

Cement Plant TEA/LCA



Sally Homsy

Research Engineer, National Energy Technology Laboratory



Carbon Management Project Review Meeting 2024

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1. “Analysis of Carbon Capture Retrofits for Cement Plants” report, published in 2023
2. “The Impact of Cement Plant Air Ingress on Membrane-Based CO₂ Capture Retrofit Cost” Carbon Capture Science & Technology, 2024
3. Ongoing techno-economic analysis (TEA) and lifecycle assessment (LCA) work on capture from cement plants & other industrial capture projects will be highlighted

Analysis of Carbon Capture Retrofits for Cement Plants

Sydney Hughes², Patricia Cvetic², Sally Homsy², Alex Zoelle³, Mark Woods², Charles White², Sandeep Pidaparti², Norma Kuehn², Hannah Hoffman², Katie Forrest², Travis Shultz¹, Tim Fout¹, Eric Grol¹, Robert James¹, Richard Bohan³

¹NETL

²NETL support contractor

³Portland Cement Association

<https://www.osti.gov/biblio/1970135>

Design Assumptions

- The base cement plants are not modeled. Emissions streams from representative plants are characterized
 - Heat integration potential and retrofit difficulty factors are applied as a mathematical exercise without consideration of host plant specifics
- In addition to capture and compression, all required balance of plant systems, including steam production via a natural gas-fired industrial boiler, are modeled
- NETL's library of legacy system analysis studies serves as the basis for cost scaling references, cement plant-specific vendor data for CO₂ capture systems, balance of plant performance and cost information, and financial methodologies

Kiln Gas Conditions

- Average CO₂ emissions factors for the representative cement plants are based on Global Cement and Concrete Association (GCCA) “Getting the Numbers Right Project” data¹
 - Each average total emissions rate is based on data collected from U.S. producers based on kiln type and accounts for kiln combustion fuel emissions and CO₂ from calcination

	For PH/PC Kilns	For Wet Kilns	Units
Cement Production Rate	1,500,000	1,500,000	tonnes per year
Percentage Clinker	91.4%	91.4%	per PCA EPD ²
Clinker Production Rate	1,371,000	1,371,000	tonnes per year
Total Emissions Rate ¹	848	1,026	kg CO _{2e} per tonne clinker
Annual CO ₂ Emissions from Kiln	1,162,608	1,406,646	tonnes per year
CO ₂ Emissions from Kiln	297,370	359,790	lb/hr at 100% operating basis
Applicable Cases	CM99-B; CM95-B CM95-B1; CM95-B2 CM95-B5; CM95-B6 CM95-B7; CM95-B8	CM95-B3 CM95-B4	

Note: PH = pre-heater; PC = pre-calciner PCA = Portland Cement Association; EPD = Environmental Product Declaration

