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# **Project Team**

| Team Member            | Organization | Title                            | Task Contribution/Role             |
|------------------------|--------------|----------------------------------|------------------------------------|
| Heather Dougherty, PhD | DOE/NETL     | DOE Project Manager              | Project Management                 |
| Seyed Dastgheib, PhD   | UIUC/ISGS    | Principal Research Scientist     | Tasks 1-5 (Principal Investigator) |
| Paul Braun, PhD        | UIUC/MRL     | Professor and MRL Director       | Task 4 (Task leader)               |
| Darshan Sachde, PhD    | Trimeric     | Senior Process Engineer          | Task 5 (Task leader)               |
| Sohan Singh, PhD       | UIUC/ISGS    | Postdoctoral Research Associate  | Tasks 2-3                          |
| Rajen Basu, PhD        | UIUC/MRL     | Research Scientist               | Task 4                             |
| Fu Wu                  | UIUC/MRL     | Graduate Research Assistant      | Task 4                             |
| Shuchi Sanandiya       | UIUC/ISGS    | Research Assistant               | Tasks 2-3                          |
| Savanna Scheffel       | UIUC/ISGS    | Undergraduate Research Assistant | Task 2-3                           |

**Organizations** DOE/NETL: Department of Energy/National Energy Technology Laboratory UIUC: University Illinois Urbana-Champaign ISGS: Illinois State Geological Survey MRL: Materials Research Laboratory at UIUC

# **Supercapacitors**

- Supercapacitors are energy storage devices that bridge the gap between rechargeable batteries and capacitors.
- The energy storage capacity of SCs is much lower than that of batteries, but SCs can charge and discharge at a much faster rate, even at low temperatures.
- Batteries combined with SCs have currently been proposed as ideal energy storage devices.
- SCs include electric double layer capacitors (EDLC), pseudo capacitors, and hybrid capacitors.



# **Electrochemical Double Layer Capacitors**

- Porous carbon-based materials (i.e., activated carbons (AC)) and carbon nanomaterials are used to fabricate EDLC electrodes.
- Opposite charge (ion) accumulation occurs on the polarized electrode surface with the applied voltage.
- □ AC provides a high surface area for charge accumulation and energy storage in EDLC supercapacitors. There is no chemical reaction.
- A high surface area, suitable surface chemistry, and other factors contribute to the high performance of carbon-based EDLC supercapacitors.



lons accumulated on the surface in the carbon pores filled with the electrolyte



## Fabrication of SC Electrodes from Carbon Materials

- □ High-grade coconut shell-based ACs are the predominant materials used by SC manufacturers. A conducting carbon additive (e.g., carbon black) is also needed for enhancing the conductivity.
- The AC powder is mixed with a binding material and other additives (e.g., carbon black for enhancing conductivity) and coated as a thin film on a conductive substrate to form the electrode. Electrodes are stacked by placing insulating plastic sheets between them.



## Current Price and Market Size of SC-Grade AC

- Reported wholesale price for a SC-grade coconut shell based YP-50F product manufactured by Japanese company Kuraray is ~\$30/kg.
- □ The current market size for SCs is estimated to be between \$500 million and \$9 billion with a CAGR between 13% and 28% from 2022-2027.



# Research Gaps in Coal-to-SC Materials R&D

| Current main gaps in coal-to-SC R&D  | Proposed approach to advance the SOTA   |  |  |  |
|--|---|--|--|--|
| 1. Absence of any comprehensive systematic study on the development of SC materials from different types of coal.  | <ul> <li>Four types of coal (lignite, subbituminous,<br/>bituminous, and anthracite) will be systematically<br/>processed.</li> </ul>   |  |  |  |
| 2. Lack of knowledge on the fate of coal impurities (metals, sulfur, halides, etc.) in the production process of SC materials from coal and their impact on the performance of SCs.                                      | <ul> <li>A deep deashing is included in the process to<br/>prepare an ultraclean coal precursor. Fate of<br/>impurities in main streams, products, and waste<br/>streams will be determined by extensive<br/>characterization of the samples.</li> </ul>            |  |  |  |
| <ol> <li>Absence of any work on co-production of both porous (i.e., AC) and graphitic/conductive SC materials (e.g., carbon nanotubes or nanofibers) from coal and their use in fabrication of SC electrodes.</li> </ol> | <ul> <li>Coal-based graphitic or conductive materials will<br/>be prepared from coal volatile matter, in addition<br/>to the production of porous carbons from coal<br/>chars. SC electrodes will be prepared from coal-<br/>based materials and tested.</li> </ul> |  |  |  |

