



Integrated Capture and Conversion of CO₂ into Materials (IC³M):

Pathways for Producing CO₂-Negative Building Composites (FWP 78606)

&

Expanding IC³M for C1 and C2 Production (FWP-80562)

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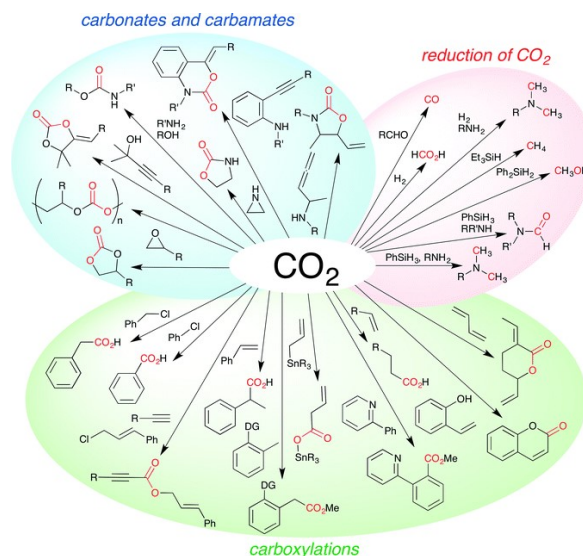
PNNL is operated by Battelle for the U.S. Department of Energy



Brickett et al, Chem. Sci., 2022,13, 6445-6456

Integrated Capture and Conversion of CO₂ into Materials (IC³M); A Multi-Product Platform for CCUS

Goal: To design CO₂ capture units that concurrently produce materials from CO₂.



