

High Efficiency Electrochemical Conversion of CO_2 to C_2H_4

Xiao-Dong Zhou

Director: Center for Clean Energy Engineering
Connecticut Clean Energy Fund professor in Sustainable Energy
The Nicholas E. Madonna Chair in Sustainability
University of Connecticut, Storrs, CT 06269
Email: xiao-dong.zhou@uconn.edu

University of Louisiana at Lafayette, Lafayette, LA 70504

Jingjie Wu

Department of Chemical Engineering
University of Cincinnati
Cincinnati, OH 45221; Email: wu2jj@ucmail.uc.edu

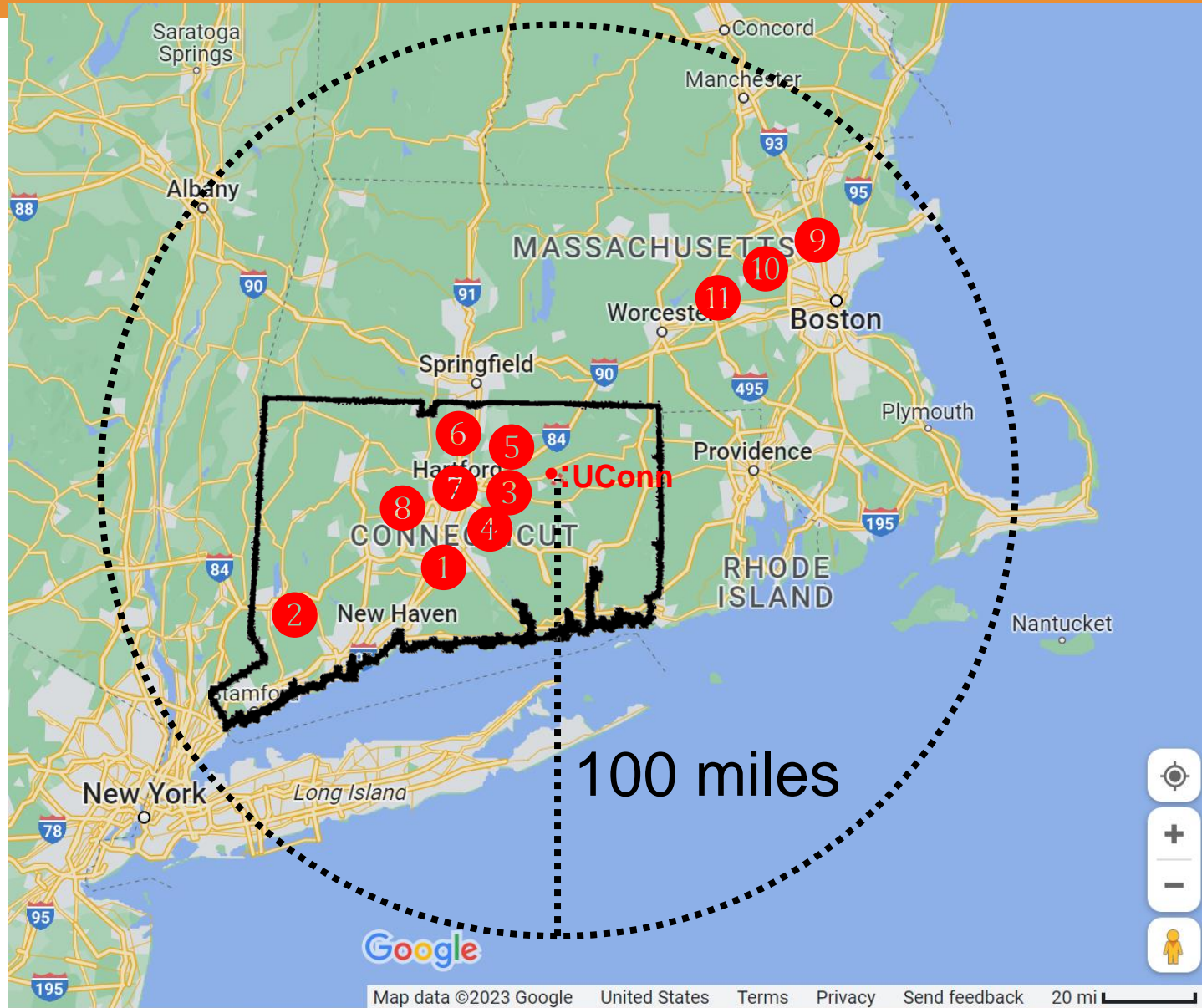


<https://www.visitpittsburgh.com/>

Project Managers
Dr. Naomi O'Neil and Ms. Erika Coffey

DE-FE0031919
August 28, 2023

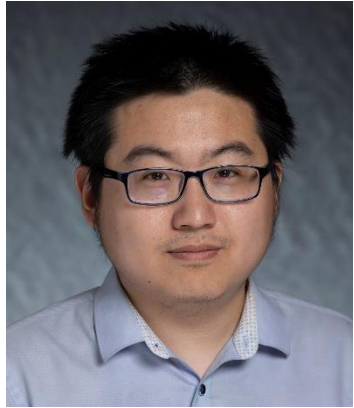
UConn – Carbon Neutrality by 2030



- ①: Nel Hydrogen
- ②: FuelCell Energy
- ③: Raytheon Technology Research Center
- ④: Pratt & Whitney
- ⑤: Connecticut Center for Advanced Tech
- ⑥: Infinity Fuel Cell & Hydrogen
- ⑦: Doosan Fuel Cell (HyAxiom)
- ⑧: Connecticut Green Bank
- ⑨: Envision Energy
- ⑩: Plug Power Electrolyzers
- ⑪: Giner Inc



Team Members – Electrochemical Transformation



Dr. Yudong Wang
Asst Res Prof



Dr. Nengneng Xu
Asst Res Prof



Dr. Dave Daggett
Adjunct Prof



Dr. Zizhou He
Postdoc Fellow



Stoyan Bliznakov
Assoc Res Prof



Leonard Bonville
Research Scientist



Wilson Chiu
Professor, Mech Eng



Dr. Atif Niaz
Postdoc Fellow



LuLu Li
Graduate Student



Gang Yang
Graduate Student



Azeem Sarwar
Graduate Student



Christabel Adjah-Tetteh
Graduate Student



Scott Blazer
Graduate Student

Outline

1. Technical and Scientific Background

Catalysts of CO₂ reduction, C-C coupling pathway

2. Factors for an electrodes to promote the formation of C₂H₄

3. Tandem Electrodes

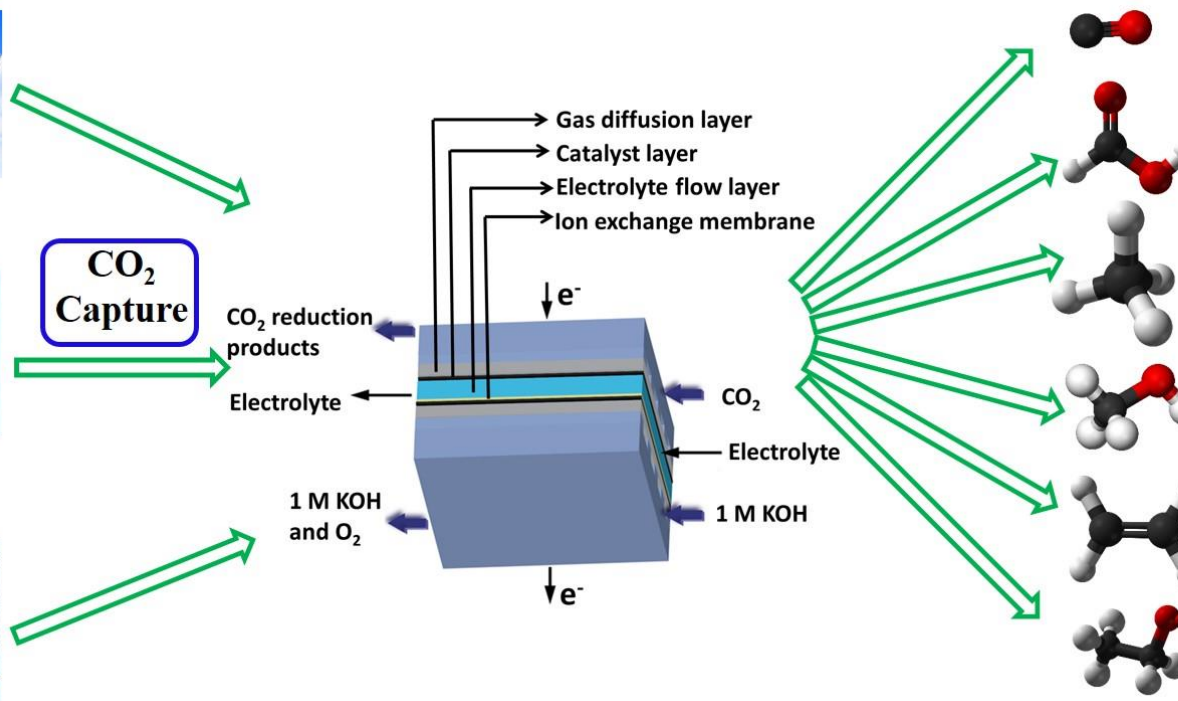
4. Pulsed Electrolysis



Electro-conversion of CO₂ to Chemicals: Electrocatalysts

Renewable electricity

CO₂ electrolyzer



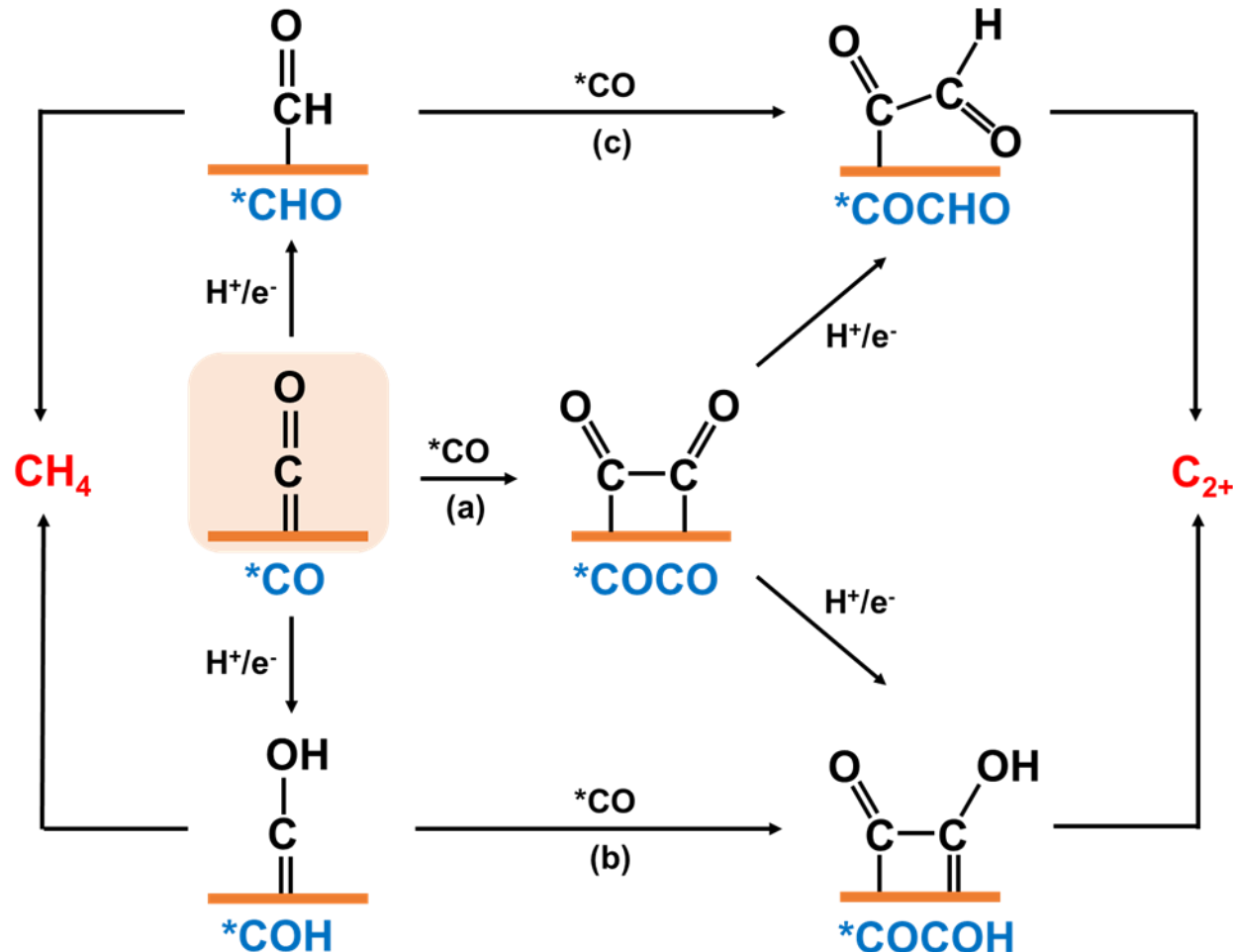
	State-of-art catalyst	Estimated market price (USD kg ⁻¹)	Estimated market size (Billion USD)
CO	Ag, Au, Zn, NCNTs, M-N-C	~1.20	2.7 - 3.2
HCOOH	Sn, Pb, In	0.40 - 0.90	0.62
CH ₄	Cu	< 0.08	4.30
CH ₃ OH	Cu oxide	0.39 ~ 0.43	54
C ₂ H ₄	Cu, NGQDs	0.80 - 1.10	155 - 248
C ₂ H ₅ OH	Cu, BN-nanodiamond	~0.52	110

- Modular processes that can be **easily coupled with renewable electricity**.
- Ease to **scale-up to MW or GW plants**.

