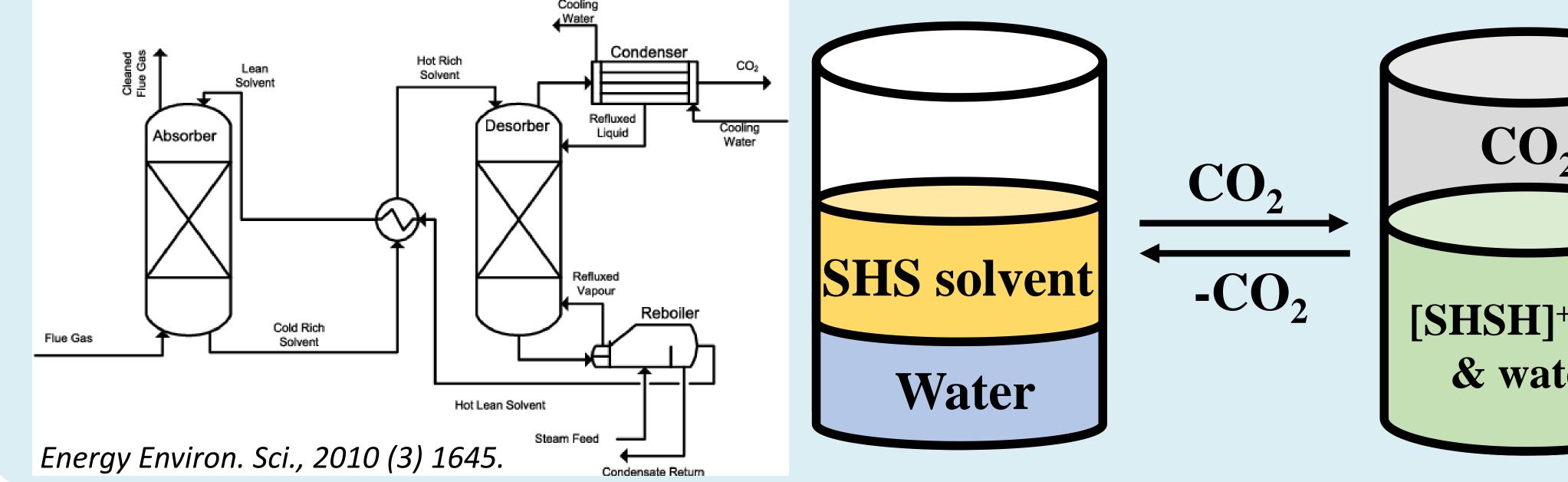
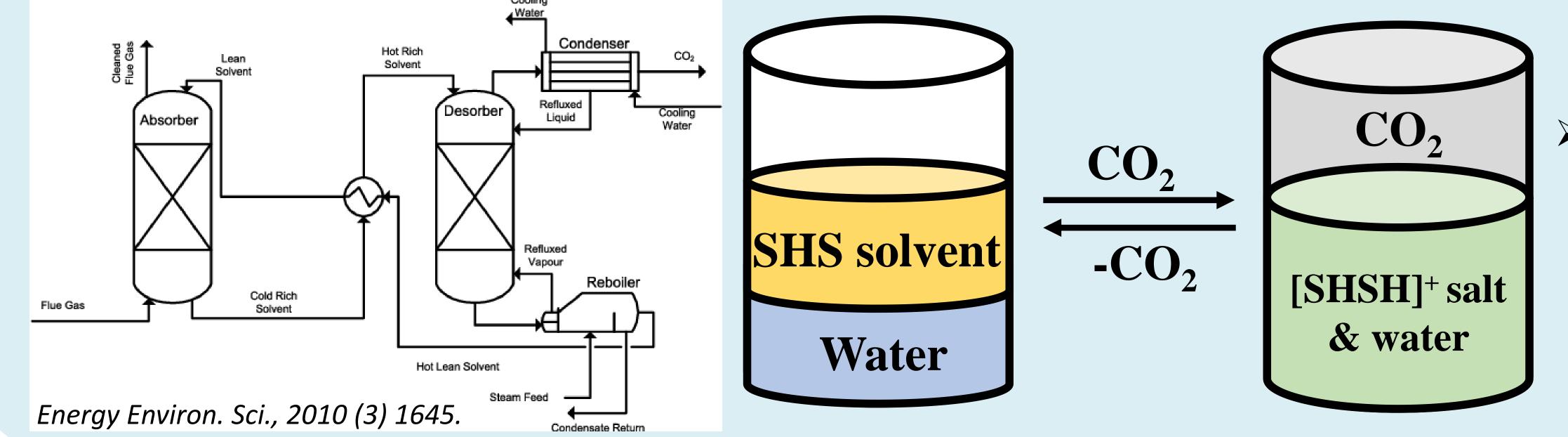
Bench-scale Development of a Transformational Switchable-hydrophilicity Solventenabled Absorption Process for Energy-efficient CO₂, Capture and Fixation