1- GCCA, “Getting the Numbers Right Project,” 2019

2- PCA, “Environmental Product Declaration: Portland Cement,” March 12, 2021

Analysis of Carbon Capture Retrofits for Cement Plants



Study Base Cases

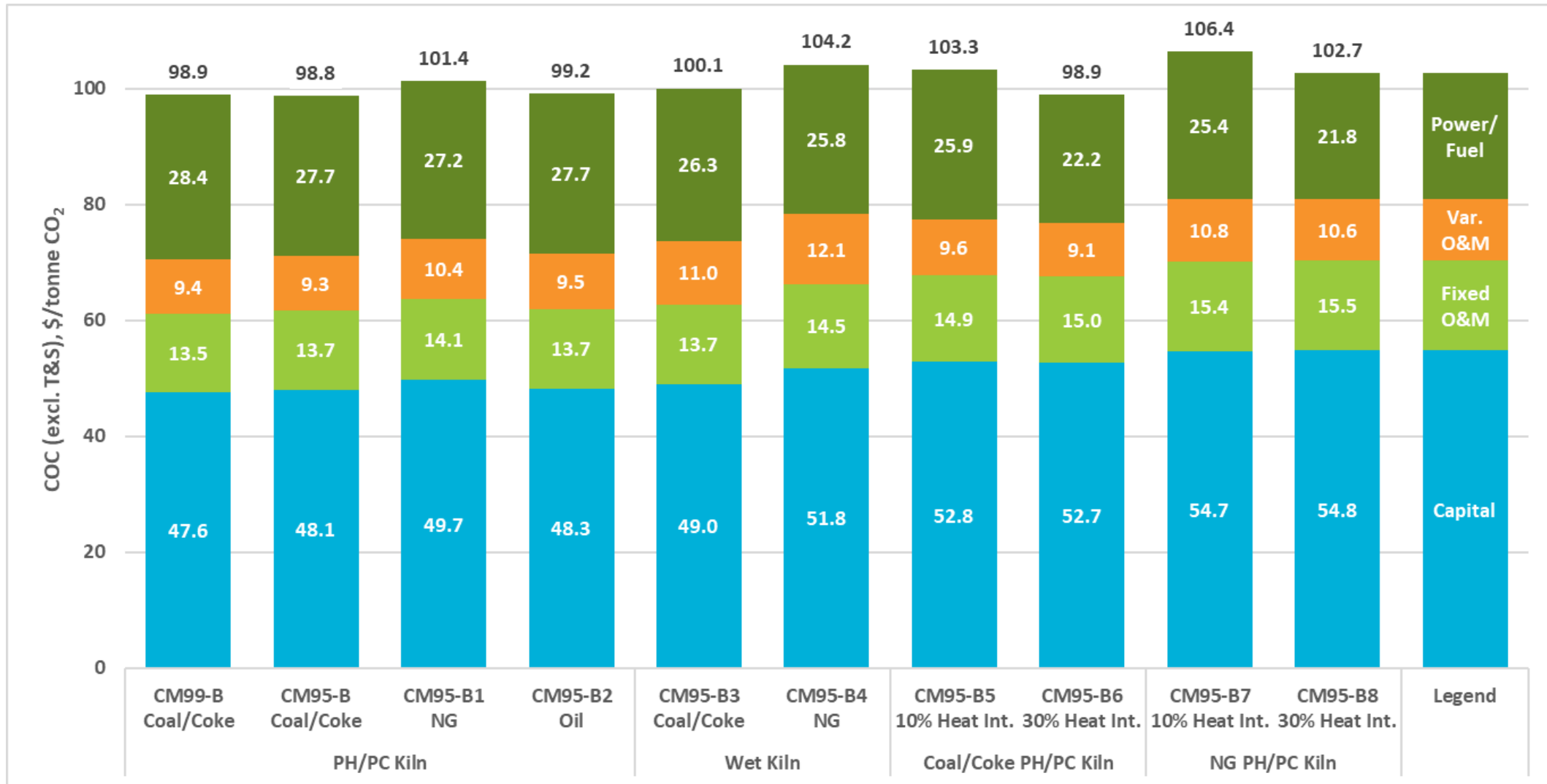
Case Number	CM99-B	CM95-B	CM95-B1	CM95-B2	CM95-B3	CM95-B4	CM95-B5	CM95-B6	CM95-B7	CM95-B8
Capture Rate	99%	95%								
Kiln Type	Pre-heater/Pre-calciner				Wet Process		Pre-heater/Pre-calciner			
Kiln Exit Gas CO ₂ Concentration, mol %	31	31	25	30	17	13	31		25	
Kiln Fuel Type	Coal/Coke		NG	Oil	Coal/Coke	NG	Coal/Coke		NG	
Heat Integration (HI)	N/A						10	30	10	30
Combined Stream CO ₂ Concentration, mol %	21	21	19	21	15	12	22	23	19	20

