

Enabling Low Carbon Feedstocks for Gasification (FWP-FEAA437)

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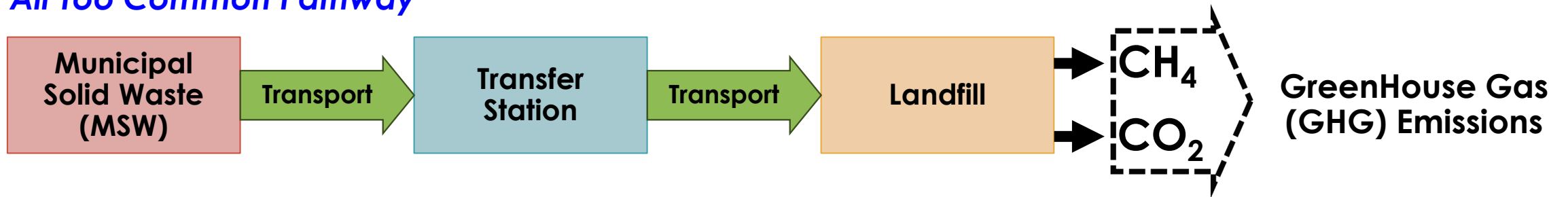
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Energy and Carbon Management (FECM) for
guidance and support of this project**

Municipal Solid Waste (MSW) Pathways

All Too Common Pathway

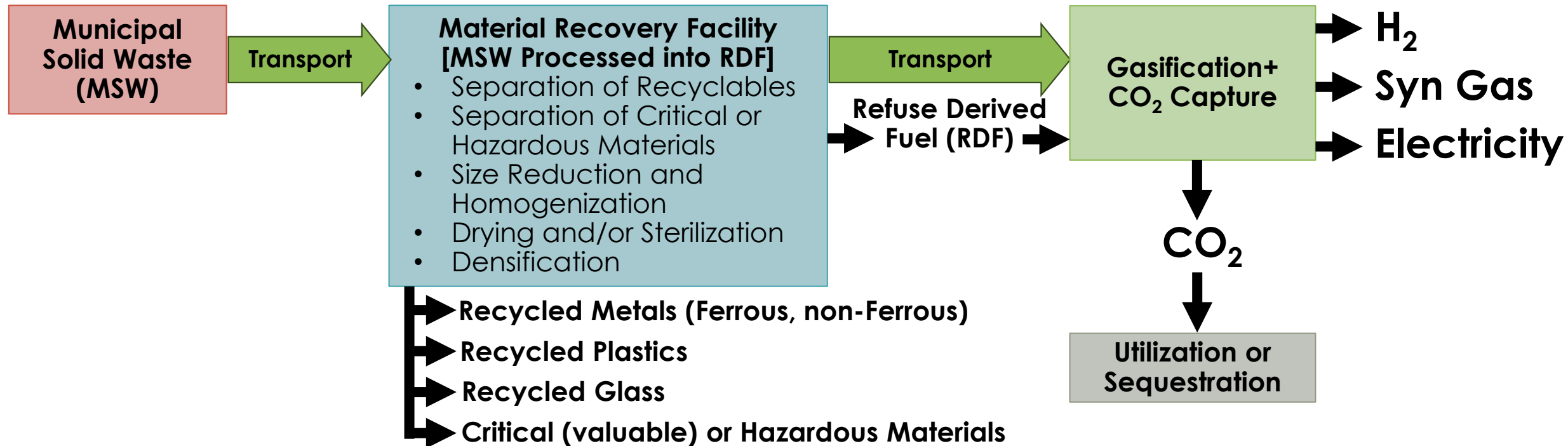


GreenHouse Gas	Global Warming Potential	Lifetime in Atmosphere
CO ₂	1 (@100-year time-scale)	300-1000 years
CH ₄	28 (@100-year time-scale)	7-12 years

14% of U.S. CH₄ emissions are from Landfills*

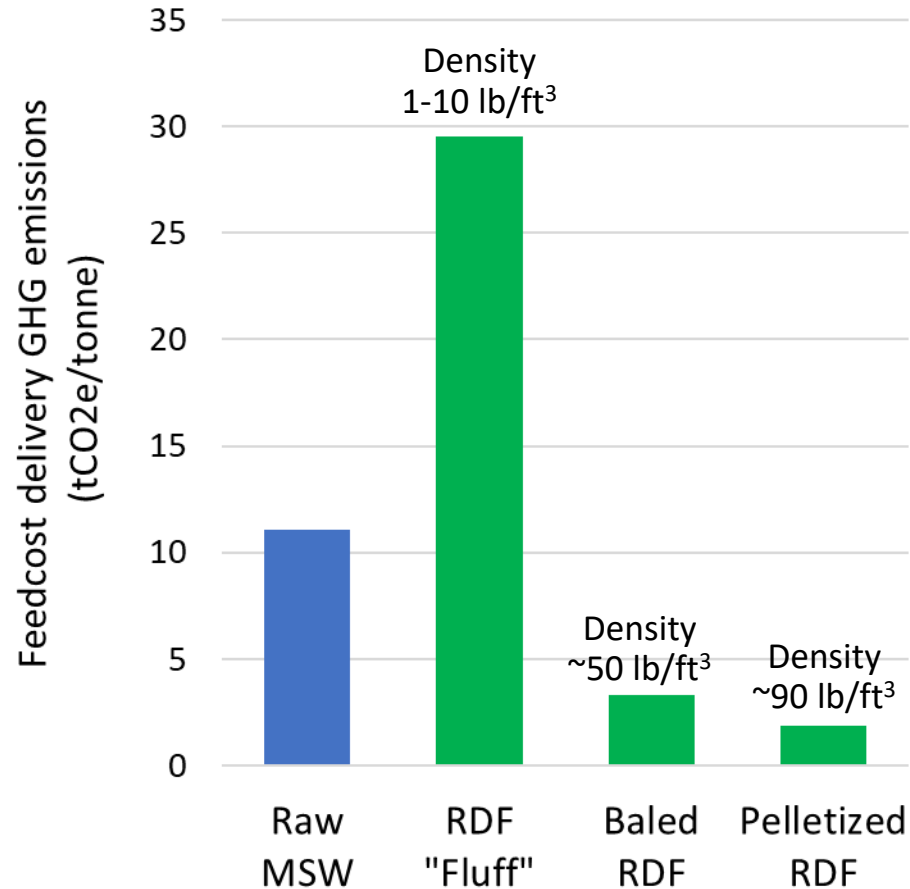
Municipal Solid Waste (MSW) Pathways

Preferred Pathway with Material Valorization, CH₄ and CO₂ Avoidance, and Clean Energy Products



Transport of MSW/RDF Affects Cost & Life Cycle Emissions

- Transportation (100-mile case shown) of MSW and RDF adds cost and GreenHouse Gas emissions
- Moisture content and density are primary factors
- Example analysis shown based on nominal values
 - MSW: 40-60% moisture
 - RDF: 5-15% moisture
- Analysis assumes natural gas for drying process



Analysis Details:

- The feedstock delivery emissions are associated with MSW drying, pelletization, and transportation operations.
- Drying GHG emissions are calculated using a natural gas emissions factor of 53.06 kgCO₂e/MMBTU.
- Energy use for pelletization was 12.1 MJ/ton assumed to be supplied via electricity.
 - An average U.S. grid emissions intensity of 0.37 kgCO₂/kWh was used.
- Transportation emissions are computed using the emissions factor of 1001 kgCO₂e/TEU-mi.

References:

- www.epa.gov/system/files/documents/2023-03/ghg_emission_factors_hub.pdf
- www.sciencedirect.com/science/article/pii/S0196890416000224
- www.transportation.gov/sites/dot.gov/files/docs/emissions_analysis_of_freight.pdf

Industry Partner: Ekamor Resource Corporation

- A continuous process for treating (recycle separation & dewatering) MSW to create RDF
- 75+% less energy consumption vs. thermal-based processes
- MSW “dewatered” to RDF with <15% moisture content



Ekamor Facility in Cookeville, TN



*New Name
in 2024*



*Vertical Shaft Impactor
(dewatering and size reduction unit operation)*



*RDF Fluff
(Processed MSW)*



*Pelletized RDF
(easy to transport and feed)*



*Baled RDF
(plastic wrap seal enables
excellent long-term storage)*

Research of Feedstock Physical and Chemical Properties during Gasification Enables Improved Gasifier Design and Control

Feedstock Characterization with ORNL Materials Science Expertise including Neutron Science Facilities



Critical Parameters, Validation Data, Design Guidance

Gasifier Reactor Modeling with NETL Computational Fluid Dynamics Expertise (MFiX)



De-watered and pelletized RDF from Ekamor

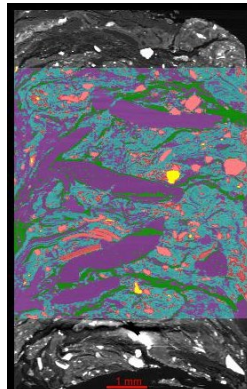


- Properties:**
- Morphology
 - Porosity
 - Density
 - Chemical composition
 - Catalytic effects
 - Ash effects

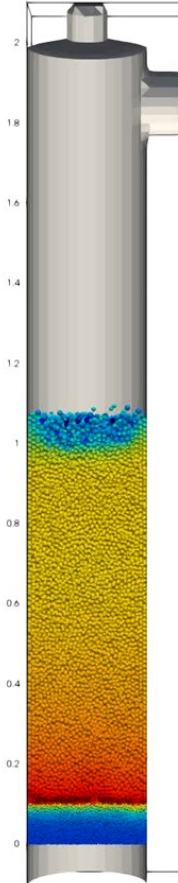


Low-carbon life-cycle feedstocks:

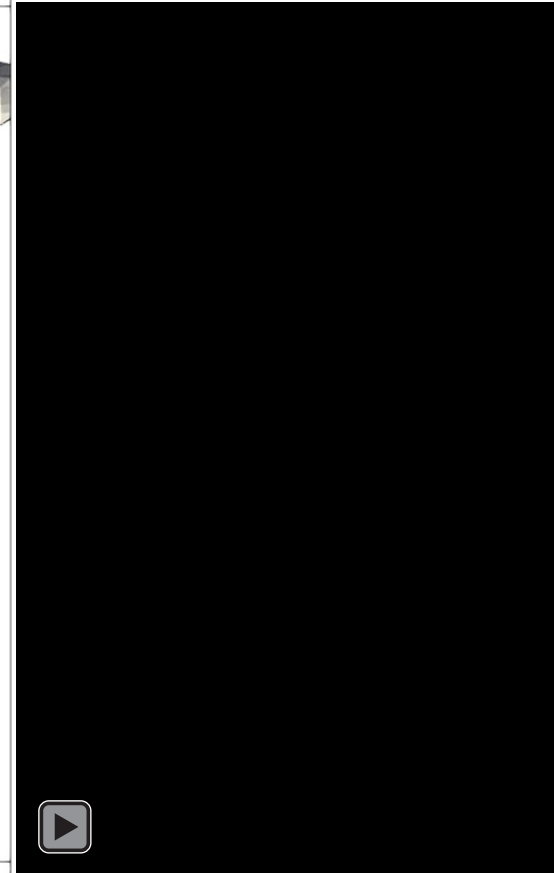
- Municipal Solid Waste (MSW)
- Sustainable Biomass
- Waste Plastics
- Food Waste
- Waste Coal