FWP-80562

Near term targets

carbon-neutral fuels and chemicals:
CH₃OH, CH₄

FWP 78606

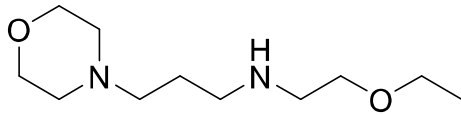
Intermediate term targets

carbon-negative building materials:
CO₂LIG

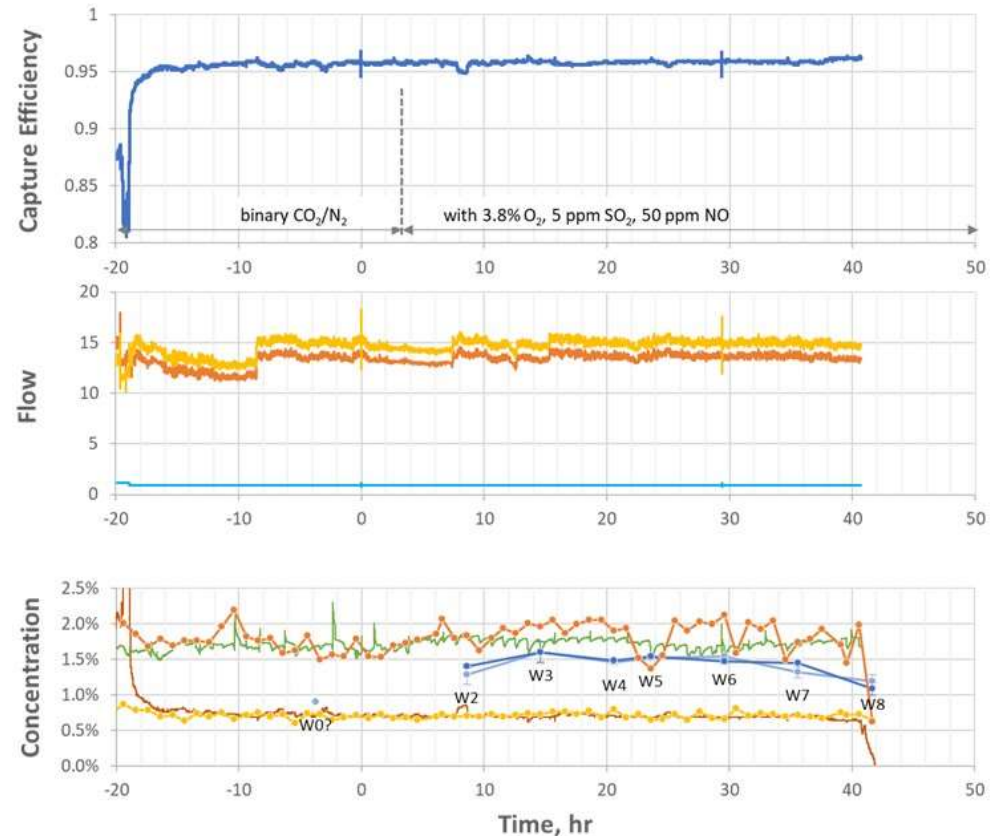
Long term targets

Mineralization materials:
CaCO₃ or MgCO₃

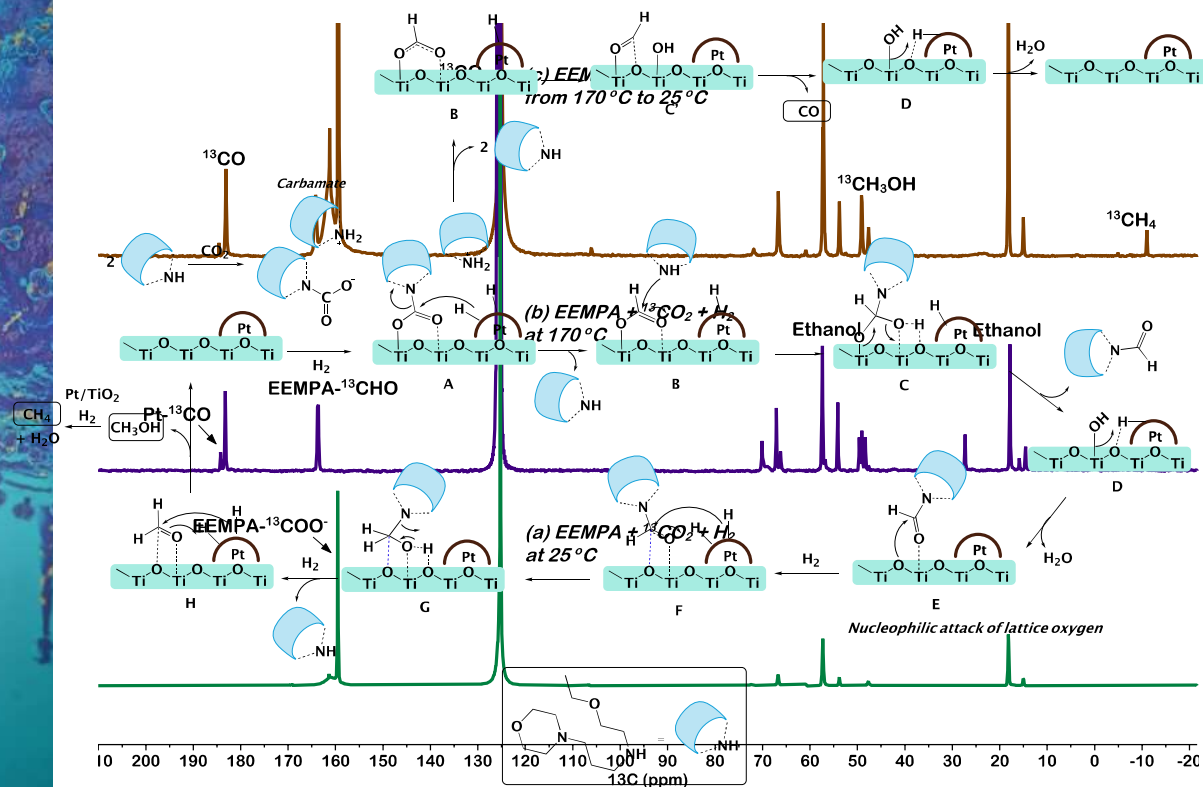
EEMPA is a promising solvent (2.0 GJ/tonne CO₂)¹ with low costs of capture (\$39/tonne² CO₂).²



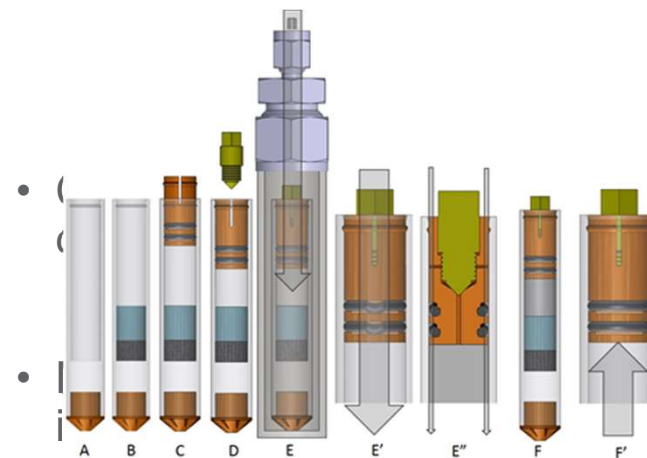
- Single component, water-lean solvent
- 19% cheaper and efficient than Shell's CANSOLV
- 90% lower corrosion and degradation than 5M MEA
- 0.5 MW coal fired plant demonstration, June, 2024



In-Situ ^{13}C MAS NMR Enables an Unprecedented View of Speciation and Kinetics of Catalytic Reactions



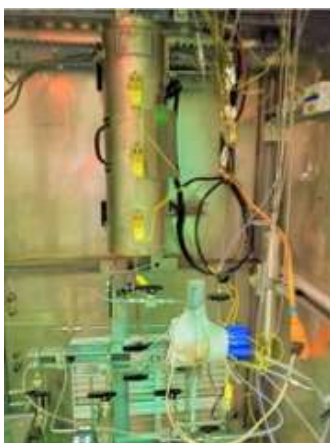
In situ ^{13}C MAS-NMR during the hydrogenation of $^{13}\text{CO}_2$ in the presence of 2-EEMPA and a 5 wt % Pt/TiO₂ catalyst at 170 °C under 60 bar H₂ (initial pressure) in an ethanol co-solvent, 2-EEMPA: EtOH=1:10 (molar ratio).



High-Temperature/Pressure WHiMS MAS Rotors
1st ever selective C-N cleavage of
an HN-formamide with a
heterogeneous catalyst

Methanol formation is sensitive to temperature and space velocity in a Post-Combustion Solvent

Hydrogenation of captured CO₂ using a packed-bed flow reactor.



Entry	Reaction T (°C)	CO ₂ Conv (%)	WHSV g _{CO2} /g _{cat} /h	TOS (h)	Selectivity (mol C%)					
					MeOH	EtOH	PrOH	BuOH	CH ₄	C ₂ H ₆
1	140	2.2	0.15	-	92.7	0.0	7.3	0.0	0.0	0.0
2	170	7.7	0.15	-	66.5	4.3	2.5	0.7	26.0	0.0
3	170	29.1	0.015	-	57.0	4.5	0.8	1.4	26.7	8.7
4	190	11.8	0.15	-	78.0	4.3	0.0	2.5	15.1	0.0
5	190	26.9	0.075	-	63.6	4.6	0.2	1.9	26.4	3.3
6	190	85.7	0.015	40	51.5	9.7	0.6	1.9	27.1	9.3
7	190	75.9	0.015	60	50.2	8.6	0.7	2.0	29.2	9.3
8	190	65.2	0.015	80	46.0	8.0	1.1	4.7	29.8	10.5

Liquid feed: captured CO₂ in EEMPA solvent (5 wt.% CO₂) Reaction conditions: 1.0 g catalyst D1, 870 psig; Gas feed: 38 sccm H₂, 5 sccm N₂. Change in WHSV is achieved by changing the liquid feed flow (0.05, 0.025, 0.005 mL/min).

