

Integrated Process for Direct Air Capture through Reactive Crystallization and Electrochemical Conversion to Ethanol

TCF-20-20118

Radu Custelcean
Oak Ridge National Laboratory

2023 Carbon Management Research Project Review Meeting
August 28 – September 1, 2023

Project Overview

ORNL Team (DAC)



Radu Custelcean
Lead PI
Organic chemist



Costas Tsouris
Co-PI
Chemical engineer



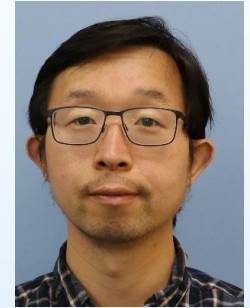
Kashif Nawaz
Co-PI
Mechanical engineer



Gyoung Jang
R&D associate
Chemical engineer



Diana Stamberga
Technical associate
Organic chemist



Kai Li
R&D associate
Materials/manufacturing

ReactWell (CO₂ conversion)



Brandon Iglesias
Chemical engineer

Project Timeline

Jan 1, 2021 – Jan 1, 2024

Project budget

\$1.5 mil/3 years (DOE: OTT/FECM)

\$1.5 mil in-kind match-up (ReactWell)



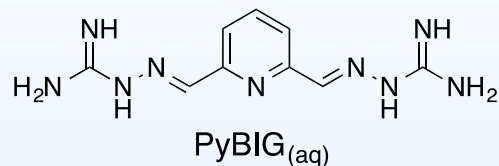
Abishek Kasturi
Grad student
Georgia Tech

Project Objectives

- Develop an energy-efficient, cost-effective, **net-zero emission** technology that closes the carbon cycle by combining **DAC** with electrochemical **conversion of CO₂ into ethanol**
- **DAC: reactive crystallization** of aq. amino acid + guanidines - **ORNL**
- **Electrochemical conversion** of captured **CO₂ into ethanol** using copper nanoparticles/carbon nanospine electrode - **Reactwell**
- **Commercialize the ethanol** as hand sanitizer, spirits, fuel - **Reactwell**
- Long-term goal: mature and scale up a standalone **DAC** technology for deployment at the much larger scale of MtCO₂/year + **geological storage** towards **NET** status (with **Holocene**)

Technology Background

Fundamental science (BES)



release

TGA
80-120 °C
- CO₂
- 5 H₂O

DSC
 $\Delta H = 223 \text{ kJ/mol}$
(H₂O: 148 kJ/mol)

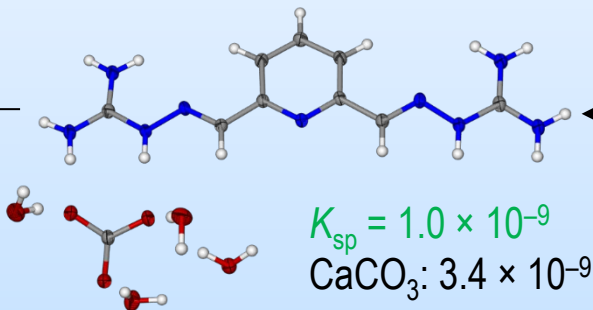
Benchmark

CaCO₃ requires 900 °C for CO₂ release

absorption

CO₂ (air)

$K = 10^5 \text{ atm}^{-1}$
 $\Delta H = -71 \text{ kJ/mol}$



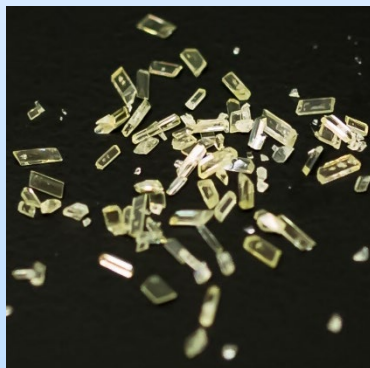
$K_{sp} = 1.0 \times 10^{-9}$
CaCO₃: 3.4×10^{-9}

Advantages

- Reactive crystallization and low solubility of BIG-CO₃ drive CO₂ removal from air
- Low regeneration T
- Low grade heat

Challenges

- Slow kinetics of CO₂ abs
- Low BIG solubility/alkalinity
- Small air-liquid contact area



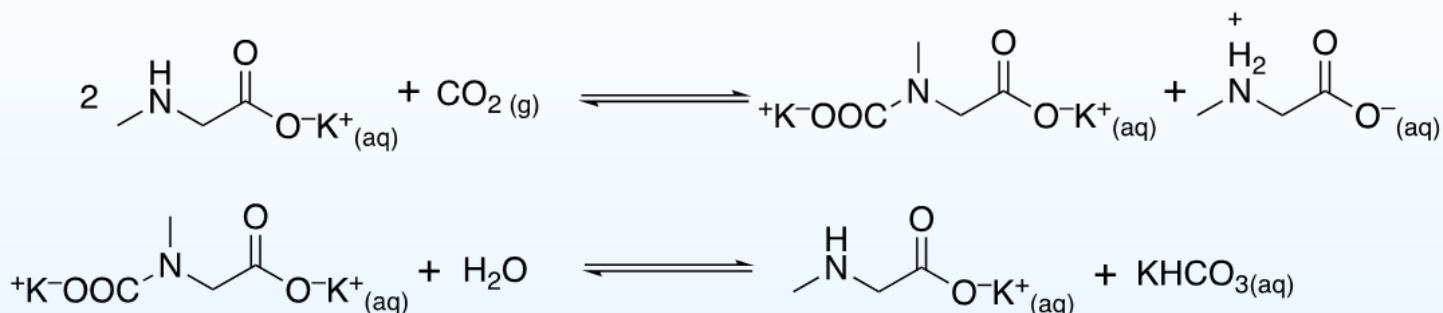
Angew. Chem. Int. Ed. **2017**, *56*, 1042