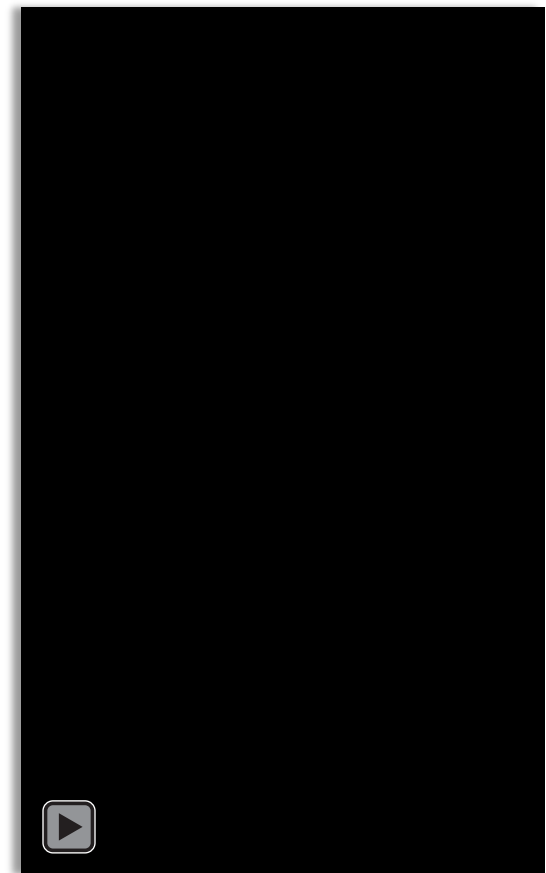
200 KW



5 MW

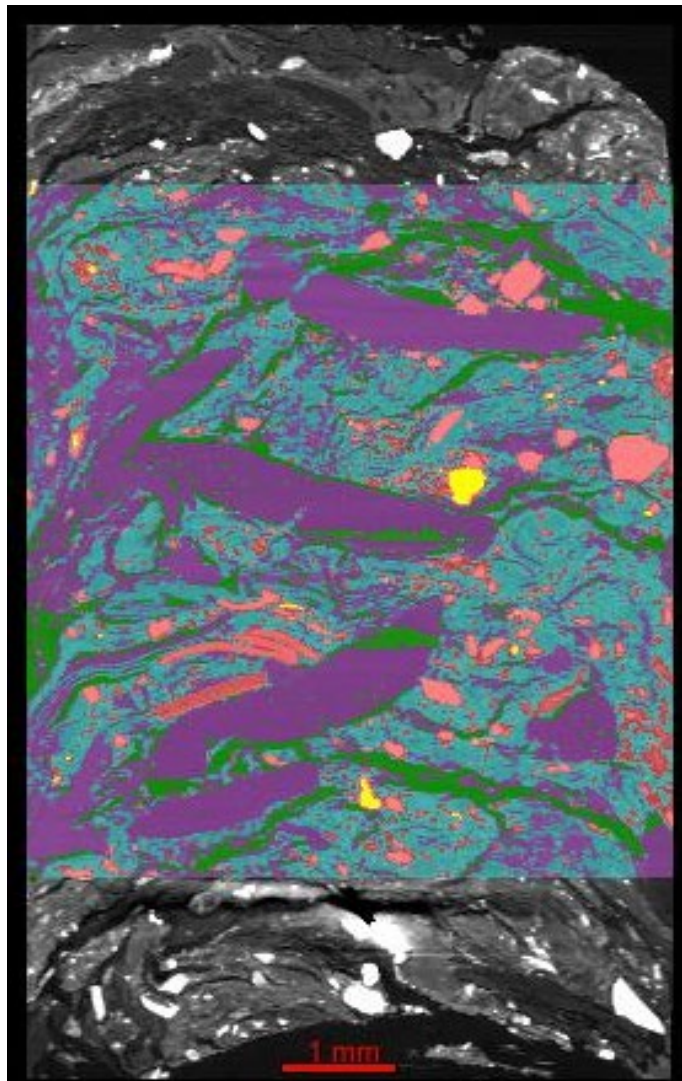


22 MW



MFiX models of a 200kw, 5MW and 22 MW modular moving bed gasifier at Sotacarbo [NETL graphics courtesy of Mehrdad Shahnam]

X-Ray Computational Tomography (XCT) of Engineered Refuse-Derived Fuel (ERDF)



Ekamor ERDF

Pellet Characteristics:

- 5-6 mm diameter
- Length varies (nominally 1 cm, but fractures shorten)
- Density: 1.1-1.2 g/cm³ (nominally)
- Moisture Content: <15% (raw MSW typically 40-60%)
- Oxygen Content: 20% (nominally)
- Energy Content: ~15 M BTU/ton (for comparison, coal ~24 MBTU/ton)

Empty Space/Air: 9.40 vol.%

Low Absorption Solid: 42.36 vol.%

Medium Absorption Solid: 36.60 vol.%

Med-Hi Absorption Solid: 11.28 vol.%

High Absorption Solid: 0.36 vol.%

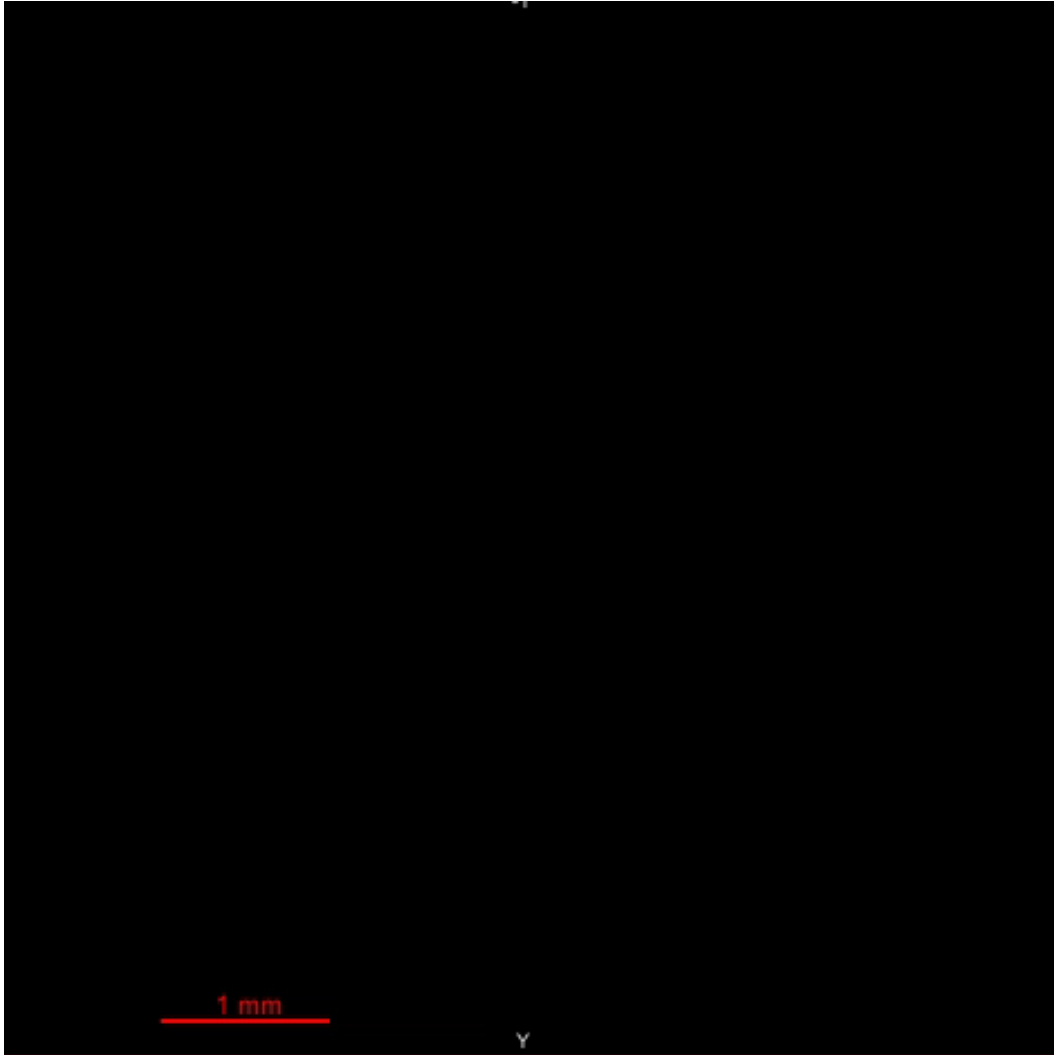
*Engineered Refuse-Derived Fuel (ERDF):
De-watered and Pelletized Municipal
Solid Waste (MSW) from Ekamor*



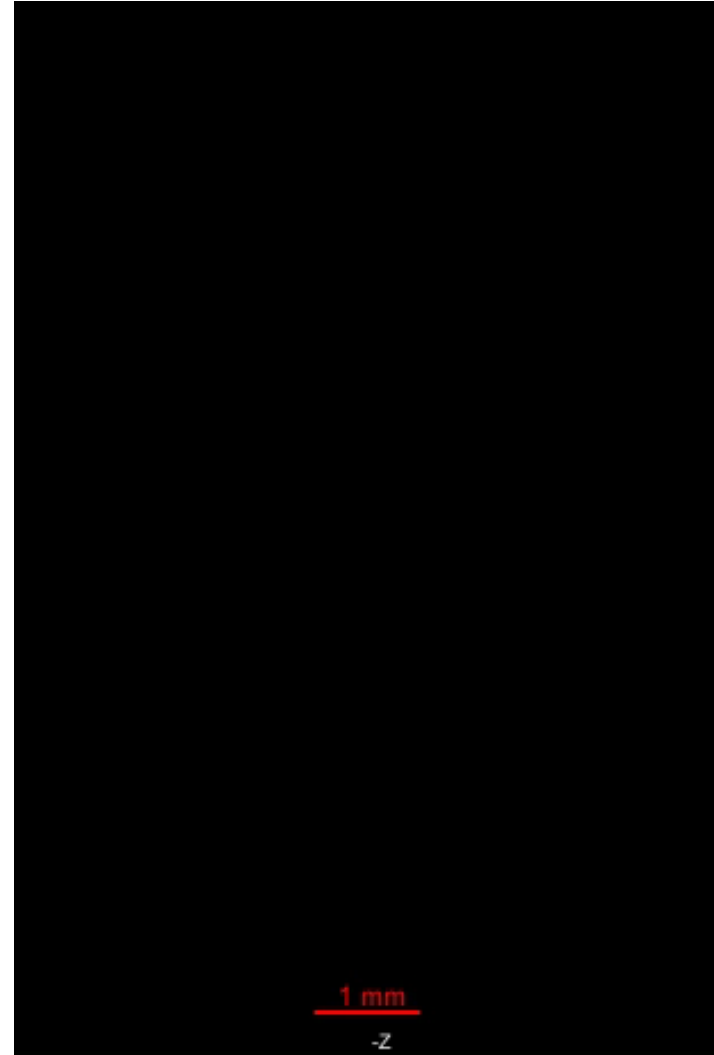
- *Most metal, glass, and large plastics are removed (for recycling) prior to drying and pelletization*
- *Size reduction of MSW components occurs during processing (homogeneity benefit)*

XCT Movies of RDF Pellet

Horizontal Slice Movie

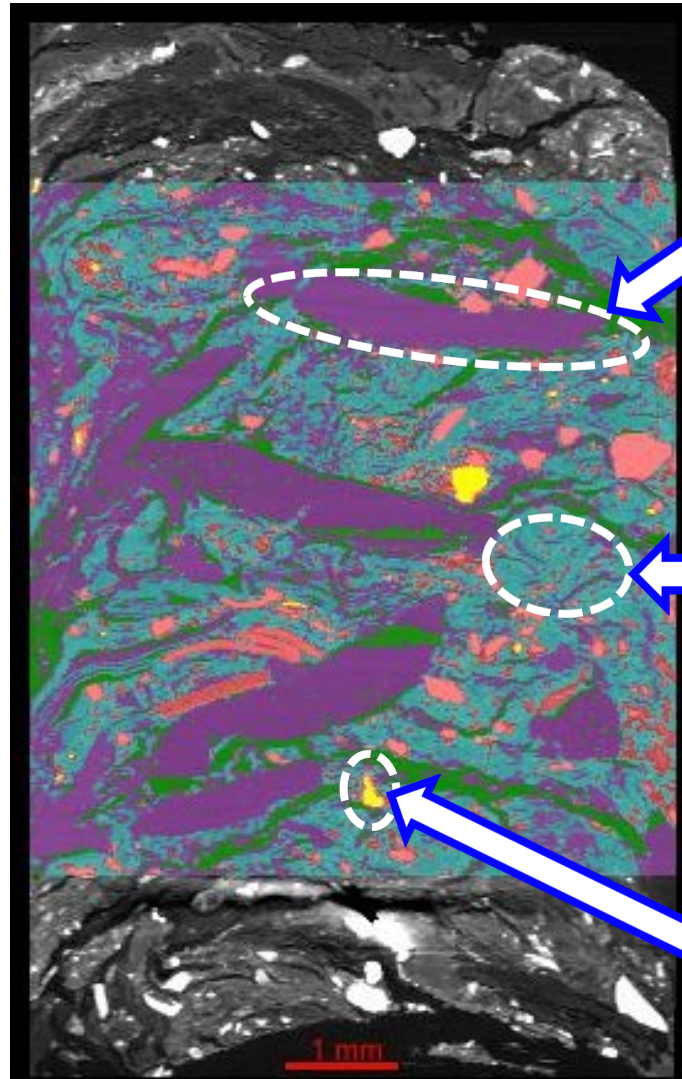


Vertical Slice Movie



In general, high absorption identified by brighter phases correspond to denser/heavier materials

Project Goal: Characterize the physical and chemical transformation of feedstocks for gasification to enable reliable low-cost hydrogen (H₂) and power generation from low-carbon life-cycle and low-cost feedstocks.