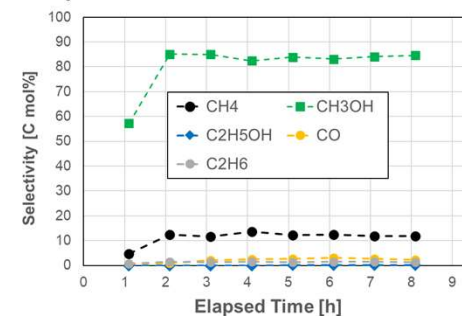
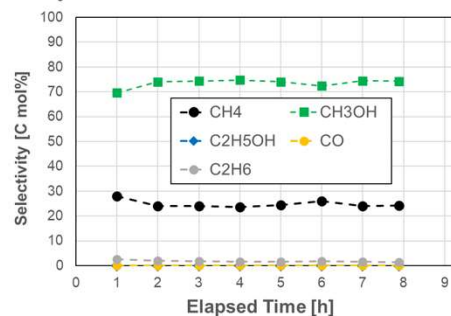
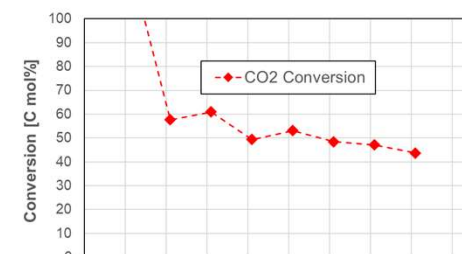
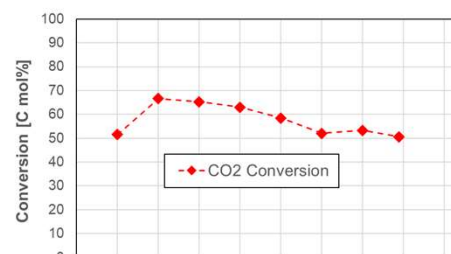
- Pt/TiO₂ is highly selective towards **methanol** with **93% selectivity** at **140 °C**.
- At 190 °C, the **CO₂ conversion** increased from **12%** to **86%** when space velocity was decreased by a factor of 10.
- Conversion decreased from 86% to 65% over a span of approximately 80 hours.

Demonstration of Semi-Batch CO₂ Capture and Catalytic Conversion to Methanol



CO ₂ Capture - LCFS			
Feed	CO ₂ /N ₂ [dry basis]	15 / 85	[mol%]
	Dew Point	15.6	[°C]
Absorber	Avg. Temperature	32.3	[°C]
	Avg. Pressure	0.08	[psig]
Stripper	Avg. Temperature	95.1	[°C]
	Avg. Pressure	14.39	[psig]
Reboiler	Temperature	114.9	[°C]
Flow	Liquid	15.3	[kg/h]
	Gas	0.61	[kg/h]
	L/G	25.2	[-]
CO ₂ Capture Efficiency		88.9	[%]

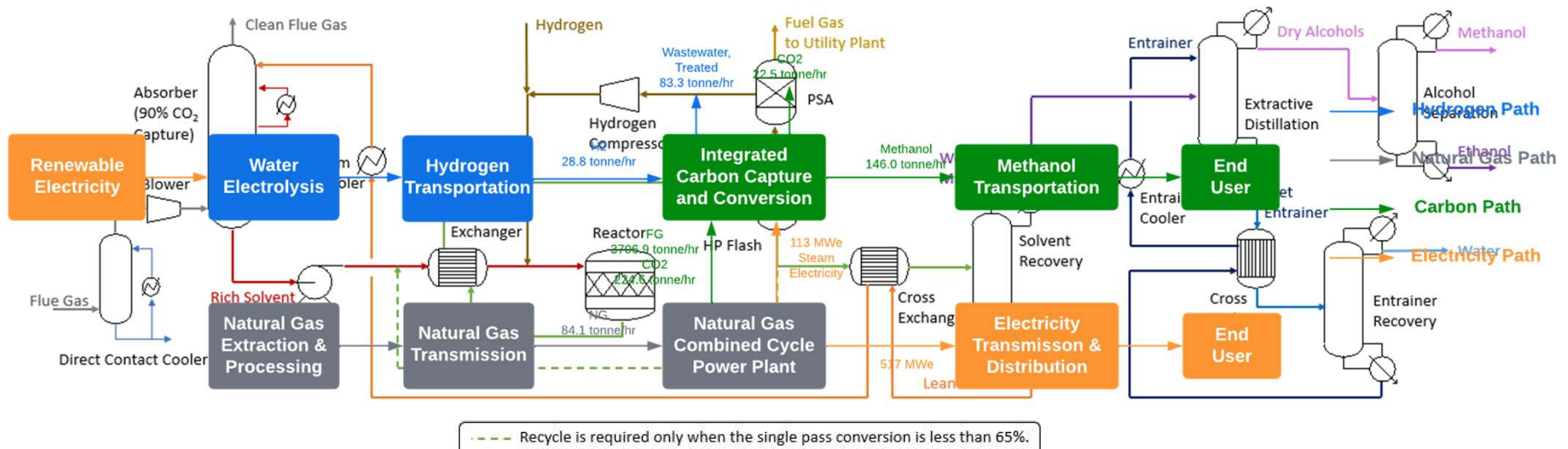
CO ₂ Conversion - TCCS			
Gas Feed	H ₂ /N ₂	93 / 7	[mol%]
	Flowrate	6.7 E-3	[kg/h]
Liquid Feed	2-EEMPA/CO ₂ /H ₂ O	78 / 5 / 17	[mol%]
	Flowrate	5.9 E-4	[kg/h]
Reactor	Temperature	170	[°C]
	Pressure	865	[psig]
	Catalyst: 5wt% Pt on TiO ₂	2.5	[g]
CO ₂ Conversion		55 → 0.8	[%]
Methanol Yield		94 → 0	[%]



