

Versatile Reversible Solid Oxide Cell System for Hydrogen and Electricity Production

Alexander Vaeth

Our vision is to create a better world through energy innovations.

We collaborate with leading global customers and partners to transform powerful ideas into solutions that make energy production safer, more efficient, and environmentally responsible.

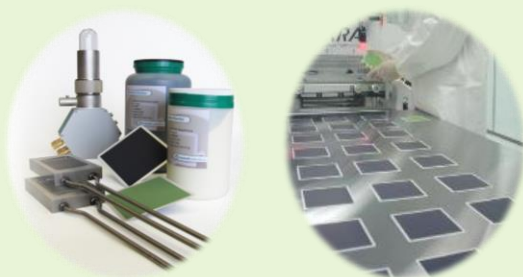
The Value of Nexceris

Nexceris is Vertically Integrated for SOC Development

Products

- **Fuel Cell Materials** provides standard and custom SOC materials and components

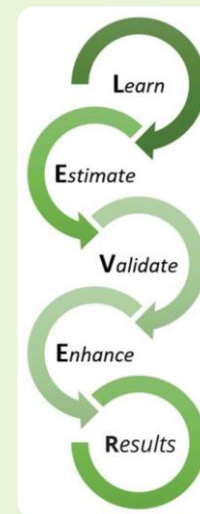
- Powders
- Inks
- Substrates
- Cells



- We work with customers to provide materials and components from lab-scale to industrial-scale
- Quickly and accurately tailor powders and components to fit the needs and processes of our customers

Services

- Joint development and contract R&D services
- Leveraging our expertise and 25+ years of know-how in the SOC industry
- Accelerate customer development timelines on material, cell, and stack levels
- Our facilities accommodate a variety of synthesis and testing methods
- Fast-paced, versatile development structure



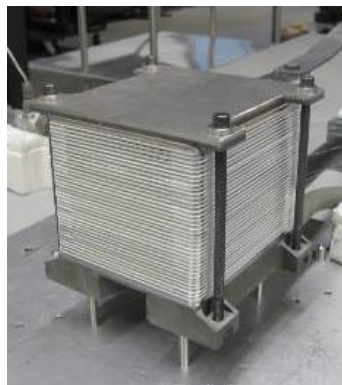
Materials

SOCs and energy storage



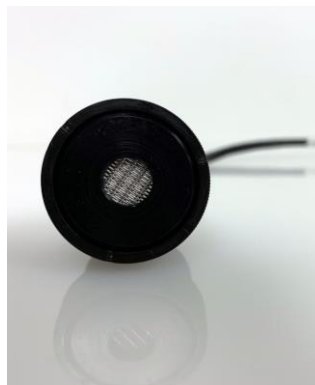
SOCs

Stationary and military



Sensors

Transportation and
energy markets



Catalysts

H₂ and chemicals
production

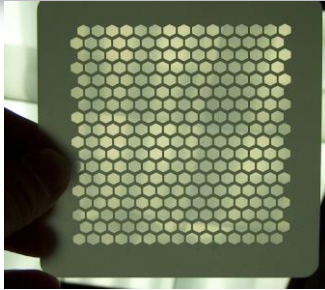


Protective Coatings

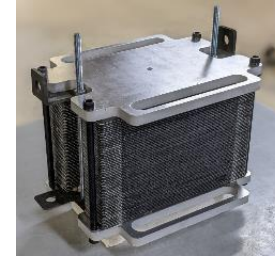
SOC and high
temperature



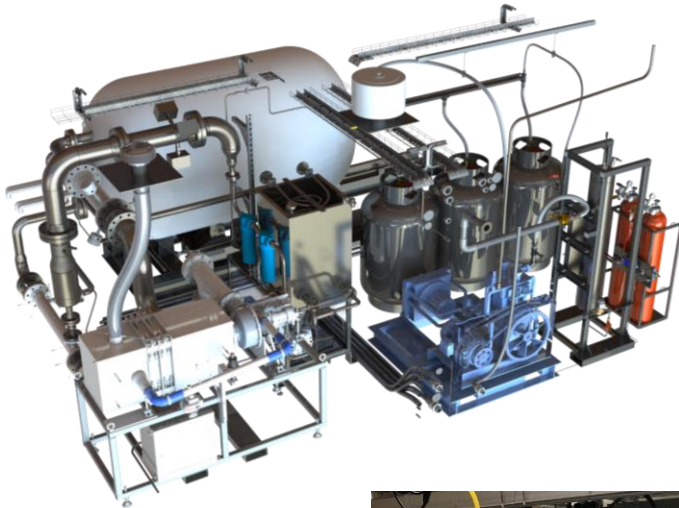
Nexceris Active Projects



Low-Cost
Manufacture
of SOEC Stacks
[DE-EE0009621]

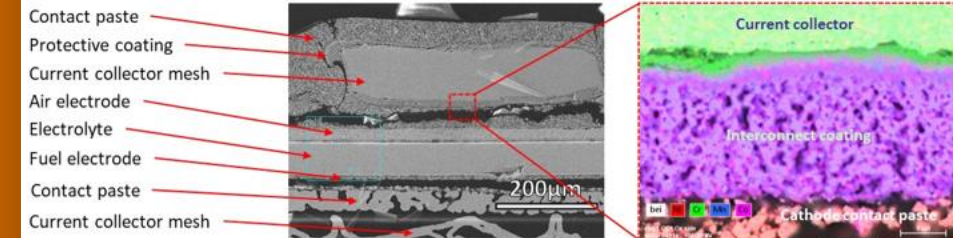


SOFC/Turbine
Hybrid Power
System
[DE-AR0000956]

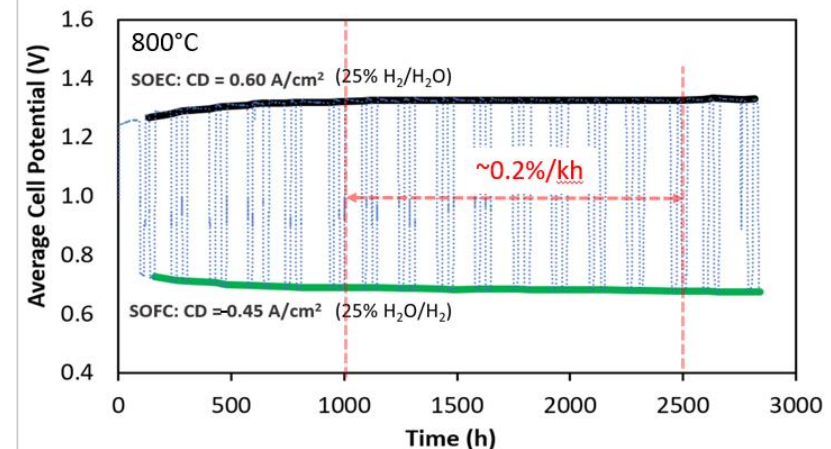


Integrated
Coating for
SOEC
Degradation
[DE-EE0008834]

Post-Mortem SEM/EDS Analysis of Stack Components



Reversible Solid
Oxide Cell for H_2
and Electricity
[DE-FE0031986]



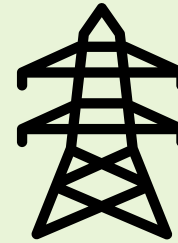


Versatile Reversible Solid Oxide Cell System for Hydrogen and Electricity Production (DEFE0031986)

Project Objectives



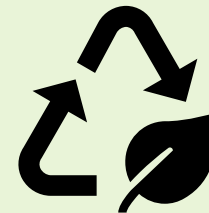
$\geq 1\text{kW}_e$ power generation in fuel cell mode with roundtrip stack efficiency (RTE) of $\geq 60\%$.