Plastics

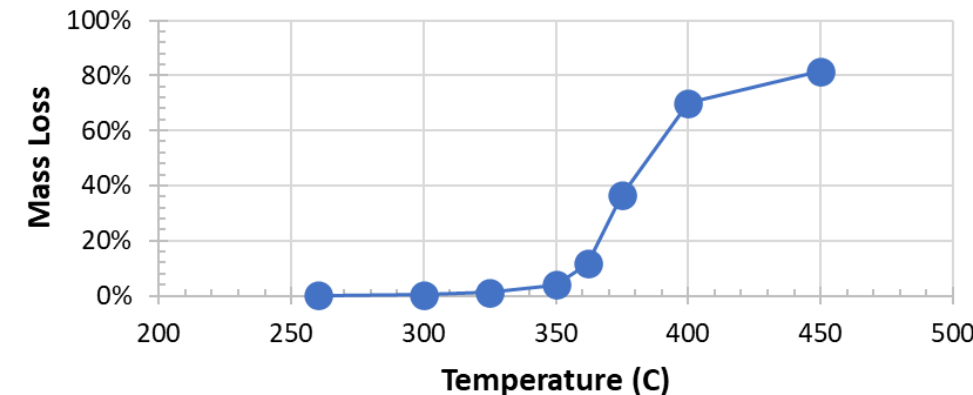
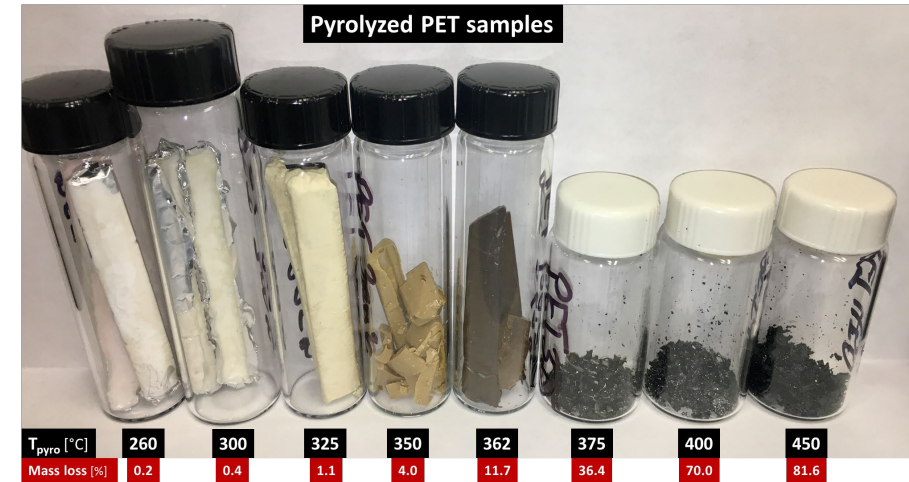
- Long shreds of plastic bags (LDPE) are common
- Relatively low-density component
- Low permeability [e.g. LDPE: $2.89 \cdot 10^{-7}$ kg/(m² Pa. days)]*

Cellulosic Materials

- Diverse sources: paper, cardboard, tissue paper, paper towels, food waste, fabrics
- High permeability [e.g. Kraft paper: $689 \cdot 10^{-7}$ kg/(m² Pa. days)]*

Unknown Materials

- Diverse sources: sand, seeds/food shells, high-density plastics, metal fragments, etc.
- May lead to ash



Morphology/Density vs. Temperature

Porosity/Permeability vs. Temperature

Chemistry vs. Temperature

Neutron-Based Analysis of Gasification of Low C Feedstocks

- Neutron Imaging of Post-Pyrolyzed Samples
- In progress plans for future in situ R&D

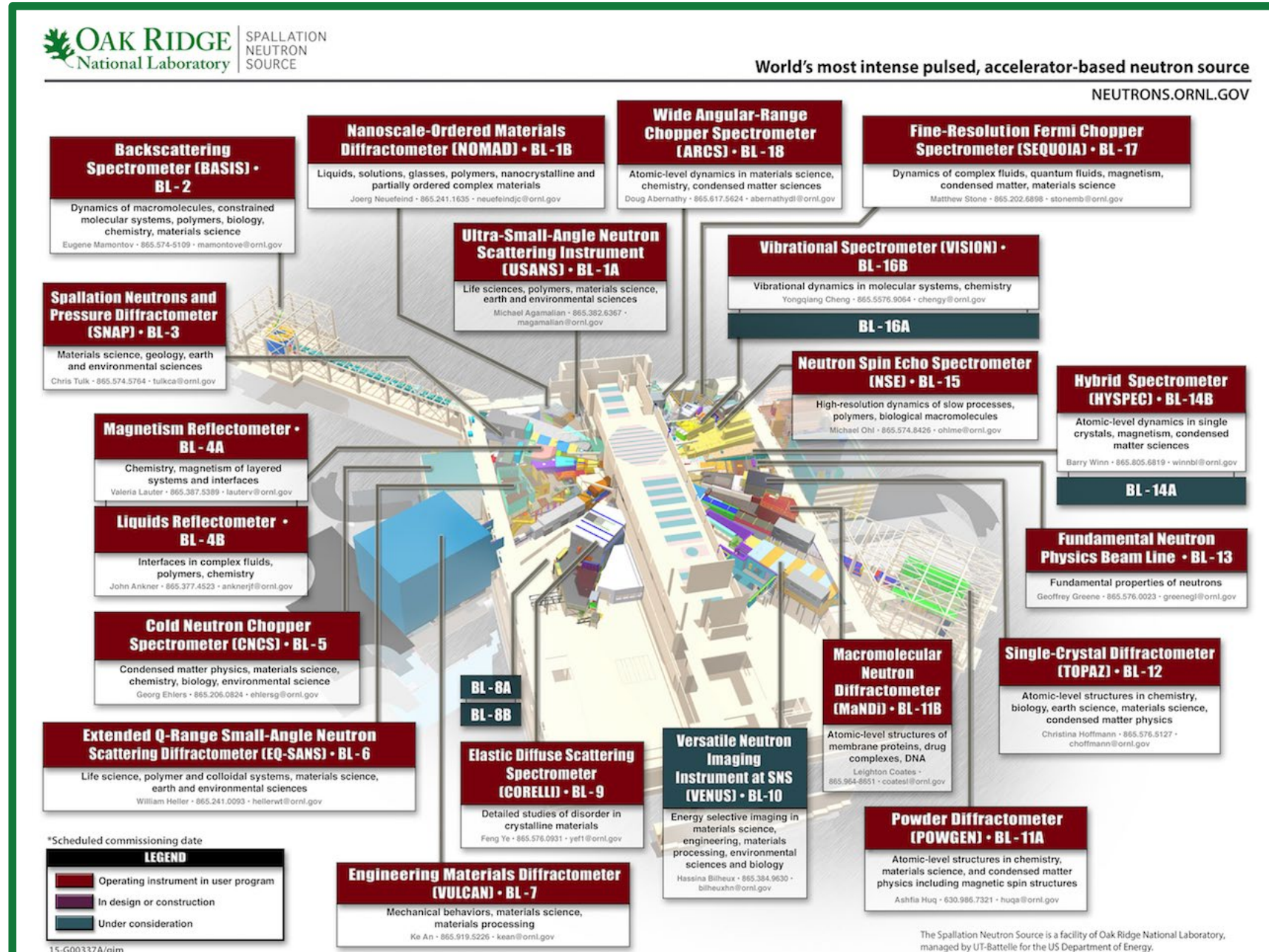


Approach Utilizes Unique Office of Science Neutron User Facilities

Office of Science User Facilities:

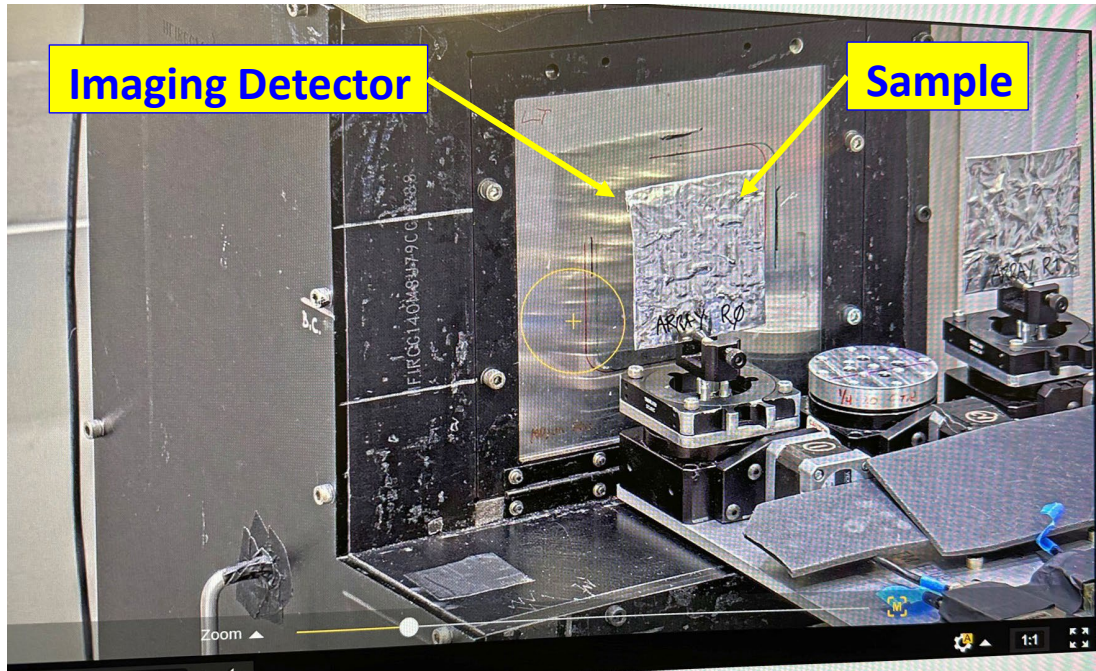
- High Flux Isotope Reactor (HFIR) at Oak Ridge National Laboratory (ORNL)
- Spallation Neutron Source (SNS) at Oak Ridge National Laboratory (ORNL)
- Center for Neutron Research (CNR) at the National Institute of Standards and Technology (NIST)

For more information on beamlines see:
neutrons.ornl.gov
www.nist.gov/ncnr



Neutron Science Techniques Utilized for Feedstock Characterization

Neutron Imaging “Multimodal Advanced Radiography Station” neutrons.ornl.gov/mars



Small Angle Neutron Scattering (SANS) neutrons.ornl.gov/gpsans



Neutron Transmission of Engineered Refuse-Derived Fuel Pellets after Pyrolysis at Set Temperatures



Temperature [°C]