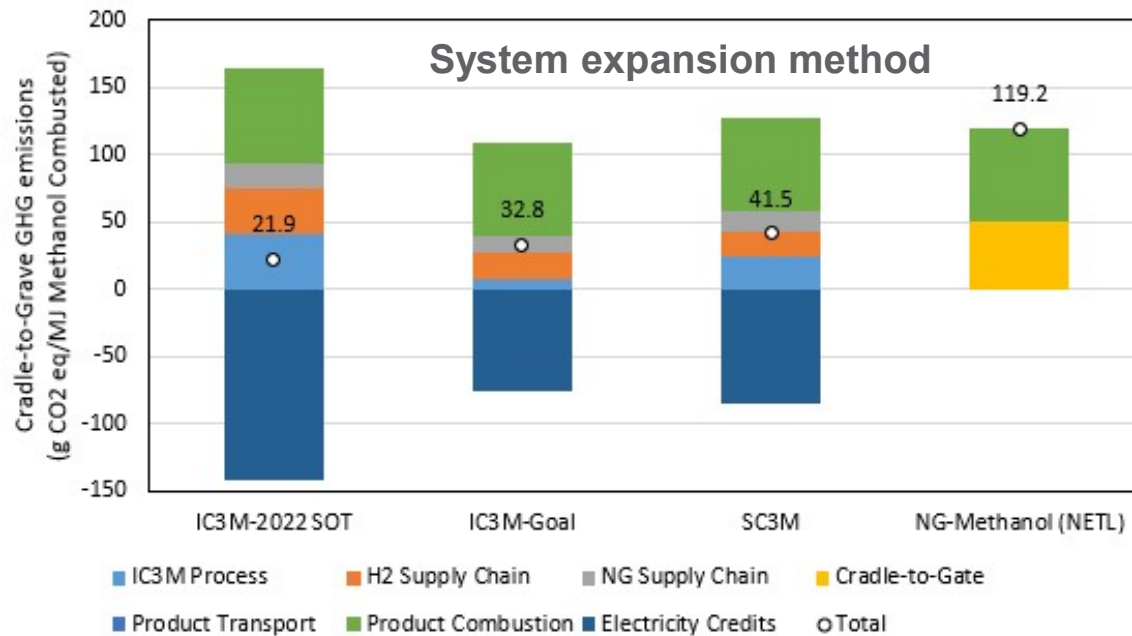
- Single-pass operation: 8-hours on simulated coal-derived flue gas (CO₂, N₂, H₂O).
- 190°C, 865 psig, 0.053 g_{CO₂}/g_{cat}/hr
- Conversion > 50%, CH₃OH selectivity ~ 80%, 8 hr TOS

Key Performance Measures for PNNL's IC³M Technology (From Previous TEA Study*)

	SOT	Goal Case
WHSV (gCO ₂ /gCat/hr)	0.075	0.15
Single-pass CO ₂ conversion (%)	26.9	85.7
Methanol selectivity (C %)	63.6	100
Methane selectivity (C %)	26.4	0
Source	Experiment	R&D Target



IC³M could achieve significant GHG emission reductions compared to conventional processes.



- Life Cycle GHG Emission Impact Assessment for byproducts
- Un-optimized 2022 SOT and Goal > 72% reduction in GHG emissions vs fossil-derived methanol
- IC³M results in 21% lower GHG emissions than separate capture and conversion (SC3M)
- Further GHG reductions via improvement in the catalyst performance

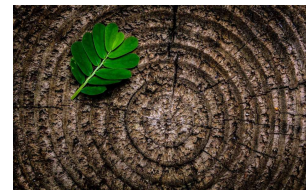
Composite materials may be economical large volume CO₂ sinks.



- Wood flour (~50 wt.% filler) and HDPE plastic
- US Market: 3.55 billion linear board feet, \$2.8 billion USD per year
- Storing 5 wt. % CO₂ in decking could sequester 250,000 tonnes per year (emissions of 54,000 cars)
- *Susceptible to rot and UV damage, 20-year lifespan

Goal: Replacing wood flour with abundant, cheap and highly chemically/UV durable biopolymers. Their use in composites also provides CO₂ emission avoidance.

- Lignin: complex organic polymer that forms structural materials in the support of plants.
- Lignite: combustible sedimentary rock formed from naturally compressed peat.