Achieve dynamic switching between modes in response to grid demands (6-hr cycles).



Achieve long-term electrolysis and define a path to produce H_2 at $\leq \$2/\text{kg}$ (at scale).



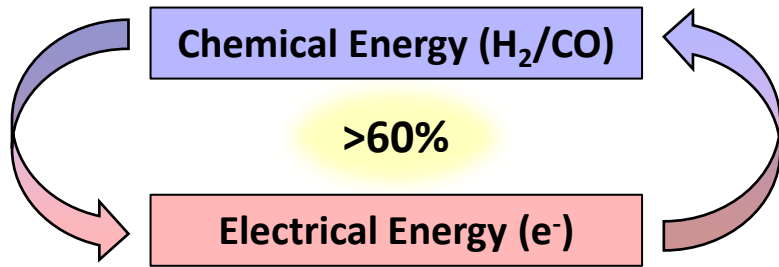
Demonstrate versatile fuel composition in electrolysis mode ($\text{H}_2\text{O} + \text{CO}_2$).



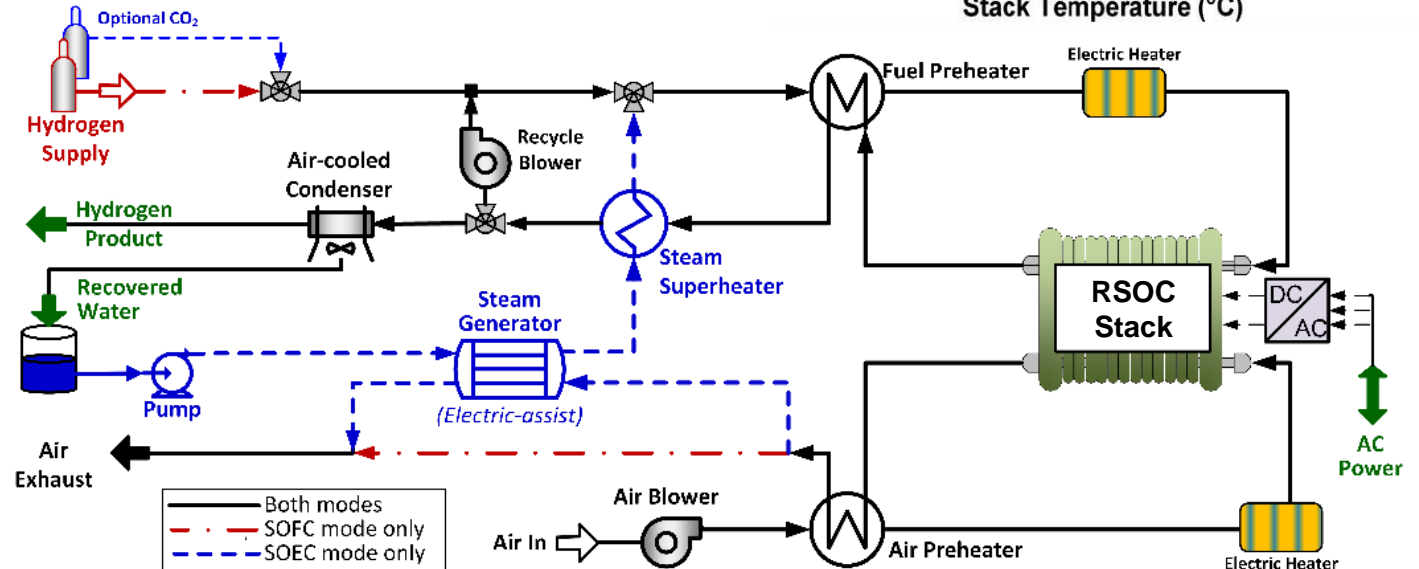
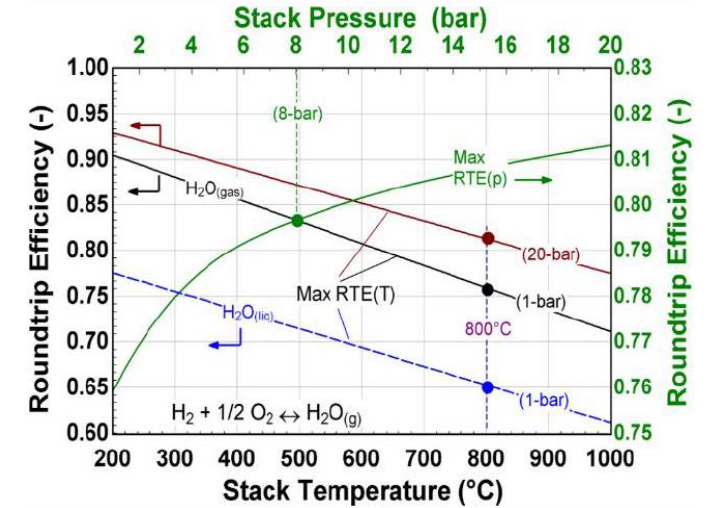
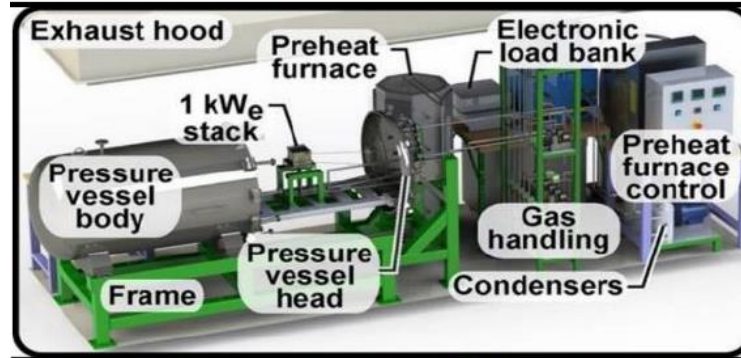
System Design

