Multi-scale Modeling Using IDAES

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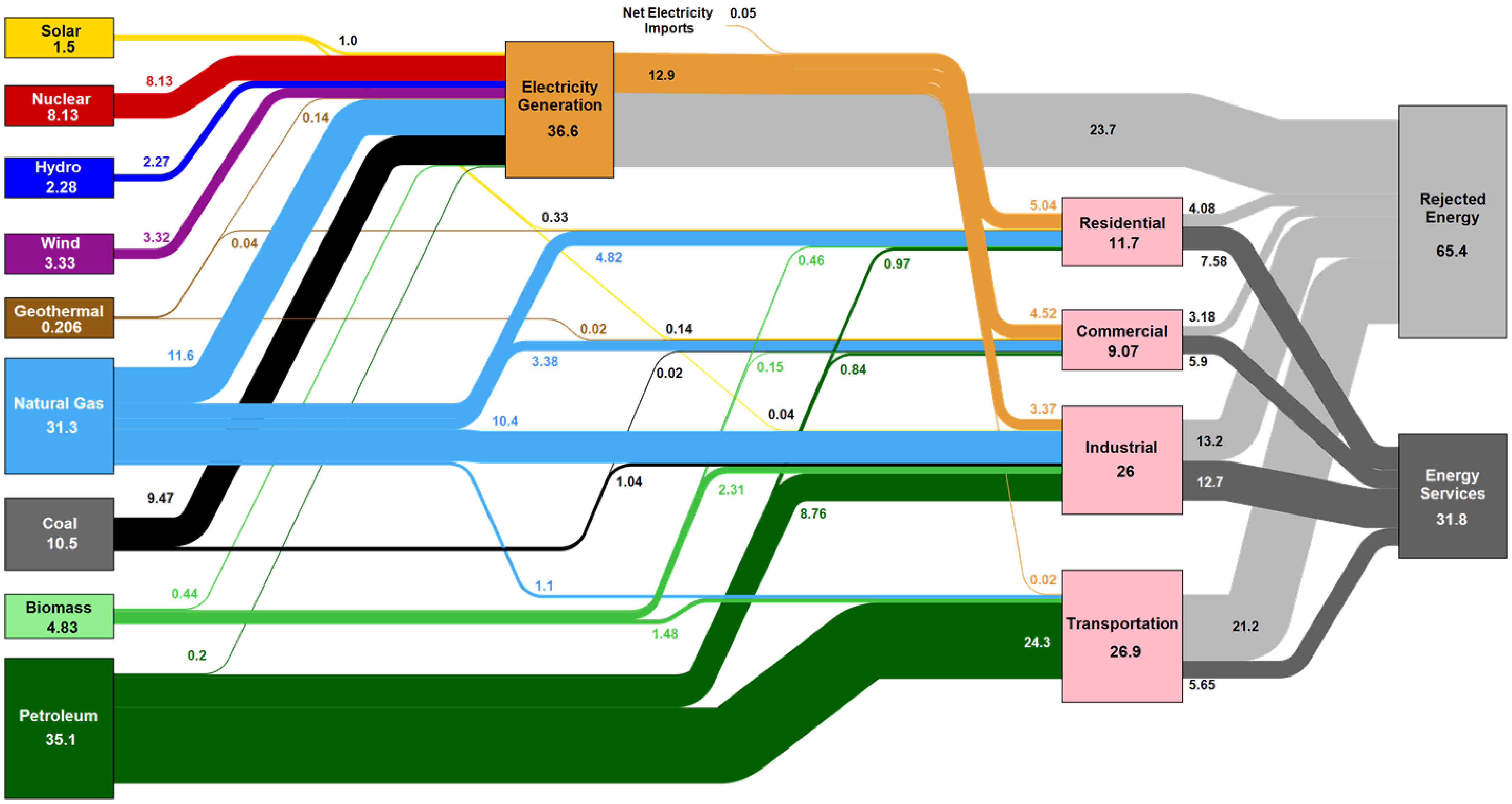
April 19th, 2023

Estimated U.S. Energy Consumption in 2021: 97.3 Quads



Source: LLNL March, 2022. Data is based on DOE/EIA MER (2021). If this information or a reproduction of it is used, credit must be given to the Lawrence Livermore National Laboratory and the Department of Energy, under whose auspices the work was performed. Distributed electricity represents only retail electricity sales and does not include self-generation. EIA reports consumption of renewable resources (i.e., hydro, wind, geothermal and solar) for electricity in BTU-equivalent values by assuming a typical fossil fuel plant heat rate. The efficiency of electricity production is calculated as the total retail electricity delivered divided by the primary energy input into electricity generation. End use efficiency is estimated as 65% for the residential sector, 65% for the commercial sector, 21% for the transportation sector and 49% for the industrial sector, which was updated in 2017 to reflect DOE's analysis of manufacturing. Totals may not equal sum of components due to independent rounding. LLNL-MI-410527

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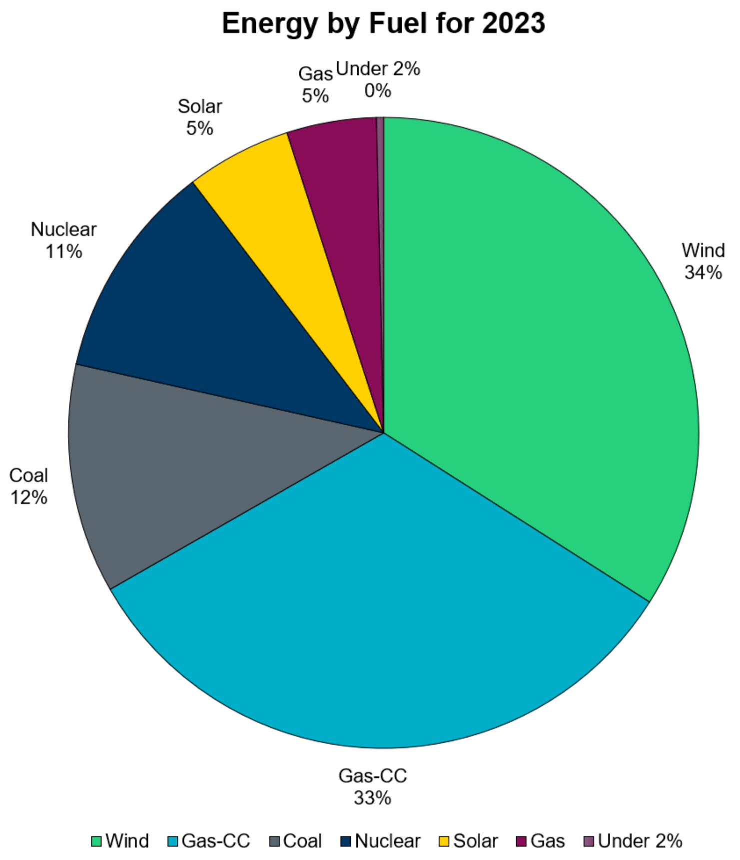
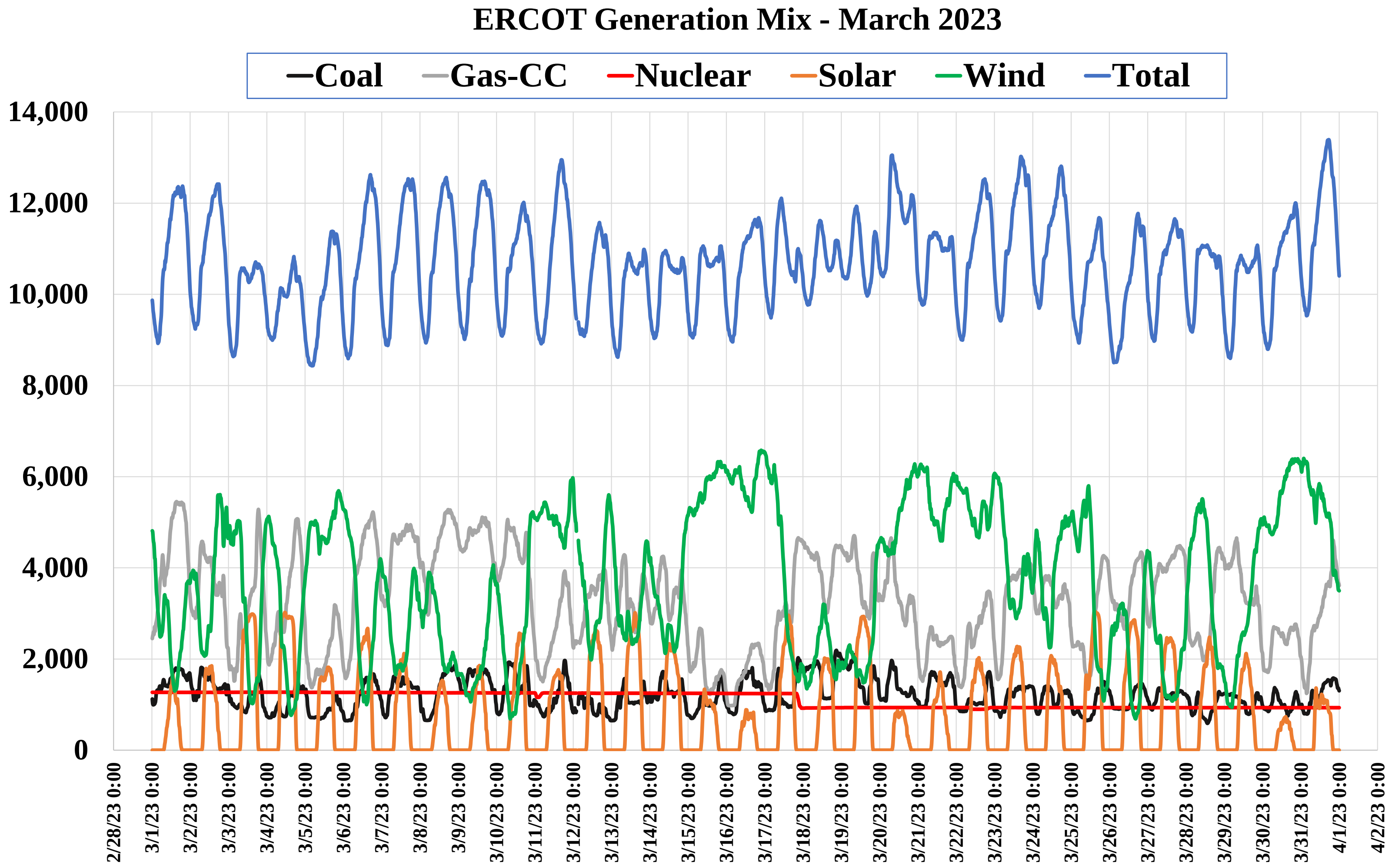
Evolving Grid Increasingly Requires Flexibility

Data for Electric Reliability Council of Texas (ERCOT) ISO





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Source: https://www.ercot.com/gridinfo/generation

IDAES Integrated Platform

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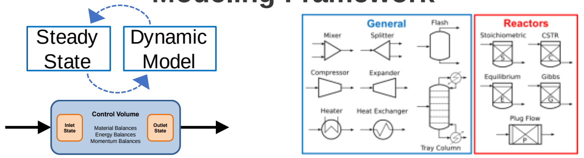
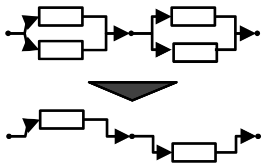
Modeling Framework



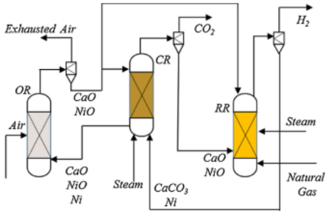
Hierarchical - Steady-State & Dynamic - Model Libraries

Conceptual Design



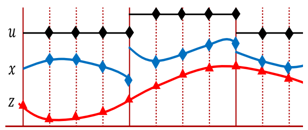
PYOMO GDP

Plant Design
Process Optimization

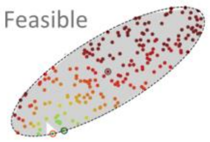


Process Operations
Dynamics & Control

caprese



Uncertainty Quantification
Robust Optimization

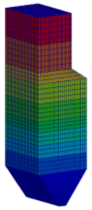


PyROS

AI/ML
Surrogate Modeling

ALAMO
a black-box modeling tool

PySMO



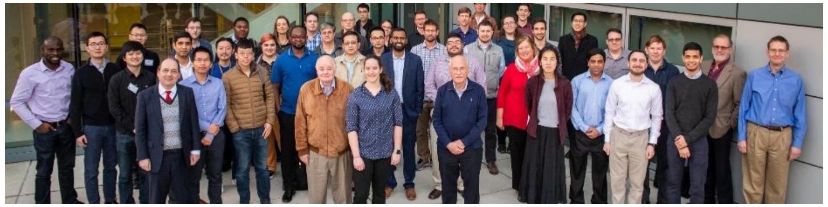
Enterprise Optimization
Grid & Planning

Materials
Optimization

MatOpt
Nanomaterials optimization

Open Source: https://github.com/IDAES/idaes-pse

Lee, et al., *J. of Adv. Manufacturing and Processing* (2021)



2020 R&D 100 WINNER

NATIONAL ENERGY TECHNOLOGY LABORATORY
BERKELEY LAB
Sandia National Laboratories
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West Virginia University
UNIVERSITY OF NOTRE DAME
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PYOMO

