

Next Generation Durable, Cost Effective, Energy Efficient Tubular Solid Oxide Fuel Cell

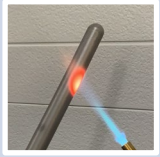
Contract: DE-FE0031674

Ted Ohrn, CTO

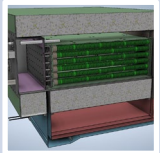
October 25, 2022



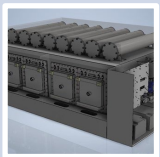
Project Objectives



Develop and optimize a YSZ electrolyte-based solid oxide fuel cell (SOFC) technology for low cost, low temperature (550~650°C), and high energy efficiency operation.



The developed technology will be implemented and demonstrated in a high efficiency 2-3kW SOFC with applicability to sub-MW system.



A modular design and cost analysis will be performed.

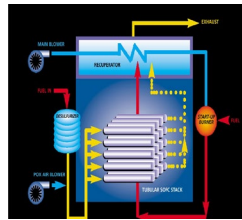
Company History



2000

SOFC Division started at Acumentrics formed in Westland, MA

10 Watts



2001

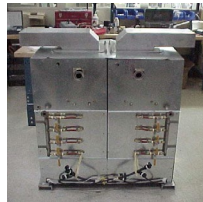
1st 1kW NG Prototype

25 Watts



2002

5000W APU Core Module



2005

5kW NG Prototype



2009

1st Remote Demonstration on NG



2011 - 2012

1st Commercial Sales & SOFC Product Suite (2012)

250W to 1.5kW



2016



2016

Acumentrics SOFC becomes Atrex Energy



CSA Certification for NG & LPG Systems

2019



2019

Special Power Sources purchases Atrex Energy

Enters in Strategic Partnership with Advanced Tech Works (ATW) for Manufacturing and Field Services

Relocates assets to Alliance OH

SPS acquired Atrex Energy and formed a new company including several former LG engineers and technicians

Field Installation Examples



Radio Network Tower in Alaska



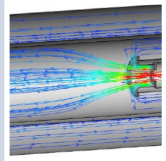
- 600+ systems previously fielded across N America
- **6,000,000+ hours of field operations**
- Single unit operations of 35,000+ hours (25X)
- **99+% availability...when it must work in high-intensity cell applications...it will**



