



Hydrogen Storage for Load-Following and Clean Power: Duct Firing of Hydrogen to Improve the Capacity Factor of NGCC (DE-FE0032008)

DOE Fossil Energy and Carbon Management (FECM)

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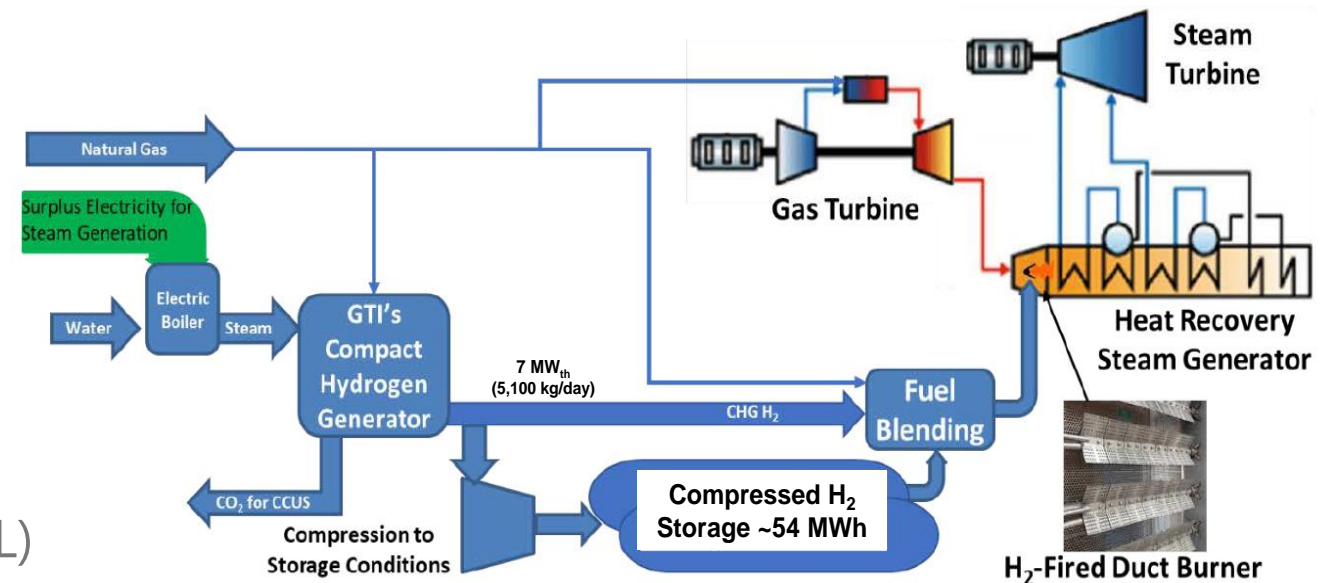
GTI Energy | April 19th, 2023

Agenda

- Project Overview/Team members
- Project Objectives
- Proposed System/Benefits
- Phase I Feasibility Study Results
- Phase II Pre-FEED Study Scope/Activities
- Phase II Pre-FEED Study Schedule
- Summary

Hydrogen Storage for Load-Following and Clean Power Project

- Scope: Pre-FEED study to advance the concept of asset-integrated production and intermediate duration (~54 MWh) storage of Blue Hydrogen for electric load following
- Team:
 - GTI Energy
 - EPRI
 - Southern Company
 - Pacific Gas & Electric
 - Service & Technology Corp
 - Zeeco
 - Low Carbon Resources Initiative
 - U.S. Department of Energy (DOE NETL)
- Schedule: Phase II through 9/2023
- Funding: Phase II Pre-Feed \$800K