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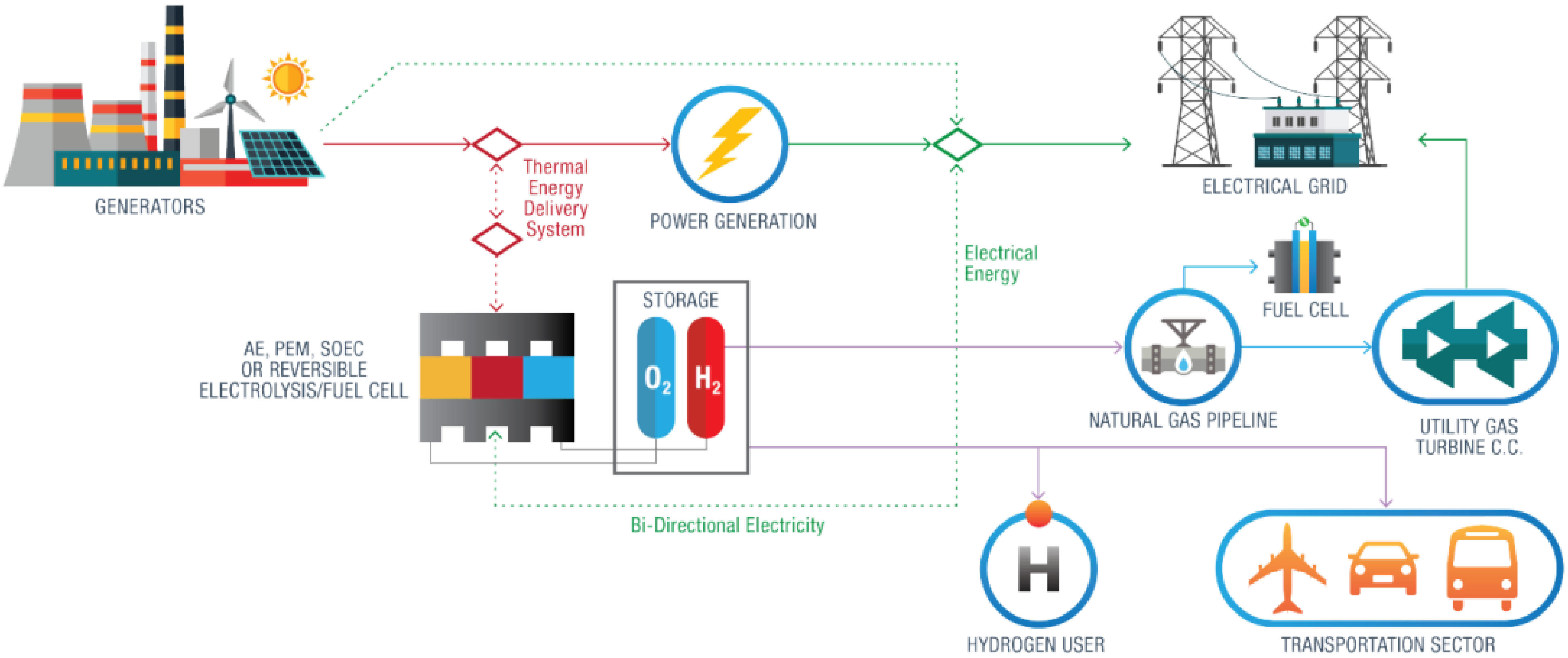
python™

Gurobi	CPLEX	Xpress	CBC	Ipopt
GAMS	NEOS	Mosek	BARON	GLPK

Integrated Energy System for Low Carbon Power and H_2



The IDAES platform is being applied to explore whether tightly coupled integrated energy systems that have the flexibility to produce both power and hydrogen should play a role in DOE's goals of decarbonizing the power sector by 2035 and broader economy by 2050.

IDAES Projects Span Multiple Time-Scales

- Technoeconomic and market analysis of SOEC/SOFC-based hydrogen and electricity co-production systems (hours → year)

- Dynamics, control, health modeling, and optimization of SOEC/SOFC-based systems (seconds (dynamic operation) → years (health))

- Integrating short-term operational realities (e.g., unit commitment and dispatch) into long-term expansion planning models (minutes → decades)

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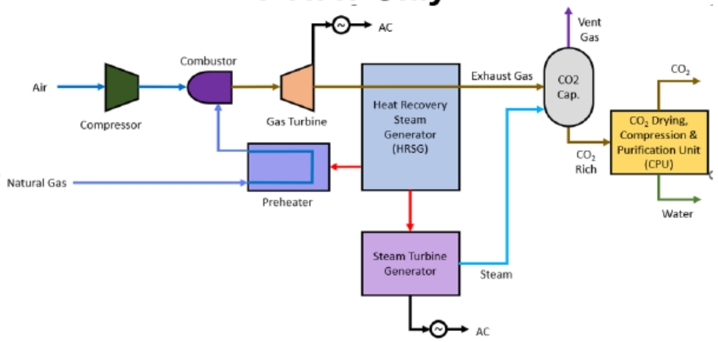
Analysis of Integrated Energy System Concepts

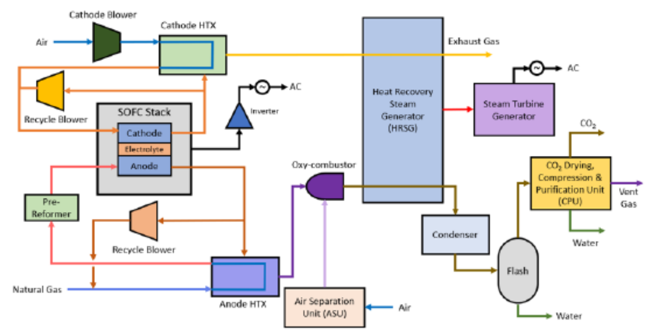
Fuel = Natural Gas
CO_2 capture > 97%

Baseline Systems Single Product

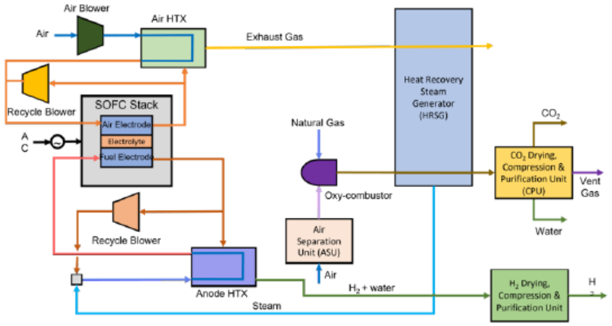
Standalone Natural Gas Combined Cycle (NGCC)
Power Only



Standalone Solid Oxide Fuel Cell (SOFC)
Power Only

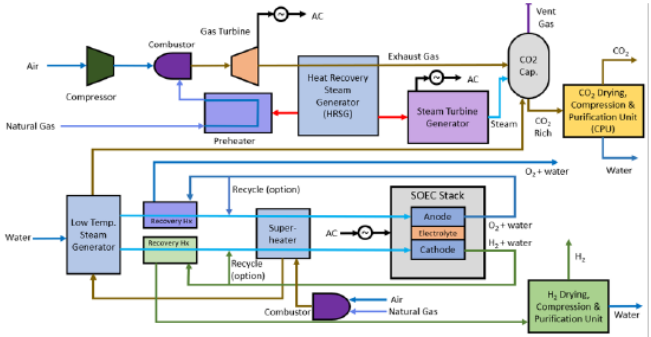


Standalone Solid Oxide Electrolyzer Cell (SOEC)
Hydrogen Only

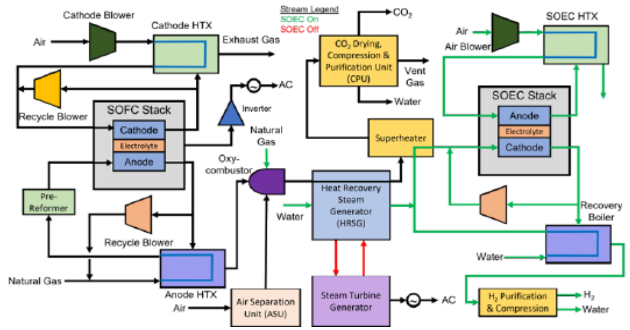


Integrated Systems Multi-Product

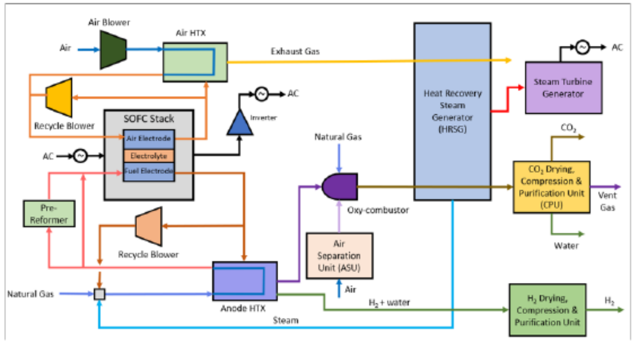
NGCC + SOEC
Power, Hydrogen, Coproduction



SOFC + SOEC
Power, Hydrogen, Coproduction



Reversible Solid Oxide Cell (rSOC)
Power, Hydrogen



Are there plausible electricity market scenarios where an integrated system makes sense? If so, which system is the best?

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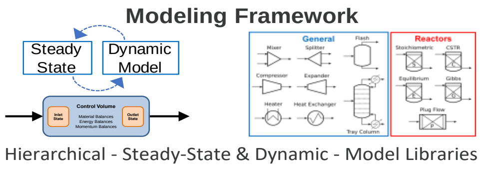
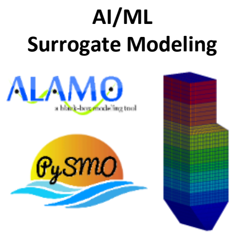
Process Concept Evaluation Strategy

Develop process and costing models using IDAES that are capable of optimization and off-design performance prediction



Calculate standard metrics like

- **\$/MWh**
- **\$/kg H_2**
- **kg $CO2_{eq}$/MWh**
- **kg $CO2_{eq}$ /kg H_2**



Develop surrogate models for each process concept that relate variable costs with power and H_2 output (and fixed costs with power and H_2 capacities)

Use surrogate models in **multi-period process/market optimization model** to calculate optimal **capacity factors** and **net profit** under several scenarios.

Design and Costing Basis*

- Greenfield Plants, Midwestern US, 2018 $'s
- Hydrogen: 6.479 MPa, < 10 ppm H_2O
- All systems designed to capture > 97% CO_2
- 100% capacity factor**

Process Concepts	Power Capacity ($MW_{e,net}$)	Hydrogen Capacity (kg/s)
NGCC	650	-
SOFC	650	-
NGCC + SOEC	650	5
rSOC	650	5
SOFC + SOEC	710	5
SOEC	-	5

- SOFC: $225/kW stack cost+
- SOEC: $105/kW stack cost
- Stack degradation rate: 0.2% / 1000 hr (~7 yrs stack life)+

* Theis, Quality Guidelines for Energy System Studies – Cost Estimation Methodology for NETL Assessments of Power Plant Performance, February 2021, (NETL-PUB-22580)

** Major assumption that process-market optimization allows us to relax.

\+ Iyengar, Noring, Mackay, Keairns, and Hackett. Techno-economic Analysis of Natural Gas Fuel Cell Plant Configurations (DOE/NETL-2022/3259).

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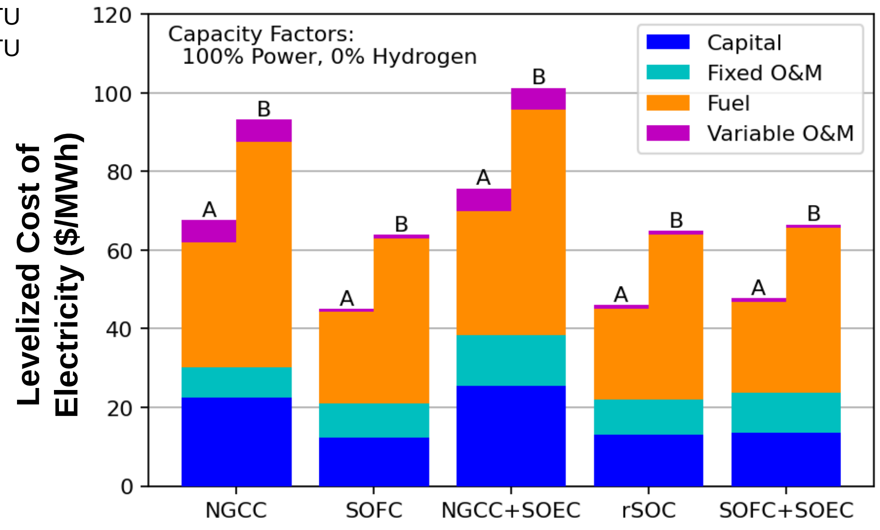
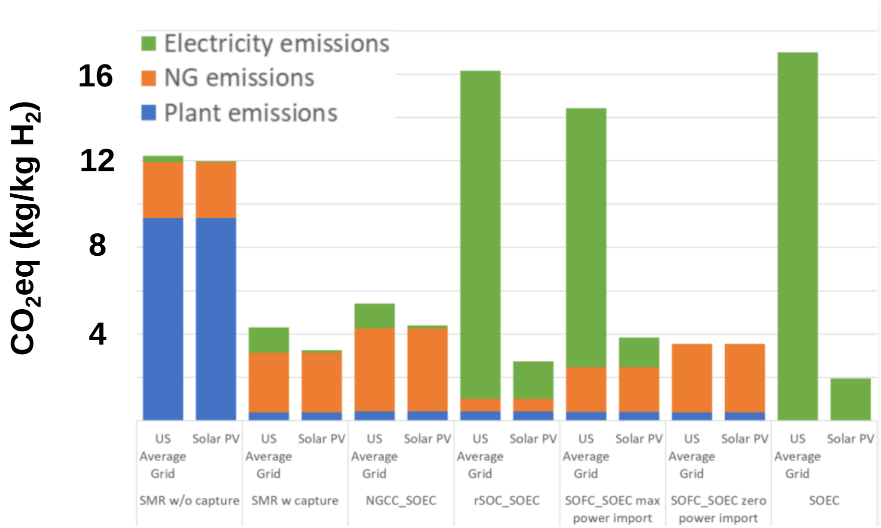
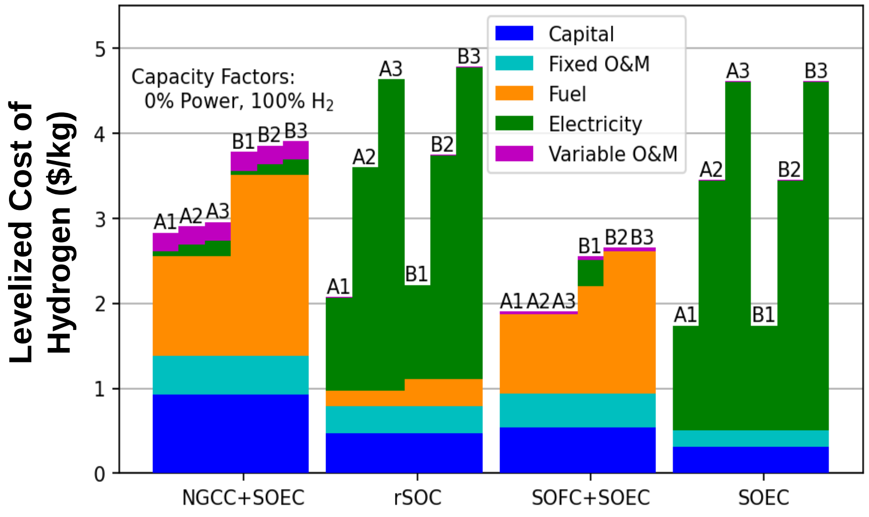
Conventional Process-Centric Analysis was Rigorous but Limited

A = $4.42 / mmBTU
B = $8.00 / mmBTU
1 = $30 / MWh
2 = $71.7 / MWh
3 = $100 / MWh







- Lowest cost system highly dependent on many factors (NG, H_2, electricity prices, CO_2 incentives or taxes)
- A different analysis approach is required to more fully understand the value proposition of such systems.

