



LOAD-Z

Low-NOx, Operable Ammonia Combustor Development for Zero-Carbon Power



FT4000® Aeroderivative Dual Fuel Gas Turbine Engine.

RTX Technology Research Center

DOE/NETL University Turbine Systems Research (UTSR) Meeting
September 25, 2024

Prime Contractor: RTX Technology Research Center (RTRC)
Subcontractor: University of Connecticut (UConn)

RTRC
RTX Technology
Research Center

UCONN
UNIVERSITY OF CONNECTICUT

This material is based upon work supported by the Department of Energy under Award Number DE-FE0032169

Disclaimer: This presentation was prepared as an account of work sponsored by an agency of the United States Government. Neither the United States Government nor any agency thereof, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof.



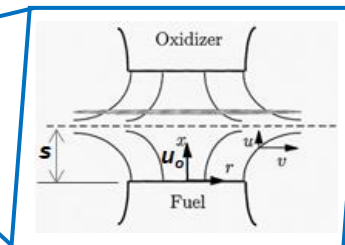
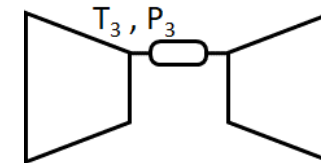
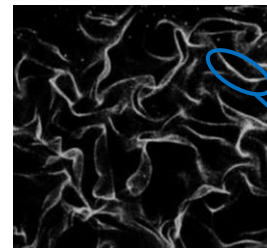
Key Project Goals WHAT / WHY

Low-NOx Operable Ammonia-Combustor Development (LOAD-Z)

(1)
EXPERIMENTS
4 lab-scale
facilities

– Fundamental NH₃ flame data relevant to turbines:

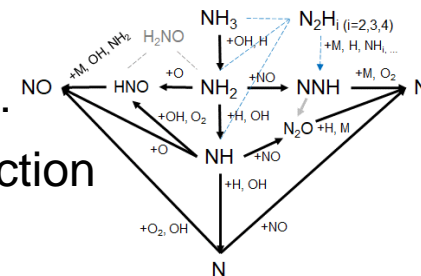
- P, T >> ambient → relevant to compressor exit conditions
- strained & turbulent flames
- Targeted outcome: expand published data w/ new, useful data (previously unreported)



(2)
MODELING

– Predictive capability for NH₃ combustion & emissions

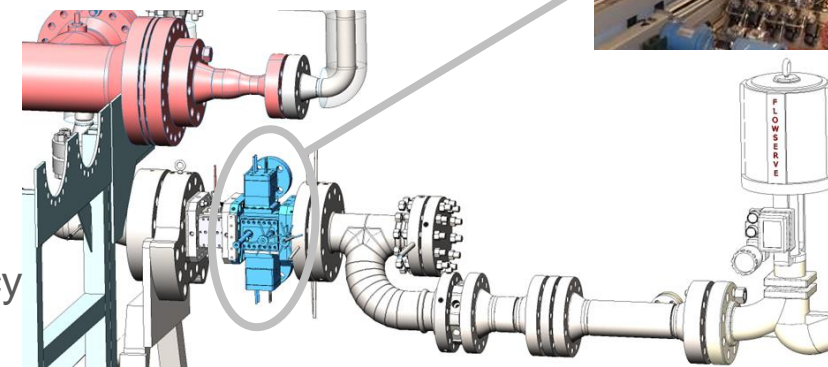
- NO_x formation kinetics integral w/ NH₃ comb. kinetics
- CFD of turb. NH₃ flames w/ NO_x & NH₃ slip (η_{COMB}) prediction
- Targeted outcome: capability for GT combustor design



(3)
DESIGN & DEMO.

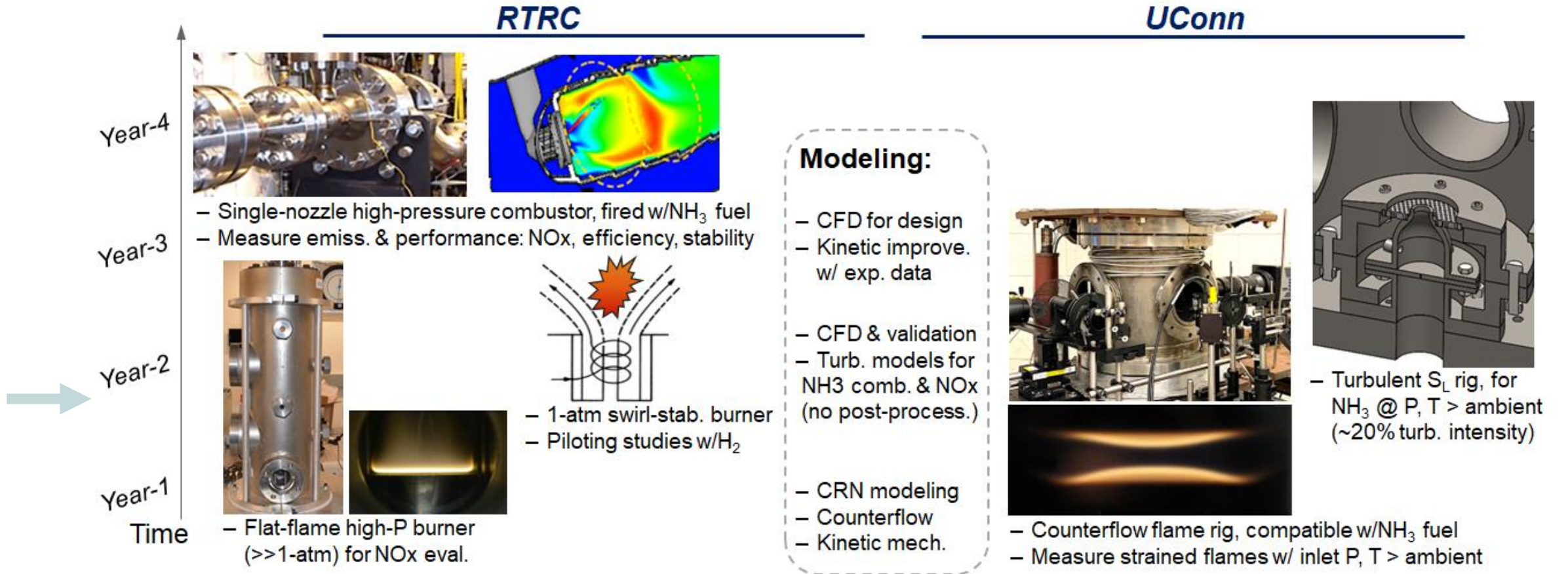
– Develop & test NH₃ gas-turbine combustor “@ scale”

- Single-nozzle-rig (SNR) scale demo. @ high P, T
- Pure NH₃ combustion @ 75% – 100% power
- Targeted outcome: < 30ppm NO_x** & >99.99% efficiency



**Note recent ETN recommendations for NO_x reporting with hydrogen-containing fuels

Approach & Work How



• 4 Lab Experiments -&- 1 Combustor Test:

– Ongoing: 2 laminar / fundamental rigs
– Start Q4 & Q1: 2 turbulent / applied rigs → complex fluid mechanics

• 3 “Kinetics” Models -&- 1 CFD Model:

– Kinetics validation: Counterflow-flame & Flat-flame
– Combustor design: Chem. Reactor Network & CFD w/species transport

Fundamental Counterflow Data UCONN EXPERIMENTS

Low-NO_x Operable Ammonia-Combustor Development (LOAD-Z)

(1)

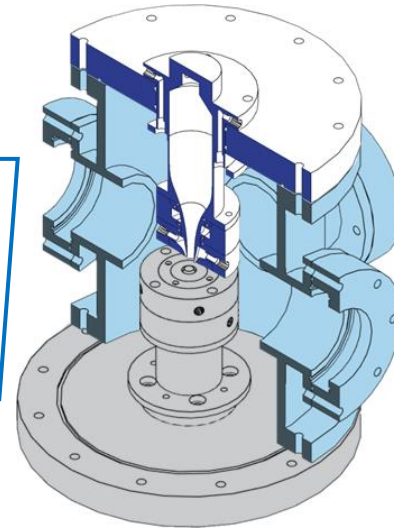
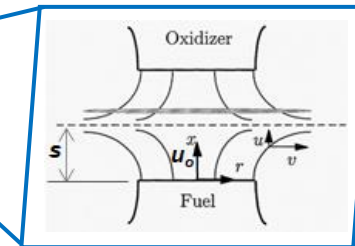
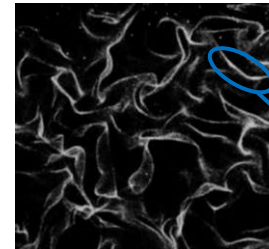
UConn
Experiments



– Fundamental NH₃ flame data relevant to turbines:

- P, T >> ambient → relevant to compressor exit conditions
- strained & turbulent flames

- Targeted outcome: expand published data w/ new, useful data (previously unreported)



- Predictive capability for NH₃ combustion & emissions
 - NO_x formation kinetics integral w/ NH₃ comb. kinetics
 - CFD of turb. NH₃ flames w/ NO_x & NH₃ slip (η_{COMB}) prediction

- Targeted outcome: capability for GT combustor design

– Develop & test NH₃ gas-turbine combustor “@ scale”

- Single-nozzle-rig (SNR) scale demo. @ high P, T
- Pure NH₃ combustion @ 75% – 100% power

- Targeted outcome: < 30ppm NO_x** & >99.99% efficiency

RTRC

RTX Technology
Research Center

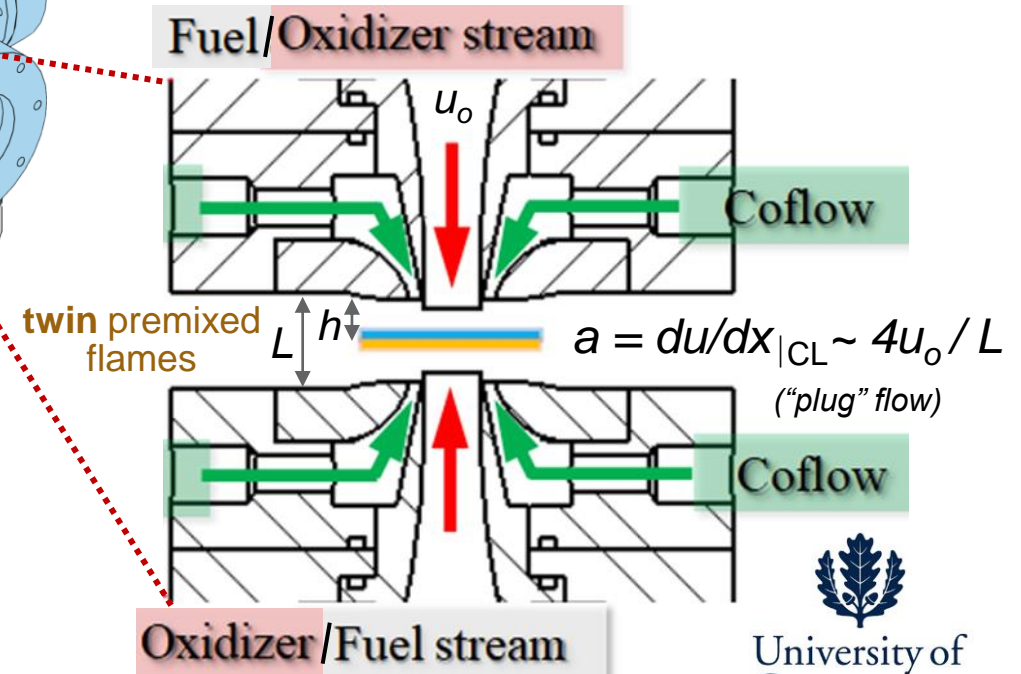
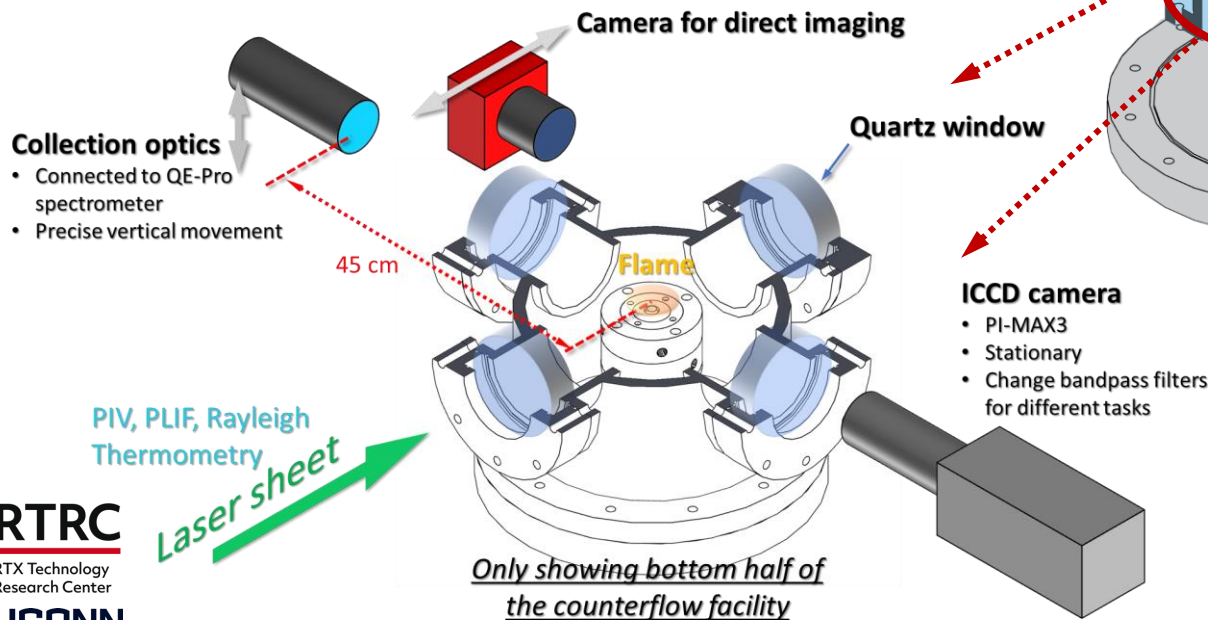
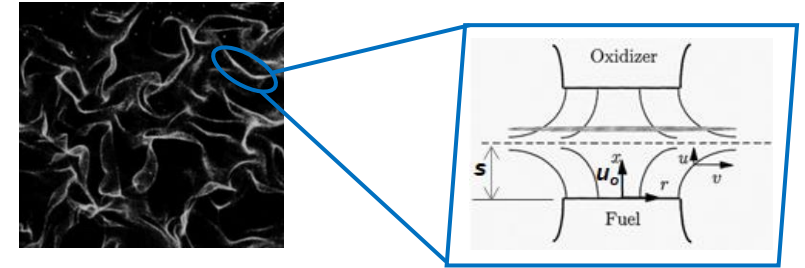
UConn
UNIVERSITY OF CONNECTICUT

Lab-Scale Experiment: Counterflow Flame Rig | *Laminar (2D)*

- Relevance:**
- Scarce data on NH_3 flame extinction, esp. @ $P, T > \text{ambient}$.
 - Stringent test of kinetic mechanisms, for comb. model development
 - Canonical representation of turbulent “flamelet”