Pressurized System to Increase RSOC Stack Efficiency

- Theoretical round-trip-efficiency (RTE) of the stack is a function of **temperature** and **pressure**



- RTE *increases* with **pressure**
 - Stack performance (kinetics, mass transport) also expected to increase with pressure
- Majority of RTE increase is gained up to ~8bar





System Design

Major Challenges and Goals for Proposed System

Electrode Performance & Stability



Cell performance $\rightarrow >1\text{Acm}^{-2}$

Cell durability $\rightarrow 0.5\%/1000\text{hrs}$

Dynamic switching

Stack Validation & Co-Electrolysis



Dynamic (6hr) stack cycling

Stack RTE > 60%

*Co-electrolysis exhaust analysis
with GC*

System Demonstration



*Pressurized BOP construction at
CSM*

*Ambient BOP construction at
Nexceris*

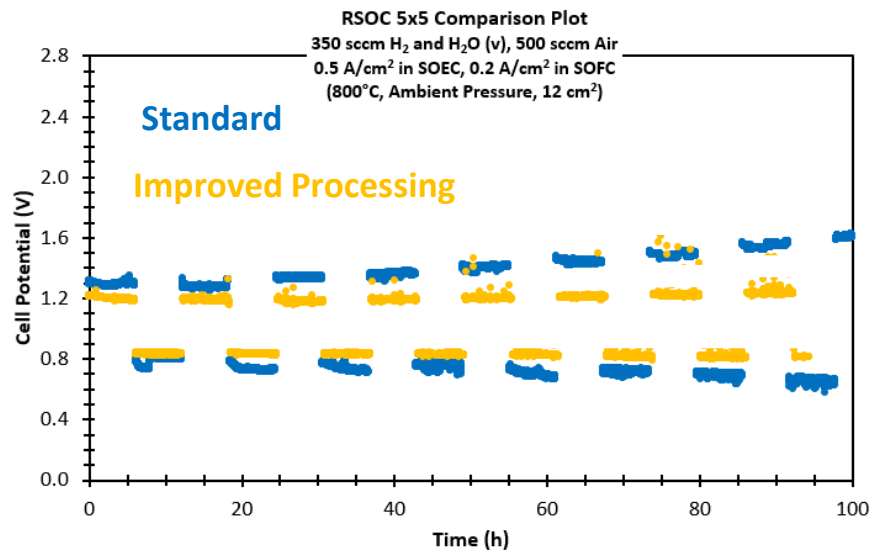
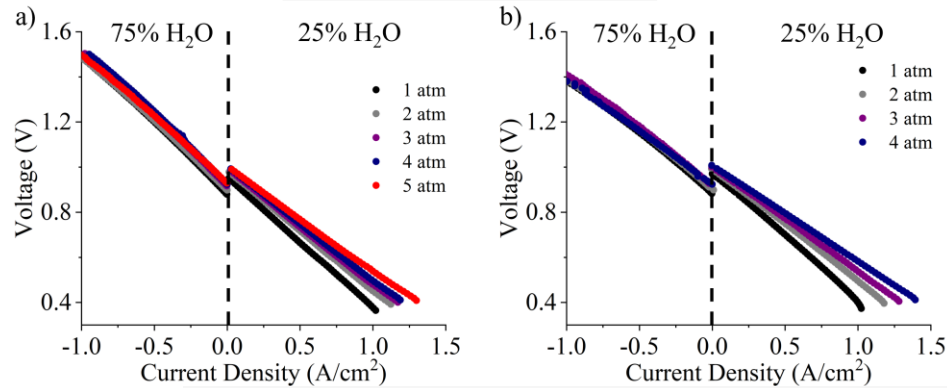
*1kW_e with 60% stack RTE at
 0.7Acm^{-2}*



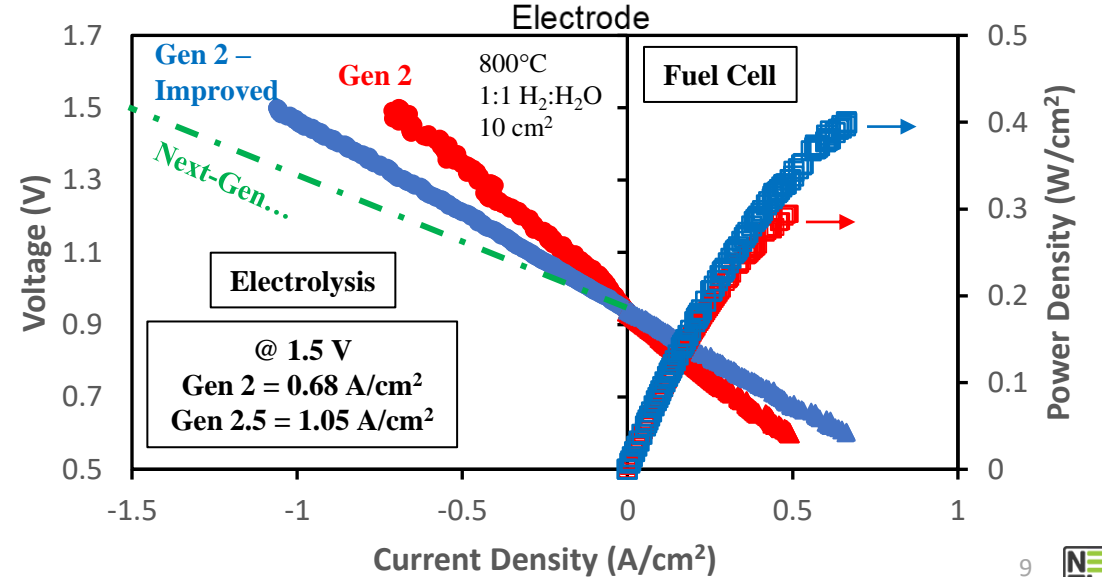
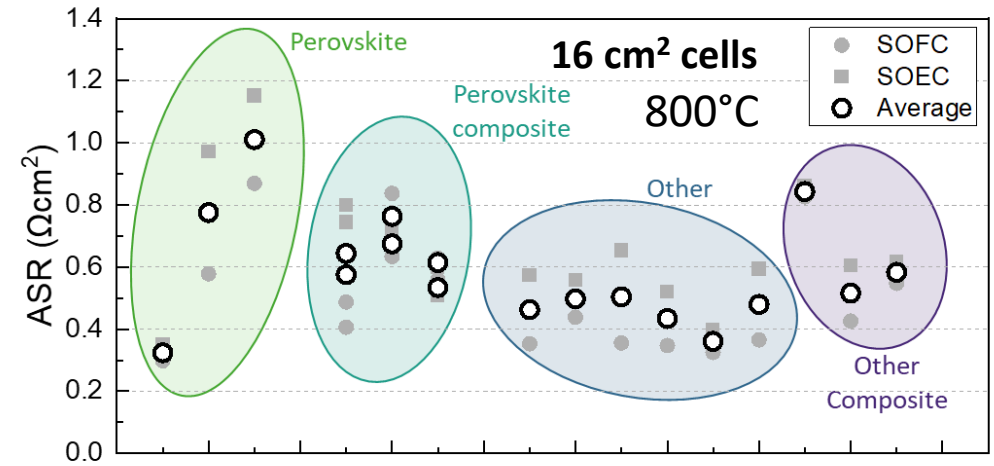
Electrode Performance & Stability

