  2-4 ppm       $\text{CO} < 10$  ppm
  - Ammonia           $\text{NO}_x < 35$ ppm       $\text{NH}_3 < 1$  ppm
- High burner stability demonstrated across both fuels.
- Igniting both fuels in a premix mode of operation were possible without facing any technical obstacles. This is very important for engine startup and engine part load operation.
- Uniform TAT spread; elimination of combustor and 1<sup>st</sup> stage vane over heating problem



- The new combustor is a disruptive technology platform ... not just an incremental change.
- This disruptive technology has the potential to transform the gas turbine industry.
- The new combustor technology can be used in:
  - Different GT combustor platforms; annular, can annular and silo type combustors
  - The technology is scalable to Gas turbine engines of different sizes
- Experimental results demonstrate very high combustion stability achieved over a wide range of combustion conditions rendering the new design superior to current conventional ones.
- Experimental and modelling results demonstrate that CO and NO<sub>x</sub> emissions of the new design can be predicted via modelling.
- The new design has the advantage of increasing the life of the hot gas path components.

# **NH<sub>3</sub> GT Combustor Demonstration**

## **Phase IIB Activities**

## DOE Phase IIB SBIR is awarded to CPS – expected to start in October 2024

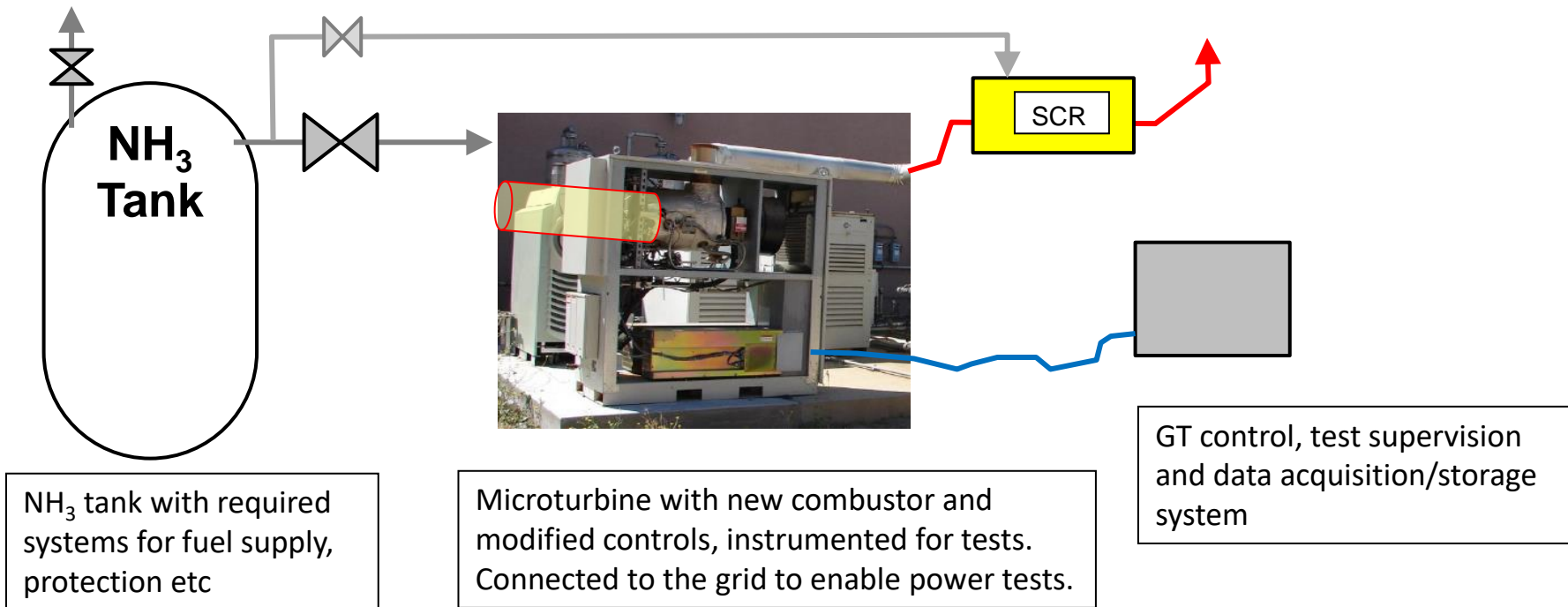
- Partnering organization – UND EERC

	Cost (USD)	Duration	Comments
Feasibility Study (Phase I - DOE SBIR)	\$250,000	9 months	Completed successfully (June 2020)
Pilot-Scale Study (Phase II – DOE SBIR)	\$1,600,000	34 months	Completed Successfully (August 2024)
Engine Demonstration (Phase IIB – DOE SBIR)	\$1,150,000	20 months	Awarded in August 2024

## Proposed Tasks & Activities for Phase IIB

- Finalize NH<sub>3</sub> combustor detailed mechanical design
- Fabricate combustor parts and retrofitting kit
- Commission GT engine with NH<sub>3</sub> combustor
- Run Performance tests from ignition to baseload conditions
- Utilize existing Selective Catalytic Reactor to further reduce engine emissions (if needed)

- The tests to be run on a demonstrator set up, the equipment is arranged for ease of access.
- We intend to focus in a first test phase on the GT without Selective Catalytic Reduction System (SCR). The results will inform the requirements and the design of the SCR, which can be added for a second test phase, if needed.
- The commercial package will include commercial ammonia validated components in a compact Form.



