

The prospects of flexible natural gas-fired CCGT within a green taxonomy

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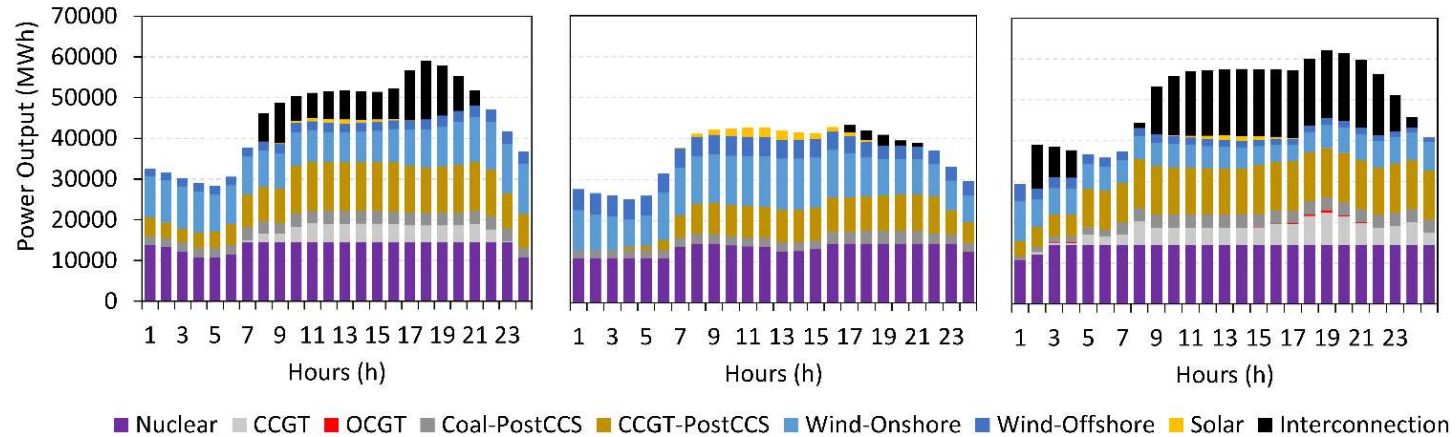
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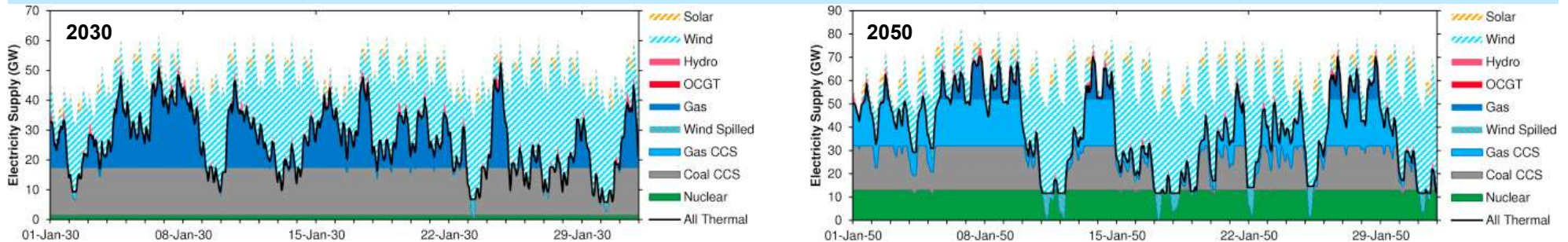
Flexible CCS in future electricity systems

Hourly power generation for three sample days in a 2035 UK power system

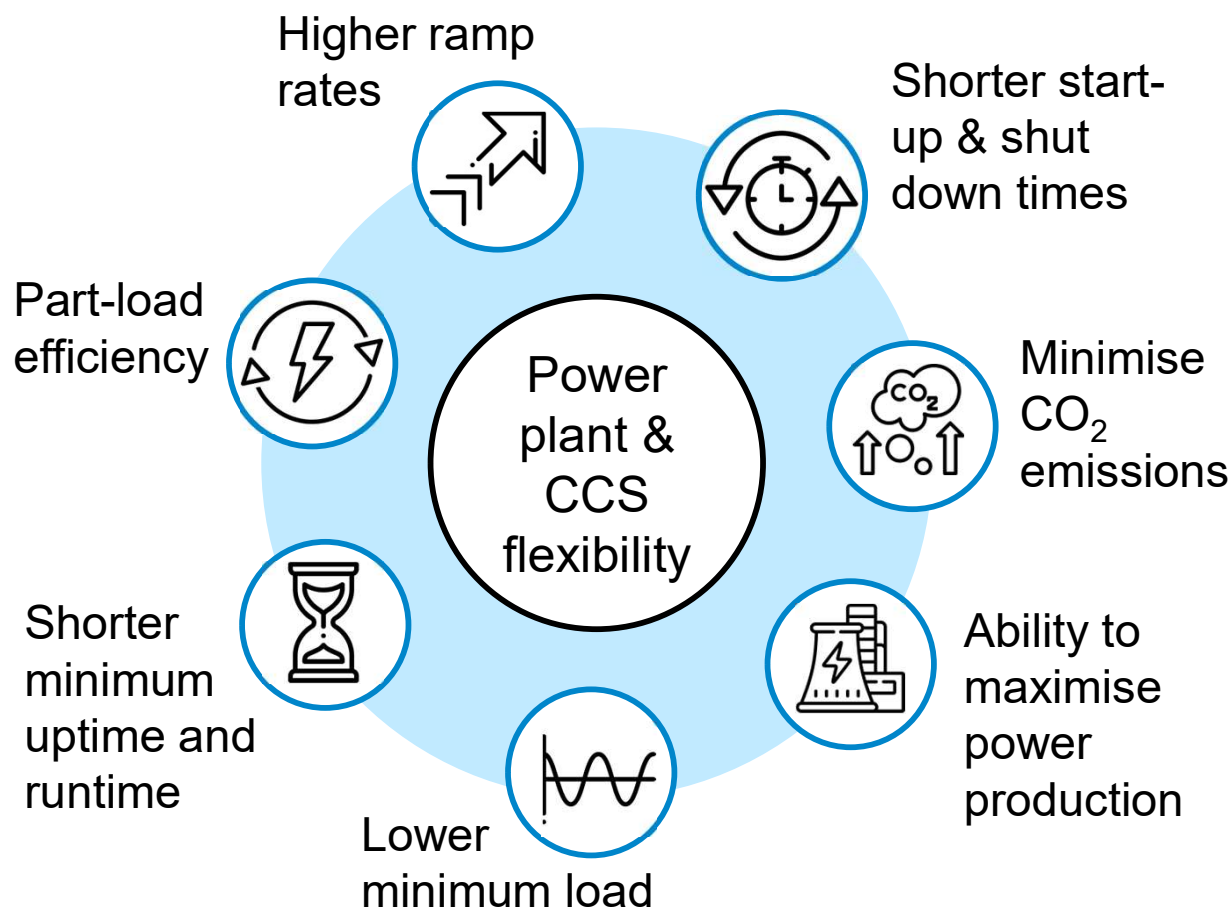
To accommodate intermittent renewables, fossil fuel power plants will need to operate flexibly.



Electricity supply for the UK from 2030 to 2050



Flexibility of power plants with CCS



Rise in the frequency of start-up and shut down cycles will be expected with higher levels of intermittent renewables.

If this significantly increases CO₂ emissions, it will undermine the value proposition of CCS.

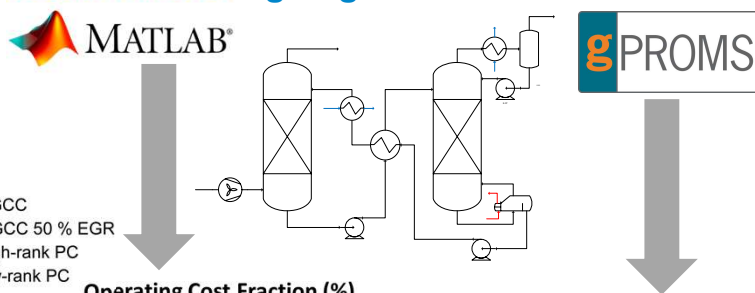
Need to ensure CO₂ emissions reduction requirements are being met.