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Eslick, Noring, Susarla, Okoli, Allan, Wang, Ma, Zamarripa, Iyengar, Burgard, Technoeconomic Evaluation of Solid Oxide Fuel Cell Hydrogen-Electricity Co-generation Concepts (**DOE/NETL-2023/4322**).

Optimization Formulation, Price-Taker Assumption

Input: Electricity prices for a given market

Input: H_2 Selling Price

Output: Power and H_2 generated at every time step

For now, just assume that capacities, P_{max} and H_{max}, are fixed

$$\max \sum \underbrace{\pi_{p,t} p_t}_{revenue\ from\ power} + \underbrace{\pi_h h_t}_{revenue\ from\ hydrogen} - \underbrace{\left(C_{var}(p_t, h_t) + C_{capital+fixedO\&M}(P_{max}, H_{max})\right)}_{sum\ of\ costs}$$

s.t.

$$p_t \leq P_{max}\ \forall t \in T$$

$$h_t \leq H_{max}\ \forall t \in T$$

Extensions not shown:

- Carbon taxes
- Ramping constraints
- Start up shutdown costs

Disjunctions at every time step to choose optimal operating mode:

$$\begin{bmatrix} C_{var}(p_t, h_t) = 0 \\ p_t = 0 \\ h_t = 0 \end{bmatrix} \veebar \begin{bmatrix} C_{var}(p_t, h_t) = f_1(p_t) \\ p_t \geq P_{min} \\ h_t = 0 \\ p_t^h = 0 \end{bmatrix} \veebar \begin{bmatrix} C_{var}(p_t, h_t) = f_2(h_t) \\ h_t \geq H_{min} \\ p_t^h = f_4(h_t) \end{bmatrix} \veebar \begin{bmatrix} C_{var}(p_t, h_t) = f_3(p_t, h_t) \\ p_t^h = f_5(h_t) \\ p_t \geq P_{min} \\ h_t \geq H_{min} \end{bmatrix}$$

Plant is off | Power only | Hydrogen only | Both Power and Hydrogen

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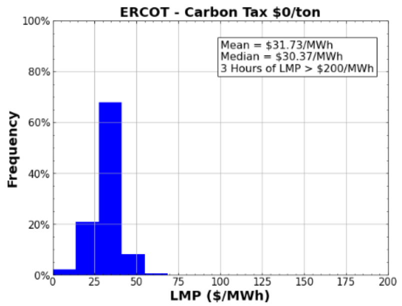
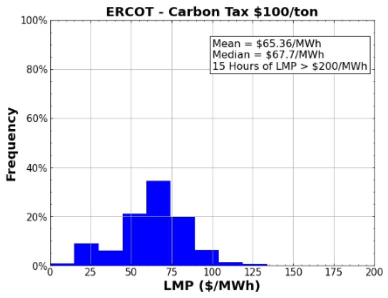
Many Electricity Market Scenarios Considered

- **61 total data sets** (every hour for a year)
- 2019 & 2022 data from ERCOT, ISO_NE, MISO, PJM, SPP, NYISO
- Future projections from NREL and Princeton from ARPA-E FLECCS program
- Future projections from NETL for ERCOT using PROMOD IV

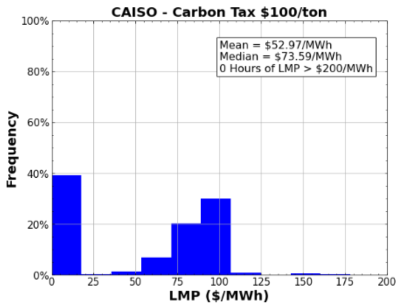
Data sets cover very broad range of potential scenarios



Low Prices

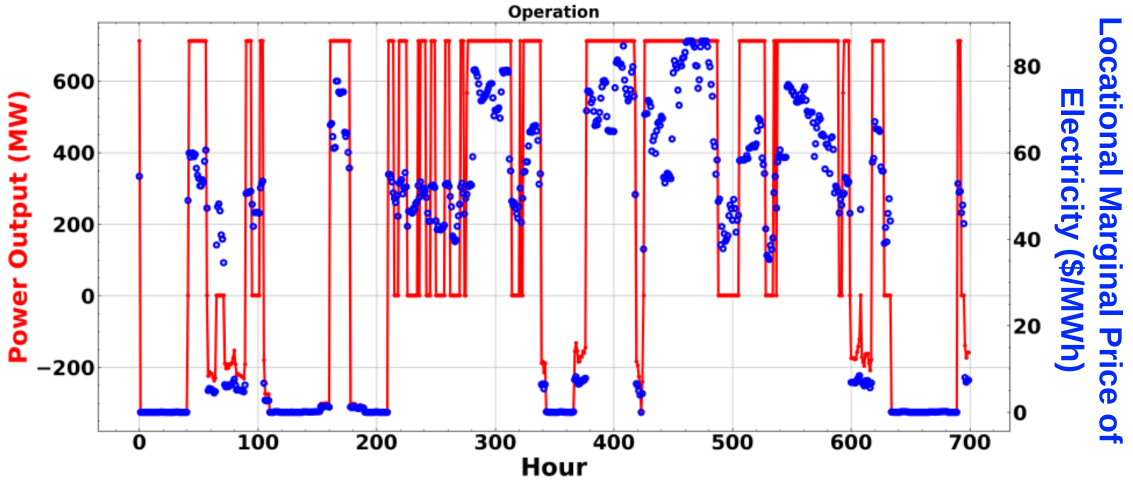


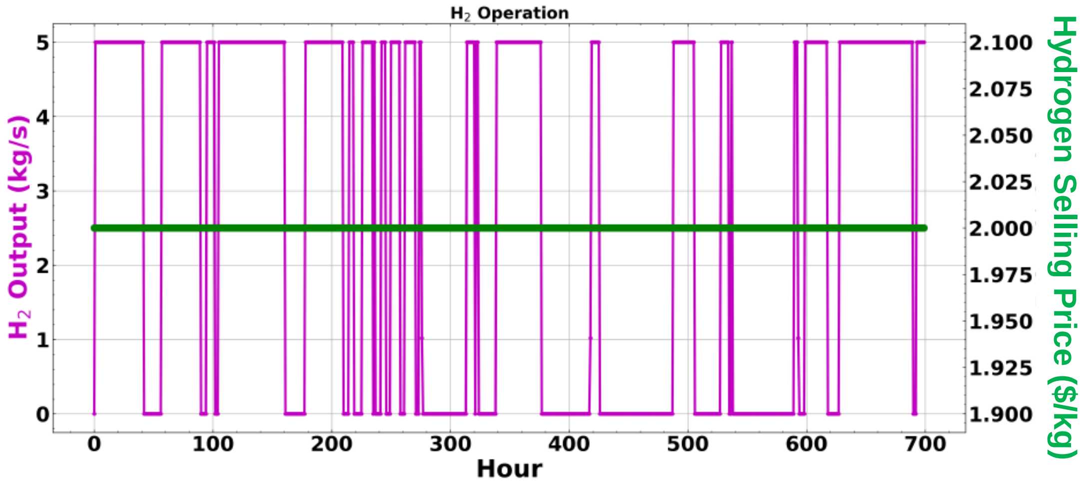
High Prices



Bimodal (e.g., high VRE)

System: SOFC + SOEC
Scenario: MiNg_$100_MISO-W_2035 (only first 700 hours of year shown)





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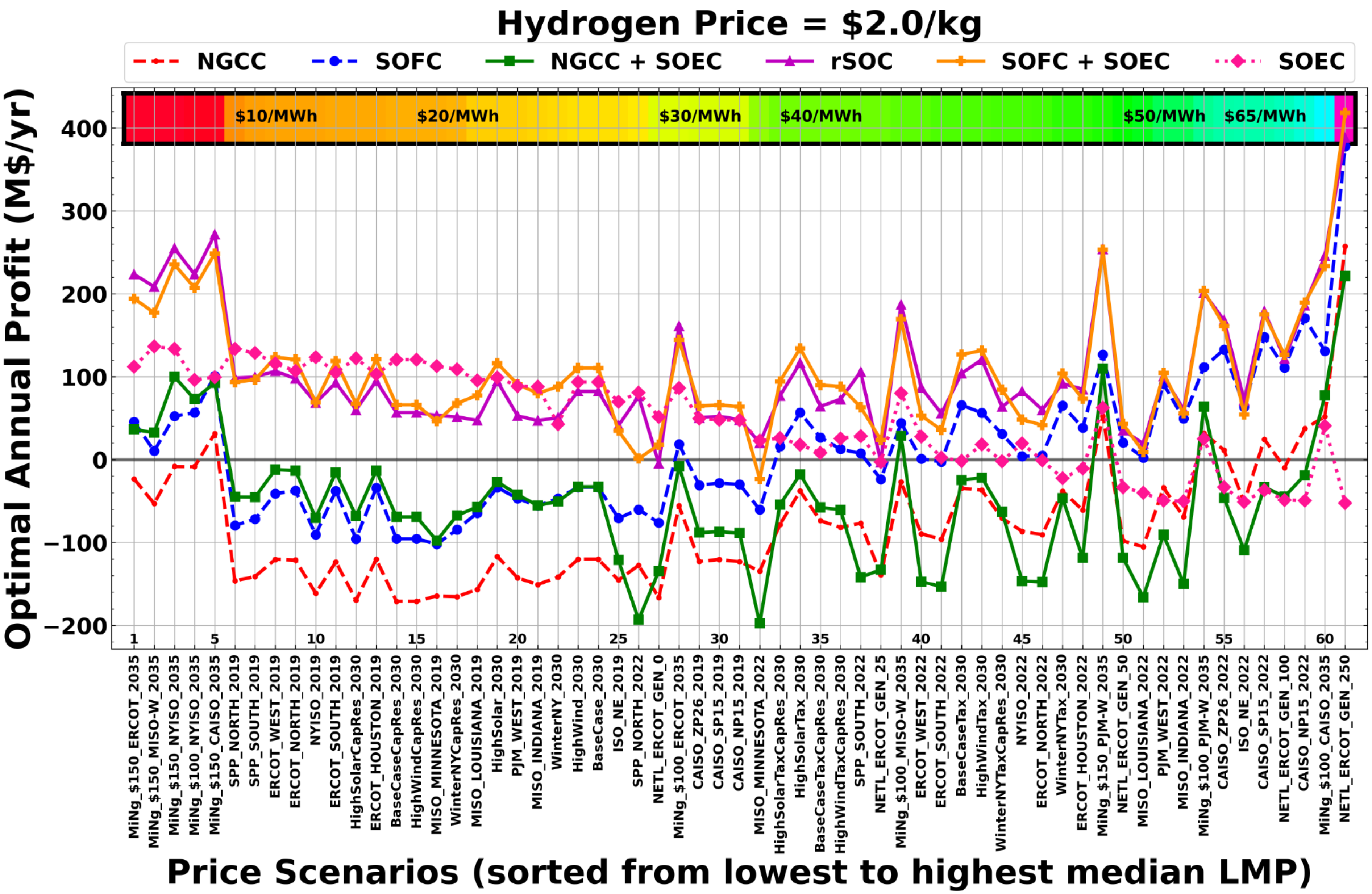
Compiled Results from Integrated Process/Market Optimization



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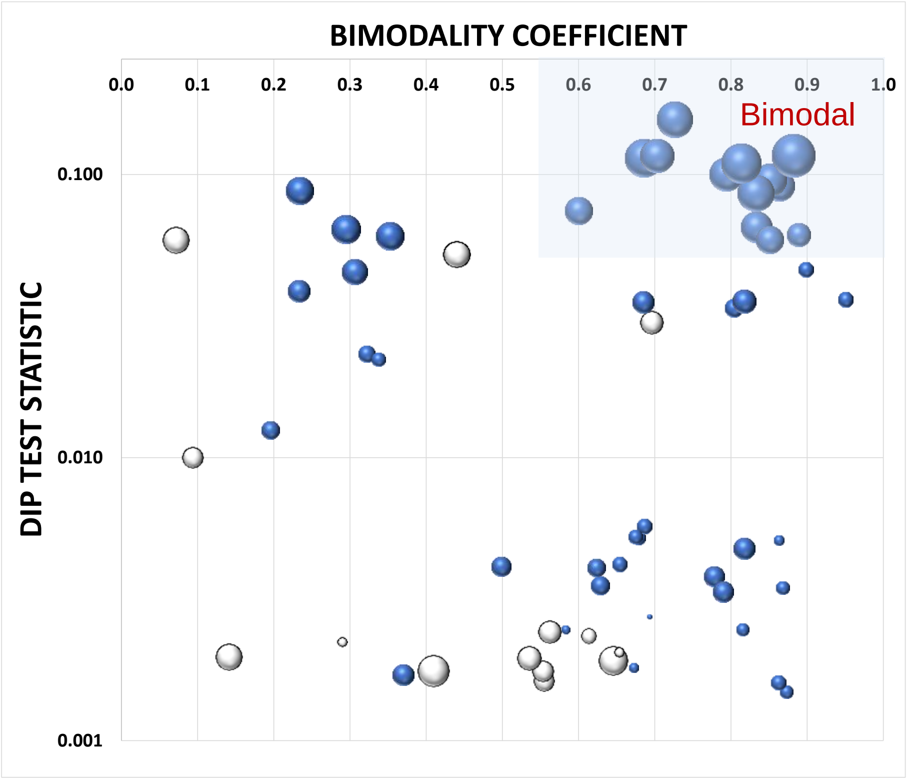
Key Conclusions

% of electricity market **scenarios with positive annualized profit** assuming \$2/kg H_2 selling price

NGCC (power only)	13%
SOFC (power only)	52%
SOEC (H2 only)	74%
NGCC + SOEC (power and/or H2)	16%
Reversible SOC (power or H2)	97%
SOFC + SOEC (power and/or H2)	98%

Integrated power and hydrogen systems are the most robust to electricity market assumptions.

Bubble Size = Value of Integration:
Annual Profit from SOEC+SOFC –
Max (Annual Profit from SOEC, Annual Profit from SOFC)



Integrated power and hydrogen systems provide greatest benefits in scenarios with bimodal electricity pricing (e.g., high VRE).

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Take Home Messages

- The IDAES platform enabled rigorous comparisons of processes across diverse market scenarios leading to insights unattainable by conventional TEA.

- Integrated SOFC/SOEC systems with flexibility to produce both hydrogen and electricity are far more robust to market assumptions than single-product systems, especially when electricity pricing is bimodal.