Cathodic Protection Site in Wyoming



Wellhead Controls in New York



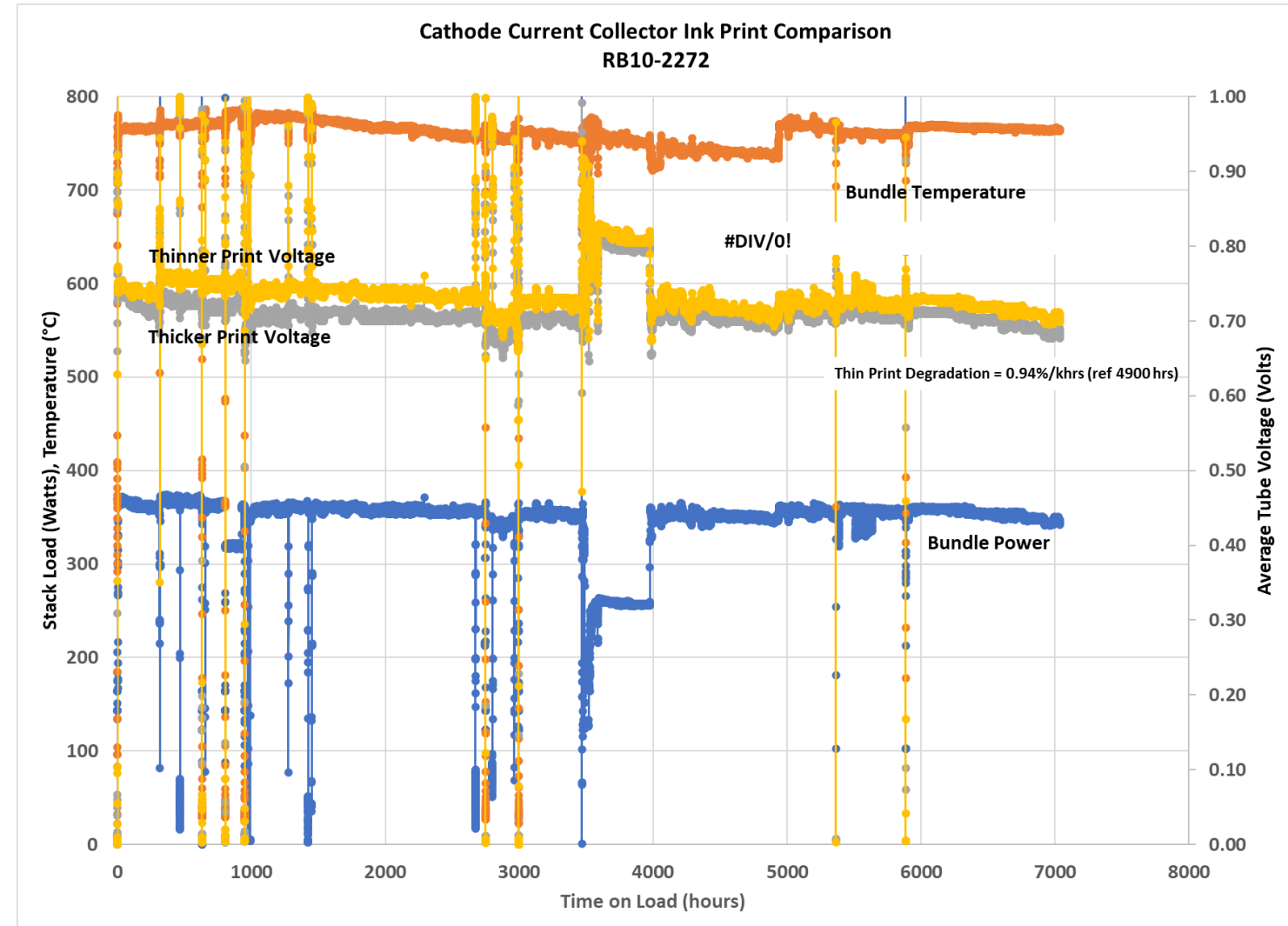
Task 2 – Cell Technology Development



Task 4 – Technology Implementation and Demonstration

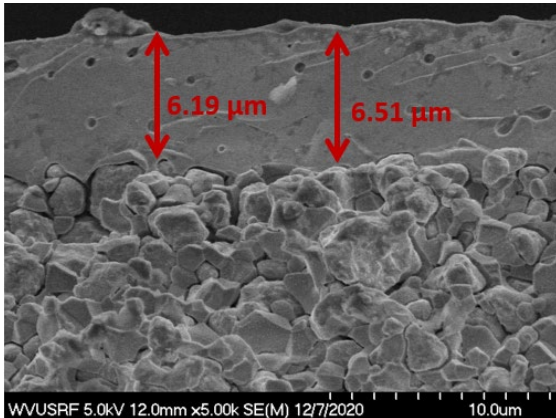
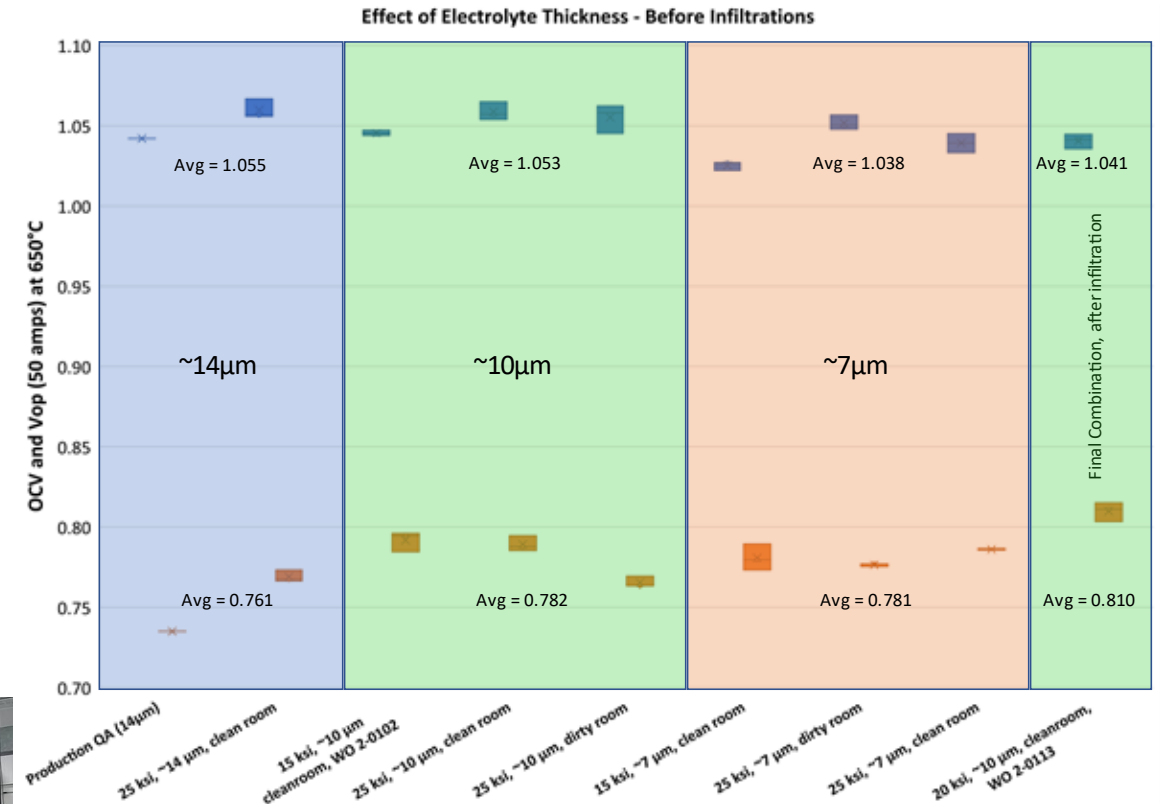
2.1 Cathode Current Collector Development

- New screen patterns evaluated for improved printing of Ag current collector mesh pattern
- Screen parameters optimized
- Long-term bundle test shows improved and stable performance
- New manufacturing specification developed to reduce cost



2.2 Thin Electrolyte

- Electrolyte slurry formulated with different solids loading and applied with different translations speeds during spraying
- Clean room was installed to minimize possible defects caused by the processing environment



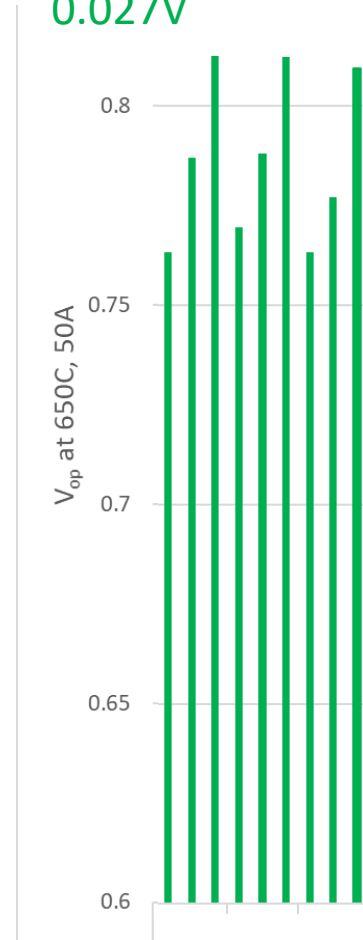
10 micron thick electrolyte provides best combination of sealing and performance

2.3 Effect of Cathode Infiltration

- PrOx infiltration chosen
- Cathode delamination issues developed – related to over-wetting of the surface
- A more concentrated solution was more robust