- The capture rate represents the % of CO₂ captured from the treated combined emissions stream
- The kiln off-gas CO₂ mol % is the assumed concentration directly from the kiln before processing through raw mill operations, prior to any additional air in-leakage, and not including comingled CO₂ from the NG boiler
- The combined stream CO₂ mol % is the assumed concentration of the comingled streams from the NG boiler and from the cement kiln before processing through raw mill operations and prior to any additional air in-leakage

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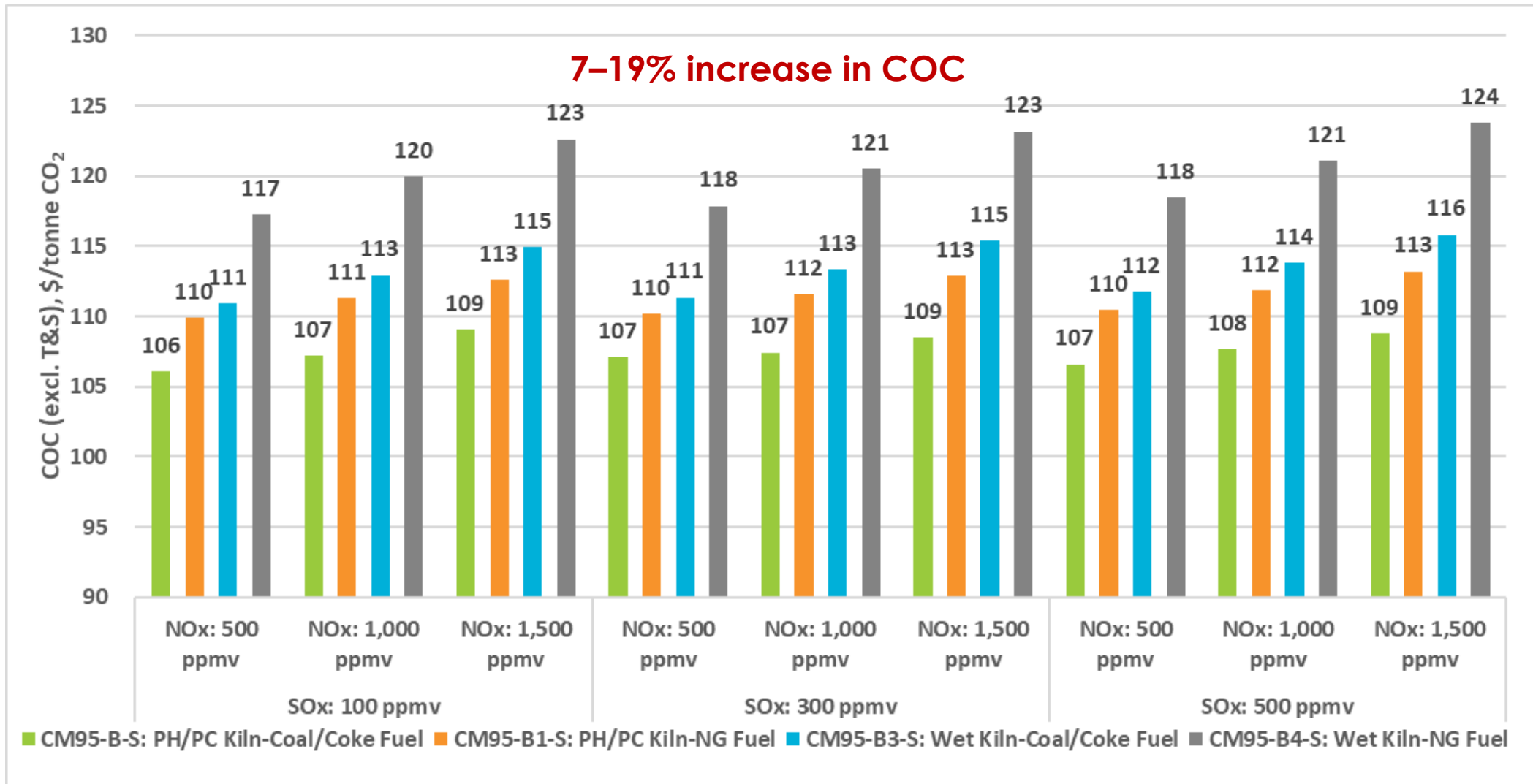
Study Base Cases



