

# DE-FE0032248

## Black River Net-Zero Lime Kiln & Carbon Removal Facility

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# Project Overview

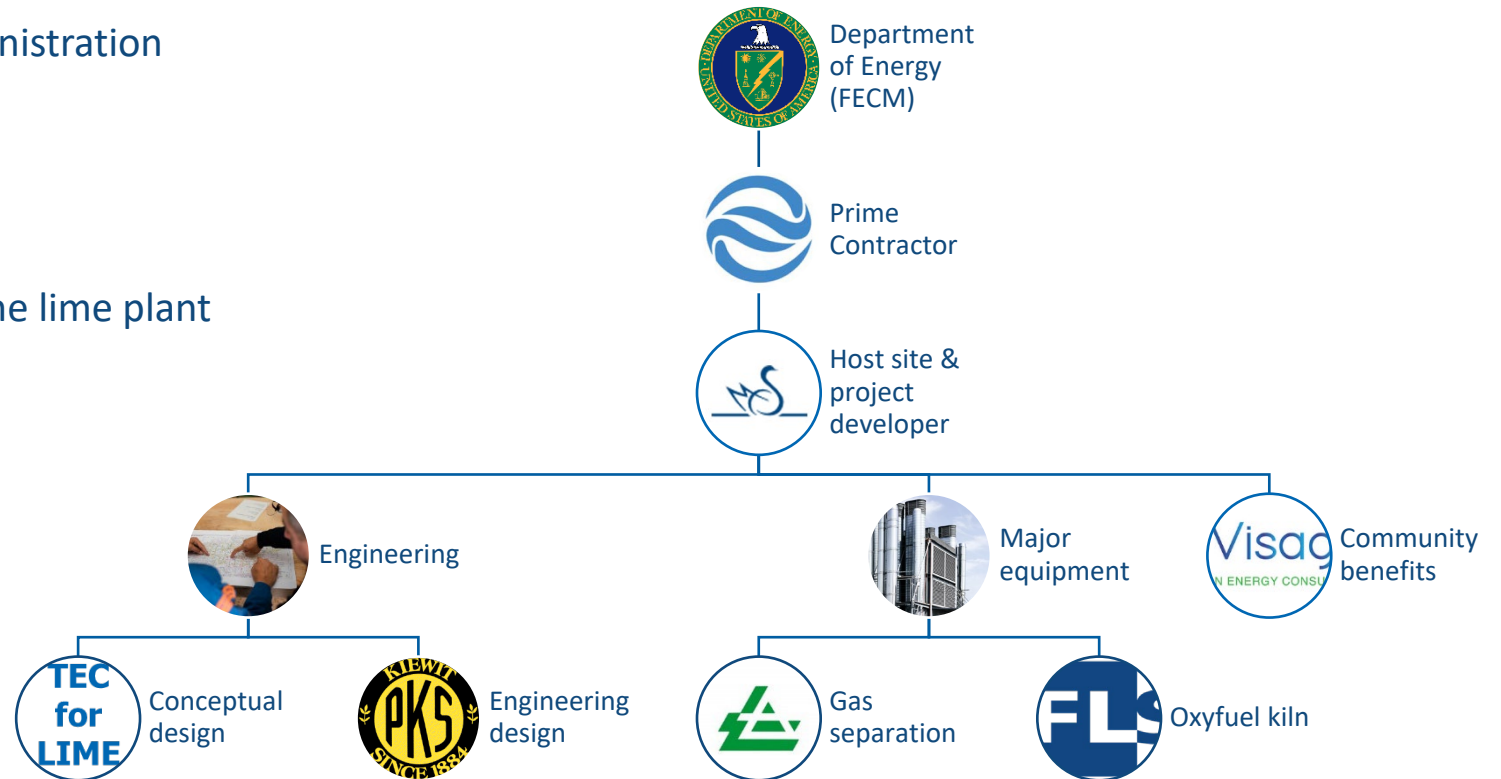
- Award Period: 7/27/2023 through 01/26/2025
- Project Funding
  - Total Funding: \$1,875,000
  - Federal Funding: \$1,500,000
  - Cost Share Funding: \$375,000
- DOE-NETL Team
  - Project Manager: Sai Gollakota
  - Contracting Officer: Lisa A. Kuzniar
  - Award Administrator: Davina Reed
- Project Objective