# Research Gaps in Coal-to-SC Materials R&D

| Current main gaps in coal-to-SC R&D  | Proposed approach to advance the SOTA   |  |  |
|--|---|--|--|
| 4. Lack of a systematic approach for characterizing coal-based AC materials and assessing their performance for SC applications through <u>comparison</u> with a baseline commercial SC carbon.                                      | <ul> <li>Both physicochemical characteristics and<br/>electrochemical properties of the developed materials<br/>and a baseline commercial SC-grade AC will be<br/>extensively evaluated and compared side-by-side.</li> </ul> |  |  |
| 5. Lack of information on the long-term performance<br>of coal-based SC materials for more than 100,000<br>testing cycles. This information is needed to<br>evaluate potential commercial application of the<br>developed materials. | <ul> <li>To demonstrate the long-term performance of the<br/>developed materials, the best-performing material will<br/>be tested up to 100,000 cycles.</li> </ul>  |  |  |
| 6. Lack of a technoeconomic analysis on the development of coal-based SC materials.  | <ul> <li>A technoeconomic evaluation and cost estimation<br/>including cost estimation for a plant processing 20 tons<br/>of coal per day will be performed.</li> </ul>   |  |  |

## Project objective, Approach, and Goals

#### □ Objective – To develop high-value SC materials from domestic coal in a cost-effective manner

#### Approach

- Coal preparation Systematically prepare lignite, subbituminous, bituminous, and anthracite coals by deashing and devolatilization treatments
- Development of highly porous functionalized materials Prepare materials with surface areas exceeding the surface area of SC-grade activated carbons with suitable surface chemistry for SC application
- Development of graphitic or conductive materials Prepare materials to be used as the conductivity enhancer additives in fabrication of SC electrodes
- Physicochemical characterization Perform an extensive physicochemical characterization
- Fabrication and testing of SC electrodes Fabricate and test SC electrodes from a baseline commercial material and from the developed coal-based materials, perform side-by-side evaluation and comparison
- Technoeconomic evaluation Perform process simulation, cost estimation, and technology gap assessment

#### Performance and cost goals

Develop cost-effective approaches to produce coal-based materials with a higher capacitance than the capacitance of the baseline state-of-the-art commercial SC carbon material tested under identical conditions. The cost of the coal-based materials should be less than the cost of the commercial material.

## Coal Selection, Preparation, and Characterization

□ Four coal samples (lignite, subbituminous, bituminous, and anthracite) are selected, prepared, and characterized



| Sources of anthracite, bituminous, subbituminous, and lignite coal samples obtained from different U.S. coal |
|--|
| mines are shown on the USGS coal resources map.  |

|                                    | Anthracite | Bituminous | Subbituminous | Lignite |  |  |
|------------------------------------|------------|------------|---------------|---------|--|--|
| Proximate Analysis (%) - Dry Basis |            |            |               |         |  |  |
| Ash                                | 9.5        | 10.5       | 6.1           | 10.3    |  |  |
| Volatile                           | 5.0        | 42.0       | 43.2          | 46.3    |  |  |
| Fixed Carbon                       | 85.5       | 47.5       | 50.7          | 43.3    |  |  |
| Heating Value - Dry Basis          |            |            |               |         |  |  |
| BTU/lb                             | 13,300     | 12,740     | 12,115        | 11,013  |  |  |
| Ultimate Analysis (%) - Dry        | Basis      |            |               |         |  |  |
| Carbon                             | 84.65      | 70.50      | 71.20         | 68.42   |  |  |
| Hydrogen                           | 2.00       | 5.00       | 4.90          | 4.49    |  |  |
| Nitrogen                           | 0.70       | 1.40       | 1.00          | 1.04    |  |  |
| Sulfur                             | 0.55       | 3.26       | 0.29          | 1.42    |  |  |
| Ash                                | 9.50       | 10.50      | 6.10          | 10.34   |  |  |
| Oxygen                             | 1.70       | 9.30       | 16.60         | 14.28   |  |  |
| Chlorine                           | NA         | 0.08       | < 0.01        | < 0.01  |  |  |