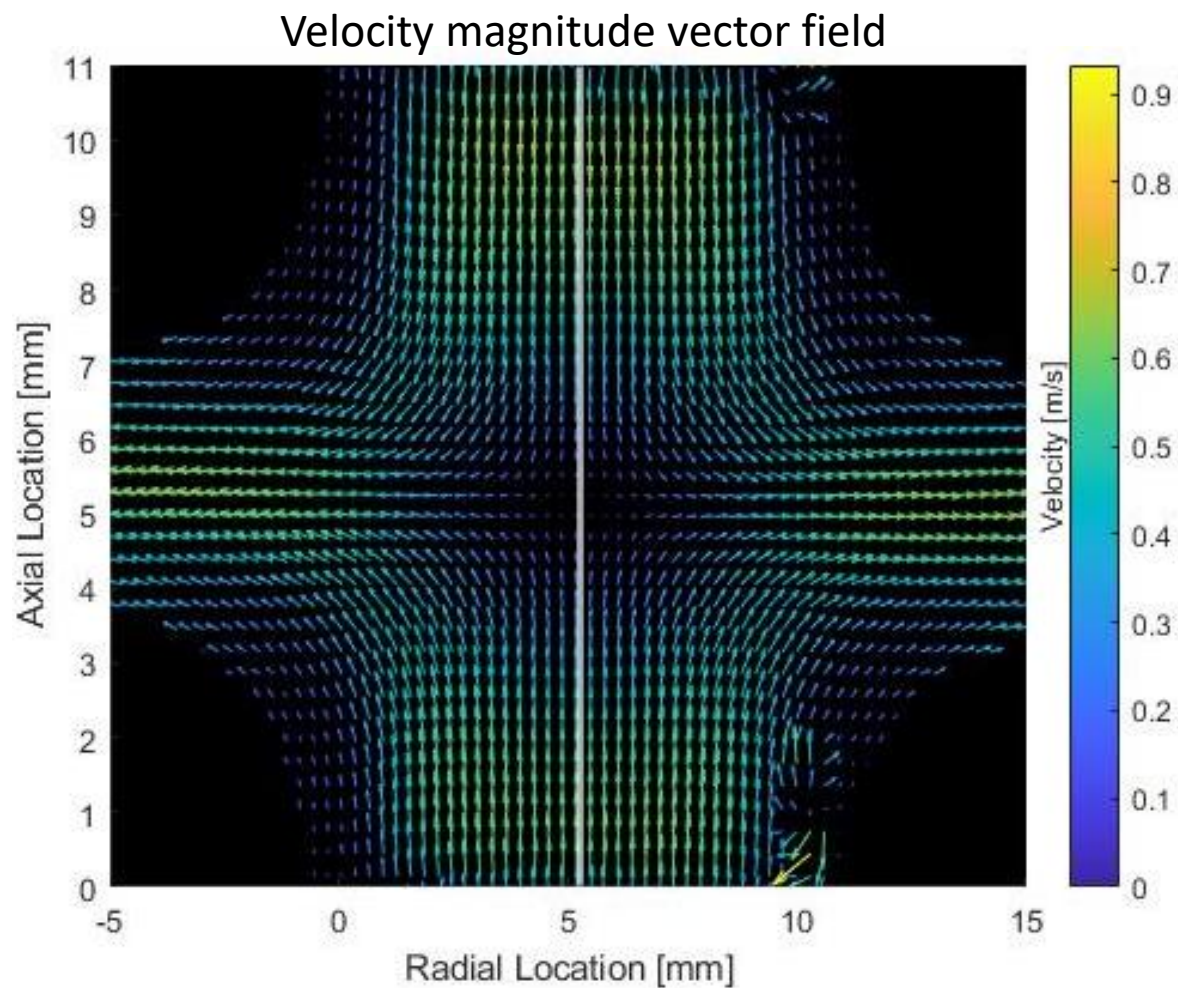
UConn configuration & capability:

- >7-atm pressure vessel & feeds
- up to 500 K preheat capability

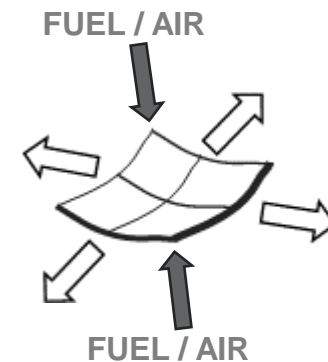
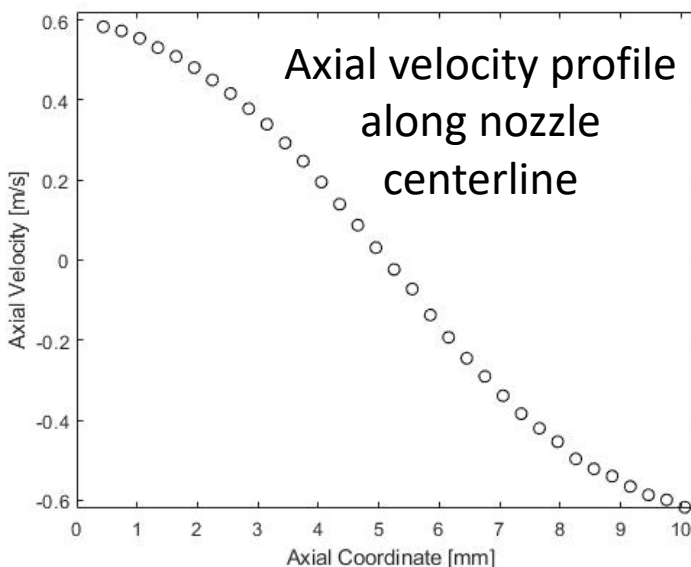
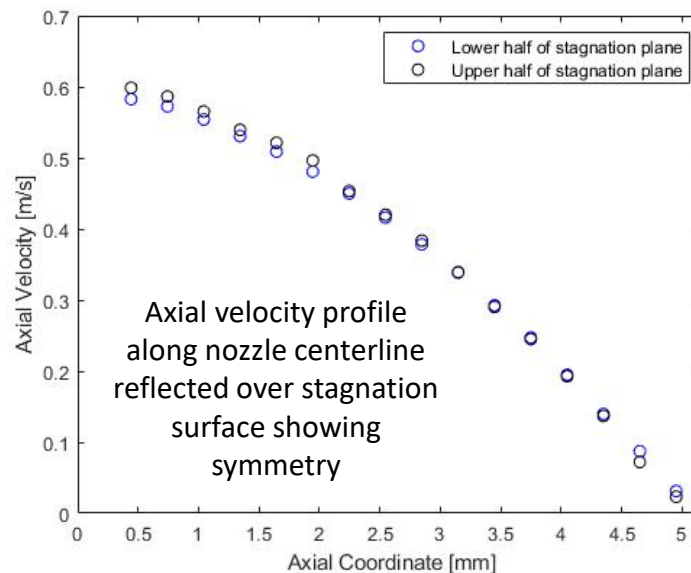


University of Connecticut

Counterflow Experiments – Measure Flow Uniformity & Strain



Air at 5 SLPM flowrate + N₂ shroud ($a \sim 200 \text{ s}^{-1}$)
 1 atm, 295 K
 L = 10.4mm; D = 10mm

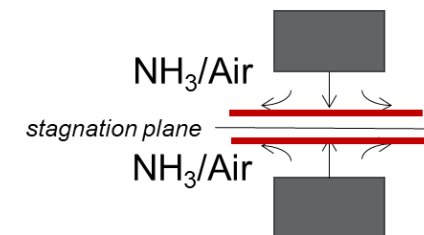


Flame stretch:

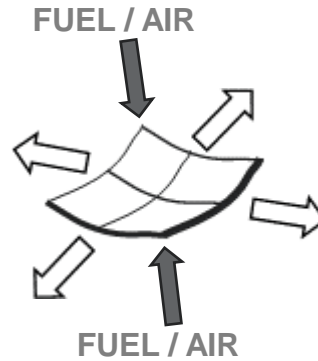
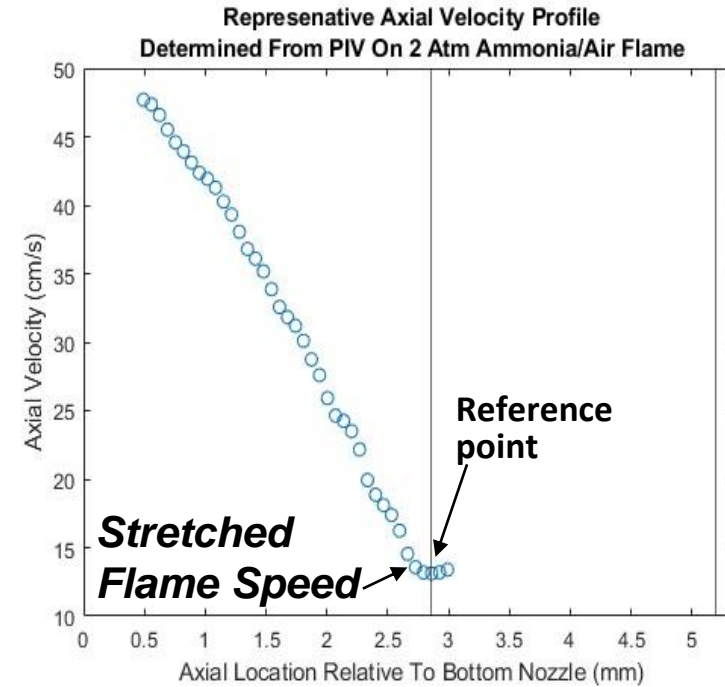
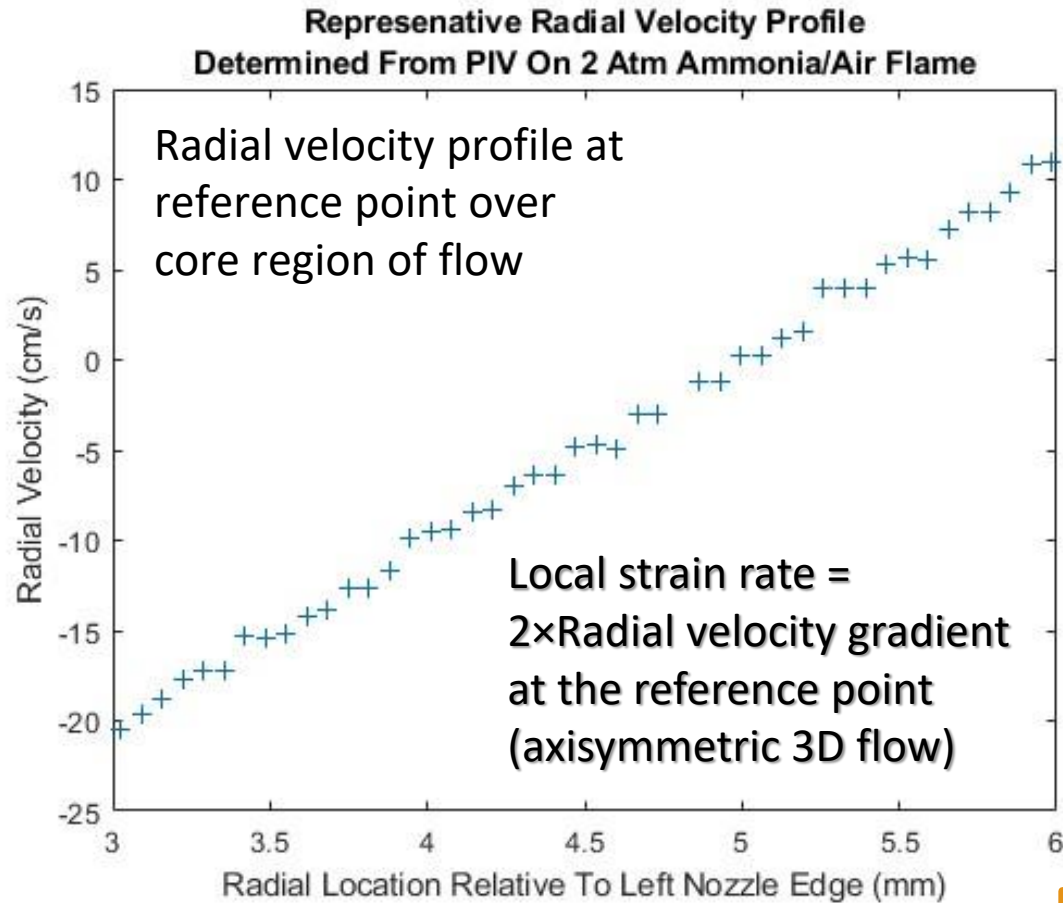
$$a_{STRETCH} = \frac{1}{A} \frac{dA}{dt}$$

Define:
 Global / Centerline strain rate (for “plug” flow):

$$a_{GLOBAL} \sim \frac{4U_{JET}}{L}$$



Counterflow Exp. – Global vs. Local Strain Rate in NH₃ flames

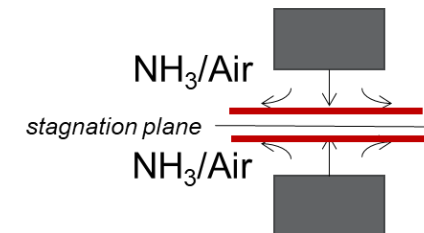


Flame stretch:

$$a_{STRETCH} = \frac{1}{A} \frac{dA}{dt}$$

Define:
Global / Centerline strain rate (for “plug” flow):

$$a_{GLOBAL} \sim \frac{4U_{JET}}{L}$$



Local Extinction Strain Rate = 229 1/s
Global Extinction Strain Rate = 212 1/s
7% difference

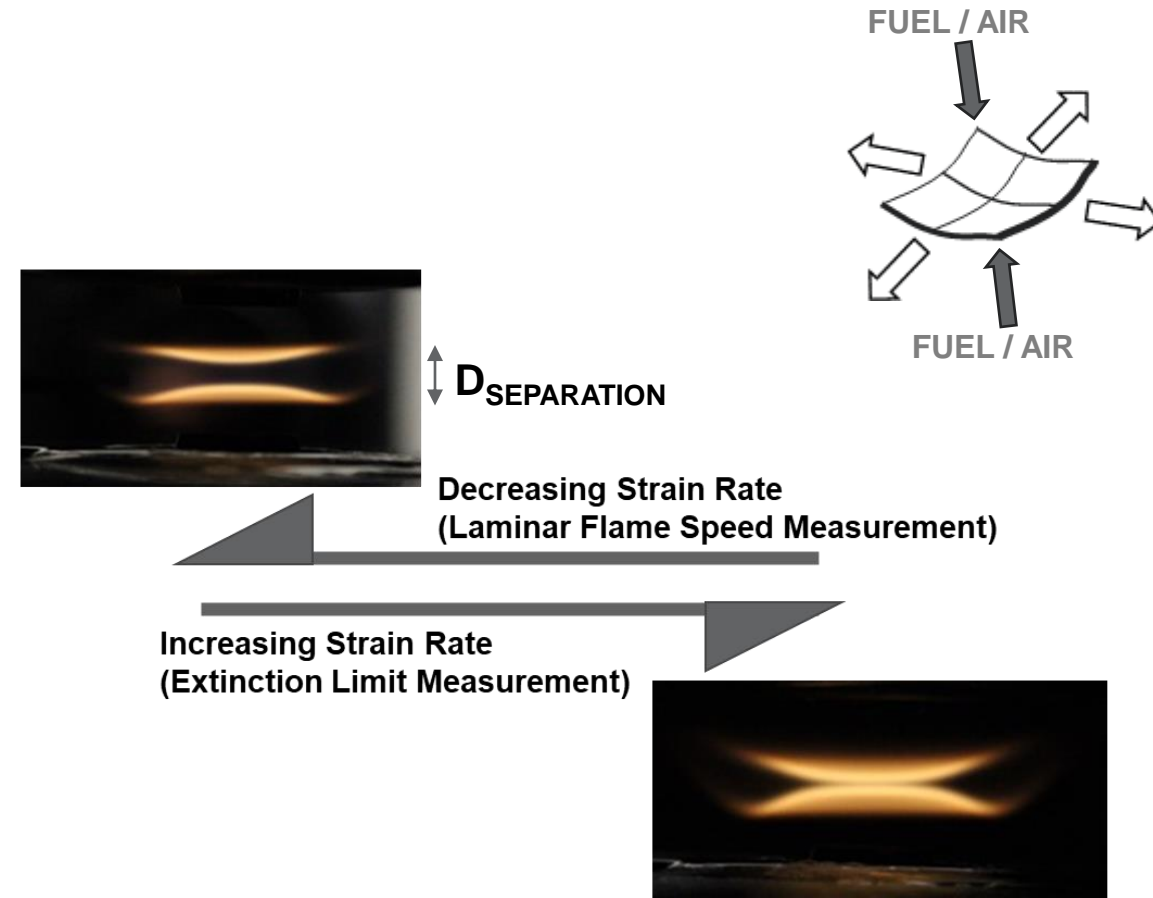
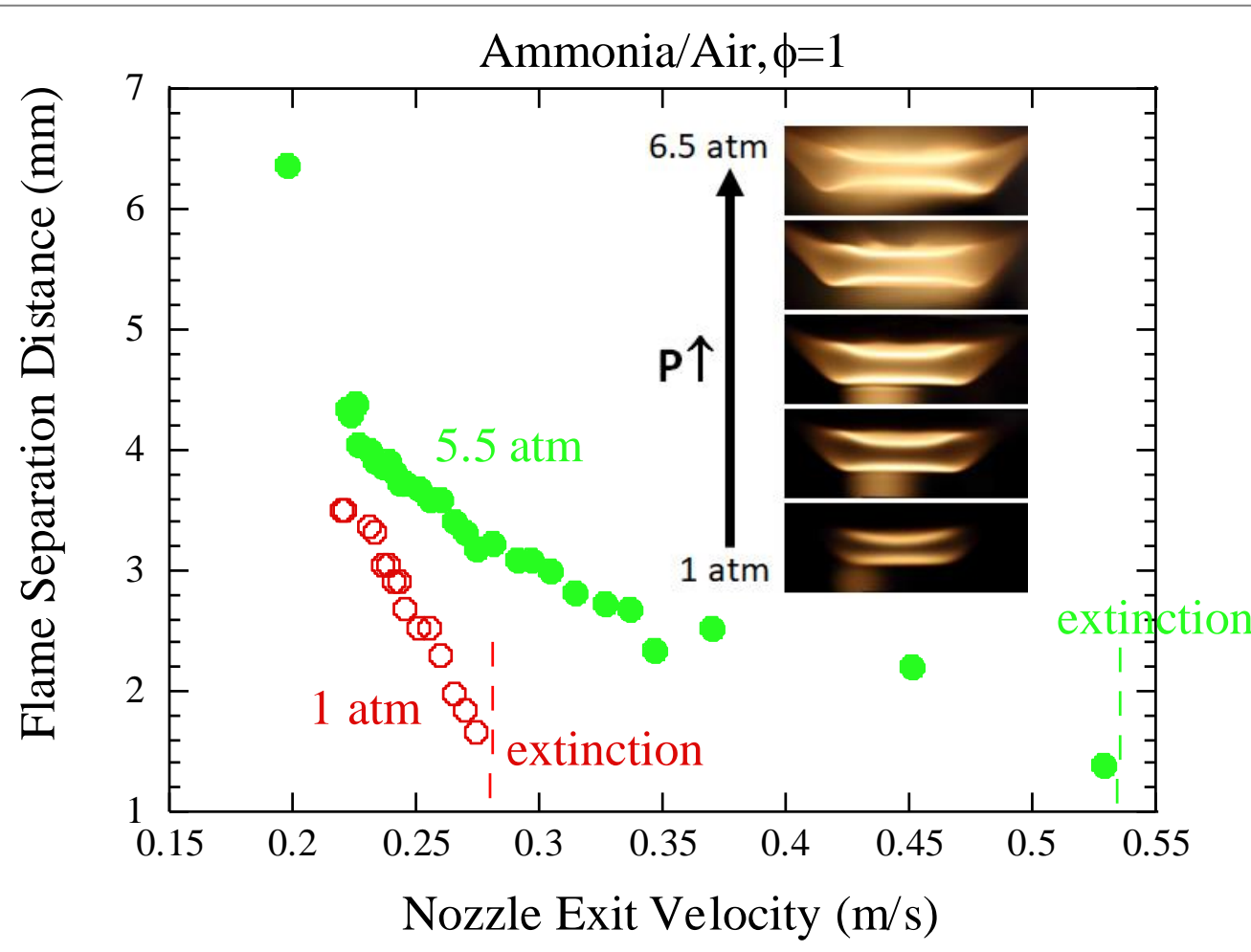
Conditions

