



DE-FE0031598

Bench-scale Development of a Transformational Graphene Oxide-based Membrane Process for Post-combustion CO₂ Capture

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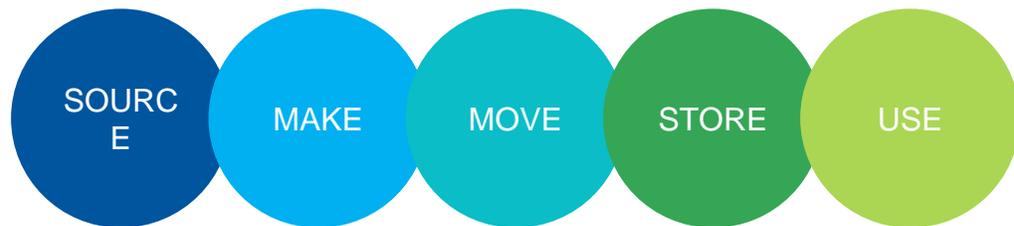
Miao Yu, Fan Wang, Dinesh Behera, *The State University of New York at Buffalo (UB)*

2024 FECM/NETL Carbon Management Research Project Review Meeting
August 5 – 9, 2024

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CCUS is one of GTI strategic focus areas
Active DOE Projects

- **Carbon capture**
 - FE0031946: 20 TPD facilitated transport membrane (FTM) for power plant application
 - FE0032466: 3 TPD ROTA-CAP for steel plant application
 - FE0032463: 3 TPD FTM for cement plant (sub to OSU)
 - FE0031598: Bench-scale GO-based membrane
 - FE0032215: Nano-confined ionic liquid membrane
 - FE0031730: Size-sieving adsorbent (sub to UB)
- **Carbon conversion**
 - FE0031909: Membrane reactors for conversion of CO₂ to fuels/chemicals
 - FE0032246: Converting CO₂ to alternative cement (sub to WashU)
- **Carbon dioxide removal (CDR)**
 - FE0031969: Trapped small amines in capsules (sub to UB)
- **Carbon transport and storage**
 - FE0032239: CarbonSAFE Phase II

Technology based on our work published in *Science* and *Nature Communications*

Science

AAAS

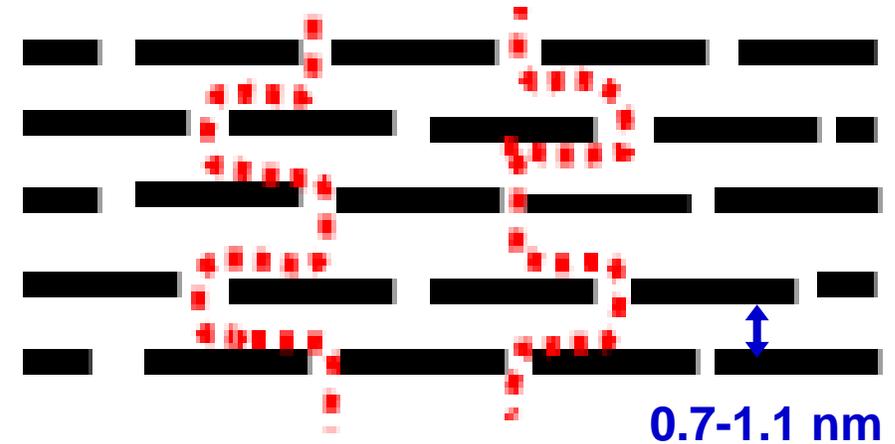
Ultrathin, Molecular-Sieving Graphene Oxide Membranes for Selective Hydrogen Separation

Hang Li *et al.*

Science **342**, 95 (2013);

DOI: 10.1126/science.1236686

➔ Approach to enable CO₂/N₂ separation: fill the space between GO layers with CO₂-philic agent



nature
COMMUNICATIONS

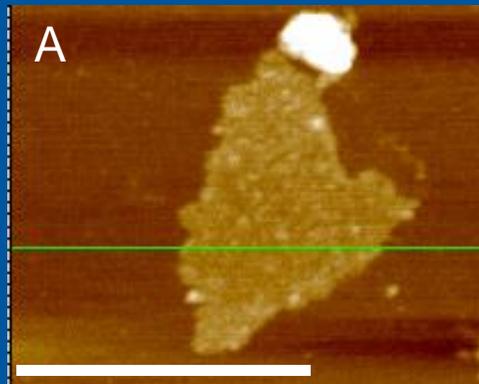
CO₂ permeance: 1,000 GPU
CO₂/N₂ selectivity: 680

ARTICLE

DOI: 10.1038/ncom1467-017-02318-1

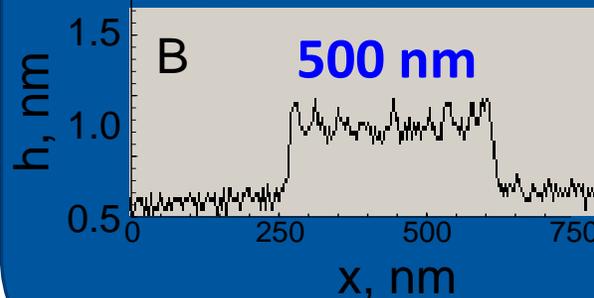
OPEN

Ultrathin graphene oxide-based hollow fiber membranes with brush-like CO₂-philic agent for highly efficient CO₂ capture