Electrode Evaluation for SOEC/SOFC

Developing & Understanding Pressurization



Screening & Scaling High Performance

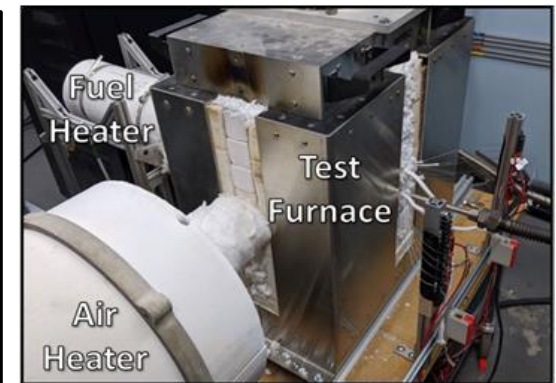
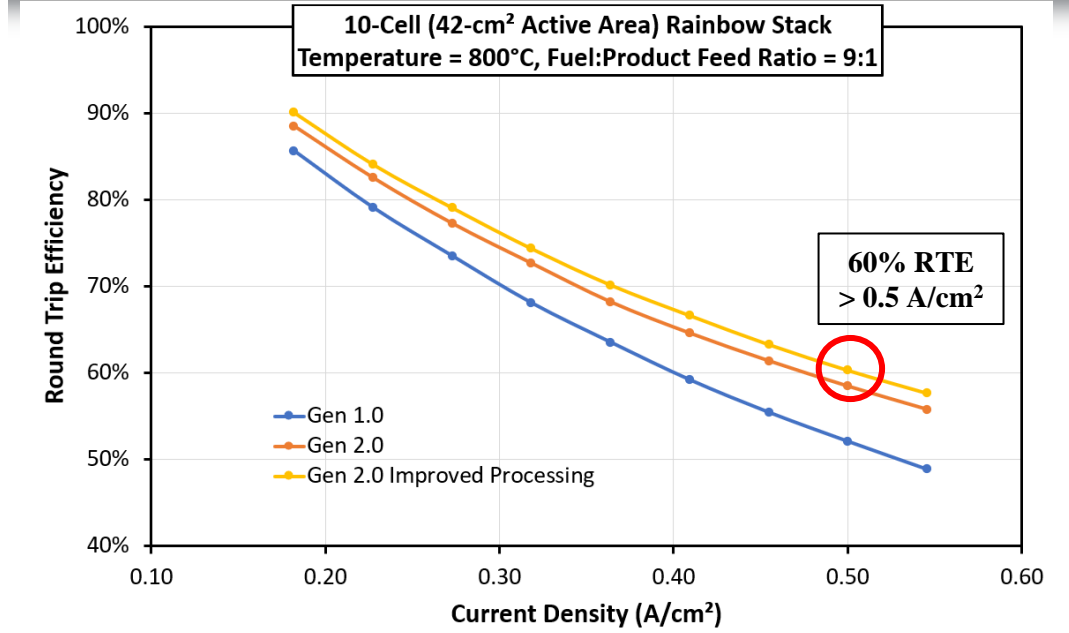
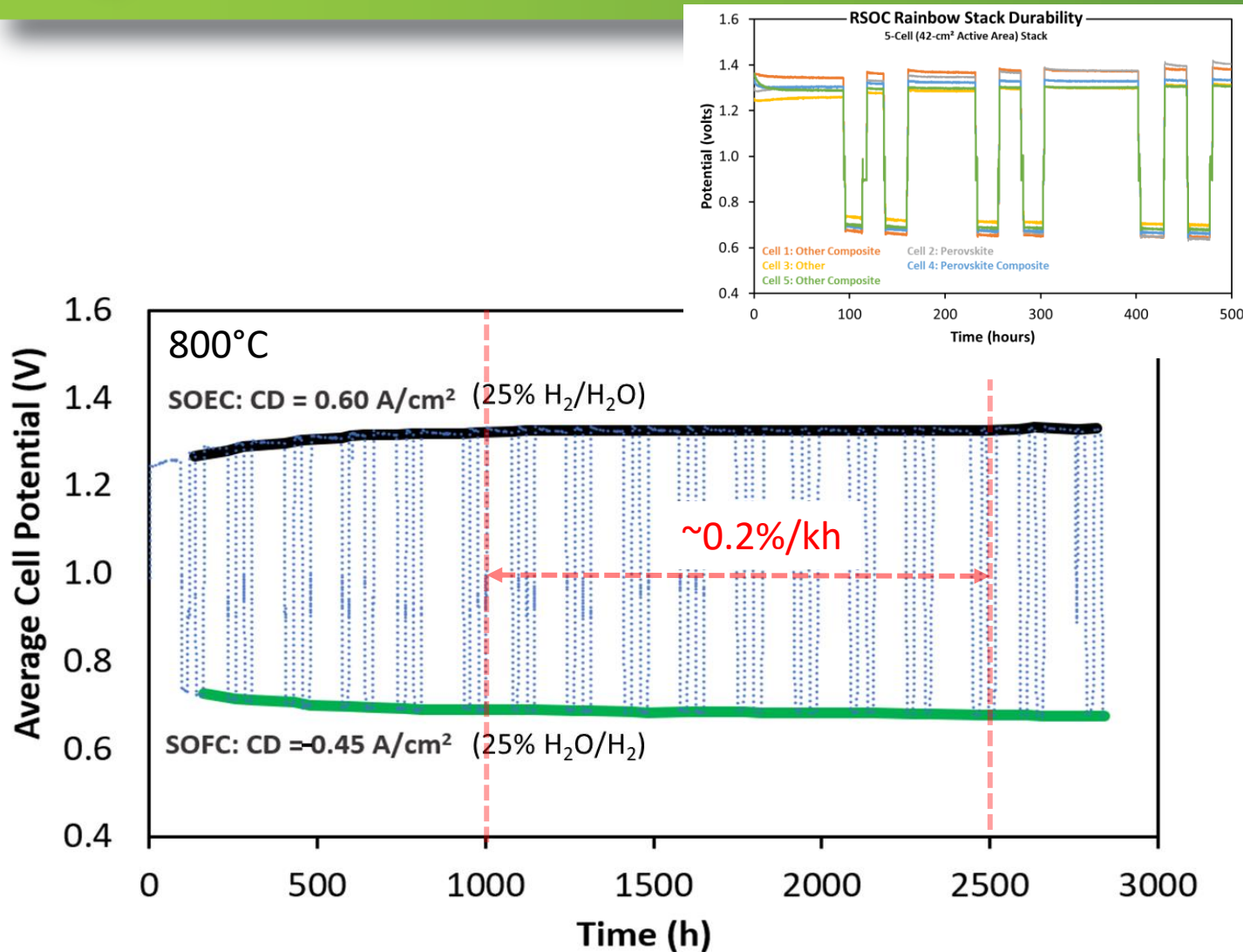