Execute and complete the initial design of a commercial-scale, oxyfuel fired flash calciner lime kiln with carbon capture system that:

  - separates CO<sub>2</sub> with 95% capture efficiency from process flue gas streams;
  - utilizes sustainably sourced biomass (SSB) alone or in combination with natural gas;
  - maximizes utilization of SSB (up to 90% thermal substitution);
  - captures and permanently sequesters 400,000 metric tonne per year (TPY) of CO<sub>2</sub> producing a net zero product and net negative emissions from operations

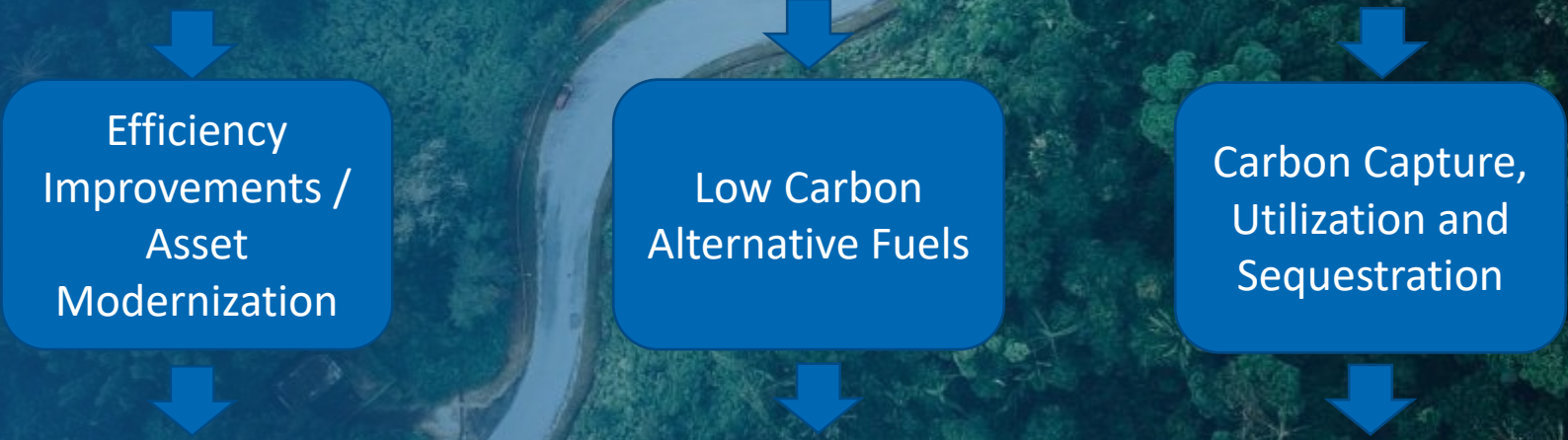
# Project Partners

- **Electricore:** Prime Contractor and program administration
- **Carmeuse:** Host site and project developer
- **Carmeuse Technologies:** Conceptual design of the lime plant and technical advisor
- **Kiewit:** EPC partner
- **FLSmidth:** Oxyfuel kiln design
- **Air Products:** Air separation and CO<sub>2</sub> purification unit design
- **Visage Energy:** Community benefits



# Carmeuse has ambitious GHG reduction Targets: Carbon neutral for our scope 1 emissions by 2050

## Pathways to Decarbonization



The Black River Net Zero Pre-Feed Study seeks to better understand the feasibility of implementing these pathways with a new modern Oxy-fired Gas Suspension Flash Calciner, utilizing low carbon fuels and sequestering CO2 emissions within known onsite geological storage