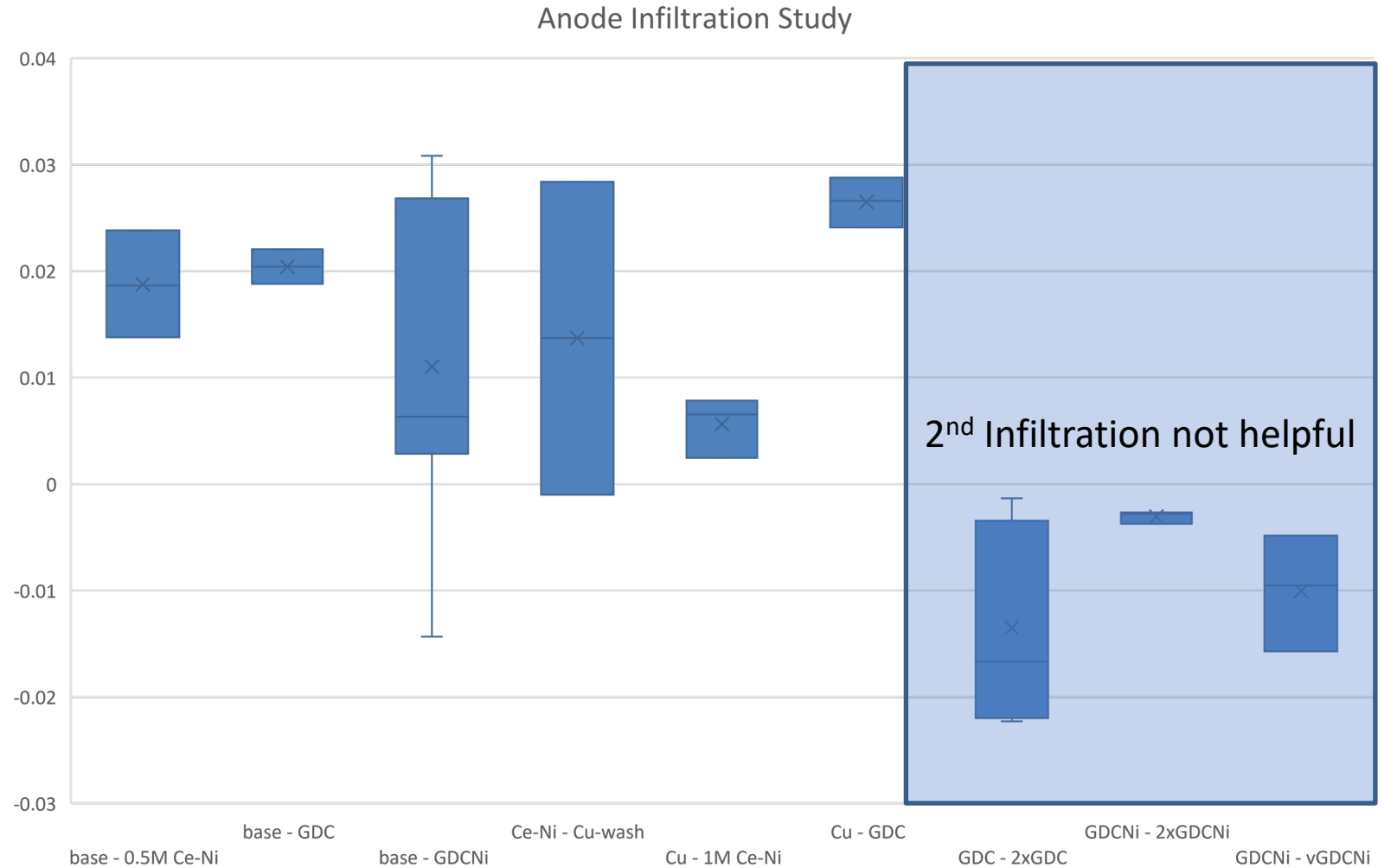


Avg improvement
0.027V



2.4 Effect of Anode Infiltration

- Ce-Ni and GDC showed similar improvement
- Results of Cu-wash were inconsistent, but process kept for carbon formation considerations



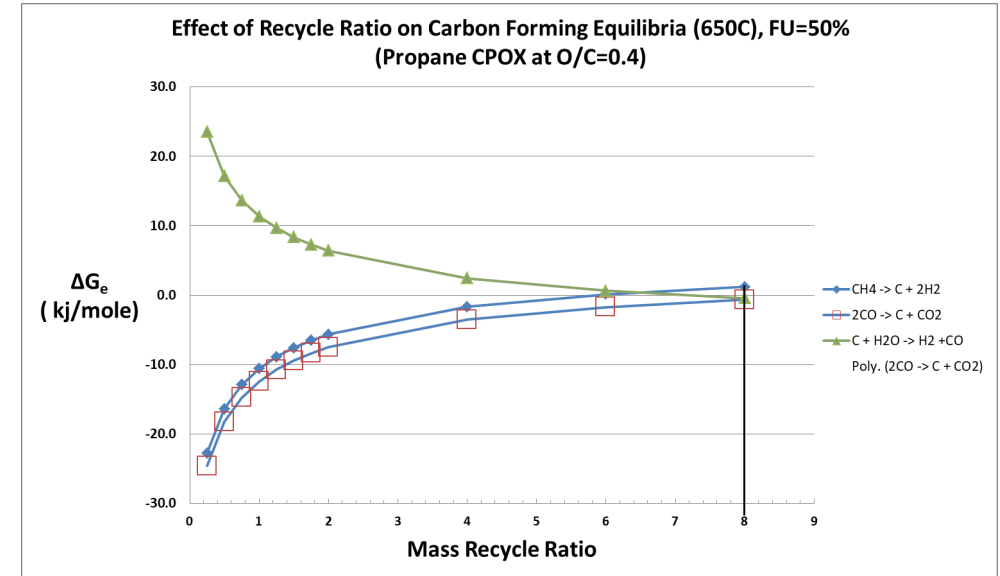
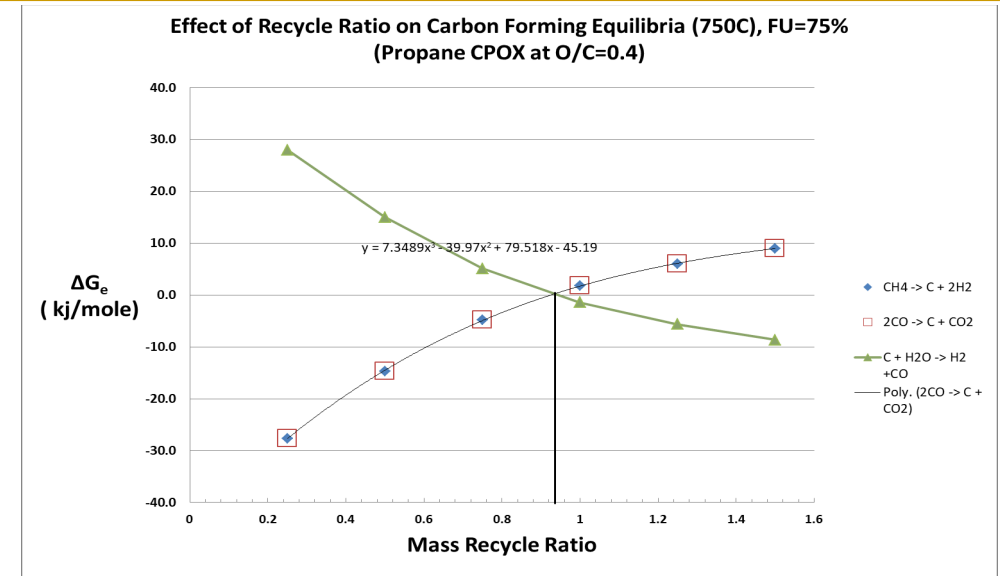
2.5 Internal Reformer Validation - Carbon Prevention using Internal Recycle