Pressure: 2 atm

Unburned Mixture Temperature: 25 °C

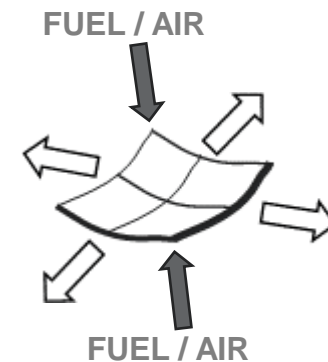
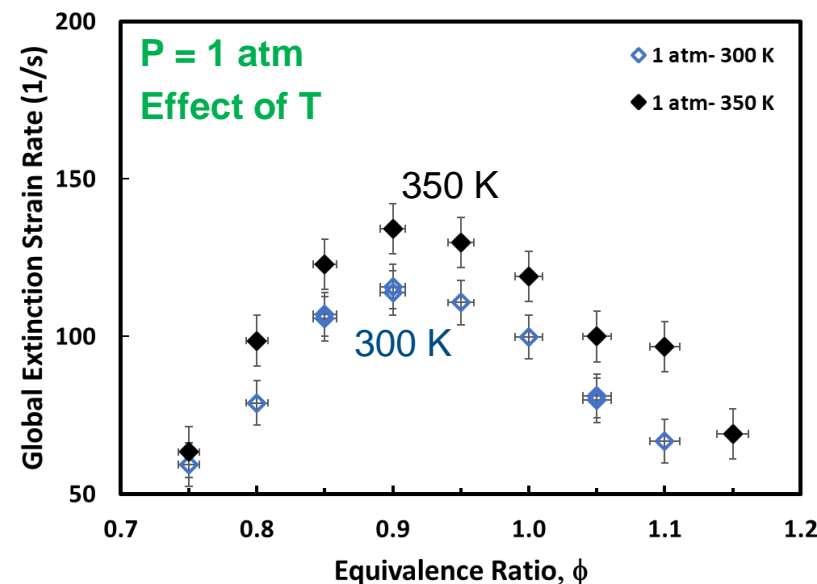
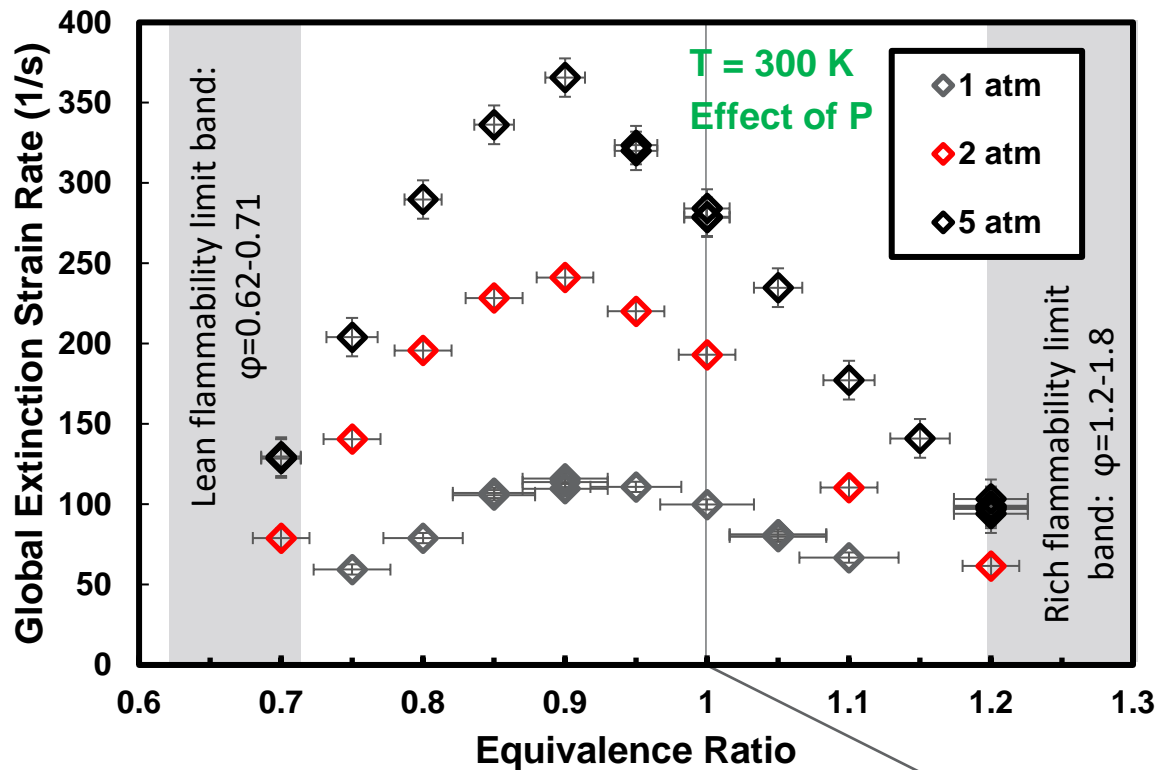
Equivalence Ratio: 1.0 (Ammonia/Air) → Quality PIV data in NH₃ flame

Counterflow Experiments – Procedure for Measuring Extinction



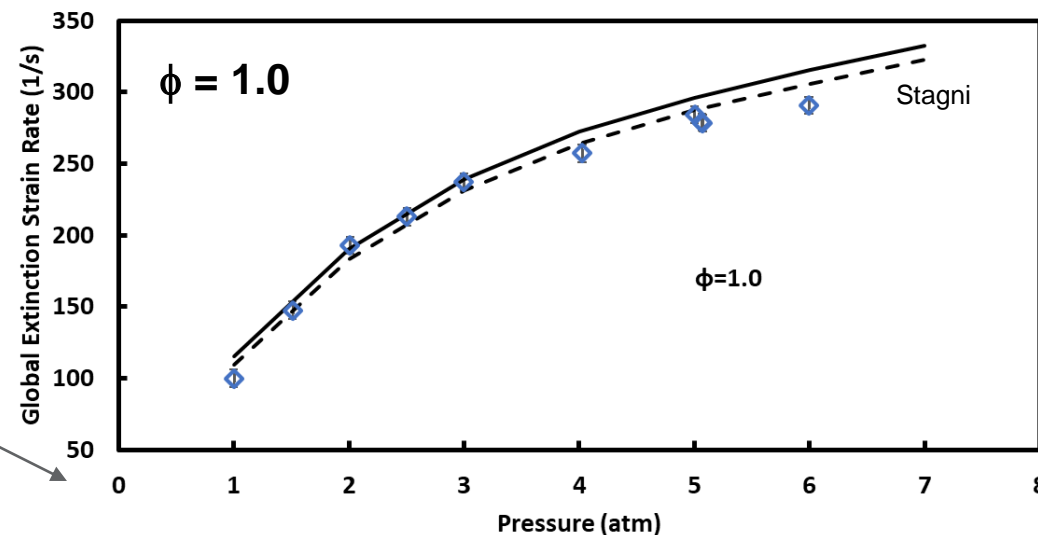
- Sequence:**
- Establish stable, premixed NH_3 / air flames @ initial $D_{SEPARATION}$ twin flames fixed in space
 - At fixed P, ϕ : uniformly increase U_{JET} & observe $D_{SEPARATION} \downarrow$
 - Quasi-steady approach to U_{EXT} at extinction $\rightarrow \frac{4U_{EXT}}{L} = a_{EXT_GLOBAL}$

Counterflow Experiments – Extinction Strain Rate vs. ϕ , p , T



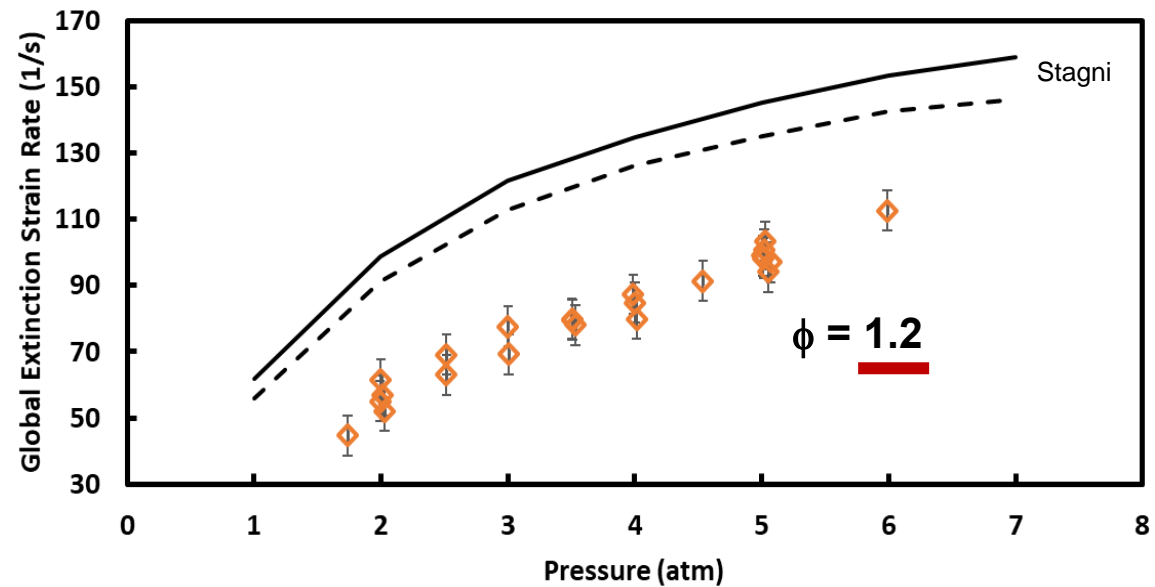
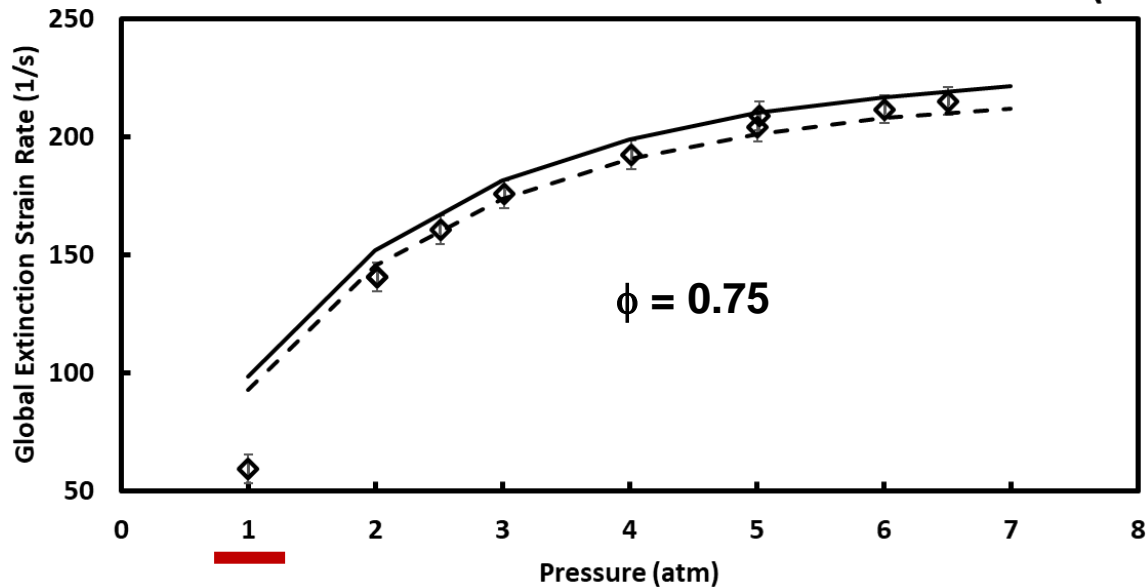
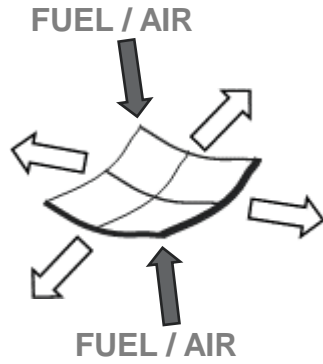
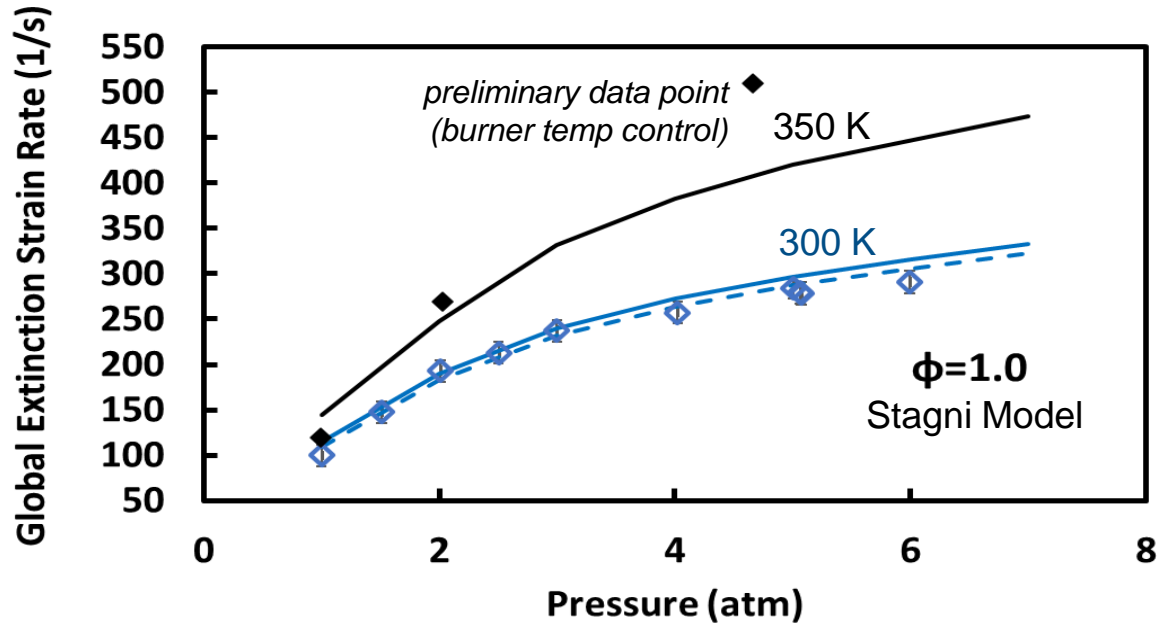
Accuracy / Error Assessment:

- Flowmeter precision incl. accuracy & calibration
- (Many) representative data points repeated to establish variability / repeatability



Roll-off in a_{EXT} with pressure (non-linear)

Counterflow Experiments – Press/Temp Effect on Extinction (3 ϕ 's)



UConn Next Steps – ... Turbulent Flame Speed Rig for NH₃

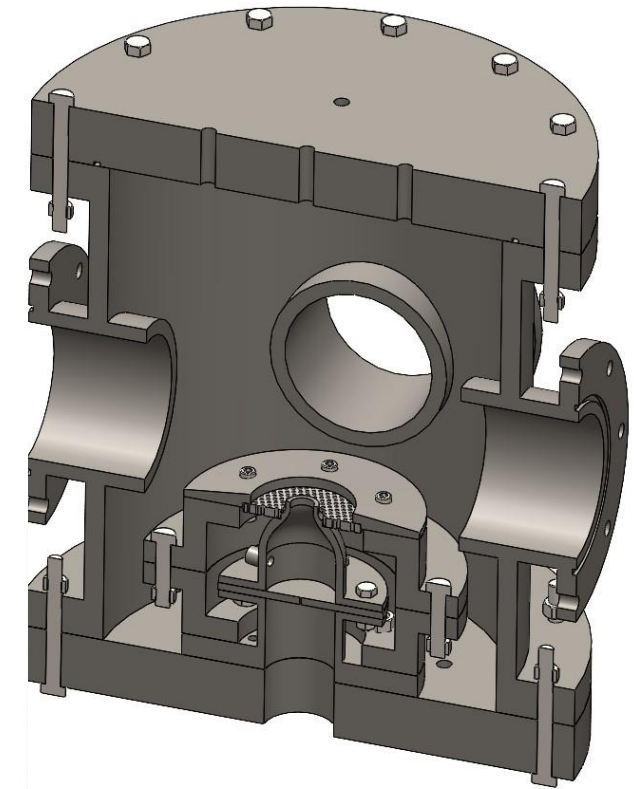
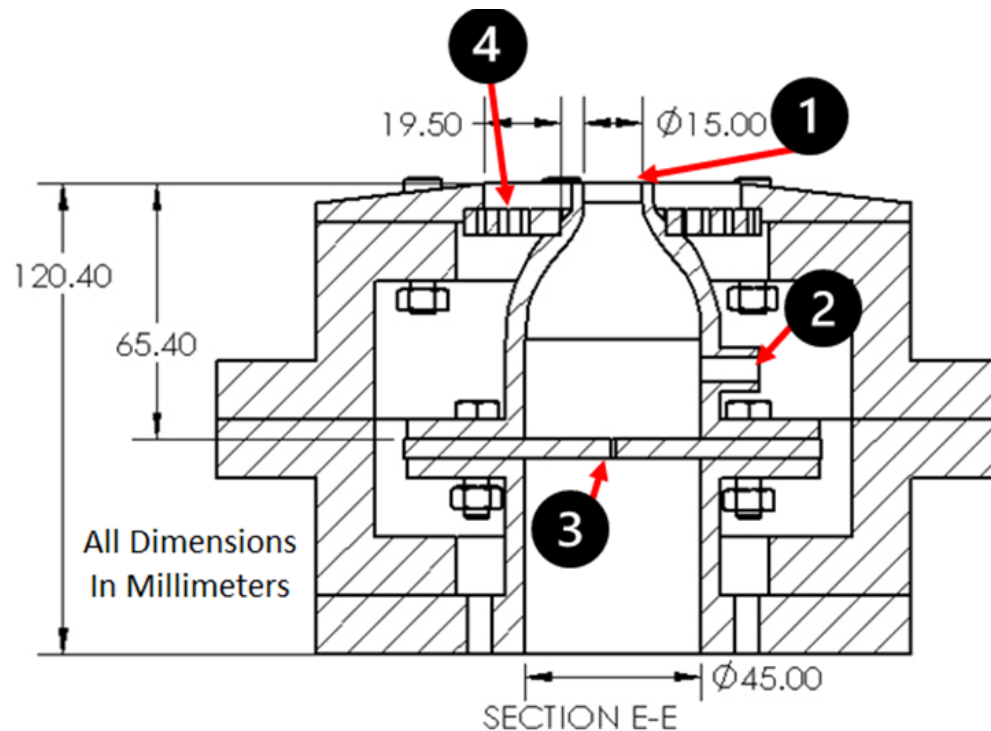
Q4- Fabricate **Turb. Flame Speed Rig**:

Turbulent intensity range: 15–25%

1. NH₃ Bunsen Burner Outlet
2. Jet In Crossflow Port
3. Sharp-Edged Orifice Plate
4. H₂ Pilot Burner Plate

- NH PLIF for turbulent flame structure imaging
- High-speed PIV for turbulent flow-velocity characterization
- Turbulent intensity enhancement utilizing jet-in-crossflow & contraction section [e.g. Michigan*/Lund** Hi-Pilot/DRZ]

*J.Driscoll, Univ. of Mich.; **M.Alden, Lund Univ.

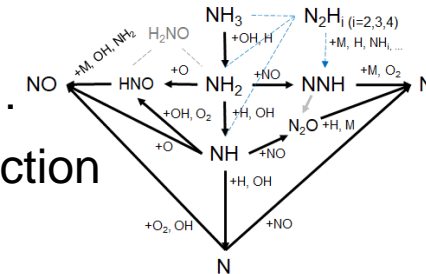


Modeling NH₃ Kinetics COUNTERFLOW & CHEM. REACTOR NETWORKS

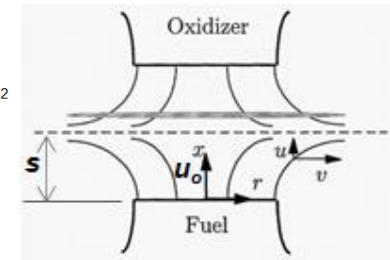
Low-NO_x Operable Ammonia-Combustor Development (LOAD-Z)

- Fundamental NH₃ flame data relevant to turbines:
 - P, T >> ambient → relevant to compressor exit conditions
 - strained & turbulent flames
 - Targeted outcome: expand published data w/ new, useful data (previously unreported)

- Predictive capability for NH₃ combustion & emissions
 - NO_x formation kinetics integral w/ NH₃ comb. kinetics
 - CFD of turb. NH₃ flames w/ NO_x & NH₃ slip (η_{COMB}) prediction
 - Targeted outcome: capability for GT combustor design



FOCUS HERE:



- Develop & test NH₃ gas-turbine combustor “@ scale”
 - Single-nozzle-rig (SNR) scale demo. @ high P, T
 - Pure NH₃ combustion @ 75% – 100% power
 - Targeted outcome: < 30ppm NO_x** & >99.99% efficiency

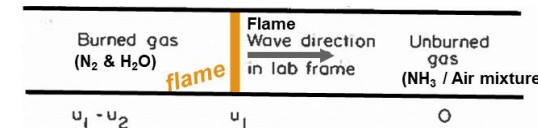
(2)
MODELING

Computational Methods w/ Detailed Kinetics

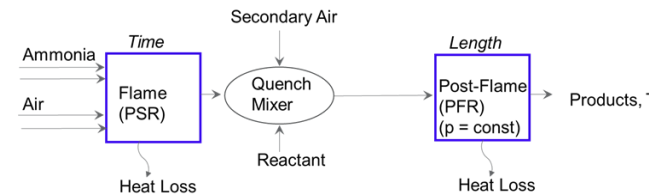


- Cantera, open-source computational framework developed by Dave Goodwin at Caltech
- Models developed for flame speed, chemical reactor networks (CRN), and counterflow flames (premixed & non-premixed)
- Additional tools developed to perform sensitivity analysis, including feature sensitivity (e.g. extinction strain rate), reaction path, chemical mechanism reduction and other diagnostic tools

(i) Freely Propagating Premixed Flames (Flame Speed)

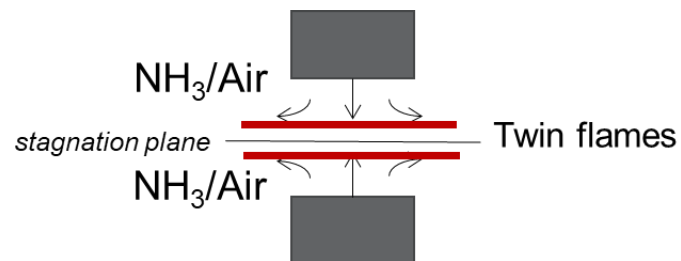


(ii) NH₃ Chemical Reactor Network (CRN) Models

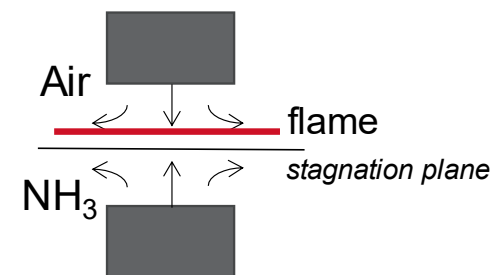


(iii) NH₃ Counterflow Flames: Premixed and Non-Premixed

Premixed Counterflow Flames



Non-Premixed Counterflow Flames



FOCUS HERE

Chemical Kinetic Mechanisms

Selected published, comprehensive N/H chemical mechanisms

- Open-source computational framework developed by Dave Goodwin at Caltech  Cantera

- **Glarborg et al. Mechanism (2018 & 2022 versions)**

[Glarborg, Miller, Ruscic, Klippenstein: Modeling nitrogen chemistry in combustion, Prog. Energy Combust. Sci. (2018) 31-68]

[Glarborg: The $\text{NH}_3/\text{NO}_2/\text{O}_2$ system: Constraining key steps in ammonia ignition and N_2O formation, Combust. Flame, Vol. 257 (2023)]

- **Stagni et al. Mechanism (2020)**

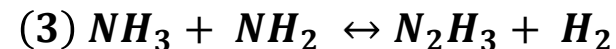
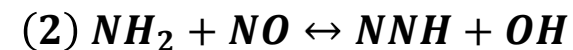
[Stagni, Cavallotti, Arunthanayothin, Song, Herbinet, Battin-Leclerc, Faravelli: React. Chem. Eng. 5 (2020) 696–711]

- **Powell & Papas et al. Mechanism- (2010 & 2011 versions) → RTRC**

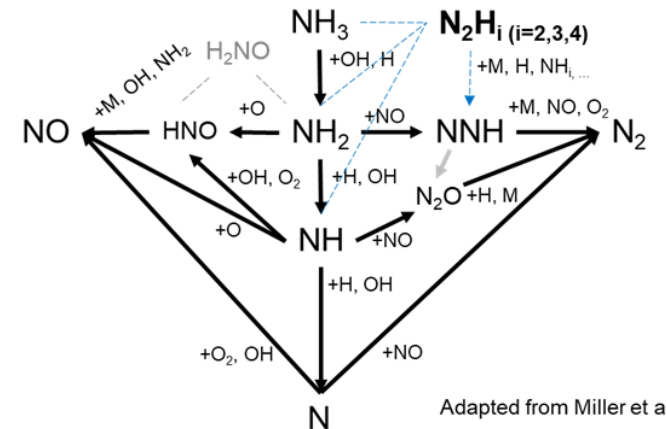
[Powell, Papas, Dreyer: Hydrogen- and $\text{C}_1\text{-C}_3$ Hydrocarbon-Nitrous Oxide Kinetics in Freely, Propagating and Burner Stabilized Flames, Shock Tubes, and Flow Reactors, Combust. Sci. Tech. 182 (2010) 252-283]

[Powell, Papas, Dreyer: Flame Structure measurements of NO in Premixed Hydrogen-Nitrous Oxide Flames, Proc. Combust. Inst. 33 (2011) 1053-1062]

- Two “Powell” mechanisms differ by only 3 different rate expressions for amine radical reactions:

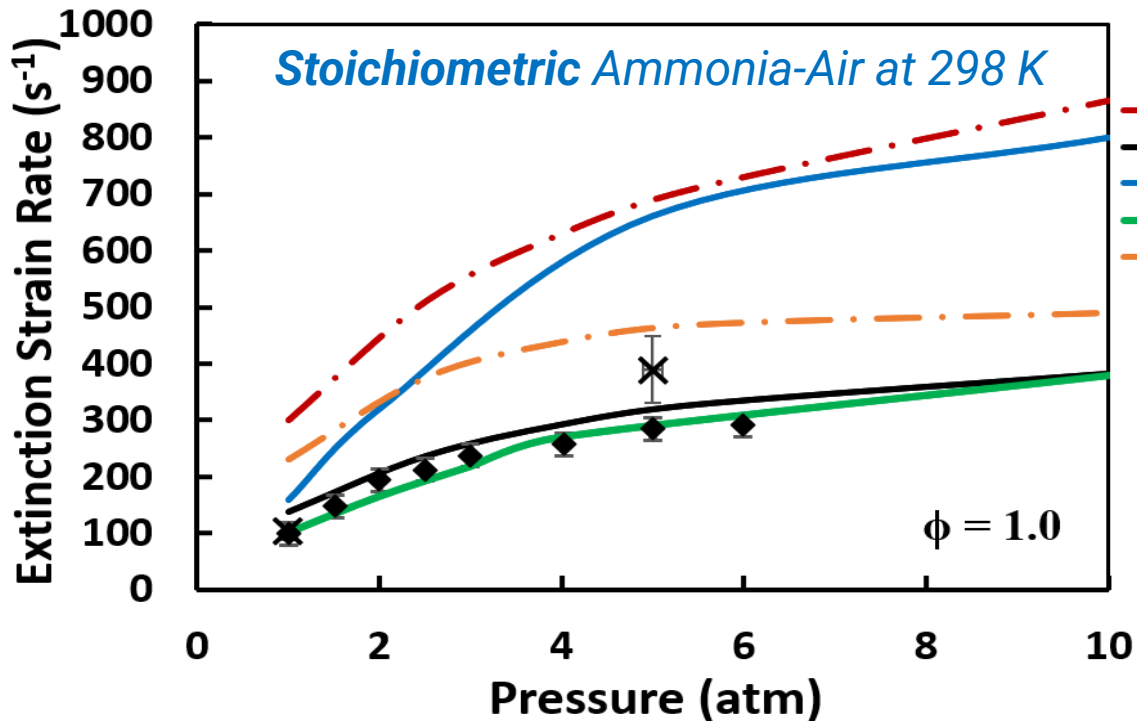
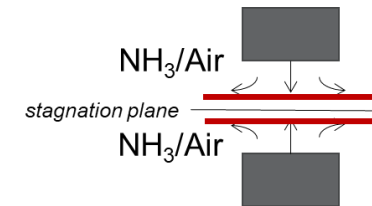


Ammonia Oxidation Pathway Schematic



Adapted from Miller et al. (1983)