# Site Selection

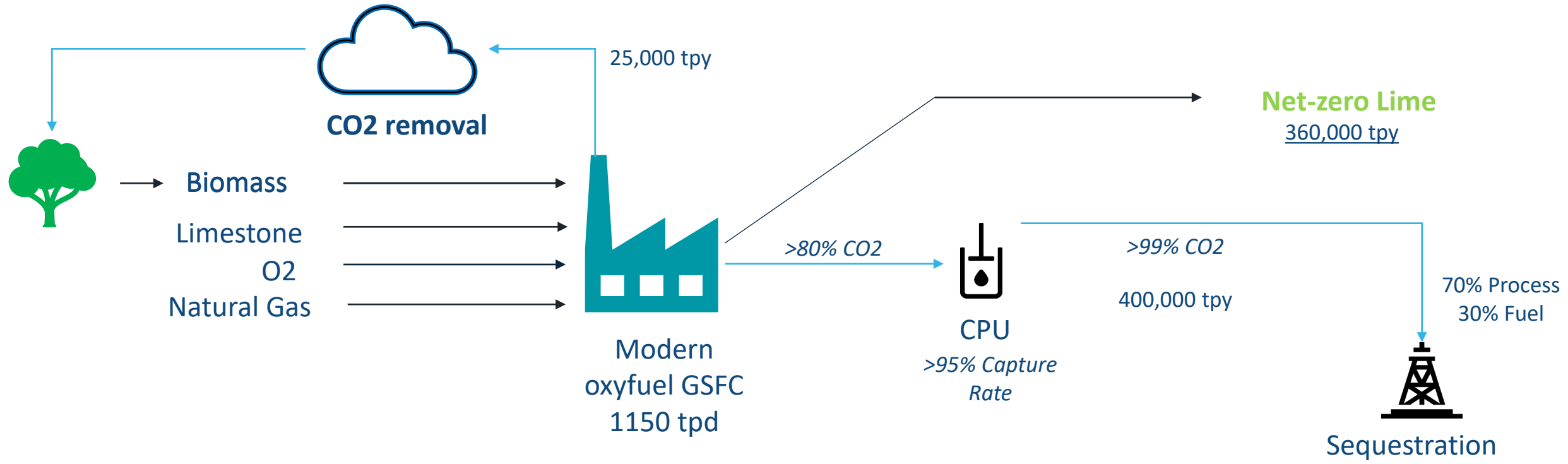
## Carmeuse Black River Plant in Butler, KY

- 5 kilns, 3 long rotary kilns, 2 pre-heater rotary kilns
- Favorable geology for on-site carbon sequestration within the Mt Simon formation
- Ability to ship via truck, rail and marine distribution to market
- Raw material reserves

This project considers the installation of a 1150 tpd Gas Suspension Flash Calciner to replace capacity from the 3 long rotary kilns currently in operation.



# Technology Overview



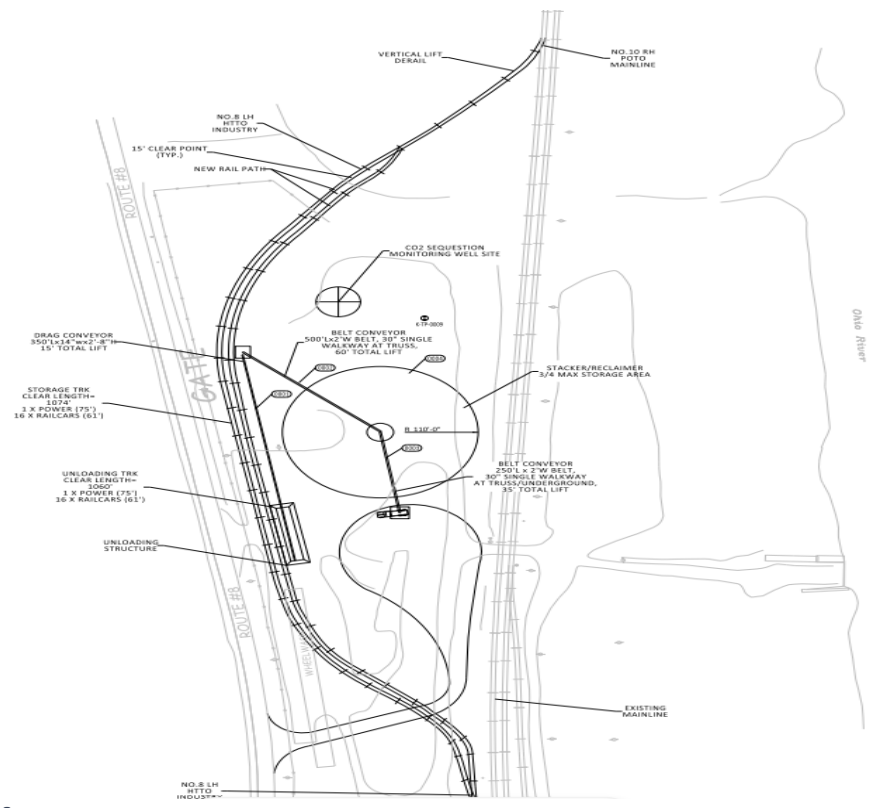
Oxyfuel Gas Suspension Flash Calciner design operates with pure oxygen for combustion avoiding nitrogen from air in the process, the CO<sub>2</sub> in flue gases exit the GSFC at >80% vol.(dry) and are concentrated and purified to >99% in the CPU for sequestration

