CO₂ Capture at LG&E Cane Run NGCC Power Plant DE-FE0032223

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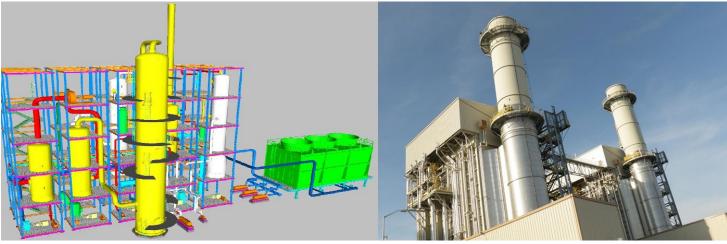
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Project Overview

- FEED study for retrofitting the LG&E (a PPL Corporation Facility) Cane Run Unit 7, a 640 MW NGCC located in Louisville KY, with the University of Kentucky's solvent-based carbon capture system
- Funding = \$7,3303,164. DOE \$5,842,517 + Cost-share \$1,460,647
- Project performance dates 12/22/2022 6/30/2024



Source UK

Source PPL

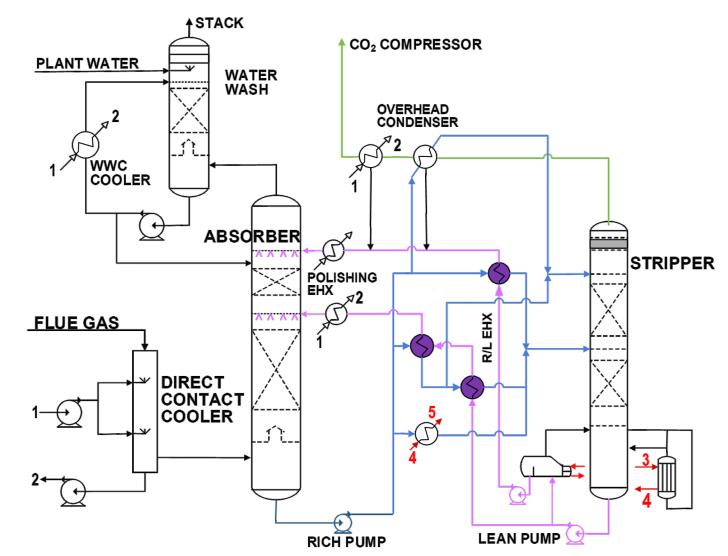
Project Team

- **EPRI**: Non-profit, electric sector R&D; prime
- Louisville Gas and Electric & Kentucky Utilities, a PPL
 Company (PPL): owners of Cane Run Unit 7 NGCC plant
 located just SW of Louisville, KY along the Ohio River
- University of Kentucky (UK) Carbon capture technology developers
 - Vogt Power International: HRSG OEM, subcontractor to UK
 - ALL4: Performing EH&S, subcontractor to UK
- Bechtel: Performing Front-End Engineering and Design (FEED)
- University of Michigan: Global CO₂ Initiative for LCA



UK CCS Process

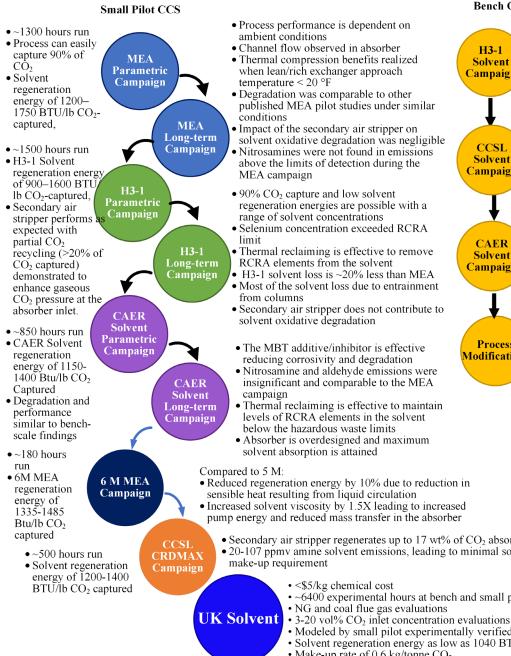
- Aqueous amine solvent
- Split lean solvent feed to absorber
 - 95% capture rate
- Split rich solvent feed to stripper
 - Reboiler duty <1060 BTU/lb (2.45 MJ/kg)
- In-duct water spray flue gas cooling
 - Reduced capital cost