GTI Hydrogen Generation (CHG) and integrated H₂ storage with GTCC

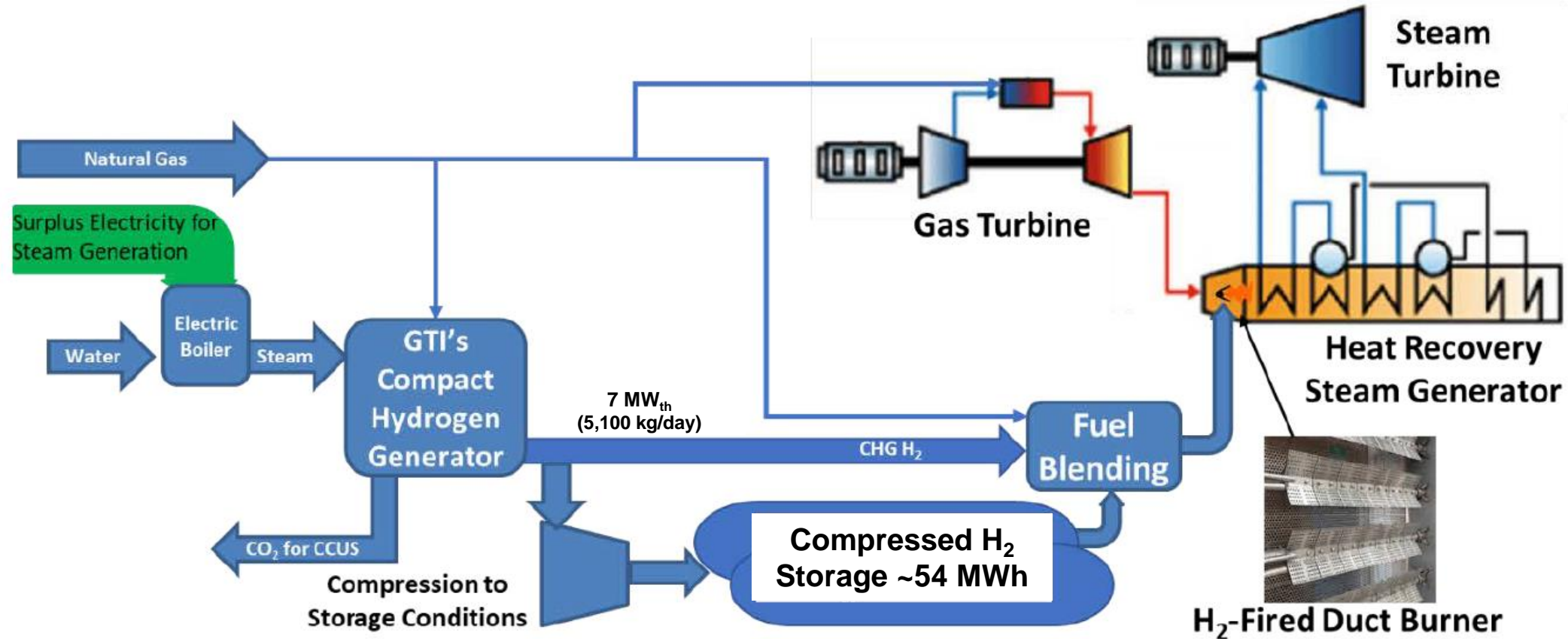


Hydrogen Storage for Load-Following and Clean Power Project Objectives



- Pre-FEED study of the concept of using asset-integrated production and intermediate duration (~54 MWh) storage of Blue Hydrogen (i.e., fossil fuel-derived, low-carbon hydrogen) for electric power generation to achieve load following
 - Existing Natural Gas Combined Cycle (NGCC) plant in Southern Company fleet
 - Retrofit with GTI's Compact Hydrogen Generator (CHG) integrated with:
 - CO₂ capture ready
 - Storage of compressed H₂ in roadable storage
 - H₂ duct burner firing within existing heat recovery steam generator (HRSG) section of an NGCC plant
 - Pathfinder for hydrogen power generation while large frame hydrogen-fired gas turbines are matured

Hydrogen Storage for Load-Following and Clean Power Project - Proposed System



- Commercial scale: Baseload = 690 MW_e, Duct-burner Augmentation = 176 MW_e Peak
- Demonstration scale: 84 MW_e, Duct-burner Augmentation = 38 MW_e Peak

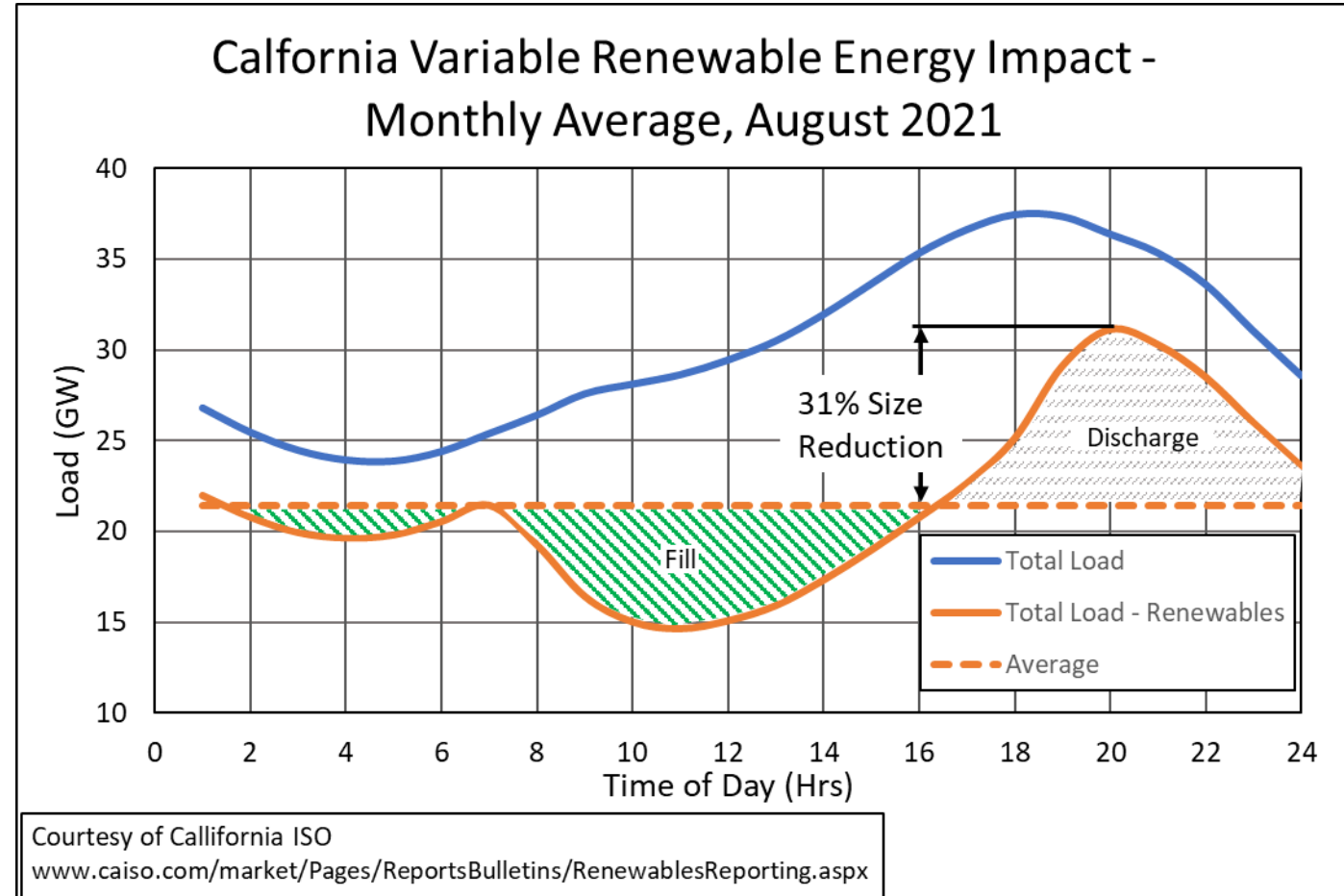
GTI Energy Hydrogen Generation (CHG) and Integrated H₂ Storage with GTCC Concept Benefits