RTRC Predictions vs. UConn Measurements



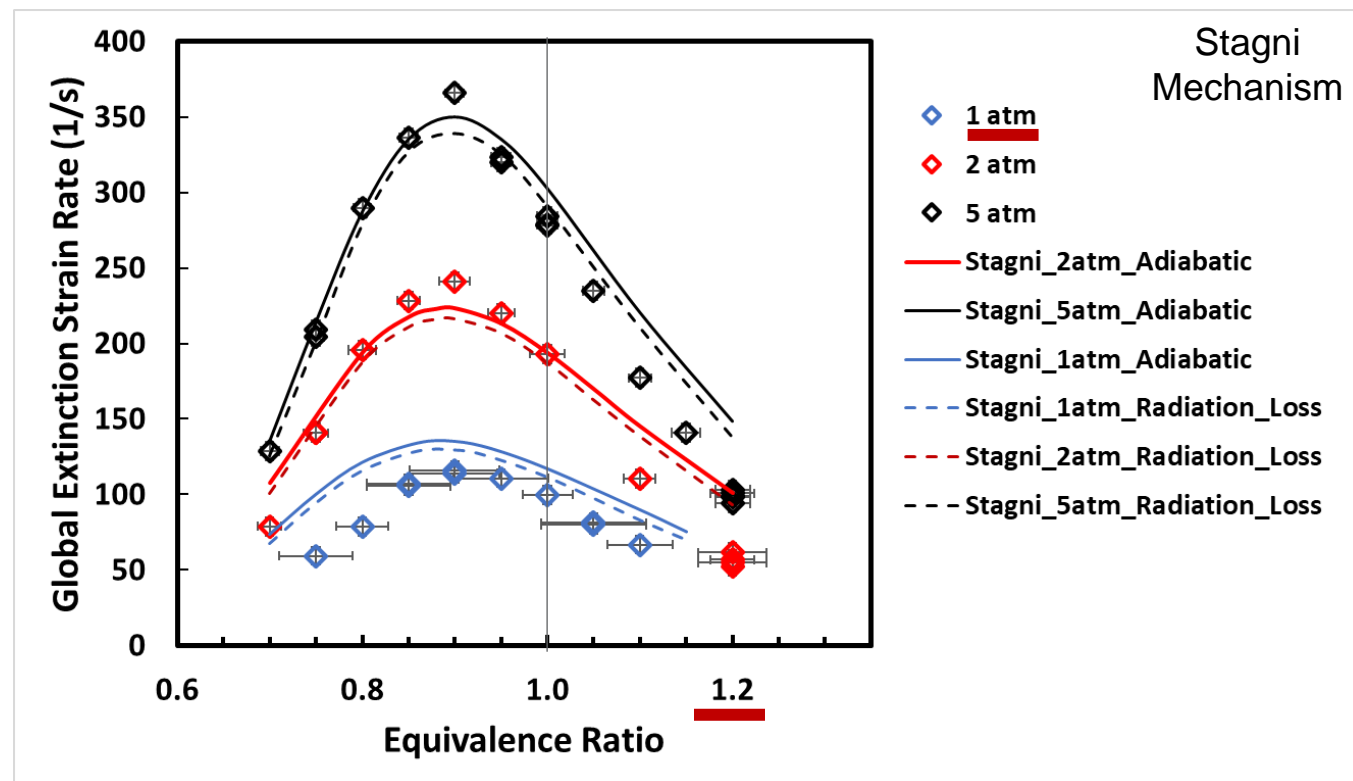
Kinetic Models

- Glarborg et al. (2018)
- Stagni et al. (2020)
- Powell et al. (2011)
- Powell et al. (2010)
- Glarborg (2023)

Experimental Data

- × Colson et al. (2016)
- ◆ Current Data

- Two “Powell” mechanisms differ by only 3 different rate expressions for amine radical reactions:

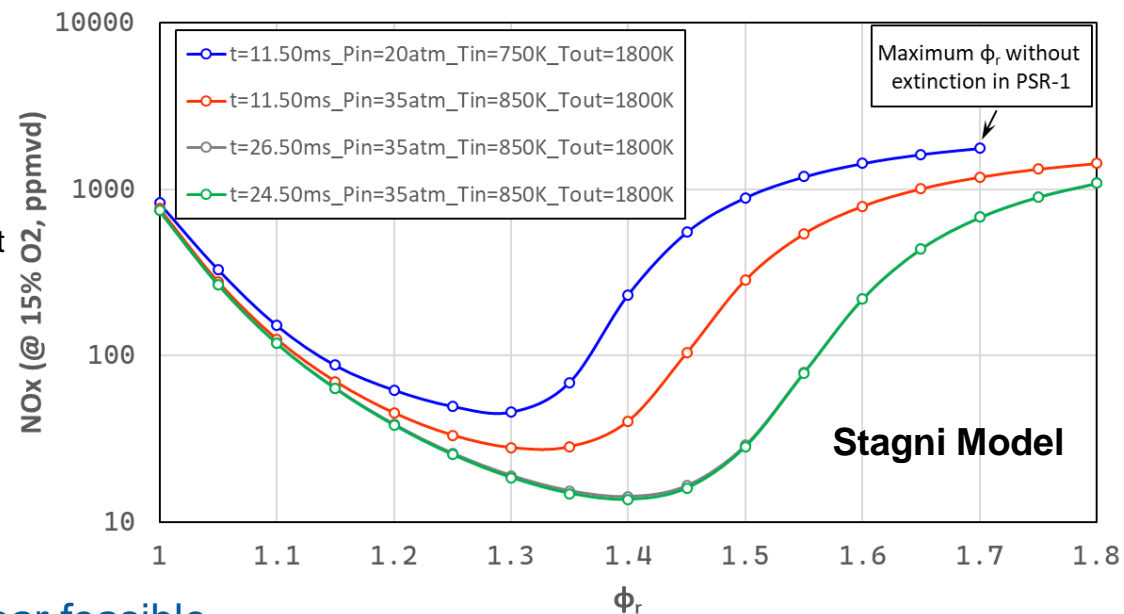
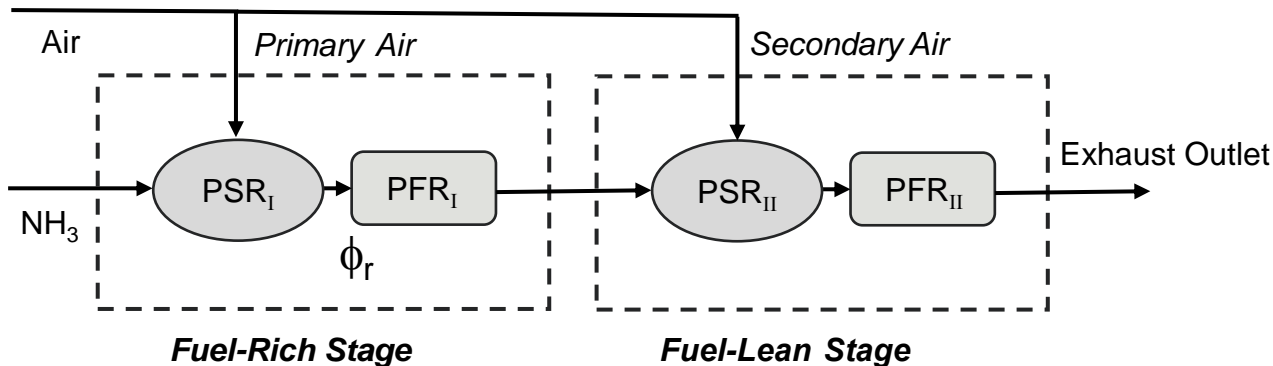


Stagni Mechanism

- ◆ 1 atm
- ◆ 2 atm
- ◆ 5 atm
- Stagni_2atm_Adiabatic
- Stagni_5atm_Adiabatic
- Stagni_1atm_Adiabatic
- - - Stagni_1atm_Radiation_Loss
- - - Stagni_2atm_Radiation_Loss
- - - Stagni_5atm_Radiation_Loss

Chemical Reactor Network (CRN) Model → ROM Design Tool

CRN Model Schematic for RQL Combustor



- Outlet temperature fixed at 1800 K.
- Overall “theoretical” NO_x levels <30 ppm for a RQL architecture appear feasible

Total Residence time τ (ms)	τ_{PSR_I} (ms)	τ_{PFR_I} (ms)	τ_{PSR_II} (ms)	τ_{PFR_II} (ms)	Pressure (atm)	Inlet Temp. (K)	Rich Stage		Lean Stage**		
							NH ₃ ($\phi_r = 1.25$) (ppm_wet)	NO ($\phi_r = 1.25$) (ppm_wet)	NO ($\phi_r = 1.25$) (ppm_wet)	NO _x * ($\phi_r = 1.25$) (ppm)	NO _{x,min} * (ppm)
11.50	0.50	5.0	1.0	5.0	20	750	9.5	121.6	68.0	49.8	46.0
11.50	0.50	5.0	1.0	5.0	35	850	8.1	75.7	40.6	33.3	28.0
26.50	0.50	20.0	1.0	5.0	35	850	6.5	57.3	31.5	26.0	14.2
24.50	0.50	20.0	1.0	3.0	35	850	6.5	57.3	30.9	25.5	13.7

** NH₃ slip <1E-5 ppm at exhaust

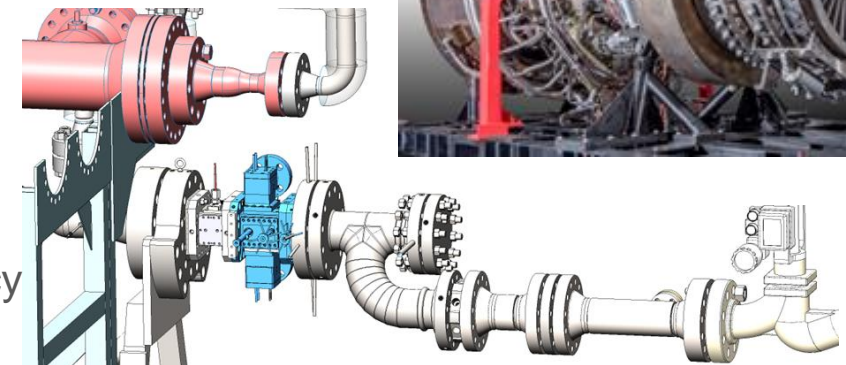
* 15% O₂ dry

Modeling NH₃ Combustor CFD for NH₃ NO_x Estimates & Combustor Design

Low-NO_x Operable Ammونيا-Combustor Development (LOAD-Z)

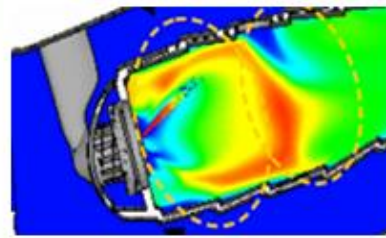
- Fundamental NH₃ flame data relevant to turbines:
 - P, T >> ambient → relevant to compressor exit conditions
 - strained & turbulent flames
 - Targeted outcome: expand published data w/ new, useful data (previously unreported)
- Predictive capability for NH₃ combustion & emissions
 - NO_x formation kinetics integral w/ NH₃ comb. kinetics
 - CFD of turb. NH₃ flames w/ NO_x & NH₃ slip (η_{COMB}) prediction
 - Targeted outcome: capability for GT combustor design
- Develop & test NH₃ gas-turbine combustor “@ scale”
 - Single-nozzle-rig (SNR) scale demo. @ high P, T
 - Pure NH₃ combustion @ 75% – 100% power
 - Targeted outcome: < 30ppm NO_x** & >99.99% efficiency

(3)
DESIGN & DEMO.

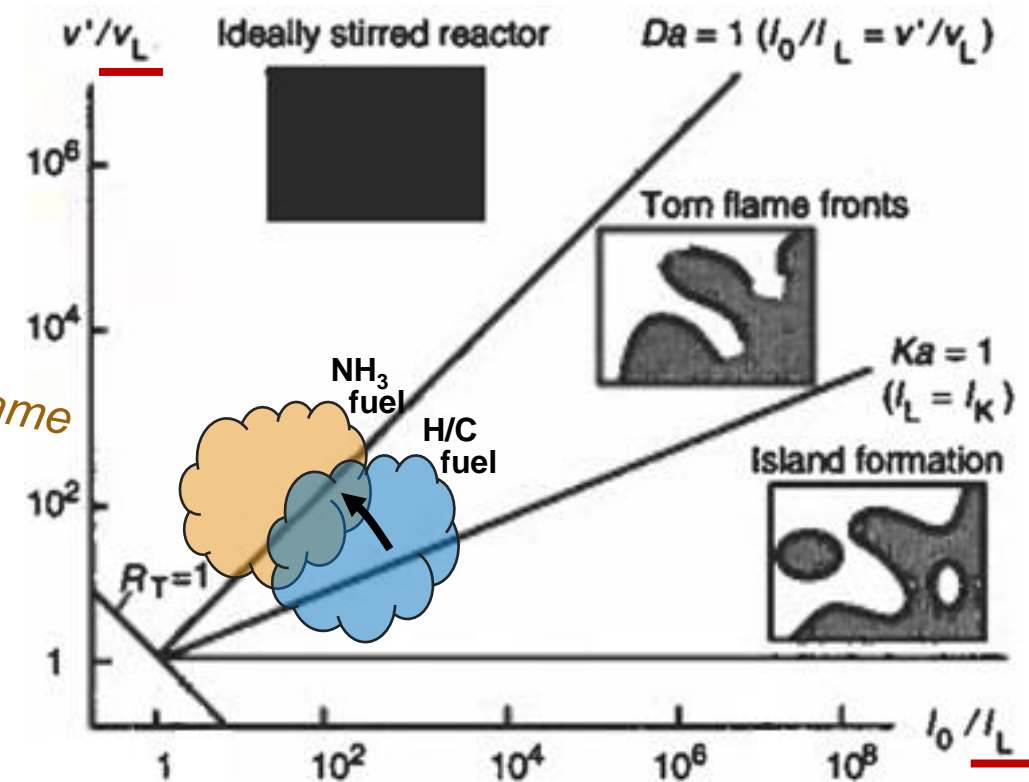
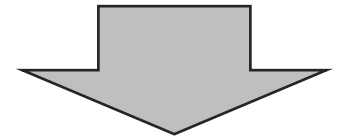


**Note recent ETN recommendations for NO_x reporting with hydrogen-containing fuels

Modeling Activities & Next Steps Toward GT Design



– Single-nozzle high-pressure combustor, fired w/ NH_3 fuel



validate w/ turb. flame rig measurements

Turbulent combustion regime for NH_3 -fueled gas turbines:

- v' & $l_0 \sim$ independent of fuel type (only aero dependent)
- $v_L \downarrow$ w/ NH_3 fuel
- $l_L \uparrow$ w/ NH_3 fuel
- shift by $\sim 5 - 10x$

CFD modeling of NH_3 -fueled gas turbine combustor:

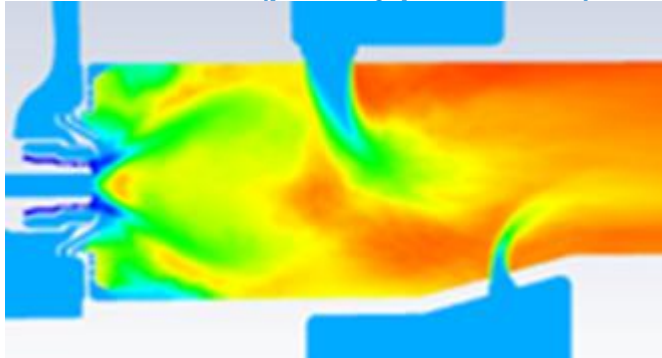
- Challenges:
 - Efficient flamelet models uncertain (regime \Rightarrow stirred)
 - NO_x cannot be post-processed (integral to comb. rxns)
- For efficient GT design calculations, *possible approach*:
 - Reduced NH_3/NO_x kinetics w/transport, e.g. EDC**
 - Steady RANS turbulence model saves computational power for chemistry/transport

Developing CFD Approach for NH₃ Combustor Aero Design

Begin CFD methodology evaluation w/H₂ combustion case from existing RTRC exp. rig:

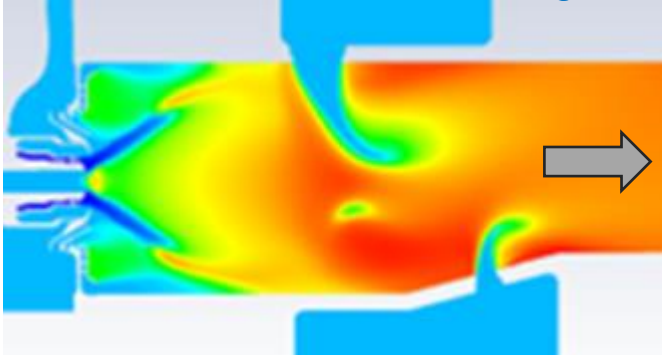
- Change **from** LES turbulence model **to** steady-RANS (realizable k-eps.)
- Change **from** 2-mixture-fraction/Zimont combustion model **to** EDC w/species transport
- Start w/complete H₂ combustion chemical mechanism (10-species)
- Then add NOx mechanism (coupled w/H₂ mechanism) & evaluate emiss. predict. (12-species)
- Then add NH₃ combustion mechanism (31-species)

LES/2mf/Zimont (partially premixed St)



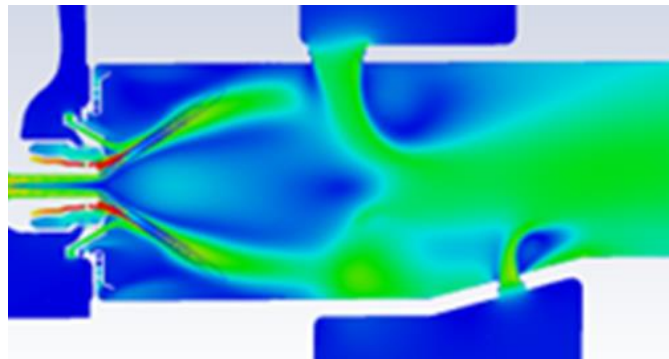
LES w/out NOx prediction capability (no species transport)

RANS/EDC/LLNL H₂/Air Mech. & Stagni NOx



EDC-predicted NOx qualitatively matches rig meas. ...within factor of 1 to 1.5 for three different FARs...