Source UK

UK CCS Experience

- Active research since 2006
- Technology validated and scaled up from lab to pilot scales
- >10,000 operational hours on coal and simulated-NGCC flue gas
- Solvent with \$6.5kg/chemical cost, 0.6 kg/tonne CO₂ makeup rate, and Aspen Plus[®] model experimentally verified at pilot scale



Bench CCS

CCSL

Solvent

Campaign

Process

H3-1 Solvent

- Thermal compression benefits realized
- published MEA pilot studies under similar

• Impact of the secondary air stripper on solvent oxidative degradation was negligible • Nitrosamines were not found in emissions above the limits of detection during the

- regeneration energies are possible with a
- Selenium concentration exceeded RCRA
- Thermal reclaiming is effective to remove
- Most of the solvent loss due to entrainment
- Secondary air stripper does not contribute to
- reducing corrosivity and degradation
- Nitrosamine and aldehyde emissions were insignificant and comparable to the MEA
- Thermal reclaiming is effective to maintain levels of RCRA elements in the solvent
- · Absorber is overdesigned and maximum
- Reduced regeneration energy by 10% due to reduction in sensible heat resulting from liquid circulation • Increased solvent viscosity by 1.5X leading to increased
- pump energy and reduced mass transfer in the absorber

• Secondary air stripper regenerates up to 17 wt% of CO₂ absorbed • 20-107 ppmv amine solvent emissions, leading to minimal solvent

- ~6400 experimental hours at bench and small pilot scales • NG and coal flue gas evaluations
- Modeled by small pilot experimentally verified Aspen Plus[®]
- Solvent regeneration energy as low as 1040 BTU/lb CO₂
- Make-up rate of 0.6 kg/tonne CO₂

H3-1 Solvent Performance: $\sim 27\%$ reduction in solvent regeneration energy, 35-45% reduction in circulation rate, Campaign low degradation compared to 30 wt% MEA

> CCSL Solvent Performance: ~30% reduction in solvent regeneration energy, 40% reduction in circulation rate, low degradation compared to 30 wt% MEA

• CAER Solvent Performance: ~20% reduction in solvent regeneration energy, 30% CAER reduction in circulation rate. Solvent low degradation compared Campaign to 30 wt% MEA • Solvent Cost <\$5/kg chemical

> • Absorber Temperature Control via discretized packing

- Modificatio • În-situ liquid redistributor • Solvent spray with <50 μm droplets leads to 2.6-4.1X?increased CO2
 - absorption per unit volume • Staged feed to Absorber and Stripper
 - Heat Integration with steam cvcle feedwater
 - Solids circulation solvent recovery system reduces amine emissions by 50%