The capture and sequestration of the biogenic CO<sub>2</sub> from biomass fuels allows for net negative emissions (BECCS) where the Lime production facility operates as a carbon removal facility

# Sustainably Sourced Biomass

2" wood chips (processed from railroad ties) delivered via rail

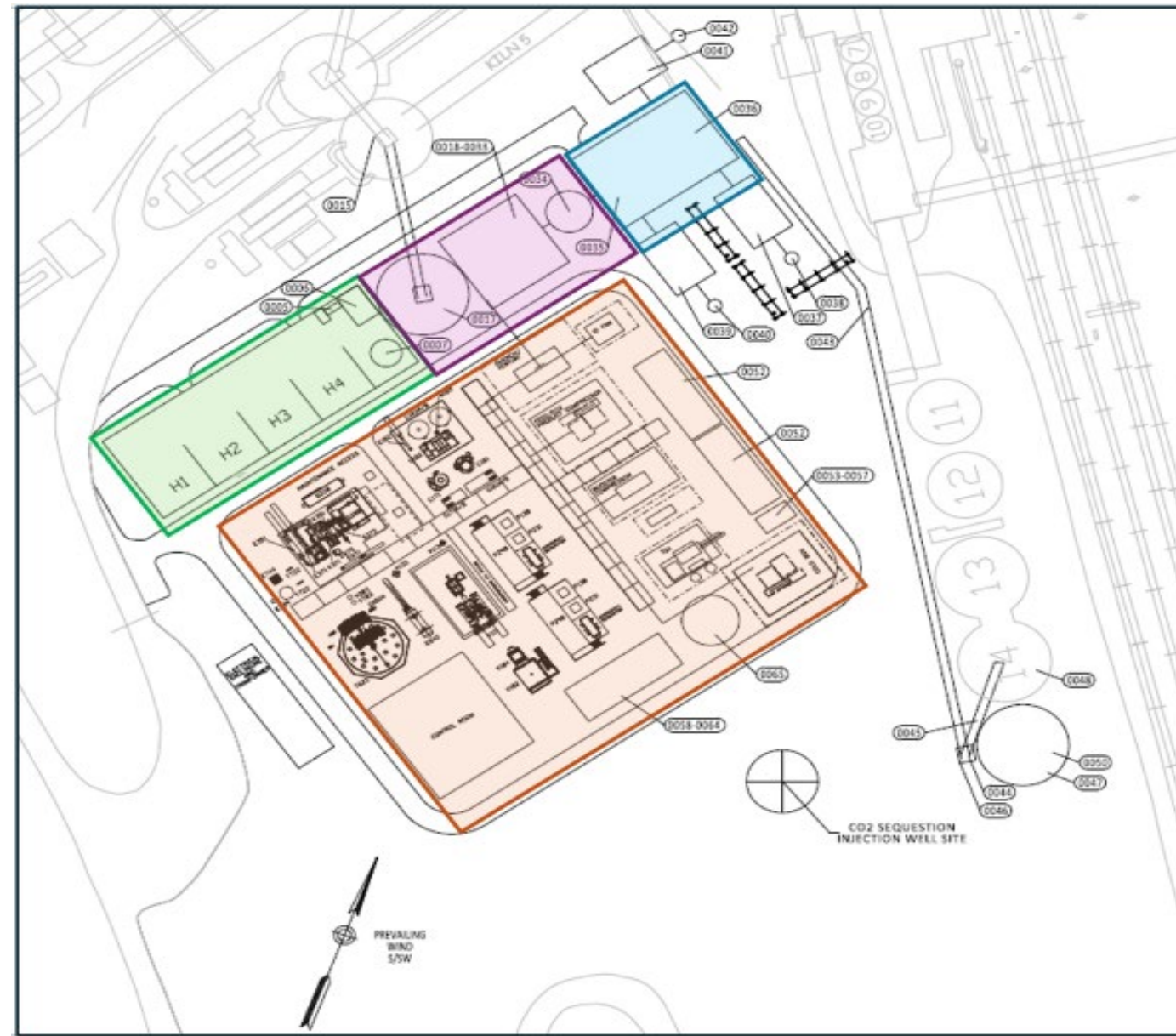
## Biomass Rail Unloading and Storage





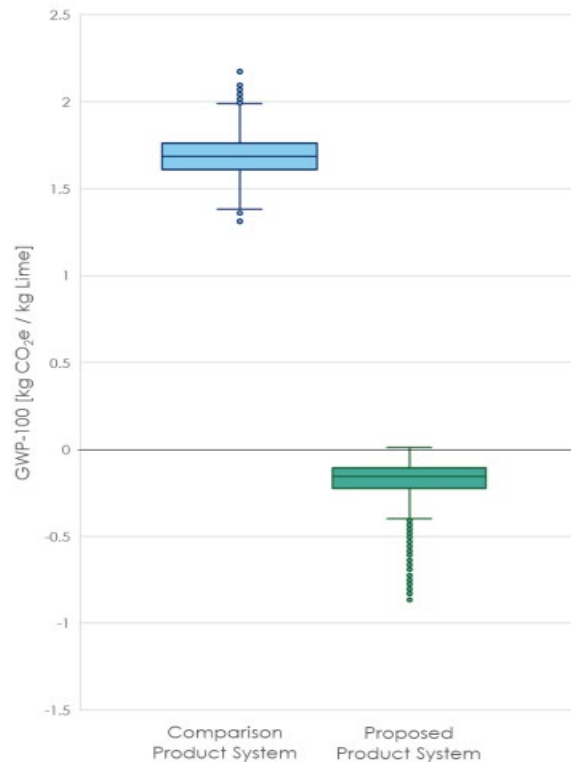
# Plot Plan

- Biomass Processing
- Limestone Storage & milling
- Gas Suspension Flash Calciner
- ASU / CPU, WSAC, Water Tower, Emergency Generators