Electrode Development

Electro-conversion of CO₂ to Chemicals: CO as a Key Intermediate for C₂₊ Products

Plausible C-C coupling pathways



- C-C coupling has various pathways, all of which involves CO.
- *CO has been identified a key intermediate for C₂₊ products formation.
- Increasing the *CO surface coverage enhances the C-C coupling kinetics according to the law of mass action.

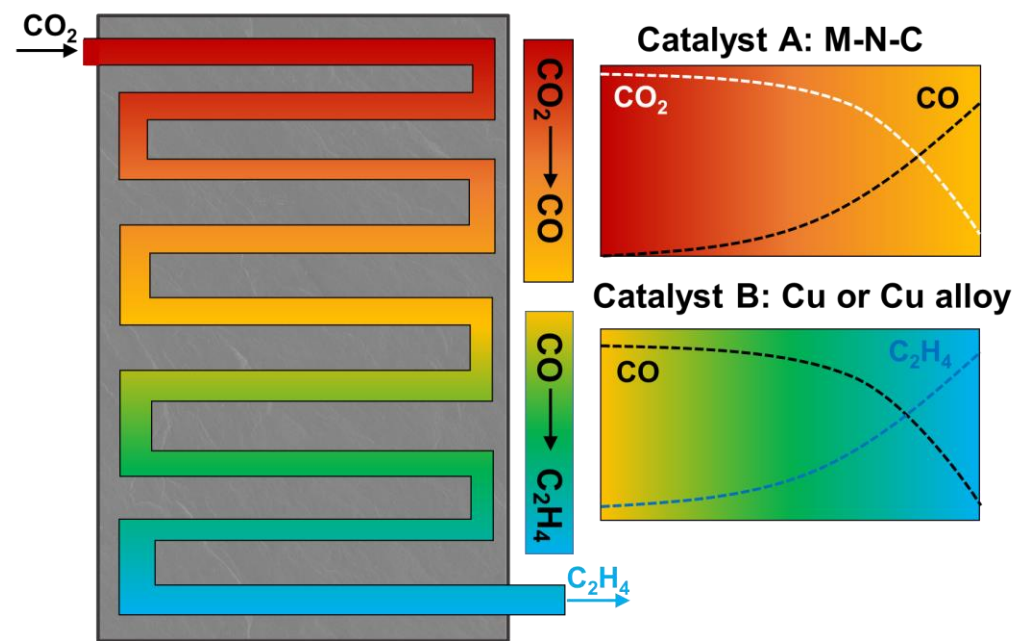
Zhao, Martirez, and Carter, PNAS, 2022

Garza, Bell, and Head-Gordon, ACS Catalysis, 2018

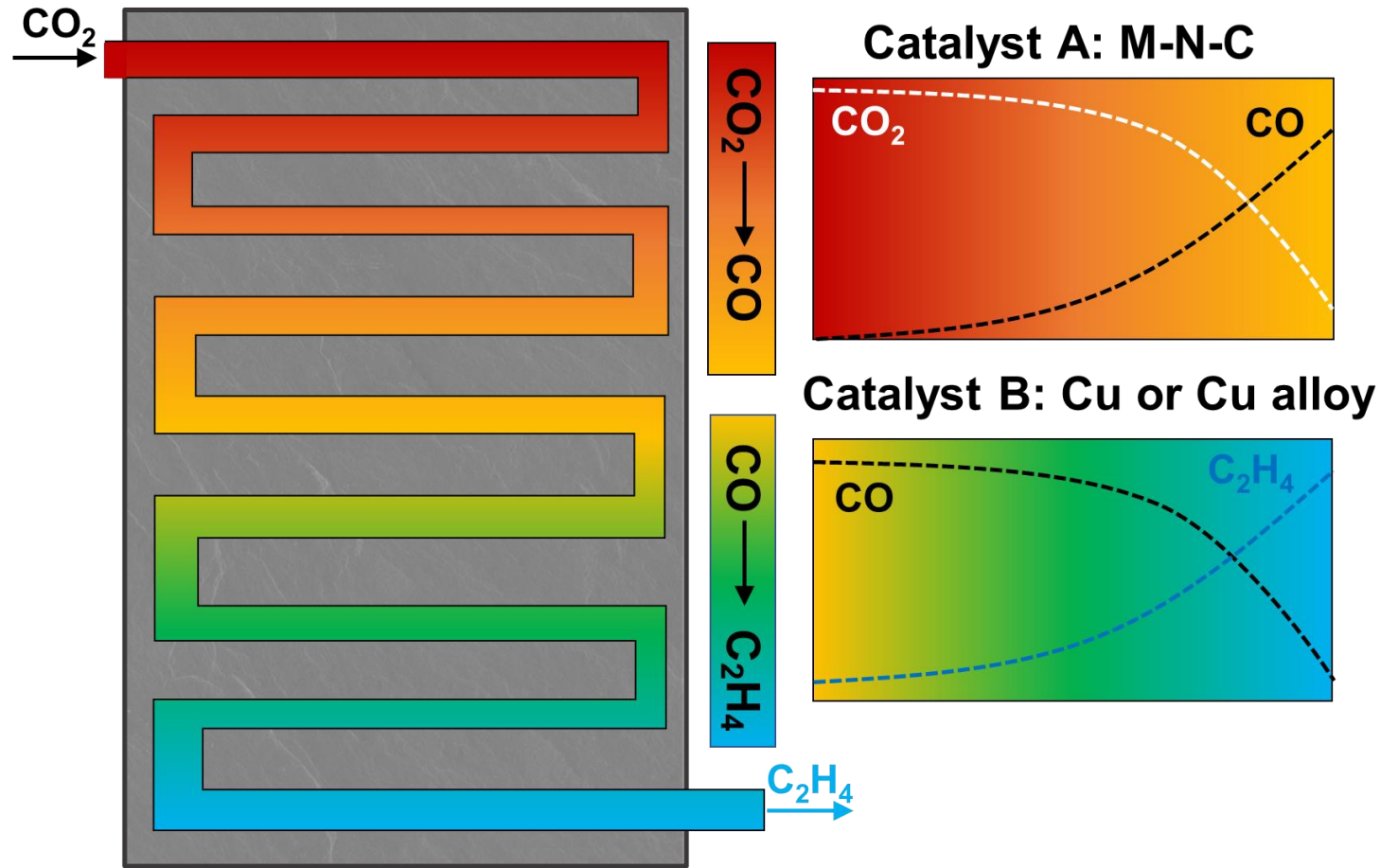
Research Objectives

- 1) To design and fabricate tandem electrodes to direct the cascade reaction of $\text{CO}_2 \rightarrow \text{CO} \rightarrow \text{C}_2\text{H}_4$;
- 2) To develop a functionally graded catalyst layer in the tandem electrodes to balance the transport of electron, ions, and reactants;
- 3) To explore the pulse electrolysis technology to boost the production yield of C_2H_4 and lower the overpotential;
- 4) To demonstrate the MEA-type cell integrating the tandem electrodes for CO_2 pulse electrolysis.

Tandem CO_2 reduction in the gas diffusion electrode



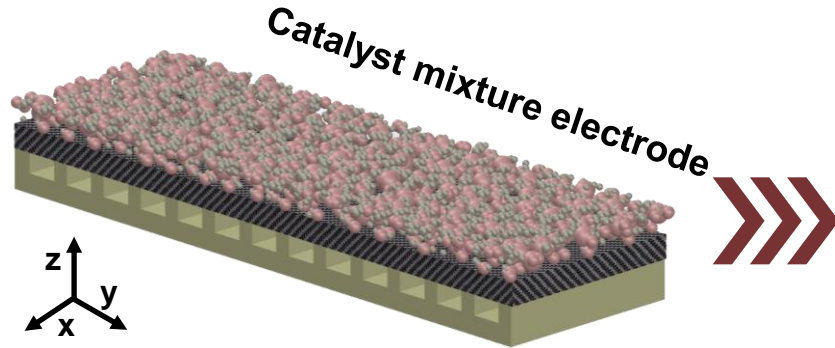
How to Utilize the Intermediate *CO to Promote the Formation of C₂H₄?



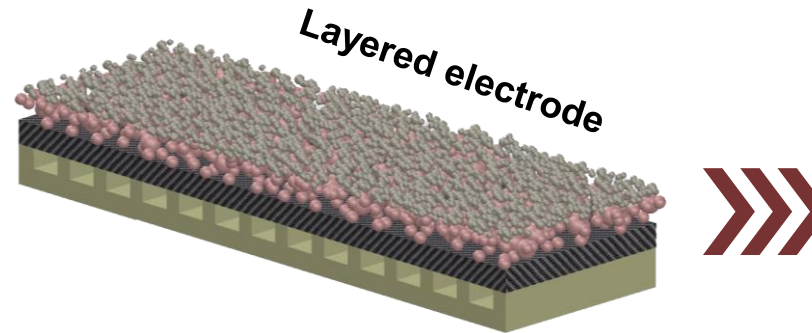
- Realize cascade reaction $\text{CO}_2 \rightarrow \text{CO} \rightarrow \text{C}_2\text{H}_4$ in **one electrolyzer** to simplify the reactor design.
- Maximize the CO utilization by using a tandem electrode design.