RANS/EDC/LLNL H₂/Air Mechanism



GT2024-121321
 Proceedings of ASME Turbo Expo 2024
 Turbomachinery Technical Conference and Exposition
 GT2024
 June 24-28, 2024, London, United Kingdom

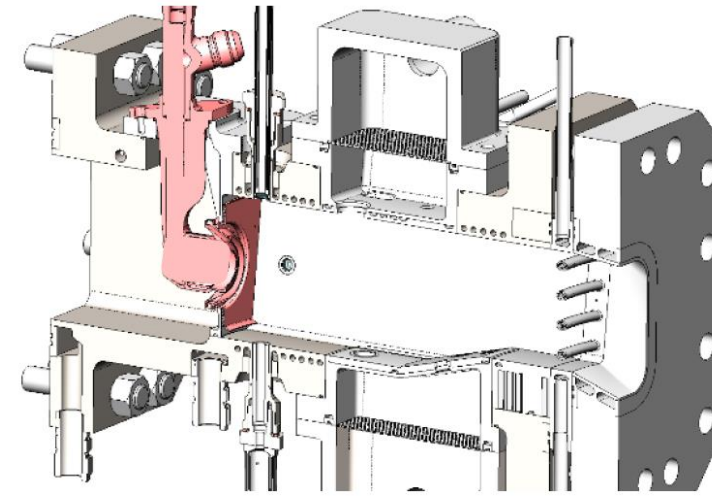


FIGURE 5. FT4000 Single Nozzle Combustor Rig (SNR).

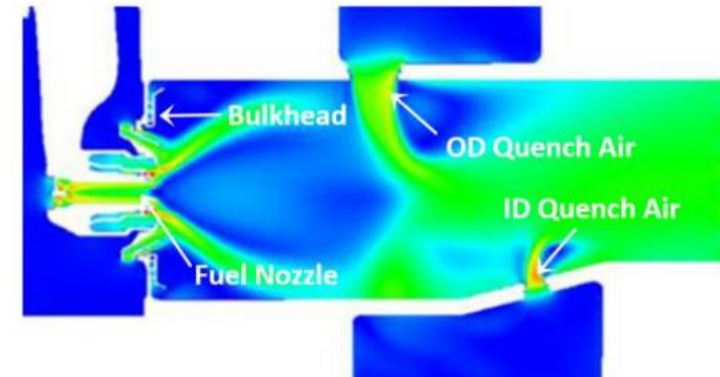
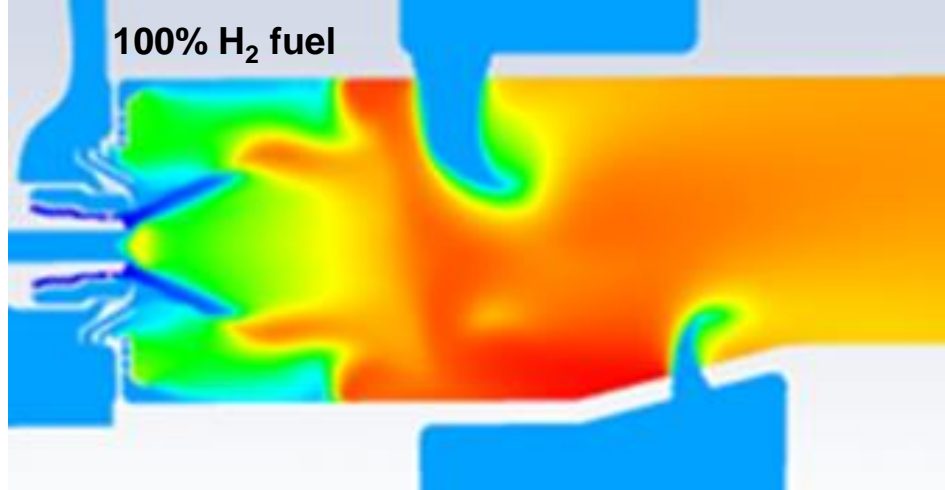


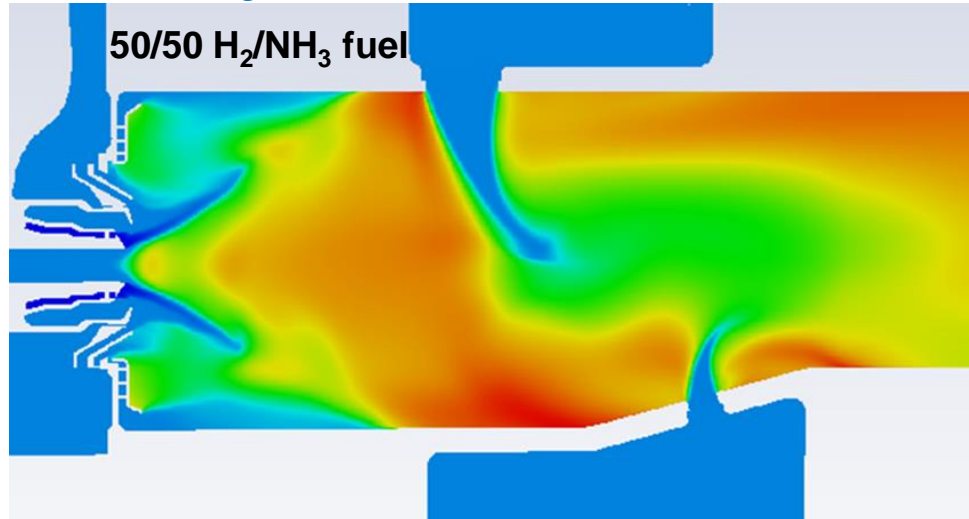
FIGURE 7. CFD analysis of engine (a) and rig (b) combustor velocity flowfields.

Initial CFD Simulation of NH₃ Combustion in Existing Geom.

RANS/EDC/LLNL H₂/Air Mech. & Stagni NO_x



RANS/EDC/Stagni Mech. for Combustion & NO_x



GT2024-121321

Proceedings of ASME Turbo Expo 2024
Turbomachinery Technical Conference and Exposition
GT2024

June 24-28, 2024, London, United Kingdom

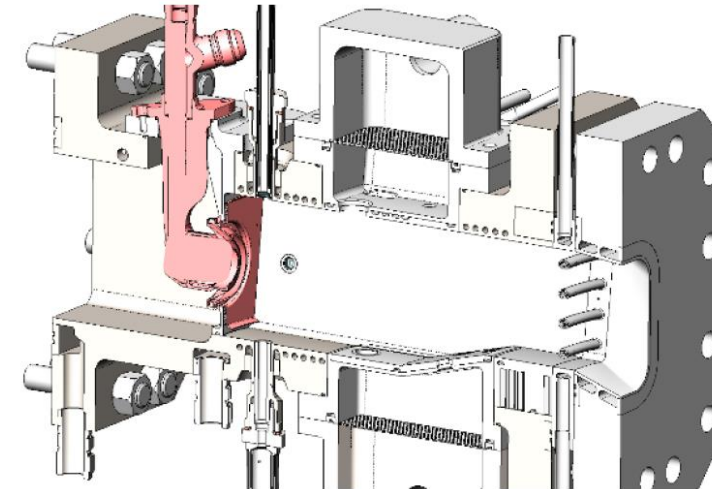


FIGURE 5. FT4000 Single Nozzle Combustor Rig (SNR).

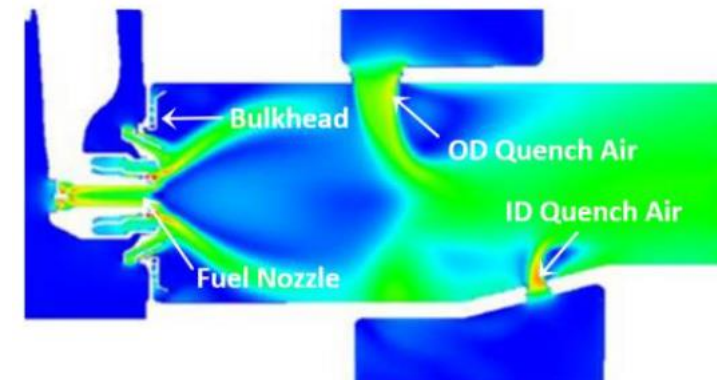


FIGURE 7. CFD analysis of engine (a) and rig (b) combustor velocity flowfields.

Fundamental Flat-Flame Data RTRC EXPERIMENTS

Low-NOx Operable Ammonia-Combustor Development (LOAD-Z)

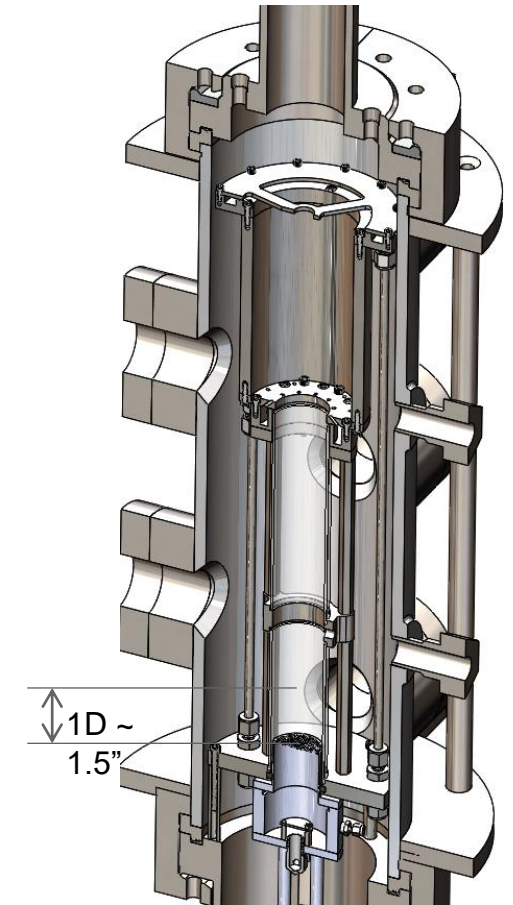
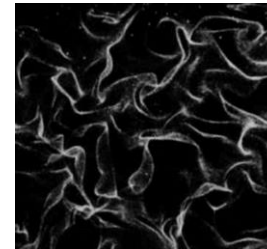
(1)

RTRC
Experiments

RTRC

RTX Technology
Research Center

- Fundamental NH_3 flame data relevant to turbines:
 - P, T \gg ambient \rightarrow relevant to compressor exit conditions
 - strained & turbulent flames
 - Targeted outcome: expand published data w/ new, useful data (previously unreported)
- Predictive capability for NH_3 combustion & emissions
 - NO_x formation kinetics integral w/ NH_3 comb. kinetics
 - CFD of turb. NH_3 flames w/ NO_x & NH_3 slip (η_{COMB}) prediction
 - Targeted outcome: capability for GT combustor design
- Develop & test NH_3 gas-turbine combustor “@ scale”
 - Single-nozzle-rig (SNR) scale demo. @ high P, T
 - Pure NH_3 combustion @ 75% – 100% power
 - Targeted outcome: < 30ppm NO_x^{**} & >99.99% efficiency



RTRC

RTX Technology
Research Center

UCONN
UNIVERSITY OF CONNECTICUT

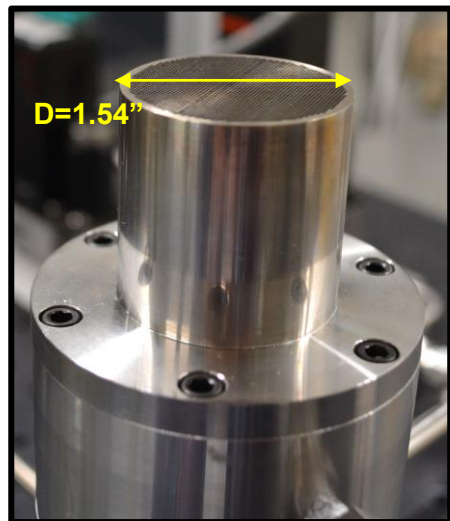
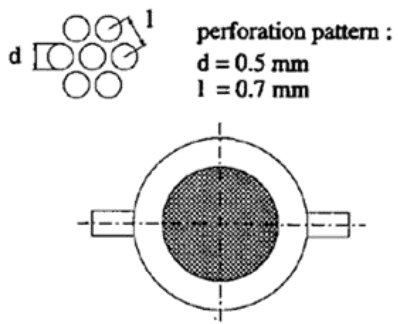
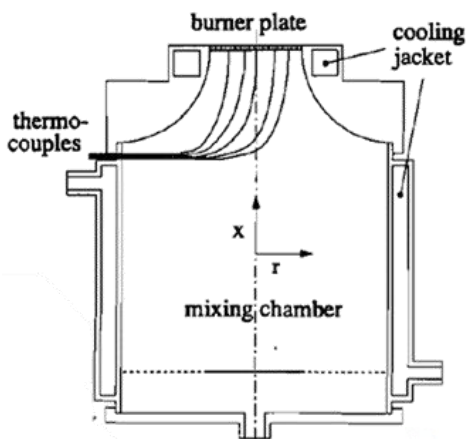
High-Pressure Flat-Flame Burner Rig

Goal: Characterize NO_x emissions from laminar flame at high pressure for model validation

Scarce data available on NO_x formation in NH_3 flames at $\gg 10$ atm

Target system operation >20 atm

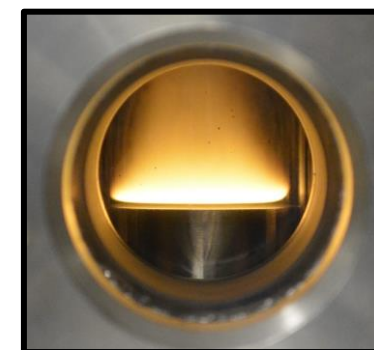
Allows evaluation of staged (RQL) NH_3 combustion



Burner Surface
~2400 holes, $D=0.020$ "



Methane Combustion



Ammonia Combustion

Facility Preparations for High-Pressure Operation

RTXC configuration & capability:

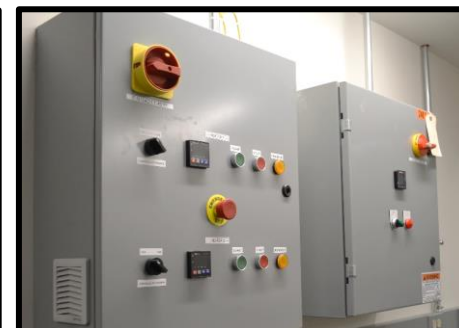
- **425** to >500+ K preheat capability (>25-atm w/new heater install.)
- **10** to >20-atm pressure vessel & feeds ... fuel, air, & N₂ chamber flow