Technology development & delivery

Process modelling

Develop understanding of the impacts on cost and technical performance

Process modelling in gPROMS and MATLAB

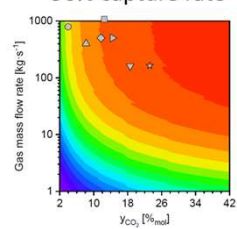


- 500 MW NGCC
- △ 500 MW NGCC 50 % EGR
- ◇ 500 MW high-rank PC
- 500 MW low-rank PC
- ▽ 500 MW biomass
- ▼ 1 MMtpa cement
- ☆ 1 MMtpa steel

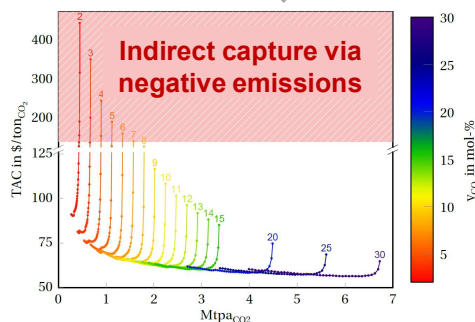
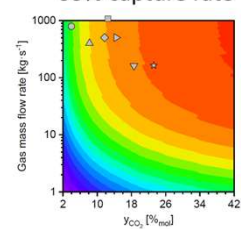
Operating Cost Fraction (%)



90% capture rate

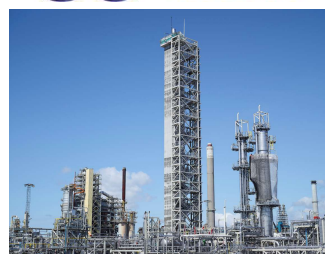


99% capture rate

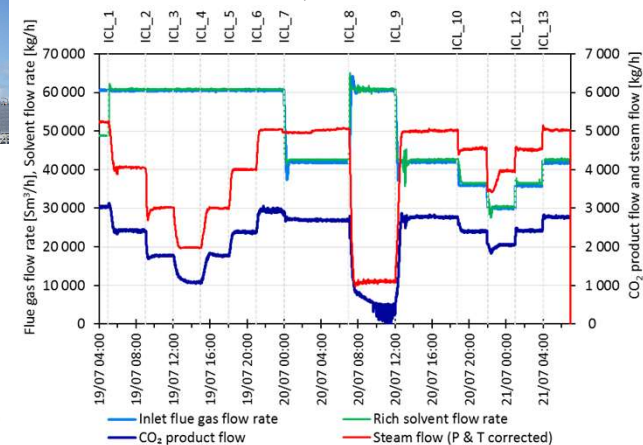
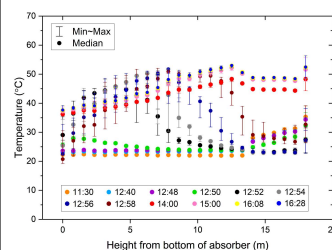


Demonstration

Demonstrates feasibility and develop understanding of plant operation



Operating data from demo plant

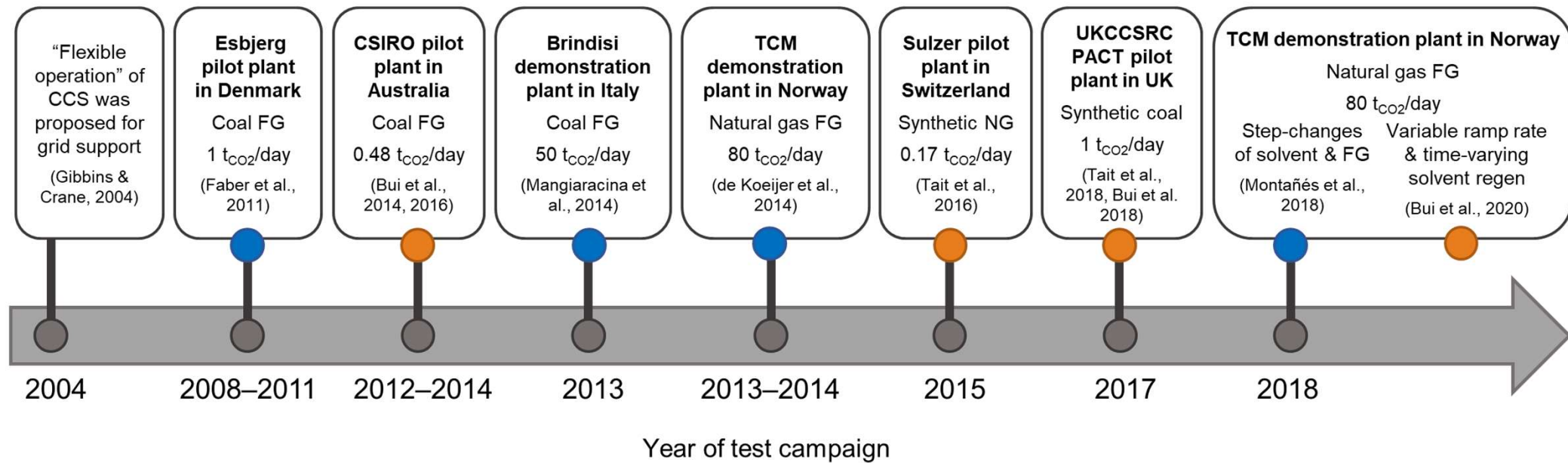


Brandl, P., Bui, M., Hallett, J. P. & Mac Dowell, N. (2021). *IJGGC*, 105, 103239.
Danaci, D., Bui, M., Petit, C. & Mac Dowell, N. (2021). DOI: 10.1021/acs.est.0c07261

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IEAGHG, 2022. Start-Up and Shutdown Protocol for Natural Gas-Fired Power Stations with CO₂ Capture”, technical report 2022-08, 2022.

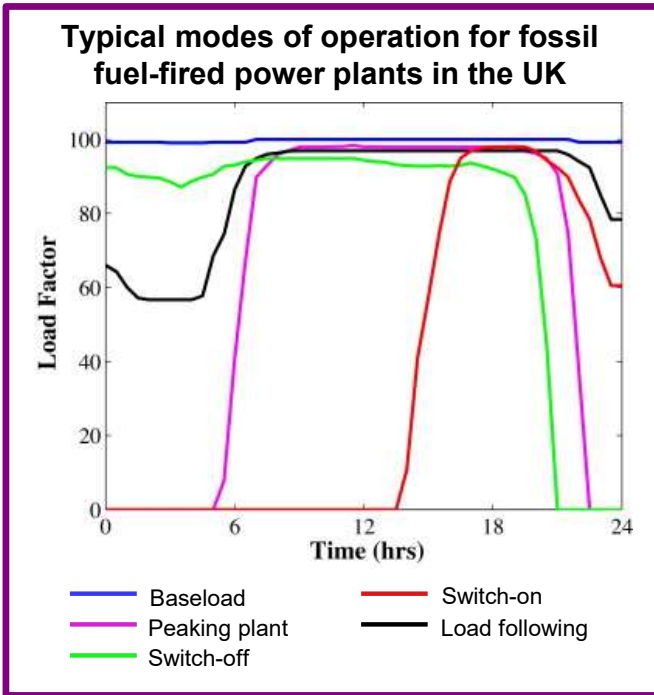
Pilot & demonstration studies of flexible CCS operation



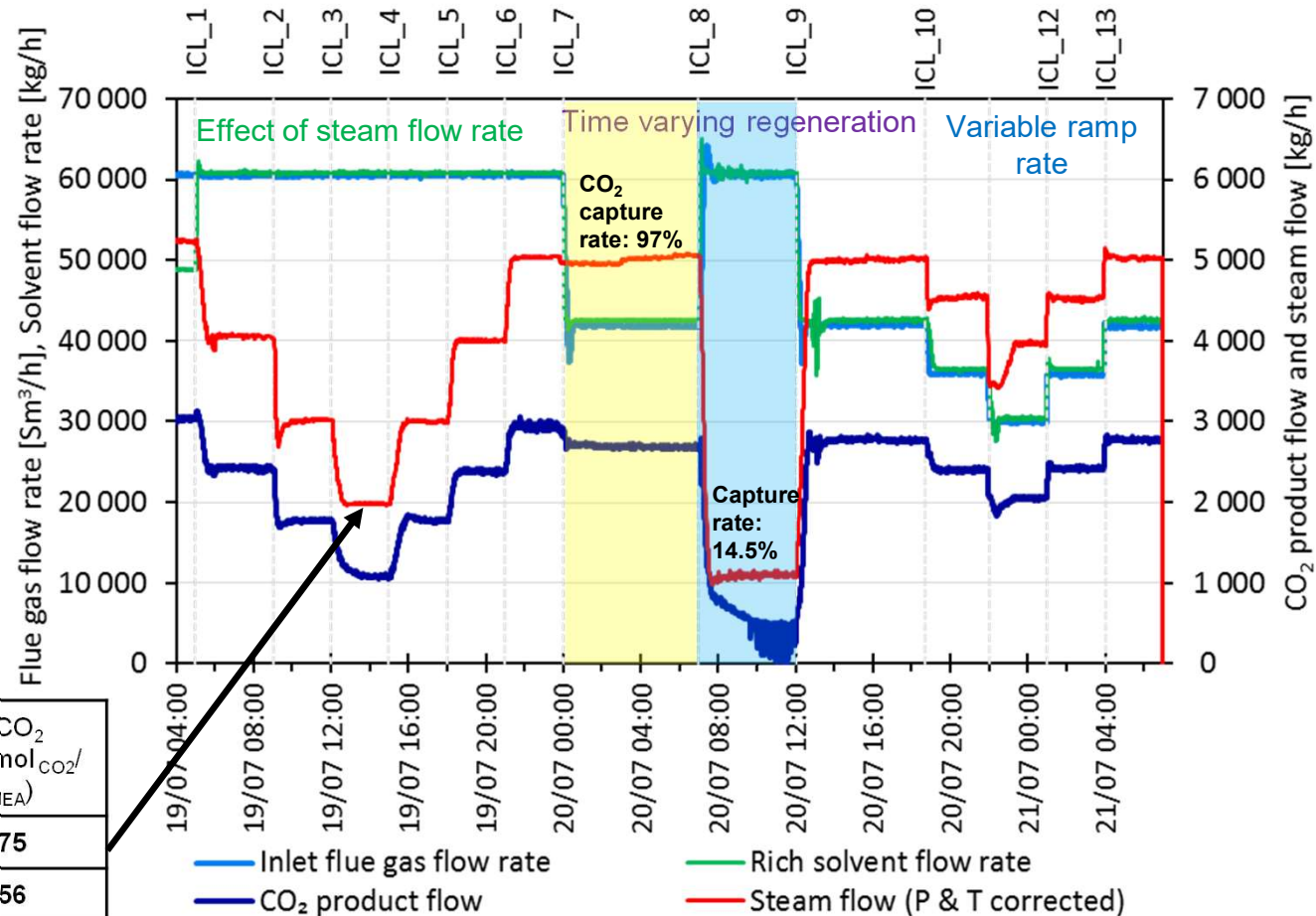
- Dynamic process data unavailable
- Dynamic process data published

We have gained valuable operating experience at dynamic conditions.
Dynamic operating data for model development is being made available.