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Stack Level Performance & Stability

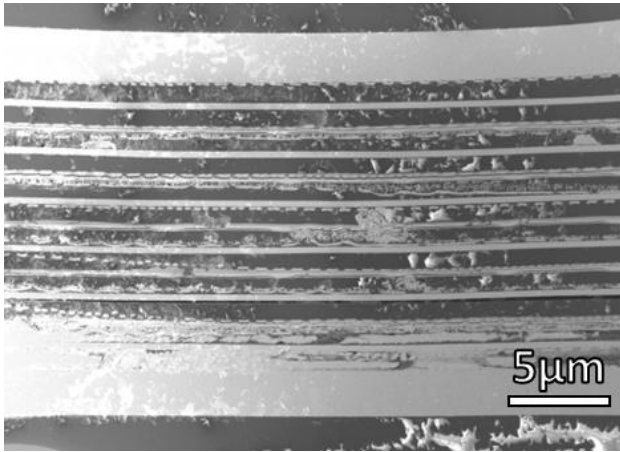
RSOC Durability Test on a 5-cell “Rainbow” Stack



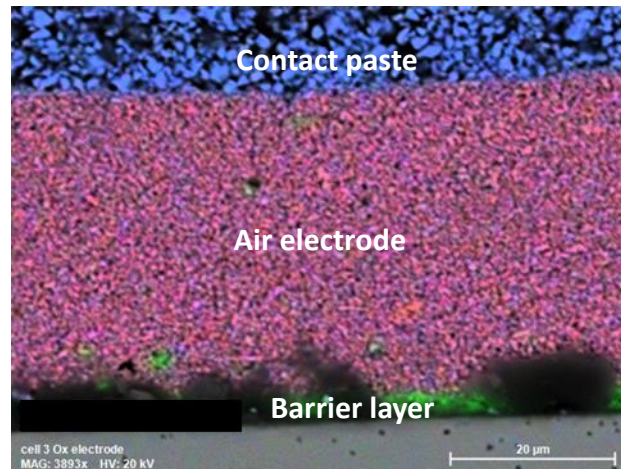
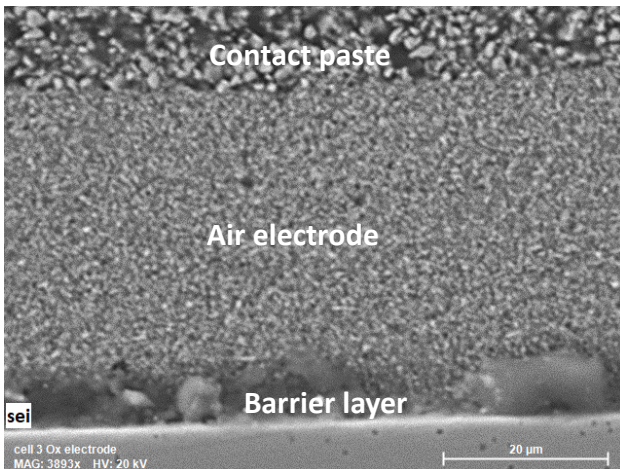
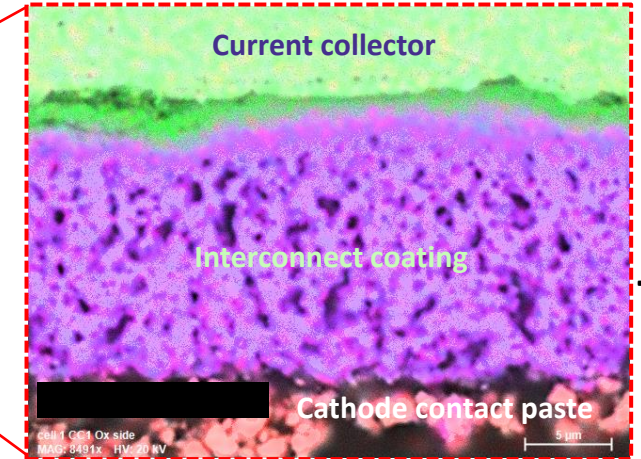
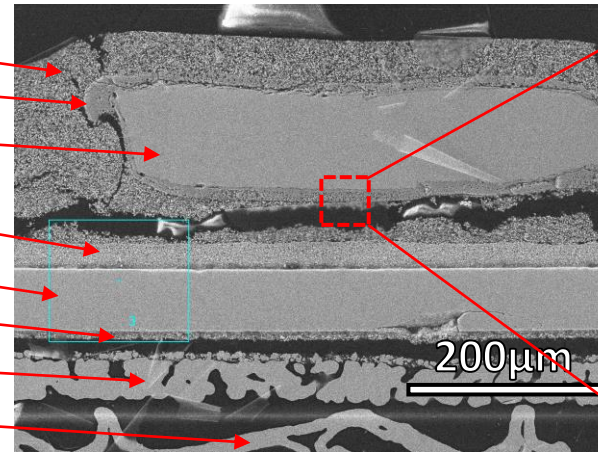


Stack Level

3000hr Post-Mortem SEM-EDS Analysis



Contact paste
Protective coating
Current collector mesh
Air electrode
Electrolyte
Fuel electrode
Contact paste
Current collector mesh