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MOTIVATION

A new switchable-hydrophilicity solvent (SHS) based post-combustion CO₂ capture technology delivering both carbon capture and fixation can significantly improve the energy efficiency of CO₂ capture process





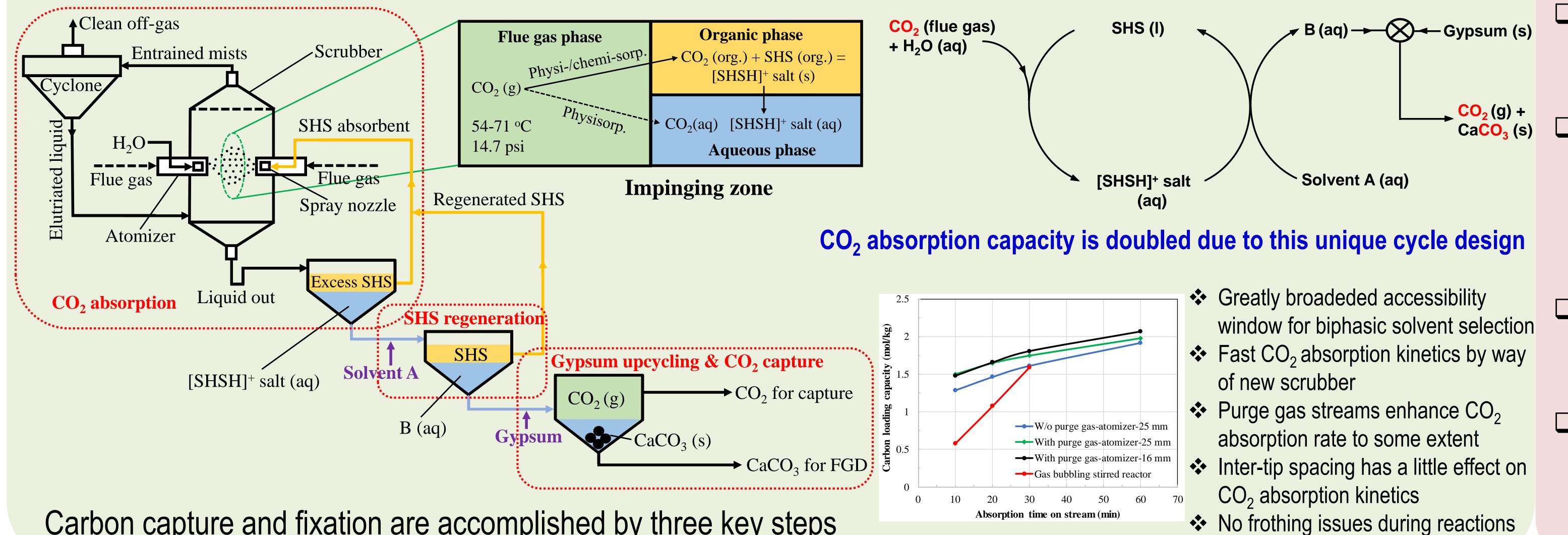
GRAND CHALLENGES FOR CCS WITH CONVENTIONAL AMINE ABSORBENTS

 \succ Fast amine solvent loss rate due to thermal and oxidative degradation > High energy penalty for rich solvent regeneration > Conventional carbon emissions mitigation technologies generally suffer up to 40% or

more of the energy output of a coal-fired power plant

OVERALL OBJECTIVES Design an integrated carbon capture process to improve energy efficiency Build a gas-liquid impinging scrubber with fast interfacial mass transfer rate Regenerate rich solvent at ambient or mild temperature Offer a sustainable approach to effective waste valorization