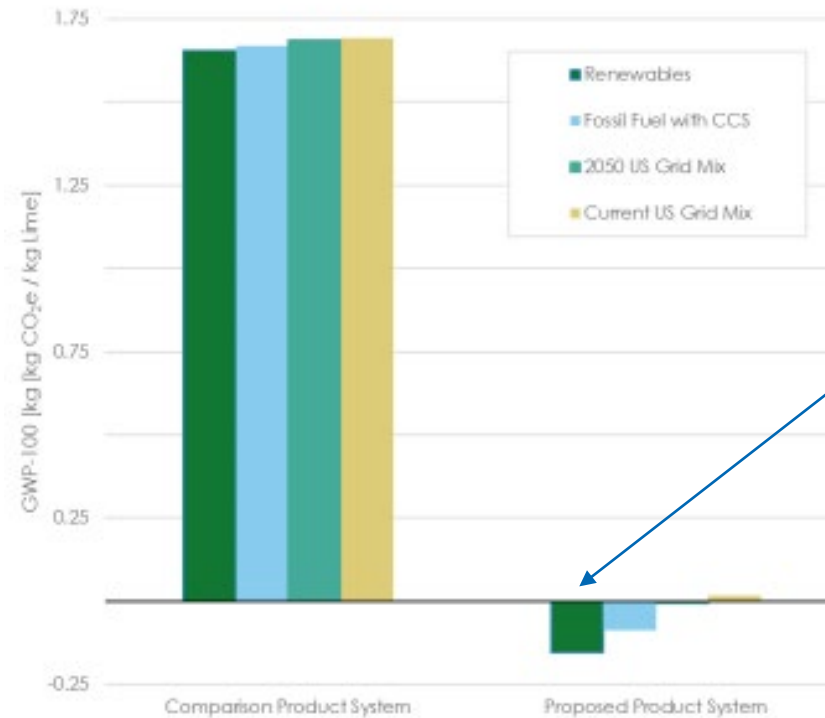


# Preliminary LCA – Emissions Reductions

## Monte Carlo simulation of Comparison and Proposed System GWP



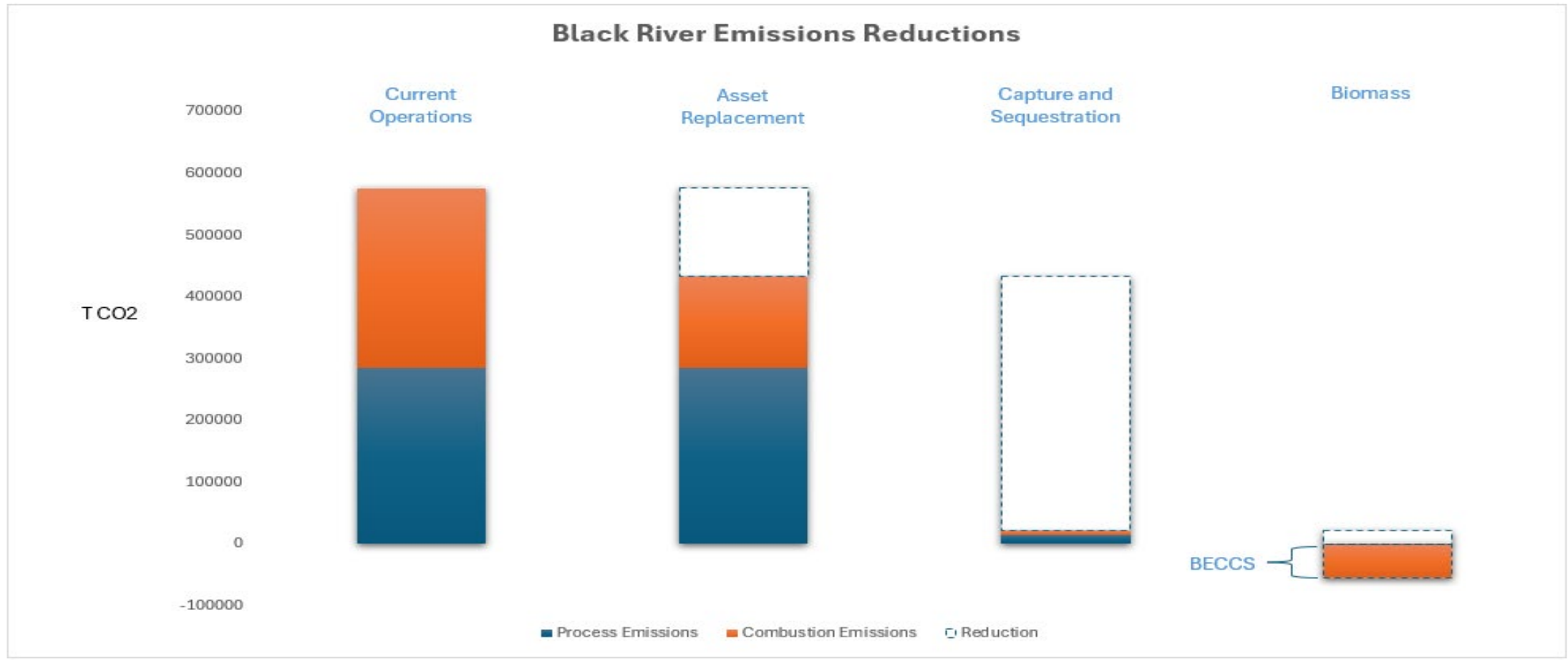
## GWP of Comparison and Proposed Systems under four electricity scenarios



TEA to assume procurement of Green Renewable Electricity achieving the negative emissions and accounting for the Scope 1 -> Scope 2 transition.