- Low-carbon H₂ produced by the CHG provides dispatchable H₂ production and is significantly cheaper than SMR-based H₂
- Utilization of stored H₂ as the energy carrier enables the system to be dispatchable and support peak energy demands with minimal impact of the fossil asset
 - This offers flexibility in VRE markets
 - Produce faster total plant ramp rates, improving efficiency
- Demonstrates utilization of stored H₂ in an economical and low-carbon manner
 - System is agnostic to the hydrogen source
 - Can provide hydrogen for other uses
- Pathfinder for hydrogen power generation as hydrogen-fired large frame gas turbines are matured

H₂ Storage Concept Benefit

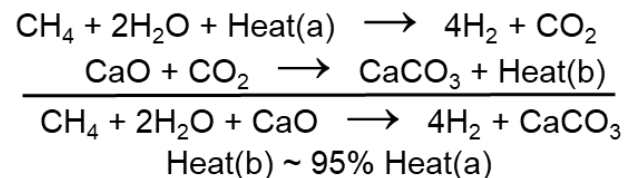
- Hydrogen storage minimizes the size of the hydrogen generation system by adding capacitance to the system.
 - Lowers overall cost (plant size reduction vs. H₂ storage costs¹)
 - Electric utility industry challenge gets worse with increased renewables
- Further benefits of storage concept is the ability to add H₂ from other sources (ex. - produced from curtailed renewable electricity) and provide H₂ to other applications (vehicles, heating, etc.)