Flexibility of power plants with CCS



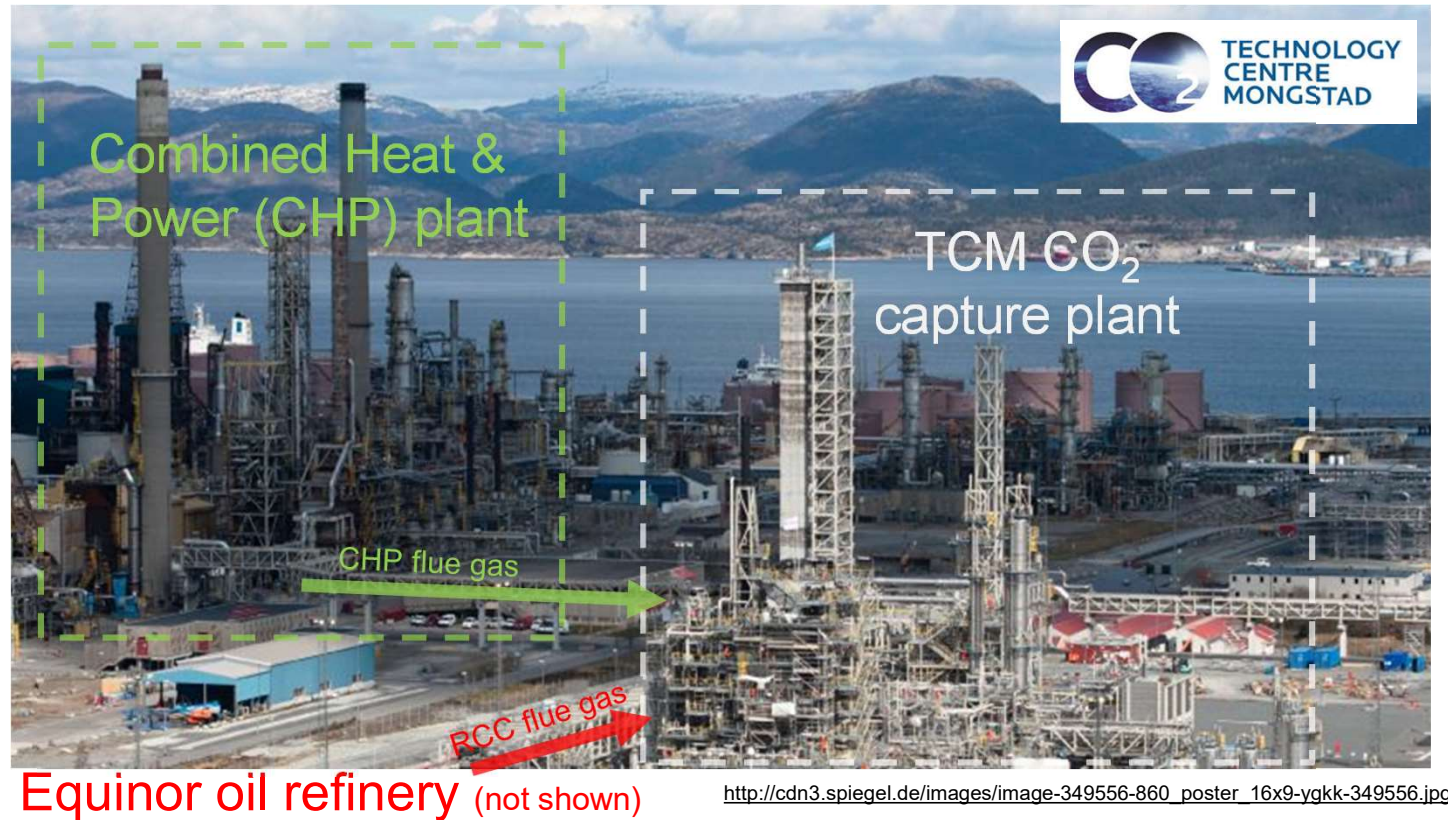
Steam flow rate (kg/h)	CO ₂ capture rate (%)	Lean CO ₂ loading (mol _{CO₂} /mol _{MEA})
2000	26.0	0.4375
5000	72.0	0.2456



Flexible operation of a demonstration- scale CO₂ capture plant

In 2020, we studied the effect of start-up & shut down on CO₂ emissions at TCM.

Studying the following: (i) hot vs cold start-up, (ii) timing of steam availability (conventional vs preheat vs delayed), (iii) solvent inventory capacity, (iv) start-up solvent loading/composition.



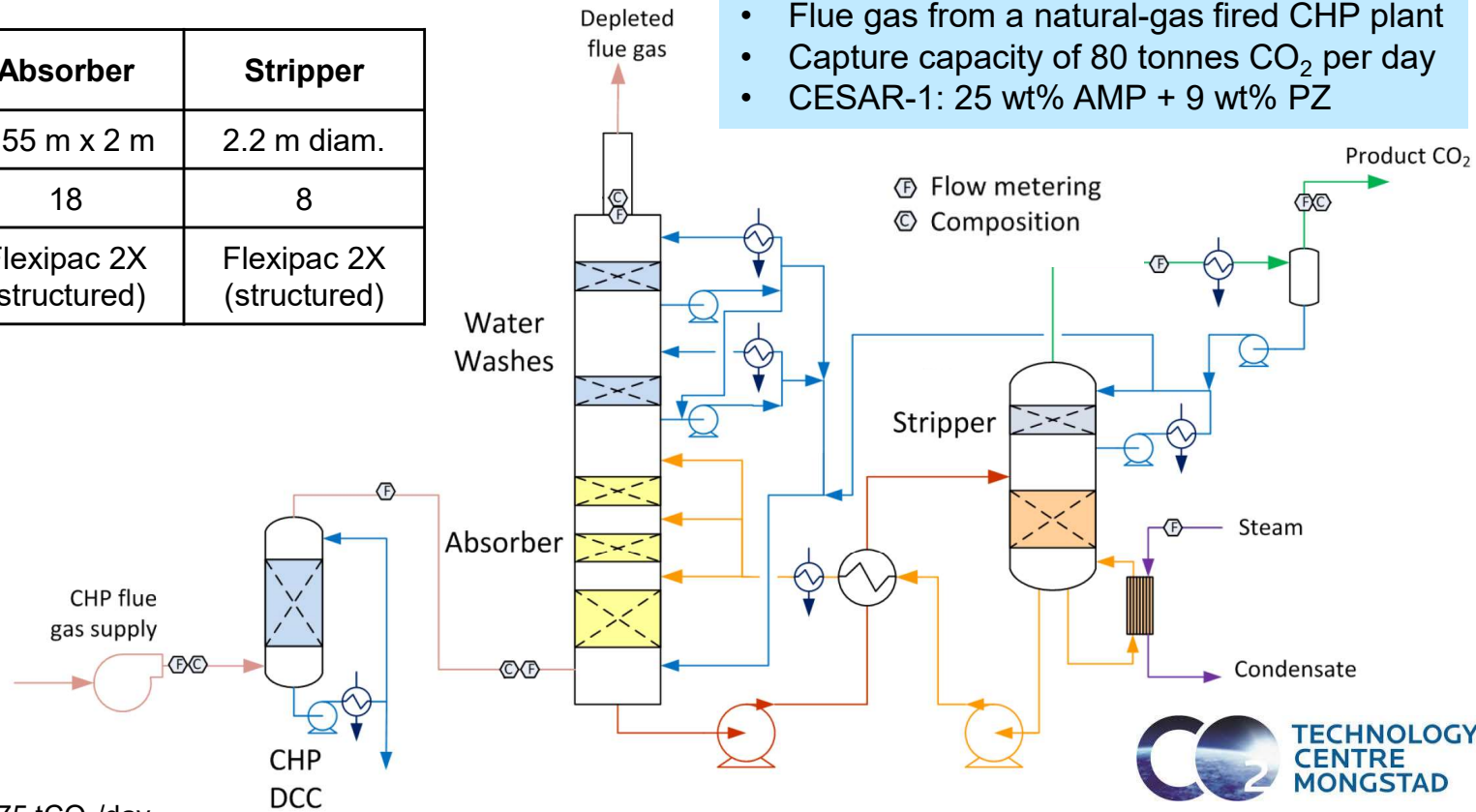
TCM CO₂ capture facility, Mongstad Norway

