

Ammonia Combustion for Gas Turbine Engines



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Solutions for Today | Options for Tomorrow



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- Advanced Turbines Goal 2 Overview
- Motivation
- Fundamental Measurements
 - Laminar Flame Speed
 - Species Concentrations
- Modeling
- Applied Testing (atmospheric pressure)
- High Pressure Developments (2025)

Advanced Turbines MYRP – Goal 2

Data Dissemination

Establish an ammonia combustion data repository on EDX (NETL data)

Continue ammonia combustion working group

Solicit external contributions to EDX repository

Atmospheric Experiments (PGH)

Conduct fundamental burner studies for model validation

Develop engineering-level CFD models of candidate burner/combustor configurations

Perform atmospheric pressure testing in PGH FCL

Application of advanced diagnostics for comprehensive validation data sets

High Pressure Experiments (MGN)

Develop high-P NHG delivery system

Modify the NETL PPC for NH₃ (and H₂) use up to 10 atm, 1MWth

Conduct high-P experiments – map combustor operability, global emissions

Application of advanced diagnostics for validation and combustor characterization

Iterate burner/quick mix designs to achieve <25 ppm NO_x, negligible NH₃ slip

Motivation

- Hydrogen expected to play an important role in meeting U.S. net-zero 2050 goals
 - VRE
 - Reserve/peak power
 - Hard-to-electrify sectors (industrial decarbonization)
- Ammonia is an attractive hydrogen carrier due to favorable storage/transport characteristics, existing industry, infrastructure
- H_2 to NH_3 must be worthwhile
 - Long distance transport
 - Long duration storage
- Direct utilization of NH_3 favorable vs. reconverting to H_2

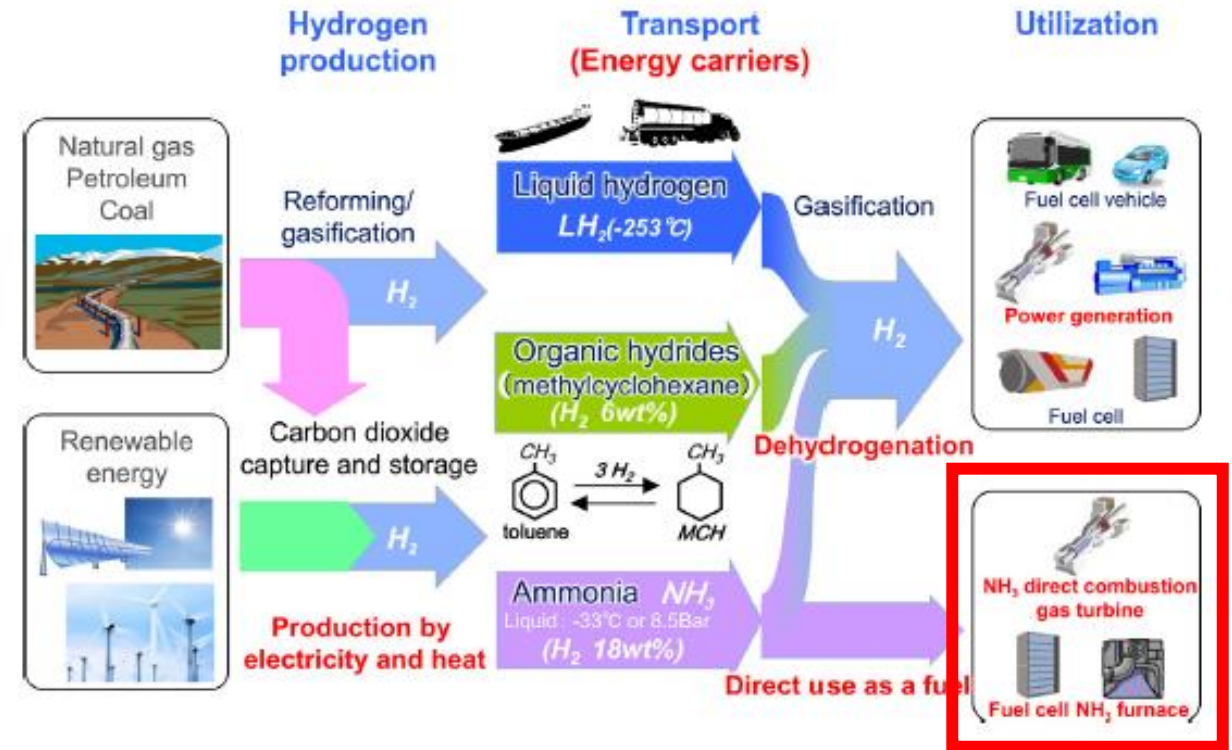
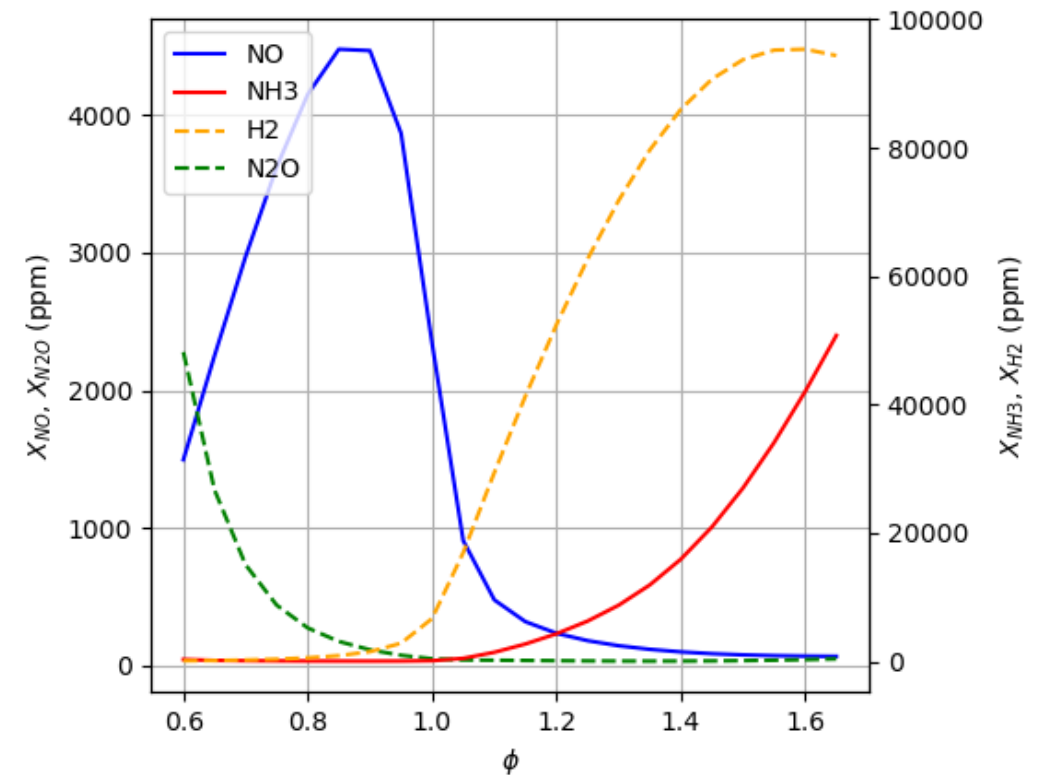


Figure from Kobayashi et al. "Science and technology of ammonia combustion", Proceedings of the Combustion Institute 37 (2019) 109–133

Combustion Characteristics of Ammonia

- Two largest technical challenges
 - Low flammability
 - High NO_x (+N₂O) or unburnt NH₃
- Chemistry differs considerably from HC fuels – requires new strategies
- Two-stage RQL proposed for low emissions
- Requires models which make accurate predictions over a wide range of equivalence ratios and compositions



PSR simulation, Otomo 2017 mech, 300K/1atm, τ_{res} =50ms

- Numerous kinetic mechanisms available for ammonia
 - Some specific to $\text{NH}_3\text{-CH}_4$ or $\text{NH}_3\text{-H}_2$ mixes
- Requires complex N-chemistry
- Validated reduced mechanisms needed for CFD
- Improved validation data needed
 - Laminar flame speeds
 - Ignition delay times
 - Species concentrations