# Coal Deashing by Molten NaOH Method

- Coal samples were deashed using the molten alkali method
- Cumulative removal of <u>Ca+Mg+Fe</u>: 95%-100%, Sulfur removal: 65% to 100%, Ash removal: 86-96%
- Deashing approach was highly effective for removal of iron and other transition metals that might have negative impact on the performance of prepared materials for SC application
- For majority of the samples iron is removed to below the detection limit, cumulative concentration of other transition metals in deashed coals is < 100 ppm</p>

| Analyte Symbol        | Ве  | В   | Mg   | Са   | Mn  | Fe   | Ni   | Cu   | Zn   |
|-----------------------|-----|-----|------|------|-----|------|------|------|------|
| Unit Symbol           | ppm | ppm | %    | %    | ppm | %    | ppm  | ppm  | ppm  |
| Anthracite coal       | 0.3 | 2   | 0.02 | 0.03 | 28  | 0.27 | 5.6  | 36.9 | 11.1 |
| Bituminous coal       | 0.8 | 195 | 0.02 | 0.38 | 30  | 0.28 | 13.2 | 11.1 | 85   |
| Subbituminous coal    | 0.2 | 30  | 0.19 | 0.97 | 6   | 0.1  | 2.4  | 10.2 | 6    |
| Lignite coal          | 0.5 | 130 | 0.32 | 1.36 | 56  | 0.29 | 4.4  | 6.7  | 7.1  |
| Deashed anthracite    | 0   | 2   | 0    | 0    | 0   | 0    | 2.2  | 10   | 0.5  |
| Deashed bituminous    | 0.2 | 67  | 0    | 0    | 3   | 0    | 7.5  | 14.1 | 73   |
| Deashed subbituminous | 0   | 44  | 0    | 0.02 | 0   | 0    | 4    | 17.7 | 1.3  |
| Deashed lignite       | 0   | 43  | 0    | 0    | 3   | 0.03 | 7.2  | 21.8 | 1.1  |

|               | S %<br>(As-received) | S% (Deashed) |  |
|---------------|----------------------|--------------|--|
| Anthracite    | 0.55                 | 0.195        |  |
| Bituminous    | 3.26                 | 0.851        |  |
| Subbituminous | 0.29                 | < 0.001      |  |
| Lignite       | 1.42                 | < 0.001      |  |

# **Coal Devolatilization**

- TGA profiles of as-received coal samples showed a weight loss of ~ 7-45% (dry-basis) when samples heated to 1000 °C (due to removal of volatiles and decomposition of surface functionalities)
- Several heat and hold sections in the temperature range of 400-600 °C are included to characterize the release of coal volatiles that occur mainly in this temperature range
- $\blacktriangleright$  As-received or deashed coal samples were devolatilized by pyrolysis under N<sub>2</sub> at 1000 °C
- Literature suggests that methane is the dominant hydrocarbon in the gas generated from coal devolatilization at 1000 °C [Felder and Gilman, 1984]



Yield of tar and gases from pyrolysis of two coals (Figure 2 of EPA-600/S7-84-082 Sept. 1984 report by Felder and Gilman).

# Preparation of Fibrous or Graphitic Carbon from Coal Volatiles

a)

Tubular

Furnace

- The catalyst substrate is initially oxidized, then reduced to activate the catalytic sites for carbon deposition and growth.
- After the catalyst preparation stage, coal is added continuously at a constant rate to generate the volatile matter as the hydrocarbon source for carbon deposition on the catalyst substrates that are preheated to a desired temperature.
- Nickel substrates showed the best catalytic performance.
- Baseline experiments were also conducted using methane as the hydrocarbon source.









### Characterization of Fibrous or Graphitic Carbon Prepared from Coal Volatiles or Methane

- Samples prepared from coal volatiles were compared with the baseline samples prepared from methane under the same conditions.  $\geq$
- SEM shows fibrous or connected bead type structures that are formed depending on the synthesis conditions.  $\geq$
- Raman spectra of coal-based samples showed D and G bands at the same frequencies as those of the methane-based samples. Compared to >methane-based samples, coal-based samples had more defects as indicated by their larger D bands, but they showed similar G bands.
- Majority of coal-based samples and samples prepared from methane pyrolysis also exhibited 2D bands, similar to those observed for multiwall >carbon nanotubes or other graphitic materials.
- XRD profiles of coal-based samples showed sharp 26° peaks, similar to those of the methane-based samples. >