Lab CCS

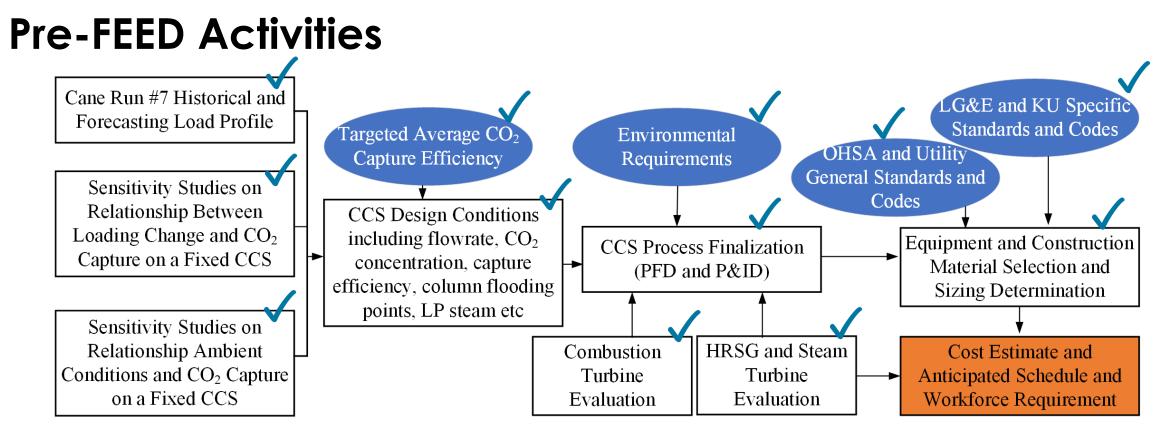
Nitrosamine Removal

Cane Run 7 – Host Site

- Location: Louisville, KY
- Capacity: 640 MW
- Fuel: Natural Gas
- **Opened:** 2015
 - Cane Run 7 is Kentucky's first natural gas combinedcycle (NGCC) generating unit
- Retirements:
 - Coal units 1 through 6 were demolished in 2019
- Capacity Factor:
 - ~ ~85% from 2016-2021



Source LGE-KU/PP



- >95% equipment/process service factor
- Baseload condition based on historic & forecasted generation data
- Solvent-independent design
- Design for reliability and operability
- Full-plant integration and CT operation impact analysis

- Vogt Power on team to analyze:
 - Impact on HRSG operations
 - In-duct cooling, without DCC
 - Elimination of flue gas boost fan, with HRSG accommodating additional pressure
 - Best steam extraction location and impact on steam cycle

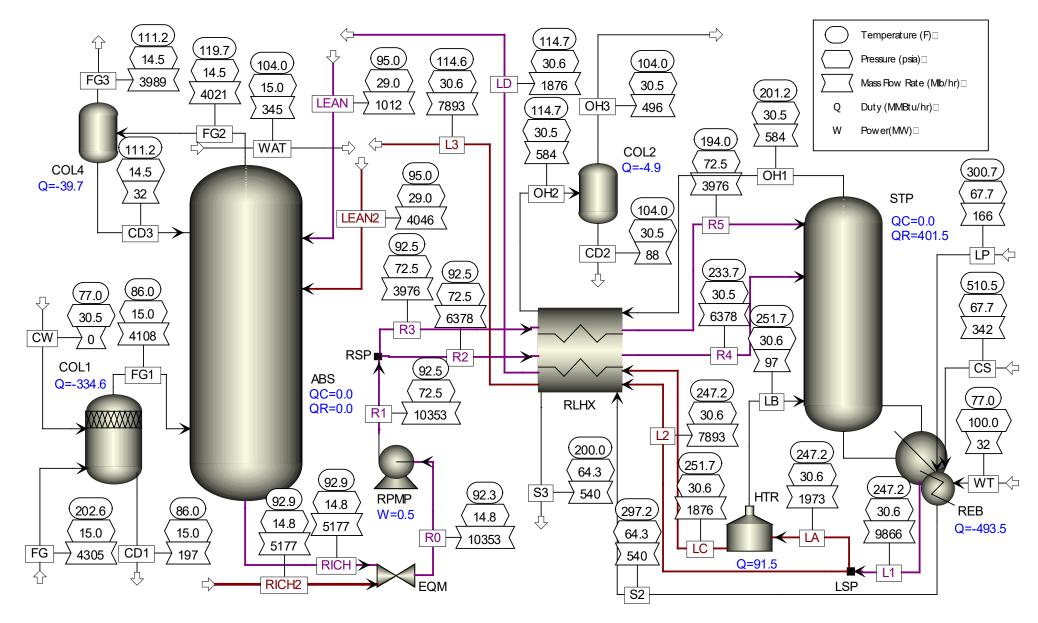
Completed

Design Condition Selected

- Evaluated historical plant operation by season
 - Cooling water temperature
 - CO_2 , O_2 , and NO_x concentration
 - Gas flow rate

Cases	Case 1: 89F Amb. 2x100% EC ON with CCS LP Drum Extraction	Case 2: 89F Amb. 2x100% EC OFF with CCS LP Drum Extraction	105F Amb. 2x100% EC ON with CCS LP Drum	58F Amb,	Case 03: 14F Amb, 2x100% EC OFF with CCS LP Drum Extraction	20F Amb.
Gas Flowrate (lb/hr)	4,375,115	4,269,000	4,305,133	4,479,781	4,283,214	4,238,141
CO ₂ Concentration (wt%)	5.97	5.92	5.96	5.98	6.15	6.21
H ₂ O Concentration (wt%)	6.80	6.57	7.02	5.30	4.95	4.90
CO ₂ Captured (ton/hr) at 95% Removal Efficiency	124.1	120.0	121.9	127.2	125.1	125.0