ChemSusChem **2020**, *13*, 6381

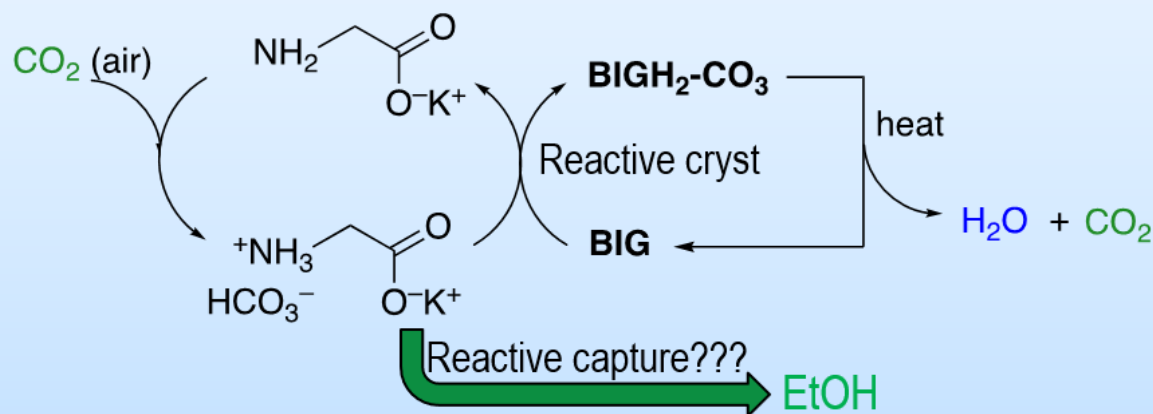
Chem. Sci. **2021**, *12*, 12518

Technology Background

Faster DAC with aq. Amino Acids



DAC with aq. Amino Acid + BIG

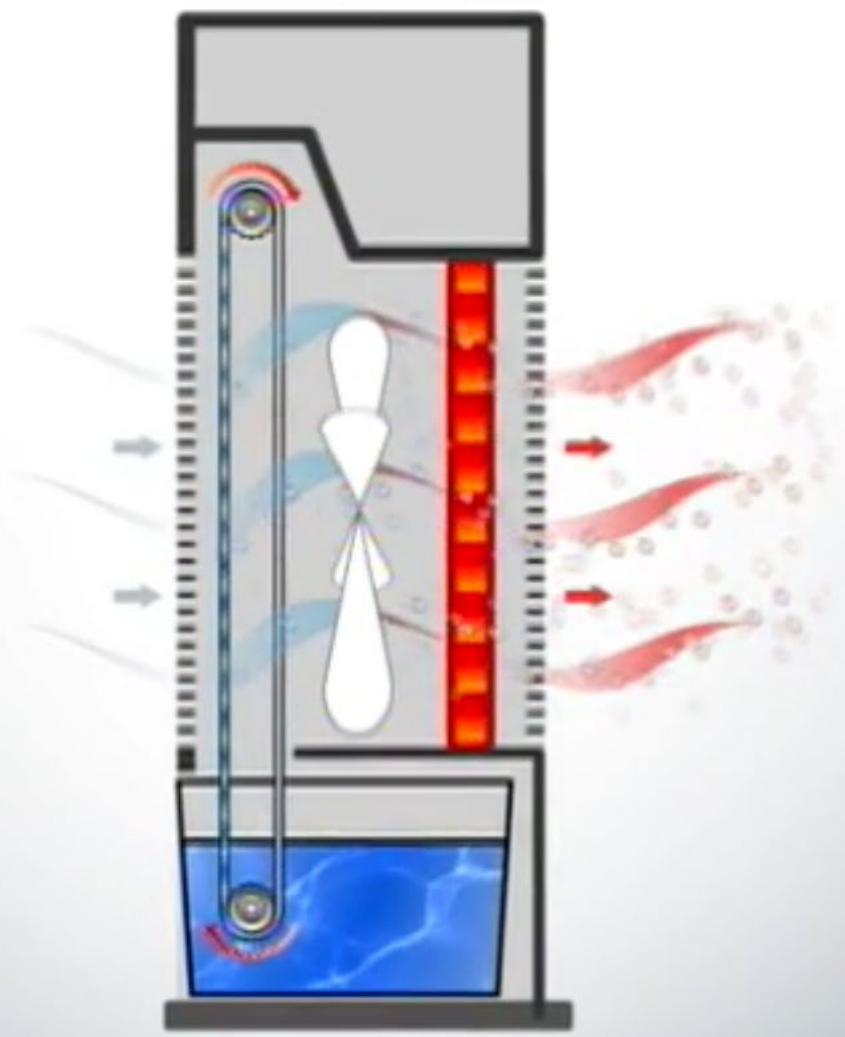


Advantages

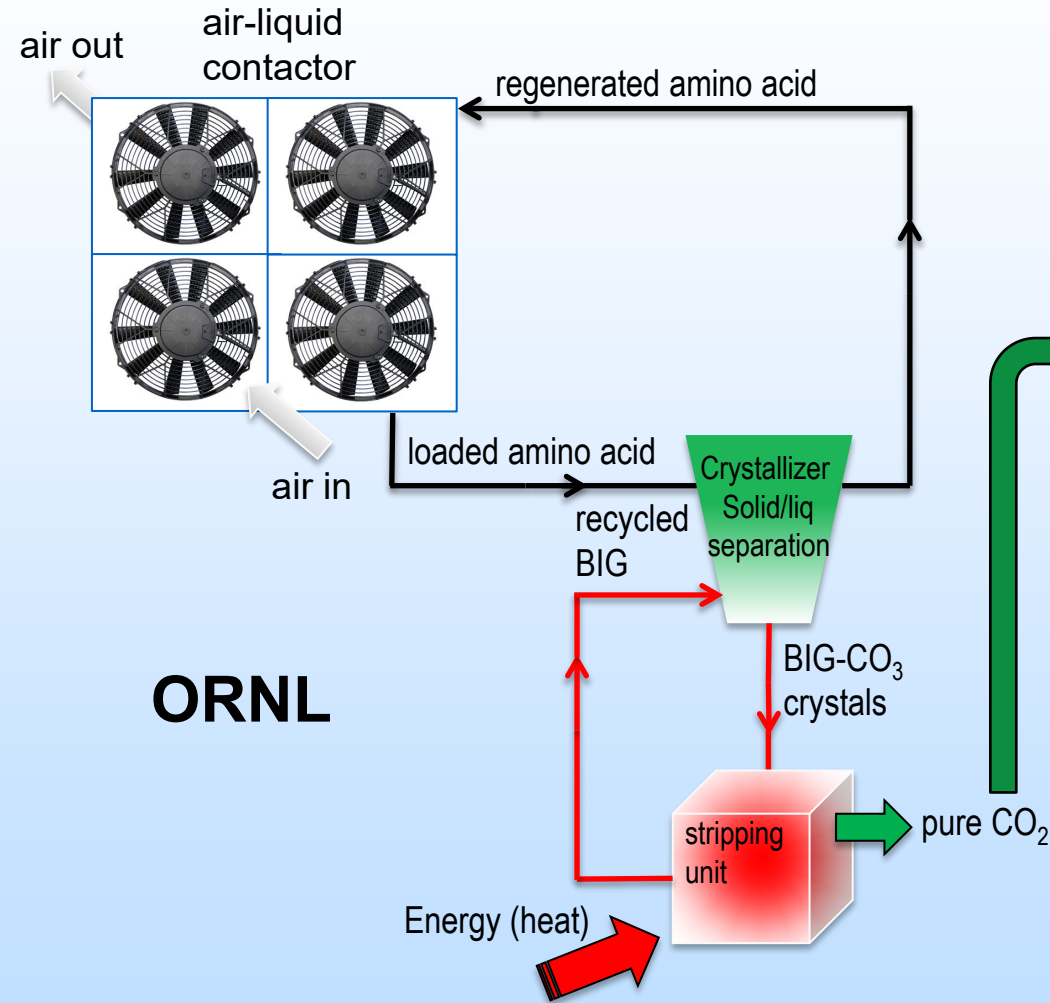
- fast CO_2 absorption rates
 $54 \mu\text{mol}/\text{m}^2/\text{s}$ for SAR 1 M, 25°C
 vs $30 \mu\text{mol}/\text{m}^2/\text{s}$ for NaOH
- negligible volatility & toxicity

Outstanding challenges

- minimize regeneration energy
- minimize degradation
- improve CO_2 mass transfer (higher air/liquid contact area)