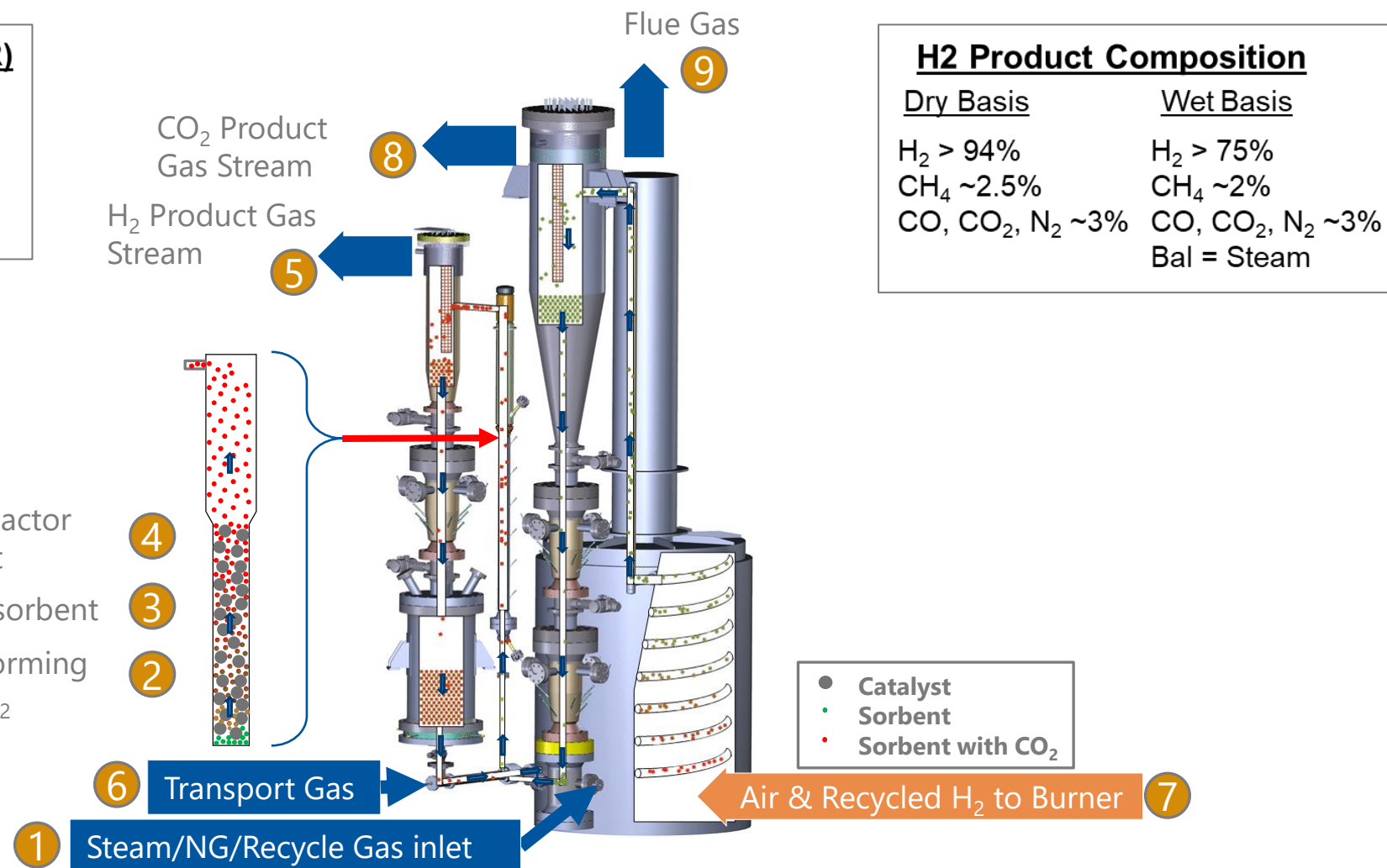
¹ Reference: Ahluwalia, R. K., et. al., *System Level Analysis of Hydrogen Storage Options*, U.S. DOE Hydrogen and Fuel Cells Program 2019 Annual Merit Review and Peer Evaluation Meeting, Washington D.C. April 29-May1, 2019, Project ID: ST001

GTI's CHG Blue Hydrogen Process Schematic

Sorption Enhanced Reforming (SER)



Sorbent elutriates through reactor to filter while heavier catalyst remains
CO₂ absorbed by sorbent
Steam Methane Reforming produces H₂ and CO₂



H₂ Product Composition

Dry Basis

H₂ > 94%
CH₄ ~2.5%
CO, CO₂, N₂ ~3%

Wet Basis

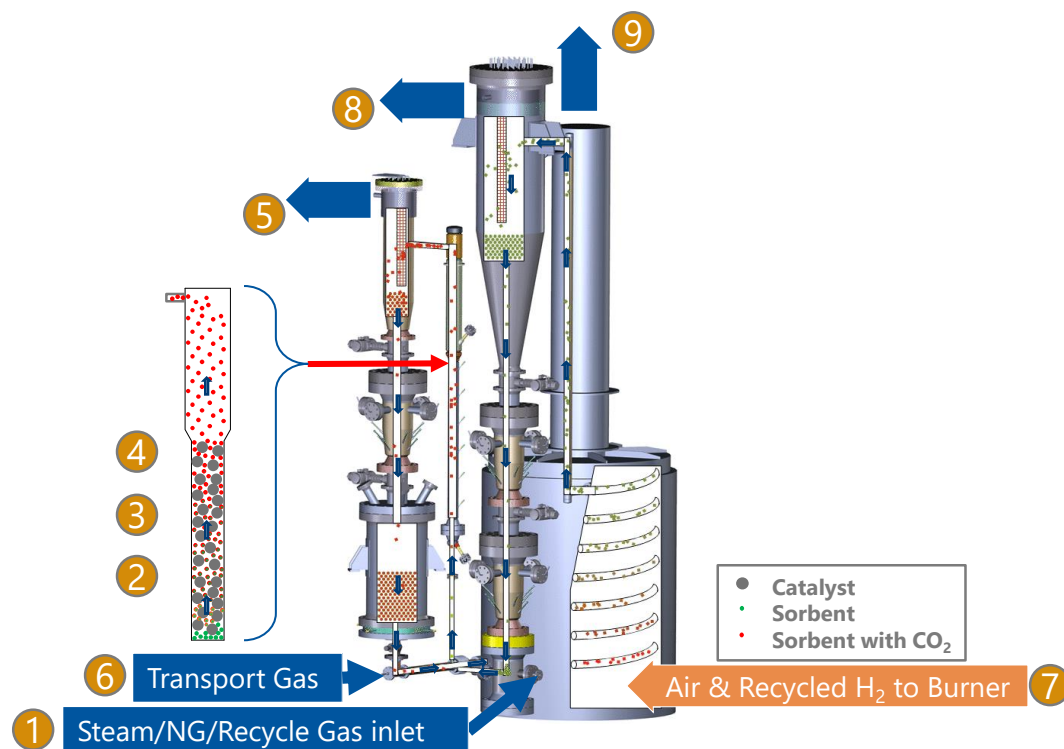
H₂ > 75%
CH₄ ~2%
CO, CO₂, N₂ ~3%
Bal = Steam