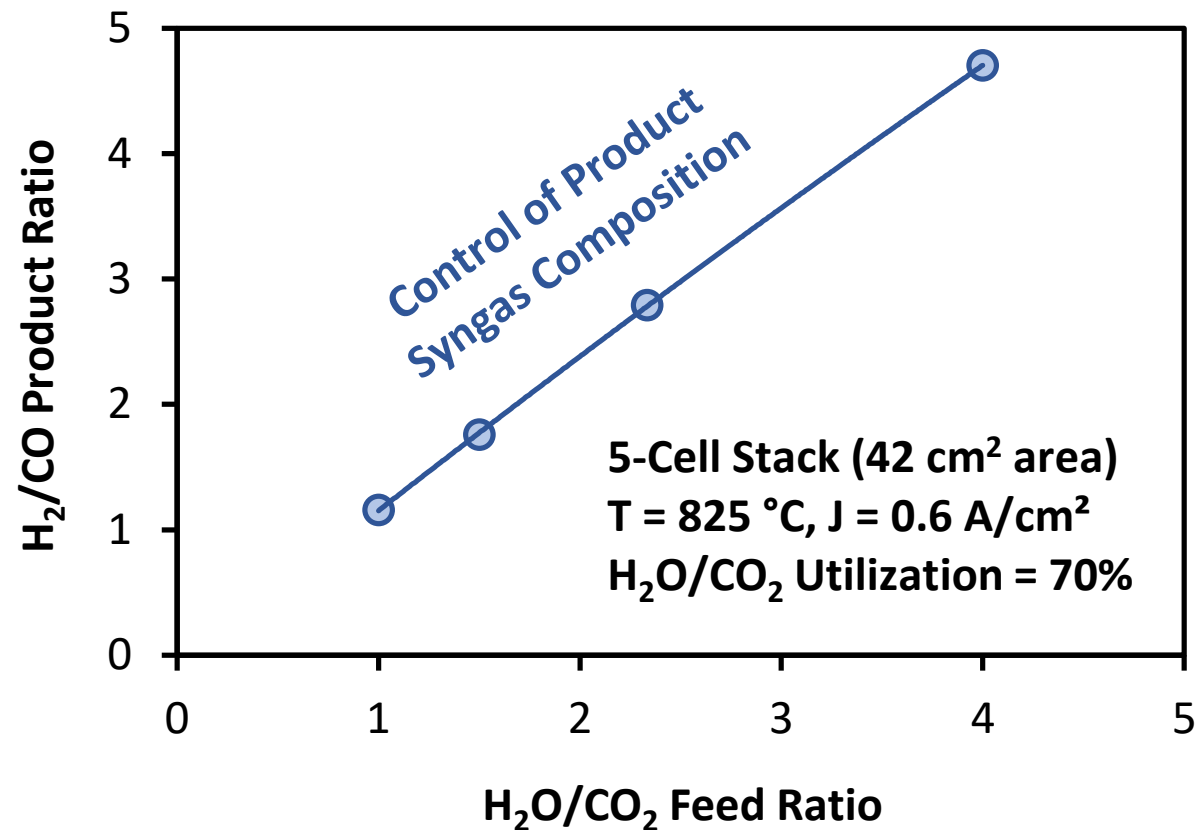
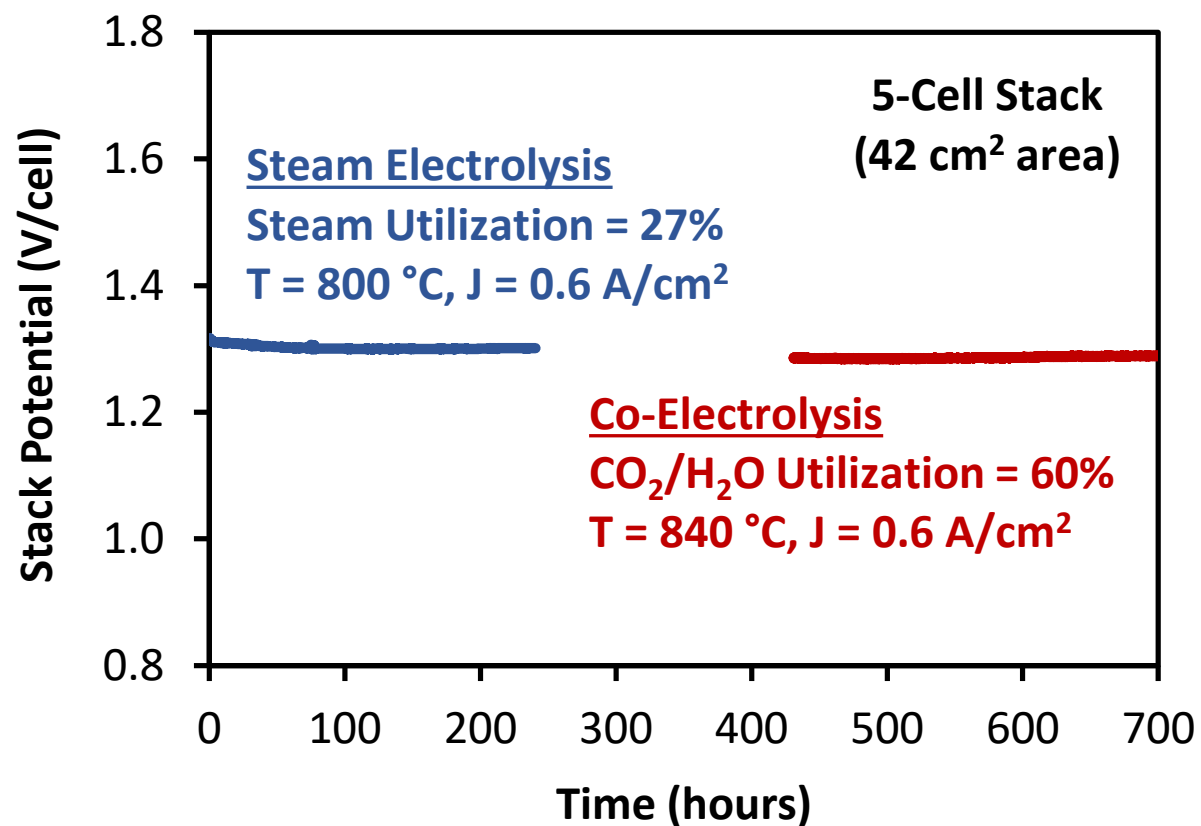


- Protective coating locks Cr evaporation in source.
- No evidence of Cr deposition in cathode.
- No evidence of air electrode or barrier layer delamination.
- Collaboration with PNNL