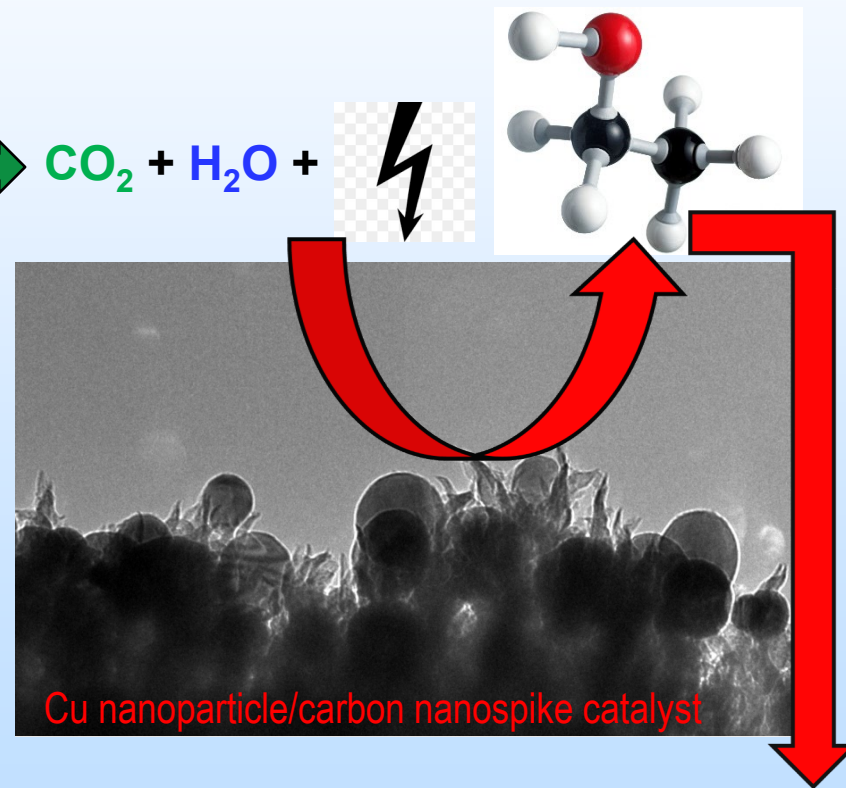


Technical Approach/Project Scope



ORNL

ReactWell



Carbon-neutral ethanol

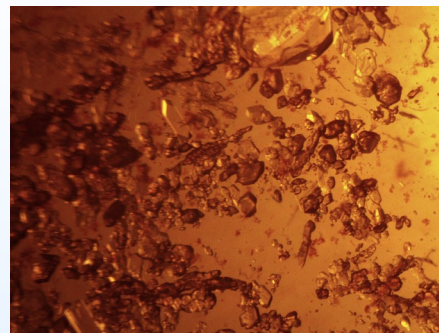
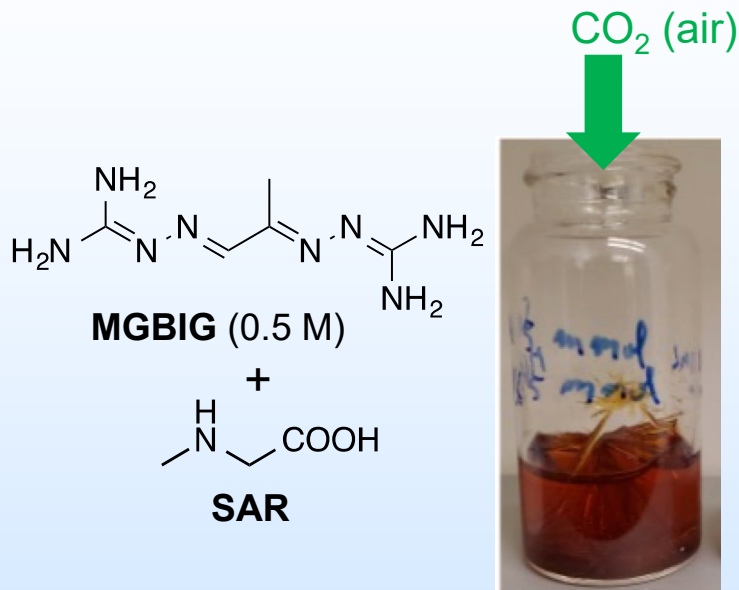
- Spirits (aka vodka)
- Hand sanitizer
- Fuel

Technical Approach/Project Scope

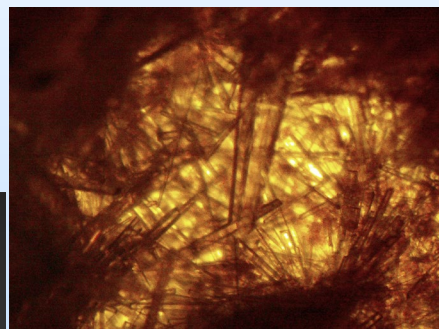
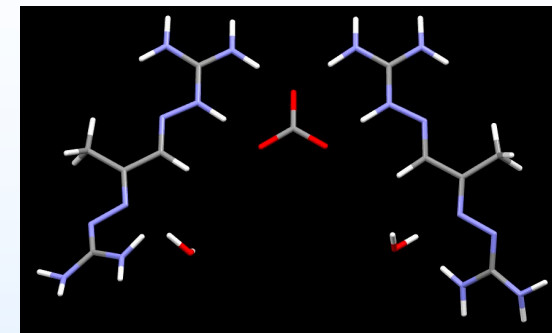
- **Optimization of DAC chemistry:** identify optimal amino acid/BIG
- **Design, build & test air-liquid contactor:** compatible with solids
- **Optimize BIG sorbent regeneration:** minimize time and energy
- **Process engineering & intensification:** combine CO₂ absorption and BIG-CO₃ crystallization into a single three-phase process
- **TEA and LCA:** evaluate the cost, energy & water consumption, carbon footprint (carbon neutral? carbon negative?)

Progress and Current Status

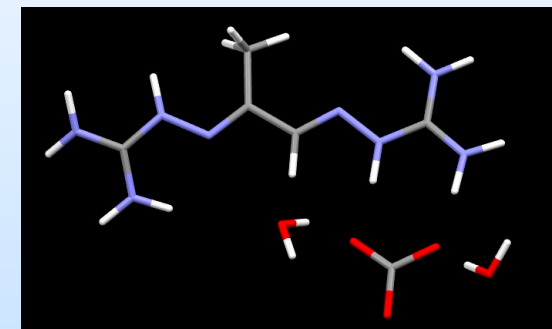
DAC Chemistry Optimization



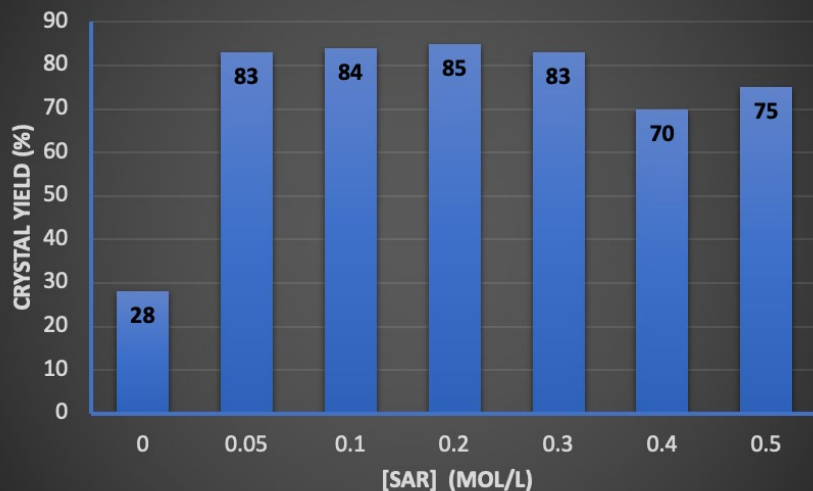
(MGBIGH⁺)₂(CO₃)(H₂O)₂ (**P1**) favored at [MGBIG] > 0.75 M



(MGBIGH₂²⁺)(CO₃)(H₂O)₂ (**P3**) favored at [MGBIG] < 0.3 M



MGBIG + SAR DAC



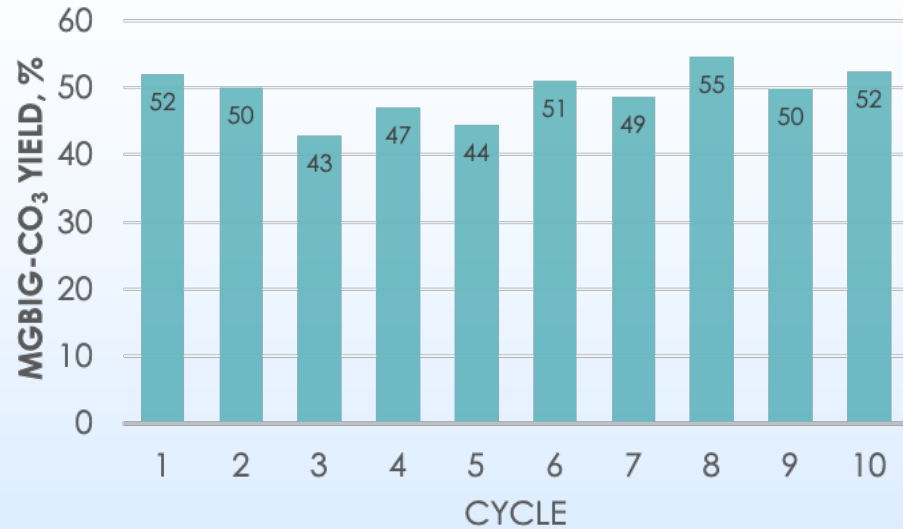
Amino acid advantages:

- No additional base (KOH) needed
- Addition of SAR favors P3 over P1

Intensified DAC process:

- Combine CO₂ capture + MGBIG-CO₃ crystallization
- Need an air-liquid contactor that tolerates solids
- Scale up 100X to 1 L and beyond