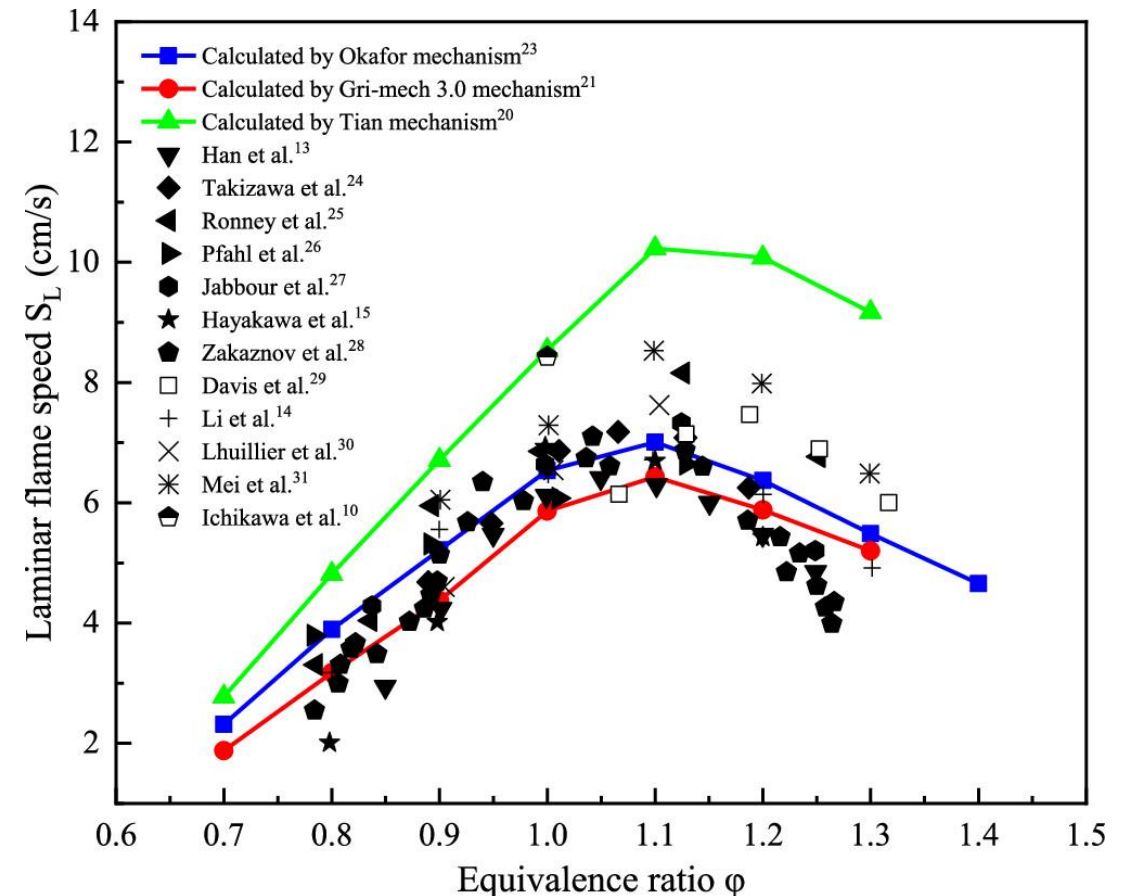


Figure: Zhang et al., "Effect of CH_4 , Pressure, and Initial Temperature on the Laminar Flame Speed of an $\text{NH}_3\text{-Air}$ Mixture", ACS Omega 2021, 6, 18, 11857–11868

Experimental Setup

Laminar Flame Speed & Species

- Off-the-shelf stainless-steel McKenna burner
- UHP gases
 - Anhydrous NH₃, vapor draw
- Alicat MFCs
 - Corrosive-compatible NH₃
- Lauda circulating bath to regulate burner plug temp
- N₂ shroud

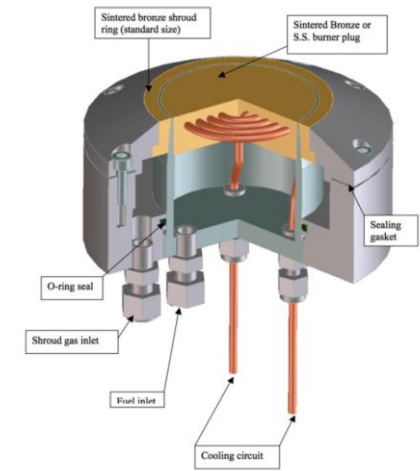
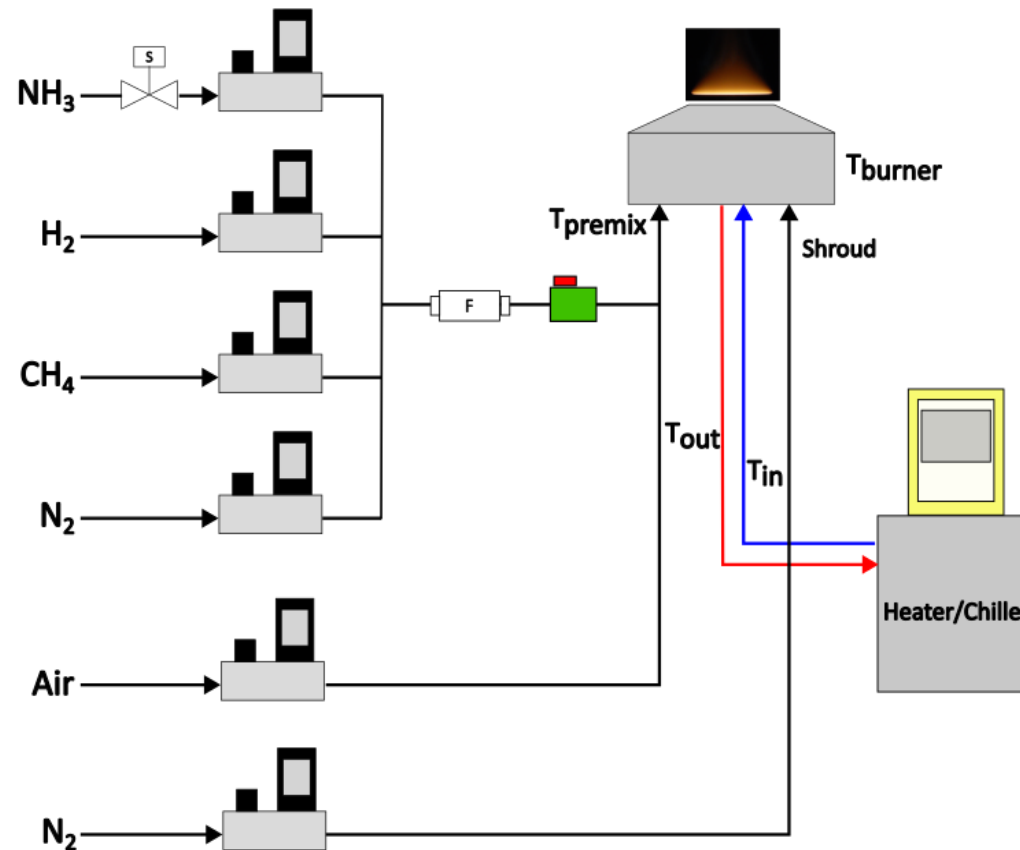


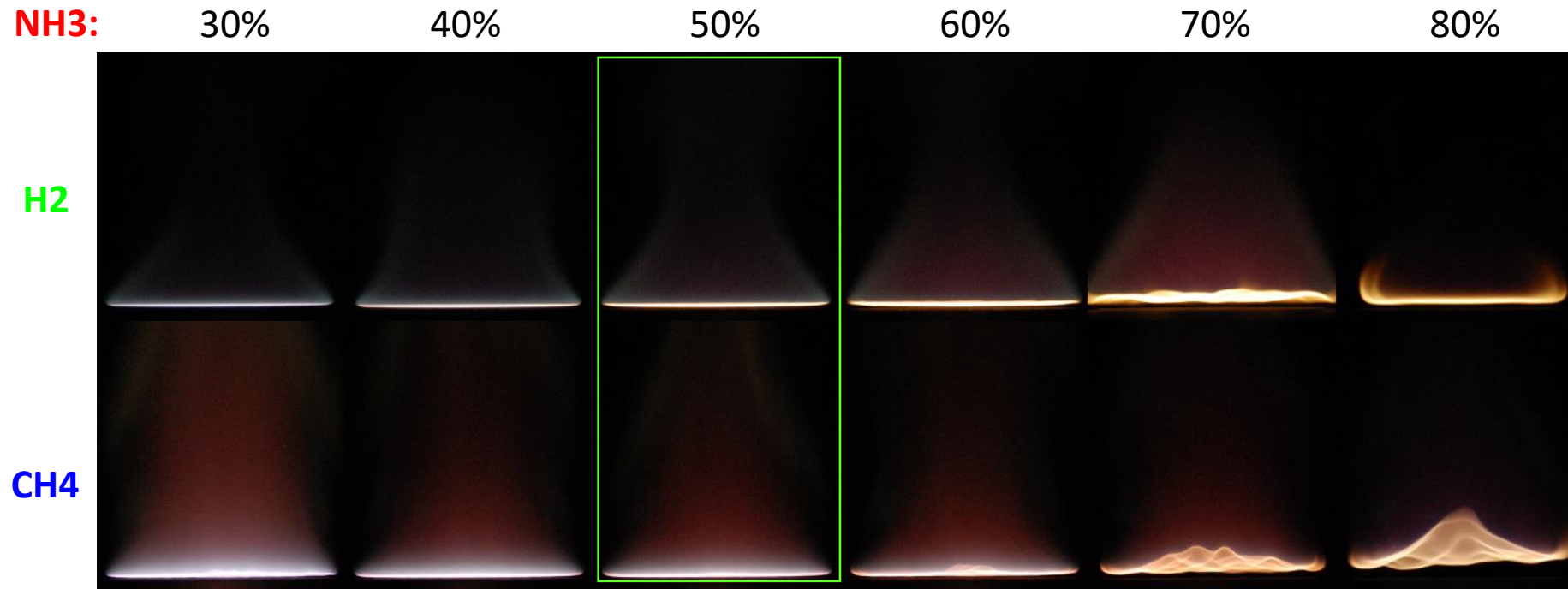
Image from Holthuis and Associates, flatflame.com



Flame Conditions

Laminar Flame Speed & Species

- Two flames selected for initial characterization



Diagnostic Approach for Laminar Flame Speed

- Burner heat flux method
 - Determine gas velocity which exactly opposes flame propagation speed
 - Heat added by burner plate equals flame heat loss
 - Adiabatic point = flat temperature profile
 - Requires measurement of burner face temperature profile
 - Interpolation vs. extrapolation
- Sources of uncertainty: flow controllers supplying gas, surface temperature measurement
- Novel approach proposed to utilize IR imaging to derive complete 2D burner face temperature profile