Potential for Carbon Increases with:

- Higher Cx
- Lower temperature
- Lower Fuel Utilization (FU)
- Lower CPOX O/C ratio

Anode Recycle Ratio must be increased to compensate.

Target for propane: O/C = 0.6, ARR = 3-4



750°C

CPOX O/C	Minimum Recycle Ratio	
	FU 50%	FU 75%
0.4	1.6	0.94
0.8	0.44	0.3
1.2	0	0

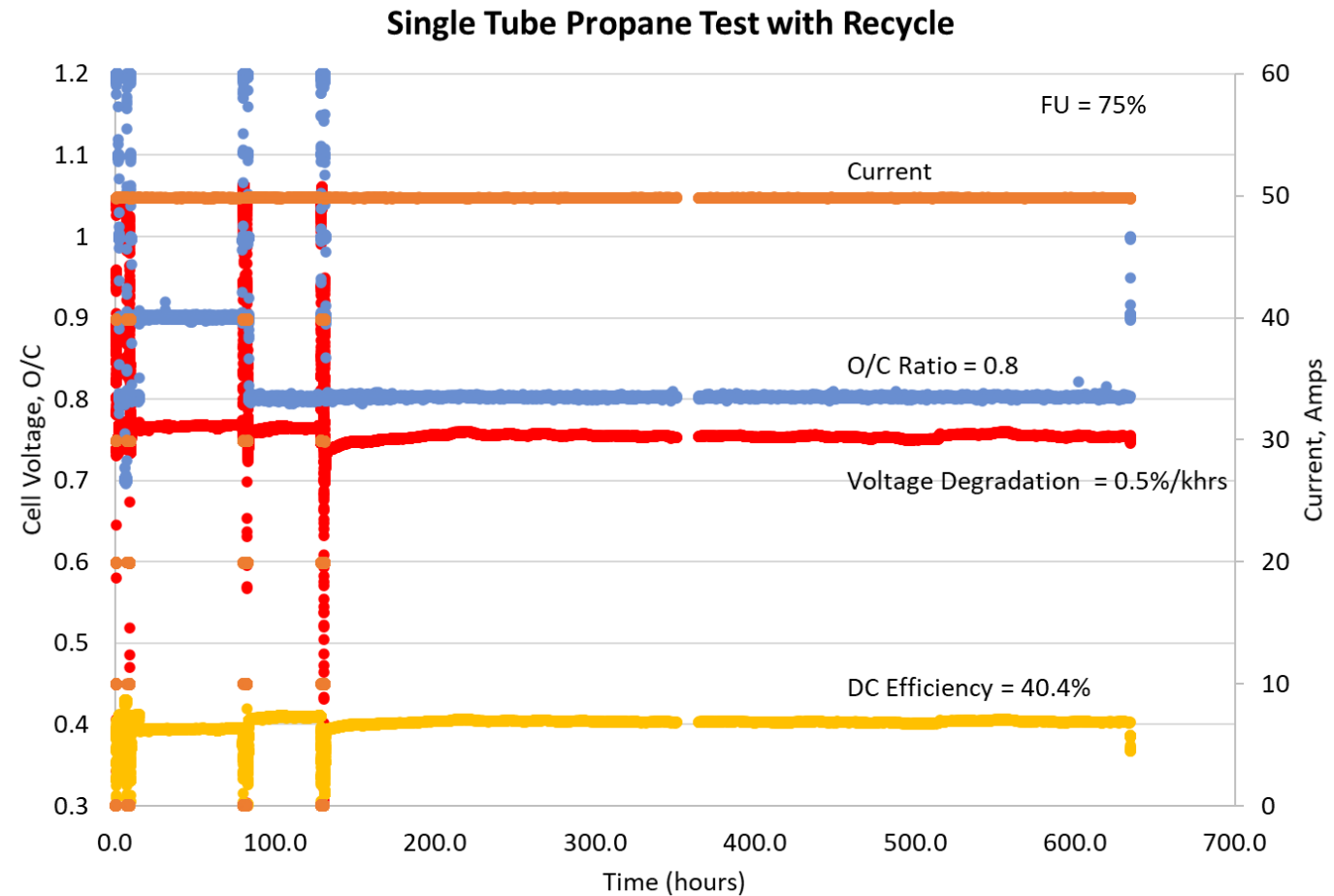
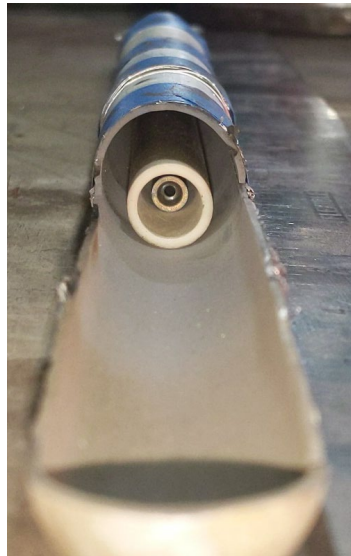
650°C