Empty

RT

200

250

300

350

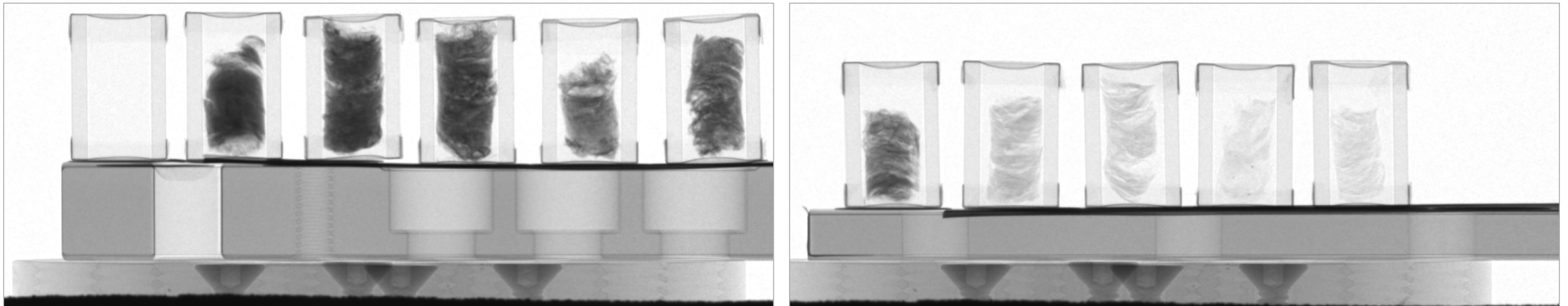
400

500

600

700

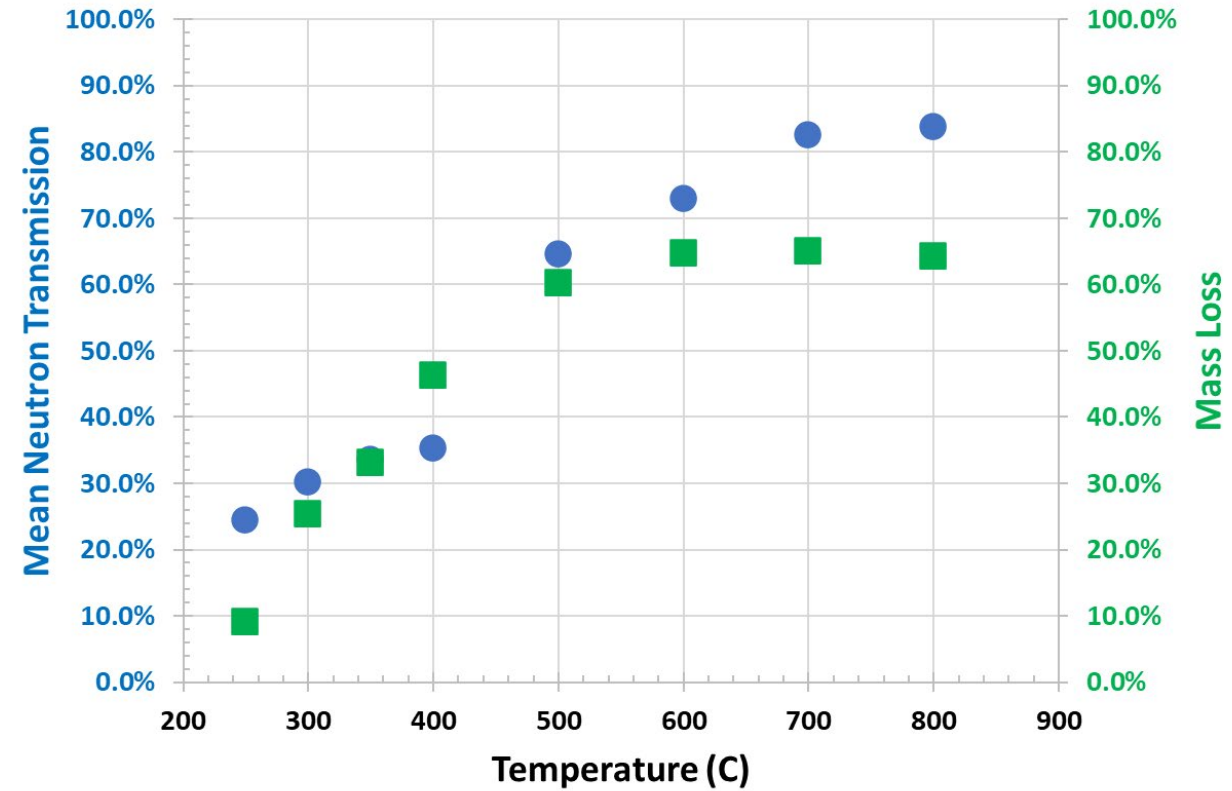
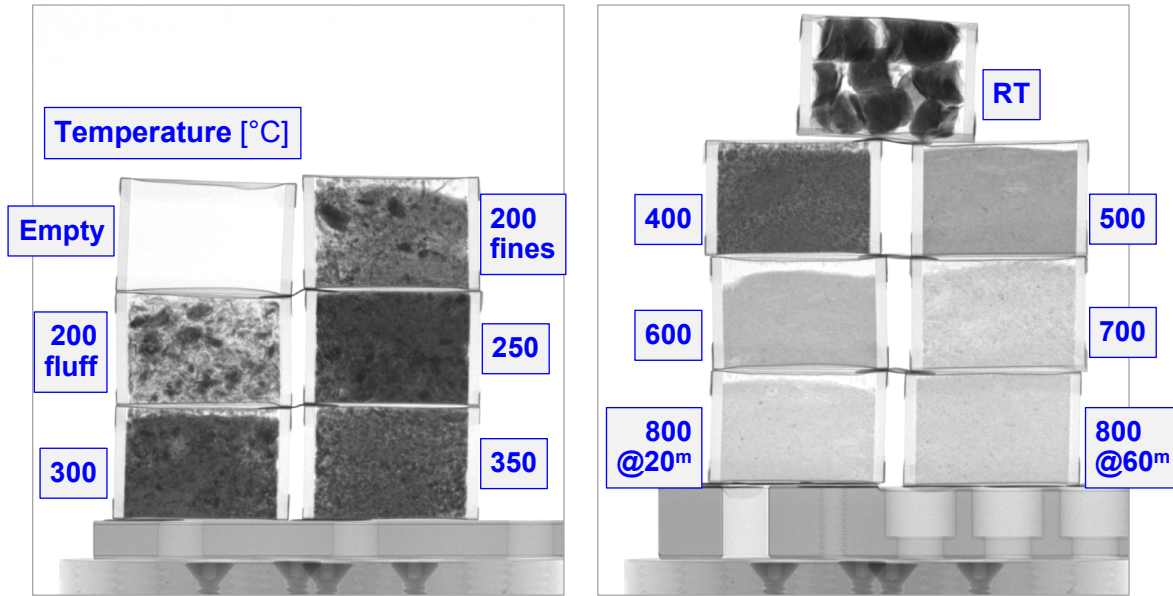
800



Darker images represent samples with higher Hydrogen content (H has highest neutron cross section)

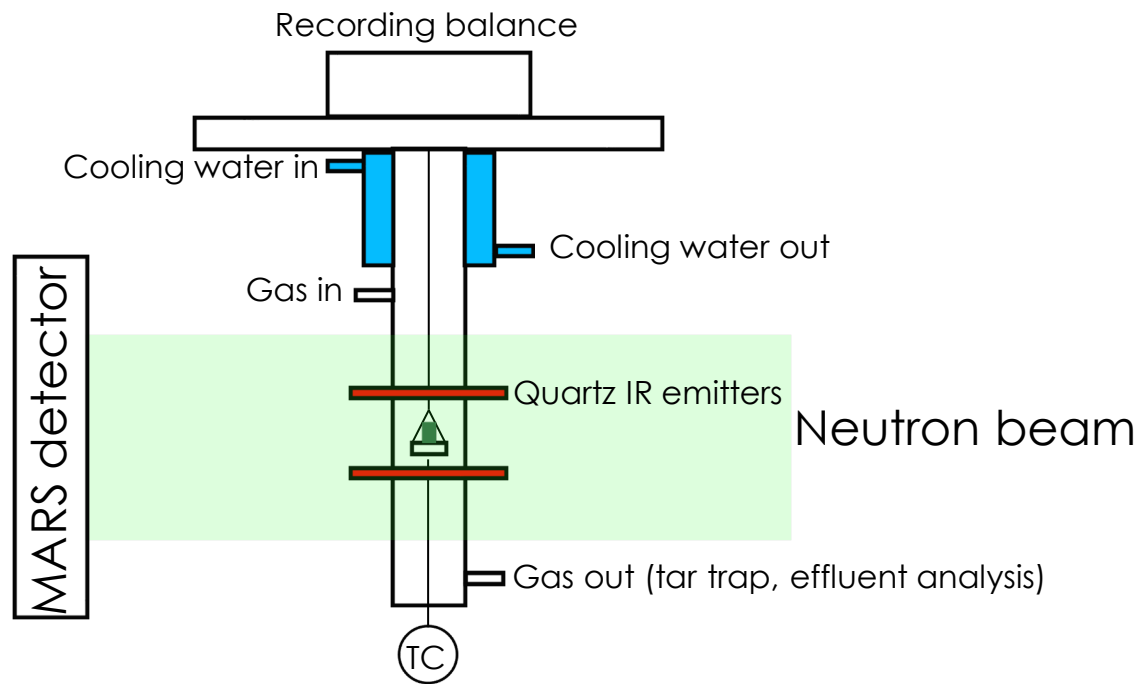
Note: each sample is a different pellet

Neutron Transmission of Pulverized Engineered Refuse-Derived Fuel Pellets after Pyrolysis at Set Temperatures



Design & Construction of in-situ Reactor for Neutron Imaging R&D

- Construction of a dedicated in-situ reactor with thermogravimetric analyzer (TGA) functionality in progress
- Design specialized to enable neutron imaging R&D of pyrolysis and gasification reactions



Heraeus-NobleLight IR Heater

Schematic inset shows gold reflector to direct infrared (IR) radiation at a 45 degree angle to the emitter



Special thanks to Reinhard Seiser of NREL for helpful discussions in the design phase based on his experience building a custom TGA for biomass pyrolysis R&D

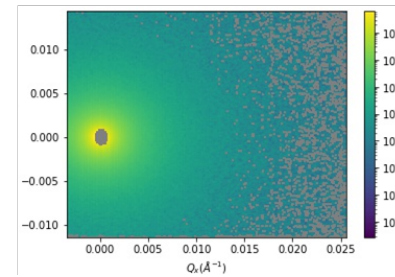
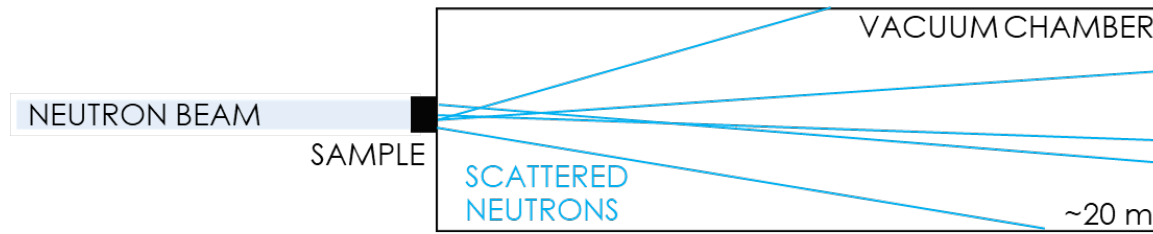
Analysis of Porosity and Permeability during Gasification of Low C Feedstocks

- Small Angle Neutron Scattering (SANS)
- Bench-Scale Permeability Measurement with Pressurized Gas Instrument



Small Angle Neutron Scattering (SANS) of MSW Components as a Function of Pyrolysis Temperature

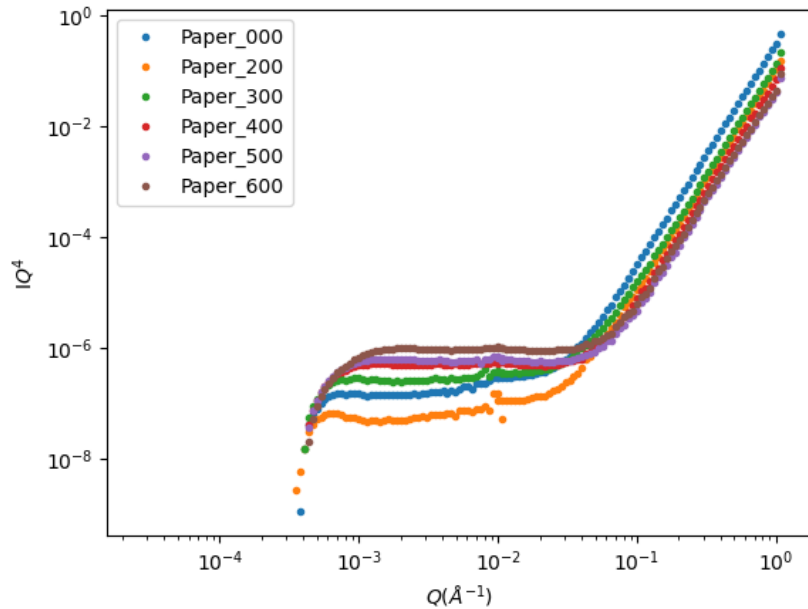
Small Angle Neutron Scattering (SANS)



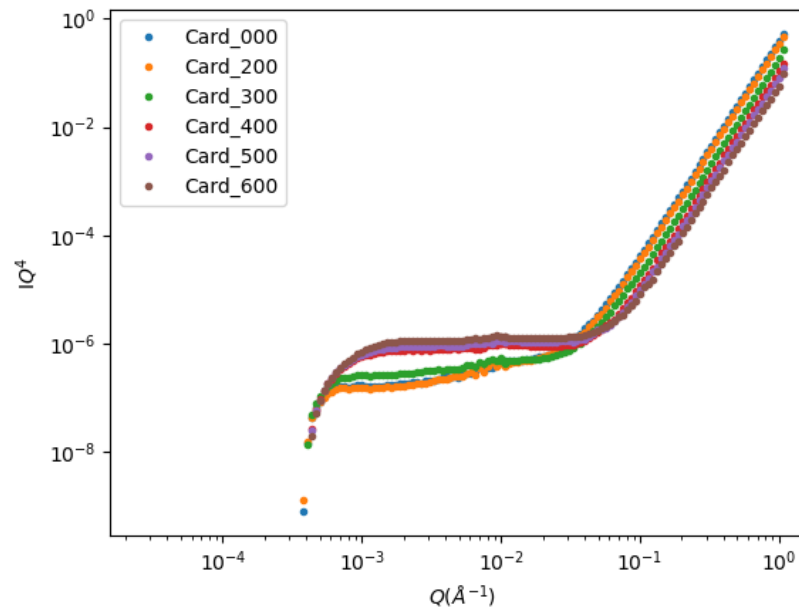
Momentum transfer (Q) is reciprocal of pore size