GTI's CHG Blue Hydrogen Economic Advantages

- Sorbent enhanced reforming adds solid sorbent to SMR chemistry
 - Balances heat allowing simple reactor and eliminates WGS reactor = lower cost
 - Inherent CO₂ capture reduces cost



Drives least cost over competing technologies



Configuration	TPC (\$MM)	% of SMR	LCOH (\$/kg)	% less than SMR
SMR w/o Capture	277		\$1.03	
CHG w/o Capture	159	42.6%	\$0.84	19.2%
SMR w/90% Capture	497		\$1.68	
CHG w/90% Capture	244	50.9%	\$1.21	27.9%

Hydrogen Storage for Load-Following and Clean Power Project - Phase I Feasibility Study Results



- 12-month Phase I Feasibility study confirmed the system is feasible
 - Hydrogen produced by the CHG/utilized in a duct burner in a HRSG
 - Demonstration will include 54 MWh of hydrogen storage
 - H_2 production is relatively constant by storing H_2
 - CO_2 capture inherent to the CHG process can capture 90% of the CO_2
 - Firing rate of the duct burner is varied for plant response to fluctuations of electrical load
- Proposed system is an improvement over alternate low carbon dispatchable power options
 - 17.4% lower levelized cost relative to an SMR with an amine system for CO_2 capture
- Revenues are improved by arbitrage between use of low-cost off-peak variable electricity generation or use of stored H_2 under peak demand

Phase II (Pre-FEED) Scope/Activities

Overall Objective - Be Ready to Launch FEED



- Pre-FEED tasks include:
 - Updating the requirements, Concept of Operations, component modeling and system modeling, performance estimates, emission estimates, fluid/process conditions (PFD), utility usage, and facility sizing/definition
 - TEA
 - Commercial Scale Plant Economics
 - Improved cost estimates from EPC (SCS) and potential CHG OEM (STC)
 - Update Technology Gaps/TMP
 - Develop Environmental Information Volume
 - Conceptual design for the dual fuel burner