CPOX O/C	Minimum Recycle Ratio	
	FU 50%	FU 75%
0.4	8	2.5
0.8	2.25	1.08
1.2	0.6	0.36

2.5 Internal Reformer Validation

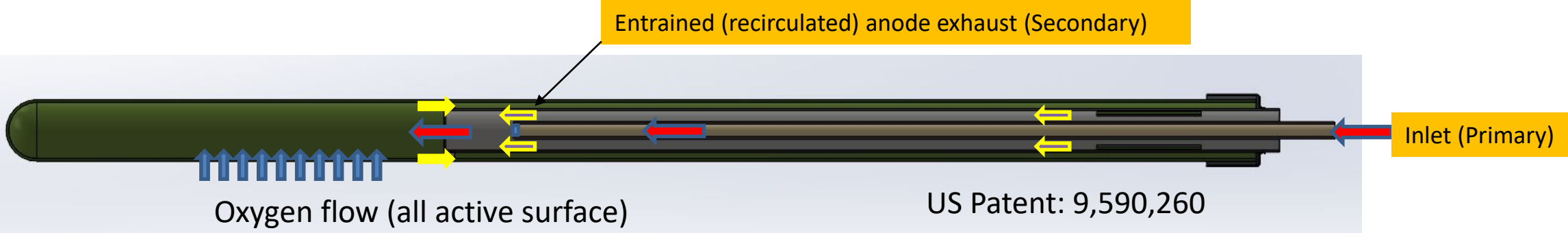
Previous Results

- Proof of concept completed in 2021
- Demonstrated carbon free operation at O/C = 0.8 for >500 hours
- Arrangement was not DFM friendly