CARBON CAPTURE AND CONCURRENT GYPSUM WASTE UPCYCLING



KEY INNOVATIONS

□ Absorption reaction/extraction coupling to break up chemical equilibrium limitations

Low *T*rich solvent regeneration to mitigate solvent makeup rate, equipment corrosion, and energy consumption

Gypsum waste upcycling to limestone sorbent to enable direct use of low-grade coal

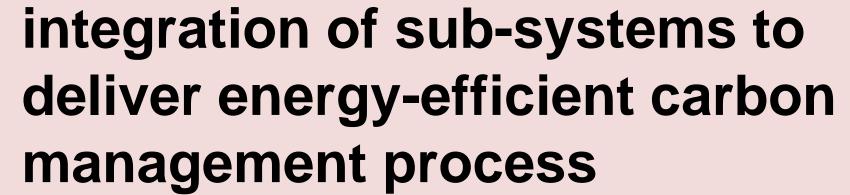
Innovative design and

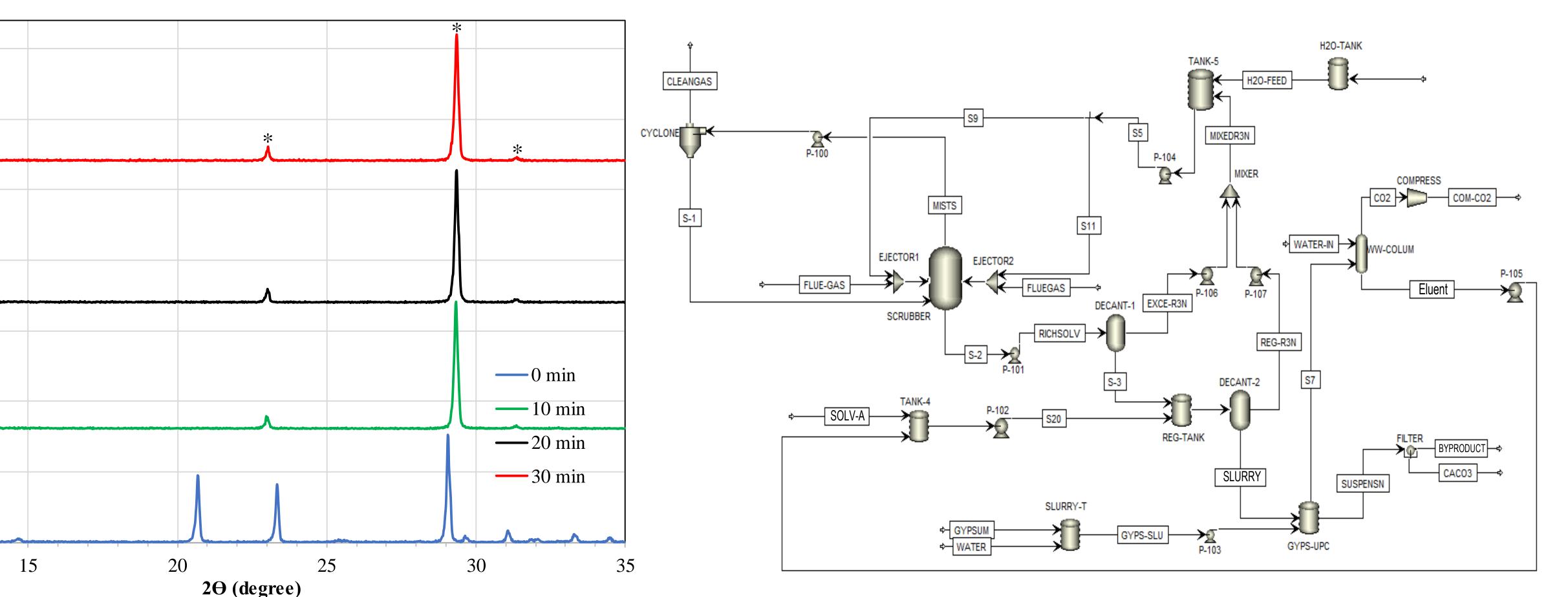
Carbon capture and fixation are accomplished by three key steps

Regenerant	Regeneration Temp. (°C)	Regeneration time (min)	ER (%)
A1	40	10	83.33
	50	10	85.71
	65	10	88.00
	65	52	88.10
A2	R.T.	10	95.23
	65	45	100.00
A3	40	20	No LLPS
	50	10	87.00
	65	10	90.72
	65	30	94.00