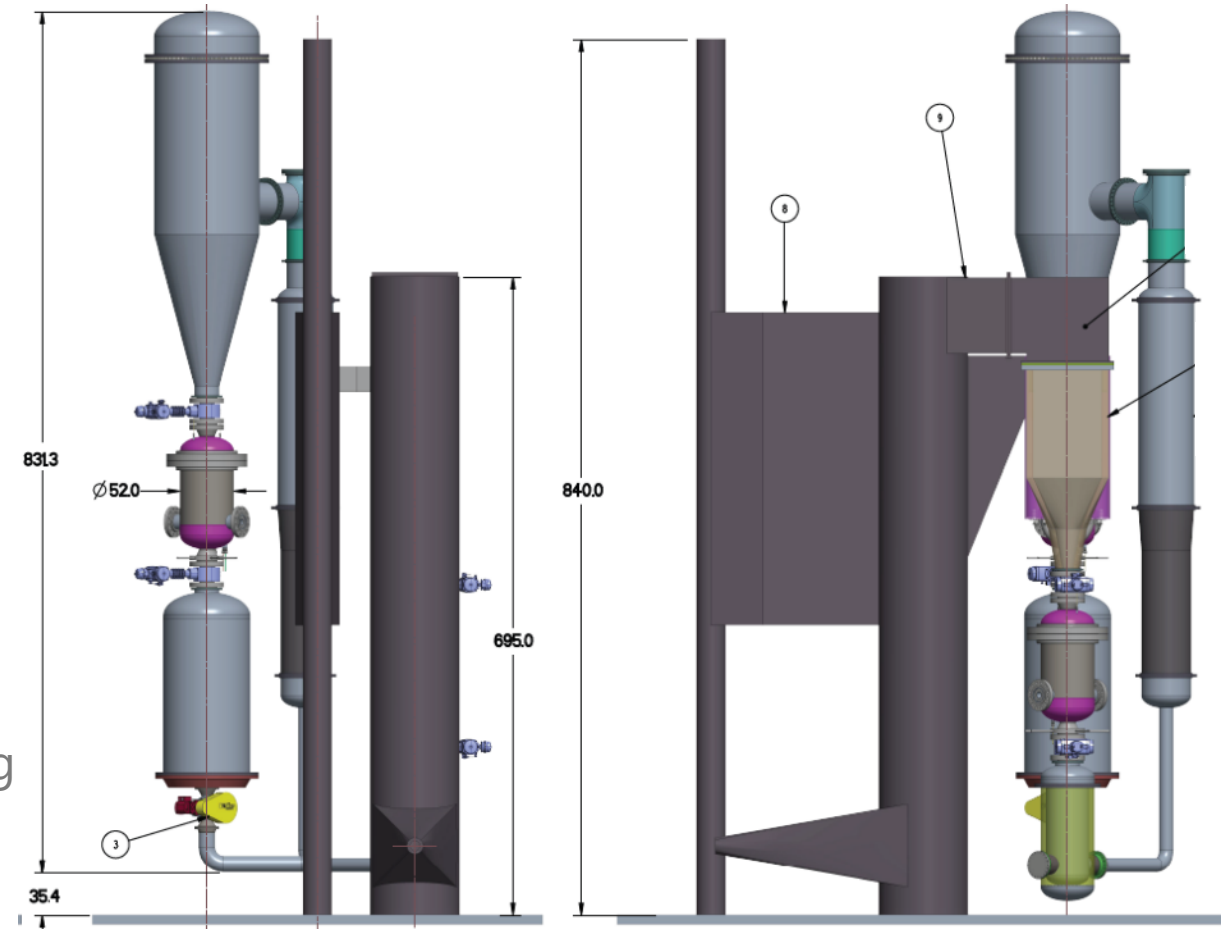
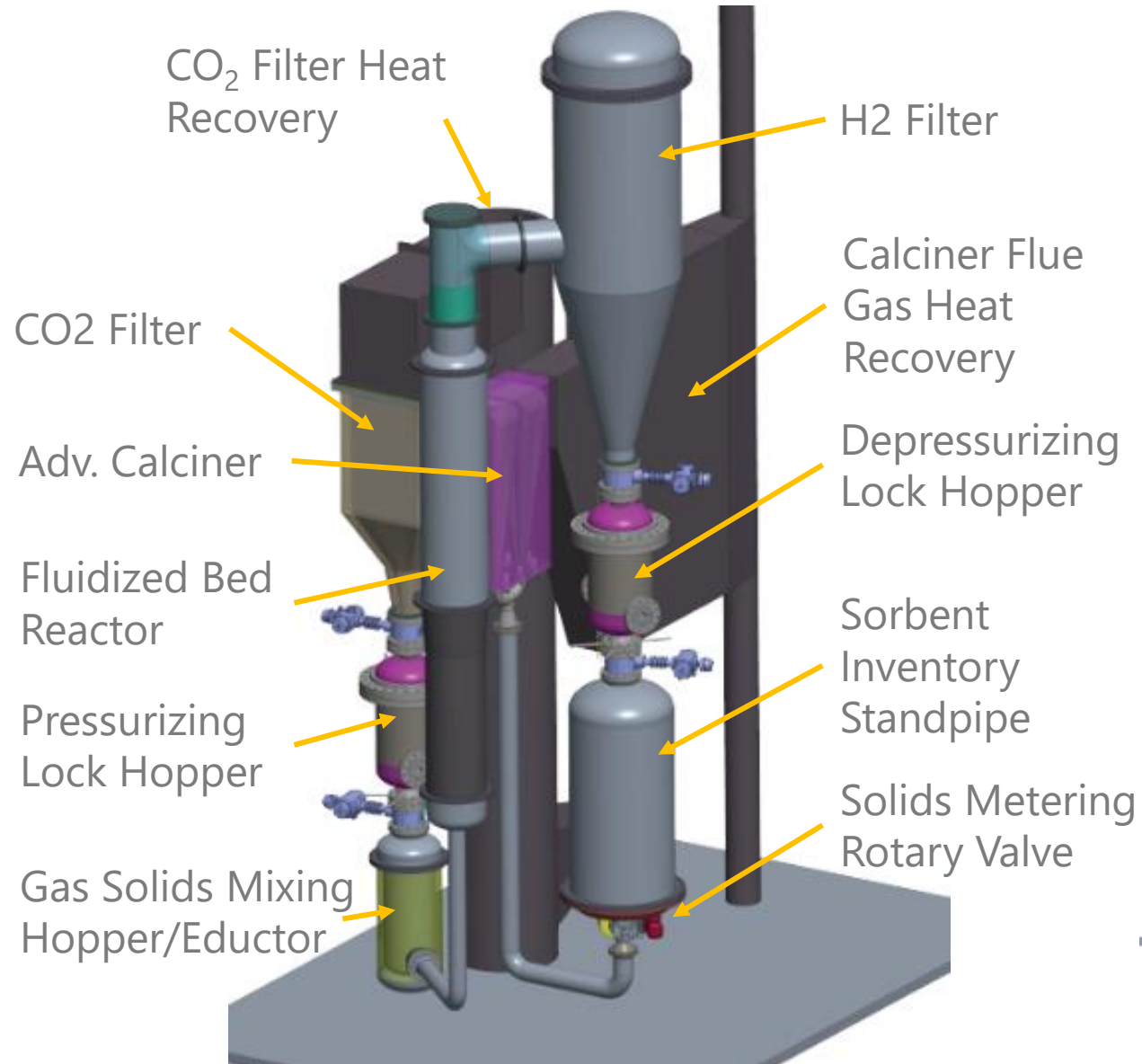
Phase II Pre-FEED Status