Stack Level Performance & Stability

Co-Electrolysis on a 5-cell Stack



Fully Integrated Demonstration System

Fully integrated and automated Reversible Solid Oxide Cell

Utilizing heat exchangers and recycler system to utilize exhaust heat

Bi-directional load box for automated mode switching

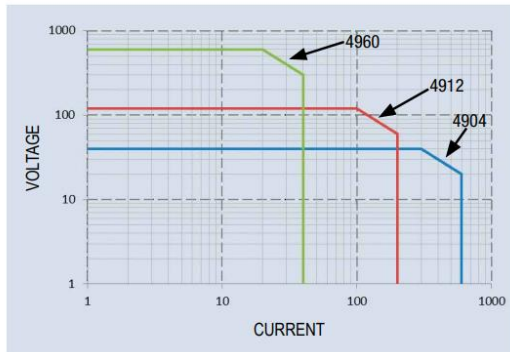
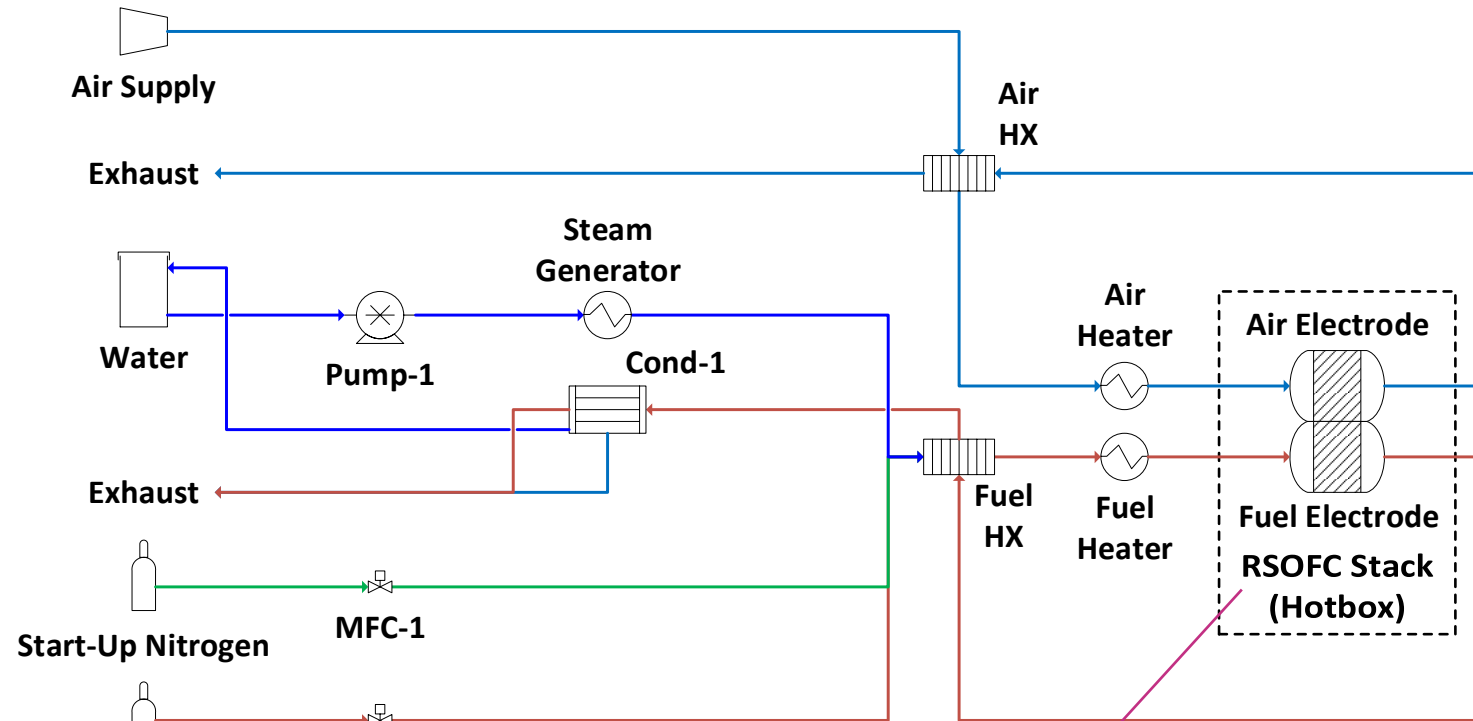
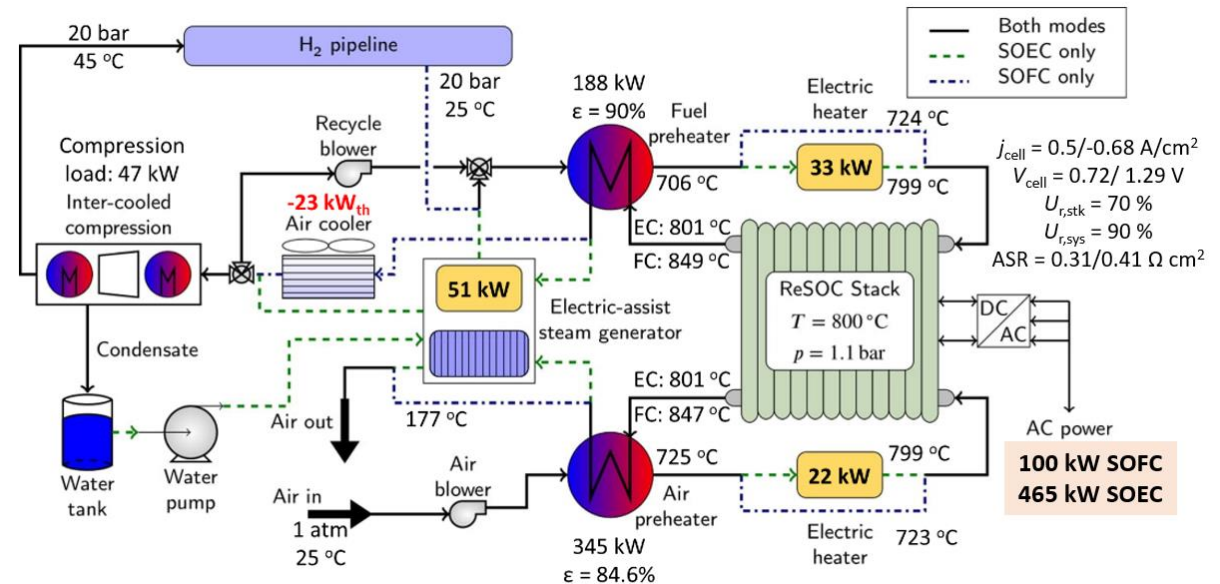


Figure 2 - Discharge Operating Envelope

Q3 2023 Nexceris will demonstrate a 1 kW_E stack and achieving >60% RTE using a 36-cell 96cm² active area cells



- Process flow diagram (PFD) developed for initial techno-economic analysis (TEA).
- PFD will be combined with an electrochemical model for TEA of a pressurized system.
- Pressurized stack testing capabilities (< 10 bar) under construction at Colorado School of Mines.
 - Long-term, stack-level durability testing under RSOC conditions