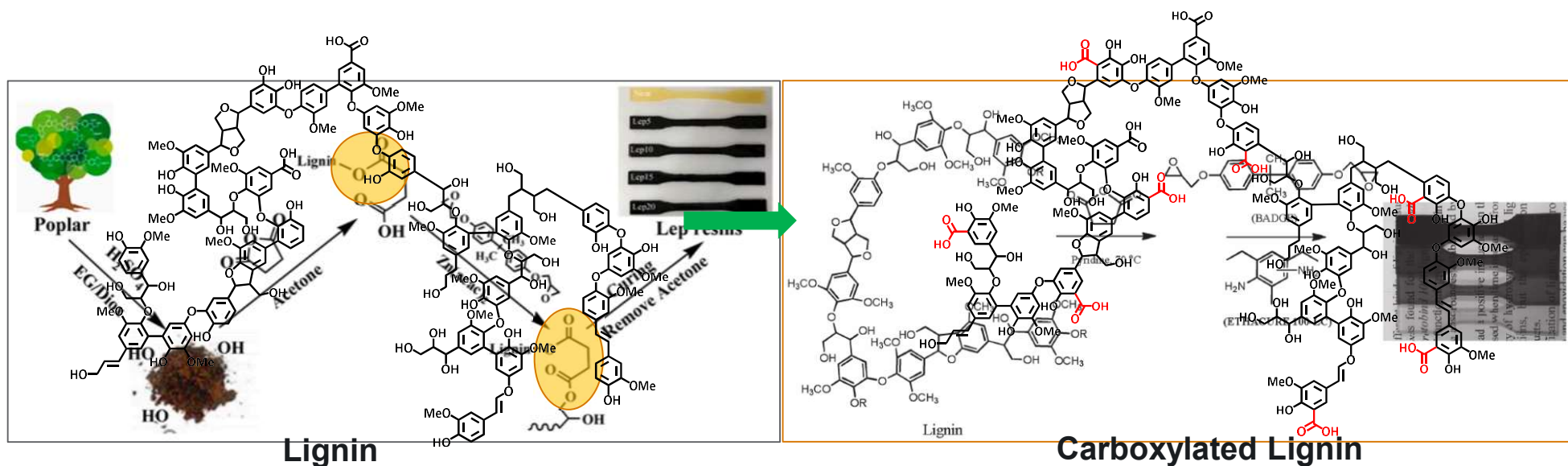


Lignin



Lignite

Lignin and lignite are strong, cheap, and chemically durable but they cannot bind well in polymer matrixes without chemical modification.



- Maleic Anhydride Polyethylene (MAPE) is chemically grafted on phenolic hydroxyls
- Functionalization is susceptible to hydrolysis of C-O-C linkage

***How can we add CO₂ to the surface of these particles to act like MAPE while being a CO₂ sink ?**

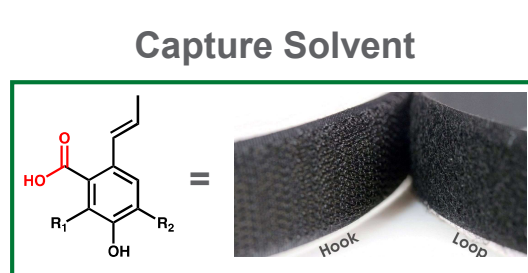
Turning CO₂ Into the “Velcro” to Improve Binding with Polymer Matrixes via Reactive Carbon Capture



HDPE



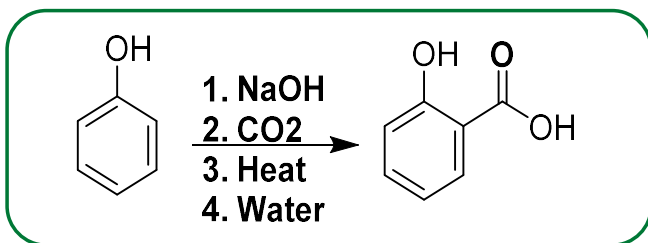
Lignin or Lignite + CO₂



(CO₂LIG) Composite

How can we add CO₂ to polyphenolic polymers...?

Kolbe-Schmidt Reaction



Production of Salicylic Acid for Aspirin



- Chemically durable (C-C bonded) composite fillers utilizing CO₂ in its entirety
- Can use any inorganic or strong organic base (capture solvent)

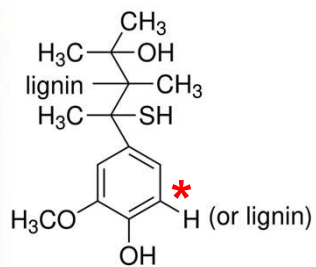
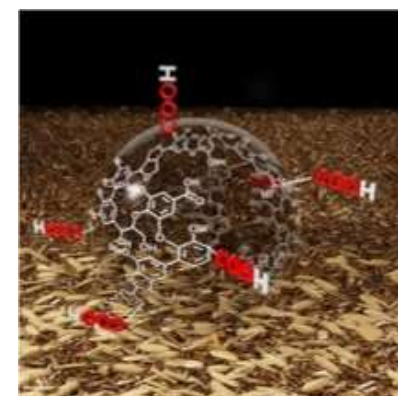
Carboxylating 200g batches of alkaline lignin, sodium lignosulfate, DEC25, Buelah Zap Lignite, and DEC26, Wyodak Sub-bituminous coal.



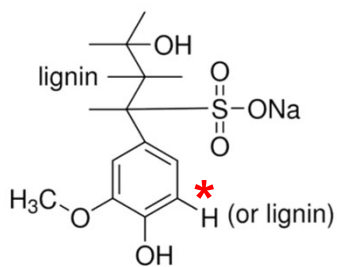
CO₂
Capture Solvent
(Base)