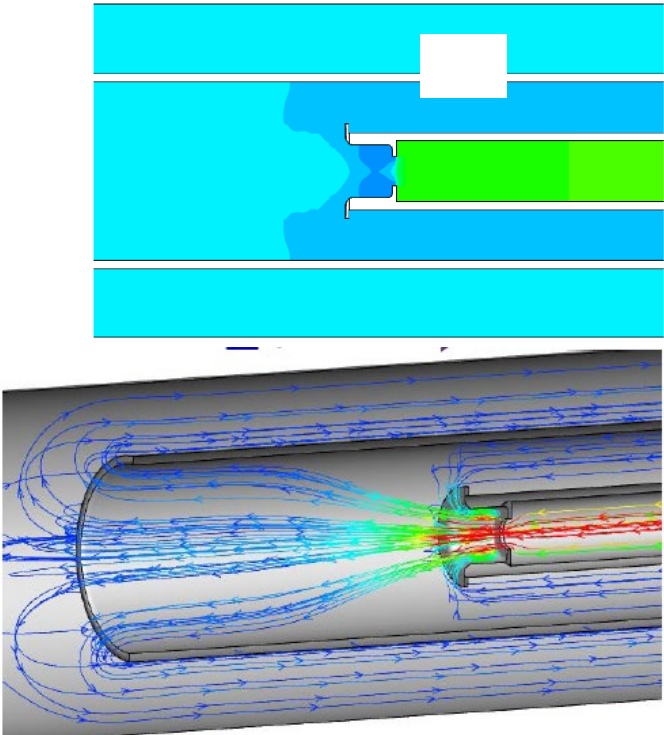


2.5 Internal Reformer Validation

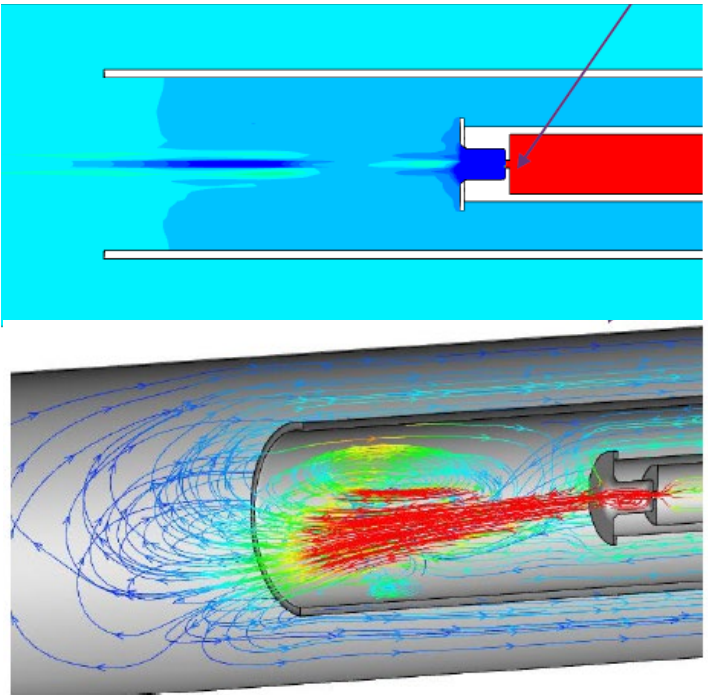
CFD Modeling – shows path to higher ARR



0.07" Orifice
Velocity = 72 m/s
ARR = 0.2

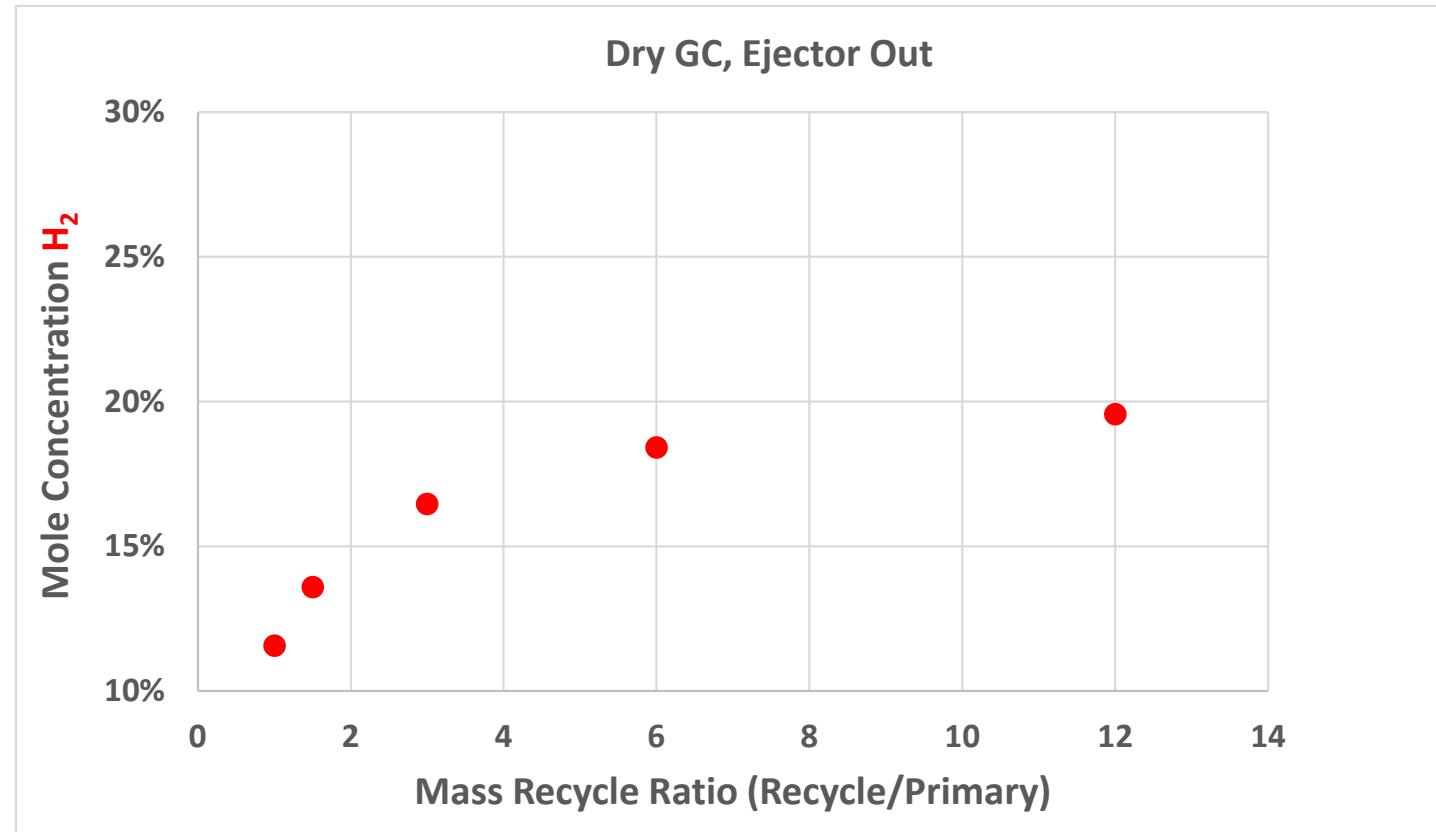


0.02" Orifice
Velocity = 830 m/s
ARR = 3.2



Ejector Testing Plan

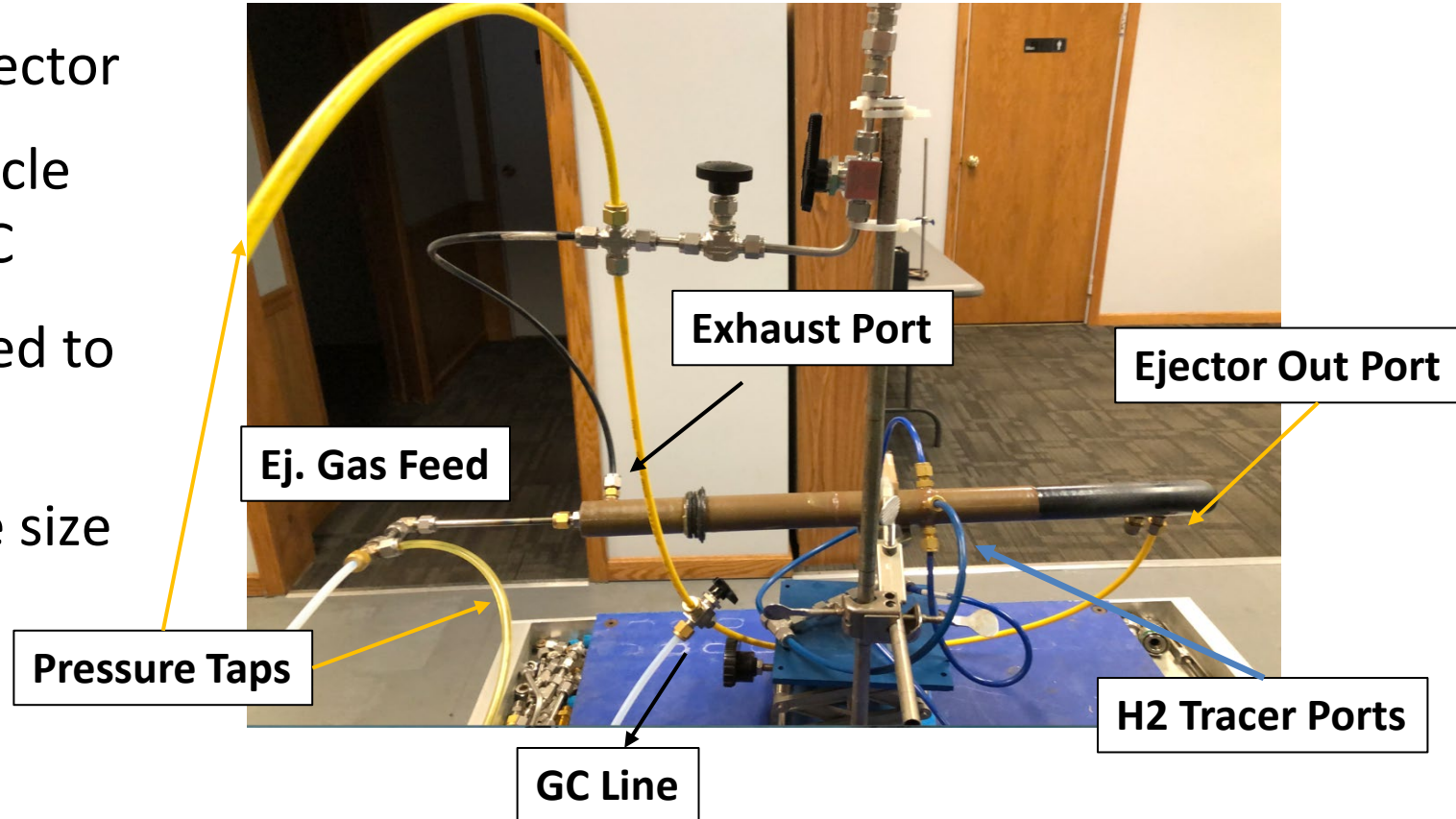
- Cold test with tracer gas and GC to confirm optimum orifice size and geometry
- Hot performance test for insertion depth to maximize performance
- Long-term (500-hr) test to confirm no carbon formation
- Bundle implementation for 2.5kW test