- Can these systems switch between operating modes frequently and rapidly enough to take advantage of their flexibility benefits, but safely enough to avoid significantly damaging the process equipment?

IDAES Projects Span Multiple Time-Scales

- Technoeconomic and market analysis of SOEC/SOFC-based hydrogen and electricity co-production systems (hours → years)

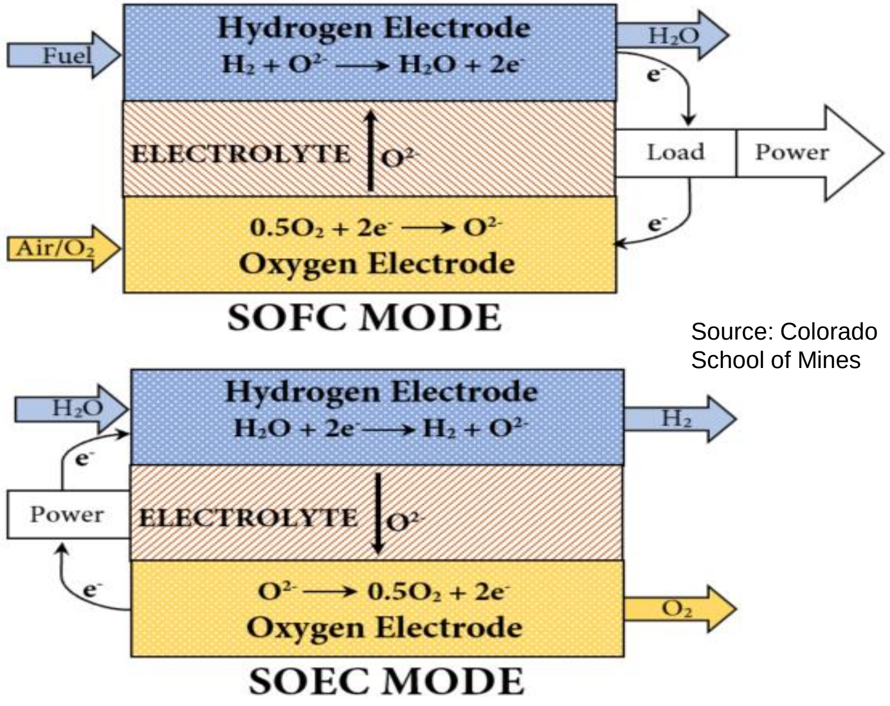
- Dynamic & health modeling, control, and optimization of SOEC/SOFC-based systems (seconds (dynamic operation) → years (health))

- Integrating short-term operational realities (e.g., unit commitment and dispatch) into long-term expansion planning models (minutes → decades)

Solid Oxide Cell (SOC)-based Integrated Energy Systems (IES)

Key Challenge

- How can we **best operate and control** SOC-based IES for **mode-switching (H_2/power)**, while **minimizing degradation** over long-term flexible operation?
  - SOCs operate at much **higher temperatures** than other fuel cell/ electrolysis technologies
  - While high-temperature operation offers **higher current density** and **efficiency**, it also poses significant challenges:
    - Additional **heat exchange** equipment
    - Accelerated **degradation**
    - **Tight controls** for optimizing performance and health during setpoint transitions and mode-switching operation



Source: Colorado School of Mines

Operating principles for H_2 fuel in SOFC mode and steam electrolysis in SOEC mode.

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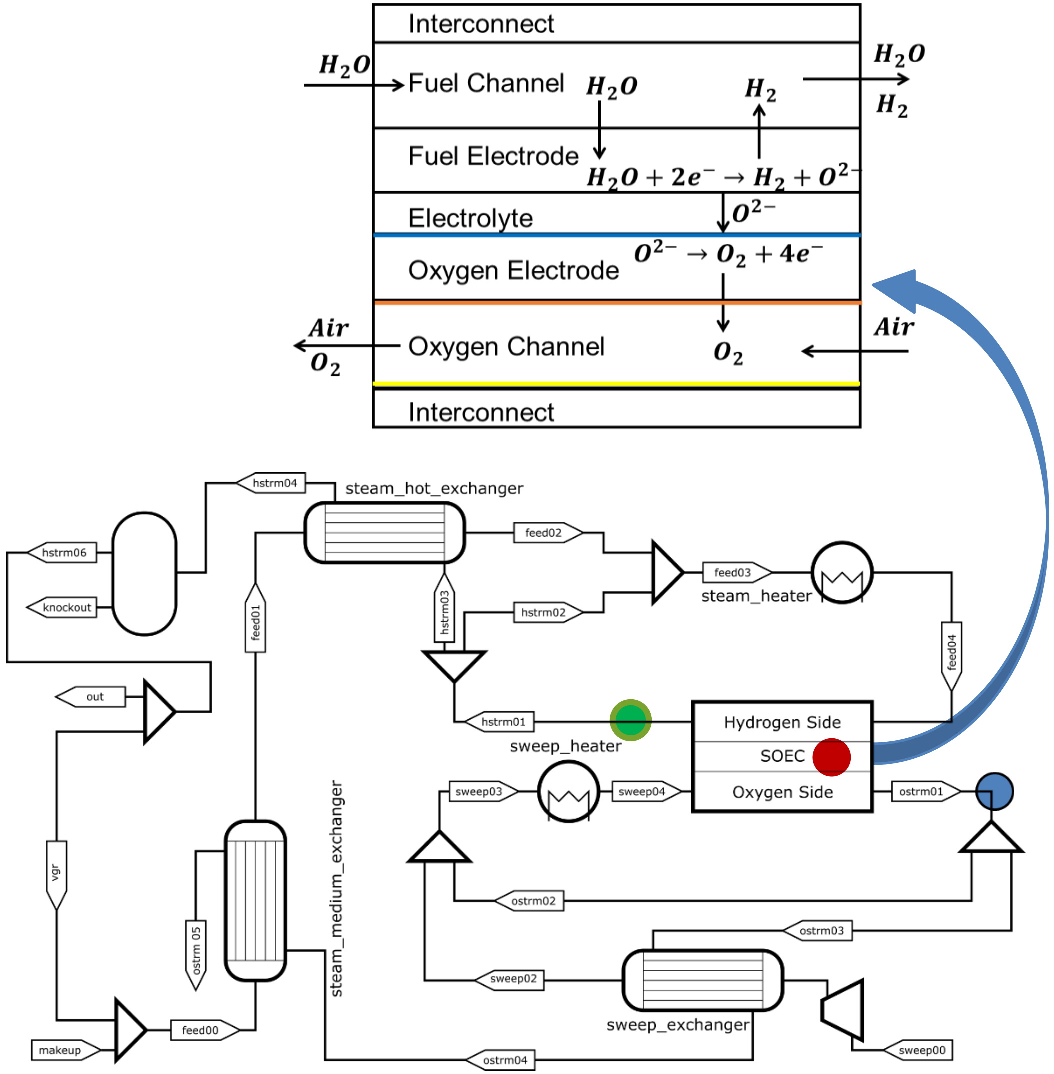
Optimization of SOC-based IES Flexible Operations
Dynamics, Control, and Health Modeling

Technical Approach

- **Dynamic Modeling**
  - Develop **first-principles dynamic model** of SOC-based IES using **IDAES** software
- **Process Control**
  - Develop **classical and advanced process controls** for effective thermal management and mode-switching operation
- **Health/Degradation Modeling**
  - Develop first-principles sub-models for **physical and chemical degradation**, as well as their **synergistic effects**, to quantify impact on cell health
- **Optimization**
  - Optimize **performance** and **health** of SOC-based IES for **long-term flexible operation**

Dynamic Model of H_2-fueled SOC-based IES for Mode-Switching

- **IDAES** open-source, equation-oriented modeling and optimization framework (Lee et al., 2021)
- **SOC dynamic model** (Bhattacharyya et al., 2007)
  - First-principles, non-isothermal, planar
  - 1D channel; 2D electrodes, electrolyte, and interconnect
  - H_2 fueled in power mode
- Equipment models for **thermal management**
  - 1D multipass crossflow recuperative heat exchangers
  - 1D crossflow trim heaters
- System **performance constraints**
  - Maximum H_2O outlet concentration to ensure good conversion (green marker)
  - Minimum O_2 in sweep outlet to prevent oxidation (blue marker)
  - Max cell thermal gradient to avoid degradation (red marker)

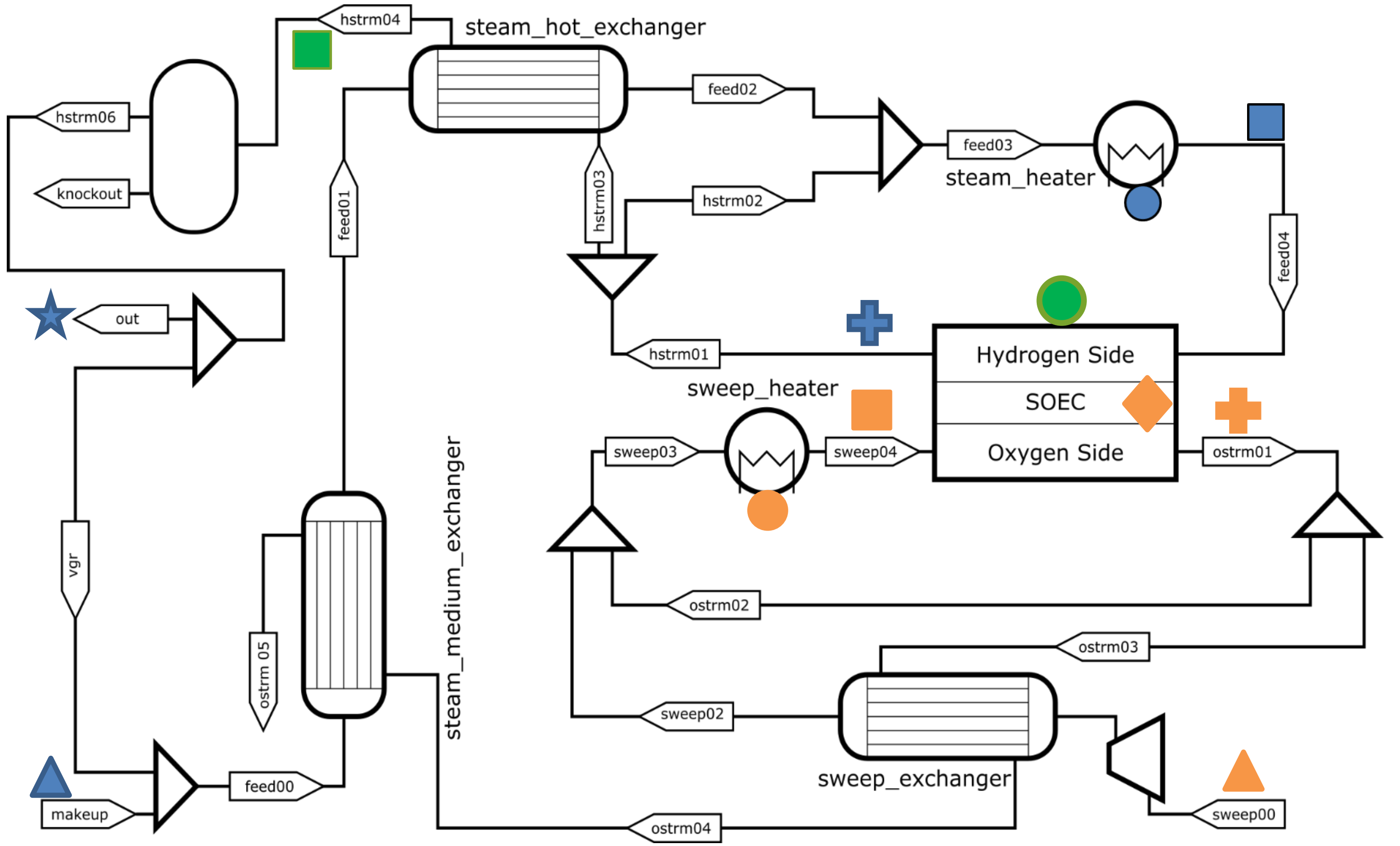


Block flow diagram of H_2–fueled SOC-based IES for Mode-Switching Operation

- Lee, A., et al.., J Adv Manuf Process 2021, 3(3) (2021).
- Bhattacharyya et al., Chem Eng Sci, 62, 4250-4267 (2007).
- Allan, D.A., et al., In Proc. FOCAPO/CPC (2023).

Process Control for SOC-based IES Mode-Switching Operation

- **Classical Control: Proportional-Integral-Derivative (PID)**
- **Nonlinear Model Predictive Control (NMPC)**



Controller	Manipulated Variables (MVs)	Controlled Variables (CVs)
PID, NMPC	Cell potential	Outlet Water Concentration
PID, NMPC	Steam/H_2 feed rate	H_2 production rate
PID, NMPC	Feed heater duty	Feed heater outlet temperature
PID, NMPC	Sweep heater duty	Sweep heater outlet temperature
PID, NMPC	Steam heater outlet temperature setpoint*	SOC steam outlet temperature
PID, NMPC	Sweep heater outlet temperature setpoint*	SOC sweep outlet temperature
PID, NMPC	Sweep feed rate	SOC temperature
NMPC	Feed recycle ratio	
NMPC	Sweep recycle ratio	
NMPC	Vent gas recirculation (VGR) recycle ratio	
NMPC	H_2/H_2O ratio in make-up	

**artificial control variables*

- Allan, D.A., et al., In Proc. FOCAPO/CPC (2023).
- Dabadghao, V., Ph.D. Thesis, CMU (2023).