Note: All monetary values real, Nov. 2022 \$

Analysis of Carbon Capture Retrofits for Cement Plants

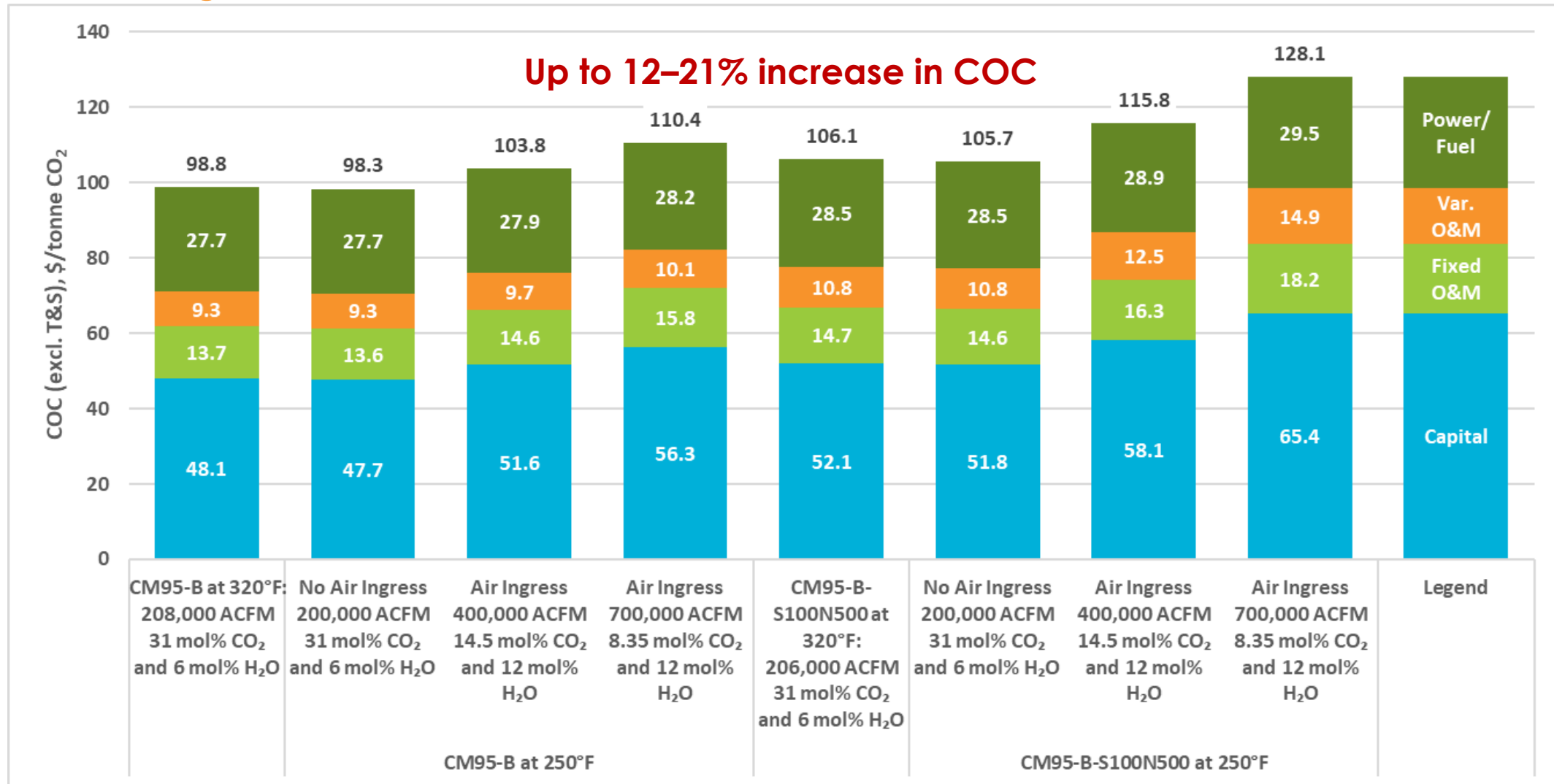
Removal of SO_x (dry FGD) and NO_x (SCR) & resulting PM (baghouse)