Tandem Electrodes

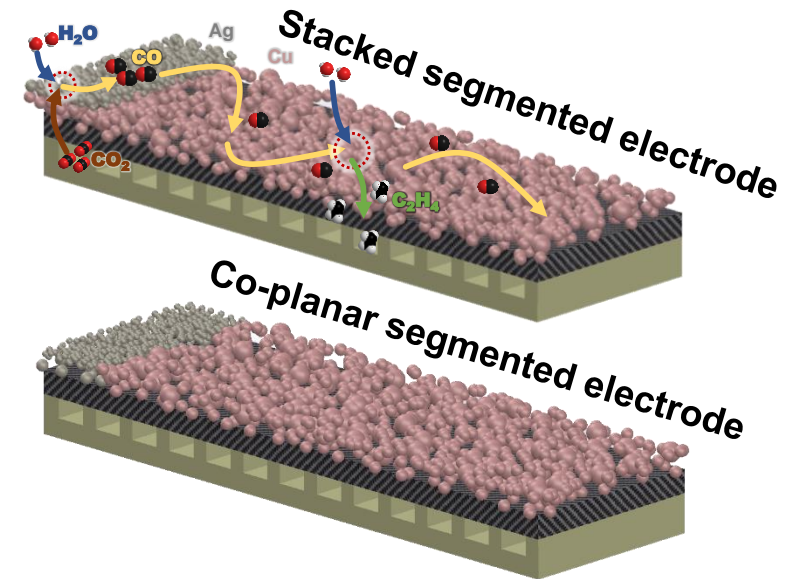
Conventional electrode



Layered electrode

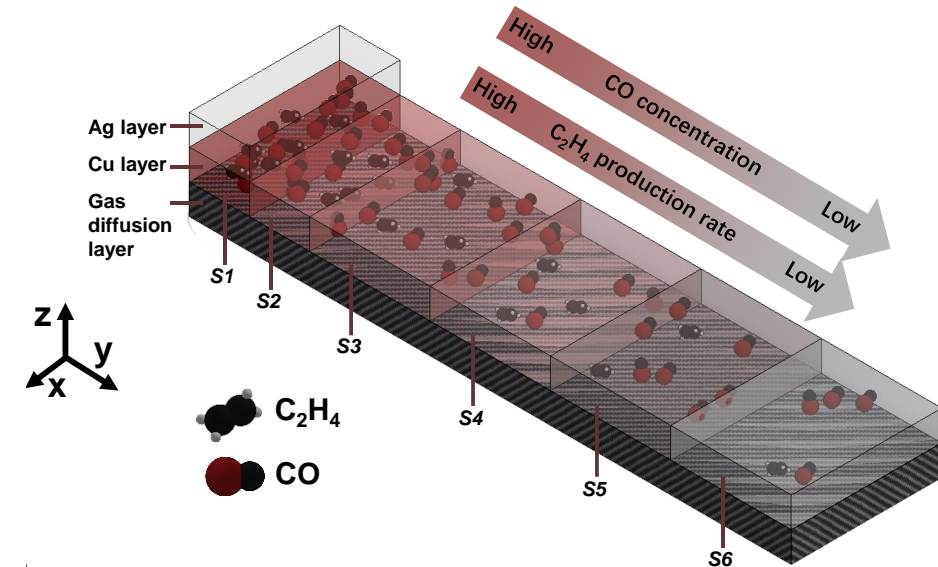
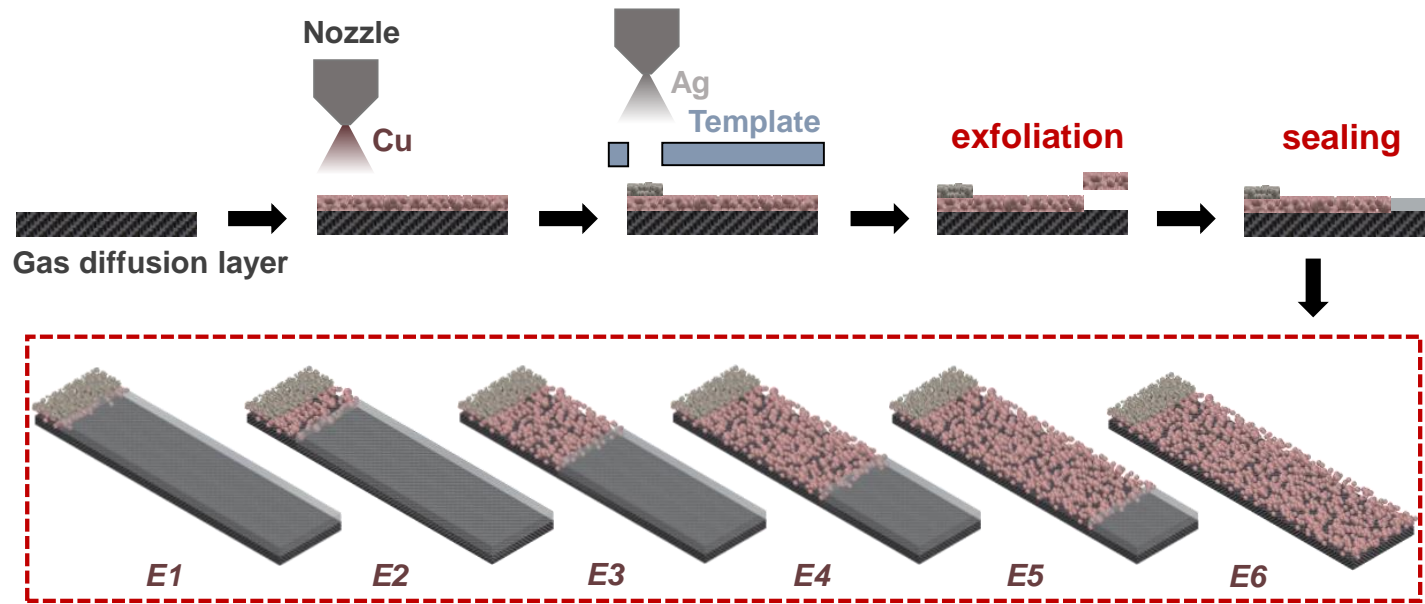


Tandem electrode

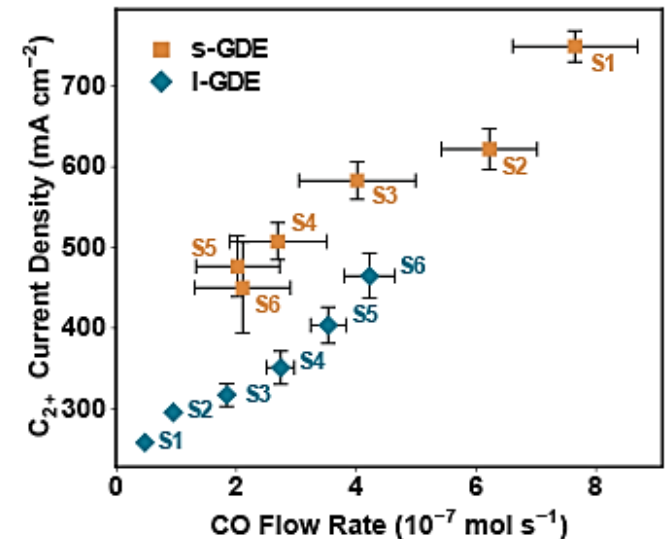


- Tandem electrode design principle: **optimize the Θ_{*CO} at the Cu surface**, leading to simultaneously maximized selectivity and productivity of C₂H₄ through cascade reaction CO₂→CO→C₂H₄.
- **Effectiveness: segmented > layered**

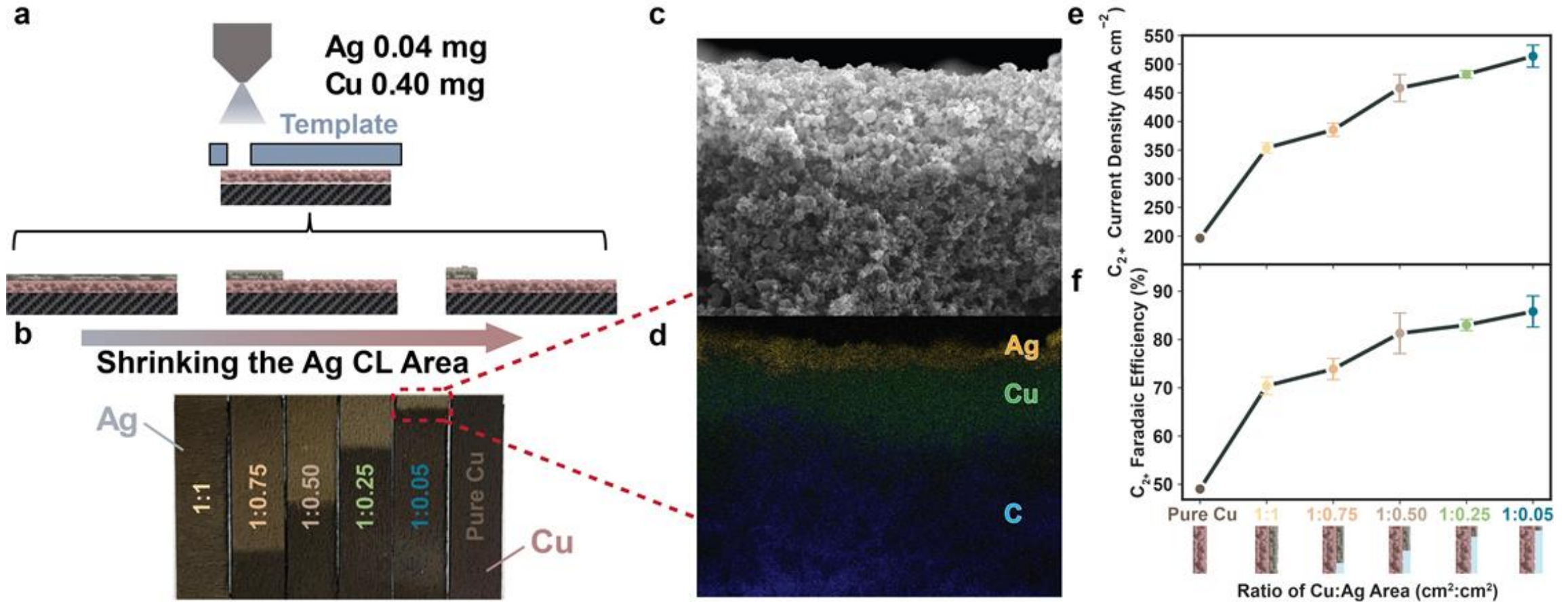
What's the role for the Ag on the conversion of C₂+ products?



- 1) As CO concentration decreases down the length of the segmented GDE, C₂+ productivity decreases as well.
- 2) Segmented GDE delivers higher CO concentration and C₂+ productivity than layered GDE.



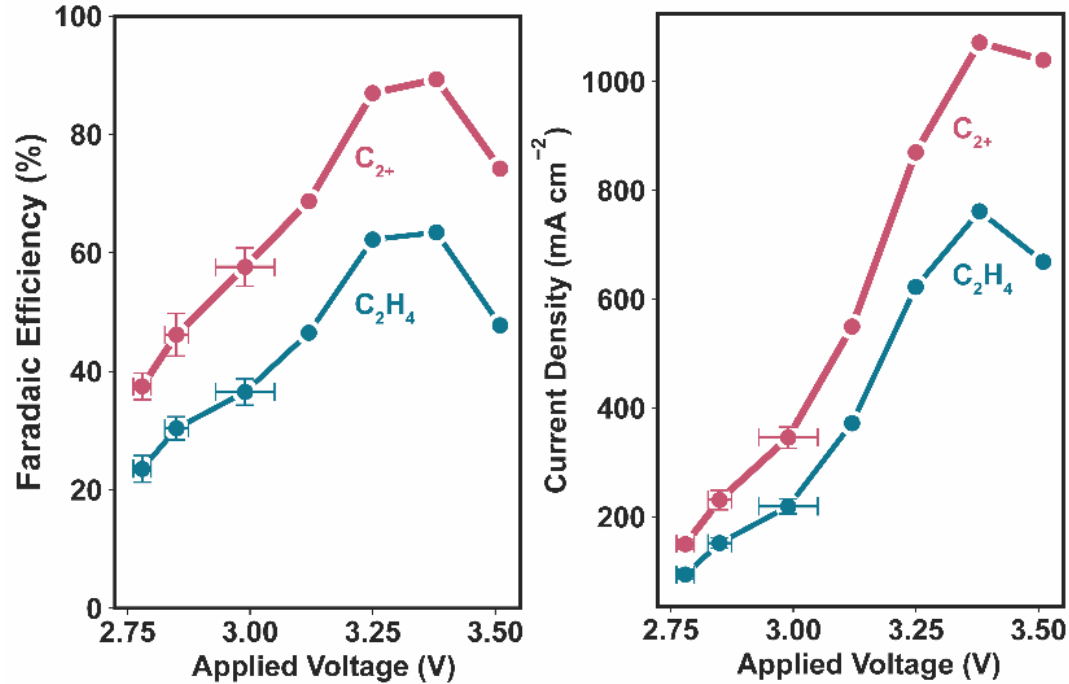
What's the role Ag/Cu exposure area ratio on FE and current density for C₂₊ products?



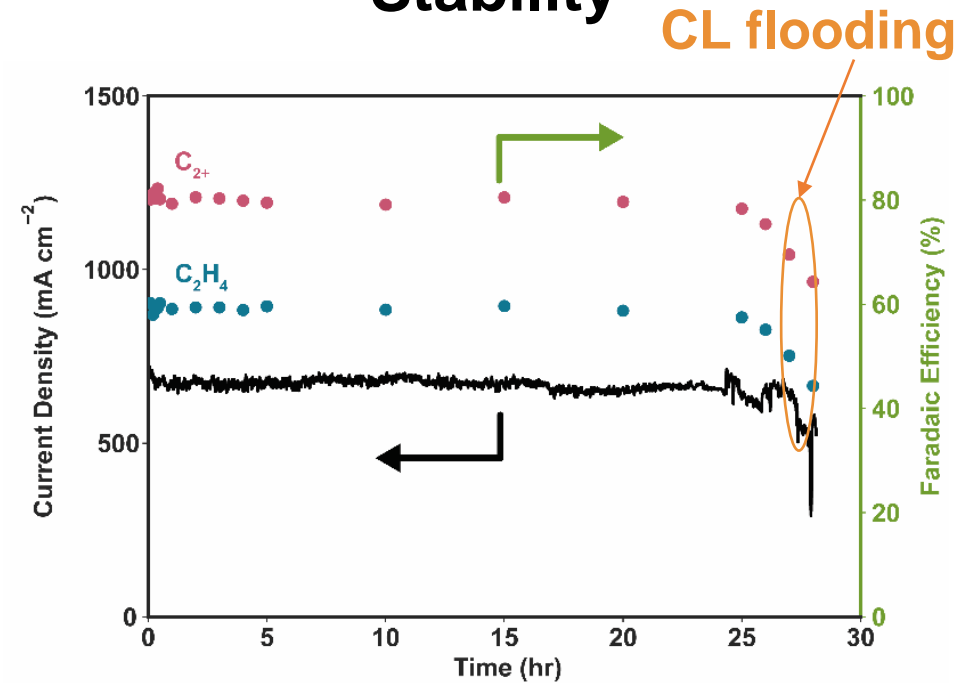
- Shrinking Ag CL providing more concentrated CO for C-C coupling on the Cu CL, and thus yielding higher selectivity and productivity of C₂₊ products.