Intensified DAC with MGBIG/SAR



Average results for 10 cycles

Crystallization yield: $51\% \pm 10\%$

Phase 3 (mol%): 91 ± 13

Cyclic capacity (mol CO₂/L): 0.23 ± 0.02

CO₂ removed from air (g CO₂/day): 10 ± 1

MGBIG loss: 0% /cycle

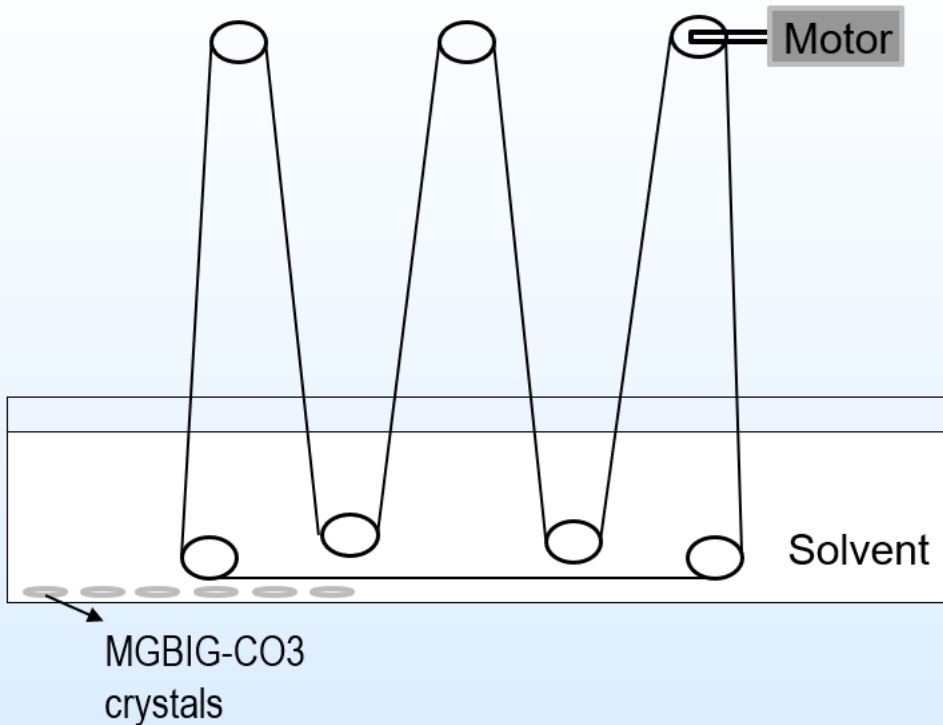
SAR loss: 1.5% /cycle

1 L scale, MGBIG (0.5 M) + SAR (0.3 M)

Run for 24 h

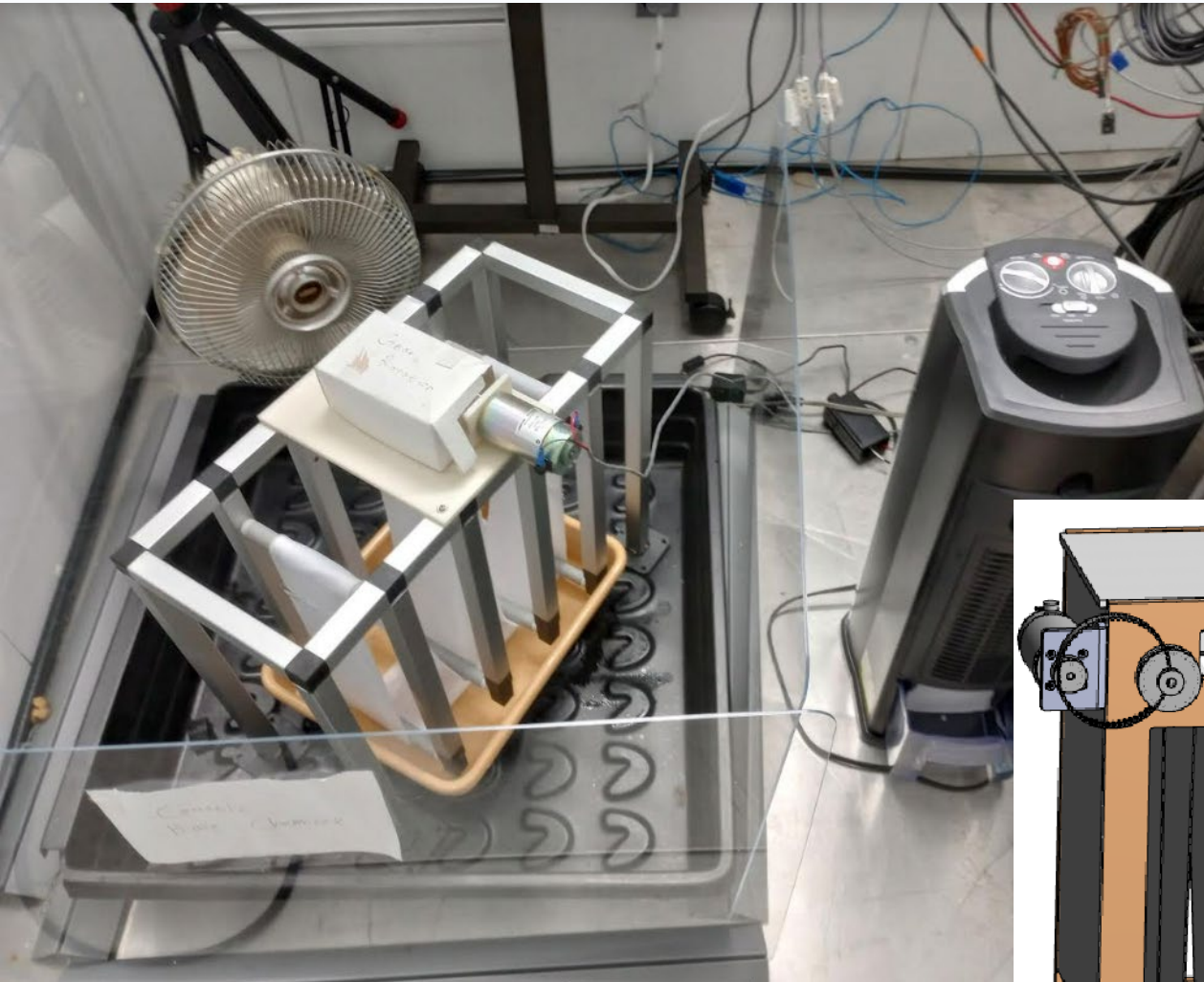
Air-Liquid DAC Contactor Design

Rotating Air Contactor (RAC) Design



Air-Liquid DAC Contactor Design

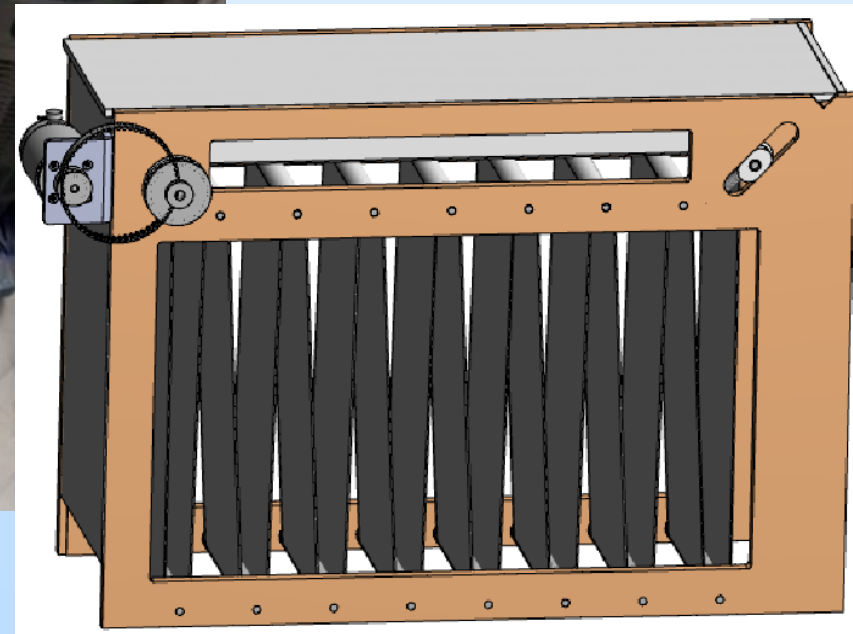