Facility Preparations – Completed

- High-pressure vessel w/ pass-throughs
- Ventilated experiment enclosure
- Interlocked PLC control system
- High-pressure air & N₂ supply
- Inlet air heater (low pressure)
- Remote flow control system for air, CH₄, NH₃, and N₂
- Backpressure valve for chamber pressure control

Facility Preparations – In Progress

- *Inlet air heater (high-pressure)*
- *High-pressure liquid ammonia pumping cart w/ refrigerated pumps*
- Heater controllers for air and NH₃ heaters



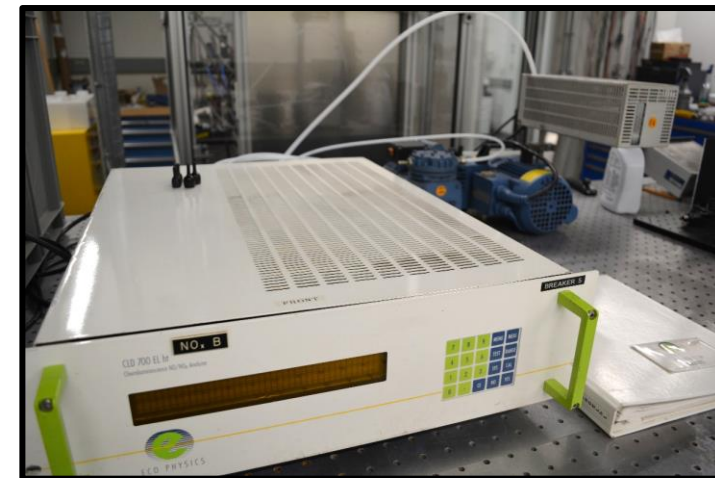
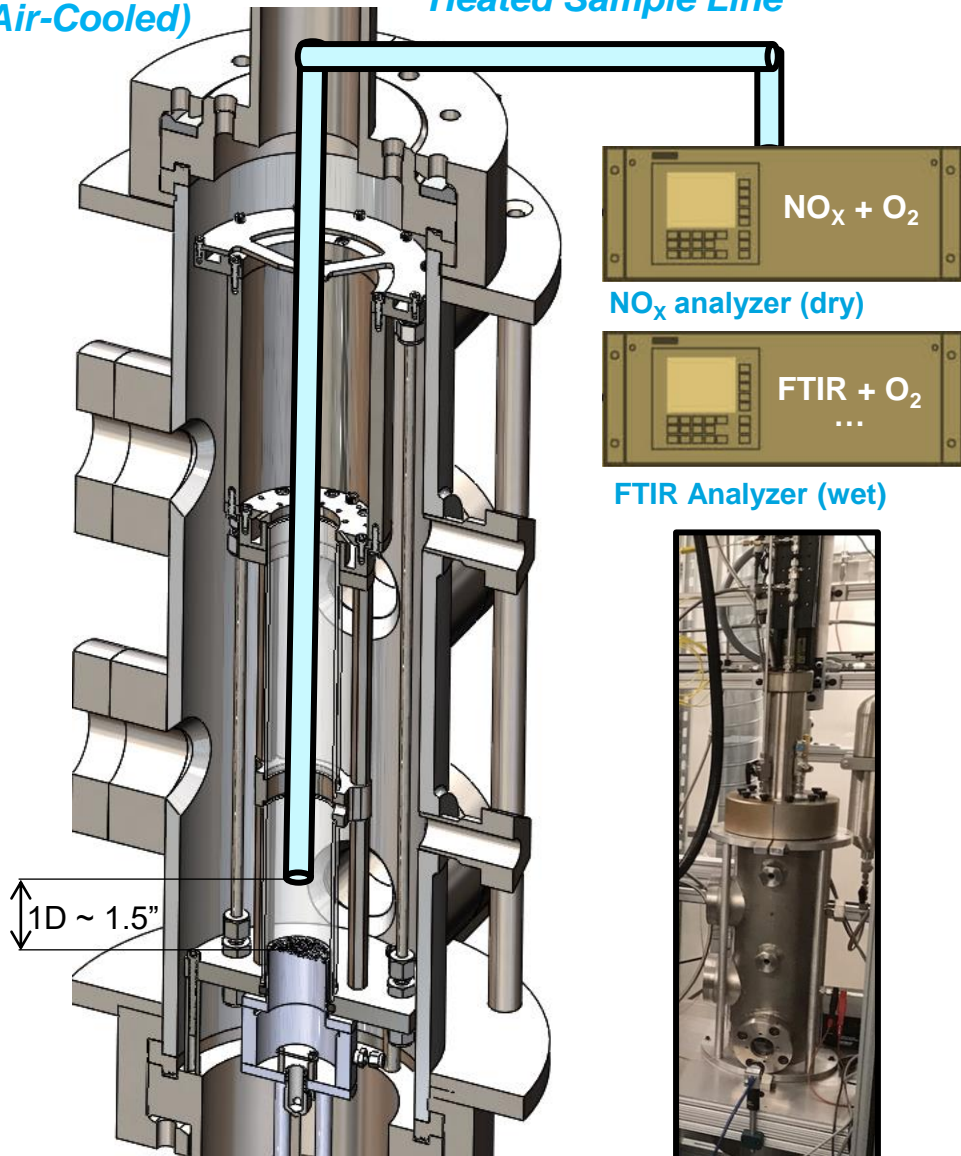
Emissions Sampling System

Emissions Sampling

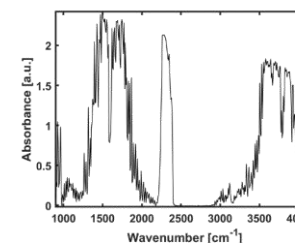
- Air-cooled sample probe
- Probe traversable using translation stage system
- Heated sample line to prevent condensation
- NO_x analyzer system with ammonia scrubber & dryer
- Heated, NH₃ compatible FTIR system accepts wet sample
 - FTIR species: H₂O, NH₃, NO, NO₂, N₂O
- Sample chain can be easily swapped from conventional analyzer to FTIR system
- Sample probe can be swapped with B-type TC-probe for heat loss characterization

Traversable Emissions Probe (Air-Cooled)

Heated Sample Line

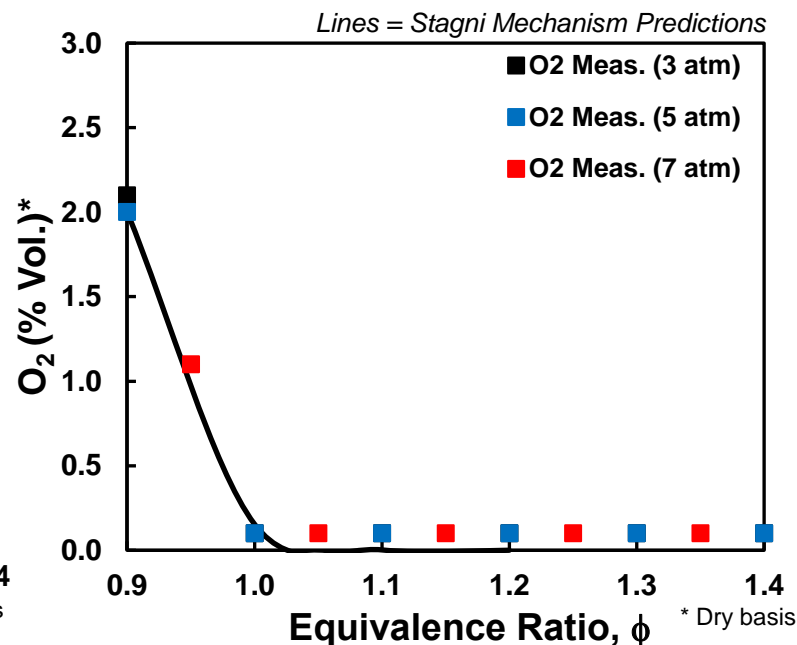
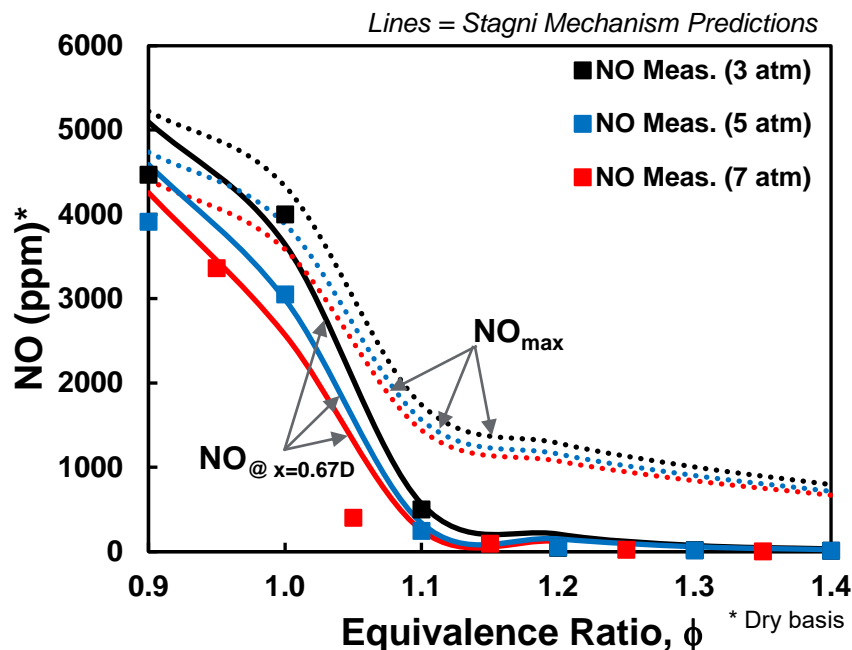


Conventional NO_x Analyzer



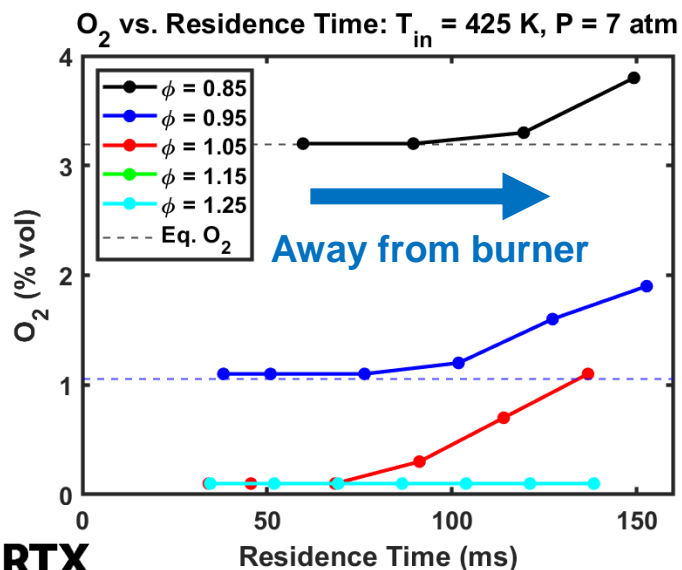
FTIR Analyzer & Sample FTIR Spectrum

Flat-Flame NO_x Emissions Results – Moderate Pressure

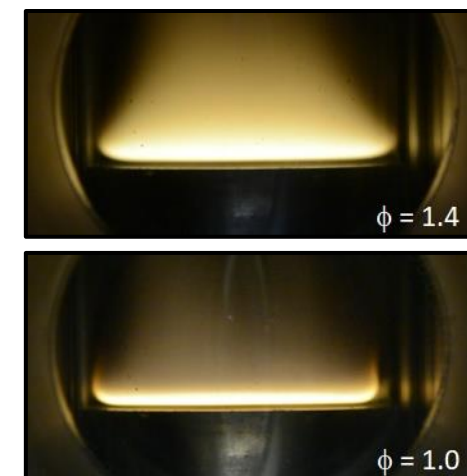


- NO_x analyzer used to collect emissions data across multiple pressure conditions
- 425 K preheat, 9-15 cm/s burner velocity
- $x=0.67D$ - 1D sample-probe location
- Stable burner operation achieved across pressures and equivalence ratios at 425 K
- Adiabatic flame model used w/ Stagni mech.
- FTIR data at select 7-atm conditions shows high NH₃ comb. efficiency (<75 ppm NH₃)

NH₃ / air flames
@ P = 3-atm



- Experimental challenges observed when translating probe to locations further from burner surface
- Measured oxygen concentration increases at locations further from surface
- Downstream cooling air entrainment is likely occurring
- **Further system optimization needed to reduce pathways for entrainment before additional measurements**



Next Steps for High-Pressure NO_x Measurements

Next Steps for Improved Emissions Data

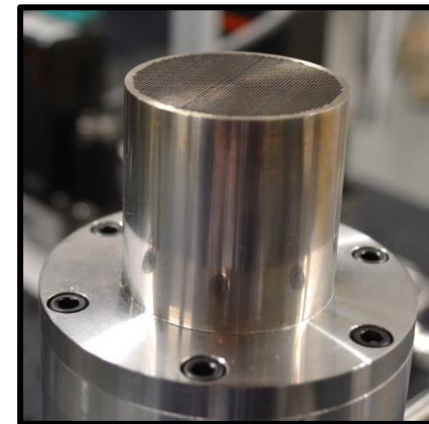
- Improve sampling/burner system for reduced air entrainment
- Collect additional data using NO_x/O₂ analyzer system to confirm reduced entrainment
- Collect temperature profile along centerline to characterize burner heat loss
- Collect additional emissions data using FTIR to measure other species

Improvements for Higher Pressure Operation

- Integrate high-pressure liquid pumping cart to allow higher-pressure gaseous NH₃ input
- Integrate liquid-pumping cart with existing PLC infrastructure
- Finish installing high-pressure-rated heater & controllers

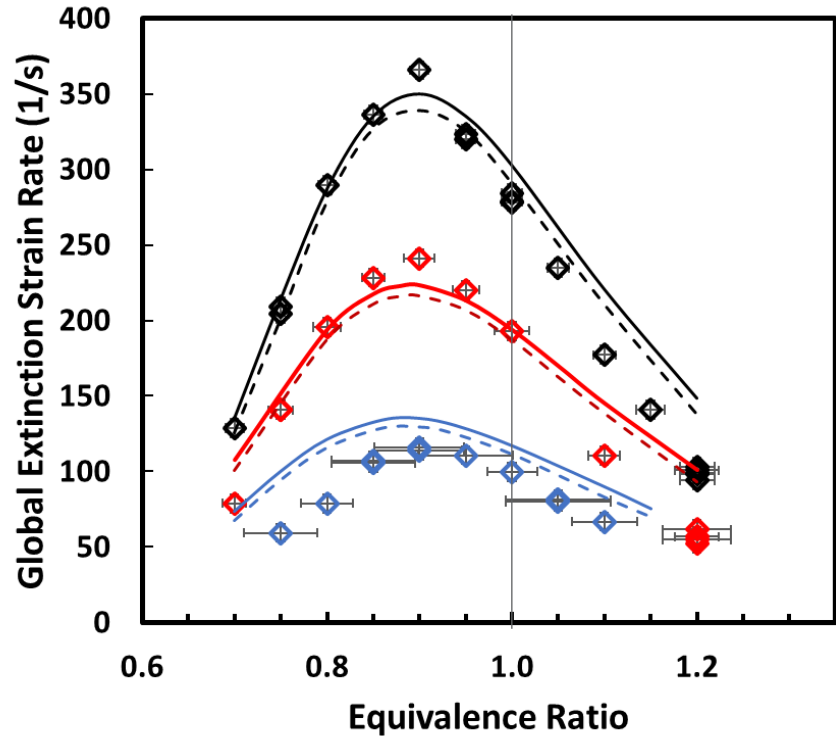
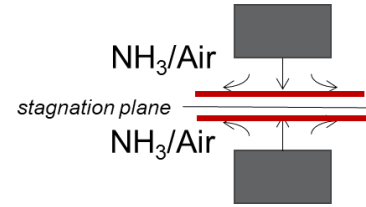
Laminar burner operating well up to 7 atm

Further improvements underway to improve & validate data quality and achieve higher pressure operation >20 atm



BACKUP

RTRC Predictions vs. UConn Measurements (1/2)