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NMPC for SOC-based IES Mode-Switching Operation

- NMPC is well suited to **highly interactive manipulated variables** and **constraint handling**
- NMPC **objective function**

$$f_{\text{obj}} = \sum_{i=0}^{N} \rho_{\mathrm{H}_2} \left(y_i - y_i^R\right)^2 + \sum_{i=0}^{N} \sum_{j \in J} \rho_j \left(u_{ij} - u_{ij}^R\right)^2 + \sum_{i=0}^{N} \sum_{k \in K} \rho'_k \left(x_{ik} - x_{ik}^R\right)^2 + \sum_{i=1}^{N} \rho' \left(\nu_i - \nu_{i-1}\right)^2 + \rho_s \sum_{i=0}^{N} \sum_{z=1}^{z_L} \left(p_{iz} + n_{iz}\right)$$

Trajectory tracking of H_2/power production rate

Deviations of manipulated variables (u_{ij}) and controlled variables (x_{ik}) from reference values

Rate of change penalties on trim heater duties

ℓ_1-penalties for temperature gradient constraints

- To prevent thermal degradation over time, the temperature gradient along the cell length (z-direction) is constrained to be below dT/dz_{ub} K/m
- An ℓ_1-penalty relaxation treats them as soft constraints with non-negative slack variables p and n penalized in the objective

$$dT/dz - dT/dz_{ub} \le p \quad \text{and} \quad -dT/dz - dT/dz_{ub} \le n$$

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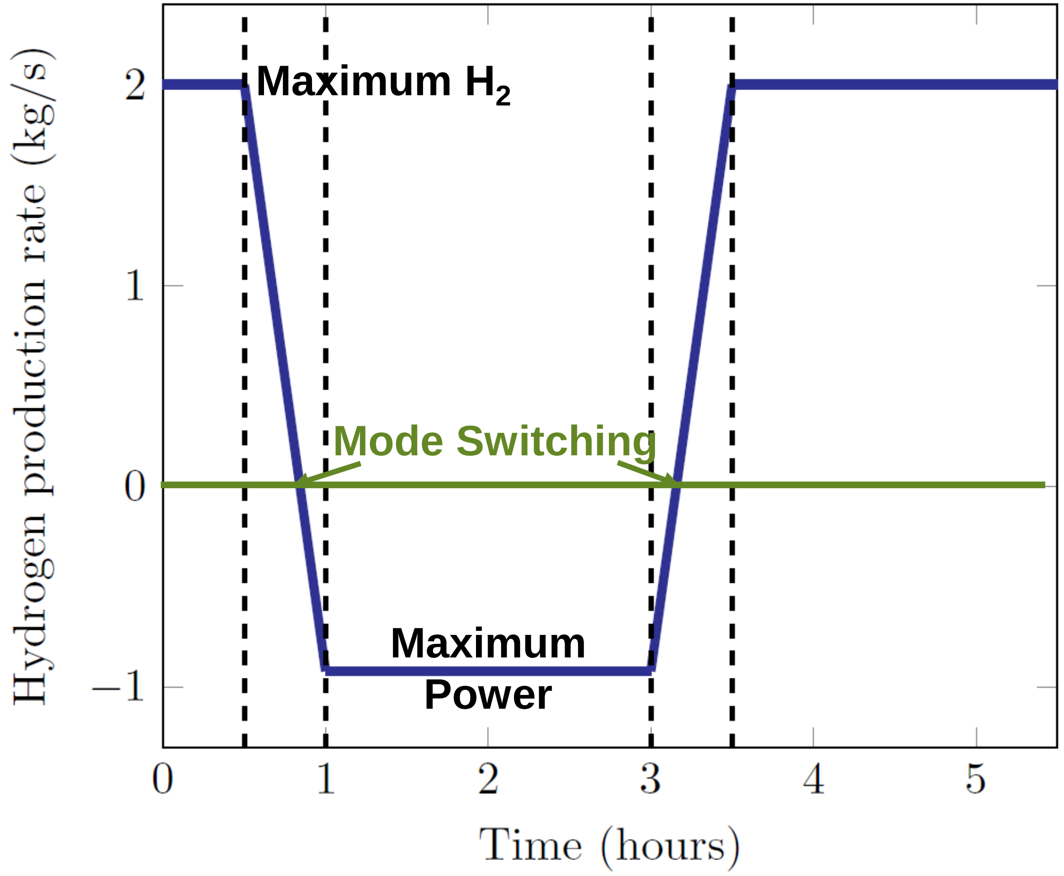
SOC-based IES Mode-Switching Operation

- **Mode-Switching**
  - Maximum H_2 (2.0 kg/s) to maximum power (-0.92 kg/s) and back to maximum H_2
  - Ramps performed over 30 min, followed by 2 hours of settling time
- **IDAES Solution Approaches**
  - Classical control: PETSc variable-step implicit Euler dynamic integrator
  - NMPC: **Full-discretization** NLP with IPOPT optimizer



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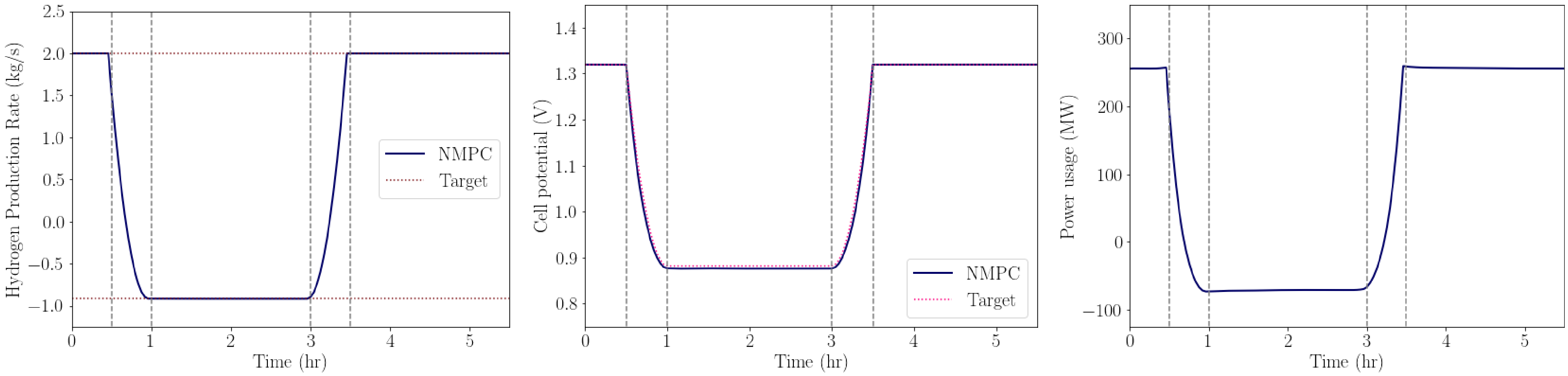
NMPC Results for SOC-based IES Mode-Switching Operation



Hydrogen production tracking has no overshoot, and is correlated to **cell voltage** and **total power usage**

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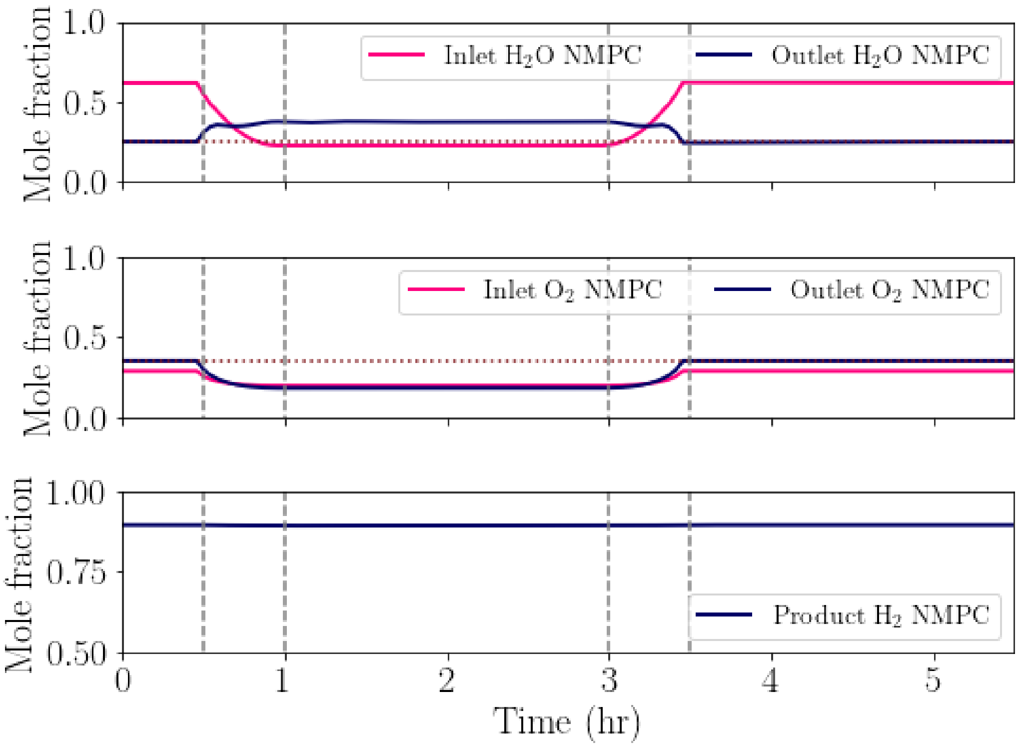
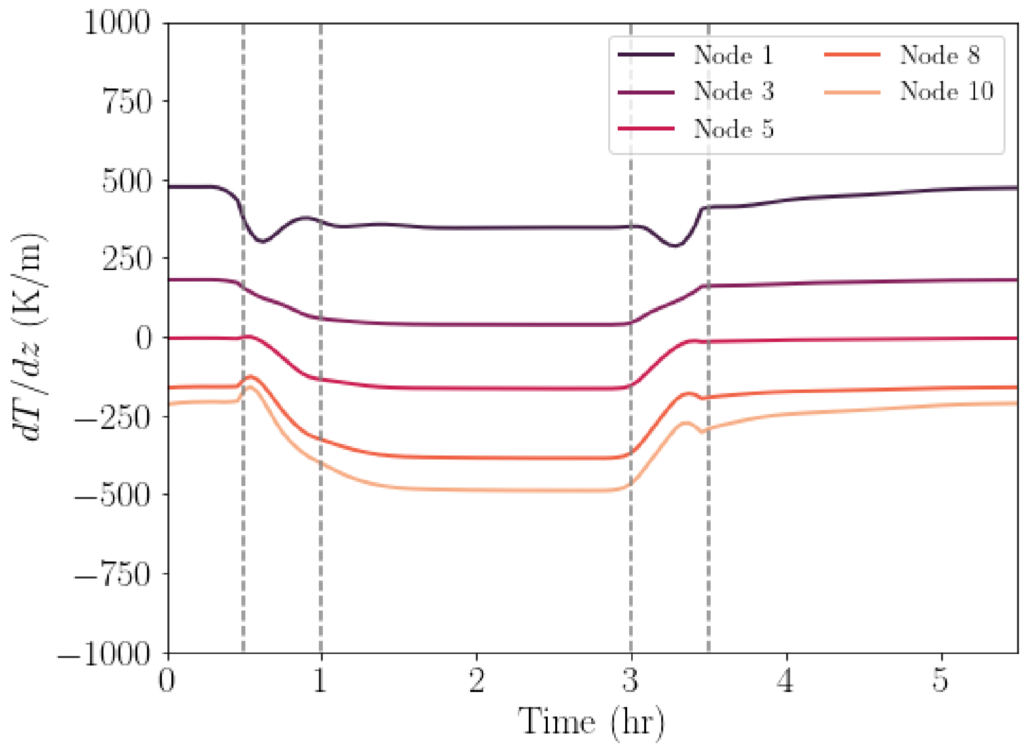
NMPC Results for SOC-based IES Mode-Switching Operation

- **Performance constraints are satisfied**
  - Maximum H_2O in outlet to ensure good conversion in SOEC mode
  - O_2 in sweep outlet ≤ 35% (mole basis) to prevent oxidation
  - Conversion of steam to H_2 ≥ 75% to avoid steam starvation
  - Maximum cell thermal gradient ≤ 1000 K/m to avoid stress





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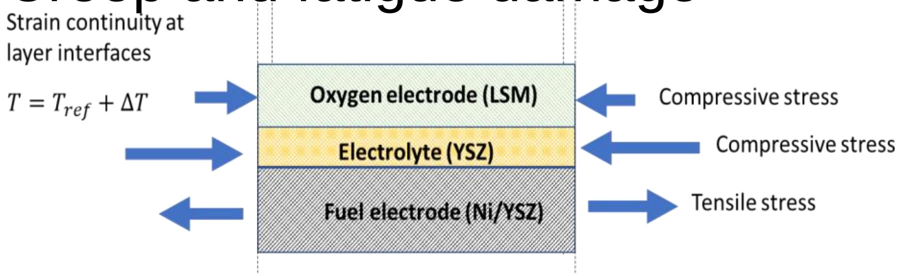
SOC Health/Degradation Modeling

- **Physical Degradation**
  - High spatial and temporal temperature gradients
  - Thermo-mechanical stresses
  - Creep and fatigue damage

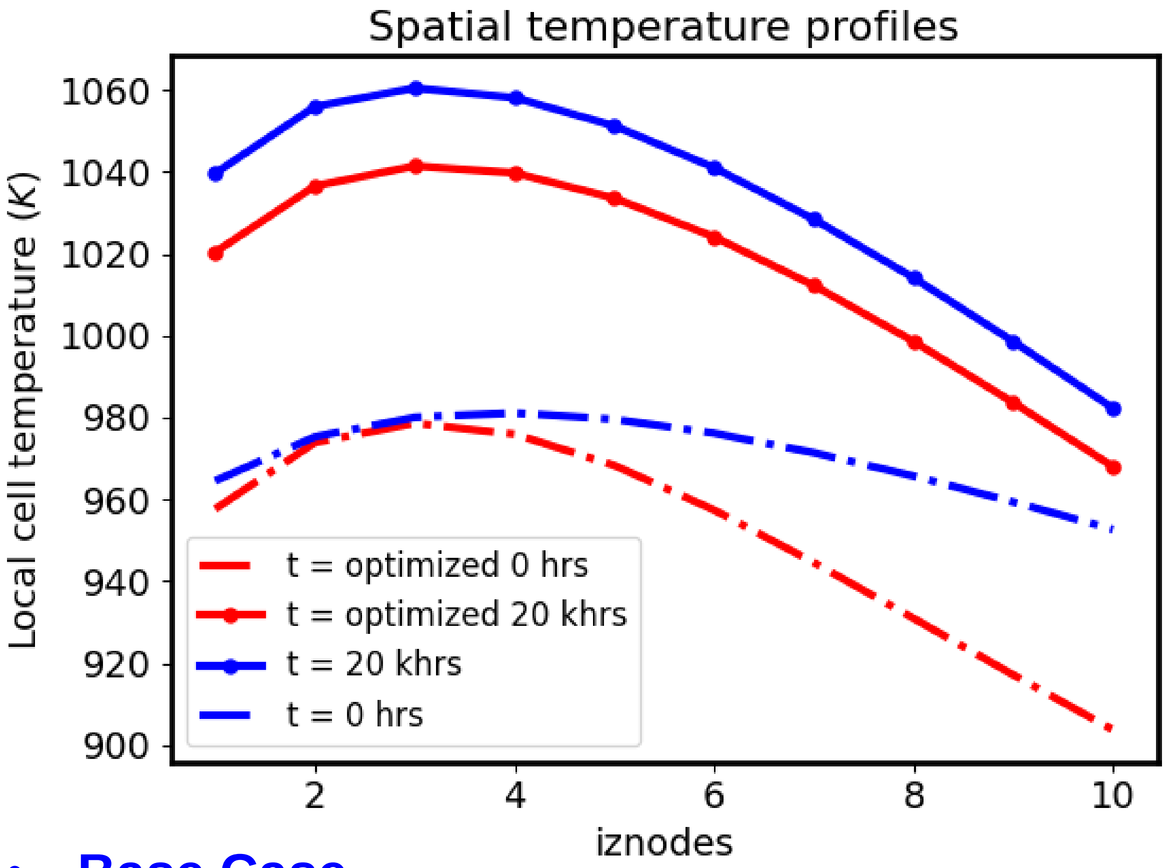


- **Chemical Degradation (H_2 fuel)**
  - Oxygen electrode
    - Chromium oxide scale growth
      - Increased local **ohmic resistances**
    - Lanthanum zirconate scale growth
    - LSM-YSZ coarsening
  - Fuel electrode
    - Ni agglomeration and volatilization
  - Electrolyte
    - YSZ electrolyte delamination