Tandem Electrode Design: synergy between Cu and CO-generating catalyst

Activity and Selectivity

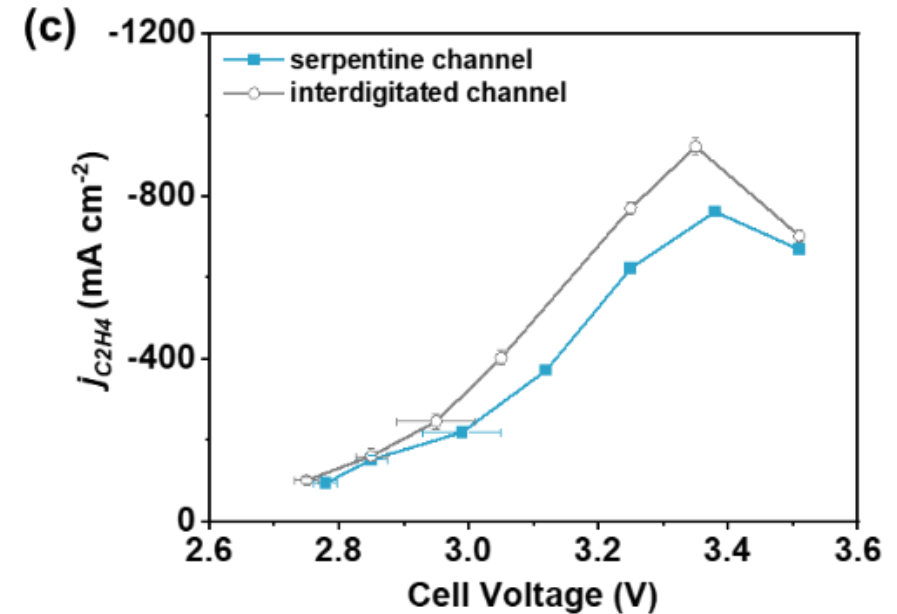
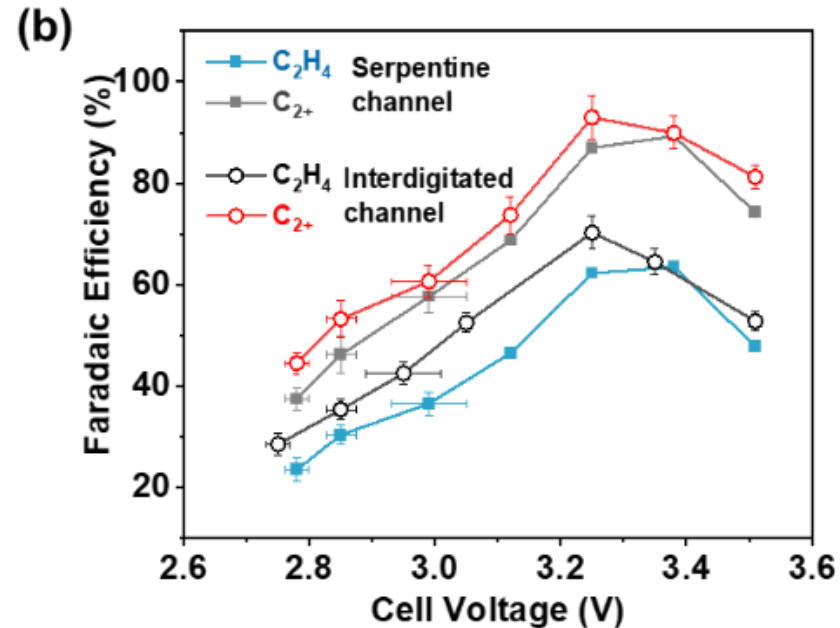
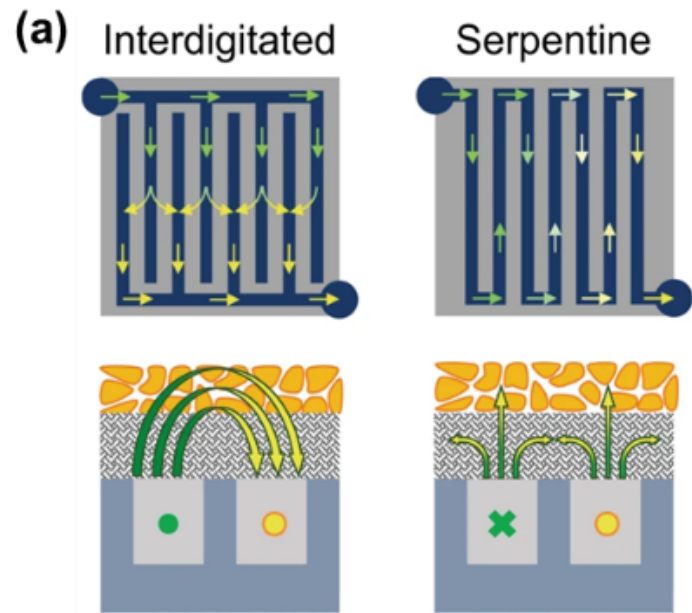


Stability



- Cu/Fe-N-C tandem electrode (Cu : Fe-N-C area ratio = 1 cm² : 0.05 cm²) achieving **60% FE of C₂H₄ at current density > 1 A/cm²** in a flow cell with a thin catholyte layer.
- Severe catalyst layer flooding limiting the long-term operation of tandem electrodes, especially at current density > 500 mA/cm².

Tandem Electrode Design: enhanced gas mass transport

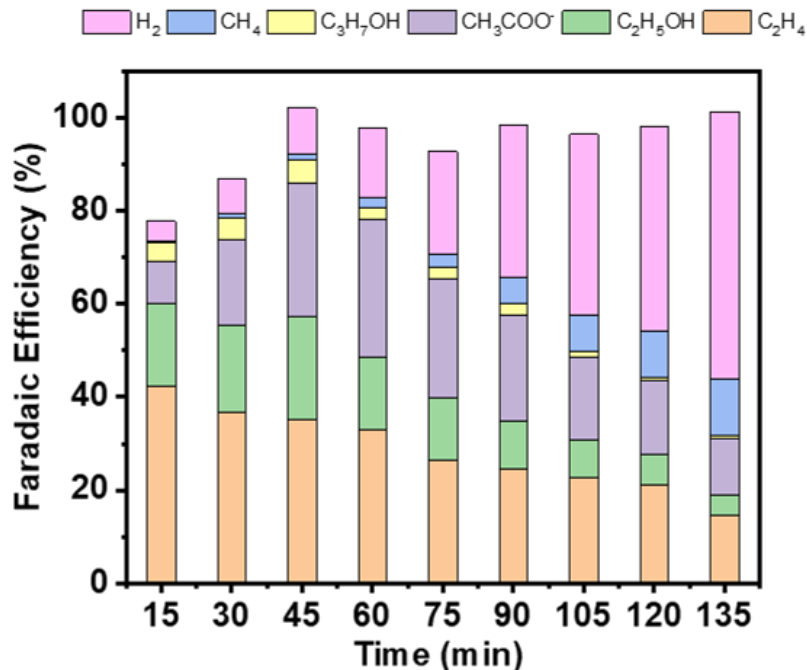


X. Feng et al., Nature Communications, 2011, 12, 136 .

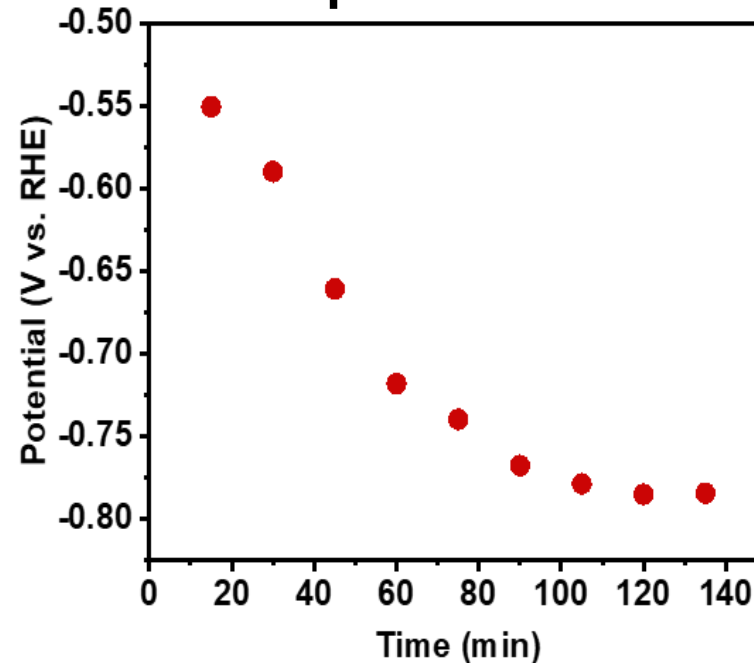
- Interdigitated flow channel forces gas convection into the electrode and then exit to the outlet channels, enhancing mass transport of CO_2/CO into the catalyst layer.
- Maximum FE of C_2H_4 increased from 60% with serpentine flow field to **~70%** with the interdigitated flow field at a **partial current density of over $750\ mA\ cm^{-2}$** on Cu/Fe-N-C tandem electrode.

Tandem Electrode Design: flooding issue of current GDE structure

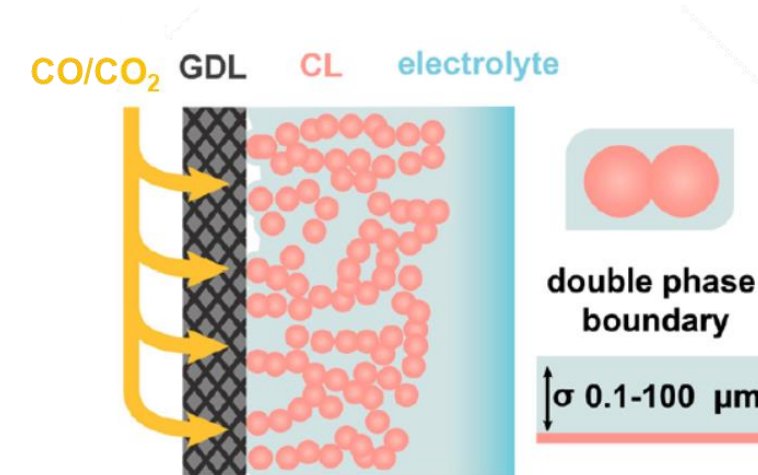
Decrease selectivity towards C_{2+}



Increase mass transfer polarization



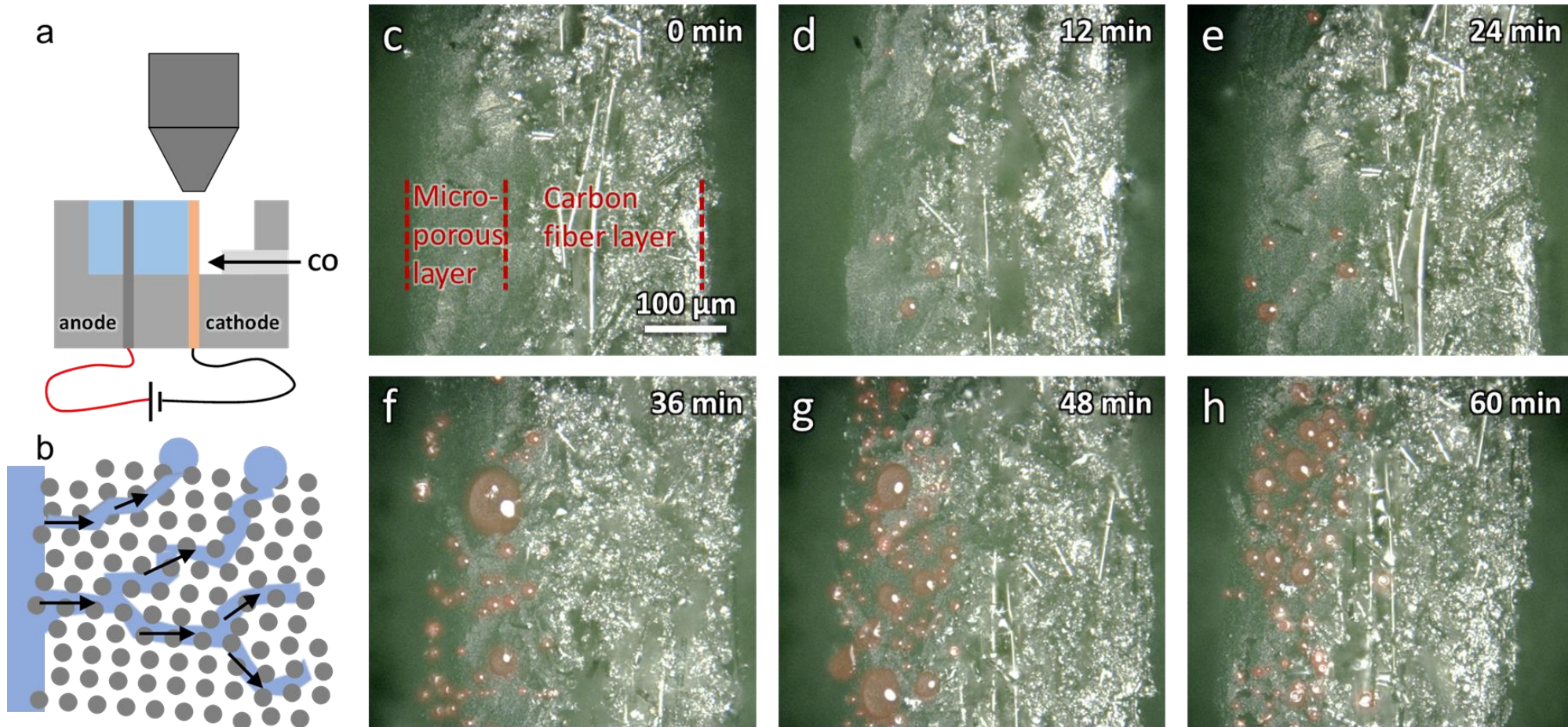
Flooding model of CL



Galvanostatic electrolysis of CORR at 400 mA cm^{-2} on a GDE composed of SGL 39BB GDL and Cu CL

- Solubility in water at 1 atm and 25 °C: CO (0.98 mM) versus CO₂ (33 mM)
- CO reduction reaction (CORR) as the probe for catalyst layer flooding
- The current GDEs with structure and formulation adapted from PEMFC are prone to flooding in a short time, limiting the CO utilization efficacy.