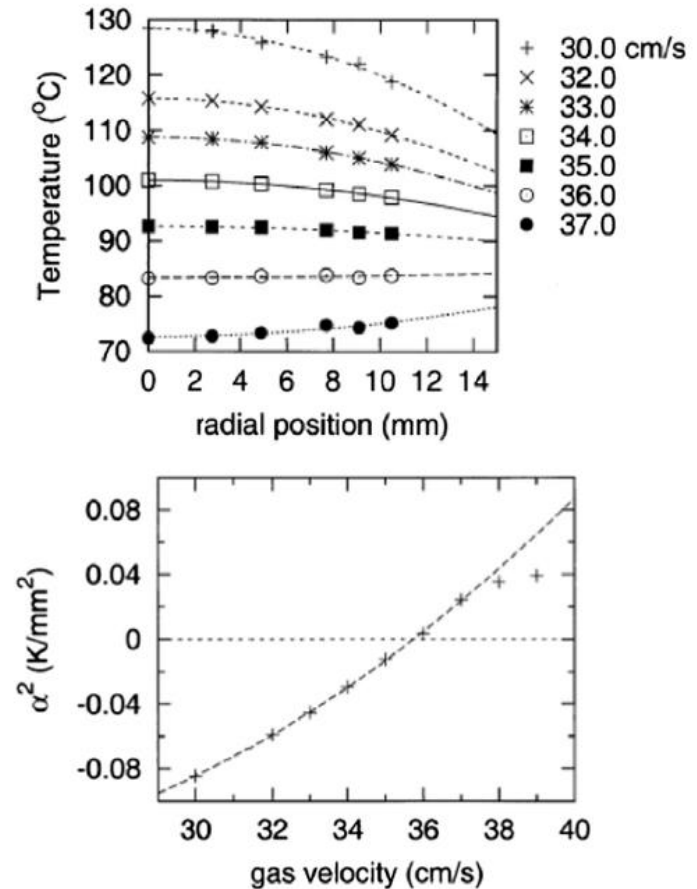
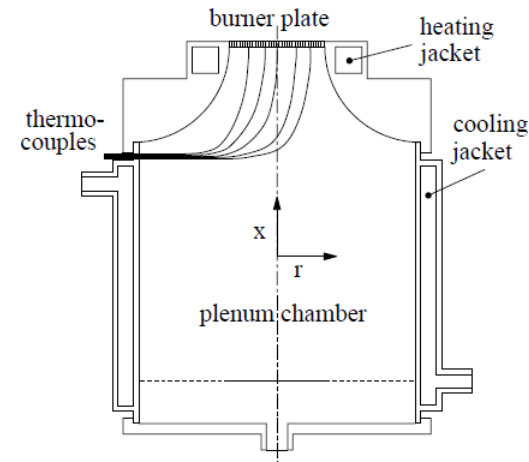


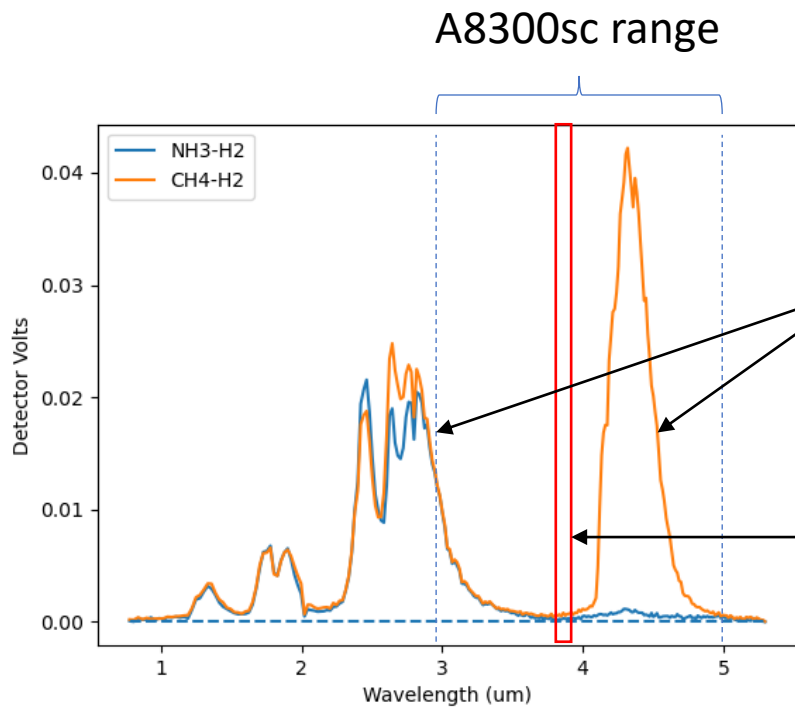
Figure from Bosschaart KJ, de Goey LPH. Detailed analysis of the heat flux method for measuring burning velocities. Combust Flame 2003;132:170e80.

- FLIR A8300SC IR camera
 - 3-5 μ m wavelength range
 - 50mm IR lens
- Can be calibrated via blackbody furnace for absolute measurements
- Nearly flat burner temperature profiles obtained without flame
- Minimal spatial emissivity effects
- Automated post-processing for perspective transform and corrections



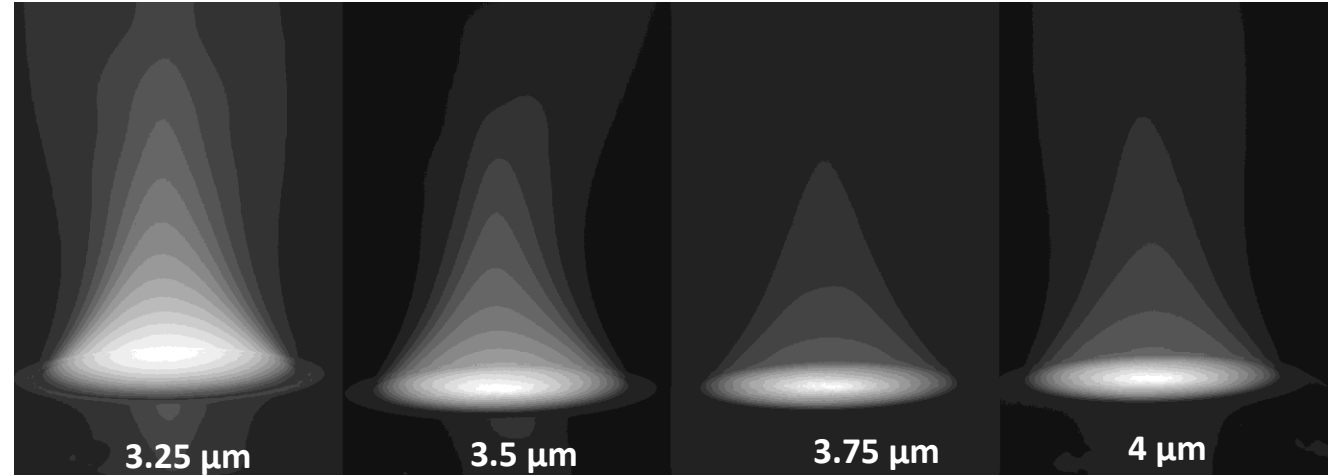
Flame Emission

- Flame emission is a major challenge
- Spectraline ES200 IR spectrometer used to determine optimal filtering strategies