- **Synergistic Effects**
  - Chemical degradation negatively impacts physical degradation by:
    - increasing local **Ohmic resistance** and cell temperature
    - affecting **thermo-physical properties** of the ceramic materials, which result in variation in the cell thermal profile
    - affecting **mechanical properties** of cell components such as Young's modulus and Poisson's ratio

Case Study: SOEC Health Optimization over Long-Term Operation

- **20,000 hrs** of operation
- **Electrolysis mode**
  - High H_2 production rate: 1.5 kg/s
- Chemical degradation (O_2 electrode)
- **Health Optimization Case**
  - Minimize final ohmic resistance
    $$\min R_{ohmic,tf}$$
  - Decision variables at every time point
    - Fuel and oxygen trim heater duties
    - Fuel and oxygen inlet flowrate
    - Fuel and oxygen recycle ratio
  - Quasi-steady optimization
    - Dynamic degradation model
    - Steady-state SOEC system model



- **Base Case**
  - No optimization for health/degradation
  - Constant inlet temperatures over operating horizon from steady-state optimization at t=0 hrs to maximize efficiency

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Case Study: SOEC Health Optimization over Long-Term Operation

High H_2 production rate : 1.5 kg/s					
Objective Function	$\left.\frac{dT}{dz}\right\|_{max}$ (K/m)	T_{core} (K)	$\eta_{average}$	R_{ohmic} (mΩ/ khr)	$P_{specific}$ (MWh/kg H_2)
Base Case	1020	1033	**0.872**	0.34	**38.05**
Degradation Optimization Case: Minimize final resistance	**980**	**1020**	**0.875**	**0.26**	**38.15**

- About **25% reduction in resistance** growth rates (R_{ohmic})
- System **efficiency** ($\eta_{average}$) and **power requirement** ($P_{specific}$) remain **unchanged**
  - **Resistive heating in trim heaters instead of inside the cell**
- Minimizing resistance can keep absolute cell temperatures (T_{core}) in control
- Thermal gradients constraints ($\left.\frac{dT}{dz}\right|_{max}$ < 1000 K/m) **remain feasible** after 20,000 hrs of optimized performance

Please stop by poster for more details/results on SOC health modeling and optimization.

Summary

- **IDAES** offers an open-source modeling framework for **optimization** of the operation, control, and health of **flexible SOC-based IES.**
- **NMPC** provides **accurate H_2/power production setpoint tracking** during mode-switching operation.
- Results for **SOEC health optimization** over **long-term operation** show that:
  - ohmic resistance growth and cell temperature are reduced,
  - H_2 production rate and efficiency are maintained, and
  - thermal gradients are kept under control.

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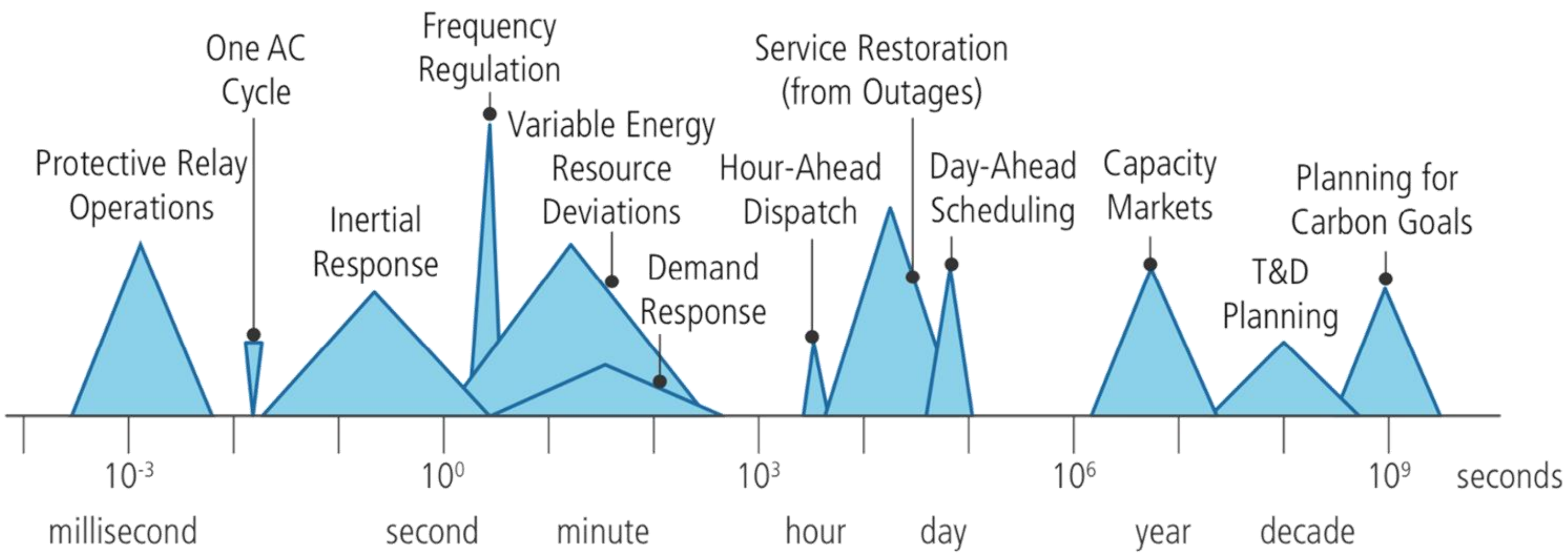
Future Work

- Enhance **NMPC** to maximize SOC system performance for **“faster” mode-switching** operation, while **reducing temperature gradients** to benefit cell health
- Analyze **synergistic effects** of **physical and chemical degradation** for mode-switching operation
- **Optimize SOC system performance** over **operational lifetime** using measure of **health** on **economics**
- Develop prototype of **multiple timescale computational approach** in IDAES for solving coupled dynamic simulations of long-term flexible operation and degradation

IDAES Projects Span Multiple Time-Scales

- Technoeconomic and market analysis of SOEC/SOFC-based hydrogen and electricity co-production systems (hours → years)
- Dynamic & health modeling, control, and optimization of SOEC/SOFC-based systems (seconds (dynamic operation) → years (health))
- Integrating short-term operational realities (e.g., unit commitment and dispatch) into long-term expansion planning models (minutes → decades)

Expansion Planning Modeling: Will Technology be Deployed?



Real-Time Operations	Electricity Grid	Capacity Expansion	Energy Economy Models
	Dispatch, Power Flow	20-30 Year Horizon	
High frequency dynamics	Complex effects of new generators	Difficult to value flexibility, reliability	Long time horizons Macro-economics

Process/Generator – Integrated Energy Systems

Design, Operation/Control, Dynamics, Multiple Products

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Expansion Planning Problems Are "Huge"

- At the core, an expansion planning model considers
  - Systems with $\mathbf{>10^2}$ generators, $\mathbf{>10^3}$ transmission lines,
  - Balancing loads over each of $\mathbf{10^6}$ **time periods**,
  - With numerous opportunities to install, extend, and retire assets,
  - And significant uncertainty in all parameters (generator costs, available technology, load growth and patterns, renewable resources),

- Too large to "directly solve"

- Numerous simplifications and approximations to develop "tractable" models
  - ACOFP → DCOPF → Transshipment
  - Full network → "skeletonized" network → "copper plate"
  - Individual generators → generator clusters
  - Full time horizon → representative days → representative loads
  - Discrete decisions → continuous relaxations

- Simplifications for tractability will impact accuracy

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Why is IDAES Developing Expansion Planning Models?

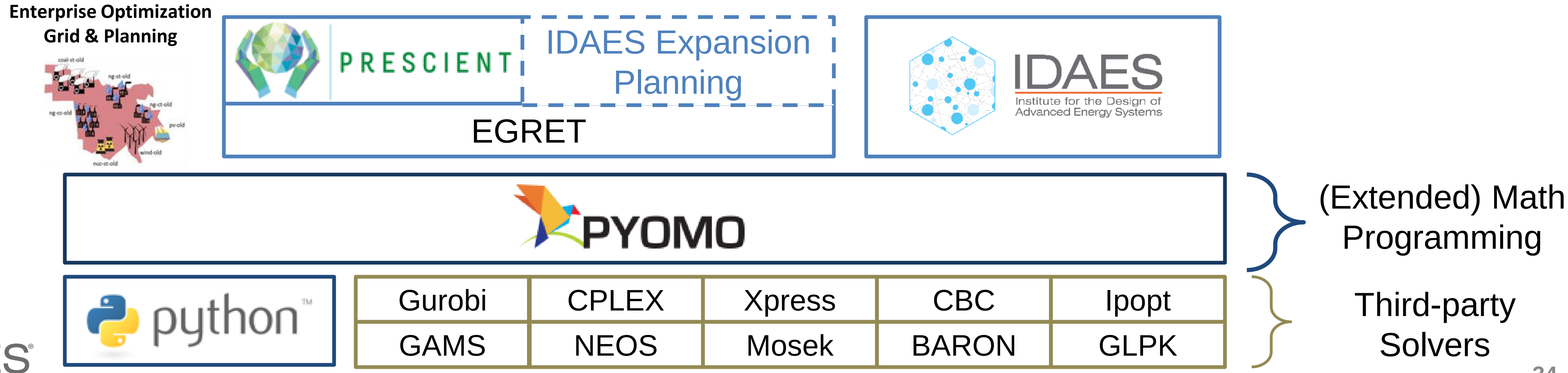
- Integrated Energy Systems must be designed for the *system*
  - Designing in isolation (e.g., “max efficiency”) does not guarantee participation / revenue from the market

- Existing expansion planning models focus primarily on *capacity*
  - Operability (e.g., the role of **dynamics, flexibility, and uncertainty**) is not explicitly included, leading to results that overvalue LCOE and undervalue dispatchability and flexibility

- Extending expansion planning models is more than just adding features
  - Scaling up the model requires exploring new algorithmic approaches to solving the model. **Model is open, allowing for customization for the problem you are interested in addressing**

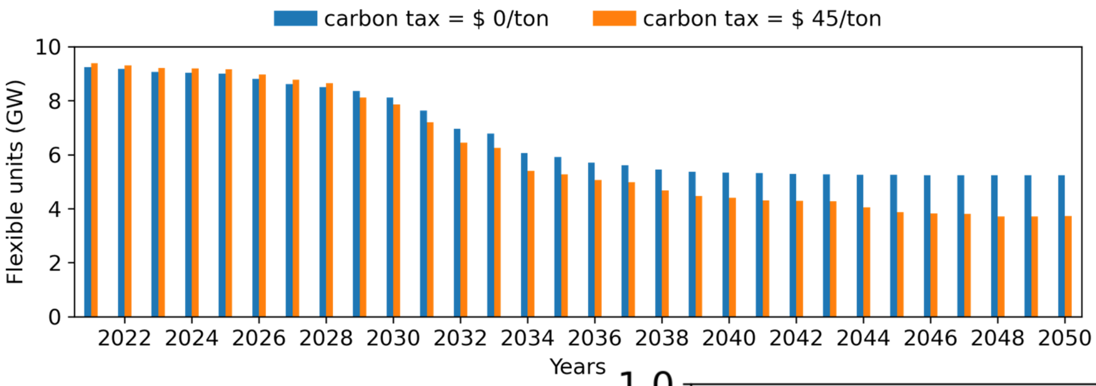
Current IDAES Expansion Planning Activities

- Develop reliability models and algorithms (Carnegie Mellon University, Seolhee Cho and Ignacio E. Grossmann)
  - Improve valuation of **flexibility**
  - Incorporate **resilience with reliability**
  - Expand to new case studies (partnering with California Energy Commission)
- Model maturation (Sandia National Laboratory)
  - **Generalizing / standardizing the models**, leveraging standardizing modeling components from **EGRET**
  - **Generalizing / standardizing algorithms** (remove explicit ties to case studies)

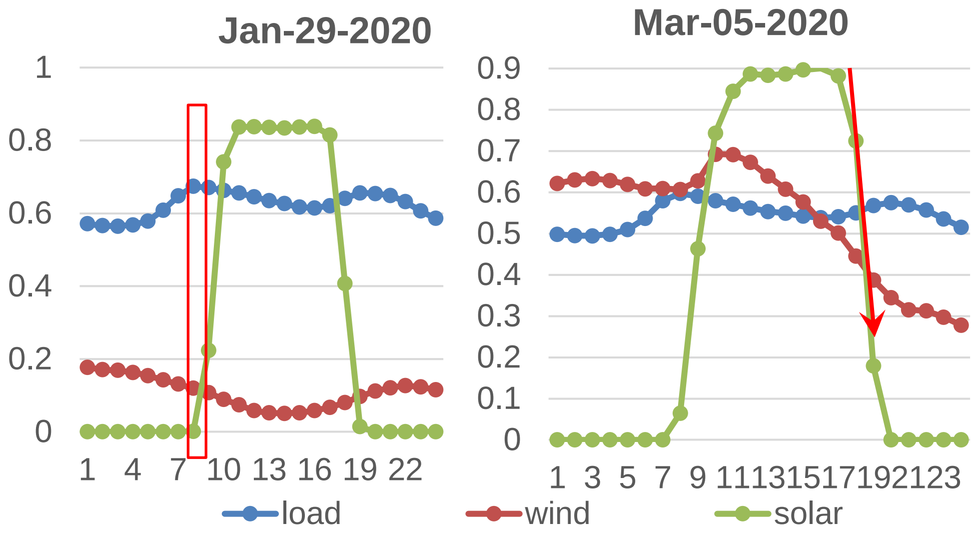


Quantifying the Impact of Flexibility

- Expansion planning with SPP case study **(hourly load balance with seasonal representational days)**
  - Results indicated significant reduction of installed flexible generation **with higher carbon tax**
    - Gas turbine, internal combustion turbine units
    - Lower efficiency, higher relative emissions
  - ***Counter-intuitive result***