Tandem Electrode Design: flooding issue of current GDE structure

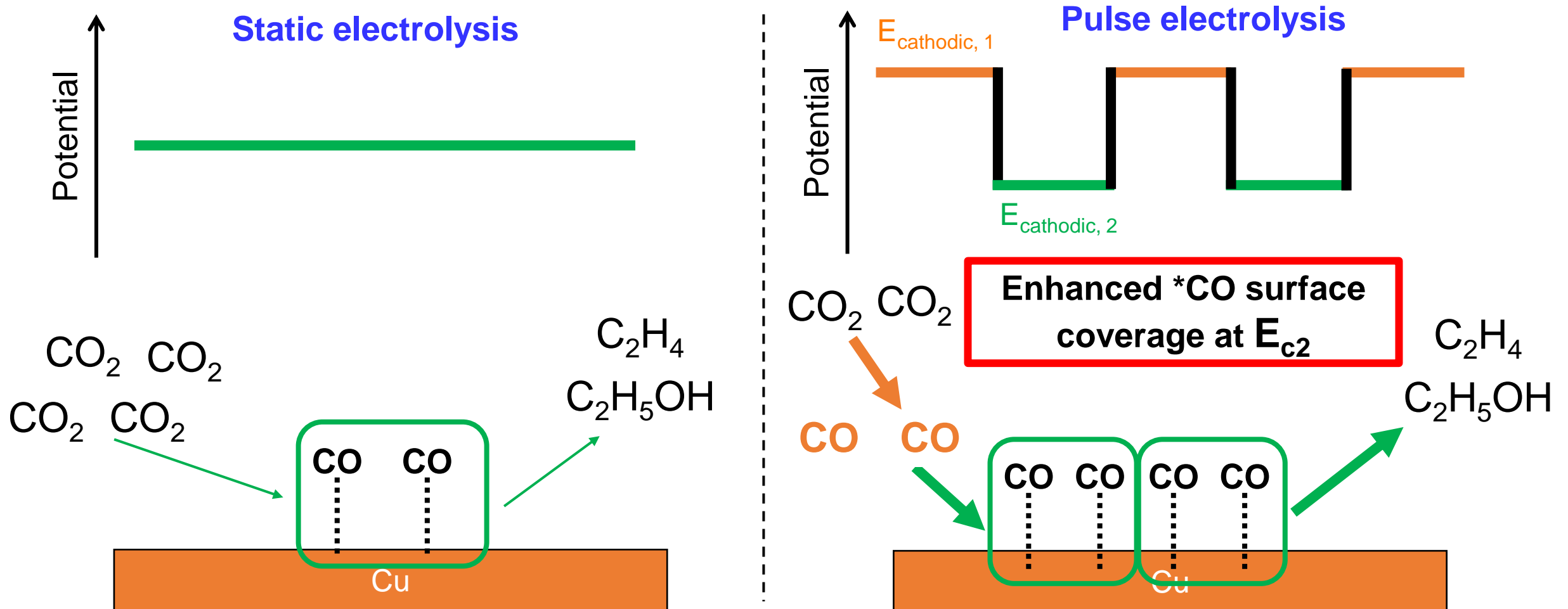


- Flooding extends to gas diffusing layer.
- Design CL and GDL microstructures with effective water management is the focus of future work in order to increase the performance and stability of tandem electrodes.

Pulse Electrolysis

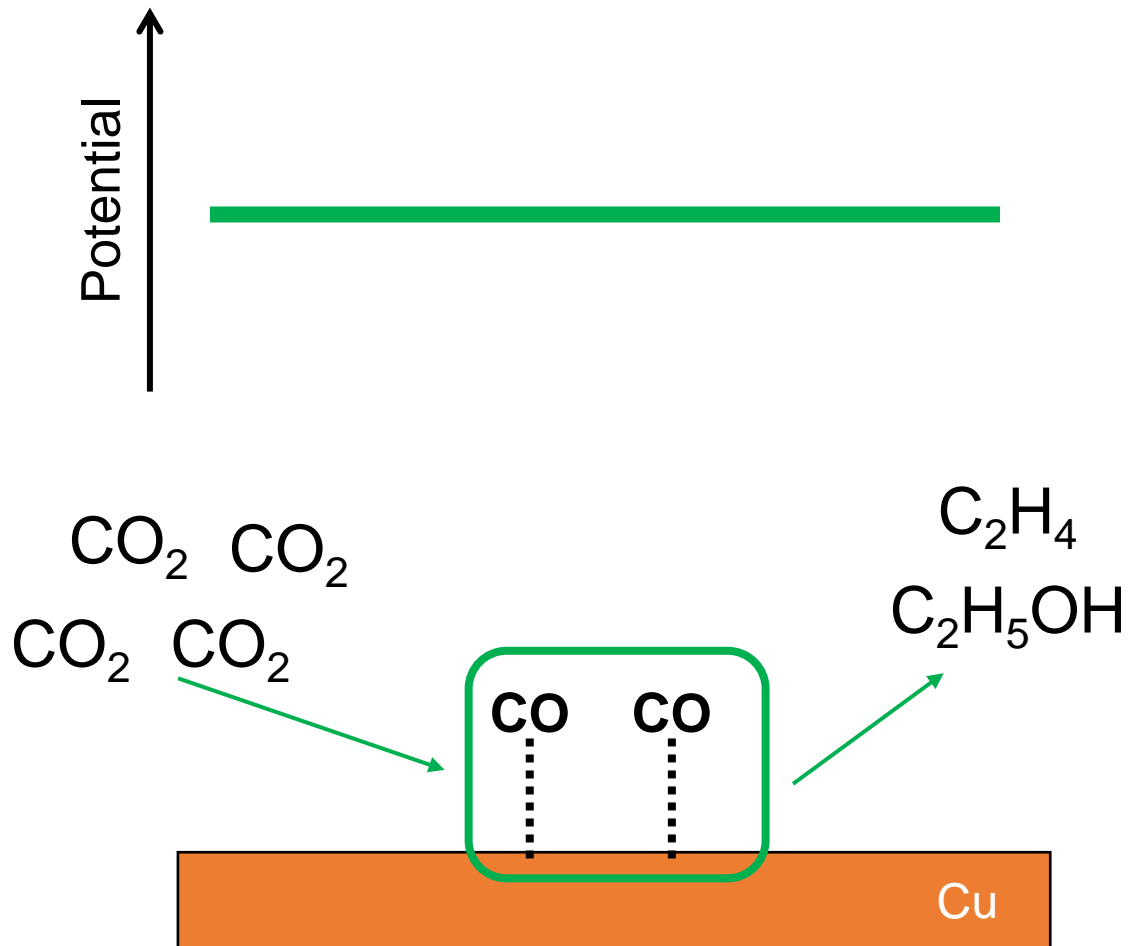
Project Progress: Pulse Electrolysis

Control pulse potential: CO supply from CO-generation catalyst layer in the tandem electrode