Contribution:

- Structural defects on GO flakes can be controlled as transport pathway for selective gas separations



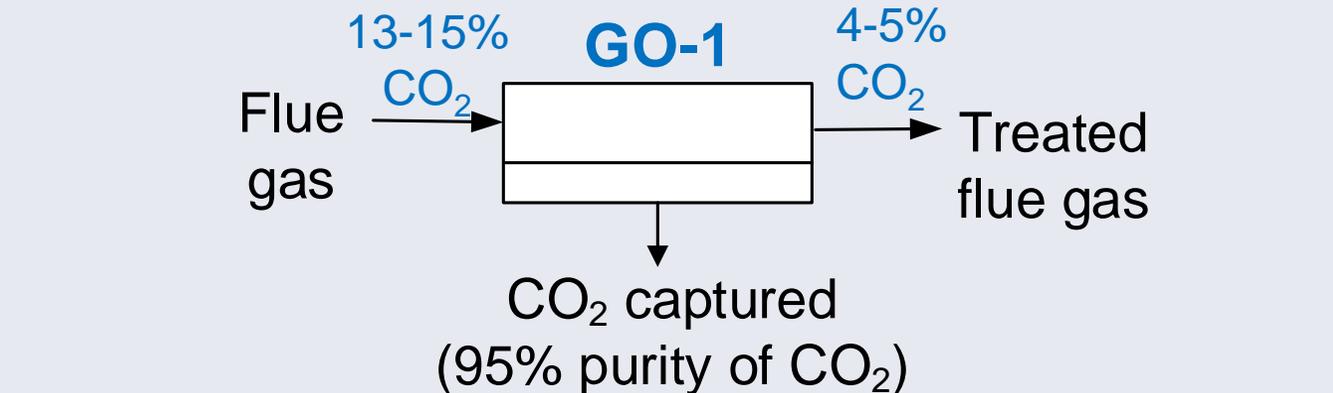
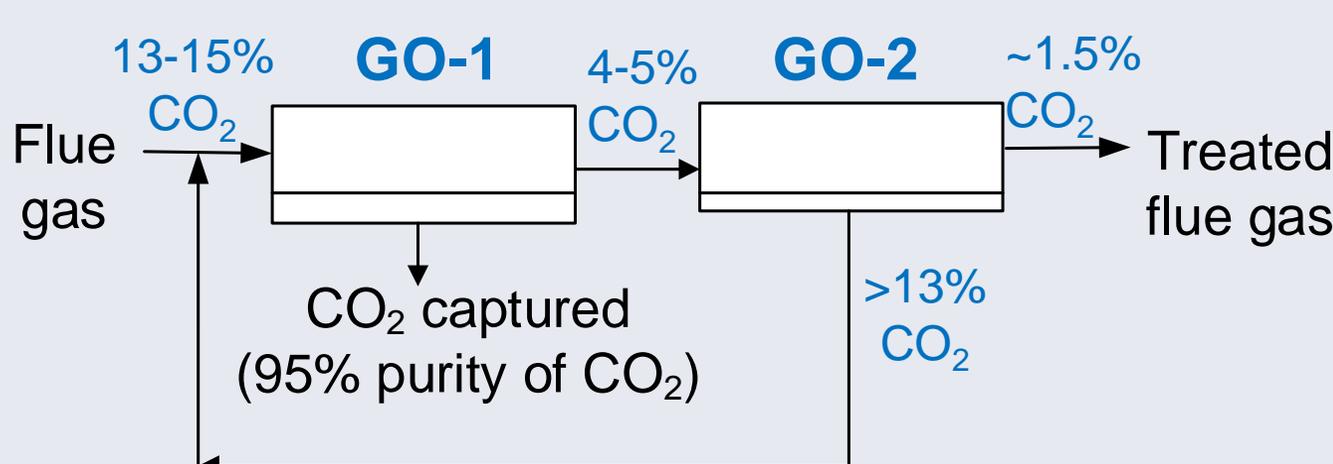
Project overview

- **Performance period**: June 1, 2018 – October 30, 2024
- **Funding**: \$2,914,074 from DOE; \$728,738 cost share
- **Objective**: Develop a transformational graphene oxide (GO)-based membrane process (**GO²**) for CO₂ capture with 95% CO₂ purity and a cost of electricity (COE) at least 30% lower than DOE amine reference baseline SC PC plant case