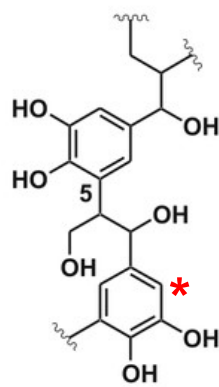
1M H₂SO₄
Filtration



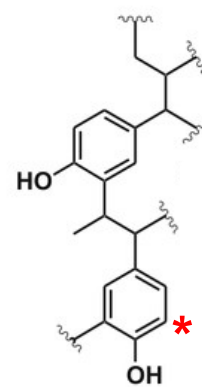
Lignin alkali



Sodium lignin sulfonate



Lignite



Sub-bituminous



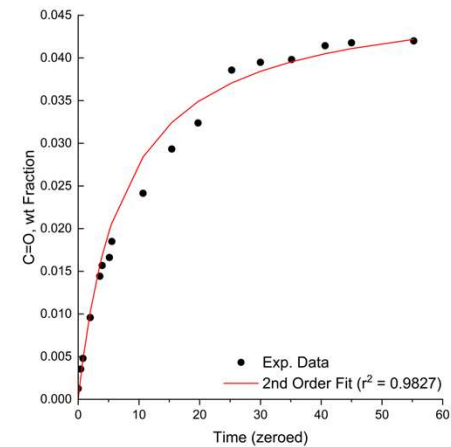
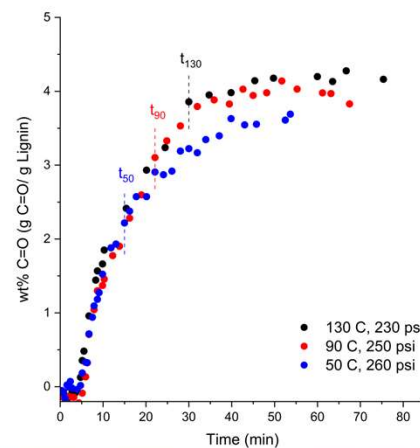
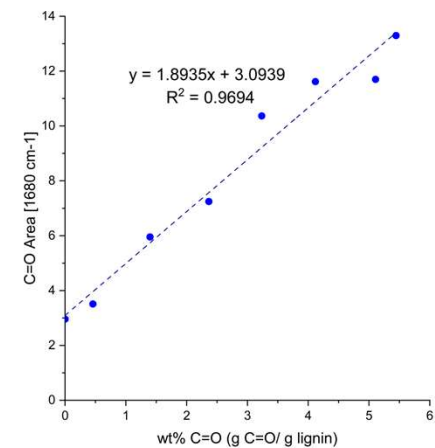
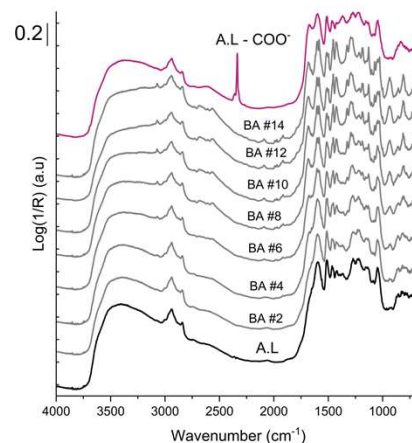
Isolated yields
Lignin = 64-98%
Lignite = 39-65%

In-situ FT-IR (Fourier Transform Infrared) to determine CO₂ loading, optimal reaction conditions and reaction rate.

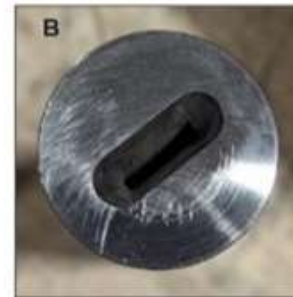
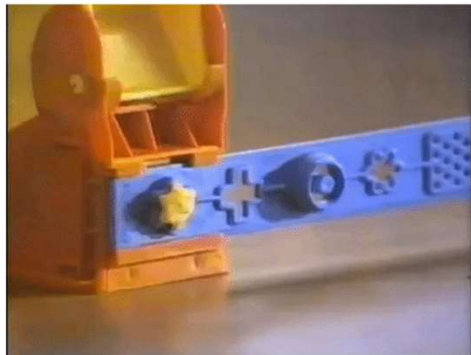
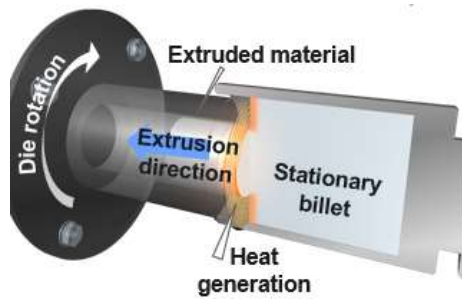
- Praying Mantis DRIFTS Cell:
 - Max temp ~ 910 °C (under vacuum)
 - Max Pressure ~ 1.5 Mpa (~215 PSI)
- Monitor carboxylic acid peak growth
- Built calibration standards
- CO₂ content in fillers ranges 2- 4.2 wt. %
- Operando kinetic measurements



Manuscript in preparation.



Shear Assisted Processing and Extrusion (ShAPE) manufacturing of wires, bars, or ribbons for property testing.

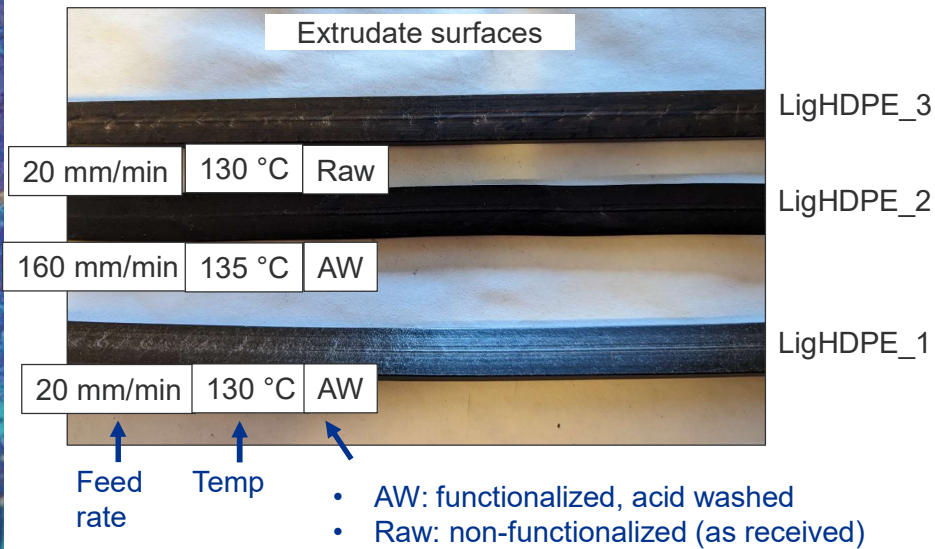


A. Reza holding an 80 wt.% filler ShAPE composite extrudate;
 B. Tooling cavity designed for manufacturing composite 'bars';
 C. Cold-pressed composite feedstock granules in ShAPE ring;
 D. ShAPE polymer composite bars with no surface defects