Q is derived from Bragg's law:
 $|Q| = 4\pi \sin \theta / \lambda = 2\pi / d$

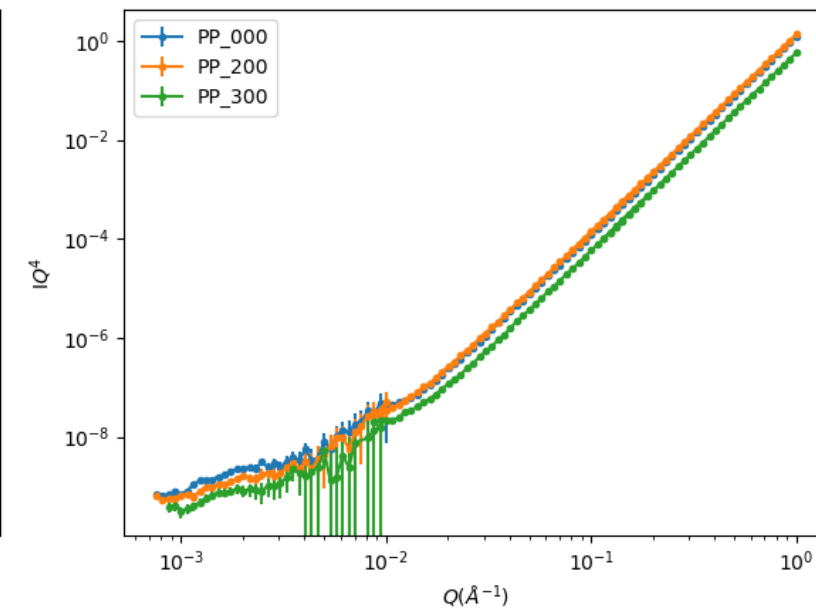
Paper Towel



Cardboard

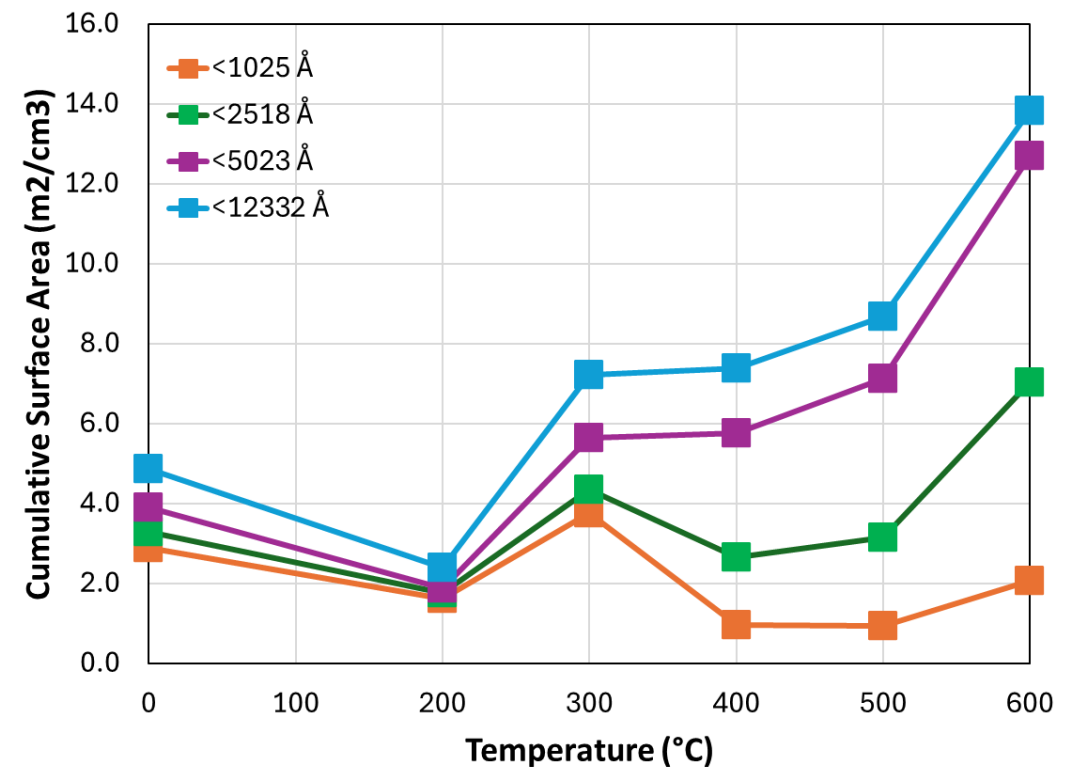
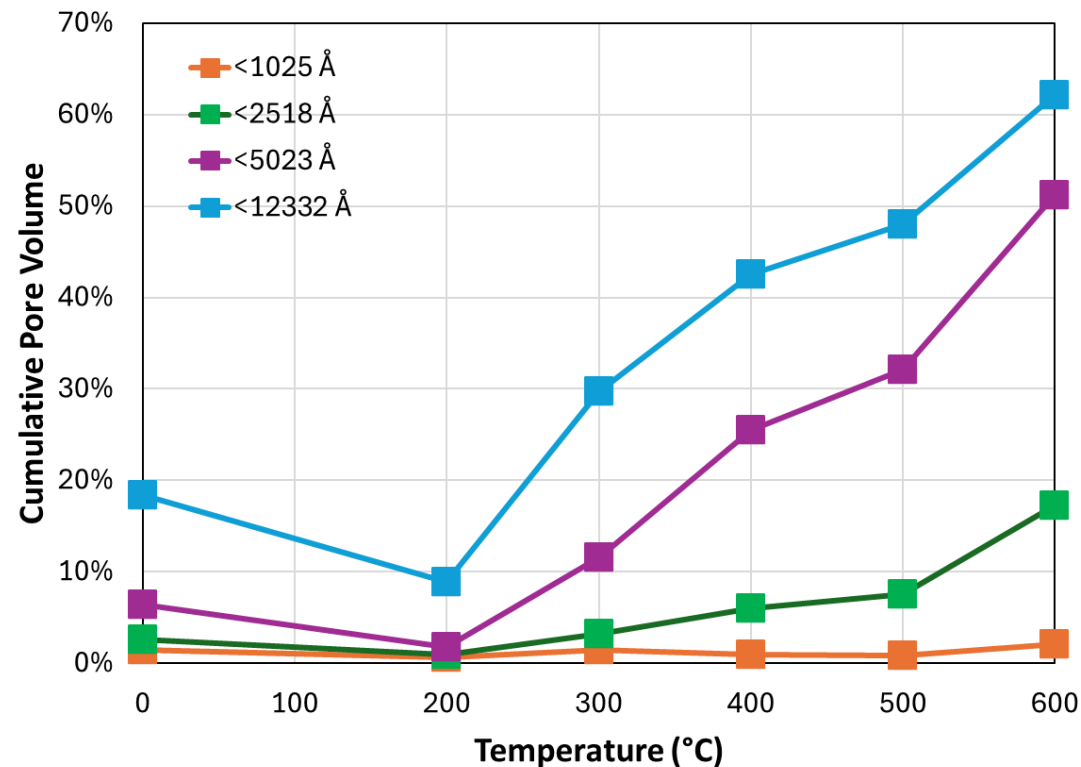


Plastic



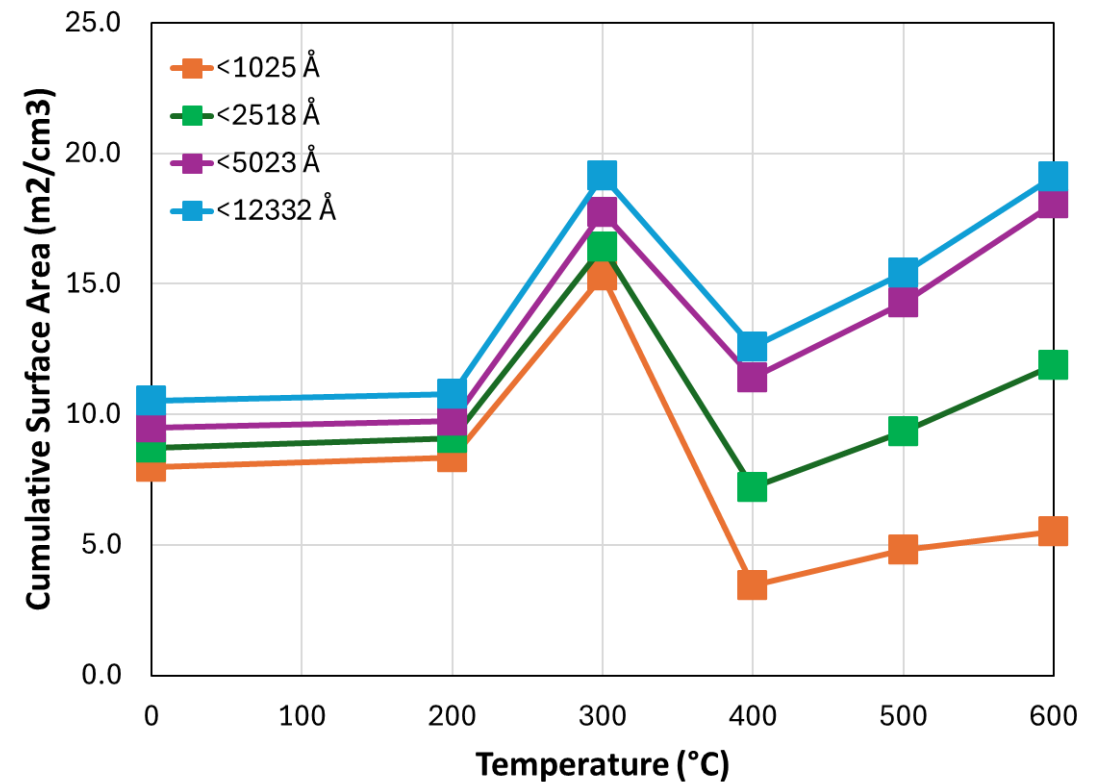
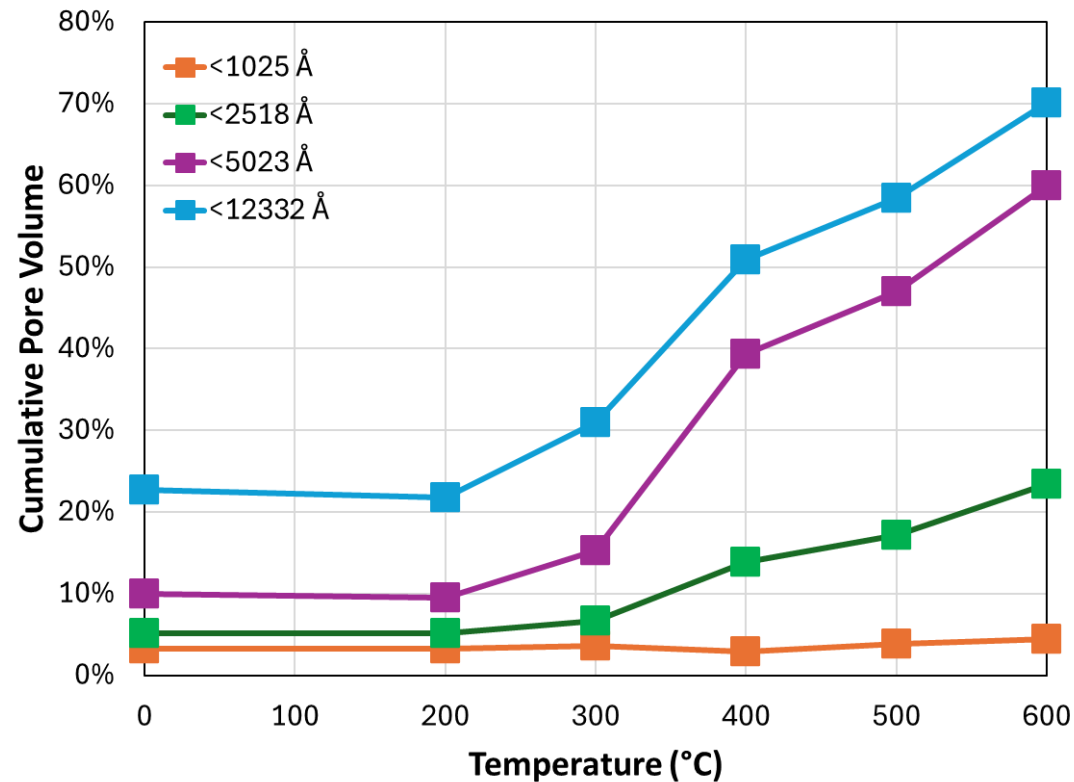
Porosity and Surface Area Changes during Pyrolysis

- Data for **paper towel** sample shown
- Overall, porosity and surface area increase with temperature
- For smaller (<250 nm) pores, there is constriction at intermediate temperatures (400-500°C)



Porosity and Surface Area Changes during Pyrolysis

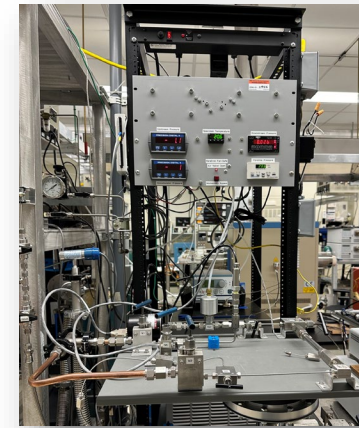
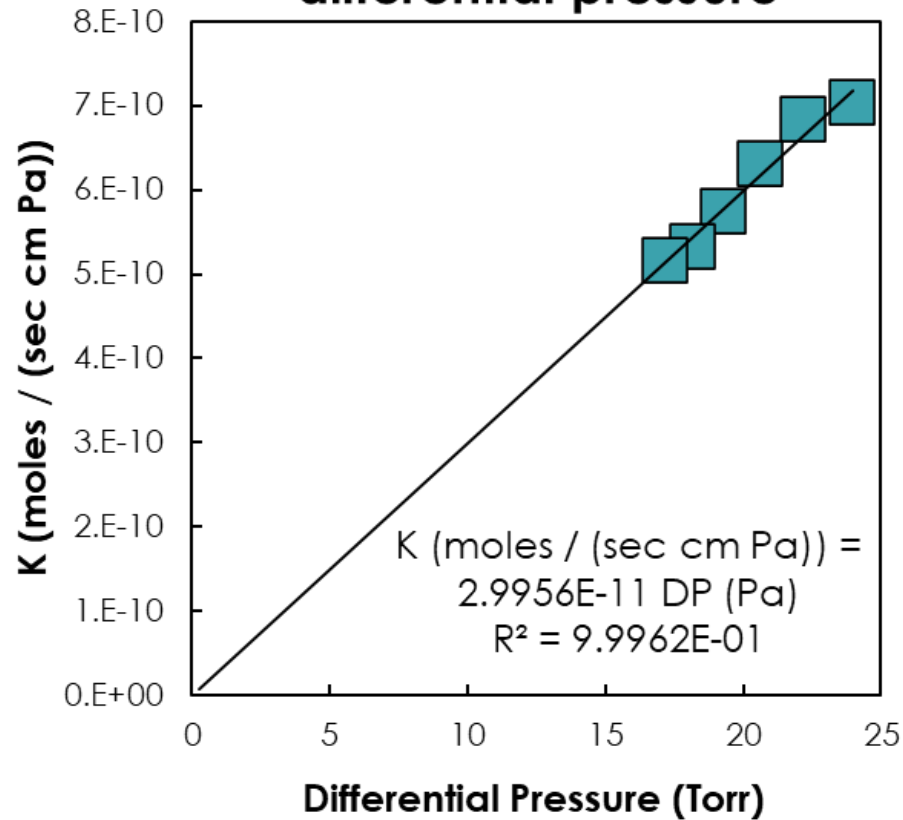
- Data for **cardboard** (corrugated) shown
- Overall, porosity increases with temperature
- Surface area changes are more prominent in 300 to 400°C transition