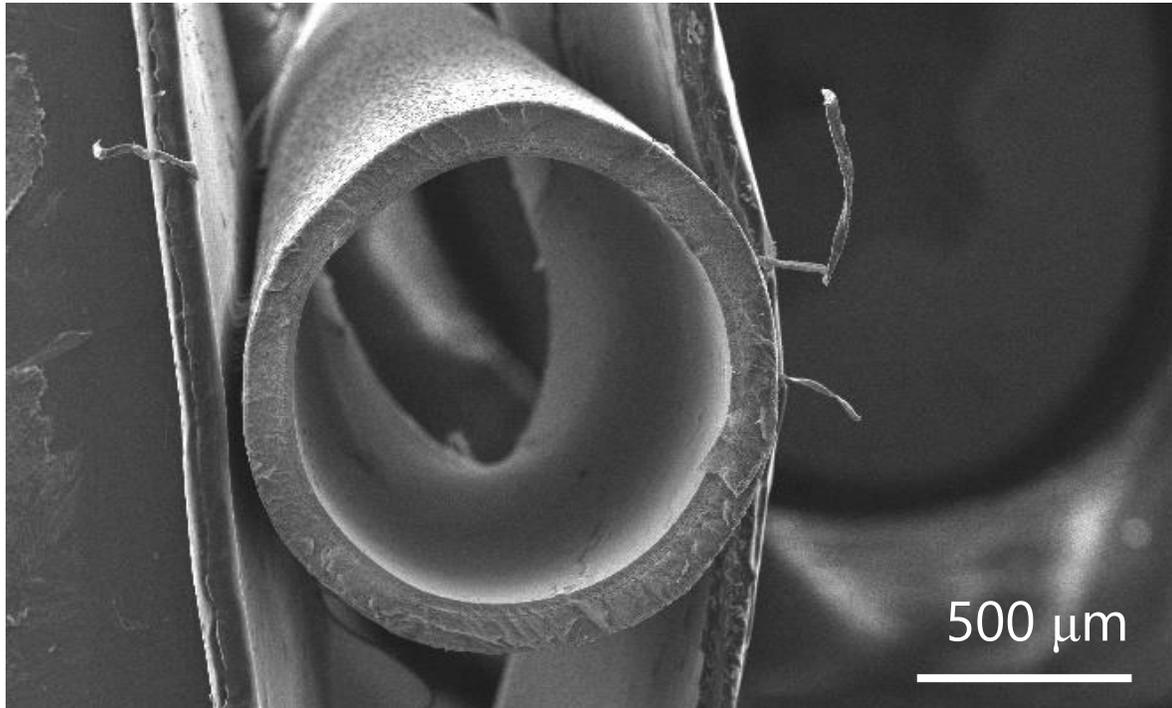
- **Team**:

Member	Roles
	<ul style="list-style-type: none"> ▪ Project management and planning ▪ CO₂ capture process development and testing
	<ul style="list-style-type: none"> ▪ GO membrane development and scale-up
	<ul style="list-style-type: none"> ▪ Site host
	<ul style="list-style-type: none"> ▪ Technical & economic analysis