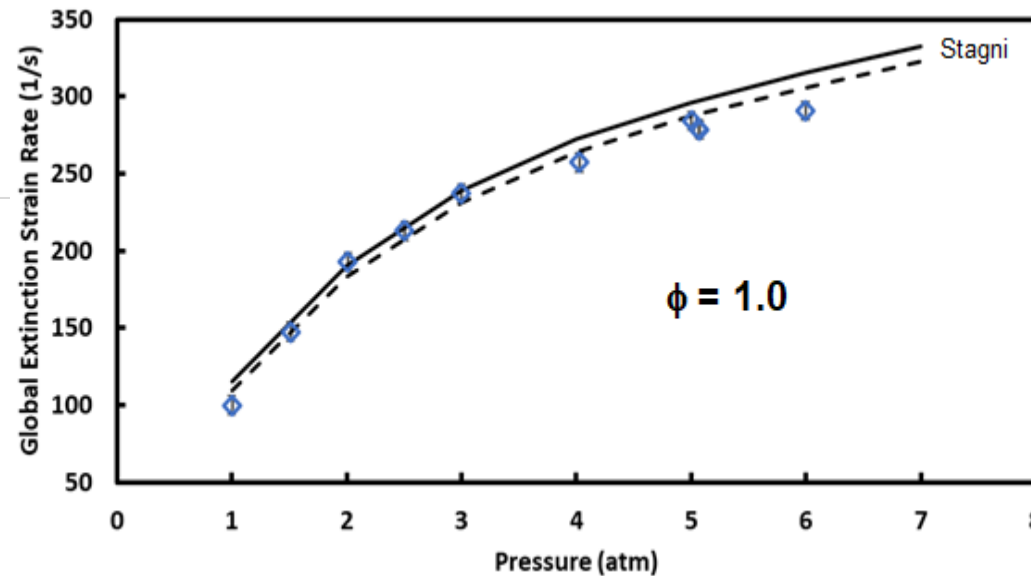


- Stagni Mechanism
- ◆ 1 atm
 - ◆ 2 atm
 - ◆ 5 atm
 - Stagni_2atm_Adiabatic
 - Stagni_5atm_Adiabatic
 - Stagni_1atm_Adiabatic
 - - Stagni_1atm_Radiation_Loss
 - - Stagni_2atm_Radiation_Loss
 - - Stagni_5atm_Radiation_Loss

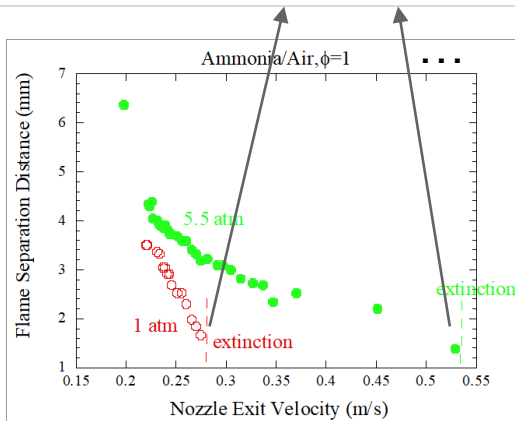
$$q_r = -4\sigma\kappa_p(T^4 - T_o^4)$$

Modified Counterflow Model scripts to account for radiative heat loss
Radiative heat loss per unit volume

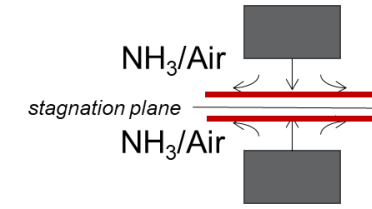
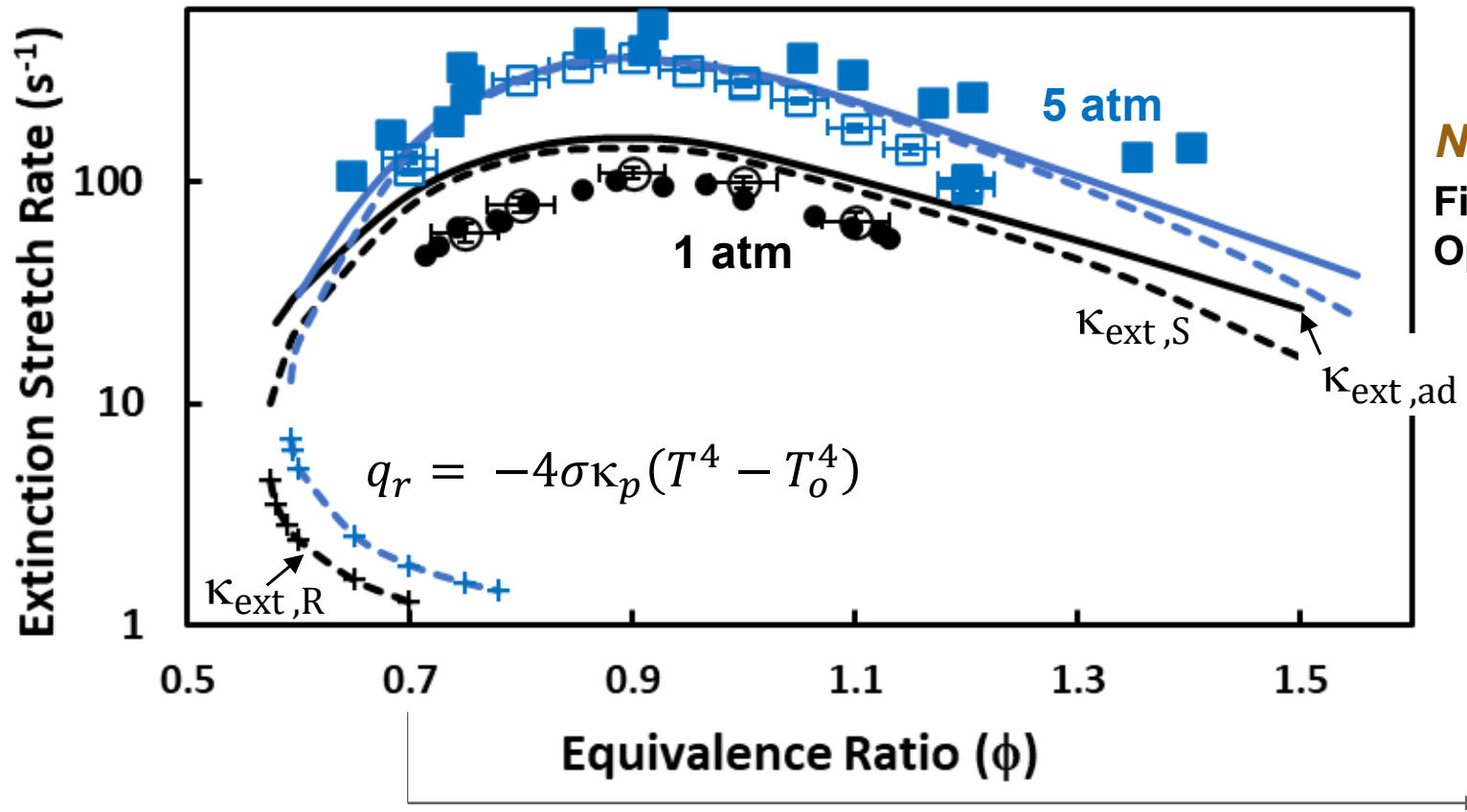
(σ = Stefan-Boltzmann constant, T_o = ambient unburnt reactant temp.,
 κ_p = total Planck's mean absorption coefficient)



Roll-off in a_{EXT} with pressure (non-linear)

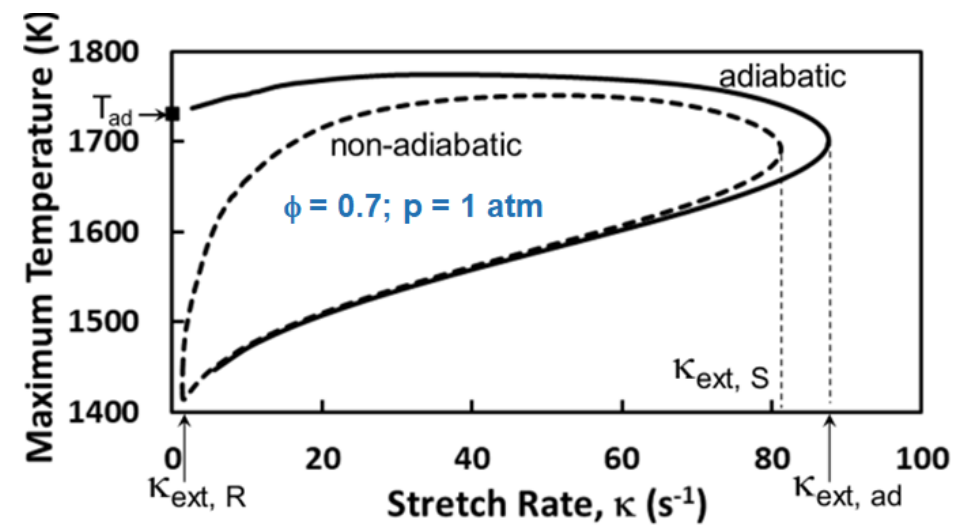


Counterflow NH₃ Flames w/Heat Loss → Impact & Lean Limit



NH₃/Air Counterflow Flames

Filled Symbols: Colson et al. (2016)
Open Symbols: UConn Data (2023-4)



C-shaped curve for counterflow premixed fuel-lean, ammonia-air flames showing:

- i. adiabatic stretch-induced stretch rate $\kappa_{ext,ad}$ (solid line),
- ii. non-adiabatic stretch-induced stretch rates $\kappa_{ext,S}$ (dashed line), and
- iii. radiative-induced stretch rates $\kappa_{ext,R}$ (+ symbols).

Take-Away:

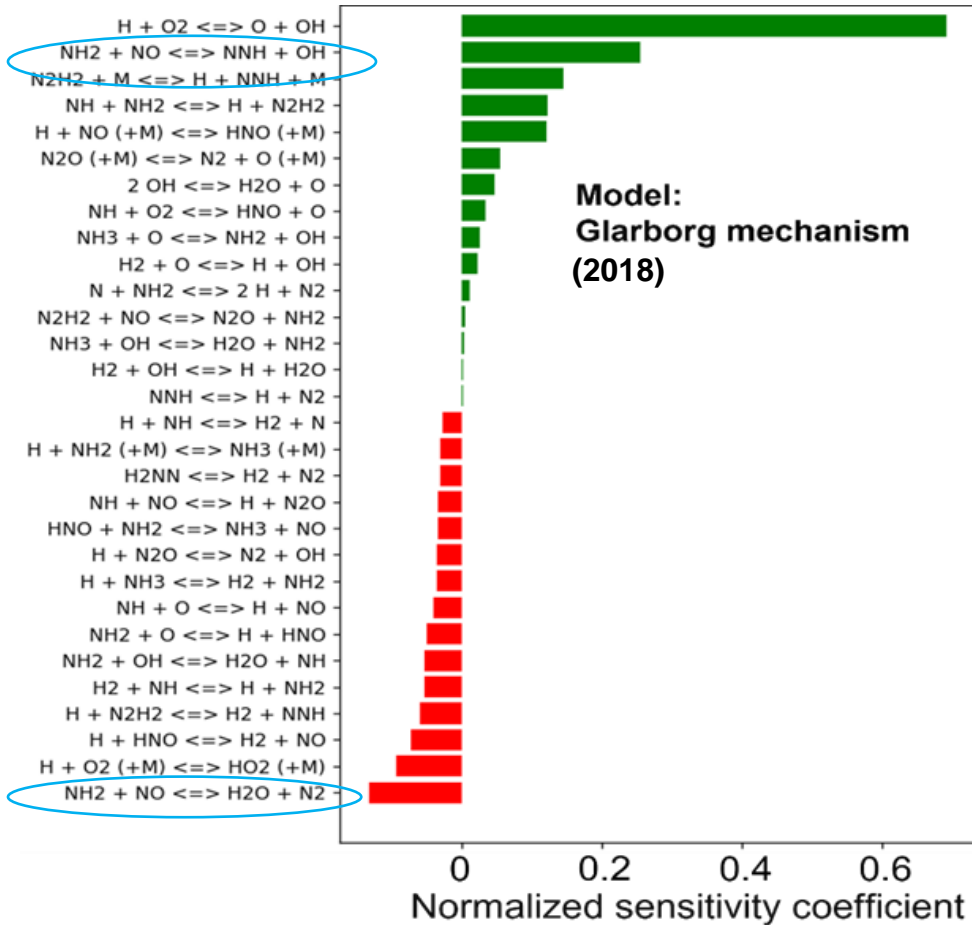
- Heat-loss weakens low-burning-rate NH₃ flames
- Stretched high-burning-rate flames more robust

Feature Sensitivity to Extinction Strain Rate

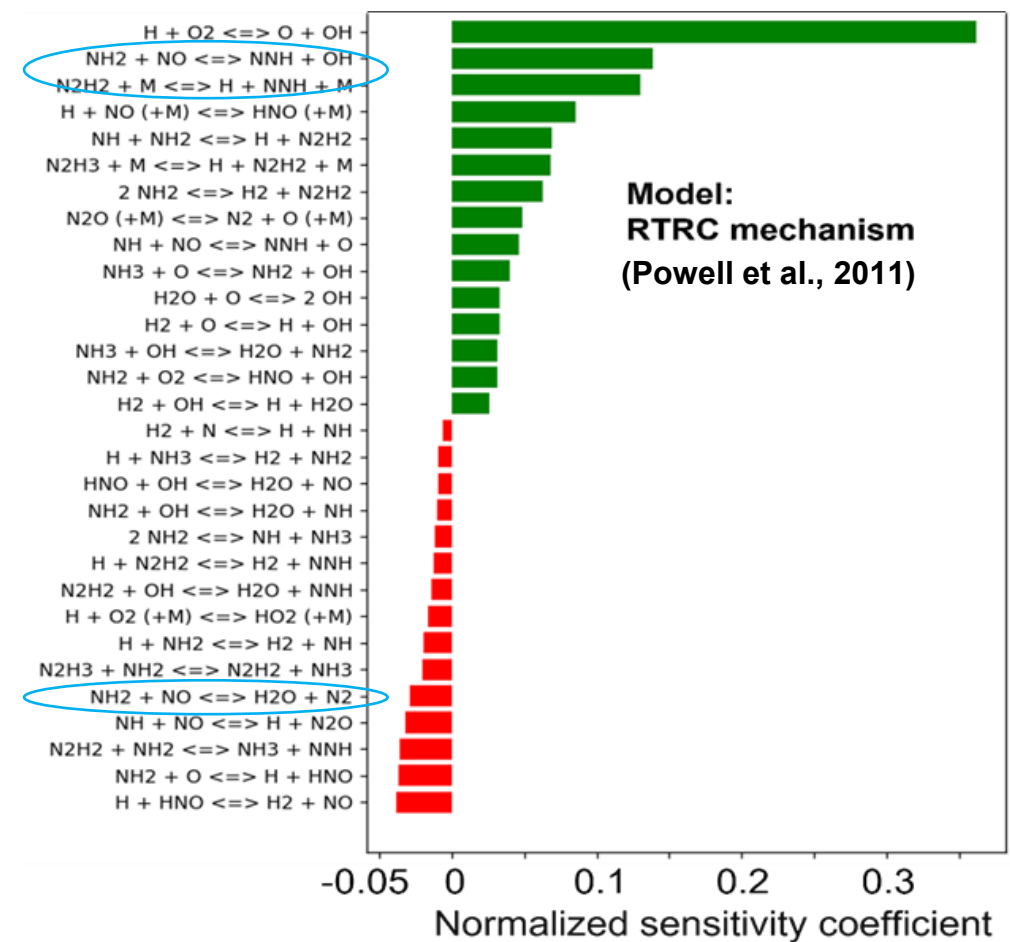
NH₃/Air Counterflow Flame

- (1) $NH_2 + NO \leftrightarrow N_2 + H_2O$
- (2) $NH_2 + NO \leftrightarrow NNH + OH$
- (3) $NH_3 + NH_2 \leftrightarrow N_2H_3 + H_2$

T_i = 301/333 K; P = 0.1 MPa



T_i = 301/333 K; P = 0.1 MPa



Sensitive rate constants:

NH₂/NO Interactions

- (1a) $NH_2 + NO \leftrightarrow N_2 + H_2O$
- (1b) $NH_2 + NO \leftrightarrow NNH + OH$

NH_i/N₂H_i Reactions

- (2a) $N_2H_2 + M \leftrightarrow NNH + H + M$
- (2b) $N_2H_3 + M \leftrightarrow N_2H_2 + H + M$

Sensitive and Uncertain rate constants

END