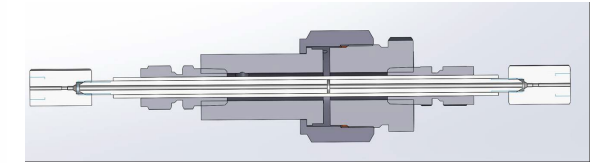
Customized Permeability Analyzer Enables Direct Measurement of Permeability Over Range of Pressures and Gases

N_2 permeability through 0.32mm card stock

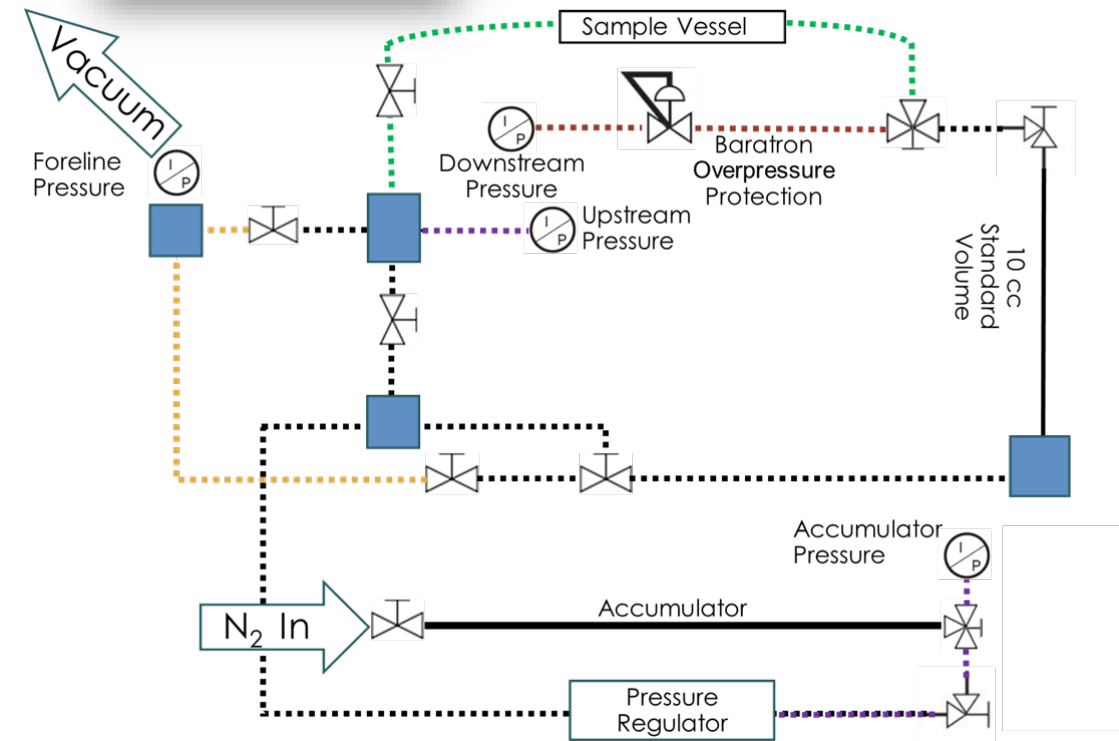
Permeability as a function of differential pressure



Custom Sample Holder Under Construction



Picture (left) and schematic (below) of Permeability Analyzer

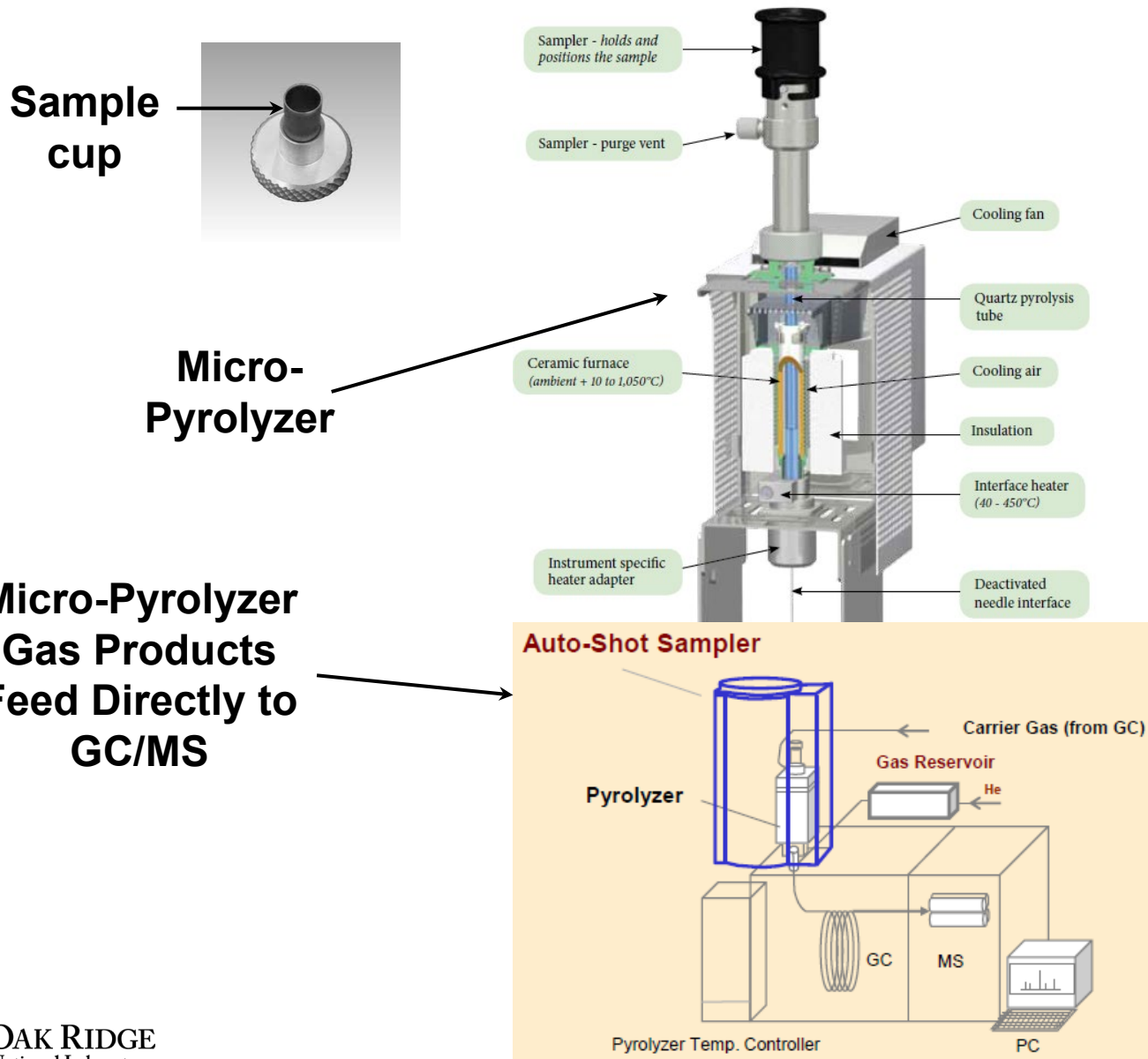


Investigation of Catalytic Effects on Gasification

- Micro-Pyrolysis GC/MS
- Thermo-Gravimetric Analyzer (TGA)



Micro-Pyrolysis Gas Chromatography/Mass Spectrometry (GC/MS) Being Utilized to Study Catalytic Effects on Gasification

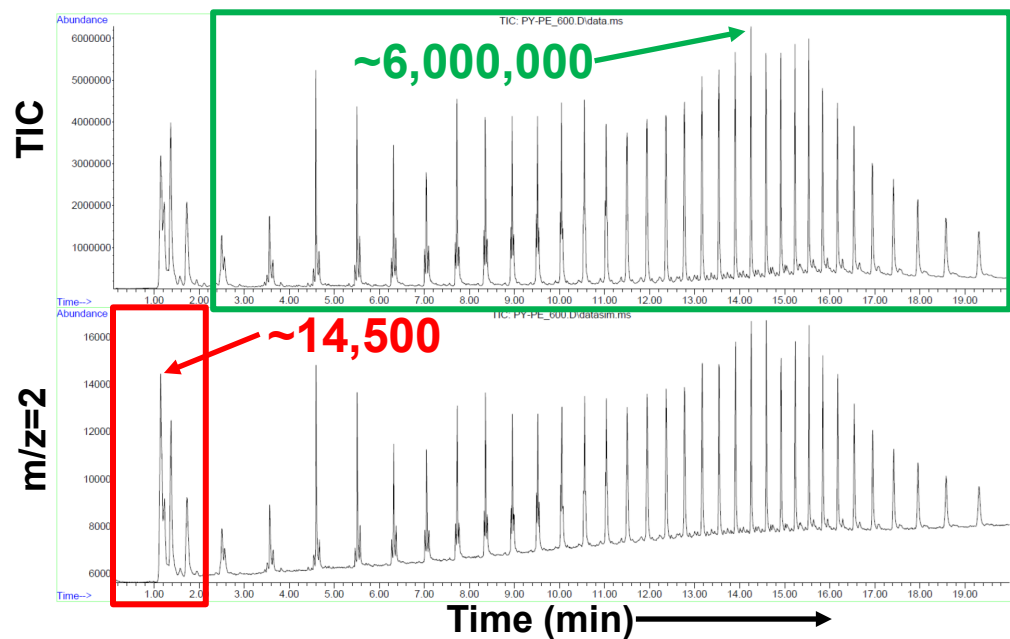


- Bench-scale studies with Micro-Pyrolyzer not directed at specific gasifier design
- Concept of staged pyrolysis and/or gasification may be optimal approach for catalytic strategy and is of particular interest for sustainable feedstocks:
 - S. Nilsson, A. Gomez-Barea, D. Fuentes-Cano, P. Ollero, *Fuel* 2012, **97**, 730-740
 - U. Henriksen, J. Ahrenfeldt, T. K. Jensen, B. Gobel, J. D. Bentzen, C. Hindsgaul, L. H. Sorensen, *Energy* 2006, **31**, 1542-1553
 - S. Heidenreich, P. U. Foscolo, *Progress in Energy and Combustion Science* 2015, **46**, 72-95
- Literature indicates significant interest in catalytic effects:
 - R. A. Arnold and J. M. Hill, *Sustainable Energy & Fuels* 2019, **3**, 656-672
 - Mandal et al., *Energy Fuels* 2019, **33**, 2453-2466
 - K. Tewari, S. Balyan, C. Jiang, B. Robinson, D. Bhattacharyya, J. Hu, *ACS Sustainable Chem. Eng.* 2024, **12**, 4718-4730.

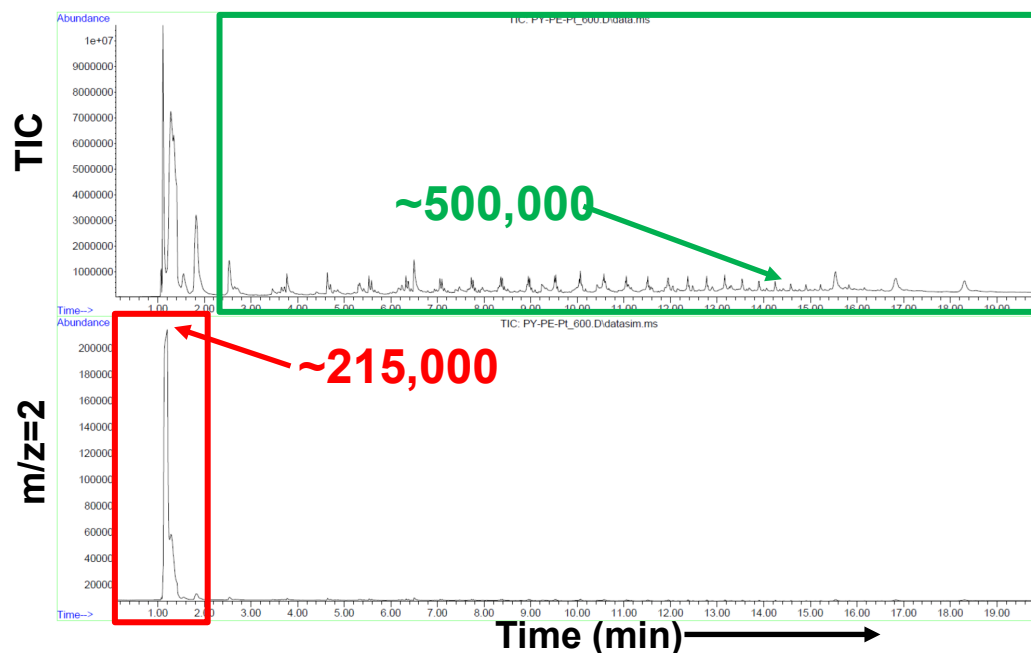
Catalytic Effects on Pyrolysis (no O₂) of Polyethylene

- MicroPy-GC/MS preliminary data shows intended effects of catalyst:
 - **HCs (tar) greatly reduced**
 - **H₂ increases (but difficult to quantify with column used)**