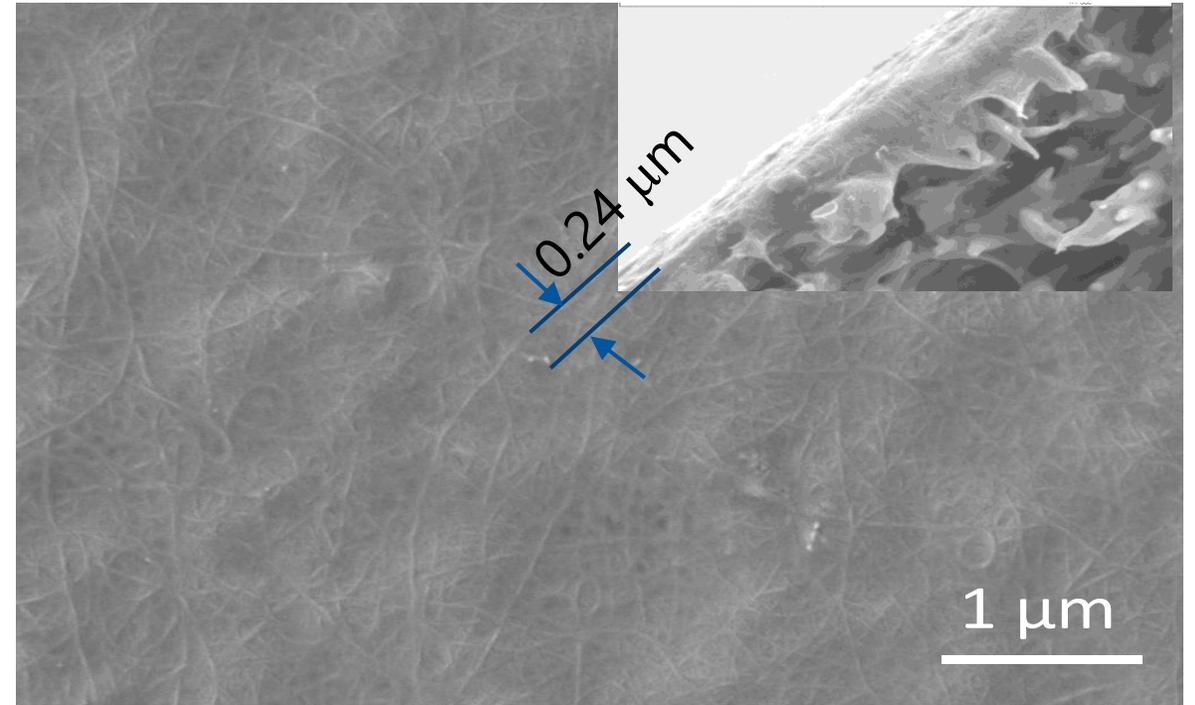
Process description

CO ₂ capture	Diagram	Description
50–70% capture	 <p>Flue gas with 13-15% CO₂ enters a GO-1 membrane unit. The treated flue gas exits with 4-5% CO₂. CO₂ captured (95% purity of CO₂) is shown as a byproduct.</p>	Single stage
70–90% capture	 <p>Flue gas with 13-15% CO₂ enters a GO-1 membrane unit. The treated flue gas then enters a GO-2 membrane unit. The final treated flue gas exits with ~1.5% CO₂. CO₂ captured (95% purity of CO₂) is shown as a byproduct from the first stage. A stream of >13% CO₂ is shown as a byproduct from the second stage.</p>	GO² process integrates a high-selectivity GO-1 membrane and a high-flux GO-2 membrane for optimal performance

High-quality GO-based membranes prepared on commercially available PES hollow fiber substrate



Hollow fiber inner diameter: 1 mm

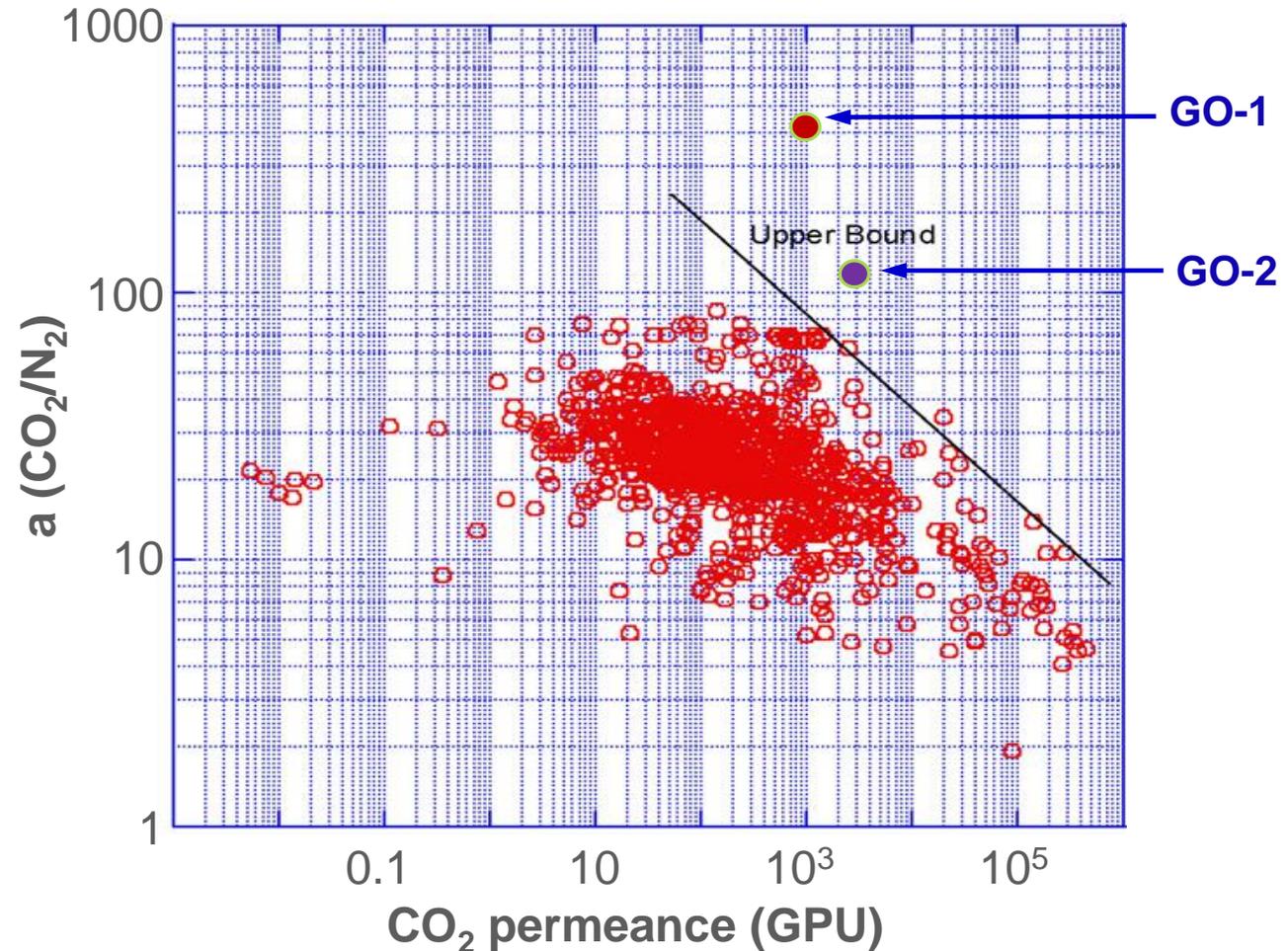


Membrane surface and cross section

In Budget Period 1 (BP1), GO-1 and GO-2 membranes (surface area: ~50 cm²) achieved performance goals