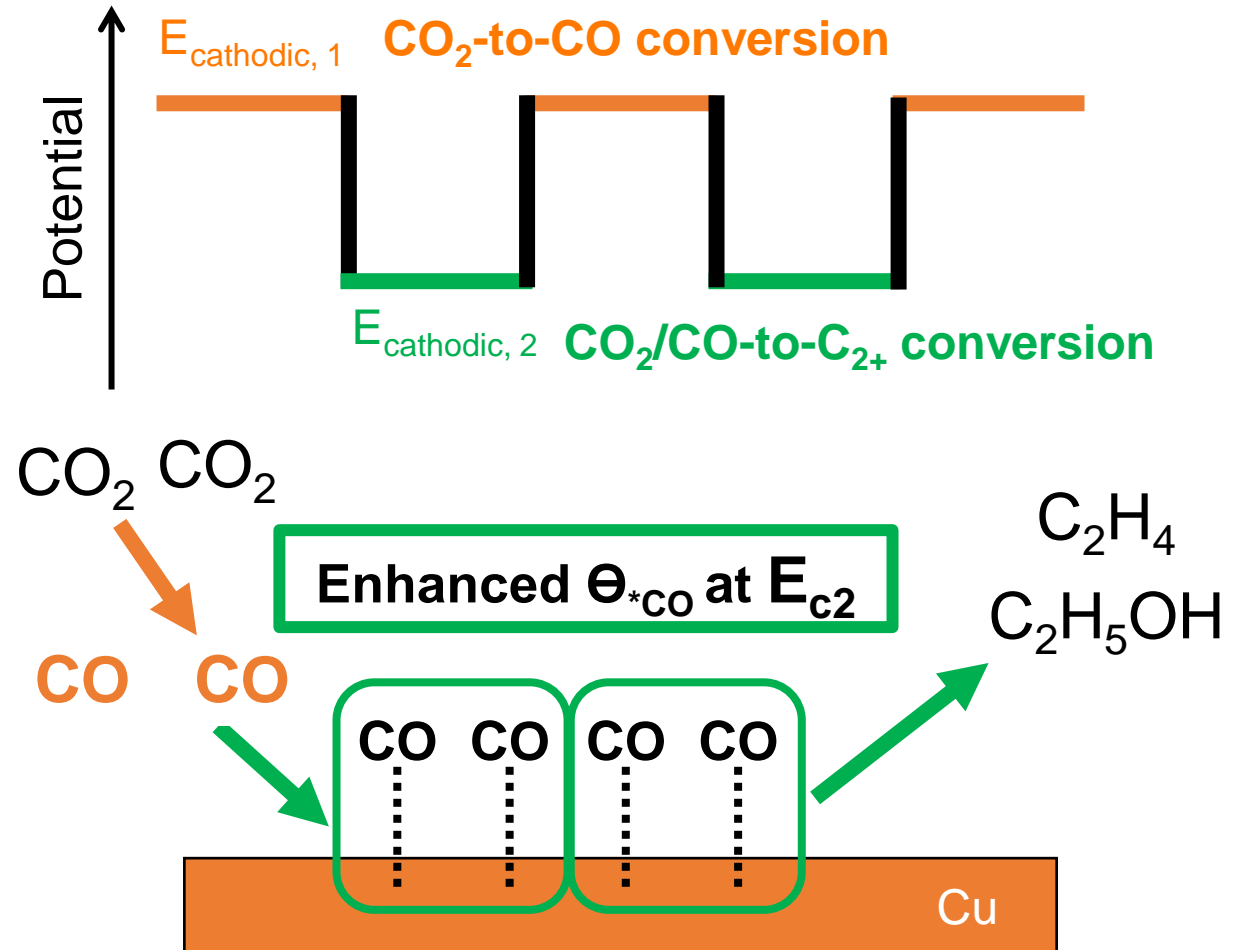


Project Progress: Pulse Electrolysis

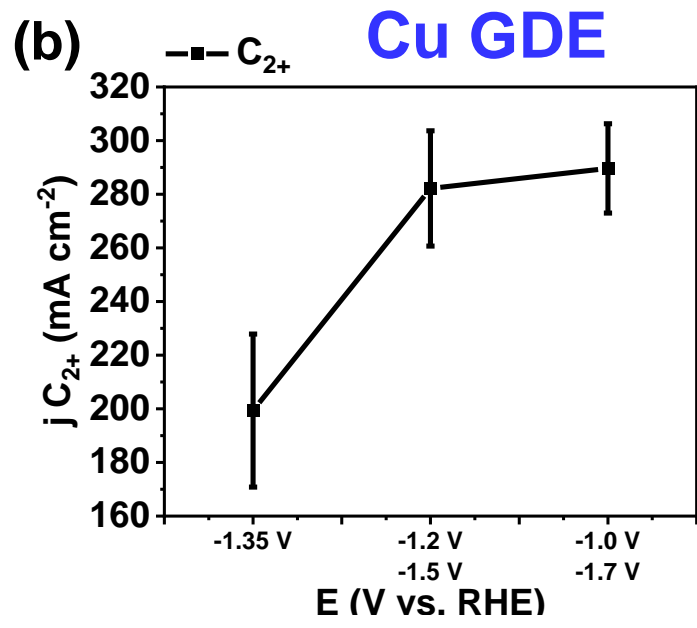
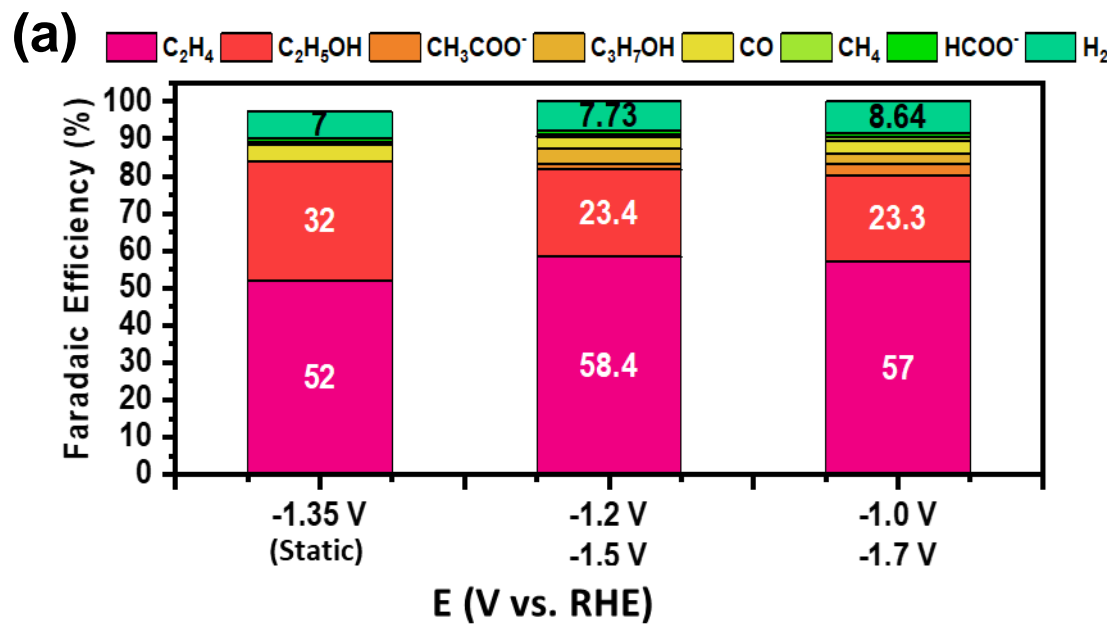
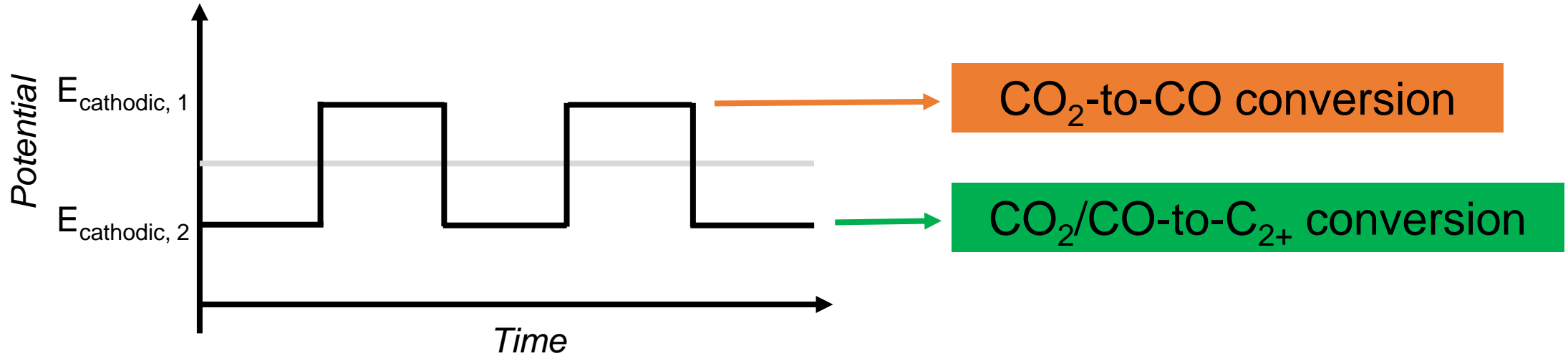
Static electrolysis



Pulse electrolysis

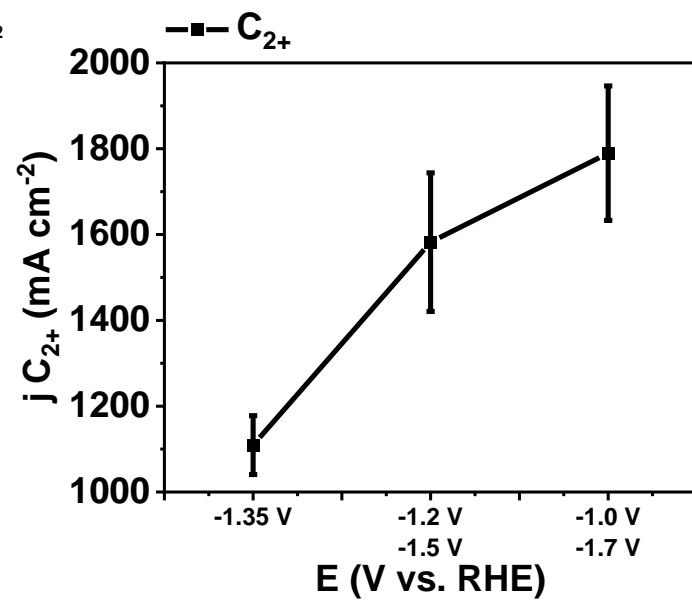
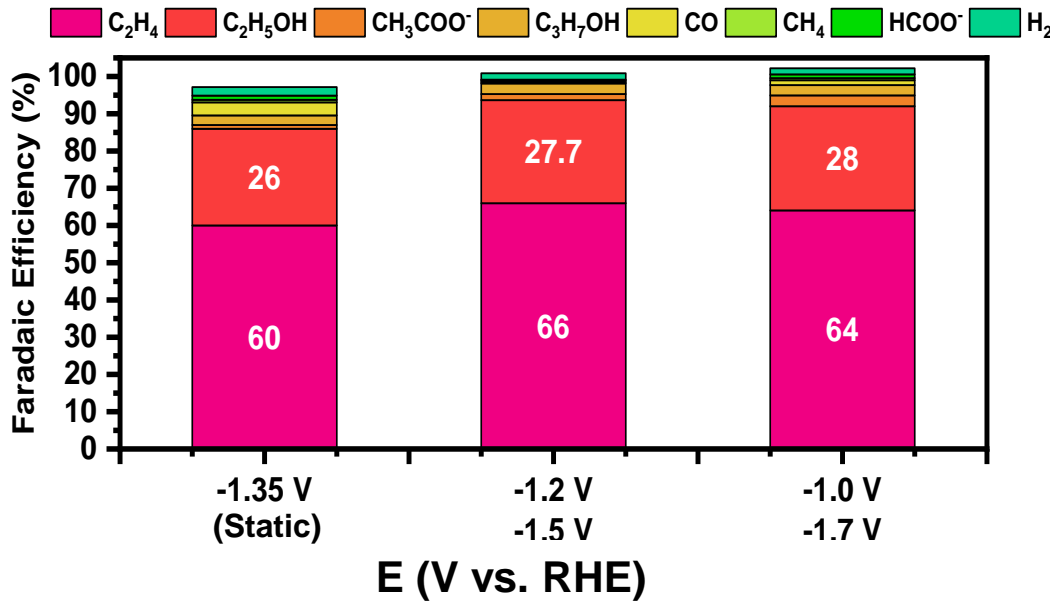
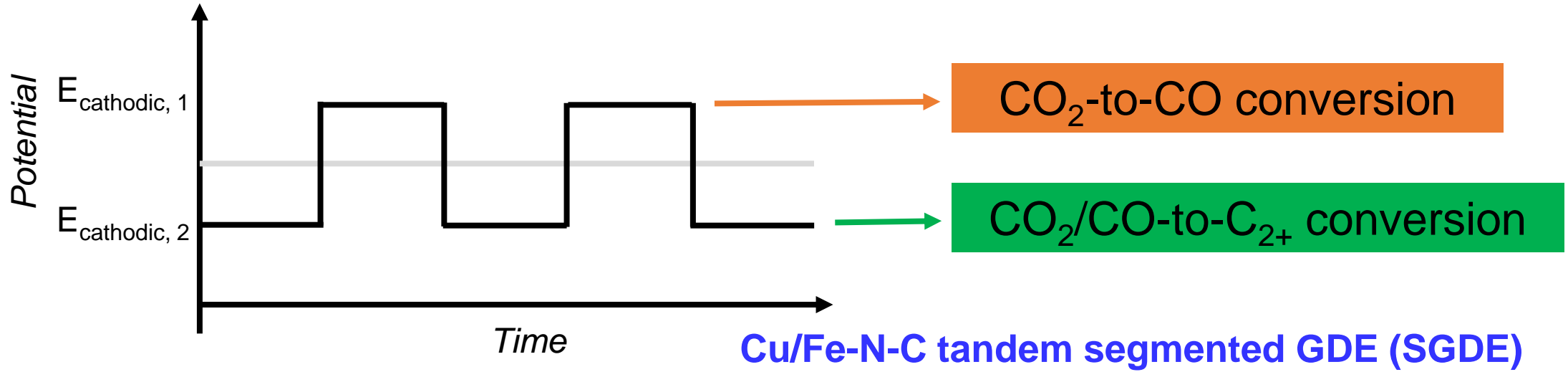


Pulse Electrolysis: enhancement of C_2H_4 selectivity and productivity on Cu GDE



- Cathode potential without iR compensation.
- Faradaic efficiency and partial current density of C_{2+} and C_2H_4 enhances with pulse electrolysis.

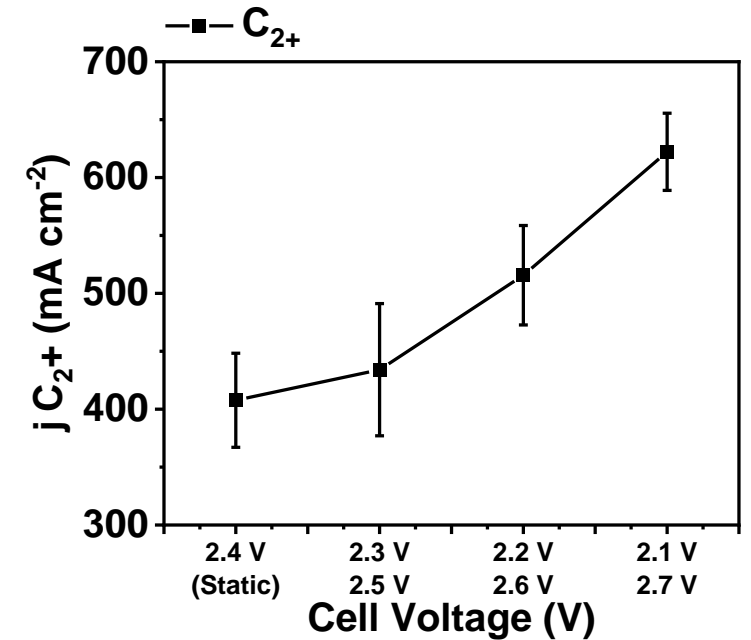
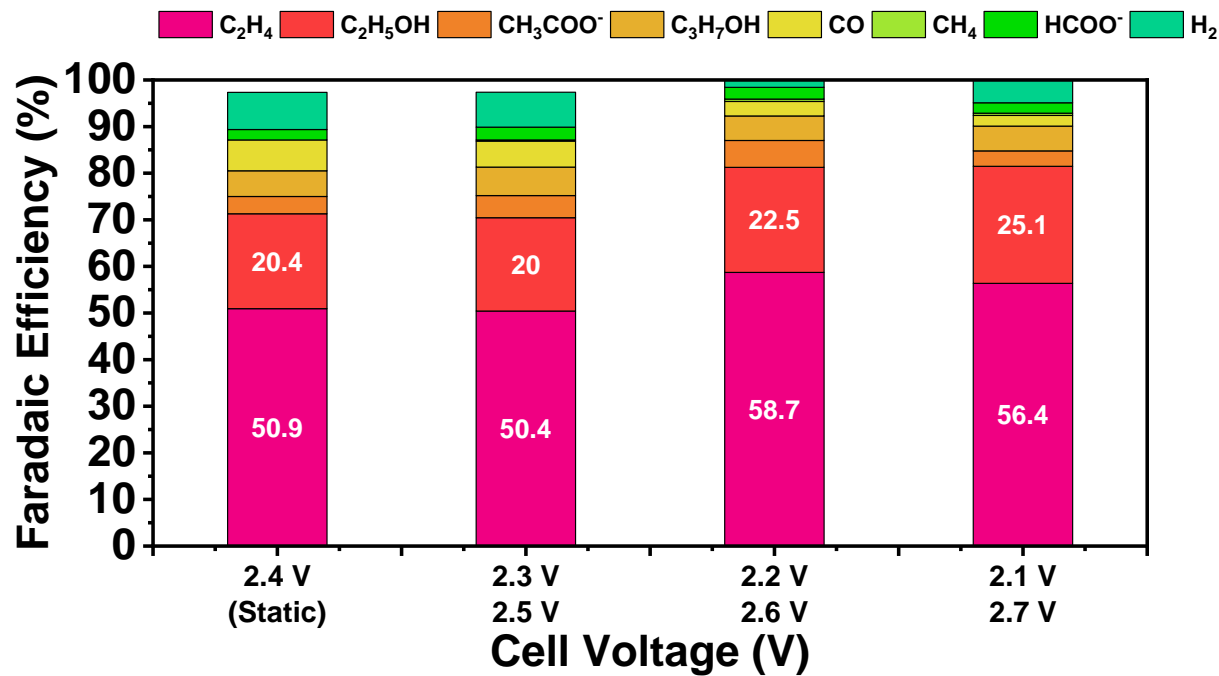
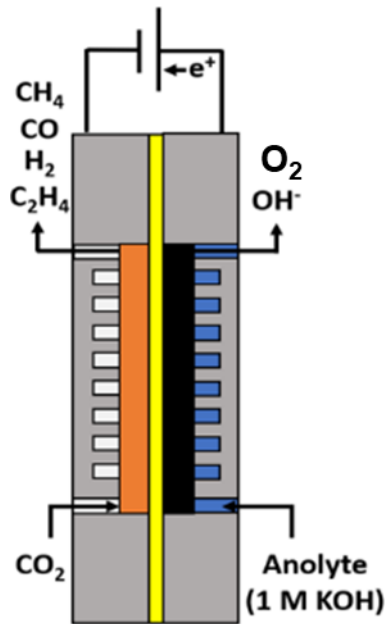
Pulse Electrolysis: enhancement of C_2H_4 selectivity and productivity on Cu/Fe-N-C SGDE