Note: All monetary values real, Nov. 2022 \$

Analysis of Carbon Capture Retrofits for Cement Plants

Impact of Air Ingress



Note: All monetary values real, Nov. 2022 \$

Conclusions

- Increasing levels of SO_x , NO_x , and PM in the kiln emissions stream incur cost premiums associated with capital and O&M costs required to abate those contaminants and avoid detriment to the solvent system
 - A 7.4–18.8% increase in COC over the respective base case (i.e., analogous cases without additional $\text{SO}_x/\text{NO}_x/\text{PM}$ abatement)
 - The capital cost increase associated with the addition of FGD and SCR was 8.4–13.7% relative to their respective base cases, suggesting that additional capital costs provide the most impact to the COC for cases with more advanced SO_x and NO_x control
- False air and moisture ingress into the kiln emissions stream can result in a notable increase to the COC due to the higher capital costs required to accommodate larger gas volumes at the capture system inlet
 - Capture costs can increase by as much as 11.7% for cases without FGD and SCR and 20.7% for cases with SCR and FGD
 - PCA contributors indicate that false air ingress and the presence of SO_x and NO_x in the emissions stream is the most likely scenario for plants in the current domestic fleet

The Impact of Cement Plant Air Ingress on Membrane-Based CO₂ Capture Retrofit Cost

Sydney Hughes², Patricia Cvetic², Richard Newby², Sally Homsy², Alex Zoelle³, Mark Woods², Eric Grol¹, Tim Fout¹