	CO ₂ permeance, GPU	CO ₂ /N ₂ selectivity
GO-1 goal	1,000	200
GO-1 developed	1,100	300
GO-2 goal	2,500	20
GO-2 developed	2,600	120

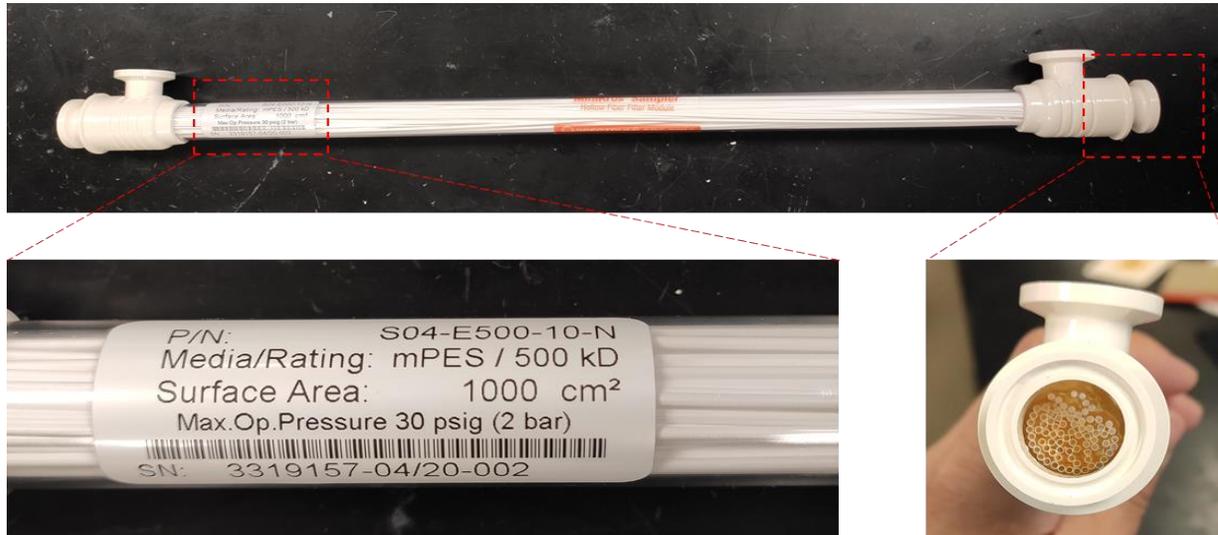
- Feed: mixed simulated flue gases
 - GO-1: 8-12 vol% CO₂
 - GO-2: ~4 vol% CO₂
- Temperature: 80°C
- Feed pressure: ~1.0 bara
- Permeate side pressure: 0.2-0.4 bara



Robeson, J. *Membrane Sci.* **2008**, Vol. 320, p390

Note: Polymer data points (red): 100 nm membrane thickness assumed

BP2: membranes scaled up to 1,000 cm²; bench scale system constructed and installed at NCCC



Material	Fiber ID, mm	Module length, cm	Effective length, cm	# of fibers	Effective surface area, cm ²
PES	1.0	47	41.5	78	1,000



- Bench system installed at NCCC

Feed gas at NCCC

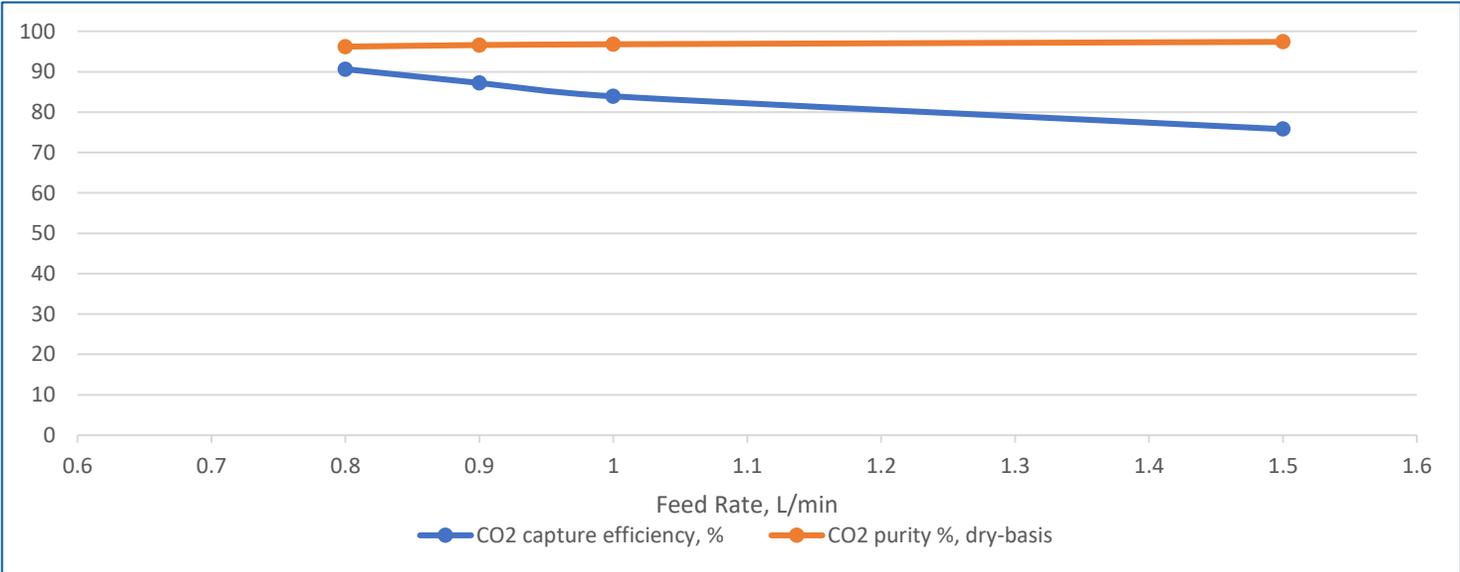
- Actual natural gas boiler flue gas was modified to replicate the CO₂ concentrations found in coal flue gas