- Pulse electrolysis further promotes Faradaic efficiency and partial current density of C_{2+} and C_2H_4 on tandem SGDE.
- 66% FE of C_2H_4 at $j_{C_2H_4} > 1100 \text{ mA cm}^{-2}$

Integration in a MEA cell: pulse electrolysis + tandem SGDE

Cu/Fe-N-C Tandem SGDE + Pulse Electrolysis + MEA Cell with a Serpentine Flow Field



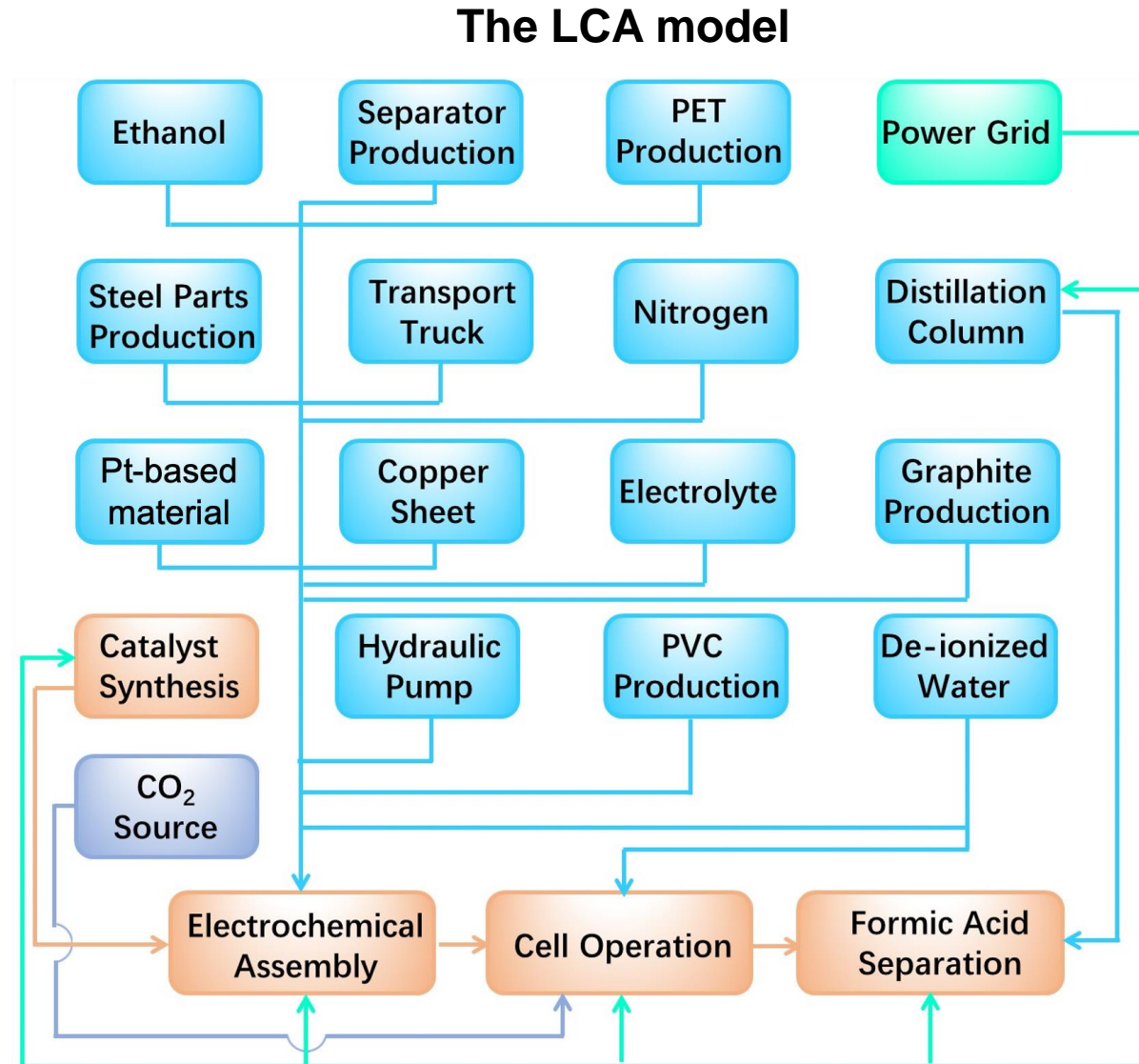
- MEA cell shows lower selectivity of C₂H₄ and compared to flow cell due to the change of GDE surface micro-environment (e.g., local pH and water saturation in the GDE).
- Pulse electrolysis compensates the decline in the MEA cell, prompting the FE of C₂H₄ to 59% at a C₂H₄ partial current density of 340 mA cm⁻².

LCA/TEA Analysis

Life Cycle Assessment of CO₂ Conversion

Goal and motivations

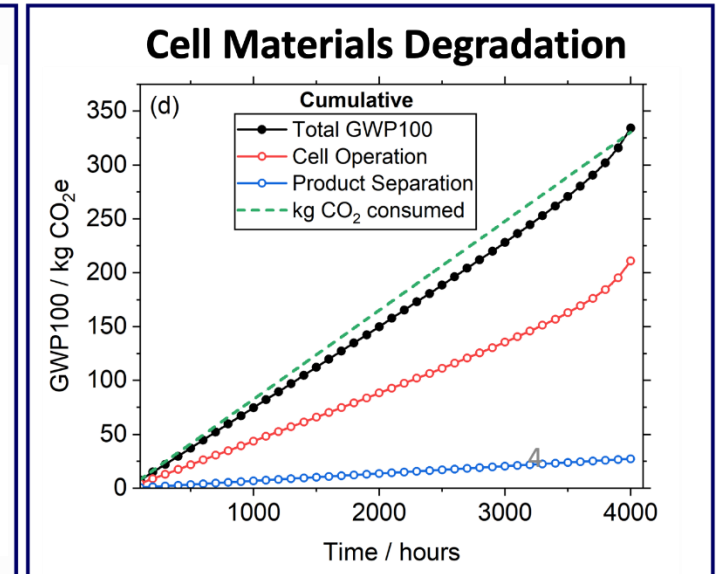
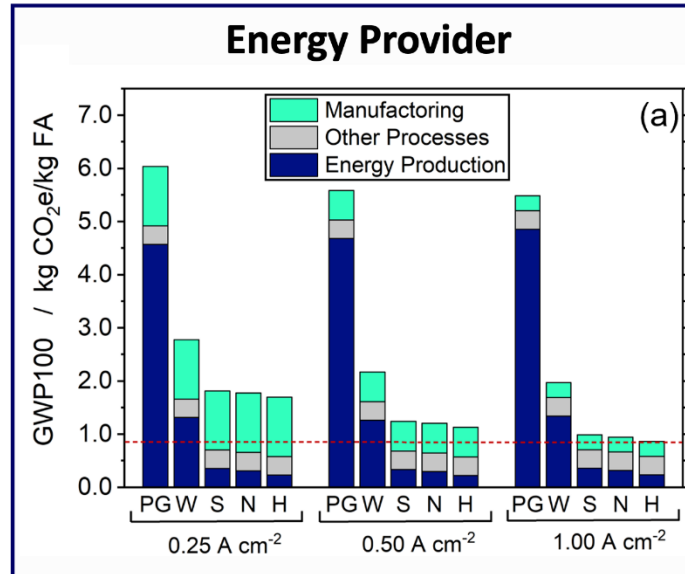
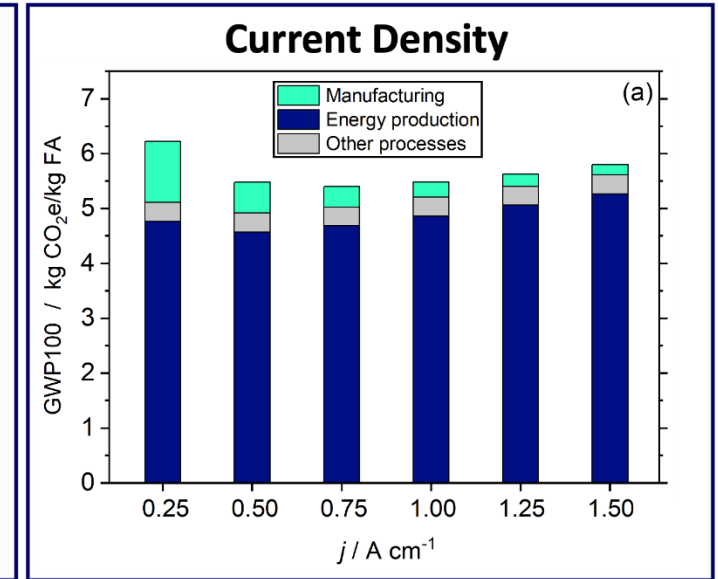
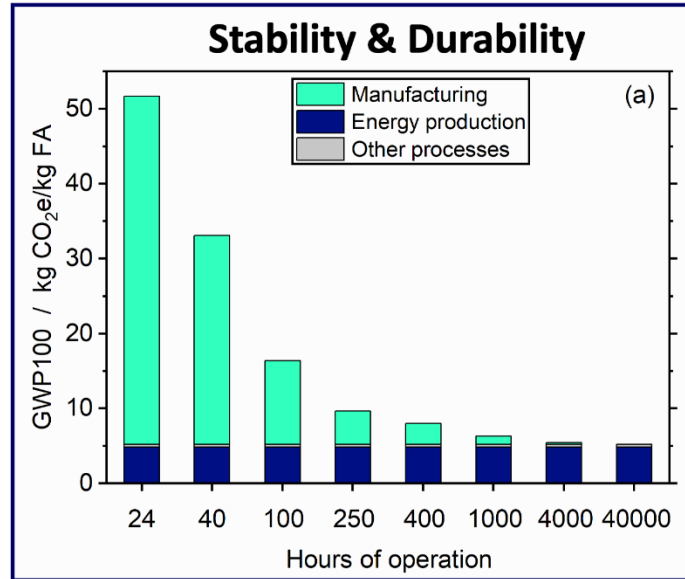
1. We completed a cradle-to-gate life cycle assessment of assembling and operating an electrochemical cell to perform conversion of previously captured carbon dioxide (CO₂), followed by product separation
2. The goal is to investigate the the environmental impact and predict ways of decreasing carbon emissions for manufacturing and using carbon capture and utilization (CCU) technologies
3. We successfully built a model to investigate the environmental impact as a function of number of operation parameters.
4. We envisage that this LCA study will provide guidance and information regarding aspects of CCU technologies which may require optimization under the environmental point of view.



