# Corrosion Rate Measurements of SC-CO2: impurity effects

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Direct Corrosion Costs: \$276 billion (3.1% of U.S. GDP)

### **General Corrosion Costs**

- In 1998, NACE found direct costs of corrosion in the US was \$276 billion
  - Estimated 25-30% saving if proper mitigation procedures used
- In 2013, costs had grown to \$450 billion in US;
  \$2.5 trillion world-wide
  - Again 15-35% saving with proper mitigation procedures
- Corrosion will continue or increase
  - Sour conditions are increasingly the norm
  - Hydrogen blending into natural gas
  - Hydrogen fuel cells

1998 U.S. GDP (\$8.79 trillion)

### COST OF CORROSION IN INDUSTRY CATEGORIES (\$137.9 BILLION)



NACE Report on Corrosion Costs and Preventive Strategies in the US (2002)

#### NIST

### **Pipeline Failures May Cause Public Safety Hazards**

According to the World Research Institute's 2008 report on CCS:

- "The main cause for CO<sub>2</sub> pipeline incidents appears to be material failure (i.e., relief valve failure, valve/gasket/weld or packing failure), followed by corrosion and outside force (Gale and Davidson 2007; Kadnar 2007)."
- "While  $CO_2$  is more benign than many other fluids transported through pipelines, it is important to note that the  $CO_2$  pipeline incident statistics are also probably related to the fact that there are many fewer miles of  $CO_2$  pipelines than pipelines transporting other fluids, and they tend to be located in less populated areas."
  - Current SCCO<sub>2</sub> pipelines have well regulated quality.
  - A large array of point sources will produce various levels of SCCO<sub>2</sub> quality, which pipelines must accommodate.

What are acceptable levels of contaminants in SCCO<sub>2</sub> to maintain pipeline integrity?

#### SCCO<sub>2</sub>: 5300 miles

To meet CCTS demands, may grow to the size of natural gas network

Natural Gas: >1,200,000 miles

Nordhaus and Pitlick 2009



# **Pipeline Steel Degradation in SC-CO2**

Constituents	Typical U.S. Industry Standard	DYNAMIS EU Standard	"Dried" Anthropogenic CO <sub>2</sub>
H <sub>2</sub> O	< 600 ppm	500 ppm	>2000 ppm?
$H_2S$	200 ppm	200 ppm	6,000 ppm
СО	2,000 ppm	2,000 ppm	4,000 ppm
O <sub>2</sub>	< 1,000 ppm	< 4 vol. %	6,000 ppm
CH <sub>4</sub>	< 5 vol. %	< 4 vol. %	-
N <sub>2</sub> /Ar/H <sub>2</sub>	< 4 vol. %	< 4 vol. %	41,000 ppm
SO <sub>X</sub>	100 ppm	100 ppm	5,000 ppm
NO <sub>X</sub>	100 ppm	100 ppm	100 ppm
CO <sub>2</sub>	>99.5 vol. %	>99.5 vol.%	-

Presence of water is a prerequisite for pipeline corrosion: keep water content low





**Result**: reported corrosion rates **vary** over **four orders of magnitude** (0.01 – 100 mm/year)



### **Material Measurement Needs**

### **Effect of Fluid Flow**



Higher impurity levels are expected to produce thicker corrosion products which could lead to spallation and erosion-corrosion

**Flow Rate** 

### **Contaminant Consumption**



### **Impurity Interactions**



### **Fracture and Fatigue?**



No published research has shown the influence of SCCO<sub>2</sub> environments on environmentally assisted cracking



### Flow rate is a key parameter



L. Wei, X. Panga, K. Gaoa, Effect of flow rate on localized corrosion of X70 steel in supercritical CO2 environments, Corr. Sci. **136** (2018)



#### MATERIAL MEASUREMENT LABORATORY







How is flow rate simulated in the lab

What is the impact of flow rate? How is flow rate simulated in the lab?

Dugstad et al. 2014

### Flow rate is a key parameter



Rotating Cage

- State-of-the-art test facility for SCCO<sub>2</sub> environmental testing
- Static and dynamic test applications to evaluate flowinduced damage on multiple alloys simultaneously
- 77 bar, 54 °C and 84 bar, 40 °C tests
- IGS Analyzer (FTIR) for contaminant monitoring
- Precision imaging facility for characterization of microscopic structures and corrosion processes on steel alloys.





- Inside a walk-in fume hood for compatibility with H<sub>2</sub>S testing
- Remote monitoring and continuous data-logging capabilities







Specification	Large Pressure Vessel	Small Pressure Vessel
Number Available	1	2
Internal Volume	7.7 L	4.0 L
Construction Material	316 SS	316 SS
Max Allowable Working Temperature	250 °C	500 °C
Max Allowable Working Pressure	206 bar (3000 psi)	103 bar (1500 psi)
Stirring Capabilities?	YES	NO

3 high-temperature, high-pressure test chambers. Rated for 300 bar at 500 °C. One stirred chamber (can vary flowrate)



- Specimens tested in stirred chamber
- Test coupons are 75 mm x 19 mm x 3 mm thick





### **Test Results**





### **Thermodynamics Issues**

### • RefProp software

- Chris Muzny, Mark McLinden
- Thermophysical properties of CO2 plus impurities
- Can be used for pipeline blowdown calculations, for instance



### Key Takeaways and Next Steps

- NIST has SC-CO2 testing facility capabilities for multiple impurities, flow effects, and mechanical load
  - Facility not currently active needs 2 months to bring back up
    - Resource needed 1 student/technician to help bring up and to run tests
- SC-CO2 corrosion rates due to impurity interactions need to be measured as function of temperature/pressure/flow rate/...
  - Start with "dry anthropogenic CO2" condition then reduce to individual effects?
- Round-robin testing should be a goal when multiple corrosion laboratories are up and running
- Goal: Help determine conditions for NACE or equivalent standards
- Reach goal: Determine mechanism of corrosion to see whether mitigating technologies can be developed





# Questions?



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- One stirred chamber (can vary flowrate)









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- 3 high temperature, high-pressure test chambers. Rated for 300 bar at 500 °C.
- One stirred chamber (can vary flowrate)







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 Specimens tested in static chambers











### **Test Results - FTIR**



Figure 4: FTIR Spectra taken in a  $CO_2$  matrix with varying water concentrations. Both the full spectrum (top) and an enlarged region containing several bands for water (bottom) are shown for water contents varying from 100 – 1500 ppm.



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