	Absorber	Stripper
Cross section dimensions	3.55 m x 2 m	2.2 m diam.
Packing height (m)	18	8
Packing type	Flexipac 2X (structured)	Flexipac 2X (structured)

Flue gas component	CHP
	mole %
N ₂	71.6 – 78.6
CO ₂	3.5 – 4.3
H ₂ O	2.5 – 6.3
O ₂	12.5 – 14.4
Ar	0.9 – 1.0

Combined heat and power (CHP) mode

- Flue gas from a natural-gas fired CHP plant
- Capture capacity of 80 tonnes CO₂ per day
- CESAR-1: 25 wt% AMP + 9 wt% PZ

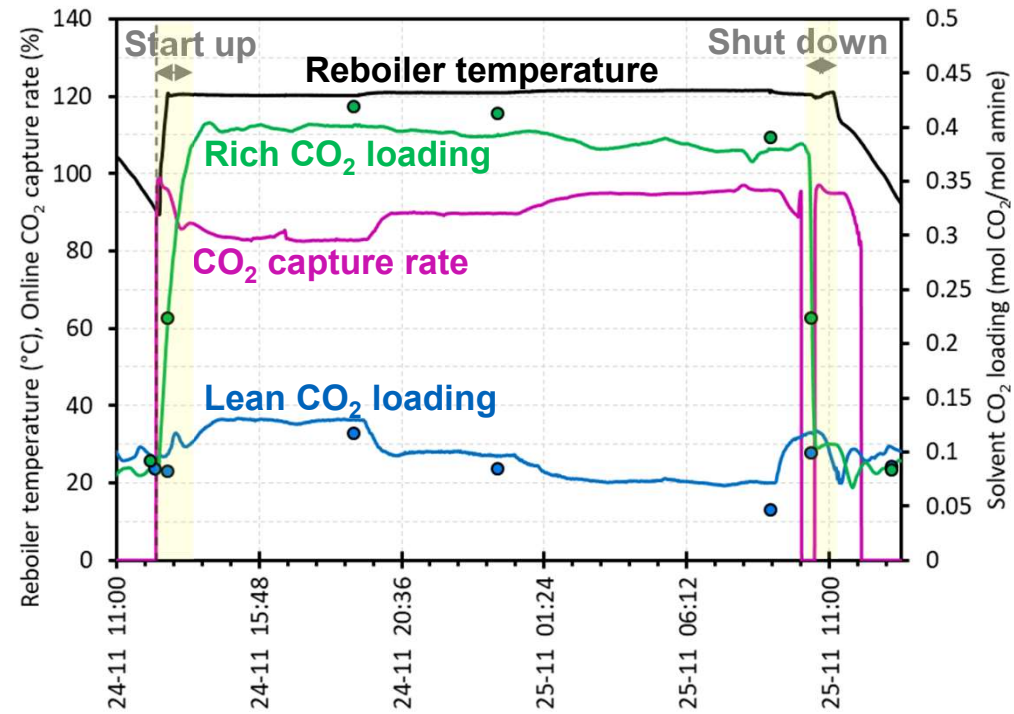
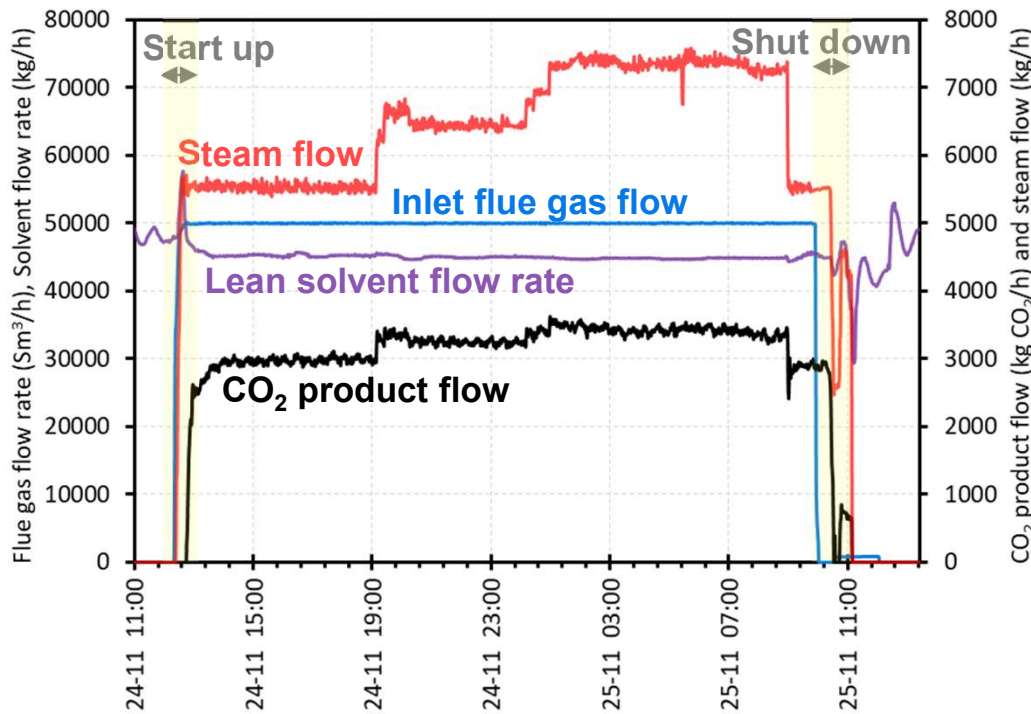


RCC mode: gas 12 mol% CO₂, captures 275 tCO₂/day

The 18 m packing height used for these test corresponds to the bottom two beds
Total height of all three beds = 24 m

Start-up and shut down tests at TCM

Hot start-up and shut down with 53 m³ solvent inventory

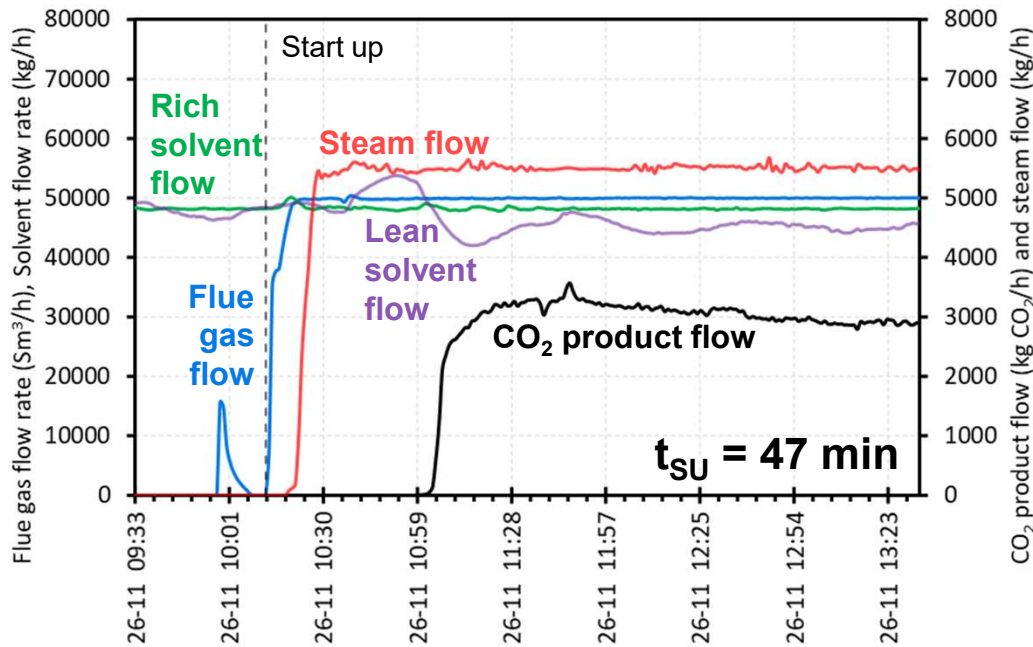


Start up: Flue gas flow is turned on, steam flow begins earlier, at same time, or delayed.

Shut down: Flue gas flow ramps down, steam flow rate continues until target solvent loading is achieved.