Rotating Air Contactor (RAC) Design



Humidifier
SA = 0.2 m²

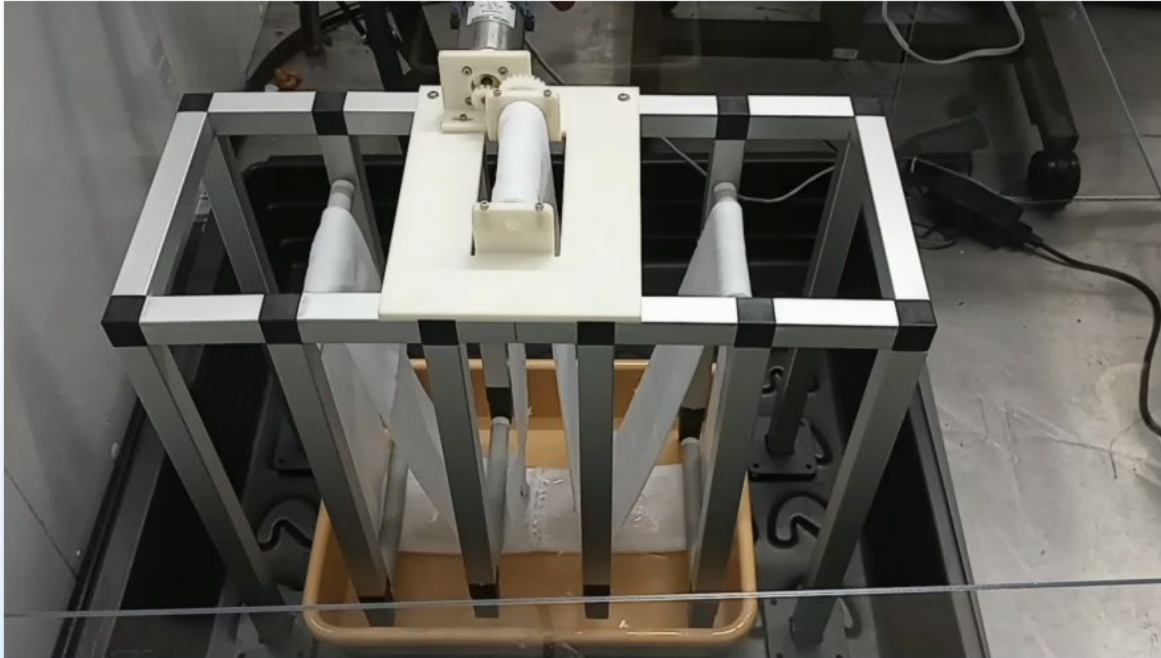
1st gen RAC
SA = 0.5 m²

2nd gen RAC
SA = 2 m²

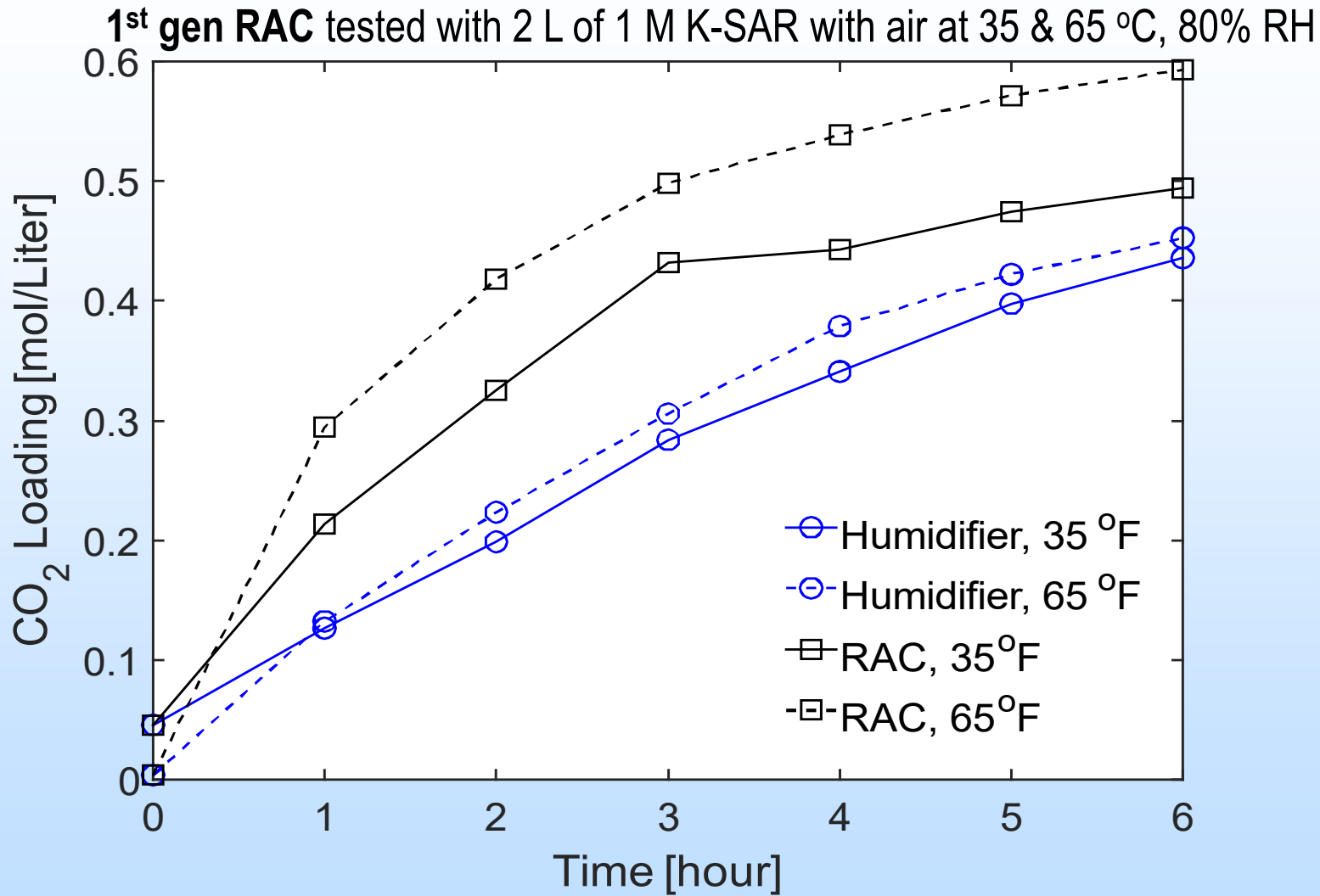


Air-Liquid DAC Contactor Testing

1st gen RAC tested with 2 L of 1 M K-SAR with air at 35 & 65 °C, 80% RH

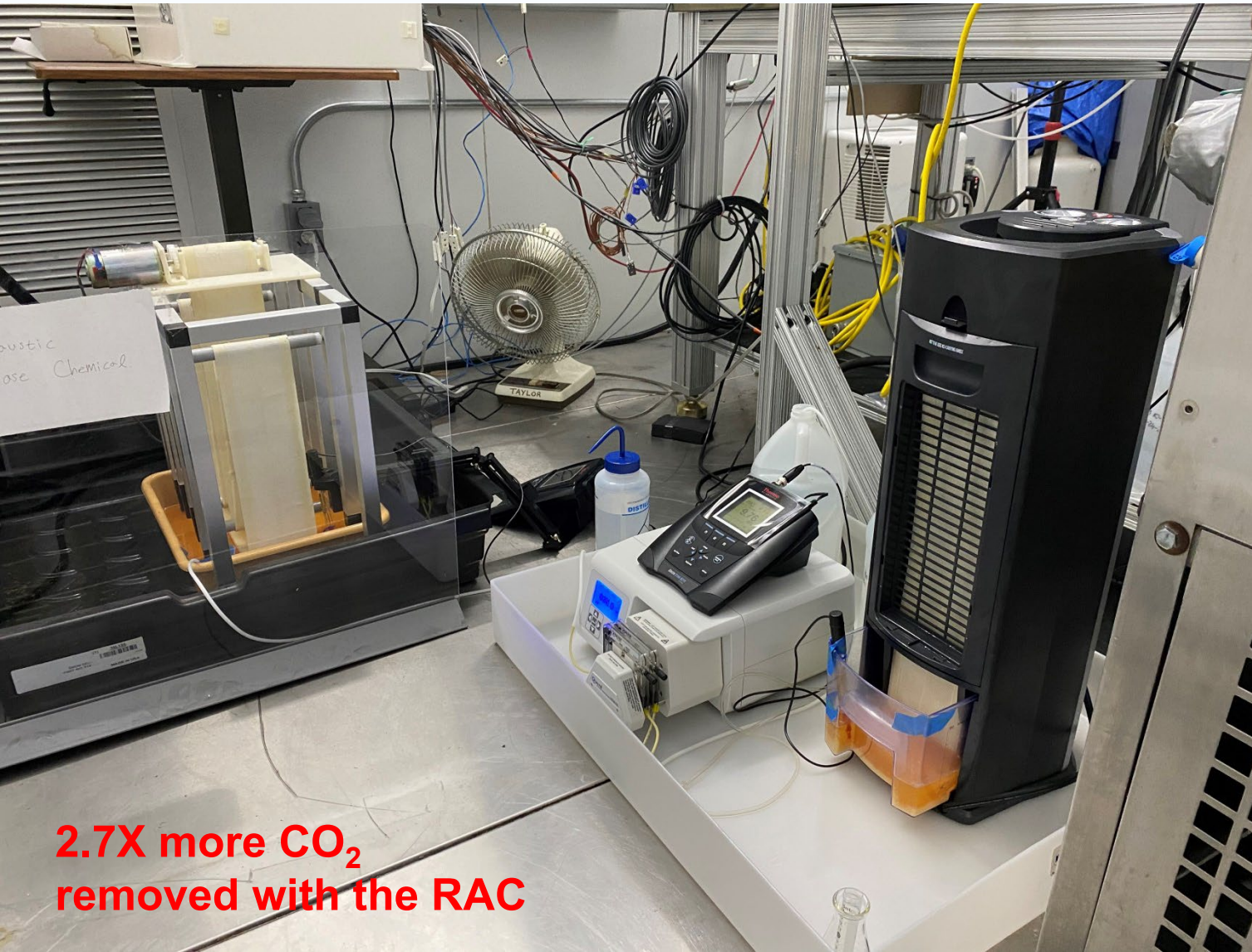


Air-Liquid DAC Contactor Testing



Air-Liquid DAC Contactor Testing

1st gen RAC tested with 2 L SAR (0.3 M) + MGBIG (0.5 M) with air at 25 °C, 70% RH, 24 h