Pyrolysis@600°C, 0% O₂ in He
No Catalyst



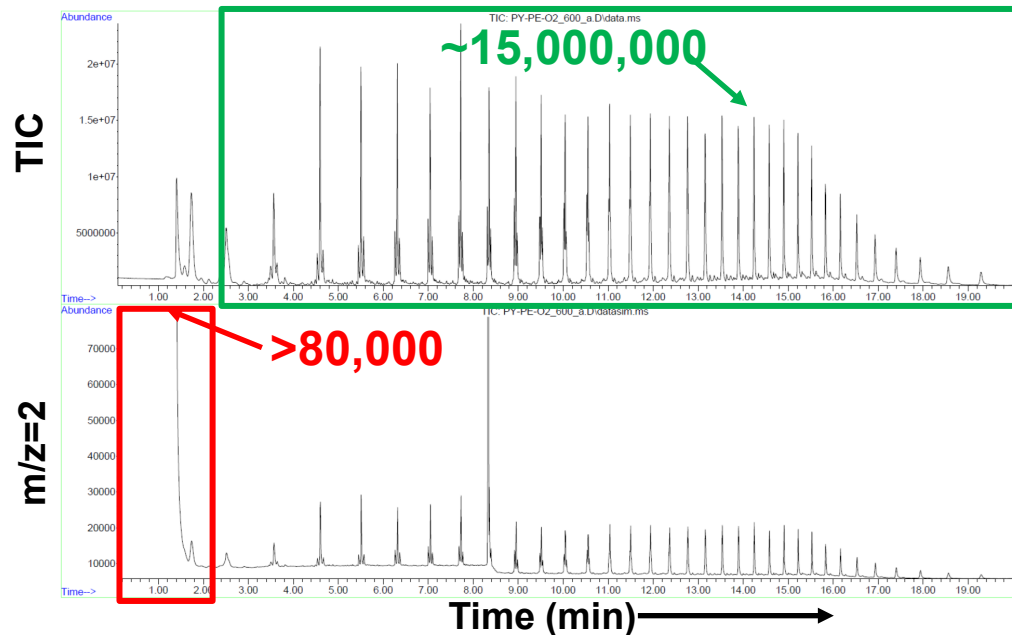
Pyrolysis@600°C, 0% O₂ in He
1% Pt/Al₂O₃ Catalyst



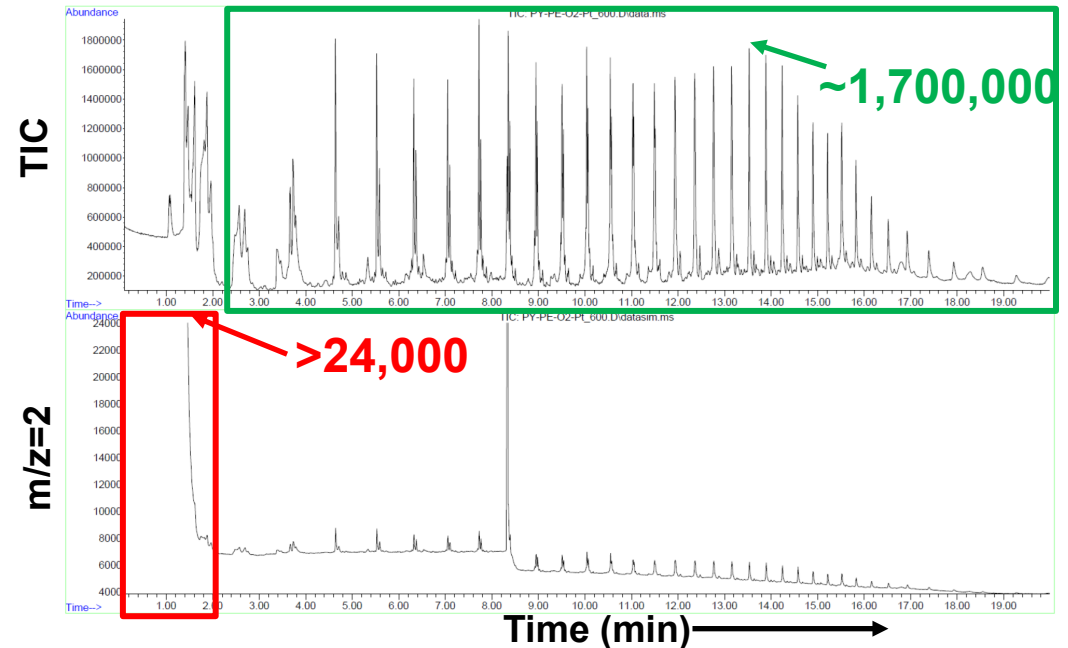
Catalytic Effects on Gasification (2% O₂) of Polyethylene

- MicroPy-GC/MS preliminary data shows intended effects of catalyst remains for gasification but with some open questions:
 - **HCs (tar) greatly reduced**
 - **H₂ difficult to quantify (and oxidation from 2% O₂ level may affect level)**

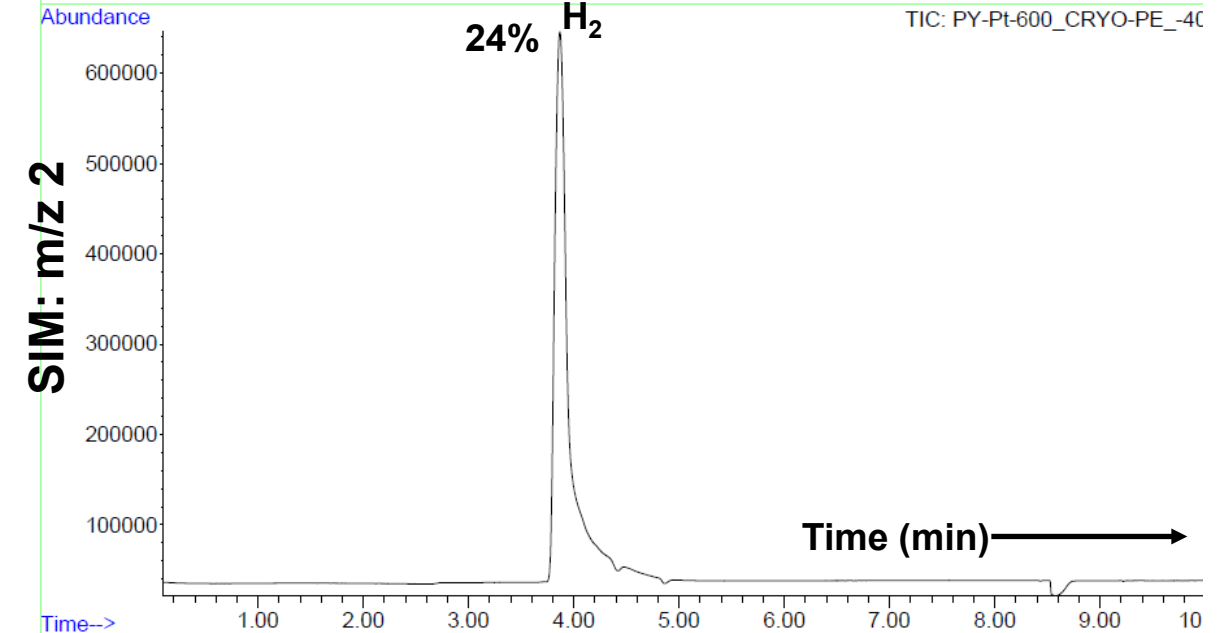
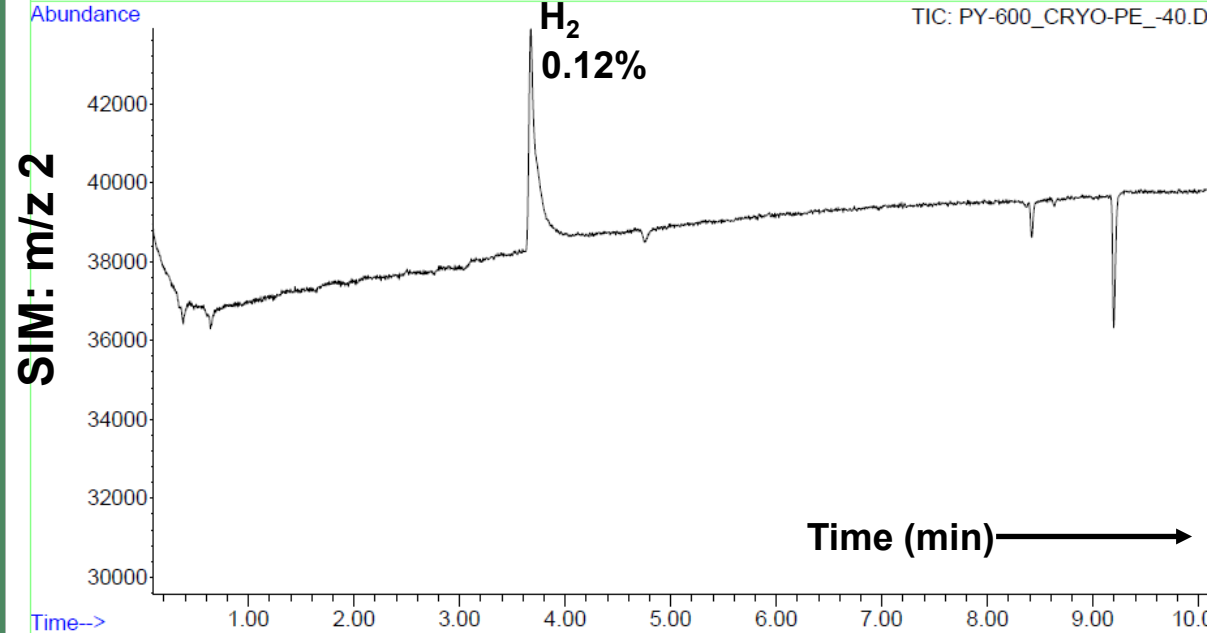
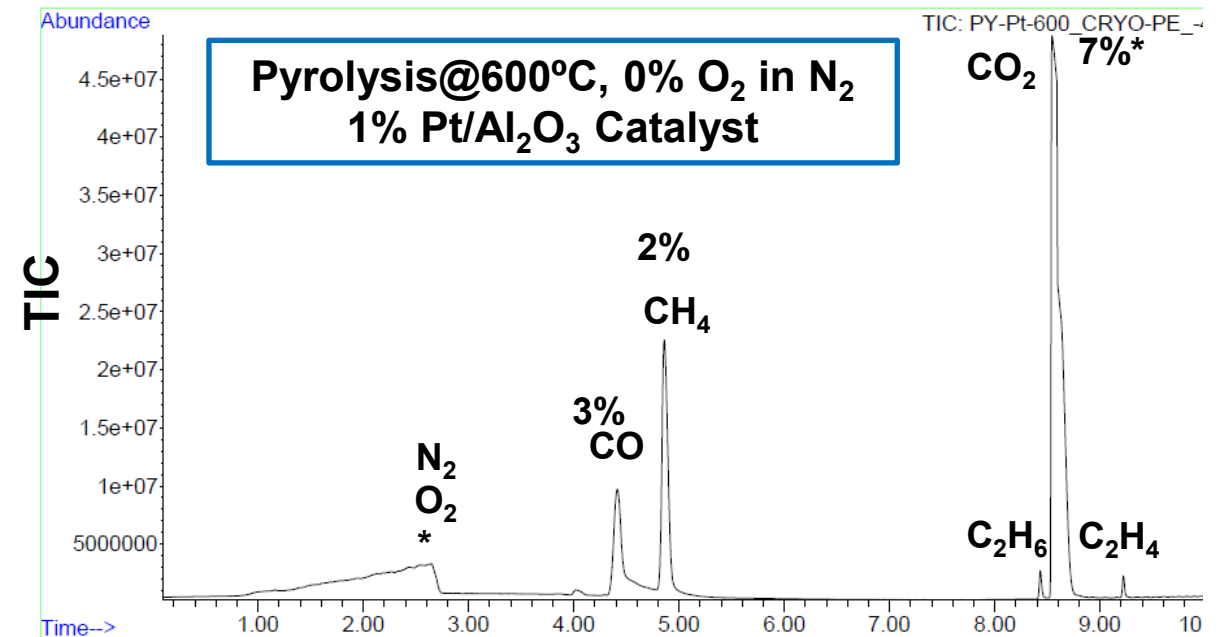
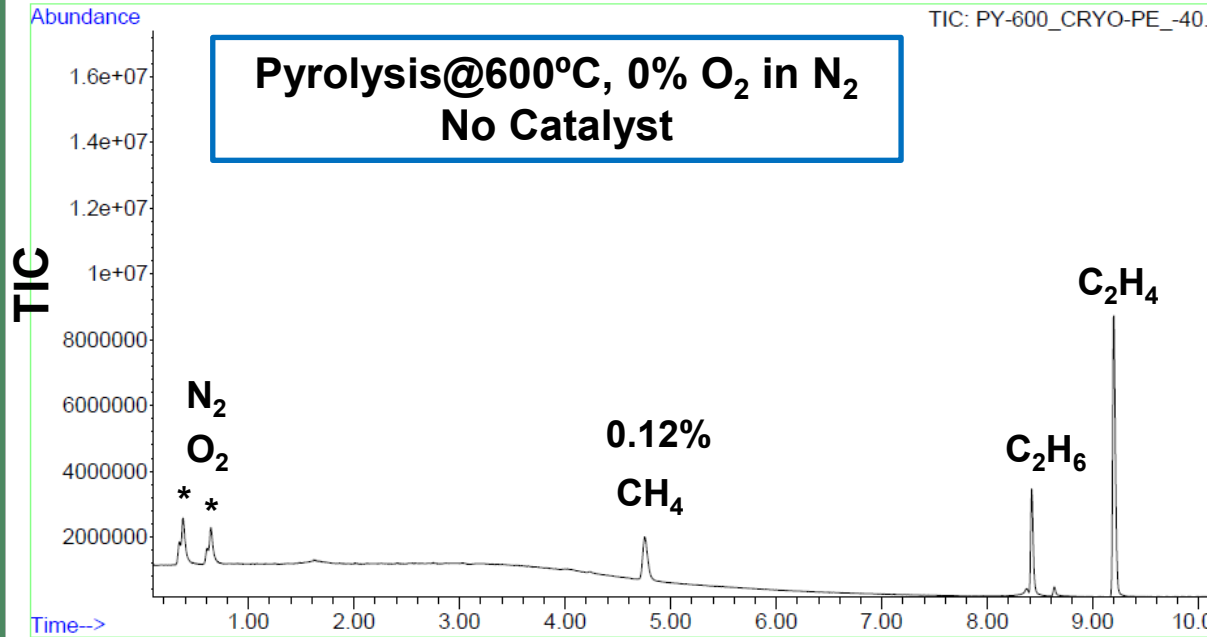
Gasification@600°C, 2% O₂ in N₂
No Catalyst