¹NETL

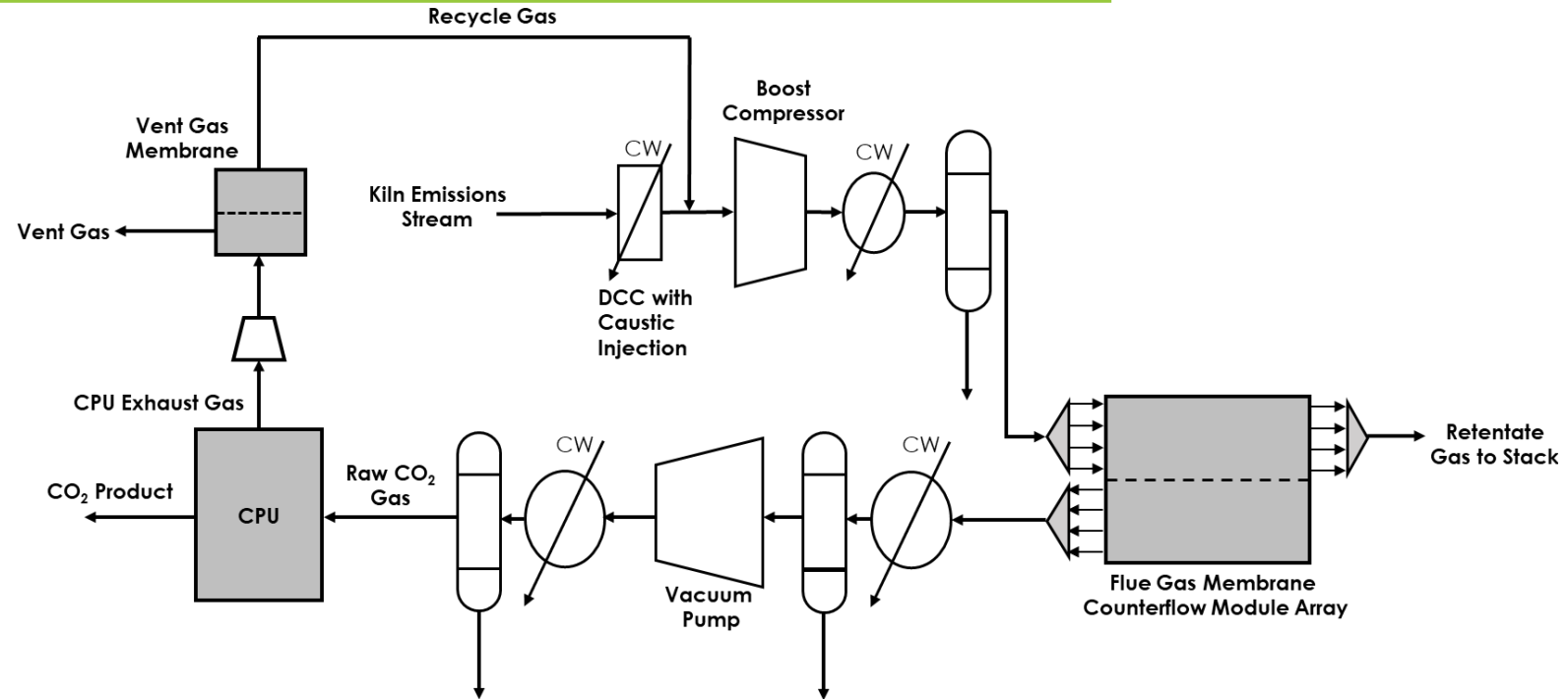
²NETL support contractor

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The Impact of Cement Plant Air Ingress on Membrane-Based CO₂ Capture Retrofit Cost

Design Assumptions

- Correlations for ideal countercurrent membrane separation and a CPU model¹ are used within an Aspen Plus[®] simulation of balance of plant equipment (e.g., boost compression, inlet conditioning, recycle) to estimate the performance of a simplified two-stage membrane system with CPU and permeate recycle