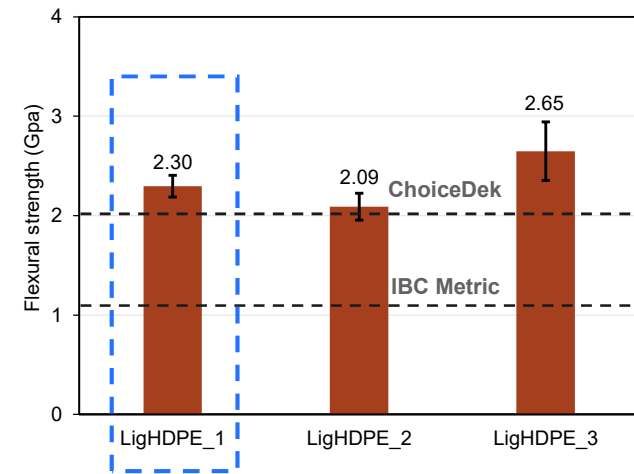
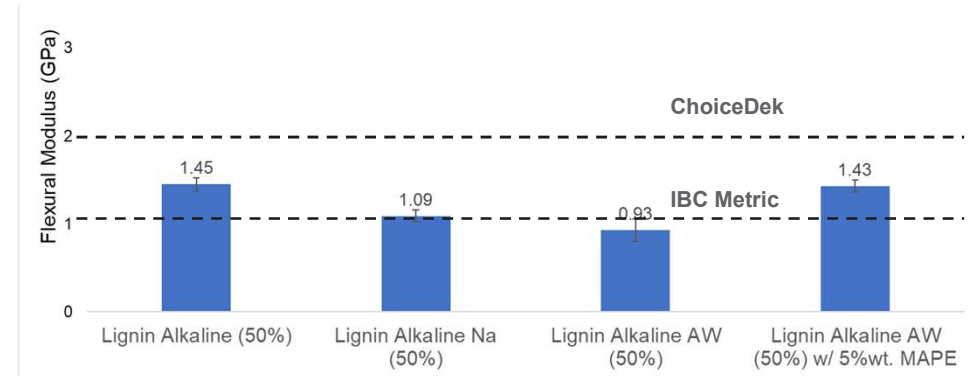


- ShAPE enables 80 wt.% CO₂LIG filler content, vs 50% for conventional injection molding

The Flexural Moduli of ShAPE Extruded Bars 80% Lignins / 20% wt.% HDPE are Above 2 GPa, Meeting International Building Code Requirements

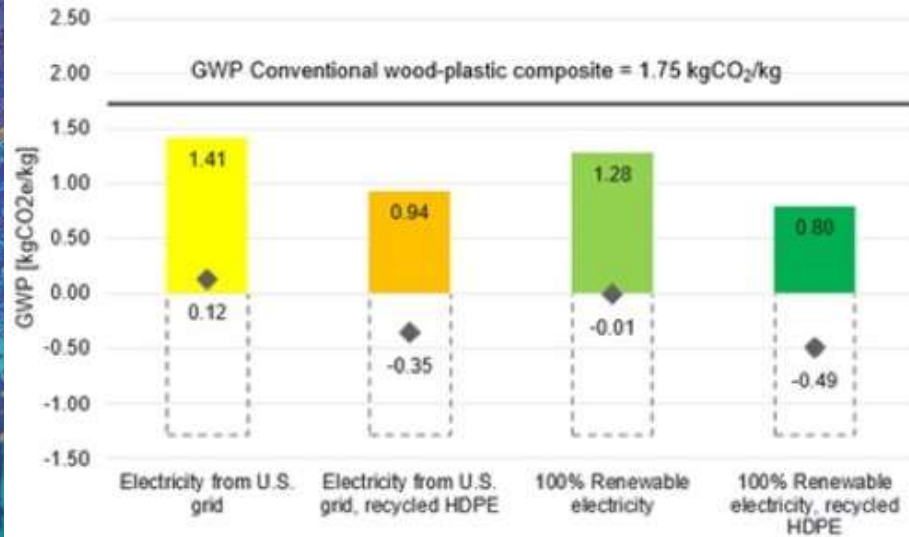


- Higher modulus was obtained for non-functionalized fillers (LigHDPE_1 vs. LigHDPE_3), and for low-speed extrusion (LigHDPE_1 vs. LigHDPE_2)

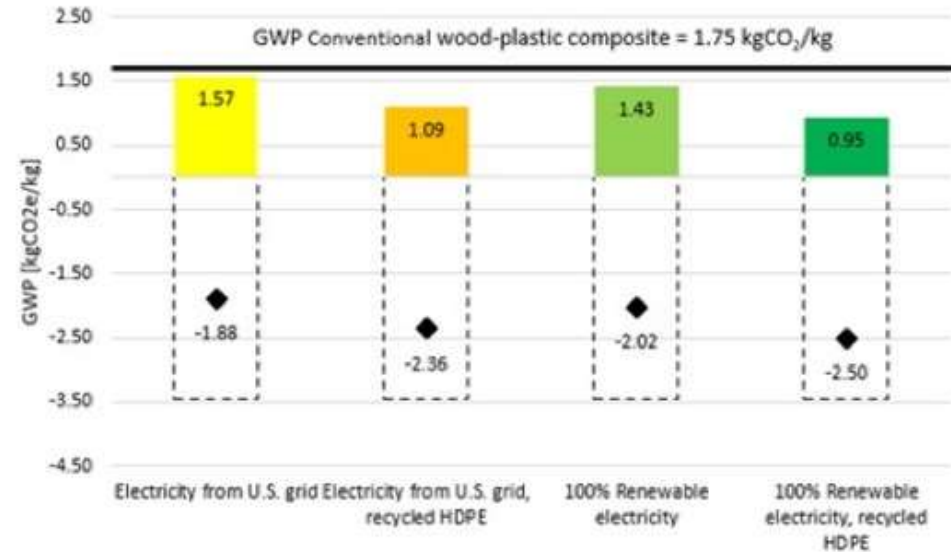


LCA for lignin composites suggests the global warming potential of CO₂LIG is much lower than that of conventional wood-plastic composites.