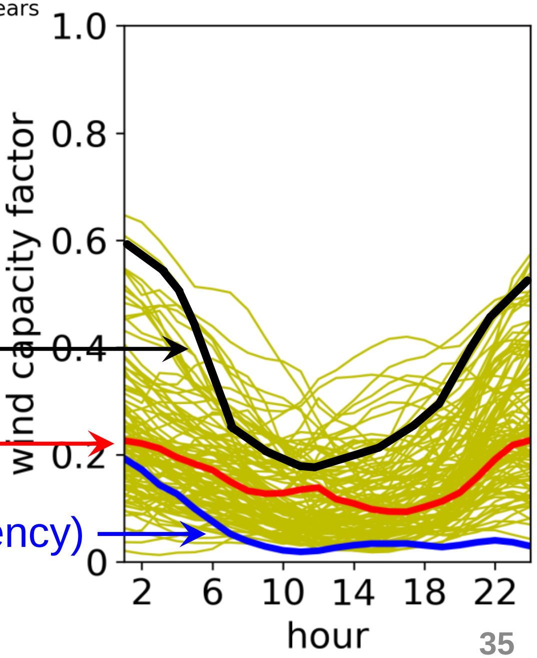
- Root cause: "representative" days did not capture
  - High ramp rates (volatility)
  - Low non-dispatchable generation (intermittency)



Scenario with high ramp rates (volatility)

Representative day

Scenario with low generation levels (intermittency)



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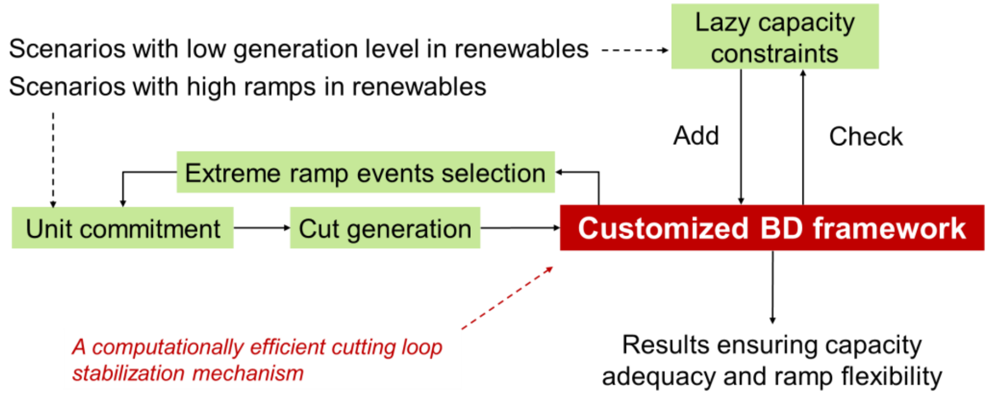
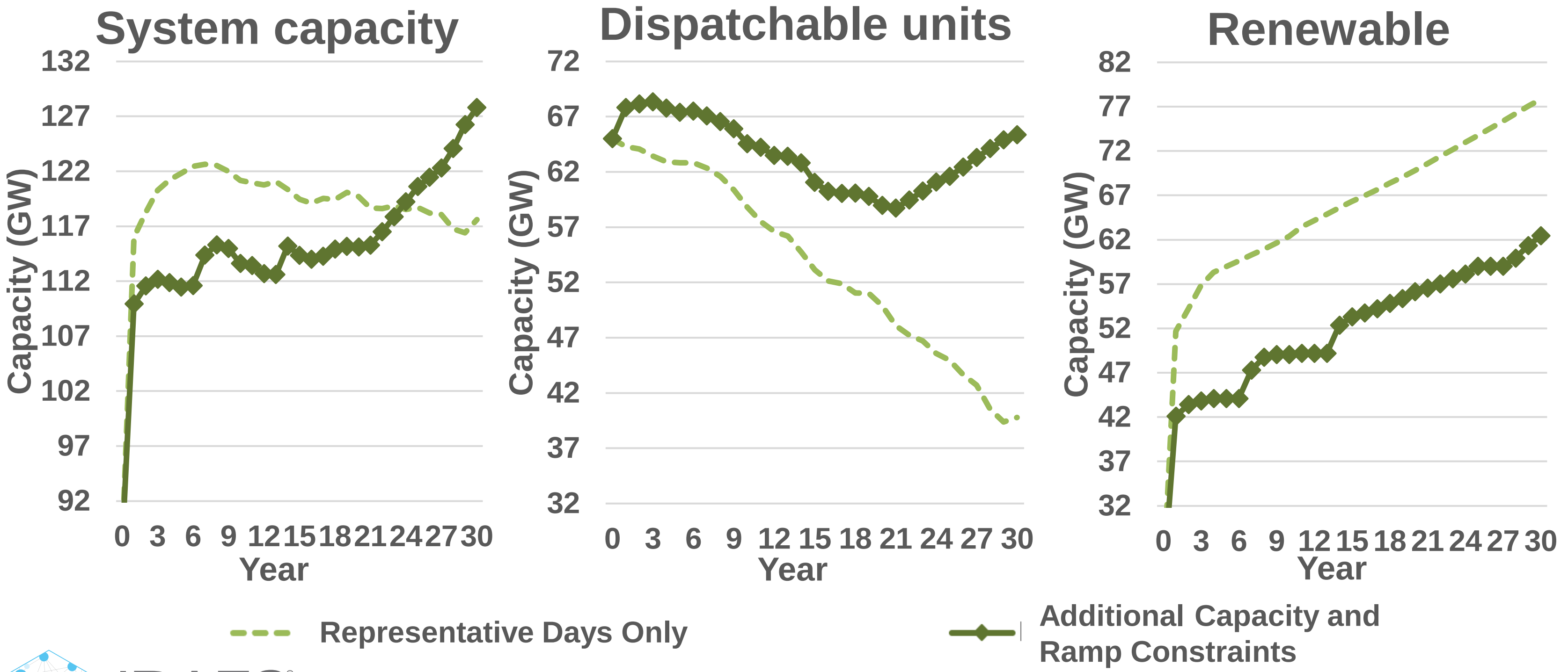
Accounting for Intermittency and Volatility

- “Non-representative” capacity and ramp scenarios critical in understanding dispatchable unit requirements
- Modified algorithm provides insights into low renewable capacity and/or rapid dispatchable ramp scenarios
  - Lazy capacity constraints
  - Extreme ramp events



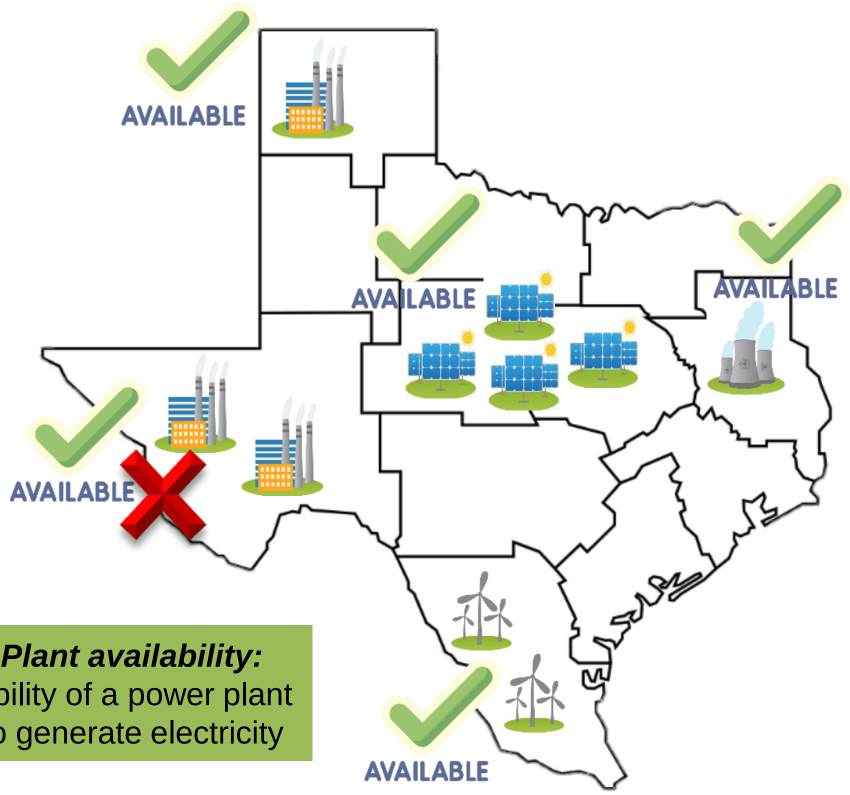


- “Representative Days Only” underestimates total required capacity
- More dispatchable capacity required with additional capacity constraints and ramp events

* SPP scenarios under high carbon tax

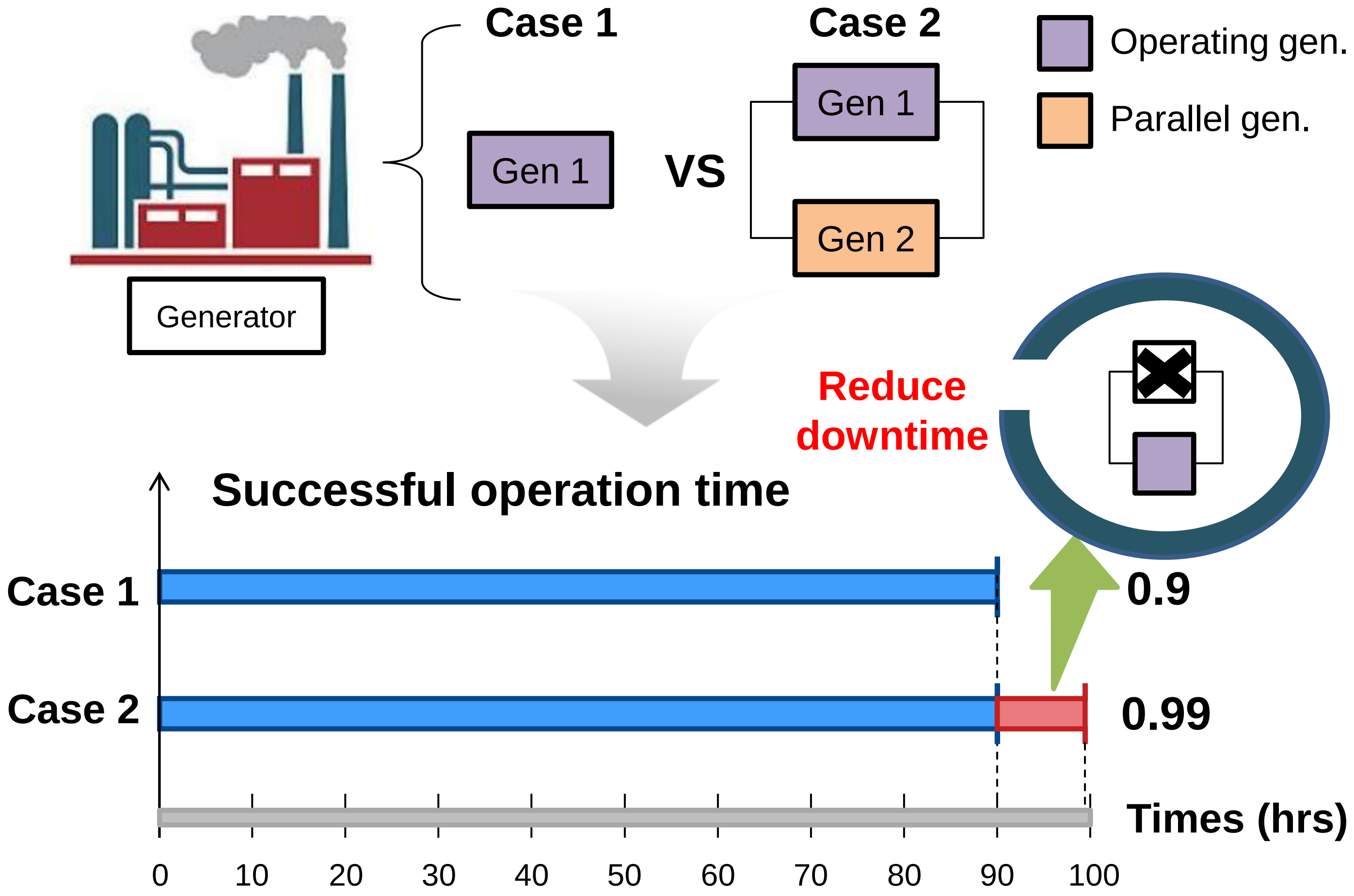
How to Improve Reliability - Redundancy

- Power systems reliability can be enhanced by improving availability of power plants.
- *Redundancy*   Adding units in parallel enables a power plant to be highly available.