✓ Spontaneous liquid-liquid phase separation (LLPS) promotes a deep regenerability of rich solvents under mild operating conditions

✓ Final equilibrium recovery (ER) of lipophilic SHSs is roughly independent of initial carbon loading of rich solvents





Process flow diagram (PFD) of the whole carbon capture and fixation process used for the TEA

Gypsum conversion to limestone at 40 °C (0 min: gypsum, *: calcite, and limestone yield: ~100%)

CARBON CAPTURE PERFORMANCE METRICS GYPSUM UPCYCLING TO LIMESTONE

3500

3000

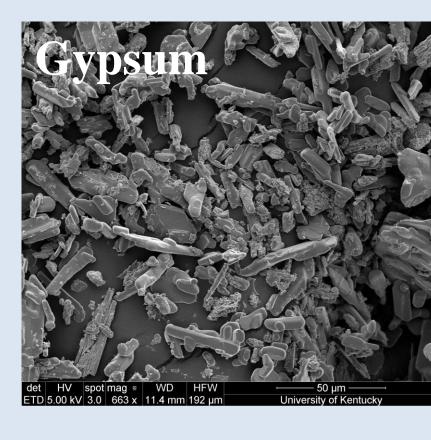
2500

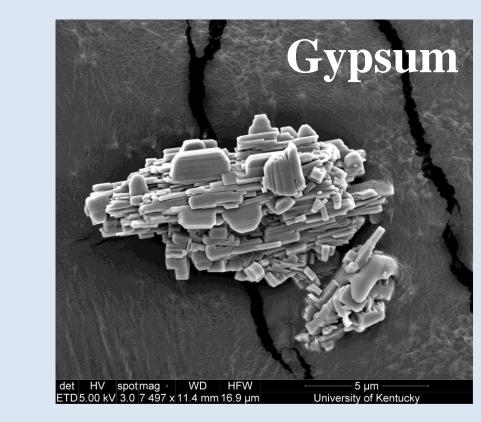
(**ne**) 2000

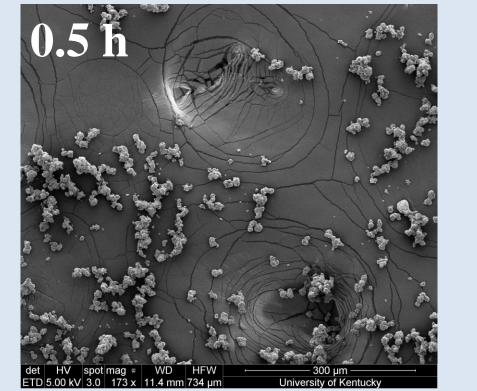
Intensity 1200

1000

500









Rod-like gypsums are fully transformed into well-faceted calcite crystals within 30 min of reaction time under mild synthesis conditions

Metrics	Values	
CO ₂ loading capacity at 40 °C	≥ 2 mol/kg	
Overall cyclic CO ₂ -equivalent loading capacity	≥ 1.8 mol/kg	
CO ₂ absorption time	≤ 10 min	
ER of rich solvents at $T \le 65 ^{\circ}\text{C}$	≥ 95%	
Regeneration reaction time	≤ 10 min	
Gypsum waste purity	≥ 95%	
Gypsum conversion efficiency	≥ 95%	
Gypsum carbonation time at $T \le 65 ^{\circ}\text{C}$	≤ 10 min	
Limestone purity	≥ 95%	
CO ₂ removal efficiency	≥ 90%	
Final CO ₂ purity in vapor phase	≥ 95%	
Increase in cost of electricity generation	≤ 35%	
Overall CO ₂ capture cost	~\$30/tonne	

FUTURE WORK

- Upgrade the whole evaluation apparatus to reach its full bench-scale potential
- Design and assemble the atomizers to enable an overall solvent flowrate on a GPM scale
- A 2nd-generation scrubber will be built and commissioned inhouse with novel packing materials in place
- CO₂ absorption kinetics and overall CO₂ cyclic loading capacity will be further enhanced
- Seamlessly integrate the key three-unit operations to enable a continuous operational process
- More exhaustive TEA of this carbon capture technology will be undertaken

ACKNOWLEDGEMENTS

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