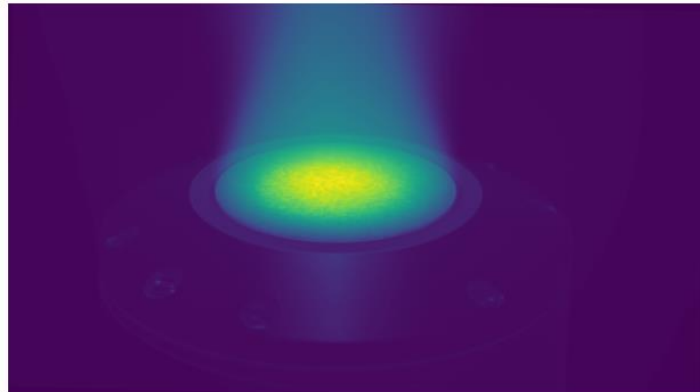


Must avoid wideband H2O and CO2 emission

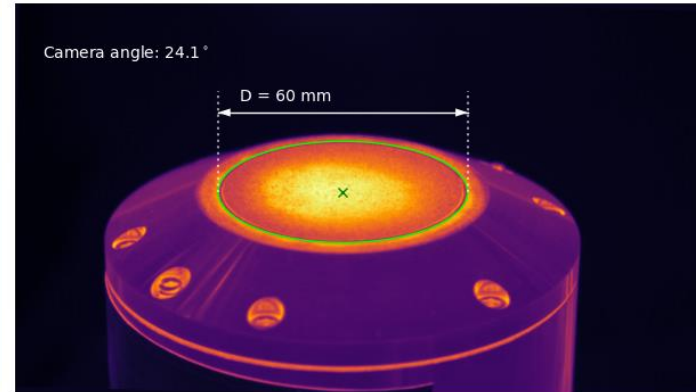
90nm FWHM filter selected at 3.9µm



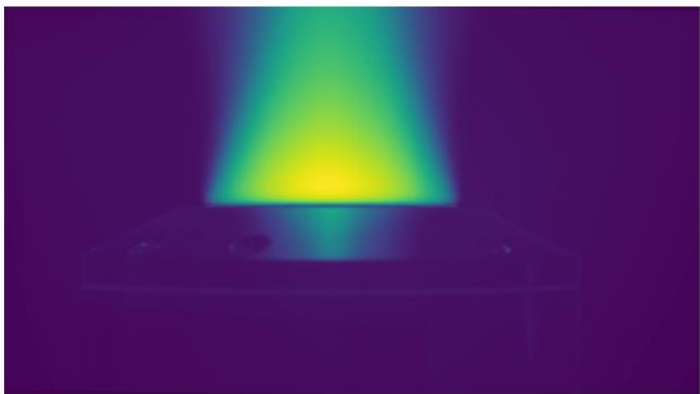
Off-the-shelf 500nm FWHM filters



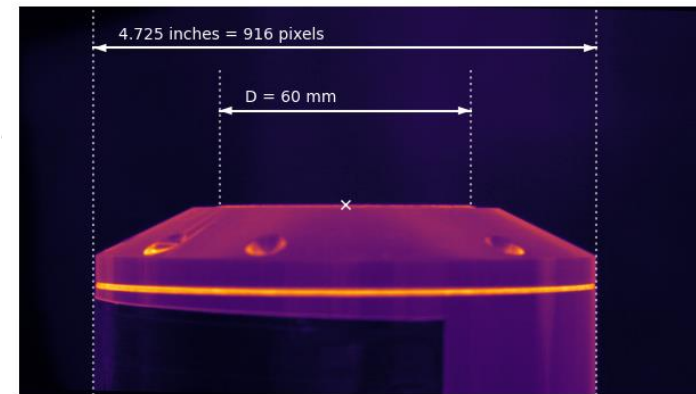
Oblique view: burner with emissions



Oblique view: burner only



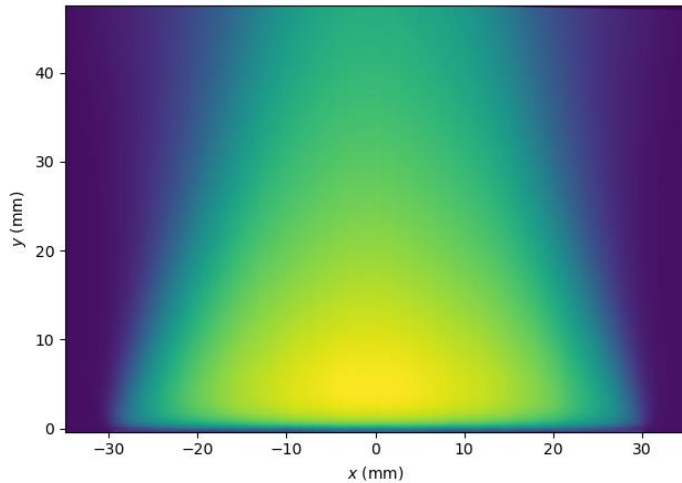
Side view: emissions only



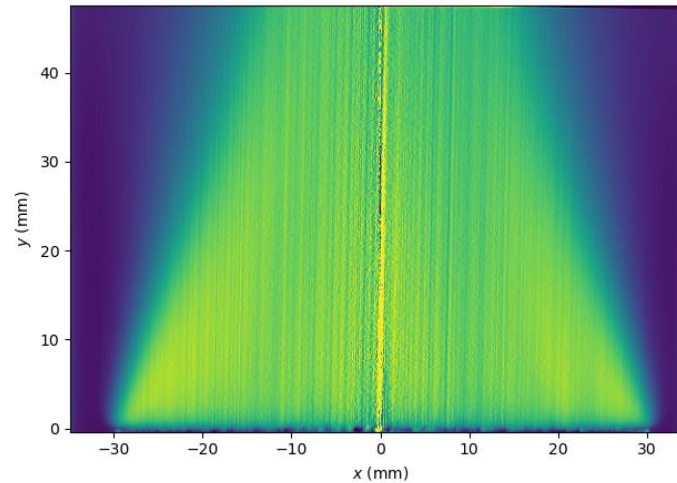
Side view: burner only

- Two orientations
 - Side view contains only emissions
 - Oblique view contains flame + burner emission
- Use side view to calculate line-of-sight emissions at any other camera angle
- Burner images for scaling, alignment, and calculation of camera angle

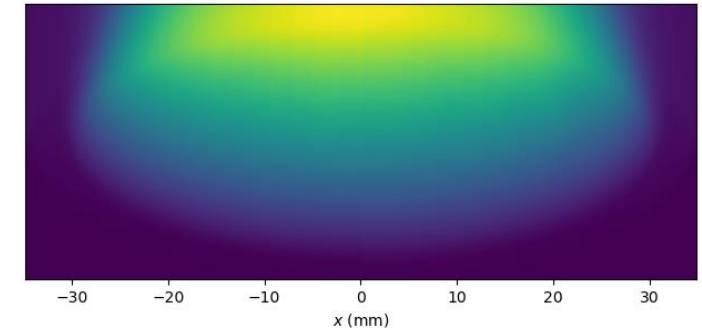
Image Post-Processing: Projected Flame Emissions



Mean side view emissions



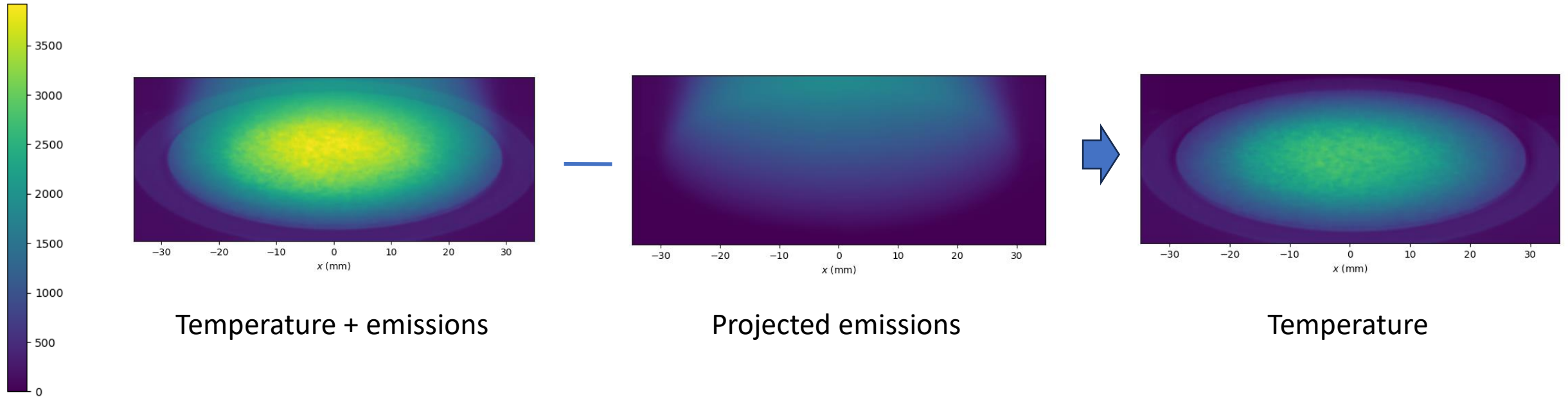
Inverse Abel transform



Projected emissions at required camera angle

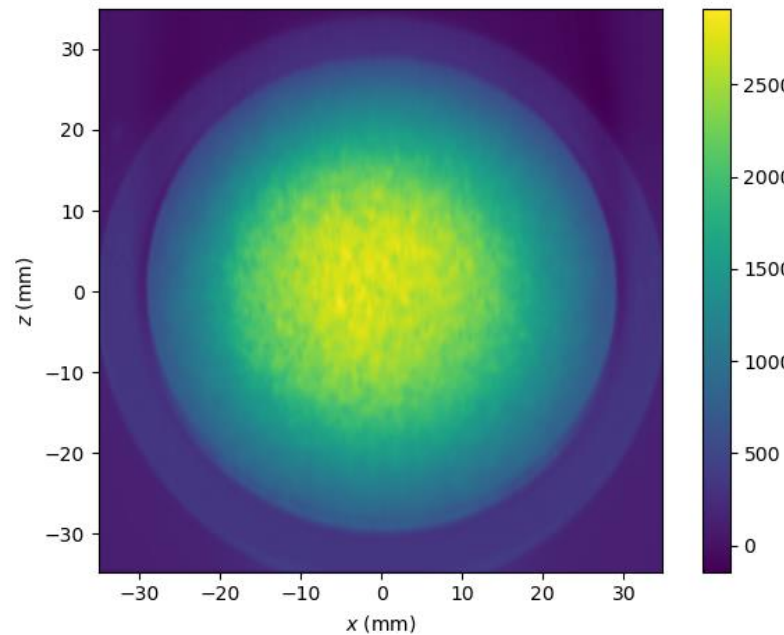
- An inverse Abel transform is applied to side-view emissions
- Abel transform used to create 3D flame emissions reconstruction
- Line-of-sight plane projection created from 3D emissions structure
- Verified at multiple angles
- Assumes negligible absorption effects

Image Post-Processing: Temperature Extraction

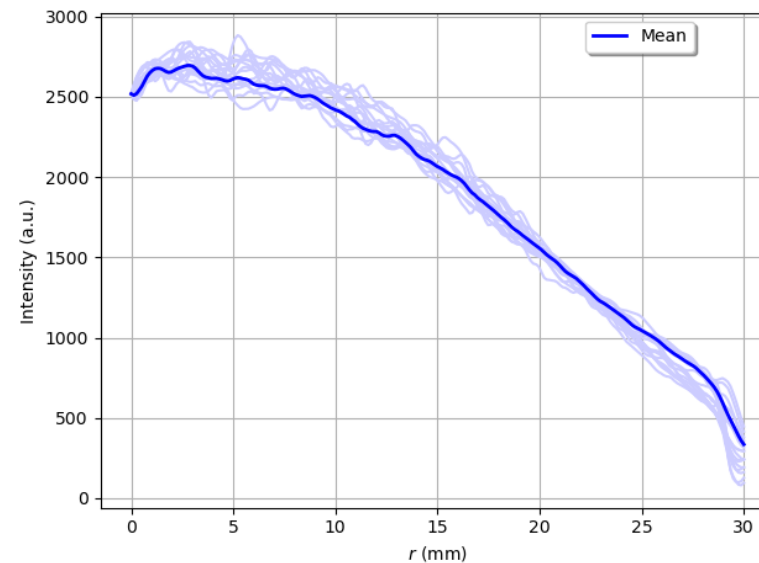


- Temperature + emissions from oblique view
- Projected emissions from side view
- Image subtraction results in temperature distribution (arbitrary units, future- absolute T calibration)