Plant availability:
Ability of a power plant to generate electricity

Power **plant availability** ↑↓
→ Power **systems reliability** ↑↓



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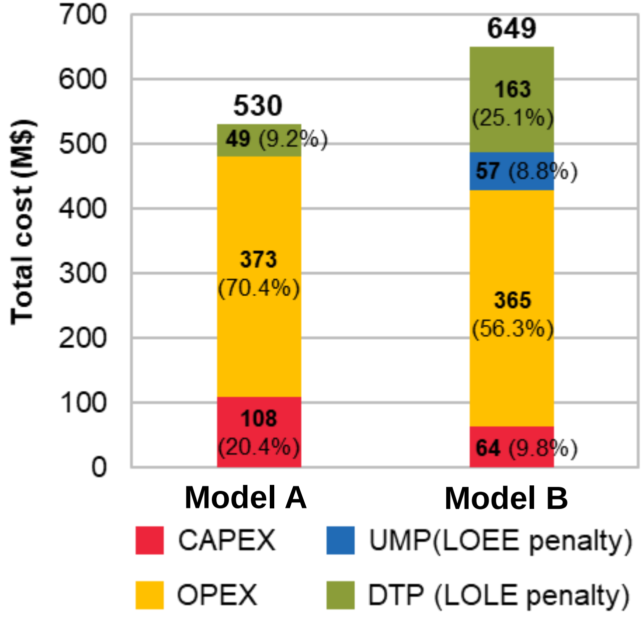
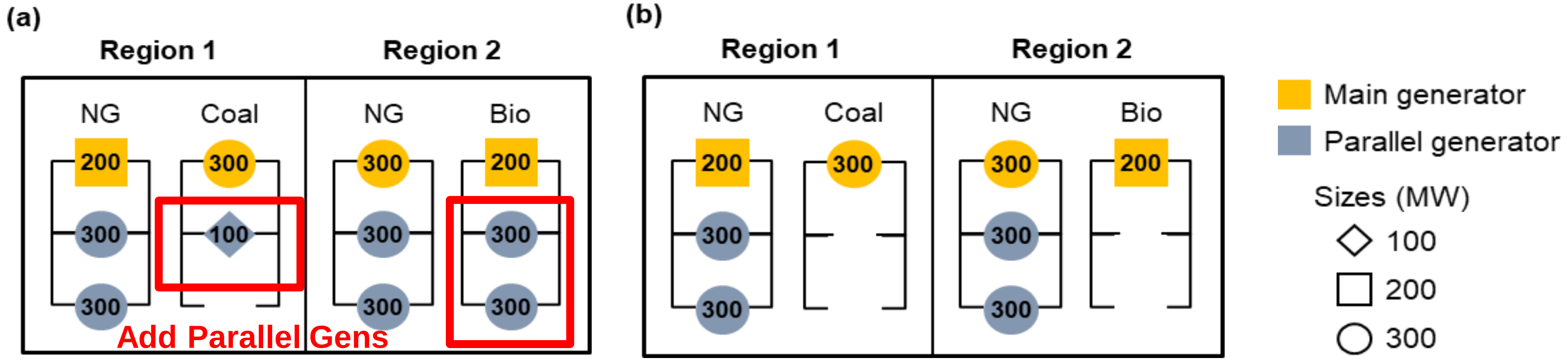
Including The Cost of Not Meeting Demand – Optimizing Considering Reliability

Illustrative example (2 regions, 3 types of power plants (Coal, natural gas (NG), and biomass (Bio))

Cost results

(a) Model A (w/ reliability), **(b)** Model B (w/o reliability)





(a) Model A (w/ reliability), **(b)** Model B (w/o reliability)

- Model A requires **higher CAPEX and OPEX** due to having **more parallel generators.**
- However, **lower reliability penalties are occurred in Model A** as the model considers slack capacity to reallocate the load demand when the generators fail.
- Model B has **lower CAPEX and OPEX** than Model A but incurs in **higher reliability penalties** due to its insufficient capacity.
- The more reliable design obtained by Model A enables the power generation systems to have a better economic performance than Model B.

LOLE (Loss Of Load Expectation) - time of not satisfying the load demand

LOEE (Loss of Energy Expectation) - The amount of demand that the system cannot satisfy

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CEC Case Study: Planning of Reliable Power Generation Systems with High Renewable Penetration

Case study with new capability (results expected 3/31/2024)

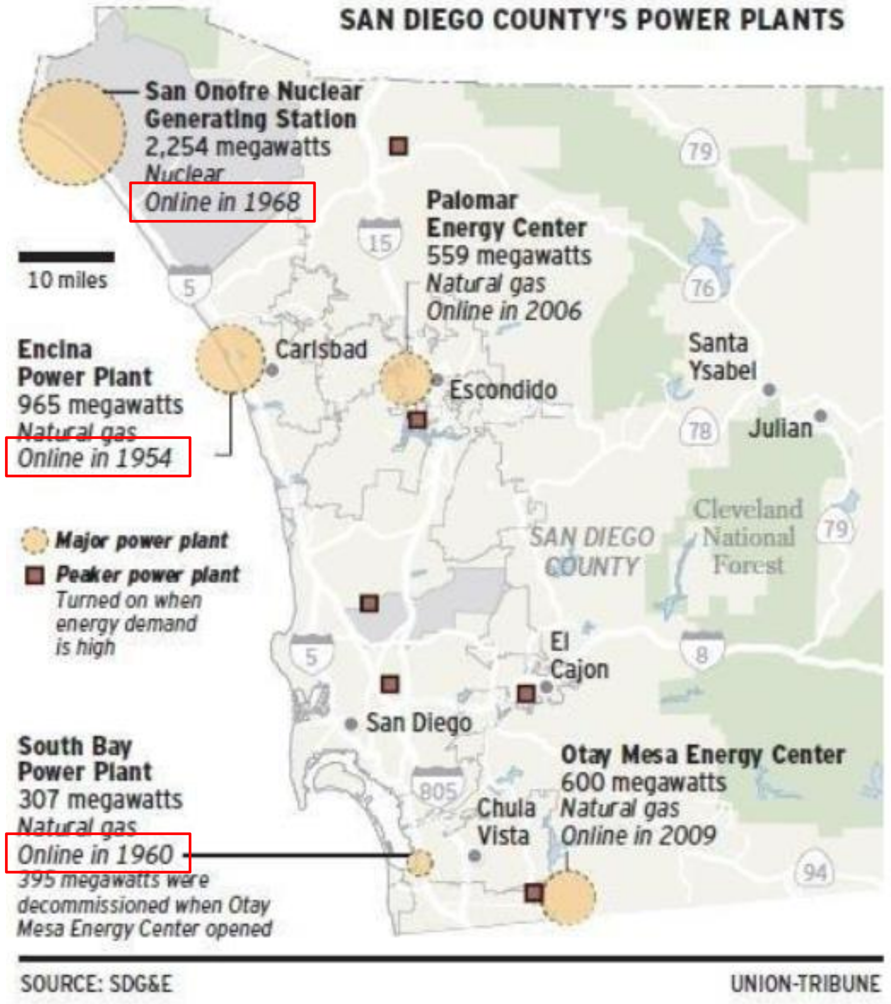
- Target area: San Diego County, California

Problem description

- For 5 major existing conventional power plants and peakers (supplementary power plants) ,
  → **determine the time to retire/decommission**
  (Installation of new conventional plants and peakers is prohibited)
- For renewable generations such as wind turbines and PV panels,
  → **time, size, location to newly install**
- By installing *batteries*, power systems reliability can be further improved.
  → **determine the time, size, location to newly install/retire, and operational strategies**
- Alternate cost of decarbonization with conventional plants with capture.

***Practical constraints**

- Target renewable generation share, CO_2 emission limit, LOLE < 0.1*



[Simplified power plants map of San Diego County]

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[1] California Peaker Power Plants: Energy Storage Replacement Opportunities, PSE Healthy Energy, 2020

*: 1 day outage with an event in 10 years

Summary

- **IDAES is a multi-lab initiative created to support long term DOE goals**
  - Decarbonizing power by 2035, economy by 2050
  - Evolving energy ecosystem requires greater flexibility & integration
- IDAES enables unique and innovative analyses across multiple time-scales
- Significant capabilities have been built to examine the market potential and controllability SOFC/SOEC-based integrated power and hydrogen systems
- Upcoming analysis entails better integrating operational realities into long term expansion planning of reliable, decarbonized electricity grids, with a key case study in collaboration with CEC.

Foundational Modeling and Optimization Partnerships Utilizing IDAES

Multi-lab Initiatives to Address Major National and DOE Priorities

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National Energy Technology Laboratory · Berkeley Lab · Sandia National Laboratories · Carnegie Mellon · West Virginia University · University of Notre Dame · Georgia Tech

DISPATCHES Design Integration and Synthesis Platform to Advance Tightly Coupled Hybrid Energy Systems

National Energy Technology Laboratory · Sandia National Laboratories · Berkeley Lab · INL Idaho National Laboratory · NREL Transforming ENERGY · University of Notre Dame

NAWI National Alliance for Water Innovation · Water TAP

And other potential future initiatives to support BIL, IIJA

PrOMMiS

National Energy Technology Laboratory · Berkeley Lab · Sandia National Laboratories · Carnegie Mellon · West Virginia University · University of Notre Dame · Georgia Tech

CCSI² Carbon Capture Simulation for Industry Impact

National Energy Technology Laboratory · Berkeley Lab · Lawrence Livermore National Laboratory · Los Alamos National Laboratory Est. 1943 · Pacific Northwest National Laboratory · Oak Ridge National Laboratory

West Virginia University · University of Notre Dame · The University of Texas at Austin · UT · University of Pittsburgh

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Georgia Tech: Nick Sahinidis, Yijiang Li, Selin Bayramoglu

2023 IDAES Technical Team Meeting, Lawrence Berkeley National Lab

Physical and Chemical Degradation Modeling of Solid Oxide Cells (FE0025912) Debangsu Bhattacharyya, West Virginia University

Optimal Design Approaches for Rapid, Cost-Effective Manufacturing and Deployment of Chemical Processes (FWP-1022423) Georgia Stinchfield (Student Presenter), Carnegie Mellon University

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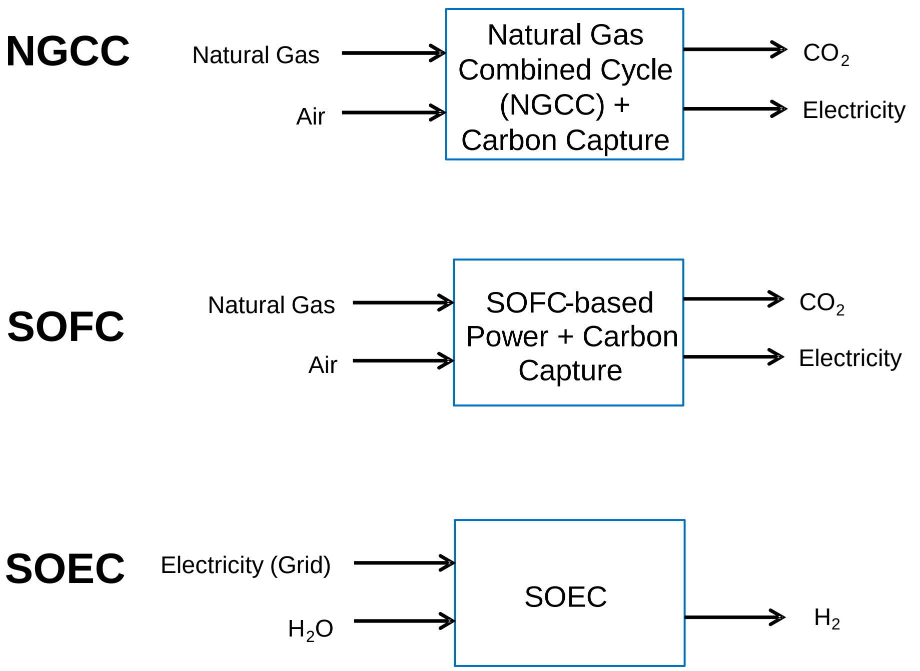
Useful Costing References for IES Work

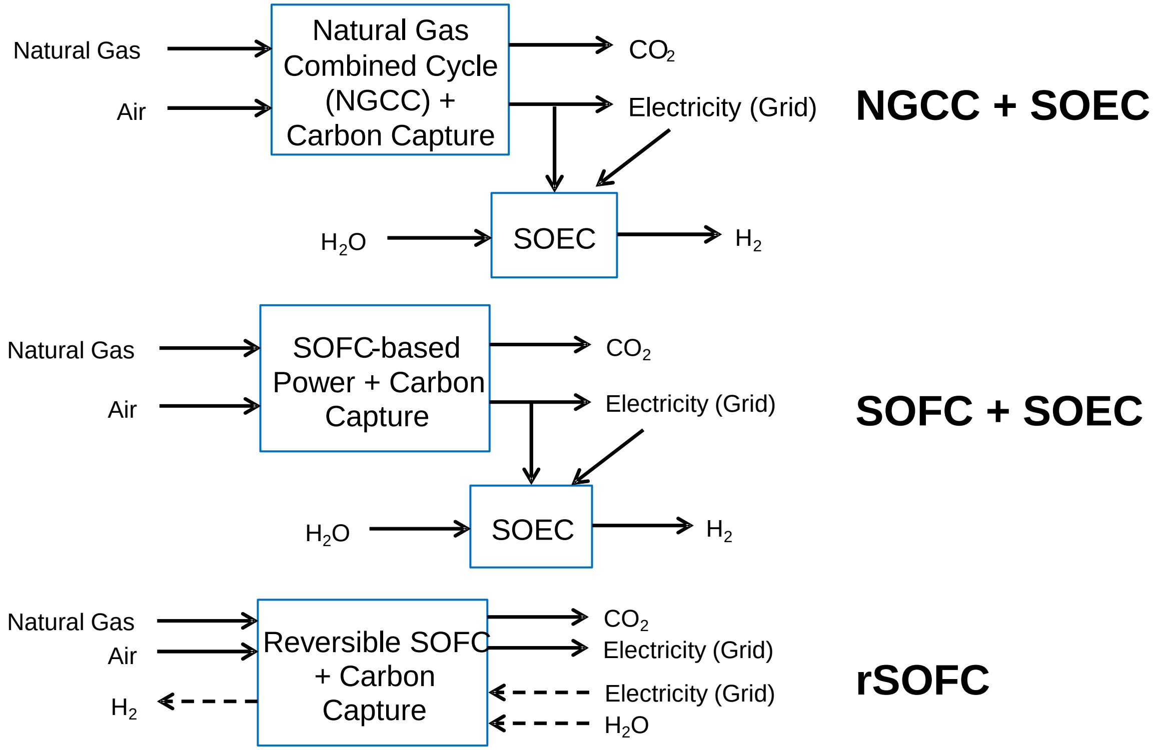
- **Integrated Energy Systems:** Eslick, Noring, Susarla, Okoli, Allan, Wang, Ma, Zamarripa, Iyengar, Burgard, Technoeconomic Evaluation of Solid Oxide Fuel Cell Hydrogen-Electricity Co-generation Concepts (DOE/NETL-2023/4322).
- **Costing Methodology:** Theis, Quality Guidelines for Energy System Studies – Cost Estimation Methodology for NETL Assessments of Power Plant Performance (NETL-PUB-22580).
- **NGCC:** Schmitt, Leptinsky, Turner, Zoelle, White, Hughes, Homsy, Woods, Hoffman, Shultz, and James. Cost And Performance Baseline for Fossil Energy Plants Volume 1: Bituminous Coal and Natural Gas to Electricity (DOE/NETL-2023/4320).
- **SOFC:** Iyengar, Noring, Mackay, Keairns, and Hackett. Techno-economic Analysis of Natural Gas Fuel Cell Plant Configurations (DOE/NETL-2022/3259).
- **SMR & ATR:** Lewis, McNaul, Jamieson, Henriksen, Matthews, White, Walsh, Grove, Shultz, Skone and Stevens, Comparison of commercial, state-of-the-art, fossil-based hydrogen production technologies (DOE/NETL-2022/3241).

High Level Block Flow Diagrams

- Compare optimized IES to stand-alone “competitive” systems
- Evaluate dispatchability in context of real energy markets

“Baseline Systems”– i.e., the competition





Time Permitting: H_2 Storage will also be considered.