System Requirements at Battery Limits

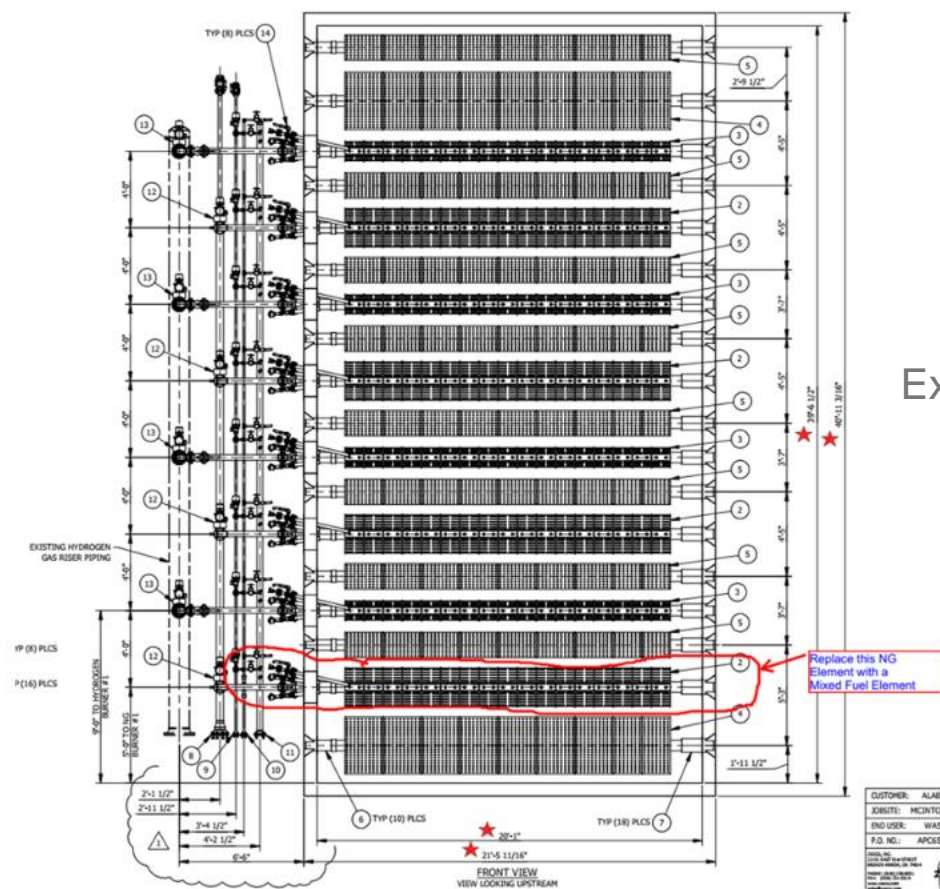
Component	Inputs	Outputs		Units	
	Flow	Flow			
Natural Gas	1,618			lb/hr	
HP BFW	5,463			lb/hr	
LP BFW	903			lb/hr	
Sorbent	14,327			lb/hr	
Cooling Water	28,436			lb/hr	
Power	0.521 Peak 0.198 Avg.			MWe	
CO2 from Calciner		3,918		lb/hr	
Product Gas		609		Lb/hr	
H2		465.2	96.9%	lb/hr	Mol%
CH4		87.8	2.3%	lb/hr	Mol%
CO2		20.9	0.2%	lb/hr	Mol%
CO		14.2	0.2%	lb/hr	Mol%
N2		15.5	0.2%	lb/hr	Mol%
H2O		4.33	0.1%	lb/hr	Mol%
Condensate Water		2,037 H2, 900 CO2		lb/hr	
Total H2 Storage (8 hr. fill)		0.7		MMSCF	
Product Gas Heat		7.7 (7.1 H2)		MWth	

- Requirements updated
- Process model updated
 - PFD updated
 - Performance estimates completed
- Layout completed
- Duct Burner emission estimates completed