(a) Results include the CO₂ stored into CO₂LIG only

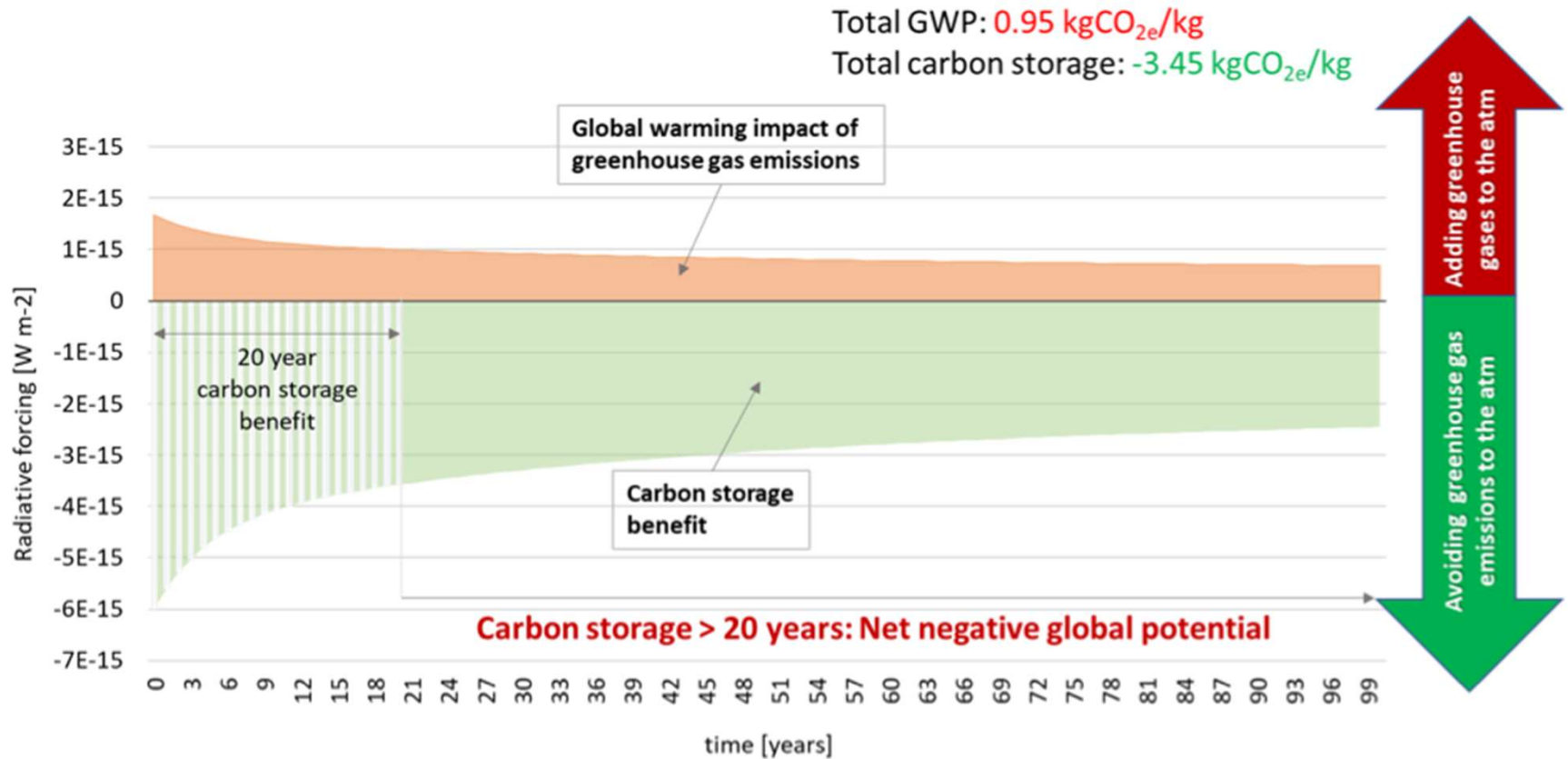


(b) Results include the CO₂ stored into CO₂LIG and the additional CO₂ sequestered and stored in the ground



- GWPs of the CO₂LIG-plastic composite panel are lower in all the scenarios, with an overall reduction between 18 and 54% (carbon storage benefits excluded).

*Temporal radiative forcing analysis CO₂ on CO₂LIG-plastic composite (lifetime of the product) needed to achieve carbon neutrality.



*100% renewable electricity, recycled HDPE with benefits from subsurface CO₂ storage



Reactive CDR can reduce costs and energy demand for CO₂-derived fuels, chemicals and CO₂-negative composites.

IC³M thermocatalytic reduction = Cheaper, more efficient fuels and chemicals

- Solvent drives condensed-phase catalytic hydrogenations
- Different mechanisms, free energy landscapes and chemical equilibria to exploit
- Minimizes enthalpy of sorbent regeneration and CO₂ compression energy
- 72% reduction in GHG emissions vs fossil-derived methanol
- 21% lower GHG emissions than separate capture and conversion (SC³M)

IC³M CO₂LIG = Economically profitable CO₂-negative building materials

- Solvent's Bronsted basicity captures and promotes Kolbe-Schmidt reactions
- 2-5 wt. % CO₂ fixation on lignin and lignite ~ 80 °C Up to 94% and 65% isolated yields respectively
- Lignin (50-70 wt.% filler) and Lignite composites (80 wt.% filler) using shear assisted processing and extrusion
- Manufactured composites meet IBC metrics for flooring or decking
- Carbon neutrality is achieved after 20 years of storage, and > 20 years results in a net negative GWP

Acknowledgements



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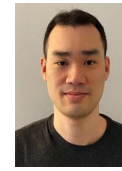
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Wontae Joo



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Keerti Kaapagantula



Deepika Malhotra



Yuan Jiang



Lesley
Snowden-Swan



Jaelynn King



Aditya Nittala



Yelin Ni



Jose Ramos



Francesca
Pierobon