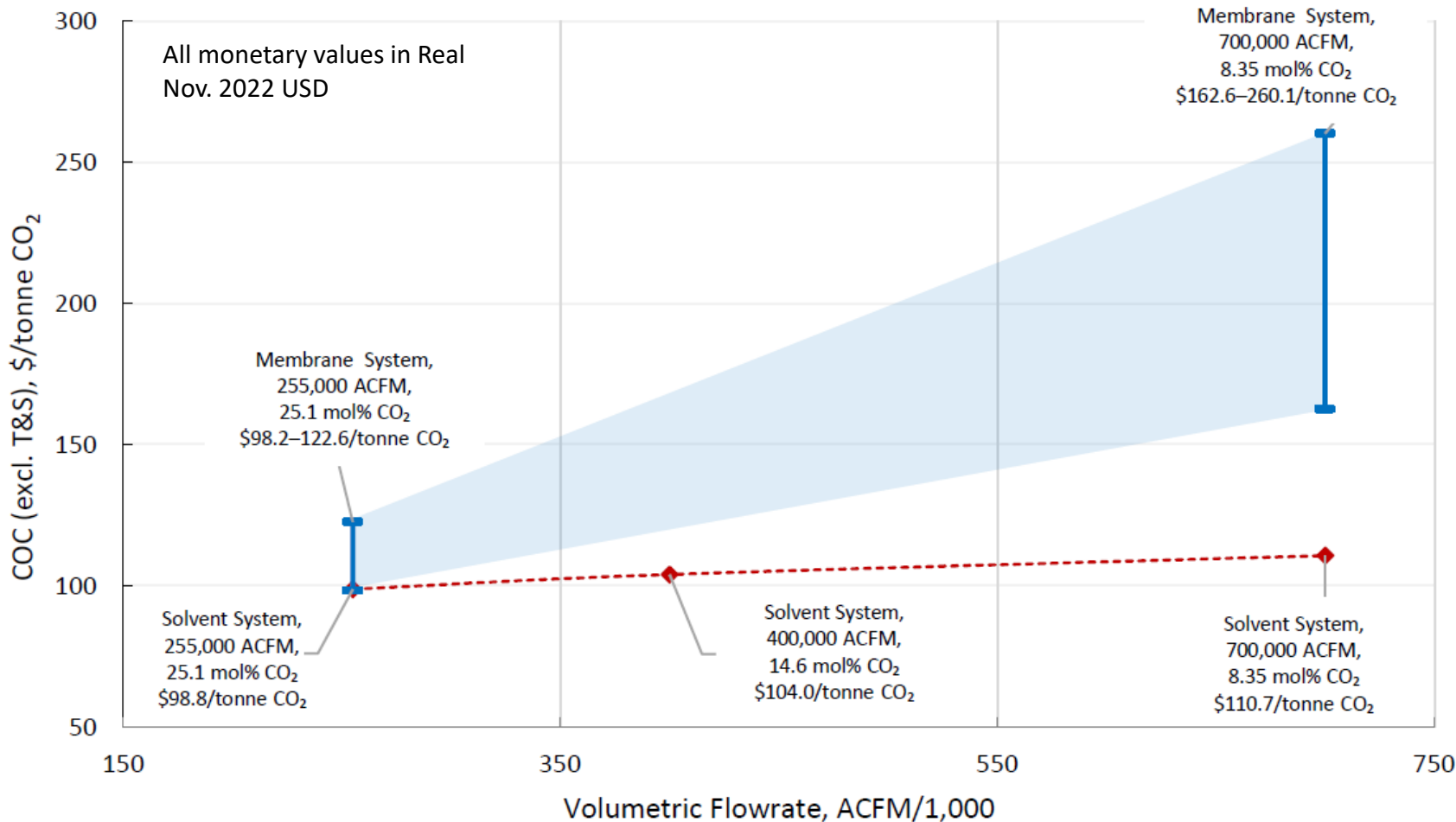
Note: CW = cooling water; DCC = direct contact cooler; CPU = compression and purification unit

The configuration chosen for this analysis is not optimized and is not particularly sensitive to changes in membrane performance. Other configurations, particularly configurations that do not consider such high flue gas compression (5 atm), would likely be more sensitive to membrane performance metrics

1. NETL, "Development of Carbon Dioxide Purification Unit and Compression System Spreadsheet Tool," U.S. DOE, Pittsburgh, 2015

The Impact of Cement Plant Air Ingress on Membrane-Based CO₂ Capture Retrofit Cost

Results



- Without false air ingress, capture costs for the unoptimized membrane-based capture system, under the design assumptions evaluated in this analysis, are comparable to a solvent-based system
- For the examined configuration, false air ingress results in a membrane system COC that is 47–135% higher than that of a solvent-based system

The Impact of Cement Plant Air Ingress on Membrane-Based CO₂ Capture Retrofit Cost

Conclusions

- Alternate configurations or operating scenarios for the membrane-based capture system are likely to be considered and have more favorable economics if the design accounts for false air ingress into the emissions stream, which is inherent to the cement production process
- Recommend examining approaches for and the cost of reducing false air ingress, and designing for lower CO₂ concentrations (considering multistage systems etc.)



Ongoing Studies

- NETL has completed a model of a cement plant allowing in-depth analysis of analysis of applying capture to newbuild and retrofit cement plants
- LCAs are being completing examining the impact of adding capture to cement plants and as a compliment to NETLs Industrial Capture TEA report
- NETL's Cost of Capturing CO₂ from Industrial Sources report and Industrial Carbon Capture Retrofit Database (CCRD) are being expanded to include capture from a petroleum refinery and from a glass plant
- A journal article reporting learnings from recent industrial pre-FEED reports is being compiled