**2.7X more CO₂
removed with the RAC**

RAC

- 2 L solvent
- SA 0.5 m²
- Cryst. yield: 62%
- Isolated MGBIG-CO₃: 120.6 g (89%)
- P3: 99.5%
- **CO₂ removed: 22 g**

vs

Humidifier

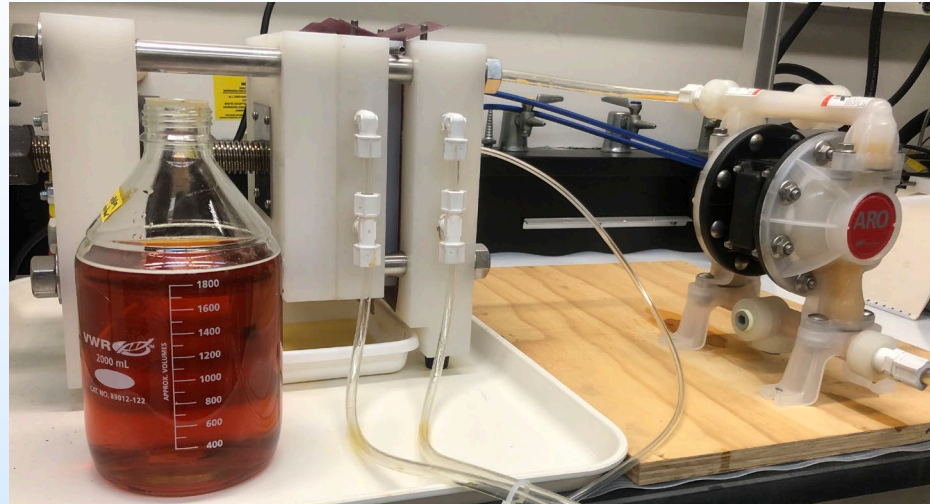
- 1 L solvent
- SA 0.2 m²
- Cryst. yield: 60%
- Isolated MGBIG-CO₃: 43.1 g (95%)
- P3: 99.1%
- **CO₂ removed: 8.3 g**

Solid (MGBIG-CO₃)/Liquid (SAR) Separation

Filter press setup



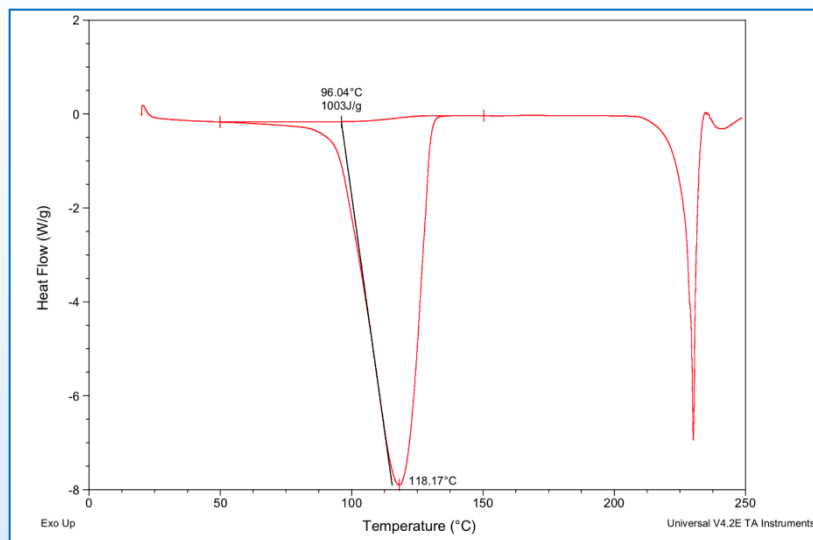
Recovered solvent at the end of separation



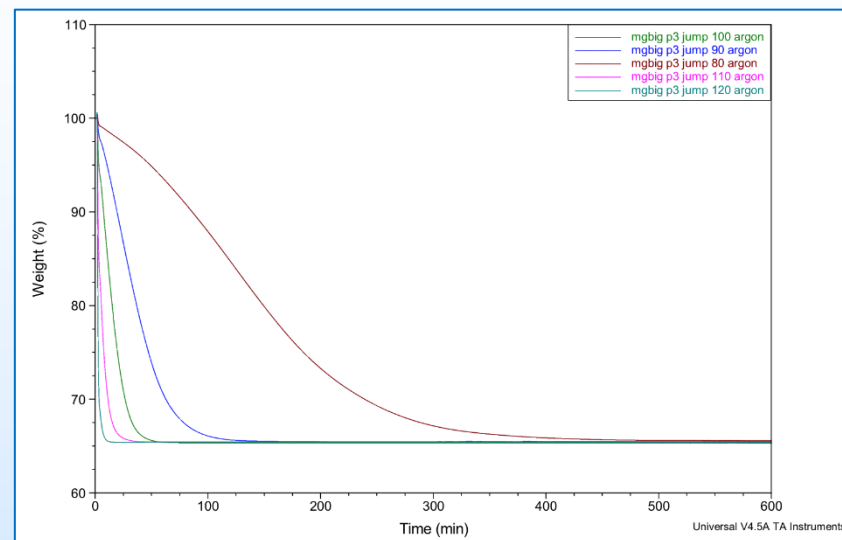
Recovered BIG-CO₃ cake



CO₂ Release – Thermodynamics & Kinetics



DSC



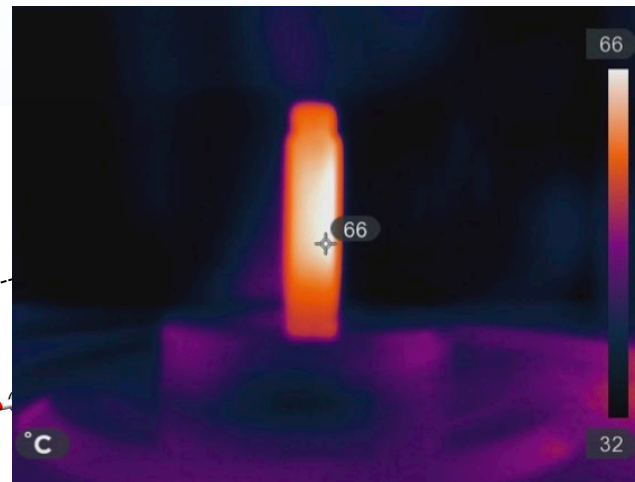
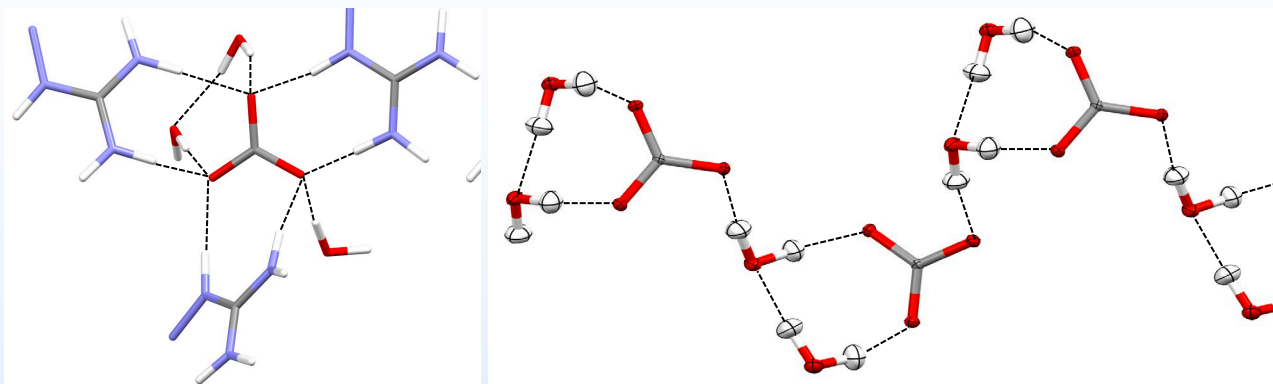
Isothermal TGA (80, 90, 100, 110, 120 °C)