Design Heat and Mass Balance





Energy Advantage of UK CCS

- Reduction in reboiler duty due to:
 - Solvent: 27%
 - Process: 17%
 - Combined: 42%
- Expected reboiler duty of 1009 btu/lb (2.35 GJ/tonne)

		nple Tre Process	UK Process Intensified Process					
Solvent		CO ₂ Capture Process		JK	MEA			
Case Name	17	D.31	ME-d		MEA-M			
Case Name	17	0.51	D.31 IVIE-d		IVIEA-IVI			
Stream	FG	FG	F	G	6	ic.		
T (°F)	202.6	202.6		2.6	FG 202.6			
		15		2.0 L5	15			
P (psia)	15			15 805				
Mass Flowrate (Mlb/hr)	4305	4305			4305			
Y_H2O	0.11	0.11	0.11 0.04		0.11			
Y_CO2	0.04	0.04			0.04			
Y_N2	0.73	0.73	0.73		0.73			
Y_02	0.12	0.12	0.12		0.12			
Block	COL1	COL1	COL1		COL1			
T (°F)	104	86	8	86	86			
Stream	LEAN	LEAN	LEAN	LEAN2	LEAN	LEAN2		
T (°F)	104	95	95	95	95	95		
P (psia)	29	29	29	29	29	29		
	3484	6224	1012	4046	1442	29 5769		
Mass Flowrate (Mlb/hr) X H2O	0.86	0.85	0.85	4040 0.84	0.85	0.85		
X_1120 X CO2	0.02	0.83	0.85	0.84	0.83	0.85		
-		0.03	0.02	0.03				
X_Am	0.12				0.11	0.11		
C/N	0.14	0.31	0.20	0.27	0.31	0.34		
Stream	R5	R5	R5	R4	R5	R4		
T (°F)	244	240	194	234	194	240		
P (psia)	72.52	72.52	72.52	30.46	72.52	30.46		
Liq C/N	0.48	0.50	0.49	0.38	0.50	0.42		
Split %			38.4	61.6	47	53		
	1202	1755	10	009	1/	150		
SRD (Btu/lb)	1282	1755	10	109	1459			

Next Steps: Feed Study

- FEED submission
- Reviews and revisions
- Class 3 cost estimate
- Transportation and logistics
- Quantity takeoffs
- Schedule
- Construction plan/Story boards
- Engineering, procurement and construction implementation plan
- Vendor quotes
- Material requisitions/RFQ'S

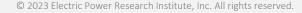
- Model Development (CAD)
- Layout
- Equipment lists
- Equipment designs/Selection
- Piping and Instrumentation Diagrams (P&ID's)
- HazOp
- Revised P&ID's
- Uncertainties Log
- Risk register
- Management control and reports

Community Benefits and Societal Impacts

- Planned evaluation of community impacts:
 - Environmental co-benefits of CO₂ capture
 - Workforce development and jobs creation
 - Economic impact
 - Development of community engagement strategy
- Societal Impacts
 - Accelerating decarbonization through de-risking CCS
 - All information to be made public except confidential vendor information
 - Potential for lowering energy and capital costs of CO₂ capture

Lessons Learned

- Design philosophy of reliability and operability has increasing importance for real-world deployment
- Increasing backpressure on gas turbine possible mechanism to eliminate FD fan
 - Requires collaboration between GT supplier, HRSG, and carbon capture
- Optimization of steam extraction point from NGCC requires full HRSG and steam turbine models
 - Modification possible, but important to bring in OEMs to understand repercussions from performance and service agreements



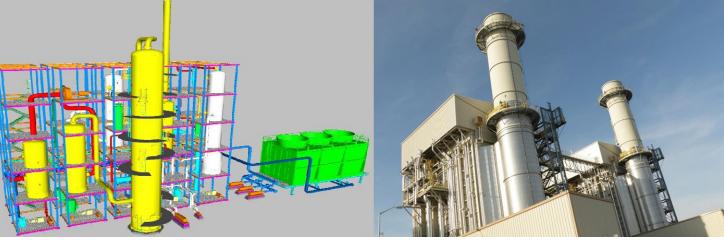
The FEED study will guide CCS scale up

- Evaluate the impact of the carbon capture process on:
 - Power delivery and cost for full scale deployment
 - The operation and possible modifications to the HRSG and steam turbine.
- Land and Permit Requirements
 - This includes the CCS system layout and long-term planning for possible future NGCC units at the site.
- Evaluation of Local Storge and Pipeline Options
- The FEED learnings combined with planned 20 MW demonstration capture unit will inform CCS at Cane Run Unit 7