100% CH₄, $\Phi = 0.8$, $U = 22.1$ cm/s



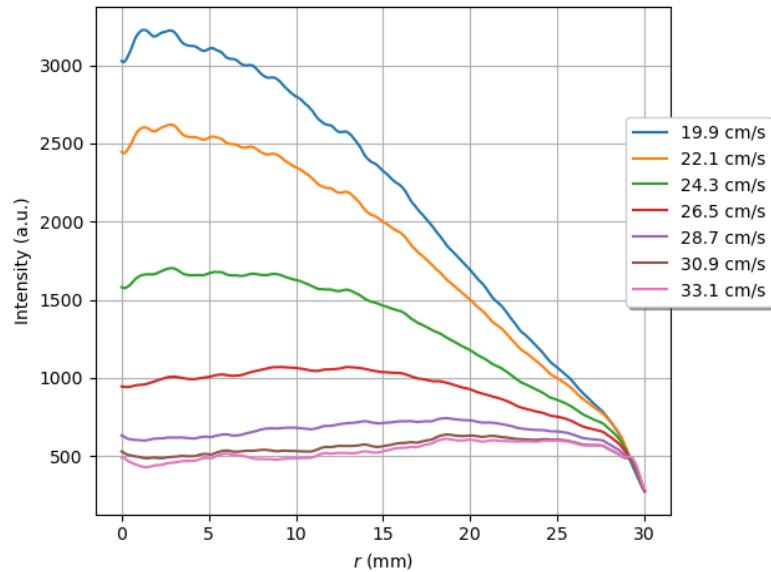
Transformed intensity (temperature)



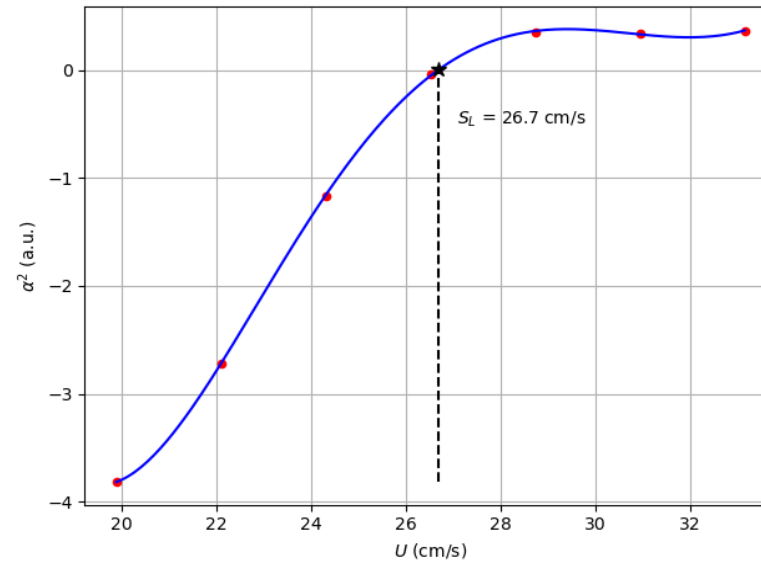
Radial intensity profiles

- Transformed intensity yields complete r - θ distribution
- Good top-bottom, left-right symmetry
- The mean of multiple profiles used for comparisons at different velocities

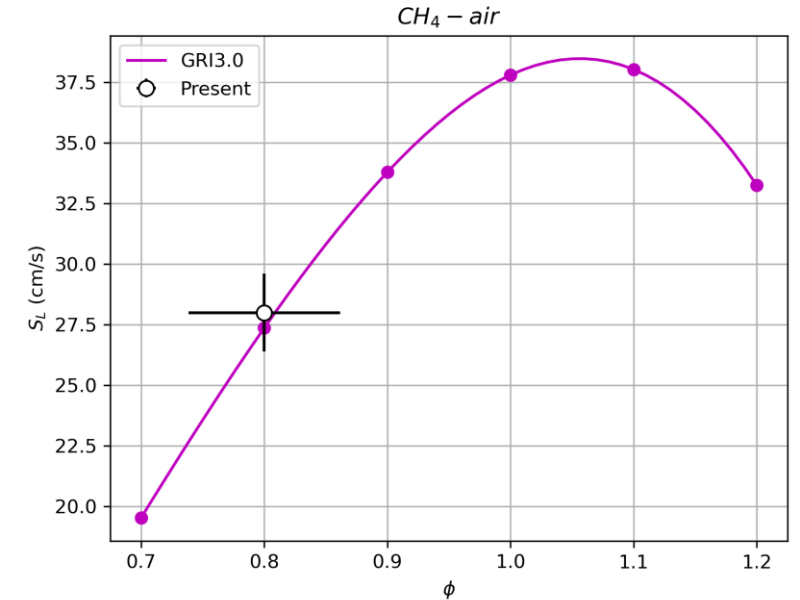
Image Post-Processing: 100% CH₄ Phi 0.8 Validation



Radial intensity profiles



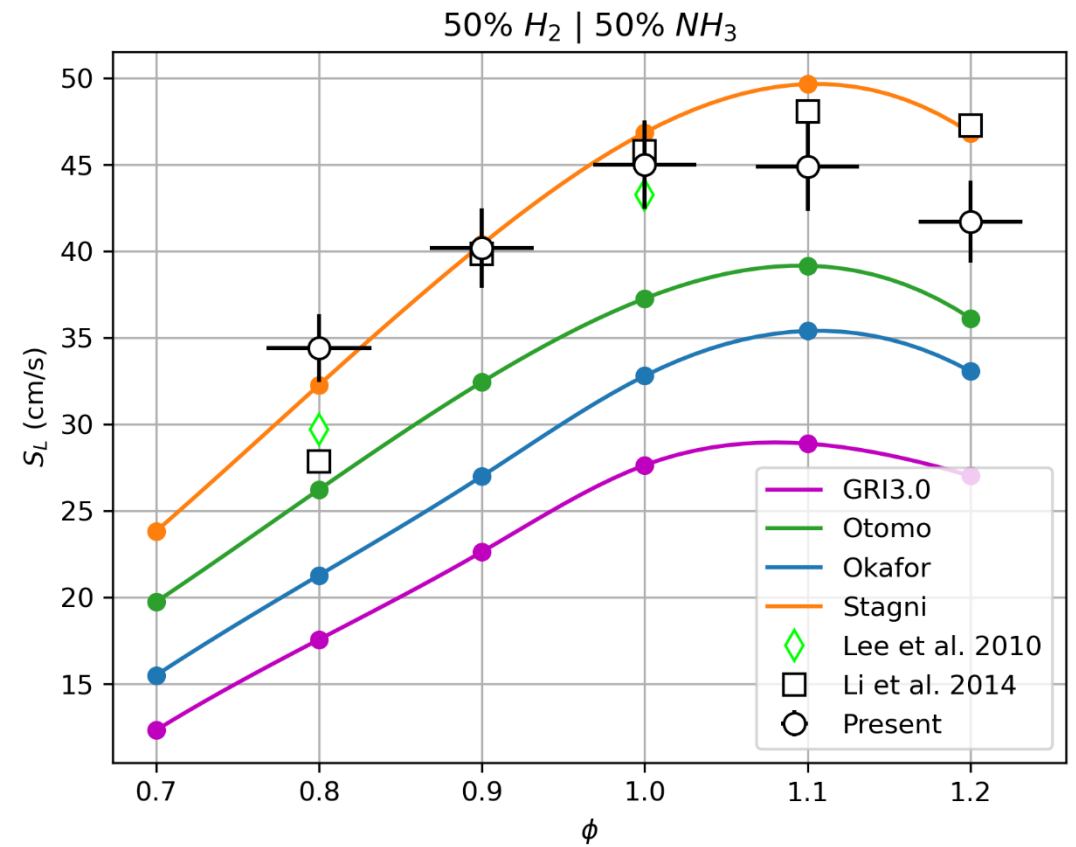
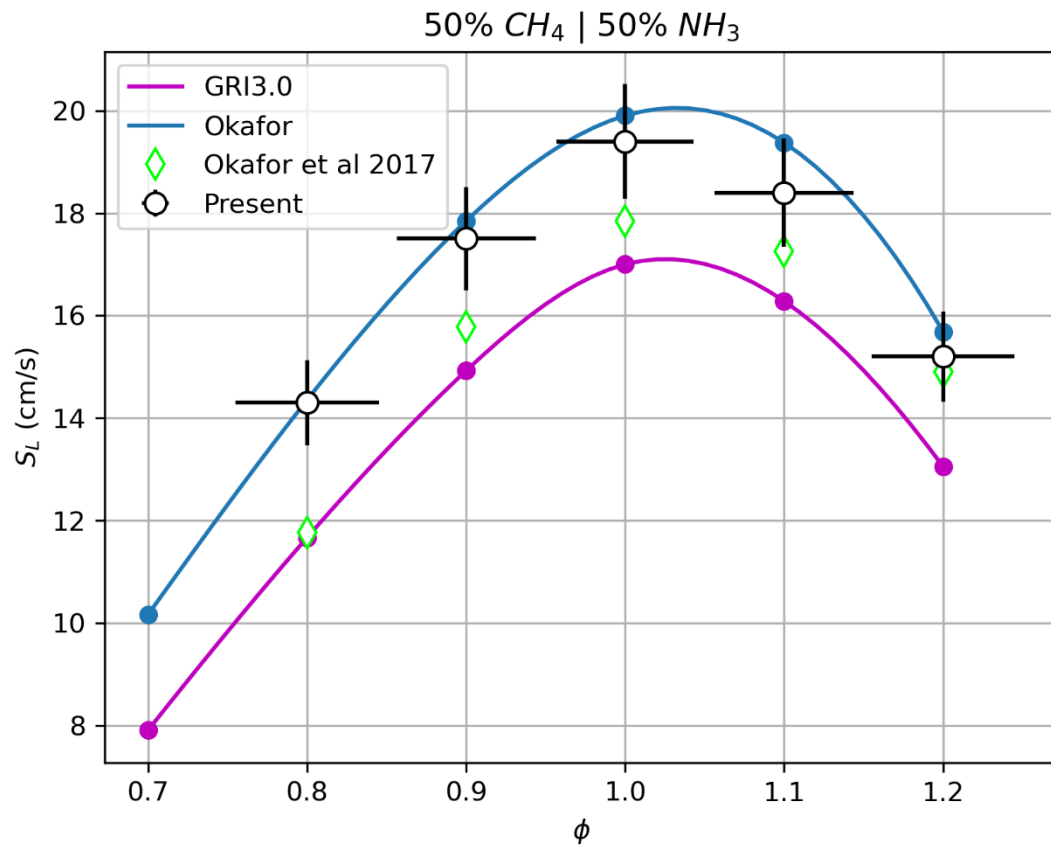
Flame speed interpolation