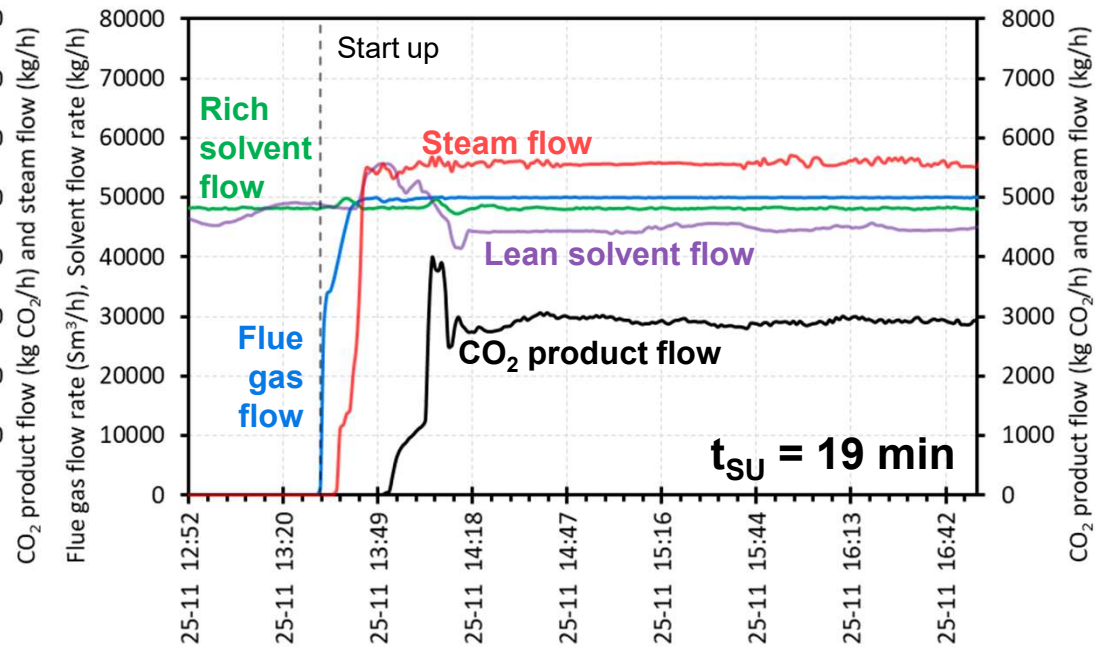
Cold vs hot start-up

Cold start-up with 42 m³ solvent inventory



Cold start-up: performed after a long downtime, i.e., >8 hours, stripper cools to near ambient temperature (25 – 40 °C). The time when CO₂ product flow starts is t_{SU} . Test above has steam flow starting at a similar time to the flue gas flow.

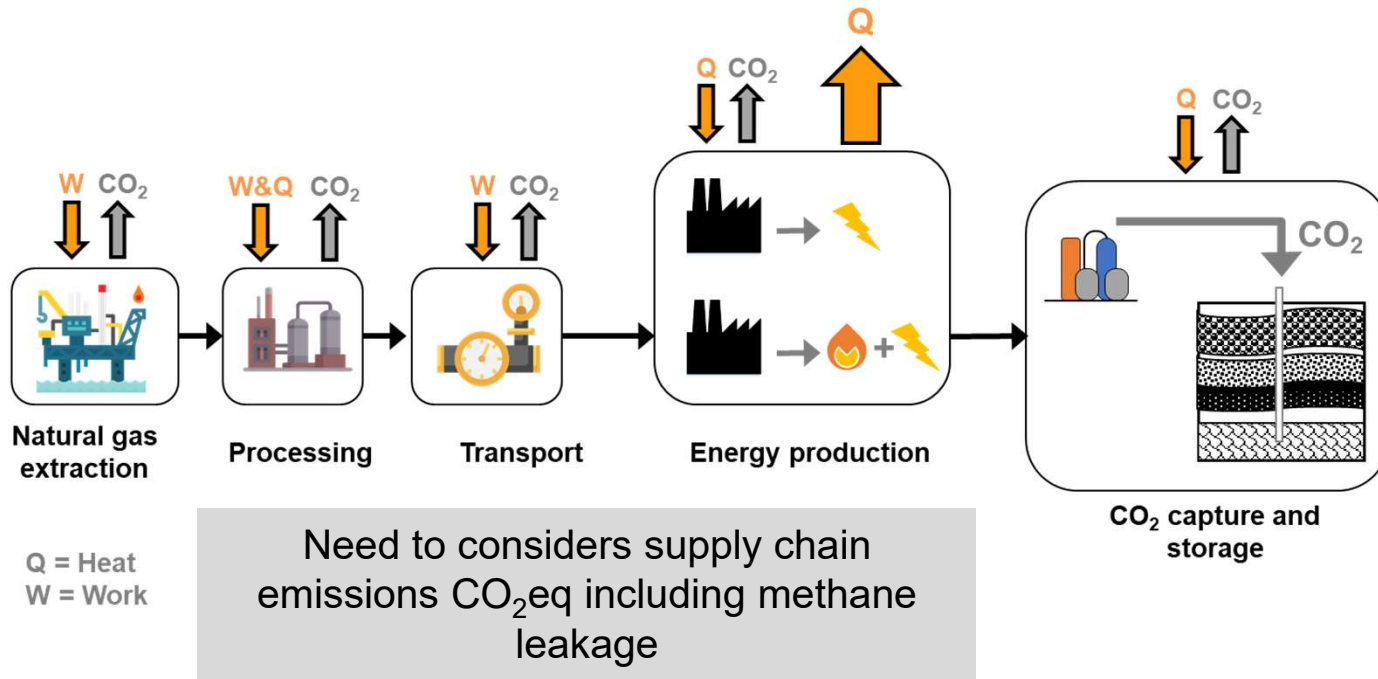
Hot start-up with 42 m³ solvent inventory



Hot start-up: performed after a short downtime, i.e., off for <8 hours, stripper is still high temperature at 80 °C or above. Thus, hot start-ups are much quicker than cold start-ups (shorter t_{SU}).

- High capture rates above 90% is techno-economically feasible (at steady state).
- During dynamic operation, 90% capture rate is feasible with load following regimes (e.g., ramp up/down) and hot start-up and shut down.
- During cold start-up and shut down, CO₂ capture rates can reduce to 50% or lower.
- Increased start-up and shut down cycles could increase CO₂ emissions of a CCGT significantly.

	Zero emissions intensity steam		With an NG auxiliary boiler for SUSD	
	Cumulative specific reboiler duty (MJ/kg CO ₂)	Cumulative CO ₂ captured (%)	Cumulative specific reboiler duty (MJ/kg CO ₂)	Cumulative CO ₂ captured (%)
82 min start-up (SU) combined with shut down (SD)				
Cold SU 53 m ³ & SD	8.15	80.0	12.42	52.5
Cold SU 42 m ³ & SD	8.51	66.3	13.04	43.3
Hot SU 53 m ³ & SD	6.06	97.3	7.26	81.2
Hot SU 42 m ³ & SD	5.94	96.5	6.93	82.9
Hot SU 42 m ³ delayed steam & SD	6.17	67.7	7.35	56.8

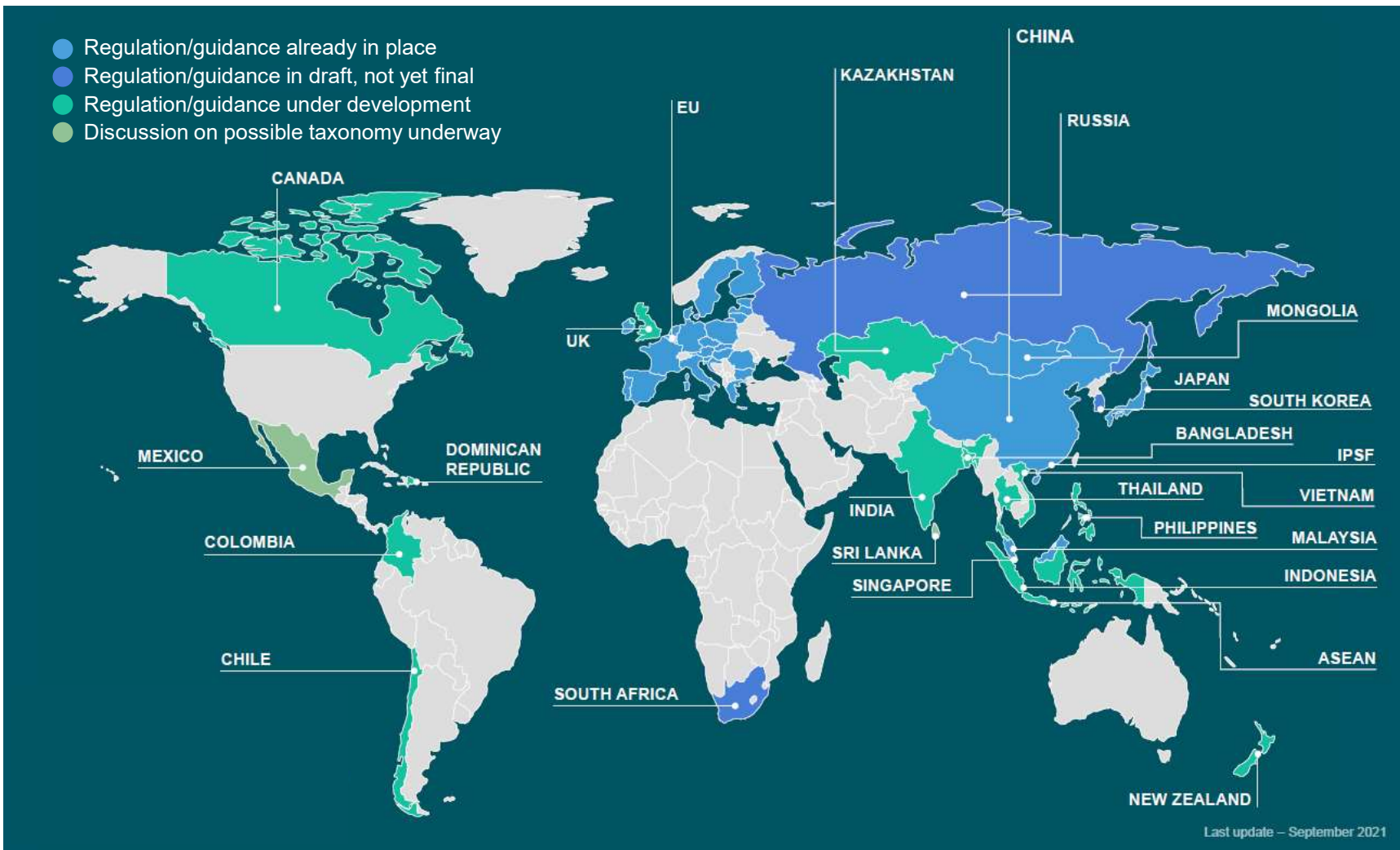


The EU green taxonomy

Provides financial firms guidance on which activities qualify as being “green”.