Gasification@600°C, 2% O₂ in N₂
1% Pt/Al₂O₃ Catalyst



Optimized Analytical Method for Light Gases (Cryogenic-GC/MS with H₂ Sensitive MS) Shows Catalyst Increases H₂ Substantially



Catalyst Enables Tar Cracking and H₂ Production

- MicroPy-GC/MS preliminary data shows beneficial effects of catalyst for decreasing tar (hydrocarbons) and increasing H₂
 - Polyethylene feedstock and 1% Pt/Al₂O₃ catalyst
 - Benefits achieved at moderate temperatures (600°C) that have the potential to decrease cost for materials of construction of gasifier

Without Catalyst

Temperature	H ₂	CO	CH ₄	CO ₂	H ₂ :CO
600°C	0.12%	0%	0.12%	0%	---
800°C	0.5%	1%	1%	0%	---
1000°C	2%	0%	2%	0%	---

With Catalyst (1% Pt/Al₂O₃)

Temperature	H ₂	CO	CH ₄	CO ₂	H ₂ :CO
600°C	24%	3%	2%	7%	8
800°C	37%	9%	3%	12%	4.1
1000°C	36%	7%	3%	18%	5.1

Note: presence of H₂O observed desorbing from catalyst which is likely oxygen source for CO and CO₂ (water-gas shift reaction likely occurring)

Thermogravimetric Analysis (TGA) R&D of Catalytic Effects

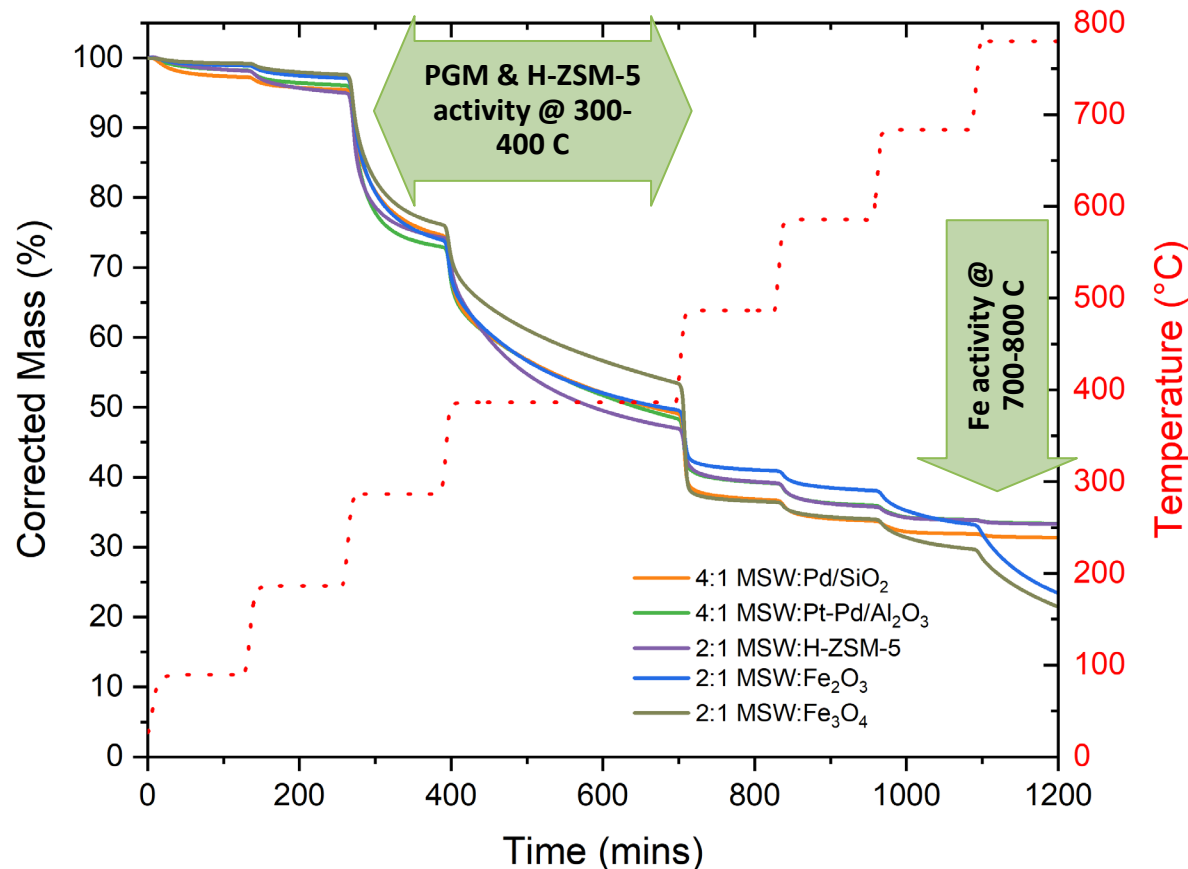
- TGA studies were conducted to investigate a variety of catalyst materials under pyrolysis (no O₂) and gasification (O₂ present) conditions
- The R&D is exploratory with intent to identify thermal regions of interest for accelerating pyrolysis or gasification processes
- Ultimately, there are many durability and coking issues that may occur with the catalysts
 - At this stage, the focus is on activity for different process conditions
- Relevant TGA study of pyrolysis or gasification of MSW/RDF feedstocks:
 - S. Aluri, A. Syed, D. W. Flick, J. D. Muzzy, C. Sievers, P. K. Agrawal, *Fuel Processing Technology* 2018, **179**, 154-166

Catalyst	Beneficial Properties	Limitations
H-ZSM-5	Strong acid sites, shape-selective	Susceptible to coking, requires regeneration
Fe₂O₃	Cost-effective, abundant	Less active than precious metals
Fe₃O₄	acid-base properties, typically stable under reducing conditions	Prone to reduction and structural changes
1.8% Pd/SiO₂	High selectivity, good hydrogenation activity	Expensive, sensitive to poisoning
2%Pt-1%Pd/Al₂O₃	Bimetallic synergy, high activity	Expensive, sensitive to poisoning

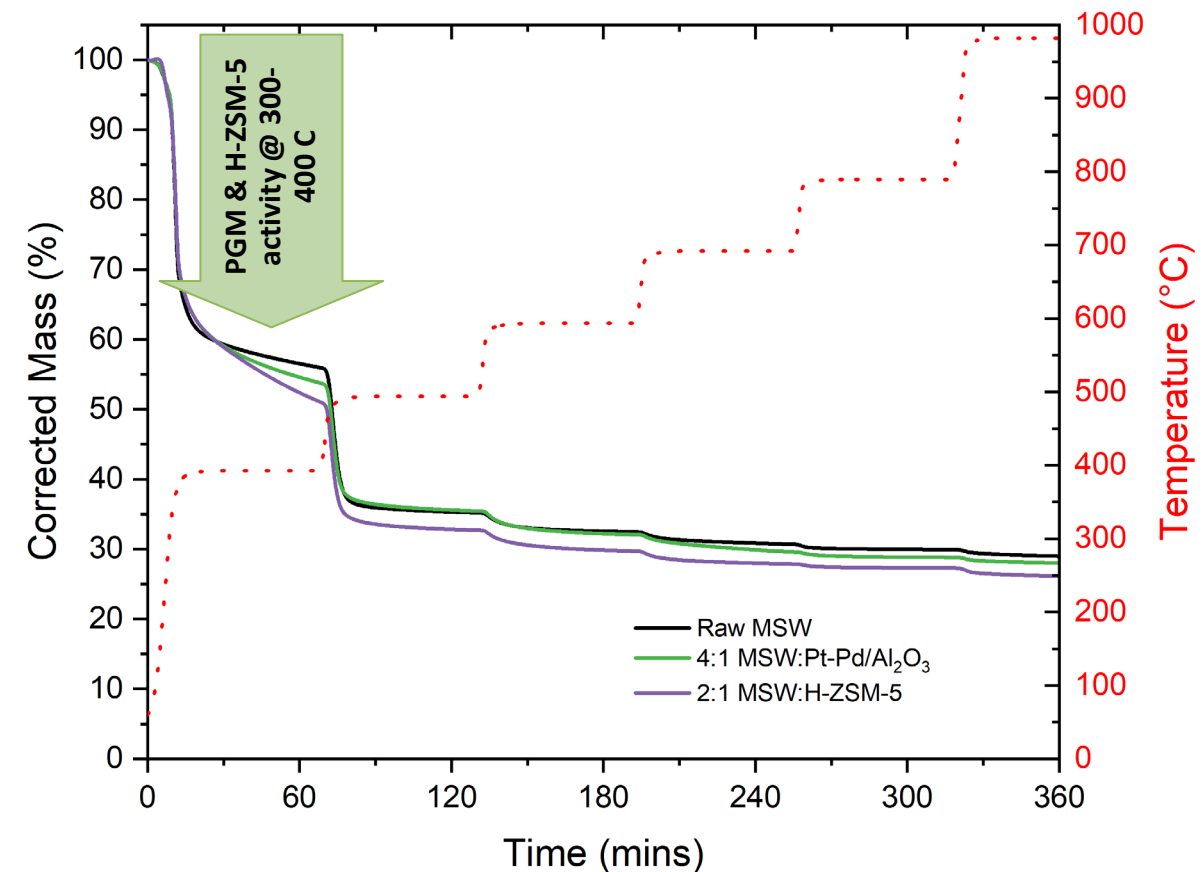
Stepwise Isothermal TGA with and without O₂

- Regions of activity observed by catalyst
- Overall, less effect on mass loss as compared with gas product changes in Py-GC/MS studies

Catalytic Pyrolysis under N₂



Catalytic Gasification under 4% O₂



Note: the masses have been corrected based on catalyst mass added and assuming the catalysts do not lose mass during the reactions.

Conclusions

- Sustainable feedstocks with low life-cycle GreenHouse Gas emissions offer economically viable fuels for gasification, but physical and chemical properties vary greatly.
 - Pelletized Refuse Derived Fuel from processing of Municipal Solid Waste offers a relatively more homogenous and transportable fuel option
- Findings to-date from feedstock characterization studies include:
 - H₂ evolution out of feedstock tracks well with mass loss measurements
 - Porosity and surface area vary greatly over the course of pyrolysis & gasification with small pores (observed via SANS technique) showing constriction at moderate (400-500°C) temperatures
 - Plastic and cellulosic (paper, cardboard) have dramatically different porosities resulting in large mass transfer differences during pyrolysis & gasification
- Preliminary catalytic effect studies show:
 - Gas product chemistry can be altered dramatically even at relatively low (e.g. 600°C) temperatures with much lower tar/HC gas products and high H₂ selectivity
 - The catalytic effects appear most dominant for gas chemistry, but some acceleration of solid mass loss was detected at different temperatures depending on catalyst material

Team Members



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Manufacturing Science Division
Spectroscopy;
Principal investigator



Larry Anovitz

Chemical Science Division
Geochemist, X-ray and neutron;
Small angle neutron & X-ray
scattering for porosity modeling



Dipti Kamath

Manufacturing Science Division
Techno-Economic Analysis;
Life-Cycle Analysis



Charles Finney

Buildings & Transportation Science Division
Combustion & fluidization
diagnostics;
Pyrolysis; neutron imaging



Matthew Ryder

Materials Science & Technology Division
Neutron scattering & spectroscopy;
Vibrational spectroscopy, neutron
diffraction, and physical
characterization



Ikenna Okeke

Manufacturing Science Division
Techno-Economic Analysis;
Life-Cycle Analysis



Costas Tsouris

Manufacturing Science Division
Chem. Eng.; Transport phenomena;
Pyrolysis; sample preparation;
neutron characterization



Vlad Lobodin

Buildings & Transportation Science Division
Analytical chemistry; Gas-
phase analysis



Stephen Purdy

Manufacturing Science Division
Neutron scattering &
spectroscopy; Vibrational
spectroscopy, Catalysis



Capt. Samuel Sasser

Manufacturing Science Division
ORAU Intern transitioning from U.S.
Marine Corp to Clean Energy
career