Validation

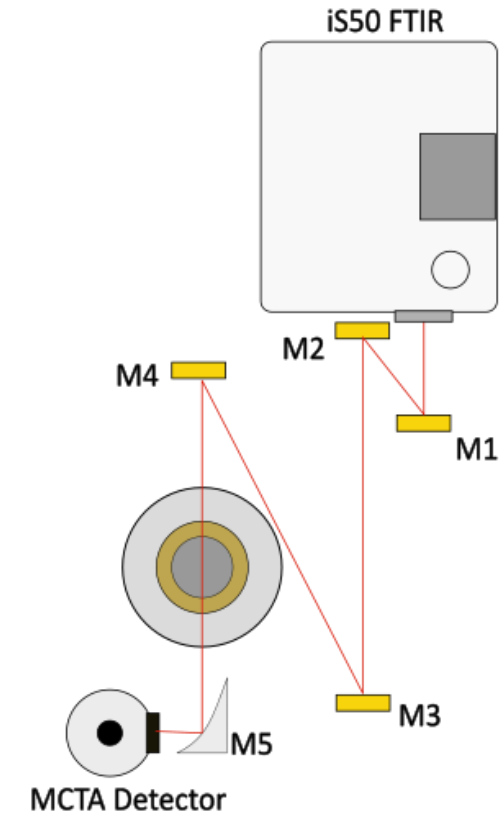
- Mean radial profiles generated for multiple velocities
- Profiles fit to $I = I_0 + \alpha^2 r^2$ for $r < 20$ mm
- $\alpha^2 = 0, U = S_L$
- Excellent agreement with prediction from GRI3.0 mechanism

Results: $\text{NH}_3\text{-H}_2$ and $\text{NH}_3\text{-CH}_4$ mixes



Diagnostic Approach for Species Concentrations

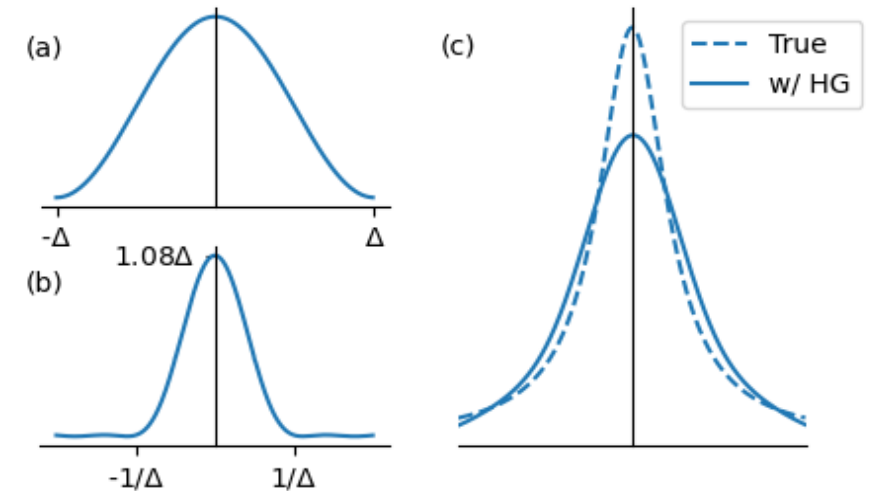
- Absorption spectroscopy used to measure post-flame species concentrations
 - Thermo-Fisher Nicolet iS50 FTIR spectrometer
 - External beam routing
 - LN₂-cooled MCTA detector
- Enables wide spectral range, good SNR – at the expense of some resolution
 - 0.125 cm⁻¹ resolution (0.015 cm⁻¹ data spacing)
 - Happ-Genzel apodization function considered during lineshape fitting
- All measurements made 12 mm from burner surface
- Beam size ~2-5 mm through flame



- Formulation follows past works in the literature
 - Beer-Lambert law
 - Voigt lineshape model w/ collisional/doppler broadening, pressure shift
 - HITEMP/HITRAN data
- Multi-spectral fitting routine via Python using Levenberg-Marquardt method
 - N-strongest lines considered
- Incorporates convolution of analytical Happ-Genzel apodization function, $a(\nu)$ ($\Delta=1/0.125\text{cm}^{-1}$)

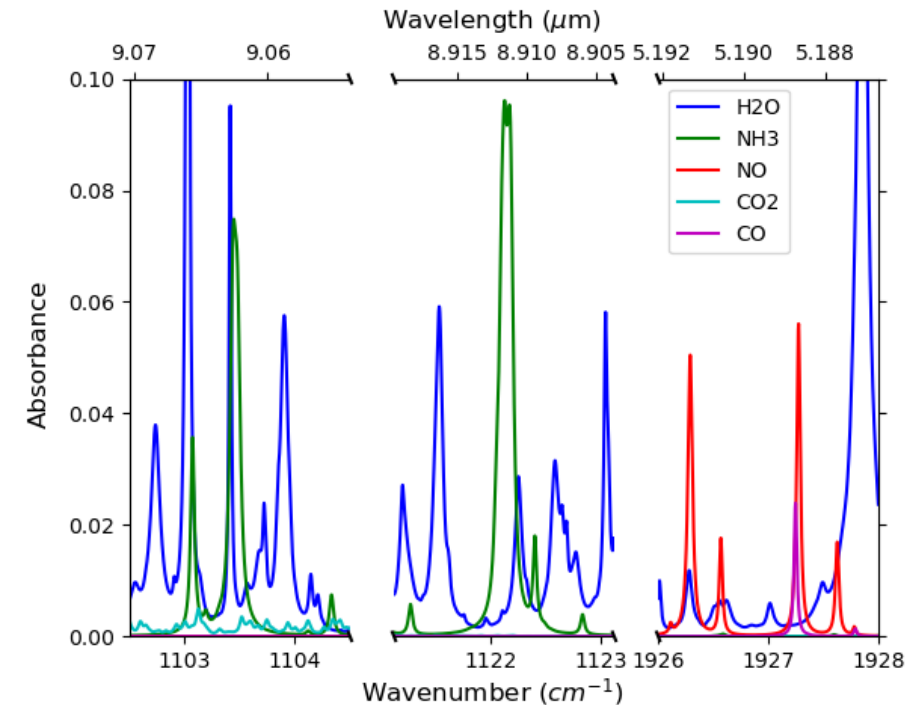
$$\left(\frac{I_t}{I_0}\right)_\nu = \exp[-S_j(T)\varphi_{\nu,j}(\nu, T, P)N_k l]$$

$$a(\nu) = \frac{0.54}{\pi\nu} + 0.46 \cdot \frac{4\pi\nu\Delta^2}{\pi^2 - (2\pi\nu\Delta)^2} \sin 2\pi\nu\Delta$$



Wavelength Selection

- Primary species of interest: NO and NH₃
- Overlapping H₂O a major challenge – but opportunity for H₂O thermometry
- Precedents in literature (most QCL/ICL laser-based):
 - NO – near 5.2 μm (ν₁ fundamental band), exhaust/flue gas applications, lineshape measurements, Hanson/Goldenstein/others
 - NH₃ – near 1.6 μm OR ~9-10 μm (ν₂ band), lineshape measurements, human breath, SCR applications, Farooq/Hanson/Peterson/others
 - H₂O – plenty of sources, ~2.5 μm from past thermometry experience