Technology-agnostic emissions threshold of 100 kg CO₂ eq/MWh for electricity generation, heat production and co-generation of heat and electricity.

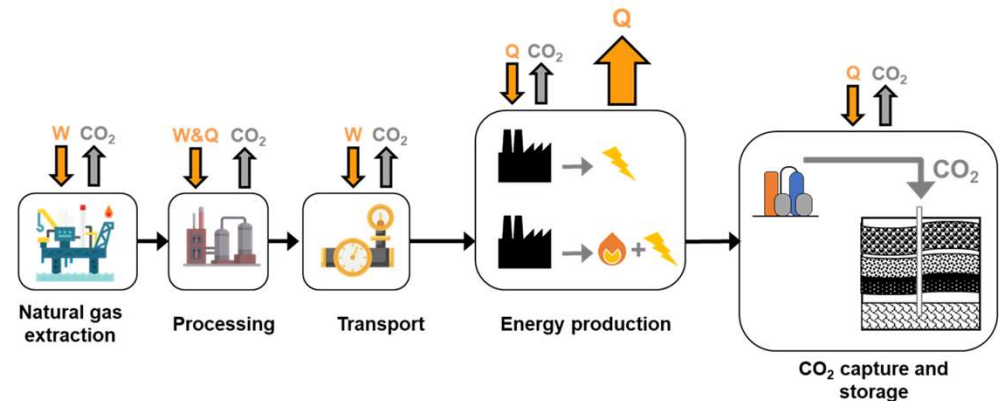
For hydrogen production, the lifecycle GHG emissions threshold needs to be lower than 3 tCO₂ eq/t H₂, which favours green and blue hydrogen.



To determine the eligibility of a combined cycle gas turbine (CCGT) power plants within any future sustainable green taxonomy.

Evaluated the effect of the following factors on the CO₂ intensity of electricity generation by a CCGT power plant:

- Natural gas supply chain emissions;
- CO₂ capture rate;
- Switching to blue hydrogen;
- Number and type (e.g., cold vs hot) of start-up and shut down cycles.



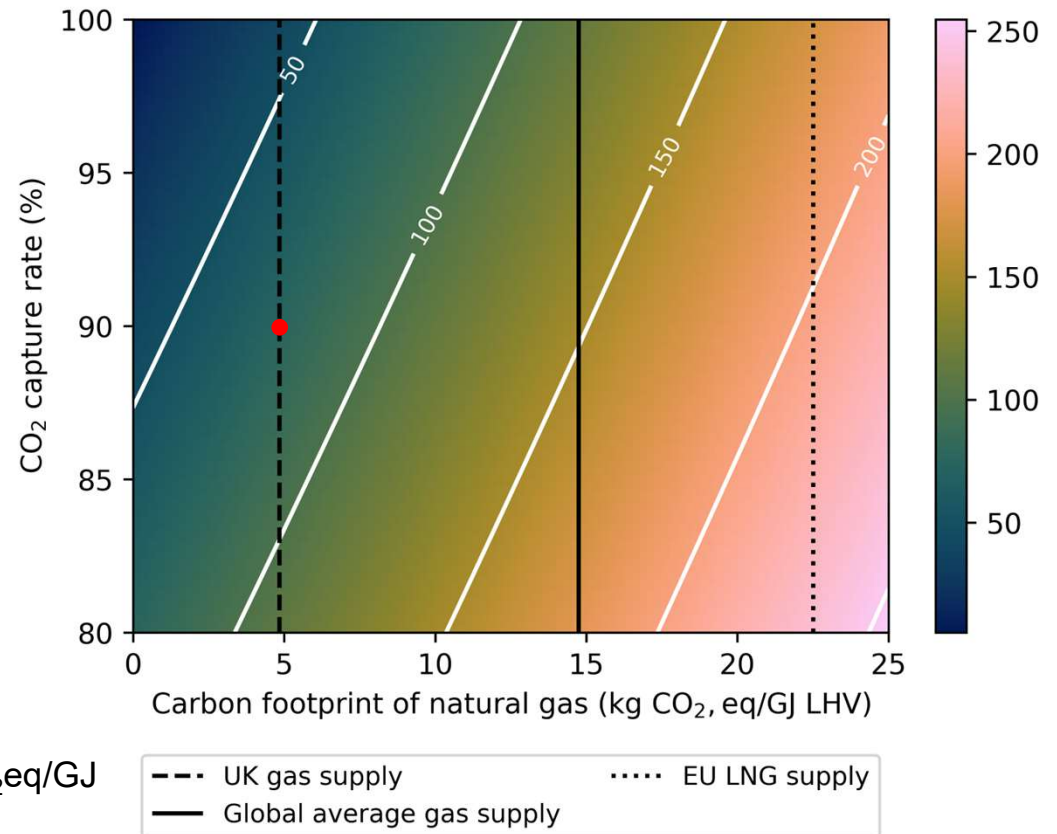
At steady state operation, a CCGT-CCS plant using UK gas would need to capture 82.5% of the CO₂ to meet the 100 kg CO₂eq/MWh_{el} criteria.

The steady state CO₂ intensity of a CCGT-CCS using UK gas with a 90% capture rate is **75.2 kg CO₂eq/MWh_{el}**.

UK supply chain carbon footprint of natural gas = 4.9 kg CO₂eq/GJ LHV (Wernet et al. 2019)

Natural gas CCGT-CCS

Carbon footprint of CCGT-CCS (kg CO₂, eq/MWh)

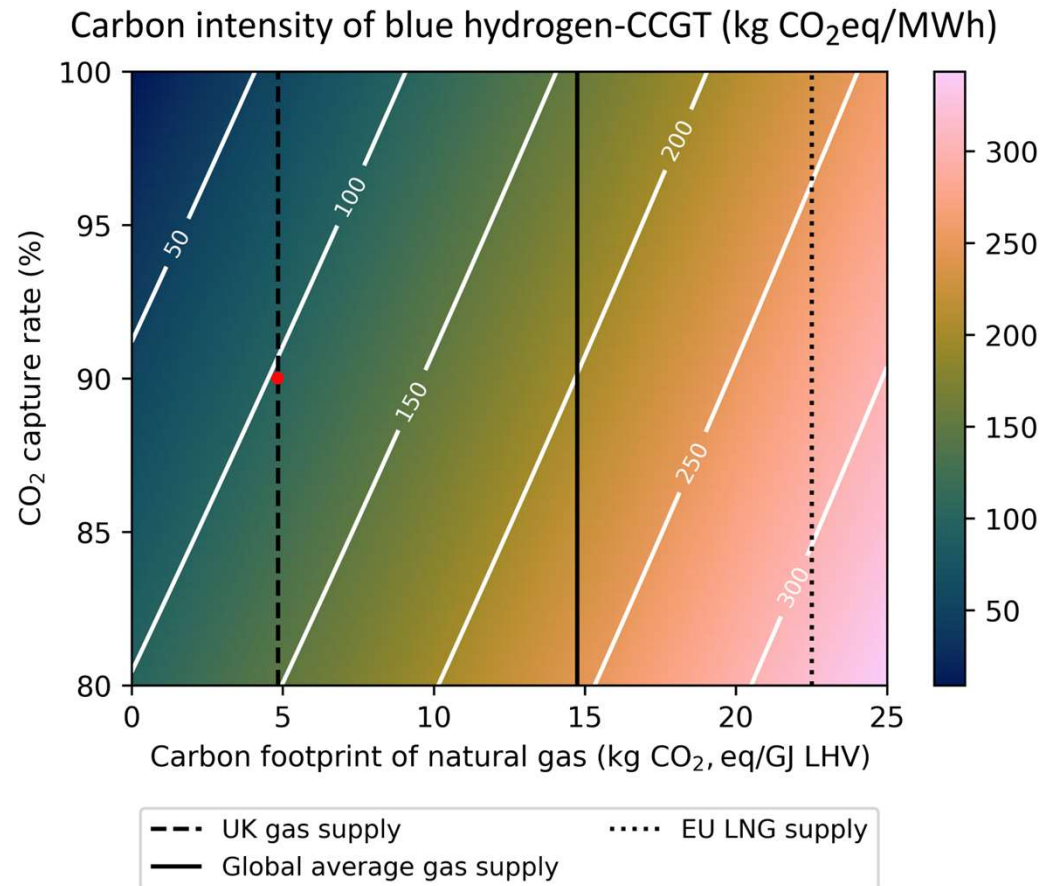


Using UK natural gas for SMR retrofitted with CCS and capturing 90% CO₂ to produce hydrogen for a steady state CCGT results in a CO₂ intensity of **103 kg CO₂ eq/MWh_{el}**.