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Questions/ Comments

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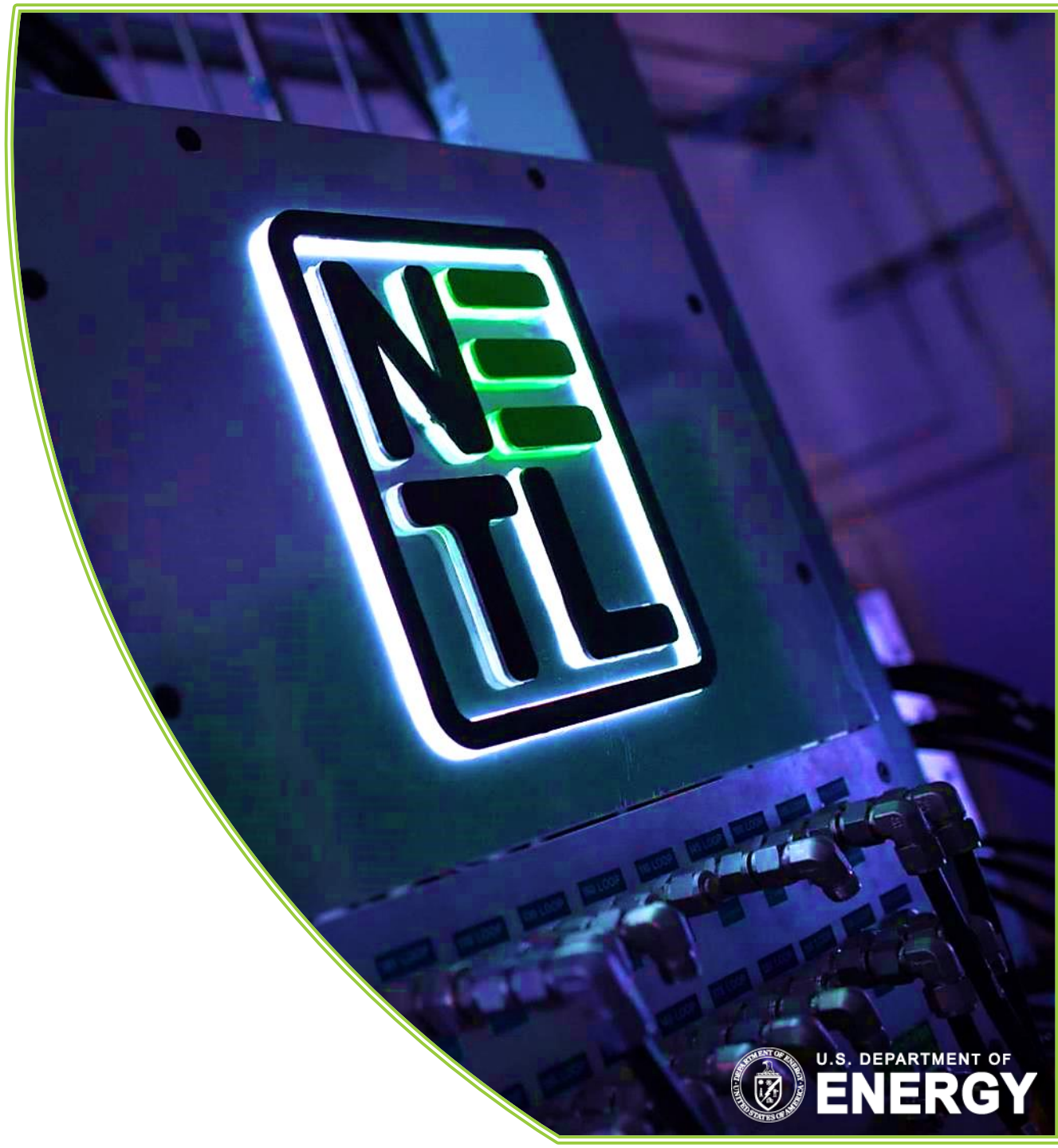


@NationalEnergyTechnologyLaboratory

CONTACT:

Sally Homsy

Sally.Homsy@netl.doe.gov



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