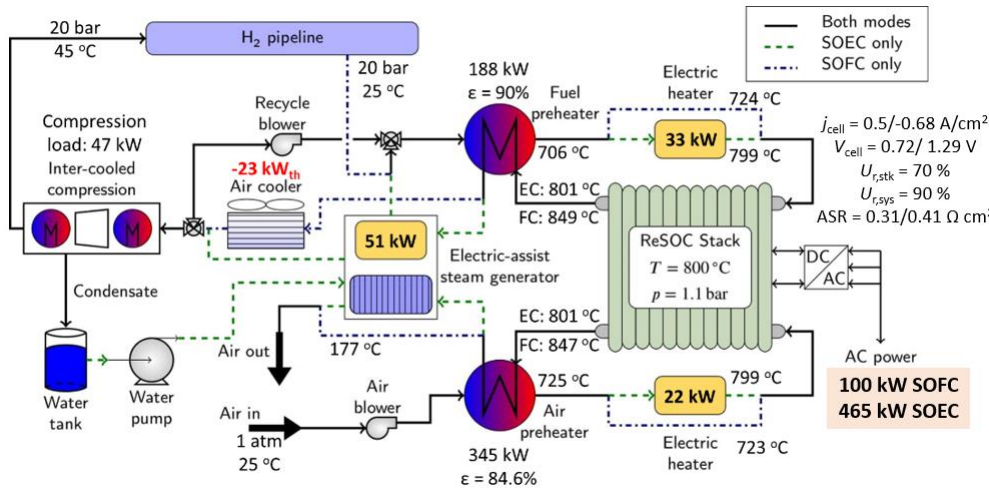
Techno-Economic Analysis

PFD, TEA, Breadboard Validation

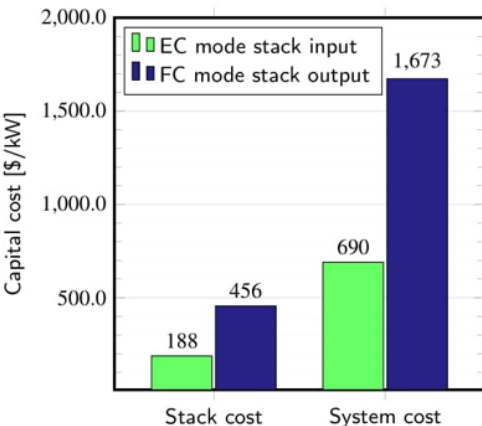


COLORADO SCHOOL OF MINES
EARTH • ENERGY • ENVIRONMENT

TEA Overview (gPROMS model)

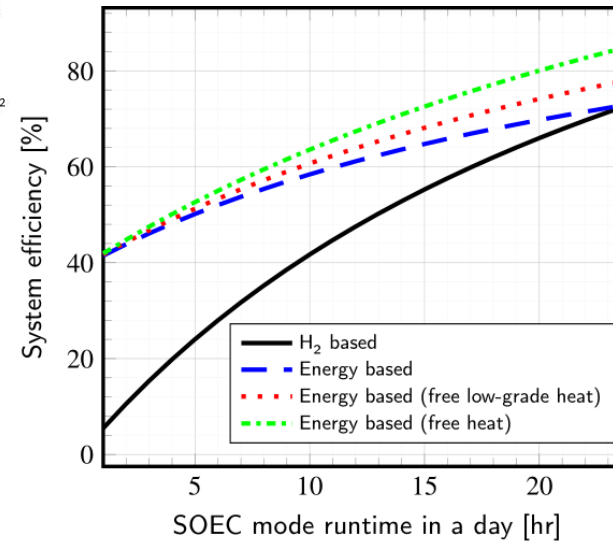


Model Parameters



- System life: 20 years
- Stack life: 5 years
- Installation factor: 1.4
- Indirect factor: 1.5
- Capacity factor: 90%
- Variable O&M cost
 - 5 ¢/kWh
 - Converted from kg H₂ to kWh using LHV of hydrogen

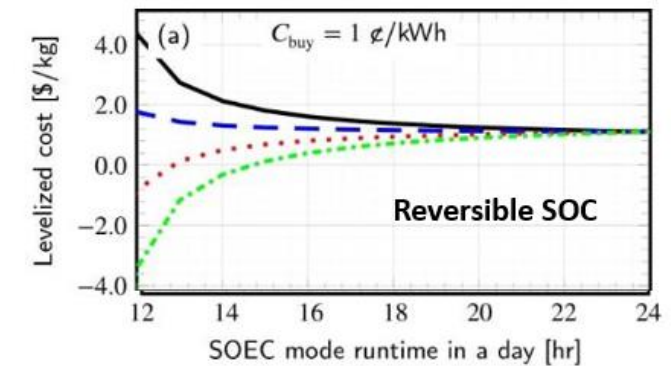
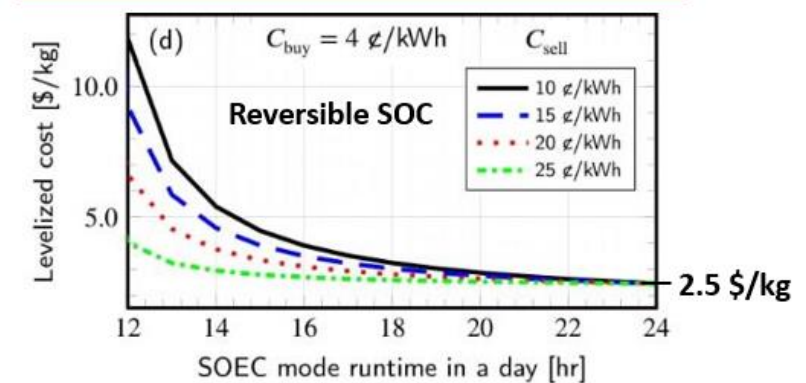
Better Definition of System Efficiency



$$\eta_{H_2} = \frac{E_{H_2, LHV, SOEC}}{E_{H_2, LHV, SOFC} + E_{elec, SOEC}}$$

$$\eta_{En} = \frac{E_{H_2, LHV, SOEC} + E_{elec, SOFC}}{E_{H_2, LHV, SOFC} + E_{elec, SOEC}}$$

SOEC or SOFC? Dependent on electric buy and sell price



Acknowledgements



Prof. Robert Braun

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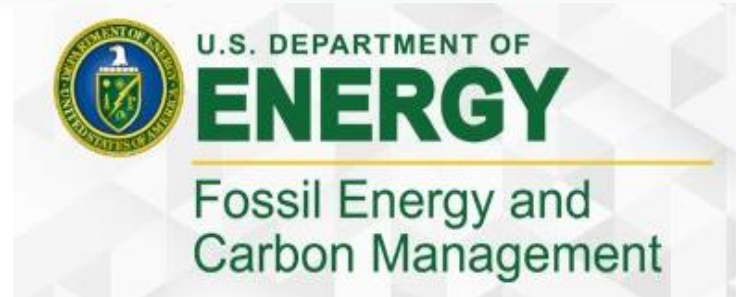
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**Questions? Feel free
to say hi!**