- The combustor will be operated in a **fully premix mode of operation** from startup to full load operation.
- Emission data will be collected throughout the whole load range.
- The designated tests will determine all limitations of the new technology, if any, across the engine operating conditions.

Proprietary



# Summary

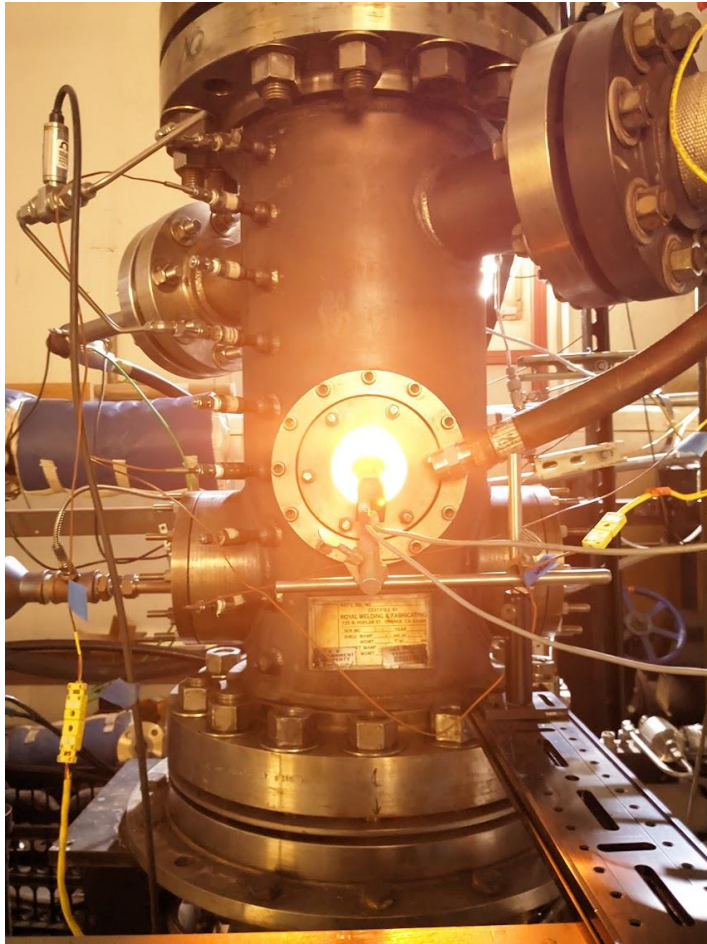
- Burner technology that allows for quick mixing of ammonia/air flows and that introduces the reactants at velocities that enable stable flames could also achieve low NO<sub>x</sub> emissions when operating conditions are optimized.
- NO<sub>x</sub> emission levels from the tests show that they approach very closely what has been achieved in the kinetic modeling studies
  - High pressures have very positive effect on reducing NO<sub>x</sub> emission levels in ammonia combustion systems
  - High temperatures as well accelerate the preferential conversion of ammonia to N<sub>2</sub> under fuel rich conditions
- The results show that tested ammonia combustion system is able achieve very high flame stability across a wide range of air to fuel ratios ( $0.7 < \Phi < 1.45$ ) as well as very low NO<sub>x</sub> and ammonia emissions.
  - The lowest NO<sub>x</sub> of 36 ppmv, corrected for 15% O<sub>2</sub> and dry basis, was recorded at 4 atm.
- Several challenges need to be overcome when using ammonia as a fuel in gas turbine applications; these include the following:
  - Reliable startup of the engine
  - Running up the engine while achieving low NO<sub>x</sub> and NH<sub>3</sub> emission levels (prevention of the brown plume phenomenon)
  - Reliability of cycling the engine between full and part load operation
  - Proper cooling management of the combustor liners especially under high load conditions

- Numerical simulation studies to explore options for further reduction of NOx emissions (< 20 ppm target)
  
- Operating regime of the combustor is defined:
  - Finalize mechanical design & build combustor prototype
  - Retrofit a microturbine package with the ammonia combustion module
  - Commission engine and conduct in-field engine demonstration tests from ignition to baseload

This material is based upon work supported by the U.S. Department of Energy, Office of Science, Office of Fossil Energy program under Award Number DE-SC-0020903.

Our appreciation is to Richard Dalton, our program manager, for his strong support and encouragement throughout the project.

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**Thank you!**



# Appendix