Prepared using

the volatiles from

a subbituminous

2500

2D band

(2690 cm<sup>-1</sup>)

2500

3000

3000

2D band

(2691 cm<sup>-1</sup>)

coal

## Preparation of Coal-Based Porous Activated Carbons

- Work is in progress to prepare highly porous activated carbon from as-received, deashed, and deashed-devolatilized coal chars
- Different activation methods are used
- Porous carbons are functionalized with oxygen or nitrogen functionalities, or impregnated with nanoparticles
- Physicochemical characteristics of the prepared coal-based materials are compared with those of a commercial SC-grade AC

Developed materials have a porous honeycomb structure with surface areas of ~1400-1900 m²/g, exceeding the surface area of the commercial SC-grade activated carbon

|                        | BET surface area (m²/g) | Total pore volume (cm³/g) | DR Micropore volume (cm <sup>3</sup> /g) | Meso + Macropore volume (cm³/g) |
|------------------------|-------------------------|---------------------------|--|---------------------------------|
| Commercial SC-grade AC | 1717                    | 0.801                     | 0.702                                    | 0.099                           |
| Coal-based AC_A        | 1419                    | 0.615                     | 0.561                                    | 0.054                           |
| Coal-based AC_B        | 1833                    | 0.863                     | 0.720                                    | 0.143                           |
| Coal-based AC_SB       | 1911                    | 1.077                     | 0.754                                    | 0.323                           |
| Coal-based AC_L        | 1890                    | 0.933                     | 0.743                                    | 0.190                           |





Slurry Preparation: AC (80-90%) + carbon black (2-10%) + additive (5-10%) + solvent (water or organic solvents)



- The optimal conditions of supercapacitor slurry formulation, substrate preparation, film quality including coated film thickness and mass loading were determined.
- Reproducibility within the slurry preparation and coating fabrication processes, and electrochemical testing procedure was demonstrated.



Fabrication of supercapacitor electrodes: a) Slurry-cast carbon film on a Ni substrate, b) Fabricated electrode (cut from the coated substrate) immersed in  $1M Na_2SO_4$  electrolyte, c) Schematic of a fabricated 1 cm X 3 cm electrode showing coated and uncoated sections.

Baseline Testing of Electrodes Prepared from a Commercial SC-Grade AC

- Cyclic voltammetry tests using a 3-electrode system were conducted to test SC electrodes as the working electrode, platinum coated on titanium mesh as the counter electrode, and Ag/AgCl as the reference electrode.
- Reproducibility of results for a baseline commercial SC-grade AC was demonstrated, by testing multiple electrodes fabricated from different batches and by testing selected electrodes for more than 500 cycles.
- > After 500 cycles, the electrode's capacitance was 97.15% of its original capacitance.





#### Capacitance Comparison: Commercial Material vs. a Coal-Based Sample

- Commercial SC-grade AC sample: AC mass: 0.0054 g; Film thickness: 70 μm; Capacitance = 54.27 F/g
- Coal-based sample prepared in this work: AC mass: 0.0060 g; Film thickness: 75 μm; Capacitance = 117.27 F/g



- Complete the work for preparation and characterization of more than 30 functionalized porous carbon materials
- Prepare additional graphitic or conductive carbon additives
- □ Fabricate SC electrodes from the developed materials and perform screening tests
- Select the best-performing materials and perform more rigorous testing (using different types of electrodes, longer testing periods, and up to 100,000 cycles test)
- □ Identify the best performing material based on the energy storage performance
- Perform the technoeconomic analysis and technology gap assessment
- Perform cost estimation for a plant processing 20 tons of coal/day

## Summary and Conclusions

- Experimental work performed included coal preparation, removal of coal impurities, coal devolatilization, preparation of porous and fibrous/graphitic SC materials, and an extensive physicochemical characterization.
- ❑ Developed coal-based materials have a porous honeycomb structure with surface areas of ~1400-1900 m<sup>2</sup>/g, exceeding the surface area of a commercial SC-grade AC.
- SC electrodes were fabricated from a baseline SC-grade AC and from the developed materials. Baseline and lab-prepared electrodes were tested side by side under the same conditions.
- □ Capacitance of the coal-based electrodes were more than twice the capacitance of the electrodes fabricated from a commercial baseline material.
- Project next steps include preparation and testing of additional SC materials from different types of coal and technoeconomic analysis.

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