Cold Flow Test: Air/CO₂/H₂

Cold Recycle Flow Testing Set-up

- Feed actual fuel/ N_2 blend into ejector
- Use H_2 as tracer to calculate recycle based on H_2 concentration via GC
- Estimate ejector pressure required to achieve adequate recycle rates
- Provide a basis to scale up orifice size for given O/C and operating temperature



Cold Anode Recycle Test Results

Recycle rates of 8 - 10 are possible

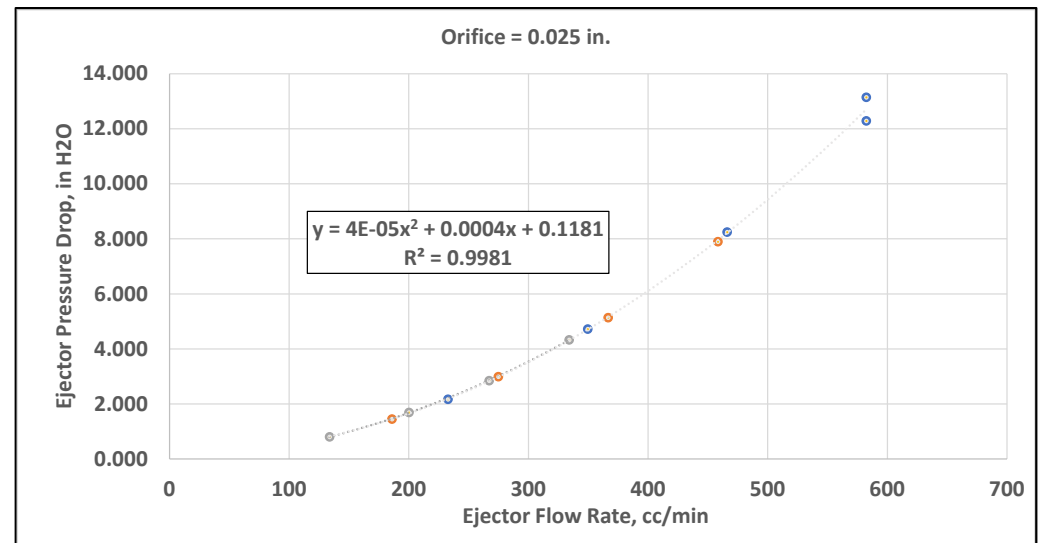
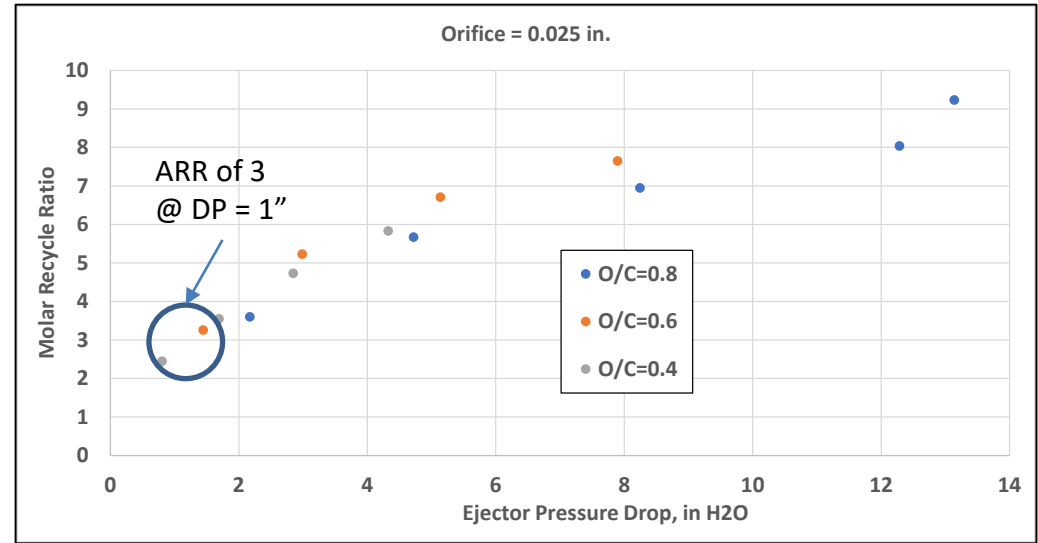
- With pressure drop less than 10 in H₂O