- Modified NETL CO<sub>2</sub>U openLCA LCI Database with project LCA and sensitivity/uncertainty analysis
- Completed NETL CO<sub>2</sub>U openLCA Results Contribution Tool

# Net Zero Lime Kiln and Carbon Removal Facility (BECCS)



# Decarbonized Summary Comparison

## Decarbonized Net Zero Lime - KPI Comparison

Comparison Unit	Unit	Current	Proposed	variance	Notes:
Installed Power	MW	5	25	20	5X, ASU / CPU make up 70% of incremental load
Specific Power Consumption	kwh / T lime	56	420	364	7.5 X, TEA to consider green renewable electricity price premium via PPA or other
Fuel Consumption	mmbtu / T lime	9.3	4.8	-4.5	0.5 X
CO2 specific emission	T CO2 / T lime	1.6	-0.15	-1.75	With renewable green electricity
Headcount	# of Employee's	25	76	46	3.0 X

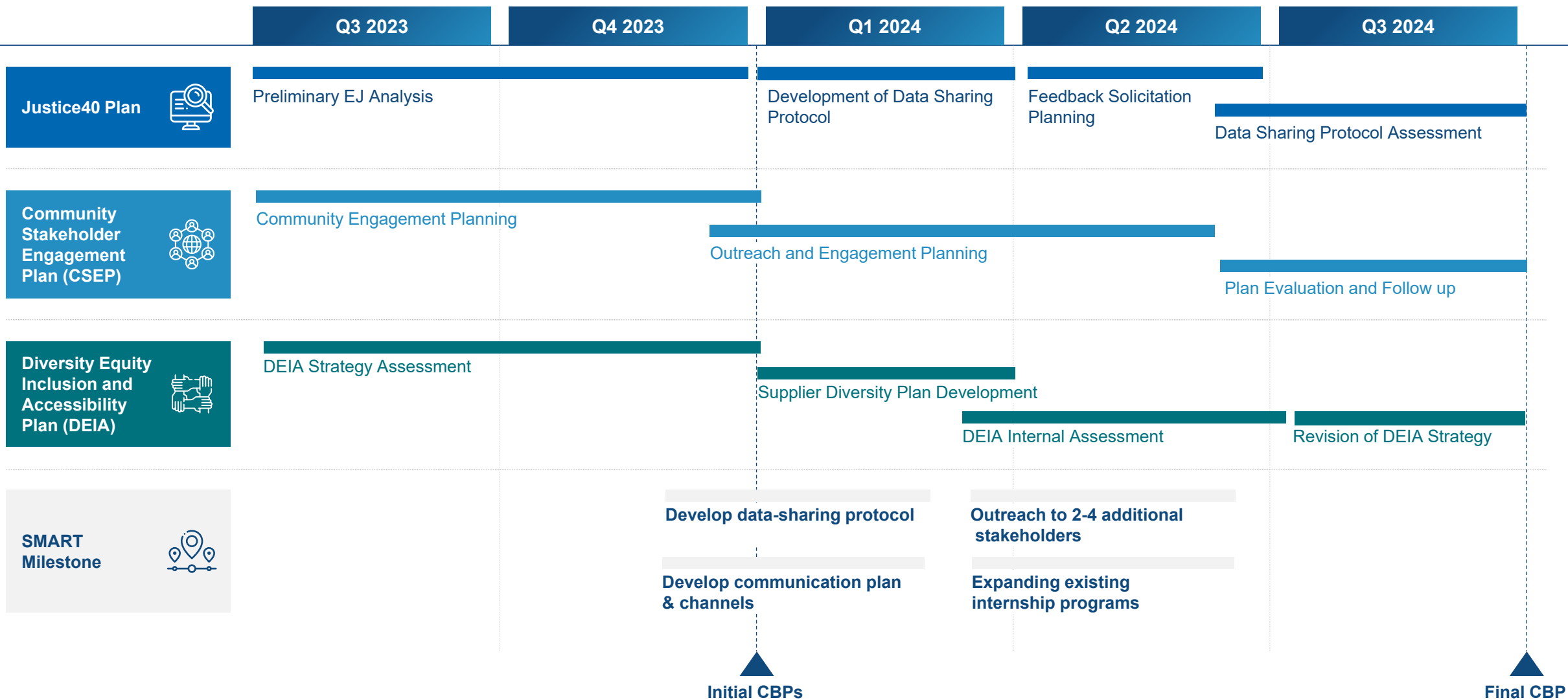
## Lessons Learned

- Wastewater treatment of impurities has significant impact to CapEx / OpEx.
  - Impurities derived from Direct Contact Cooler / CPU effluent of Flue Gas Condensates
  - Waste water treatment considers water recycle to maximum feasible extent driven by current permitting requirements
- Green premium on net zero CO<sub>2</sub> products not yet mature
- Wash column for acid gas removal was required despite oxy-fuel combustion, derivative of biomass selection
- AP CPU + Membrane system benefits overall system performance
  - Increases capture rate from approx. 95% to >99%
  - Reduces overall system O<sub>2</sub> consumption by 5 to 10% through recycle