(2) Options for NH₃

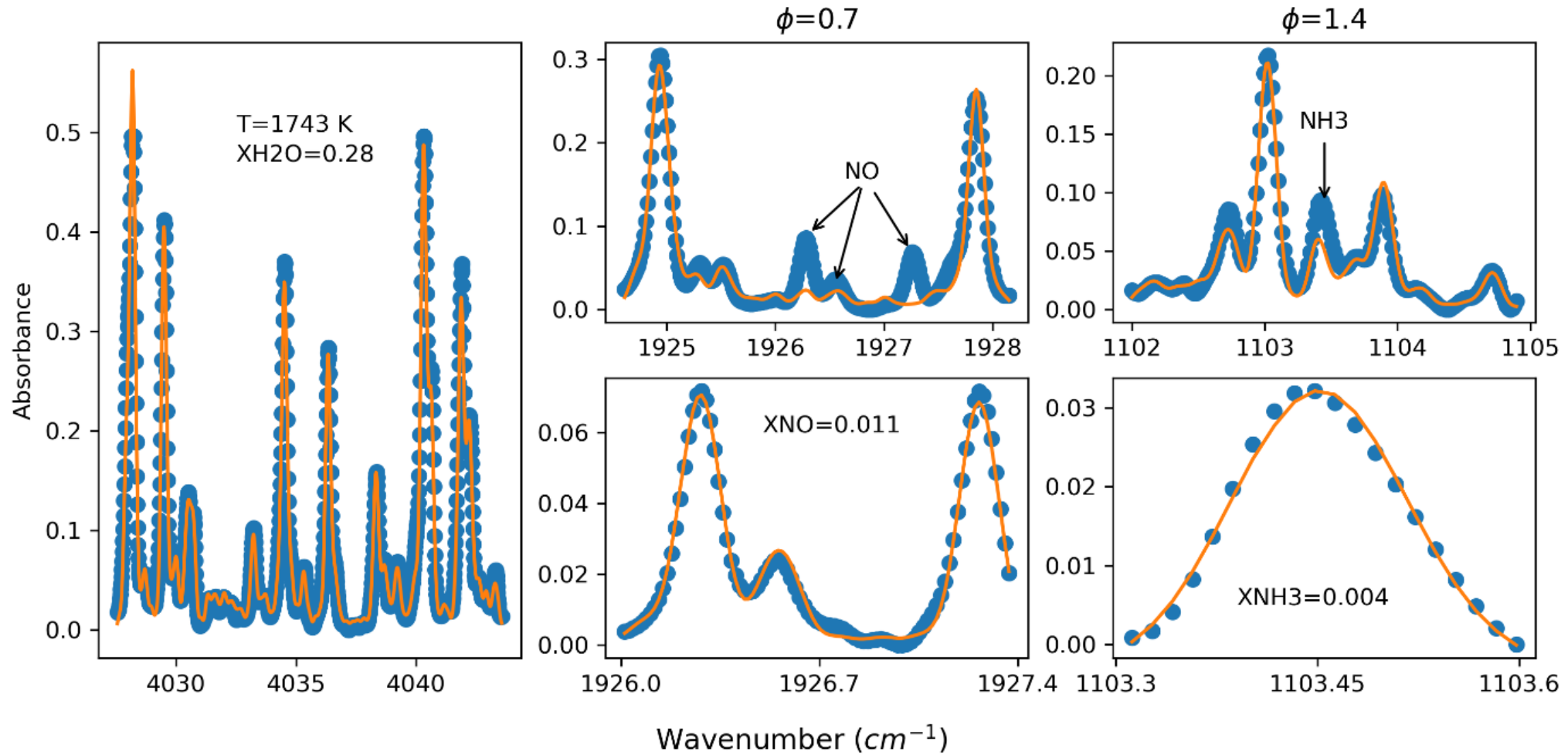
- ~1103 cm⁻¹
- ~1122 cm⁻¹

~1926-1927.5 cm⁻¹ for

- NO - (3) main features
- CO overlap near 1927.6 cm⁻¹

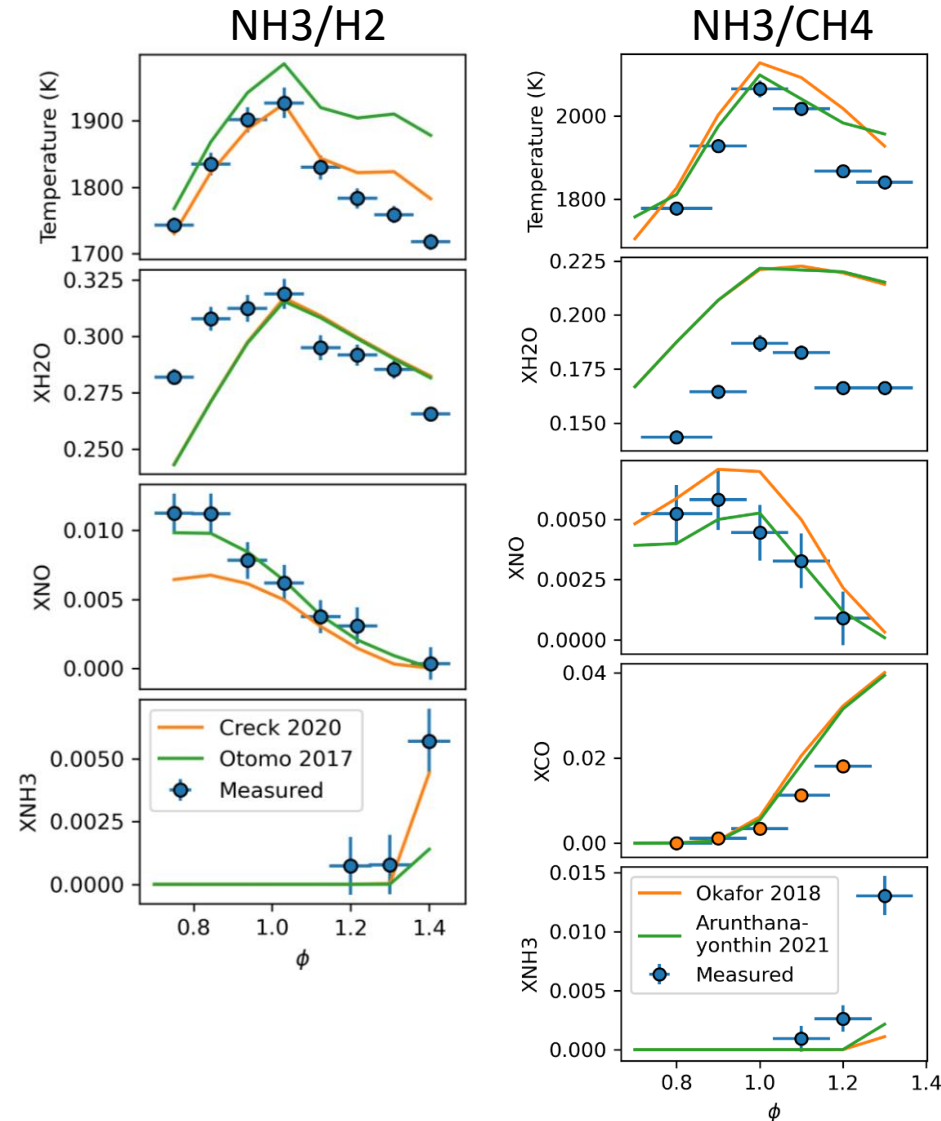
Example: Lineshape Fitting

50-50 NH₃-H₂



Results

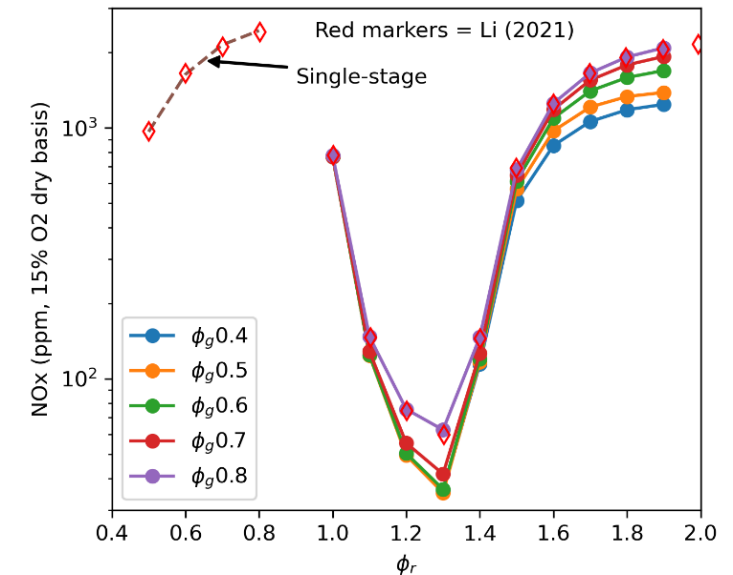
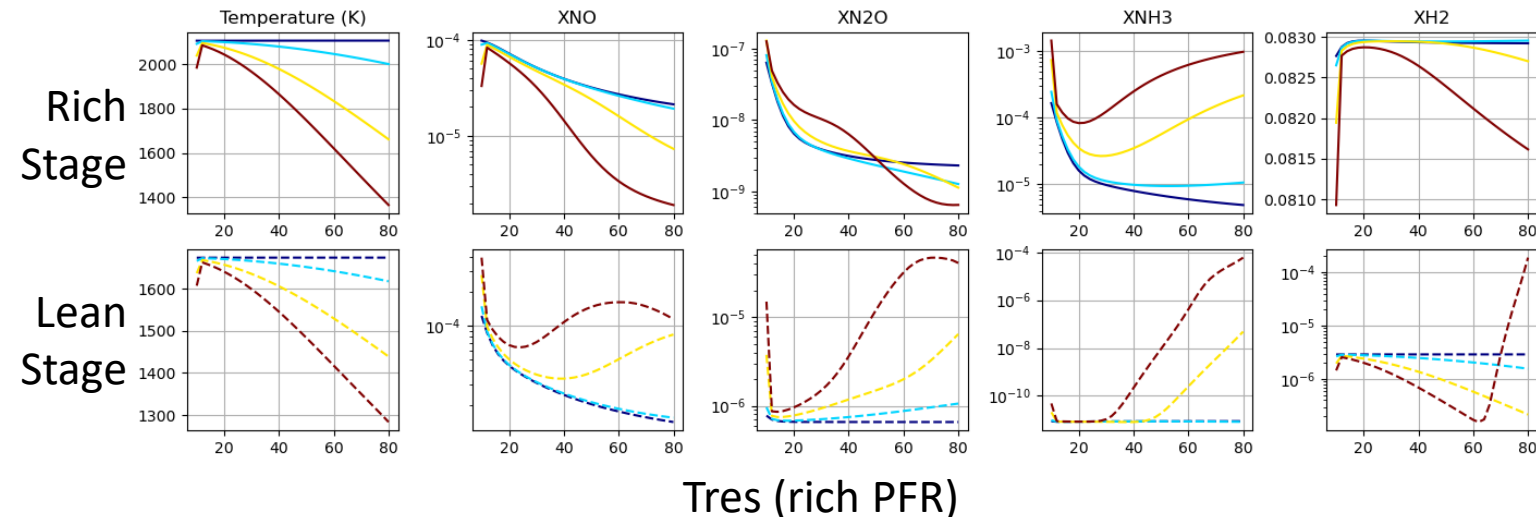
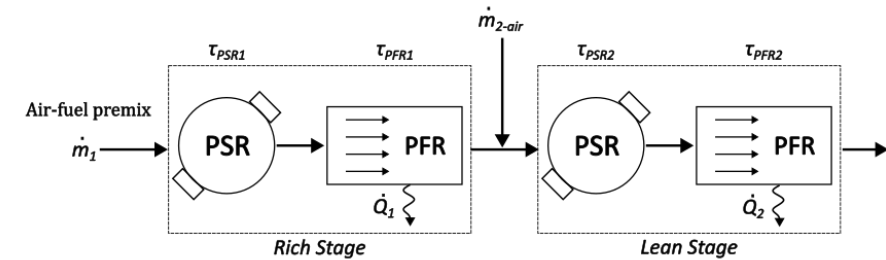
- Equivalence ratios swept from 0.7-1.4
- 25 C burner temperature
- Results compared to Cantera burner-stabilized flame simulations
 - Required due to heat-loss stabilized flames generated by McKenna burner
- Data only reported for $SNR > 5$