E (kJ/mol CO ₂)	MGBIG P1	MGBIG P3
Reaction enthalpy	288	284
Sensible heat	70	39
Regeneration energy	358	323

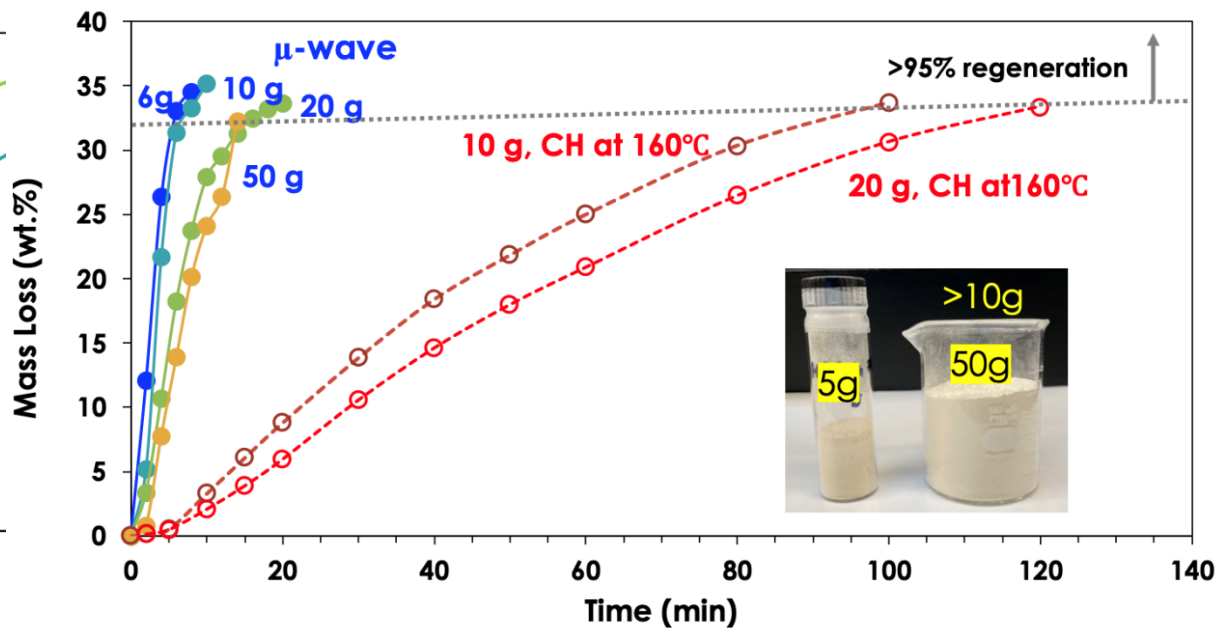
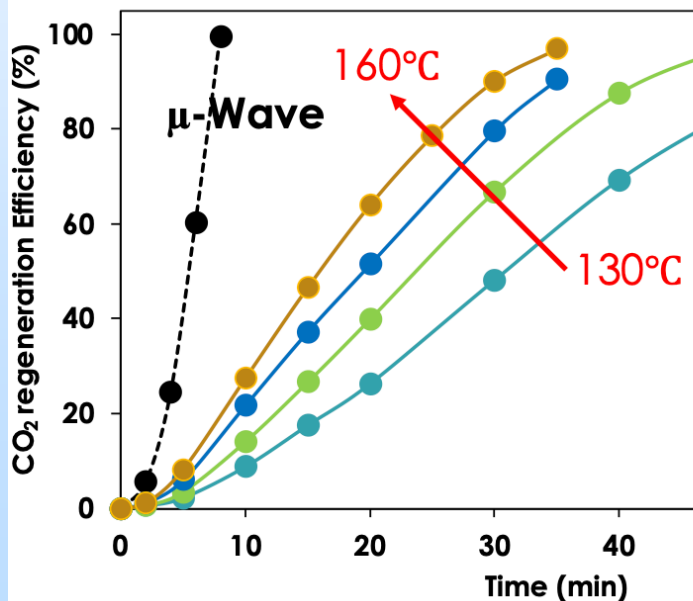
Crystal dehydration costs a lot of energy

MGBIG Regeneration – Microwaves

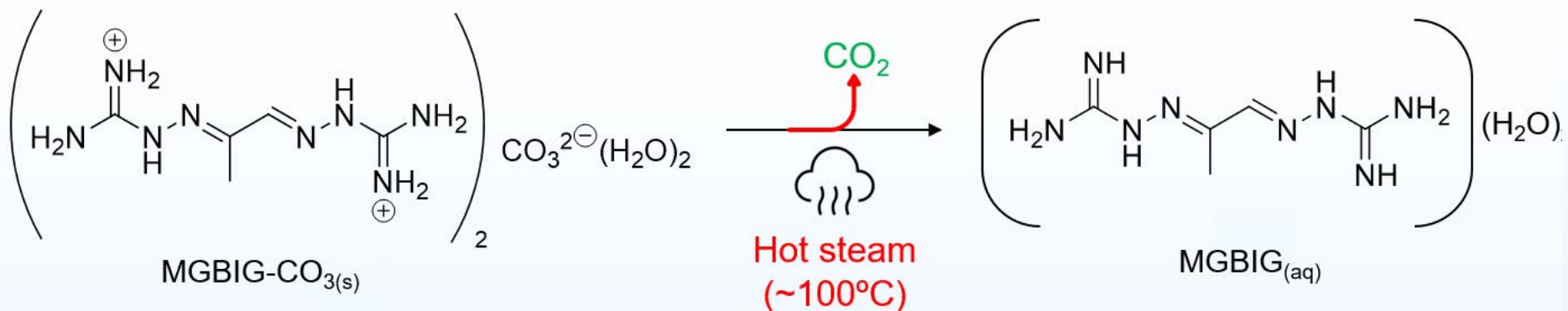
(MGBIGH₂²⁺)(CO₃)(H₂O)₂ (P3) crystal structure:
Water bound to carbonate