Summary

- FEED study for retrofitting the LG&E (a PPL Corporation Facility) Cane Run Unit 7, a 640 MW NGCC located in Louisville KY, with the University of Kentucky's solvent-based carbon capture system for 95% CO₂ capture
- Pre-FEED nearly complete with promising performance estimates
- All results to be made public other than confidential vendor information



Source UK

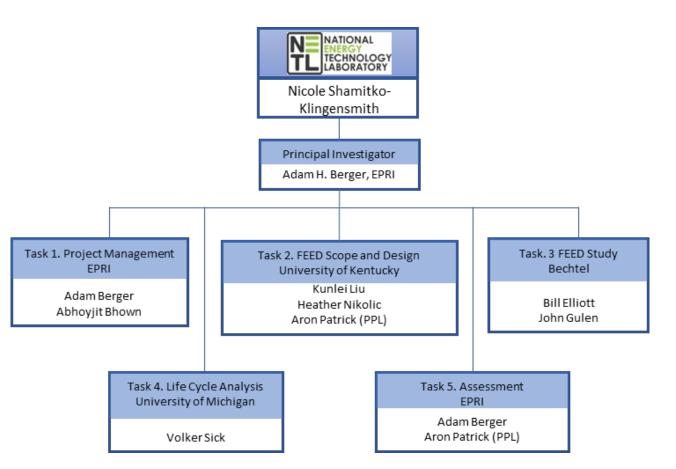




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Overall Task List and Org Chart

- Task 1: Project Management and Planning
- Task 2: Preliminary-Front-End Engineering Design (Pre-FEED)
- Task 3: FEED Package
- Task 4: Life Cycle Assessment
- Task 5: Commercial, Environmental, and Economic Assessments



Gantt Chart (12/22/2022 – 6/30/2024)

Fask	list and sch	nedule		20	23		20	024	Project	month
	Lead Orga	anization	Q1	Q2	Q3	Q4	Q5	Q6	Start	Finish
1	EPRI	Project Management and Planning			1				1	. 18
1.1	EPRI	Project Management and Planning							1	. 18
1.2	UKy	Technology Maturation Plan							2	2 15
1.3	EPRI	Workforce Readiness Plan							12	2 12
2	Uky	FEED Scope and Design							1	. (
2.1	UKy	FEED Scope		2					1	
2.2	UKy	CCS Design Basis							1	
2.3	UKy	Initial Design							1	. (
2.4	UKy	CO2 Transportation and Long Duration Storage			2				4	L (
2.5	UKy	Environmental Health and Safety					\mathbf{Z}		14	1
3	Bechtel	FEED Study							1	. 1
3.1	Bechtel	Initial Design Support	777						1	-
3.2	Bechtel	Process Engineering Design Package Review		777	2				3	6
		Initial Electrical, Automation Systems, Utilities,			_					
3.3	Bechtel	and Other Engineering Design Package							7	,
3.4	Bechtel	Layout Design Package							9) 1
		Final Electrical, Automation Systems, Utilities, and								
		Other Engineering Design Package and Material								
3.5	Bechtel	Take-Off of Main Components Design Package							11	. 1
3.6	Bechtel	Site Security & Logistics							12	2 1
		Basic Contracting/Purchasing Strategy, HAZOP,								
3.7	Bechtel	and Constructability Review							13	1
3.8	Bechtel	Cost Estimating Design Package							14	- 1
3.9	Bechtel	Close-Out							16	5 1
4	U Mich	Life-Cycle Assessment								
4.1	U Mich	Preliminary LCA							4	
4.2	U Mich	Final LCA							14	1
5	EPRI	Assessment							14	1
5.1	EPRI	Techno-Economic Analysis							14	1
5.2	EPRI	Environemntal Justice Analysis							15	5 1
5.3	EPRI	Economic Revitalization and Job Creation							14	1
5.4	EPRI	Business Case Analysis							15	5 1