Life Cycle Assessment of CO₂ Conversion

Results and Discussion

1. Stability/durability and operation variables (current density or cell voltage) have high impact on the carbon emissions.
2. The optimal parameters include stable operation for at least 4,000 hours at (ultra)high current densities (0.50 - 1.00 A cm⁻²).
3. Through use of renewable energy sources zero carbon emissions may be achieved only if high cell performance conditions are met.
4. The cumulative carbon emissions were predicted during the entire life cycle of the system (4,000 hours), while modelling cell aging and corresponding decline in performance. Here, the use of renewable energy is of outmost importance to achieve climate change mitigation.

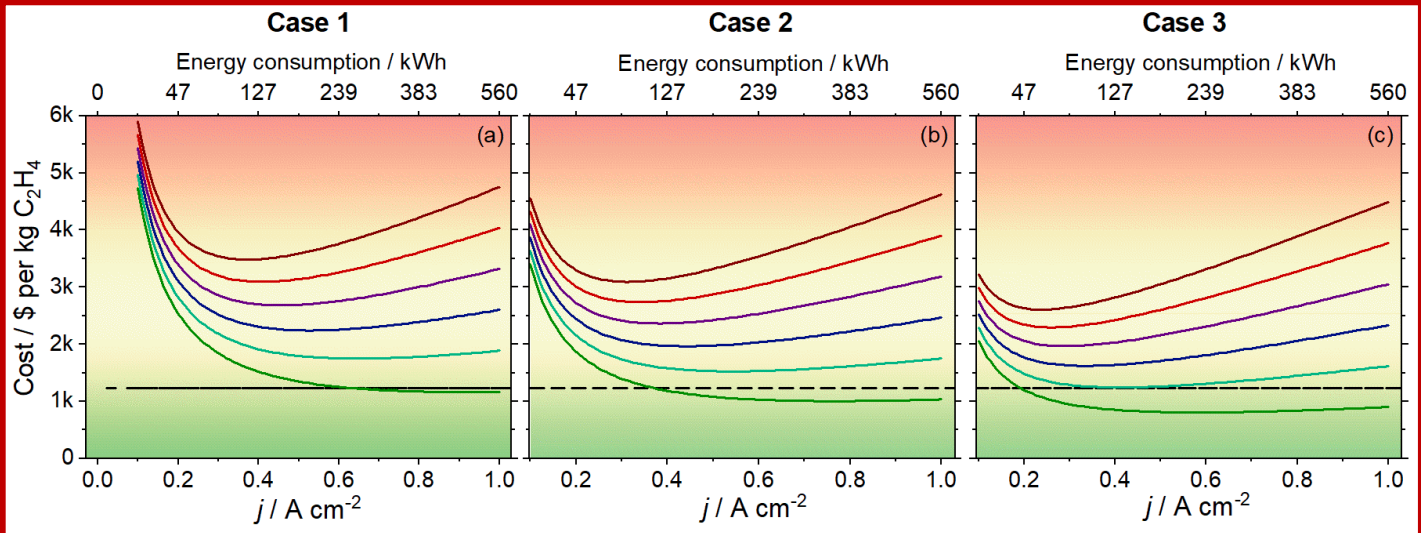
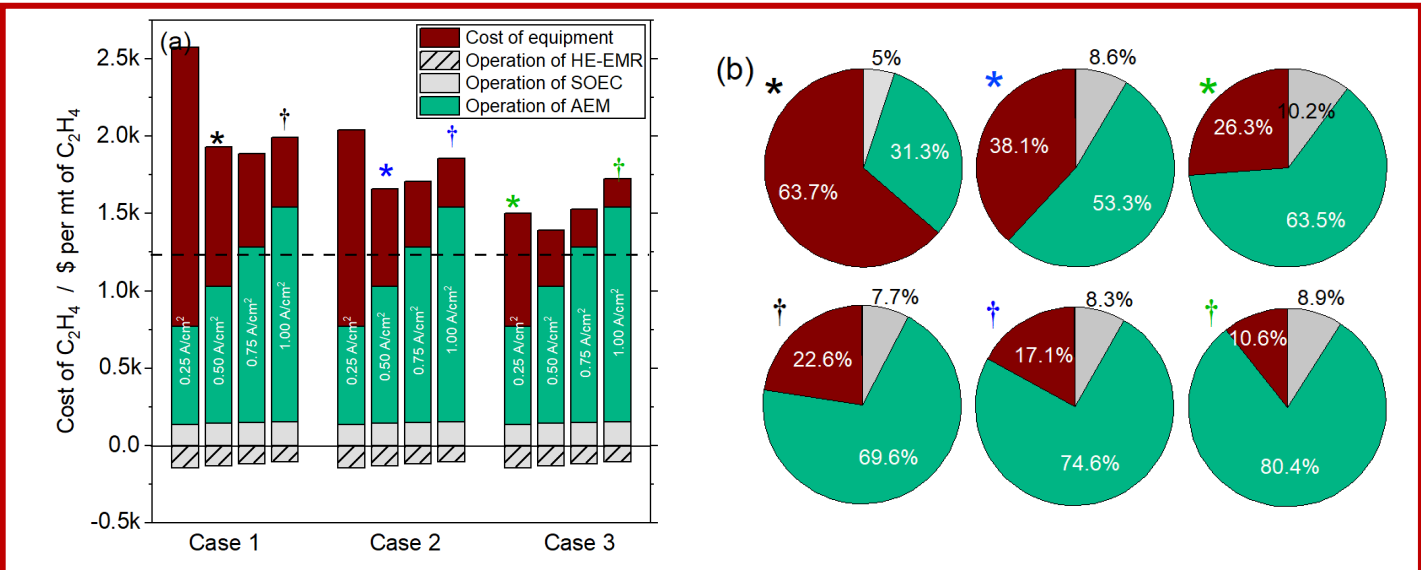


Technoeconomic Analysis of CO₂ to Ethylene

Results and Discussion

1. Reducing the area-specific resistance of an AEM reactor and achieving a high selectivity for ethylene (>50%) have the potential to significantly lower the product cost.
2. Operation of carbon capture unit allows reduction in production cost up to ~30%.
3. Cost of equipment is not negligible and can contribute up to ~28% to the overall production cost (60% of which is attributed to the AEM)
4. With renewable electricity of \$0.02-0.04/kWh, competitive production costs of ethylene are achievable.
5. From LCA studies, when renewable energy is used, conversion of CO₂ to ethylene yield to negligible environmental impact and allows achieving negative emissions.

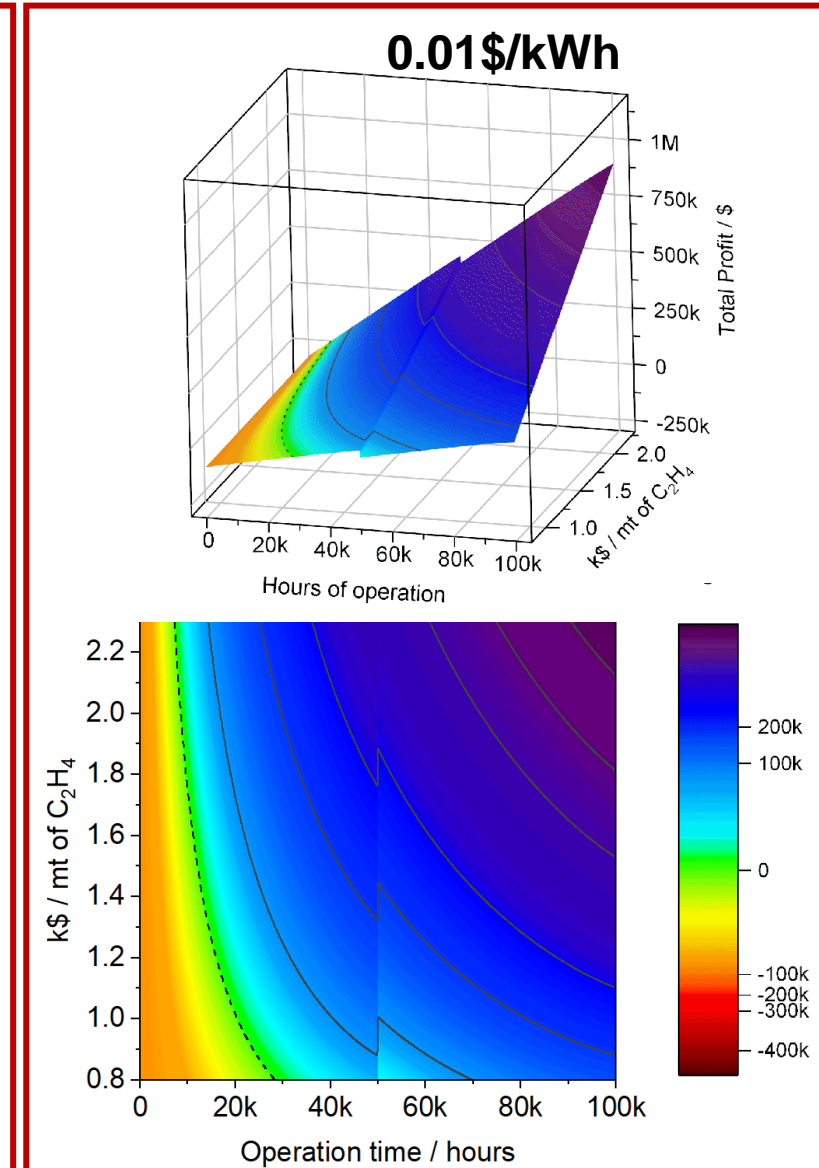
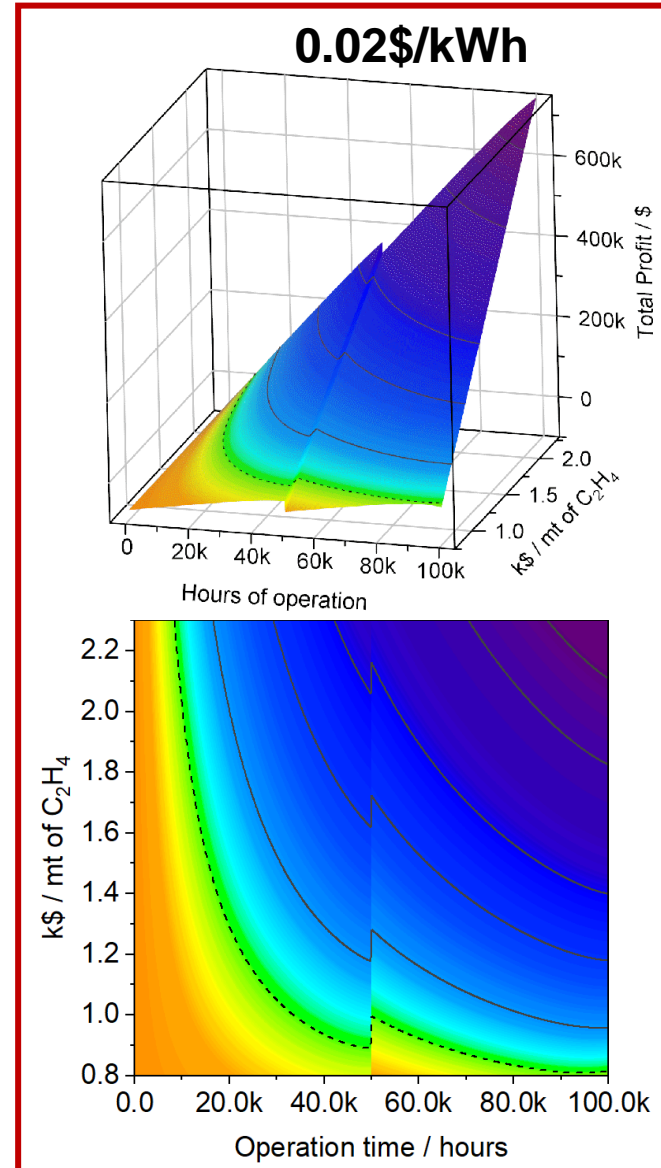
Equipment cost & Current density



Technoeconomic Analysis of CO₂ to Ethylene

Profit Analysis

1. Total profit for production of ethylene using the modelled set-up for CO₂ capture and electrolysis, accounting for degradation of cell performance over operation time.
2. The profit is dictated by the energy consumption and its cost, as well as the projected market price of ethylene.
3. For cost of electricity 0.01\$/kWh, positive value of the total profit are observed at competitive prices of ethylene, when the set-up operates for longer than 20,000 hours



Summary and Major Accomplishments

- Established the design principle of tandem electrodes
- Achieved **70%** selectivity of C_2H_4 at **1 A cm⁻²** current density on segmented electrodes in the flow cell
- Developed pulse electrolysis protocol involving two reduction potentials and applied pulse electrolysis to tandem electrodes
- One formal patent for tandem electrodes was filed.

- Develop advanced Cu-based catalysts to increase the selectivity to C_2H_4
- Optimize the microstructure of catalyst layer to increase the CO flux and CO utilization efficiency in the tandem electrodes
- Intensify the process in the MEA cell
- Perform final TEA and LCA