Gas	Simulated coal-fired flue gas
CO ₂	12.5%-16%
O ₂	3.3%-7.5%
SO ₂	<1ppm
NO ₂	2-3 ppm
Water	80-90% saturation
N ₂	Balance

Parametric tests: As flow rate decreases, capture efficiency increases with a small effect on product purity



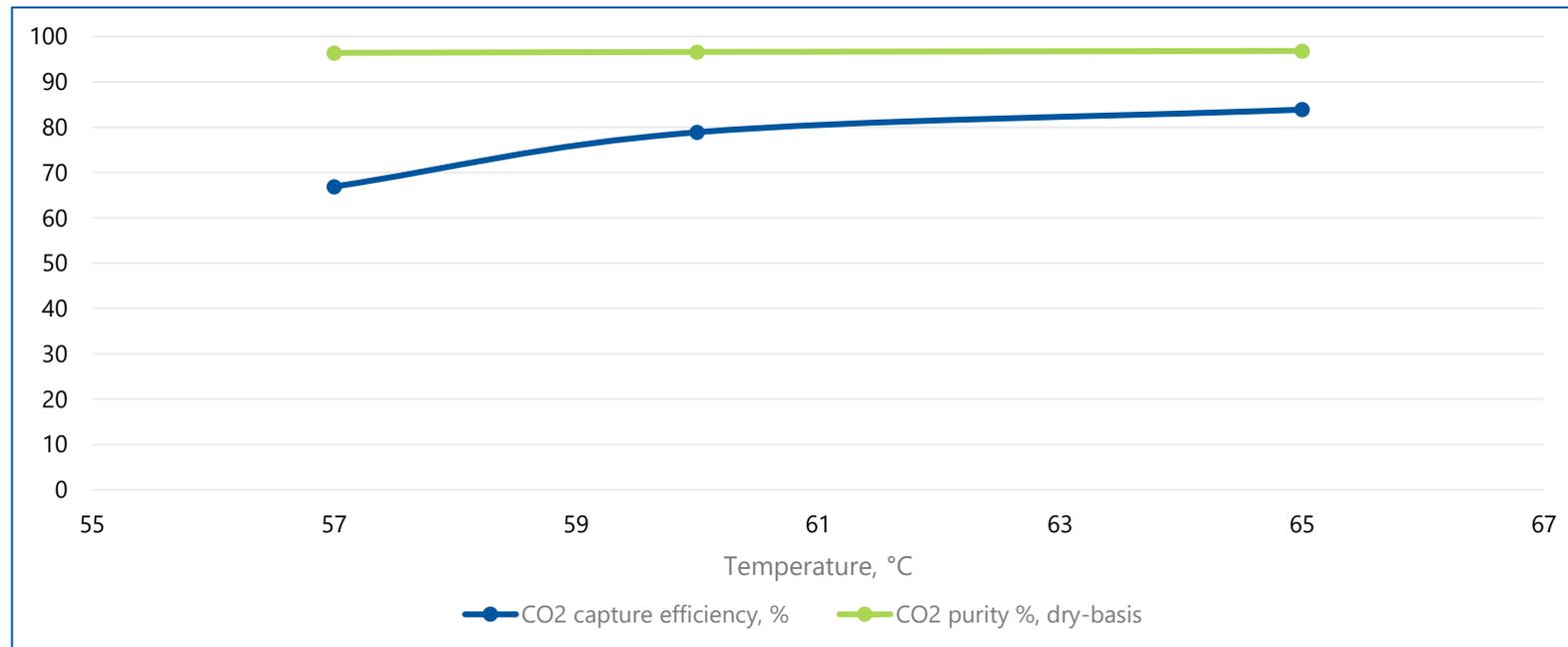
#	Parameters	T, °C	Pressure, bara		Feed CO ₂ concentration, vol% dry-basis	Feed flow rate, L/min	CO ₂ capture efficiency, %	CO ₂ purity %, dry-basis
			Feed	Permeate				
1	Feed flow rate	65	1.2	0.15	15	1.5	75.8	97.4
2		65	1.2	0.15	15	1.0	83.9	96.8
3		65	1.2	0.15	15	0.9	87.2	96.6
4		65	1.2	0.15	15	0.8	90.6	96.2



Parametric tests: Capture efficiency increases as temperature increases with a small effect on purity