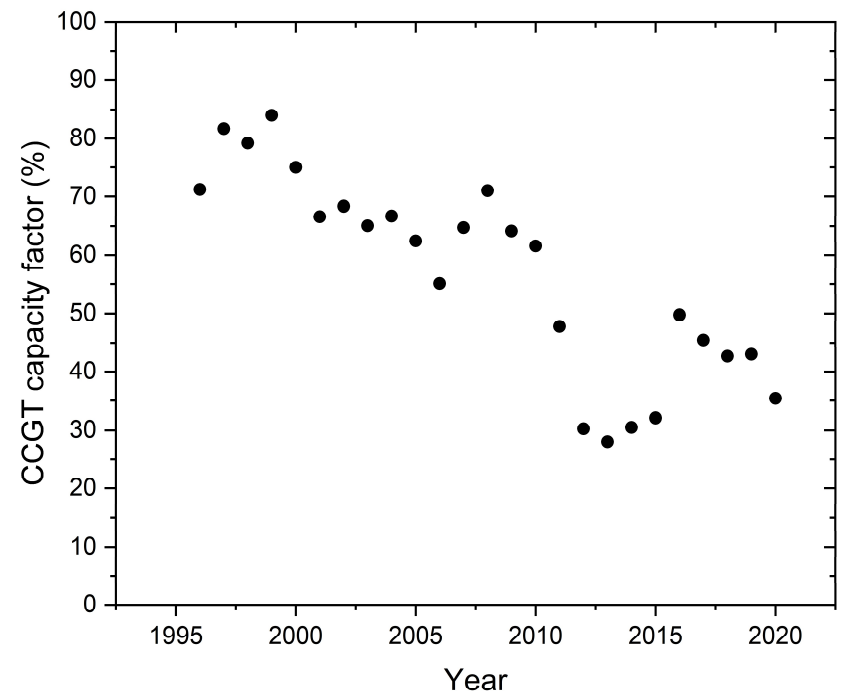
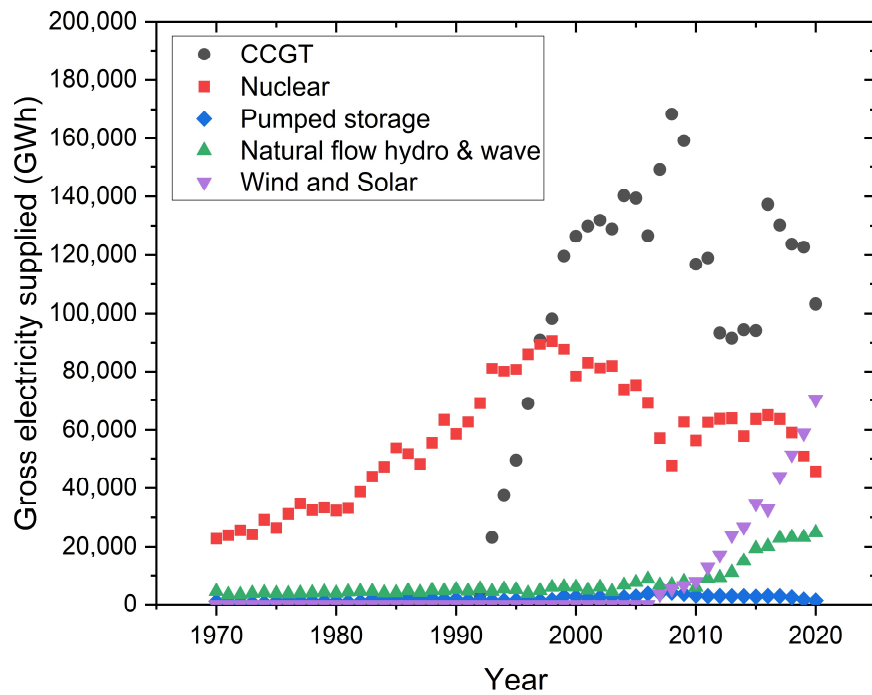
To satisfy the green taxonomy, need to use: (i) >91% CO₂ capture rate, (ii) reduce natural gas supply chain emissions, or (iii) use green hydrogen.

Assuming a CO₂ capture rate of 95% could achieve 80 kg CO₂ eq/MWh_{el} with a blue hydrogen-CCGT.

Hydrogen CCGT-CCS



Gross electricity supply and average annual capacity factor of UK gas-CCGT plants

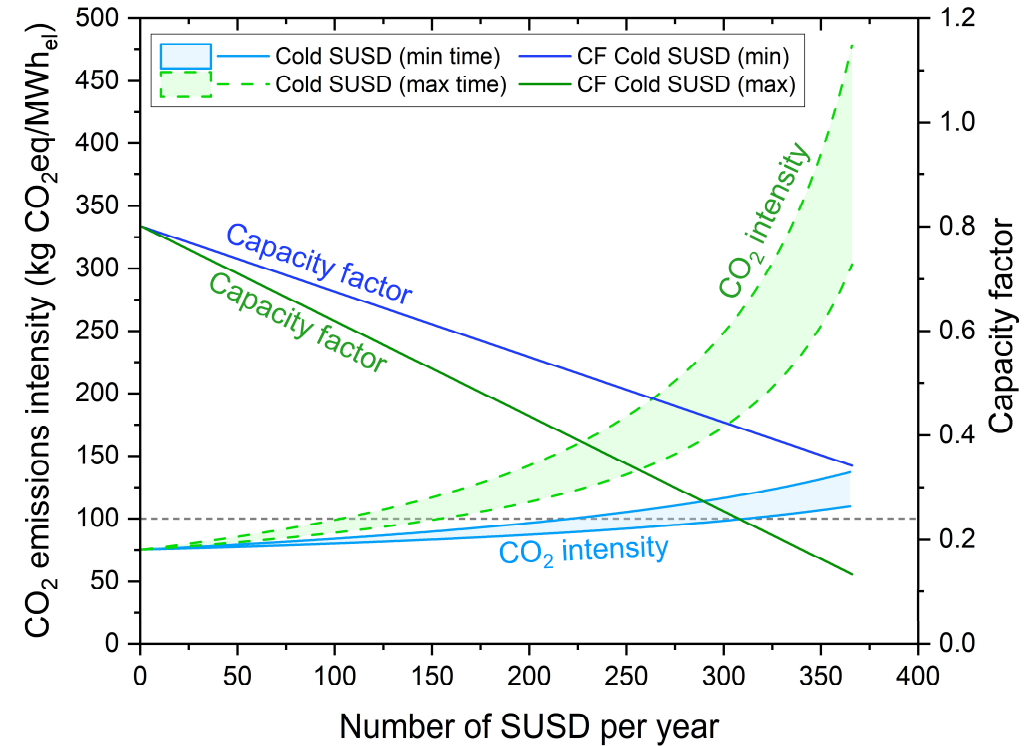
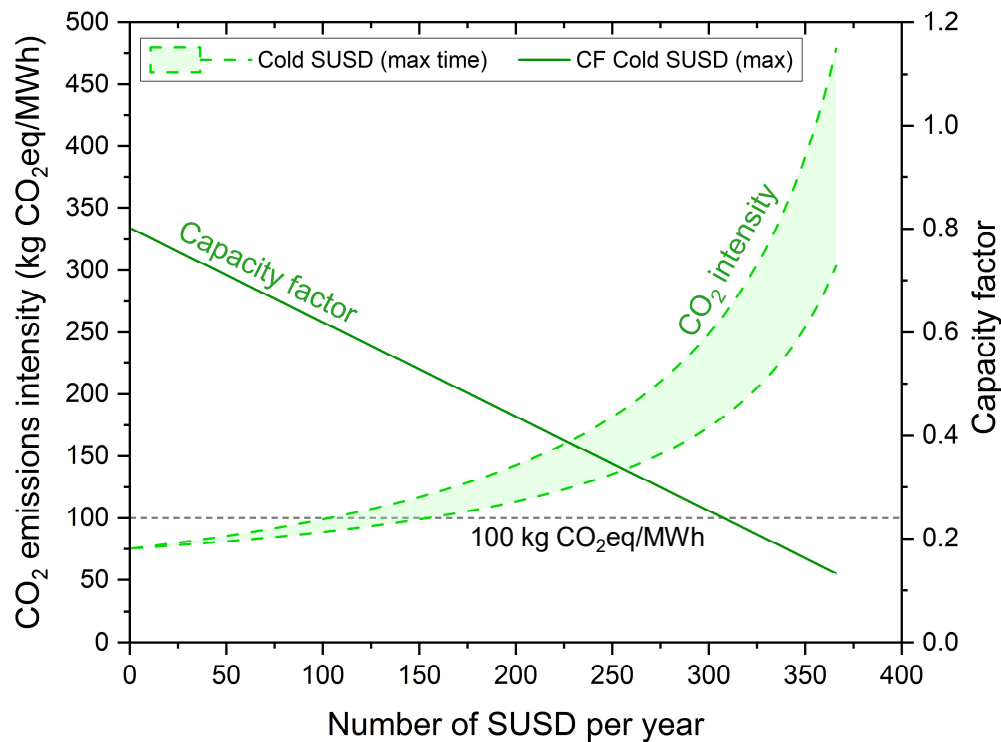