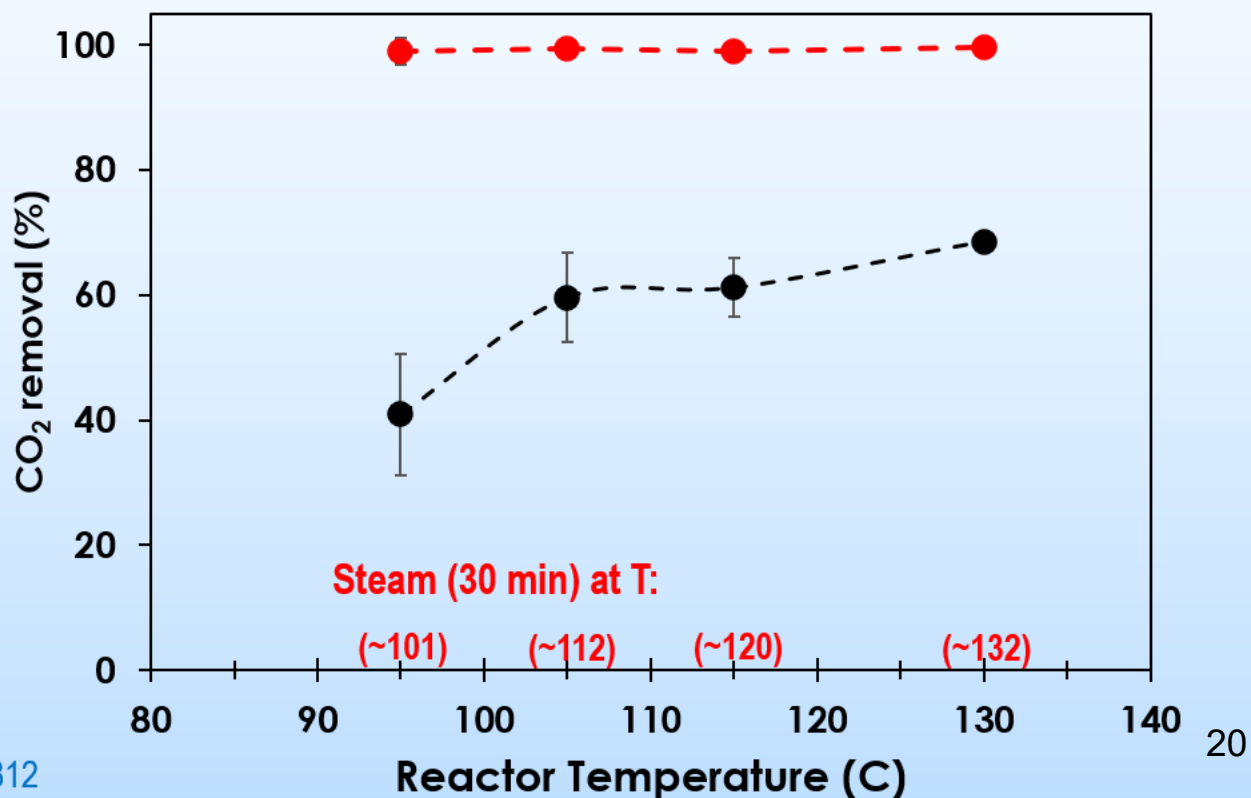
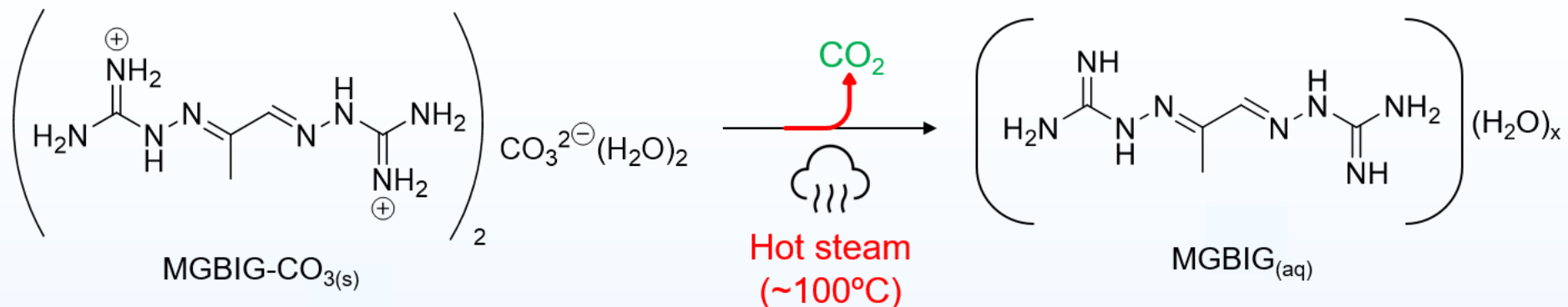
Kinetics of MGBIG regeneration: convection vs μ -wave heating (2.54 GHz, 1250 W)



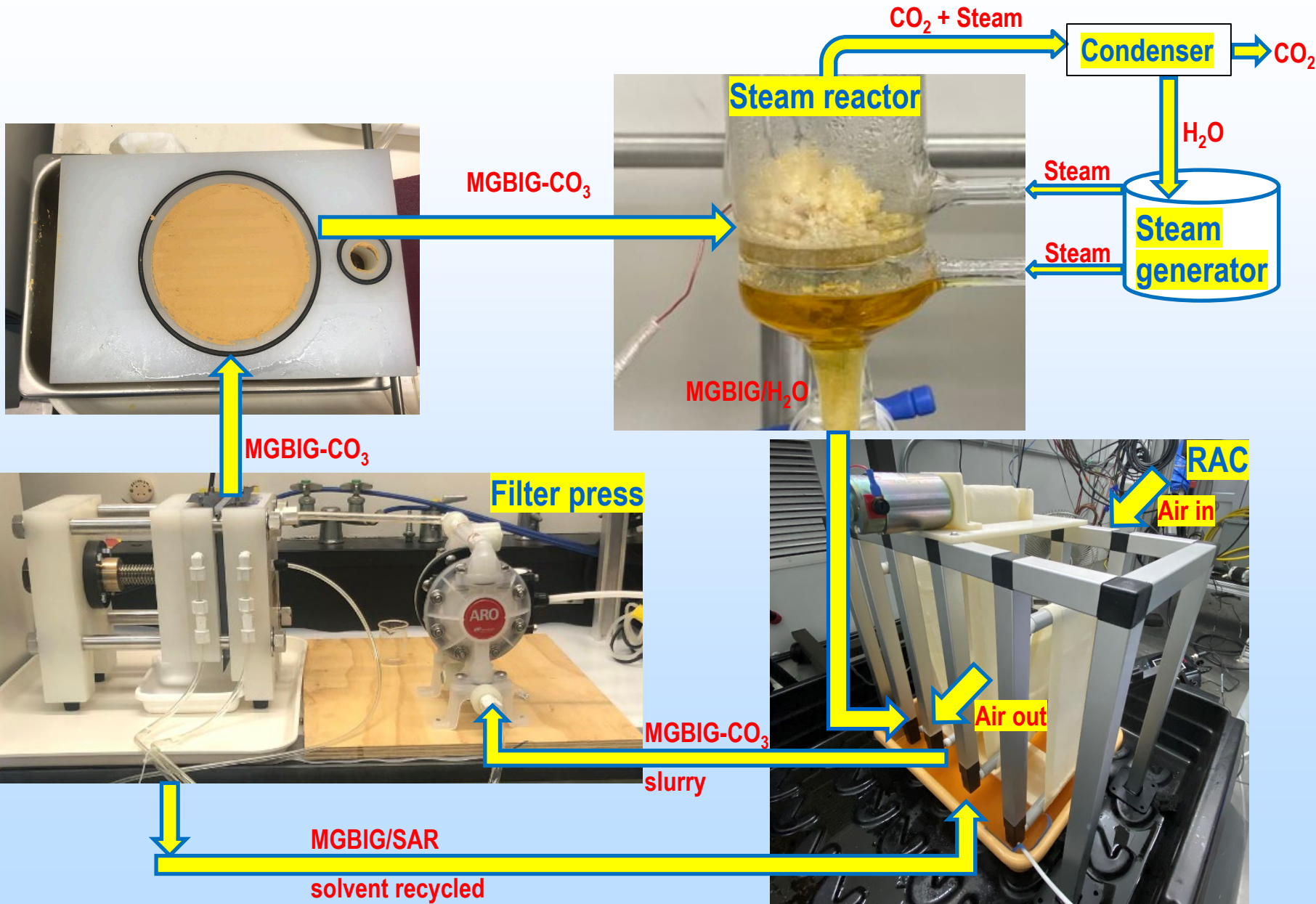
MGBIG Regeneration – Steam



MGBIG Regeneration – Steam



Summary: DAC Process



Lessons learned

- Reactive capture only makes sense if the conditions for CO₂ conversion are compatible with those for solvent regeneration
- Standalone DAC process may have some advantages over a continuous, integrated (capture + conversion) process:
 - 1) Potential for NET
 - 2) Scaleup of DAC independent of conversion
 - 3) CO₂ stored temporarily as BIG-CO₃, transported and released on demand for conversion

Plans for future testing/development/ commercialization

In this project

- Complete bench-scale DAC process and demonstrate multiple cycles at 100 g CO₂/day
- TEA and LCA
- Send MGBIG-CO₃ batches to **Reactwell** for on-demand CO₂ release & **conversion to EtOH for commercialization**

After this project

- Collaborate with **Holocene** on further developing a **scalable, commercial DAC technology for CO₂ removal and storage**

Project Output

Publications

1. Kasturi, A. et al., Determination of the Regeneration Energy of Direct Air Capture Solvents/Sorbents Using Calorimetric Methods, *Separation and Purification Technology* **2023**, 310, 123154.
2. Jang, G. G. et al., Ultra-fast Microwave Regeneration of CO₂ Solid Sorbents for Energy-Efficient Direct Air Capture, *Separation and Purification Technology* **2023**, 309, 123053.

Patent applications

1. Gyoung Jang et al., *Microwave Regeneration of Carbon Dioxide Sorbents* **2023**, Application no. 18/235,081; Patent ID 81944506.
2. Gyoung Jang et al., *Methods of Energy Efficient Sorbent Regeneration Used for Direct Air Capture* **2023**, Application no. 63/534,893; Patent ID 81947812.
3. Keju An et al., *Direct Air Capture of CO₂ using RAC (Rotating Air Contactor)* **2023**, Application no. 63/535,383; Patent ID 81948020.

Awards

2021 R&D100 Award for BIG NET: ORNL + Holocene + Reactwell