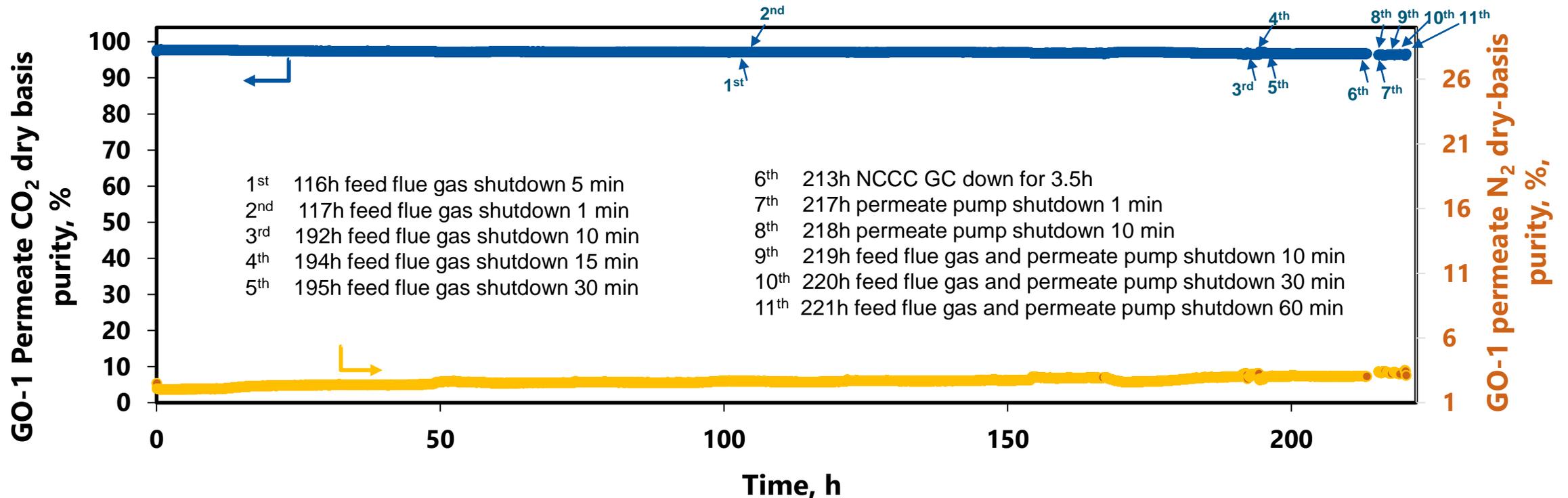


#	Parameters	T, °C	Pressure, bara		Feed CO ₂ concentration, vol% dry-basis	Feed flow rate, L/min	CO ₂ capture efficiency, %	CO ₂ purity %, dry-basis
			Feed	Permeate				
1	Operating temperature	57	1.2	0.15	15	1.0	66.9	96.4
2		60	1.2	0.15	15	1.0	78.9	96.6
3		65	1.2	0.15	15	1.0	83.9	96.8



220-h single-stage testing indicated good dynamic stability and long-term stability

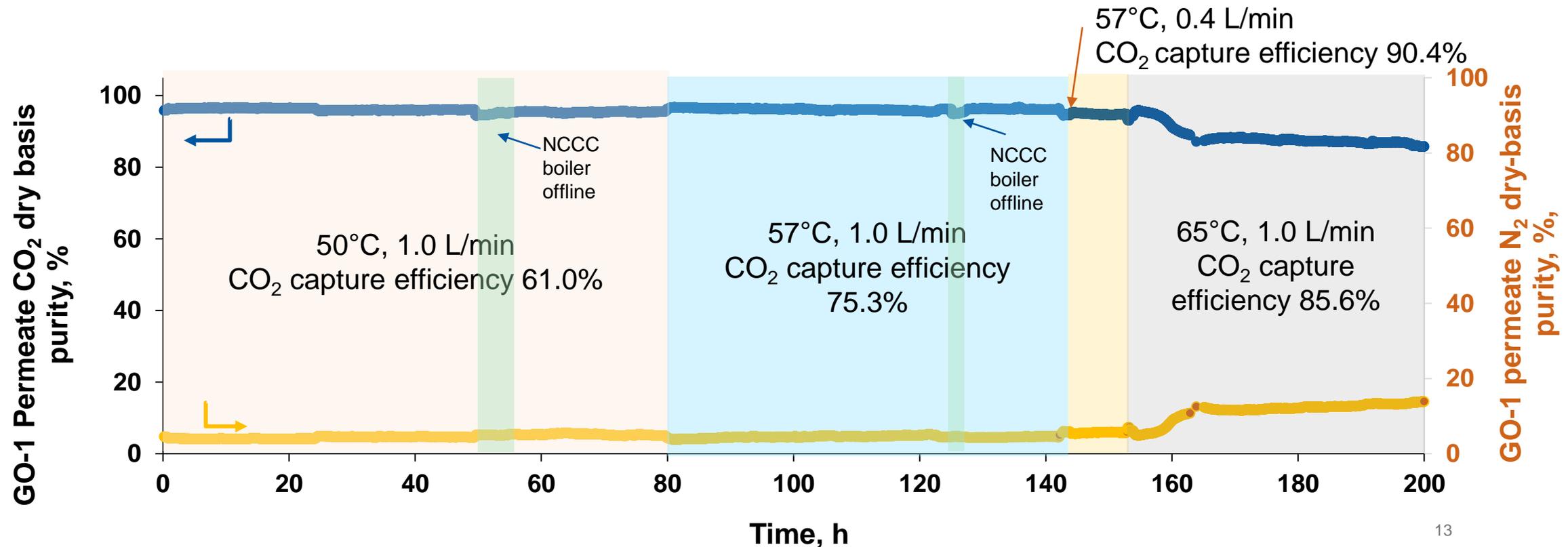
GO-1 membrane area, cm ²	Feed composition, vol%	Temperature, °C	Feed pressure, bara	Permeate pressure, bara
1,000	16% CO ₂ , 4% O ₂ , 80% N ₂ dry-basis	50	1.06	0.15