Y-error bars consider shot noise, fitting uncertainties, x-error bars consider MFC uncertainties (~10-20% total)

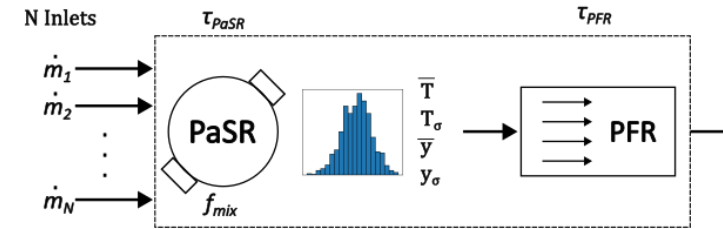
Chemical Reactor Network Modeling

- Custom CRN models developed in Python/Cantera
- Used to understand practical Rich-Quench-Lean (RQL) approaches
- Impacts of heat loss considered – important during rich relaxation phase



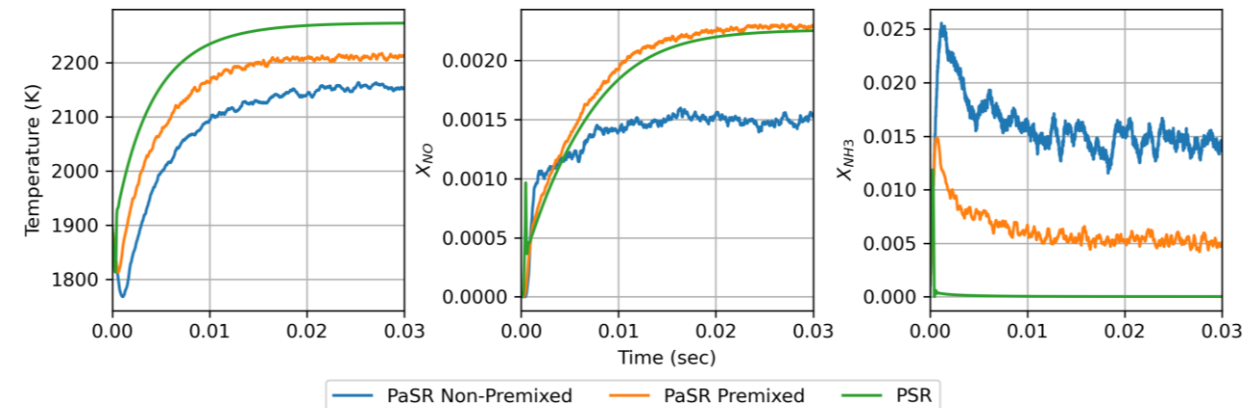
Chemical Reactor Network Modeling

- Models extended to consider impacts of mixing via Partially-Stirred-Reactor (PaSR) model
 - Reduce computational expense vs. Chemkin via use of pyjac and parallelization
- Allows consideration of non-premixed operation
- Primary interest – understanding impacts of mixing in lean burn phase

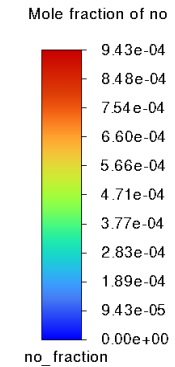
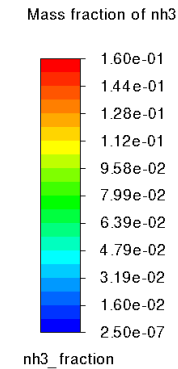
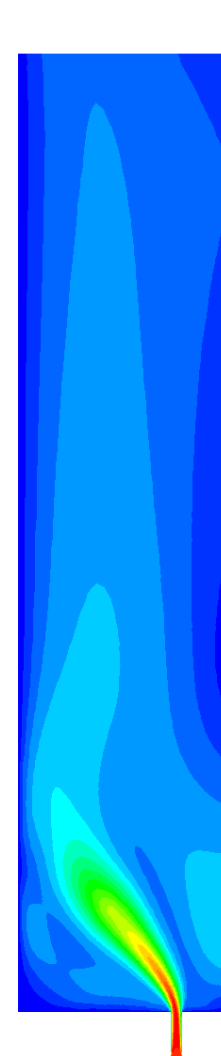
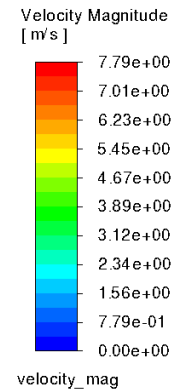


(top) Generic gas turbine combustor configuration with PaSR

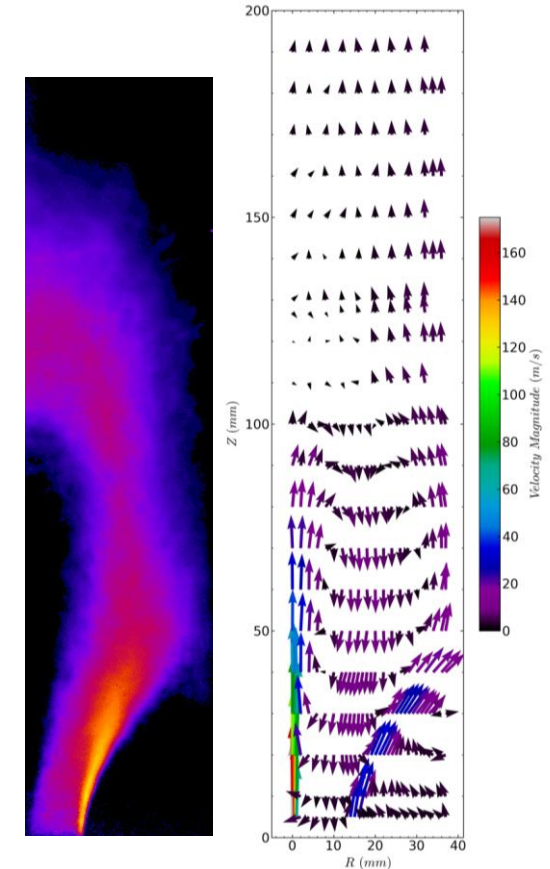
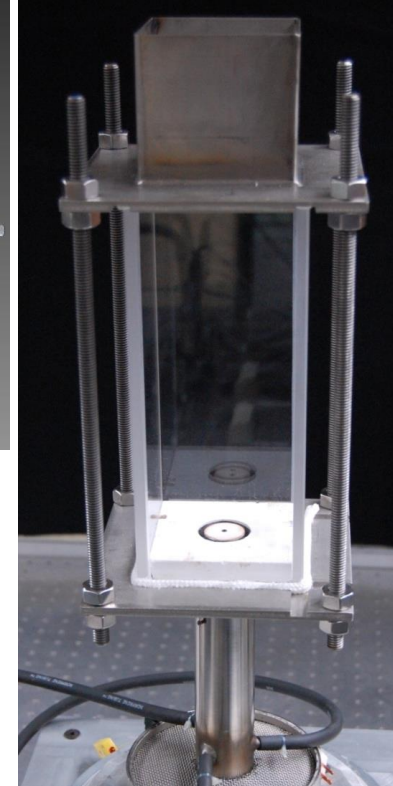
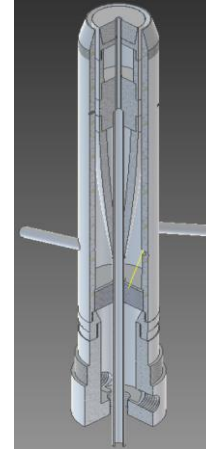
(bottom) Example temperature, NO, and NH₃ results for NH₃/air combustion using the PaSR model w/ intermediate mixing ($f_{mix}=1E4$ 1/s), for premixed and non-premixed operation, compared to perfectly-mixed (PSR) case; results illustrate higher unburnt NH₃ for finite mixing cases



- Engineering-level modeling of various burner configurations
 - Inform burner and RQL designs for upcoming applied studies
- OpenFOAM and Fluent
- Collaboration with Argonne National Lab for additional modeling support

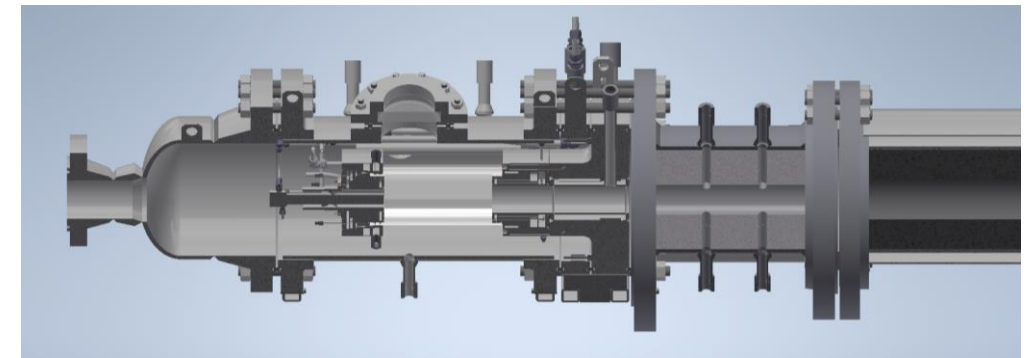


- Leverage existing burner platform to study swirl-stabilized NH₃ flames
 - Premixed operation
- Repeat prior measurements done for CH₄ and H₂
 - Stability mapping
 - Global emissions (FTIR) - NO/NO₂/N₂O/NH₃/H₂O
 - PLIF/PIV/LDV
 - Thermal BCs
- Modify burner for RQL operation (in progress)
 - Baseline secondary air ring



High Pressure Developments

- Adding H₂ & NH₃ capabilities to existing NETL PPC rig (1MWth, 10 atm)
- Development of high T&P storage/delivery system underway
 - 150 lb liquid-draw anhydrous cylinder
 - Piston-pump accumulators
 - Off-the-shelf electric vaporizer (~80kW)
- Will provide ~30 min run time at full power
- Combustor mods for RQL
 - NG (current) and NH₃ (when available)



NETL RESOURCES

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