GTI's 7.7 MW_{th} CHG for Pre-FEED study



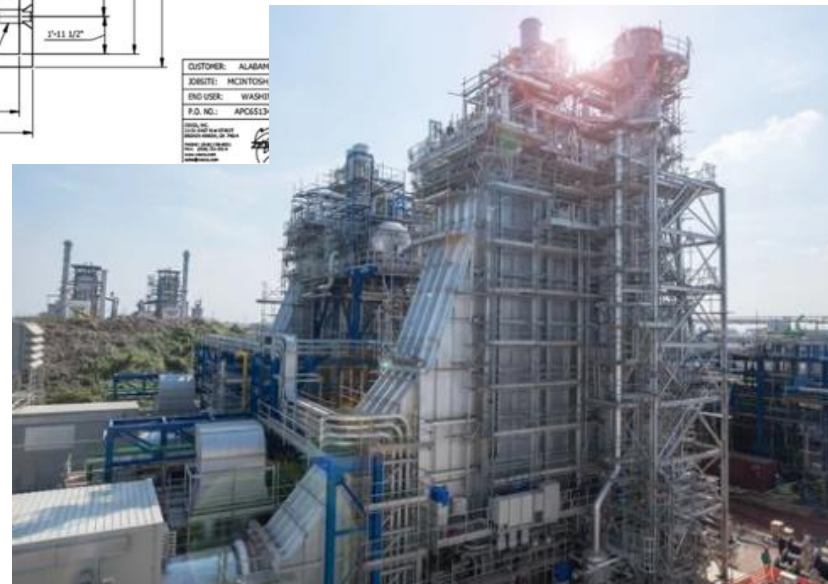
Phase II Pre-FEED Dual Fuel Duct Burner



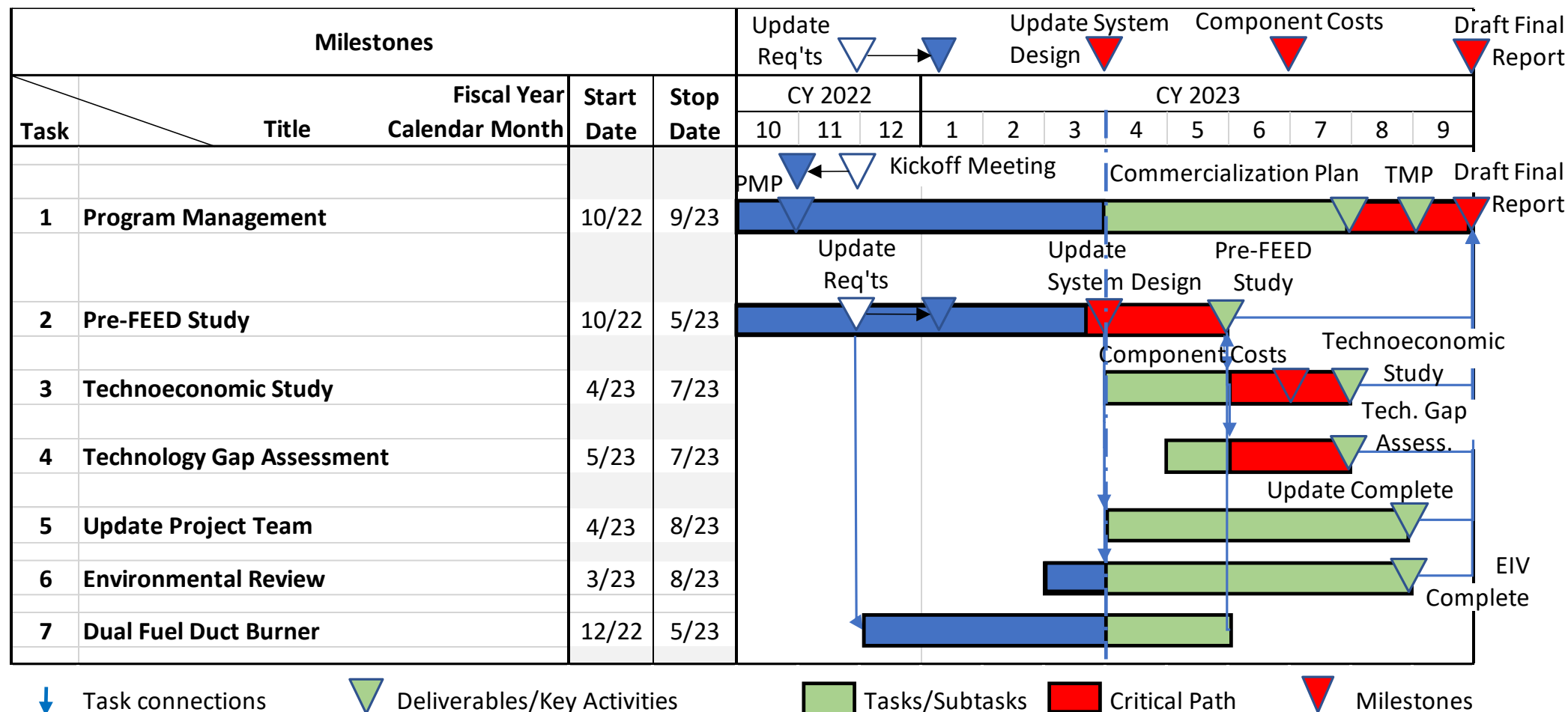
Existing HRSG and Burners

- Current Heat Recovery Steam Generator (HRSG) Duct Burners
 - Four (4) Hydrogen Duct Burner Elements (see item 3)
 - Four (4) Natural Gas Duct Burner Elements (see item 2)
- Bottom Natural Gas Element clouded in red will be replaced with a Dual Fuel Burner

HRSG from significantly larger power plant



Phase II Pre-FEED Schedule



Hydrogen Storage for Load-Following and Clean Power Project Summary



- 12-month Phase I Feasibility study confirmed the system is feasible
 - 17.4% lower cost than alternate low carbon dispatchable power option
- 12-month Phase II Pre-FEED is ongoing:
 - Requirements definition, process modeling, performance, emissions, PFD, utility usage, and facility sizing/definition are now complete or ongoing for specific site
 - Gathering detailed costs for the TEA
 - Conceptual design for the dual fuel burner ongoing
- Team is pursuing multiple paths for the demonstration (FEED is the next step)



Team thanks Heather Hunter (DOE PM) and DOE for the support to the project



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