200-h two-stage (GO² process) continuous testing showed stable performance

- Dry-basis feed mixture: 16 vol% CO₂, 4 vol% O₂, 80 vol% N₂; feed mixture is saturated with H₂O

GO-1 membrane area, cm ²	GO-2 membrane area, cm ²	GO-1 permeate pressure, bara	GO-2 permeate pressure, bara
1,000	75	0.15	0.15



Status of the milestones

Budget Period	M #	Task #	Milestone Title/Description	Planned Completion Date	Actual Completion Date
1	1.1	1	Updated Project Management Plan	11/30/18	9/6/18
1	1.2	1	Kickoff Meeting	1/15/19	2/6/19
1	1.3	1	Technology maturation plan submitted to DOE	1/15/19	12/28/18
1	2.1	2	50-100 cm ² GO membranes prepared	1/30/19	1/15/19
1	2.2	2	For 50-100 cm ² area membranes, GO-1 exhibits CO ₂ /N ₂ selectivity ≥100 and CO ₂ permeance ≥1,000 GPU and GO-2 exhibits CO ₂ /N ₂ selectivity ≥10 and CO ₂ permeance ≥2,500 GPU	6/30/19	6/11/19
1	1.4	1	Continuation application for BP2 submitted	12/31/19	12/28/19
1	3.1	3	For 50-100 cm ² area membranes, GO-1 exhibits CO ₂ /N ₂ selectivity ≥200 and CO ₂ permeance ≥1,000 GPU and GO-2 exhibits CO ₂ /N ₂ selectivity ≥20 and CO ₂ permeance ≥2,500 GPU	2/28/20	12/18/20
1	4.1	4	Stability testing shows the CO ₂ permeances and CO ₂ /N ₂ selectivities decreased by less than 10% in the presence of flue gas contaminants	3/31/20	11/23/20
2	1.5	1	Submit BP1 Report	4/30/20	4/15/20
2	5.1	5	For 1,000 cm ² area membranes, GO-1 exhibits CO ₂ /N ₂ selectivity ≥200 and CO ₂ permeance ≥1,000 GPU and GO-2 exhibits CO ₂ /N ₂ selectivity ≥20 and CO ₂ permeance ≥2,500 GPU	5/31/22	8/25/22
2	6.1	6	CO ₂ permeances and CO ₂ /N ₂ selectivities decrease by <10% during a 100-h continuous testing	2/28/23	2/28/23
2	7.1	7	Complete process design for low and high CO ₂ flue gas conditions; and process simulation indicates that the CO ₂ capture system can achieve ≥95% CO ₂ purity	9/30/21	9/20/21
2	7.2	7	Constructed skid ready for testing	12/31/21	12/31/21
2	8.1	8	95% CO ₂ purity achieved when testing the constructed GO ² system using simulated flue gas	5/30/23	4/12/23
2	9.1	9	Commissioning complete and system ready for testing at NCCC.	6/30/23	8/19/23
2	9.2	9	1,000 cm ² GO membrane modules shipped to NCCC	6/30/23	8/15/23
2	9.3	9	Skid testing at NCCC complete, 70-90% CO ₂ removal rate achieved, 95% CO ₂ purity validated, and membrane shows good stability during a 200-h testing	6/30/24	6/3/24
2	10.1	10	Issue techno-economic analysis (TEA) report	7/31/24	7/31/24
2	1.6	1	Submit Final Technical Report	1/29/25	

Summary

- GTI and UB have developed a transformational graphene oxide-based membrane process for post-combustion CO₂ capture
- Membranes successfully scaled to 1,000 cm² surface area
- Bench-scale system designed, constructed and tested at NCCC
- 220-h single-stage testing indicated good dynamic stability and long-term stability
- 200-h two-stage (GO² process) continuous testing showed stable performance, 70-90% CO₂ removal rate achieved, 95% CO₂ purity validated

Acknowledgements

- Financial and technical support



DE-FE0031598



CO₂ Capture Project - Phase 4



- DOE NETL: Dustin Brown, Andrew O'Palko, José Figueroa, Dan Hancu and Lynn Brickett
- The CCP4: Betty Pun and technical team
- NCCC: Frank Morton and Tony Wu

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