## Plans for Future Testing / Development / Commercialization

- Oxy-fuel firing and the Carmeuse / FLS Gas Suspension Flash Calciner has promising technological advantages
  - Next step includes commercialization and deployment in a CCU project as an industrial demonstrator.
  - Identify synergies with GHG reduction potential in additional use cases
  
- Upon completion of final CapEX development (Class IV), review of significant cost drivers IE;
  - Biomass selection and associated impurities
    - Waste water treatment reduction
    - Acid gas removal reductions
    - Total LCA impacts from upstream treatment process of recycled railroad ties

# Community Benefits Plan Roadmap



## Work Plan

Task/ Subtask	Milestone Title & Description	Planned Completion Date	Actual Completion Date	Verification method
1.0	Kick-Off Meeting	10/02/2023	10/02/2023	Presentation File
1.1	Project Management Plan	08/25/2023	08/25/2023	Submitted PMP IAW Appendix G
1.2.1	Initial Technology Maturation Plan	10/25/2023	10/25/2023	Submitted TMP IAW Appendix J
1.2.2	Final Technology Maturation Plan	10/29/2024		Submitted TMP IAW Appendix J
1.3	Workforce Readiness Plan	10/29/2024		Submitted Workforce Readiness Plan IAW Appendix V
1.4	Data Management Plan	07/27/2023	07/27/2023	Submitted DMP IAW Appendix H
2.2	Preliminary Engineering Design Package	01/23/2024	01/23/2024	Submitted Preliminary Engineering Design Package
2.3; 2.4; 2.5	Final Engineering Design Package	10/29/2024		Submitted Final Engineering Design Package
2.6	Project Cost Estimate	10/29/2024		Submitted Project Cost Estimate IAW AACE Class 4
3.0	Business Case Analysis (BCA)	10/29/2024		Submitted Business Case Analysis (BCA) IAW Appendix S
4.0	Technology EH&S Risk Assessment	10/29/2024		Submitted EH&S Analysis IAW Appendix R
5.0.1	Initial Life Cycle Analysis (LCA)	11/24/2023	11/22/2024	Submitted LCA IAW Appendix P
5.0.2	Final Life Cycle Analysis (LCA)	10/29/2024		Submitted LCA IAW Appendix P
6.0	Environmental Justice Questionnaire	10/29/2024		Submitted Environmental Justice Questionnaire IAW Appendix T
7.0	Economic Revitalization and Job Creation Outcomes Questionnaire	10/29/2024		Submitted Economic Revitalization and Job Creation Outcomes Questionnaire IAW Appendix U
8.0.1	Initial Justice40 (J40) Initiative Plan	11/24/2023	11/22/2024	Submitted Justice40 (J40) Initiative Plan
8.0.2	Final Justice40 (J40) Initiative Plan	10/29/2024		Submitted Justice40 (J40) Initiative Plan
9.0.1	Initial Community and Stakeholder Engagement Plan (CSEP)	11/24/2023	11/22/2024	Submitted Community and Stakeholder Engagement Plan (CSEP)
9.0.2	Final Community and Stakeholder Engagement Plan (CSEP)	10/29/2024		Submitted Community and Stakeholder Engagement Plan (CSEP)



## Success Criteria

Budget Period	Date	Success Criteria
BP 1	1/26/2025	<ul style="list-style-type: none"><li data-bbox="805 658 2058 801">• Initial engineering design completed for commercial-scale, advanced carbon capture system that separates CO<sub>2</sub> with at least 95% capture efficiency from process streams at an existing industrial lime facility</li><li data-bbox="805 808 1798 851">• All required deliverables are complete and acceptable</li></ul>

# Thank You!





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