Flexibility Requirements of gas power plants

		OCGT	Recips	CCGT
Efficiency	%	<40%	<40%	<63%
Plant size	MW	1 – 299	5 – 49	500 to 2500
Location / scale		Utility or industrial, centralised or decentralised	Industrial	Centralised / utility
Operating mode		Peaking	Peaking	Baseload / shifting
Number of starts	#	350 – 700	350 – 700	50 – 300
Hours per year	hrs/yr	500 – 2000	500 – 2000	4000 – 8500
Start time to min load	mins	5 – 10	3 – 4	20 – 90
Start time to max load	mins	20 – 30	6 – 10	60 – 180
CCS connection				
Plant retrofit		☹	☹	☹
Plant new build		☹	☹	☺

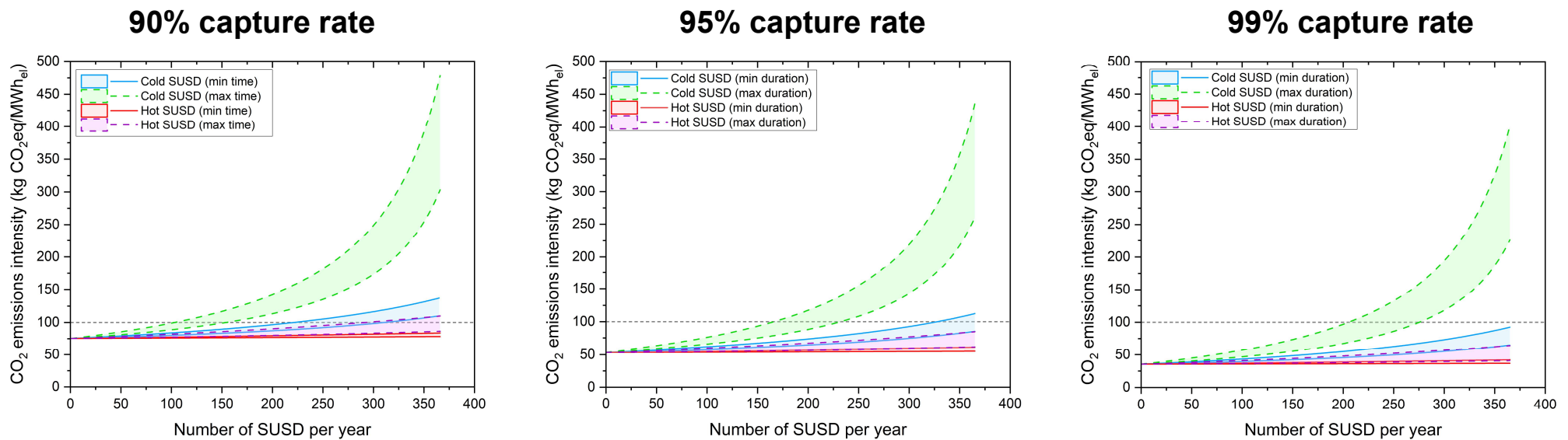
Effect of start-up & shut down on CCGT-CCS emissions

The EU taxonomy proposes an overarching, technology-agnostic emissions threshold of 100 kg CO₂ eq/MWh for electricity generation, heat production and co-generation of heat and electricity.



Effect of start-up & shut down on CCGT-CCS emissions

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As the number of SUSD cycles increases, the CO₂ emissions intensity becomes increasingly higher, and the capacity factor reduces. Higher CO₂ capture rates ensures that taxonomy emissions threshold can be met during flexible operation.

NG CCGT-CCS: Green taxonomy

To remain below 100 kg CO₂eq/MWh_{el}

	Number of start-up and shut down cycles	
90% capture @ steady state	NG auxiliary boiler	Zero emissions aux boiler
Cold SUSD (min duration)	221	311
Cold SUSD (max duration)	102	153
Hot SUSD (min duration)	No limit	No limit
Hot SUSD (max duration)	291	No limit

	Number of start-up and shut down cycles	
95% capture @ steady state	NG auxiliary boiler	Zero emissions aux boiler
Cold SUSD (min duration)	328	No limit
Cold SUSD (max duration)	166	232
Hot SUSD (min duration)	No limit	No limit
Hot SUSD (max duration)	No limit	No limit

Flexibility Requirements of gas power plants

		OCGT	Recips	CCGT
Efficiency	%	<40%	<40%	<63%
Plant size	MW	1 – 299	5 – 49	500 to 2500
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CCS connection				
Plant retrofit		☹	☹	☹
Plant new build		☹	☹	☺

Conclusions

With higher penetration of renewable energy, thermal power plants with CCS could have an important role in providing low carbon, dispatchable electricity.

Understanding the potential impact of key process decisions on the prospects of existing and future fossil fuel-based power generation under a green taxonomy will be essential to ensure a cost-effective transition to net zero.

For NG CCGT-CCS, key considerations include reducing methane leakage, high CO₂ capture rates, and minimising the impacts of start-up and shut down cycles performed by the CCGT-CCS plant.

The main advantage of hydrogen-fired CCGT is that SUSD and highly flexible operation will not increase the CO₂ emissions intensity of the electricity. However, the hydrogen fuel needs to be highly carbon efficient to meet the EU taxonomy.

In order for natural gas to play an enduring role in the transition towards net zero, managing GHG emissions from both the upstream natural gas supply chain and the conversion facility is key.

The ability to maximise the CO₂ capture during start-up and shut down reduces residual CO₂ emissions, thus easing the need for CO₂ removal offsets, e.g., from bioenergy with CCS or direct air capture technologies.

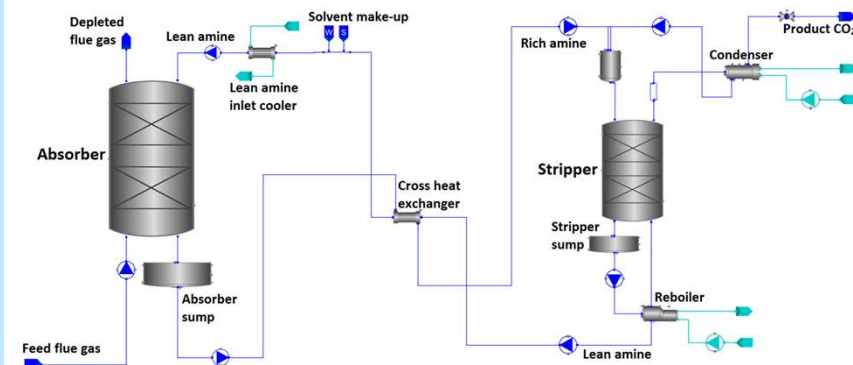
Conclusions and future work

These learnings will help improve the performance of flexible operation and SUSD strategies in CO₂ capture plants.

The data from this study will help in the development more robust process control systems, as well as improve the description of flexible and dynamic operation in process & systems models.

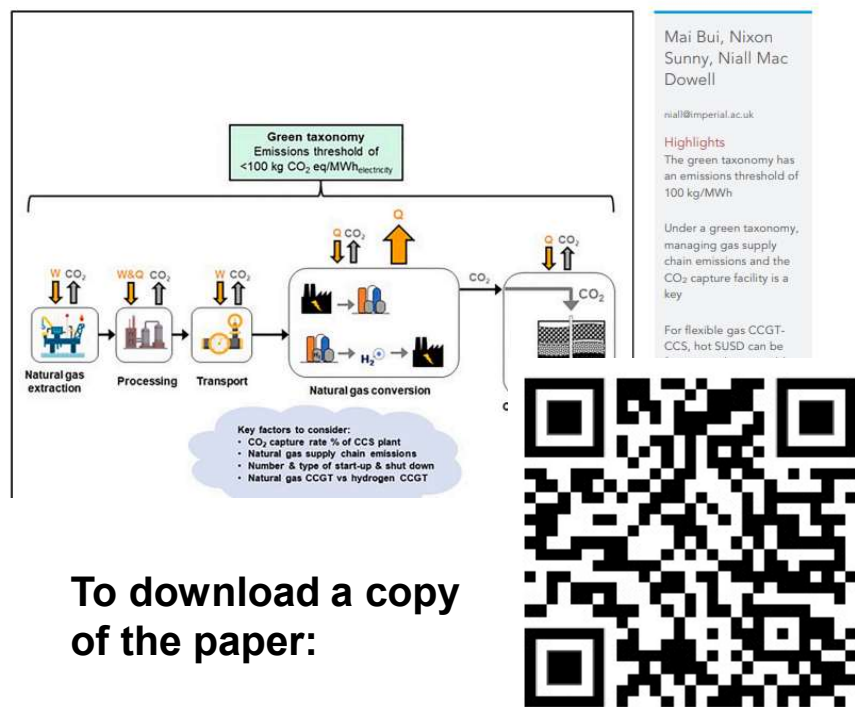
Future work:

- Investigate the impact of different process configurations and process control systems that could improve plant flexibility and SUSD performance, e.g., via process modelling.
- Effect of different solvent types on CO₂ capture plant flexibility and SUSD performance.
- Study dynamic interactions between the power plant and CCS process, also upstream/downstream effects.
- Techno-economic analysis to understand the cost implications of different SUSD strategies.
- Understand the impact of SUSD cycles at a systems scale, i.e., effect on ability to reach net zero.



Article

The prospects of flexible natural gas-fired CCGT within a green taxonomy



Evaluating technology options to mitigate greenhouse gas emissions

IEAGHG Technical Report
2022-08
August 2022

Start-up and Shutdown Protocol for Natural Gas-fired Power Stations with CO₂ Capture

To request a copy of the IEAGHG report, please email tom.billcliff@ieaghg.org with the report reference number **2022-08**