For recycle ≥ 2 , cold flow test show:

- Min ejector pressure ~ 1 in. H₂O
- 50% to 100% load of 2-10 in H₂O

Hot Flow Testing will occur in single cell test stand to:

- Verify orifice size at the anticipated operating conditions
- Assess potential issues with coke formation or reaction exotherm

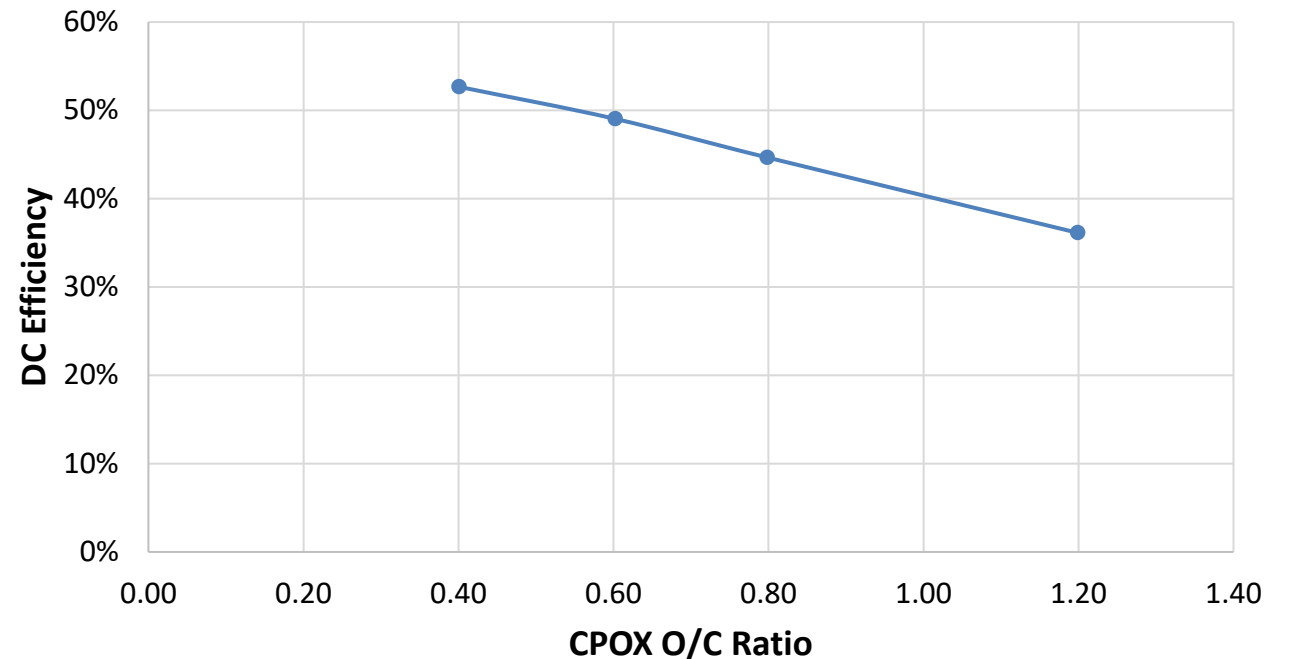


Single Tube Tests with Propane



US Patent: 9,590,260

Propane Fuel, 50 Amps



Concept designed which can be more easily produced

Single-cell testing confirms good efficiency with low O/C operation

Long-term operation at low O/C now ongoing

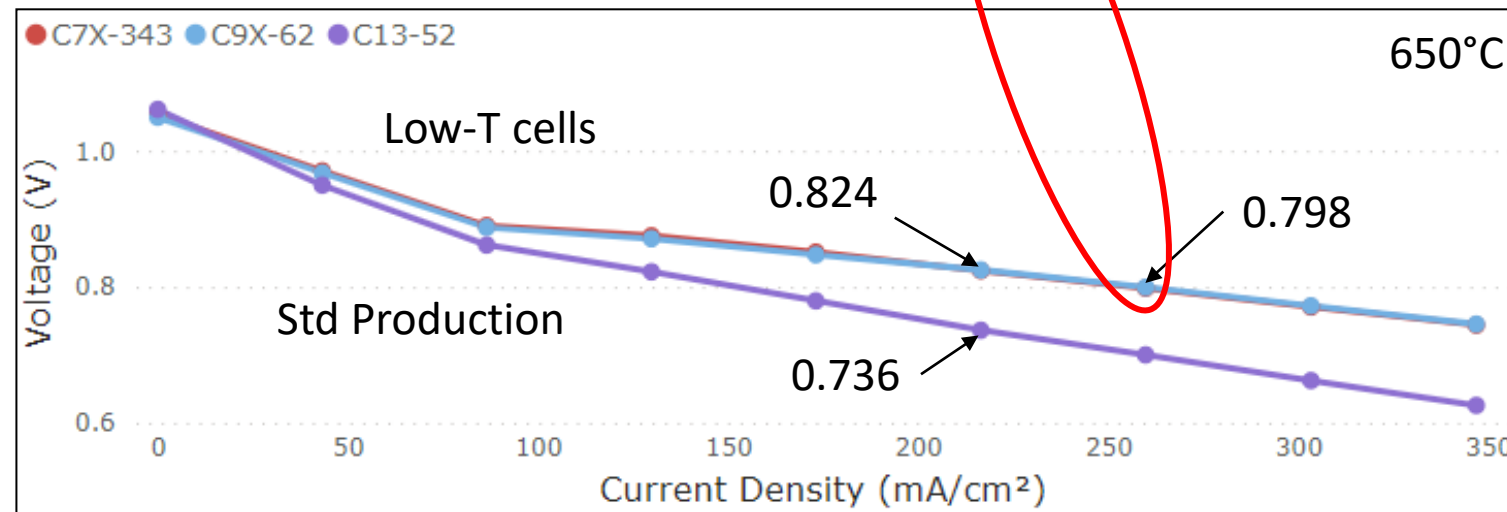
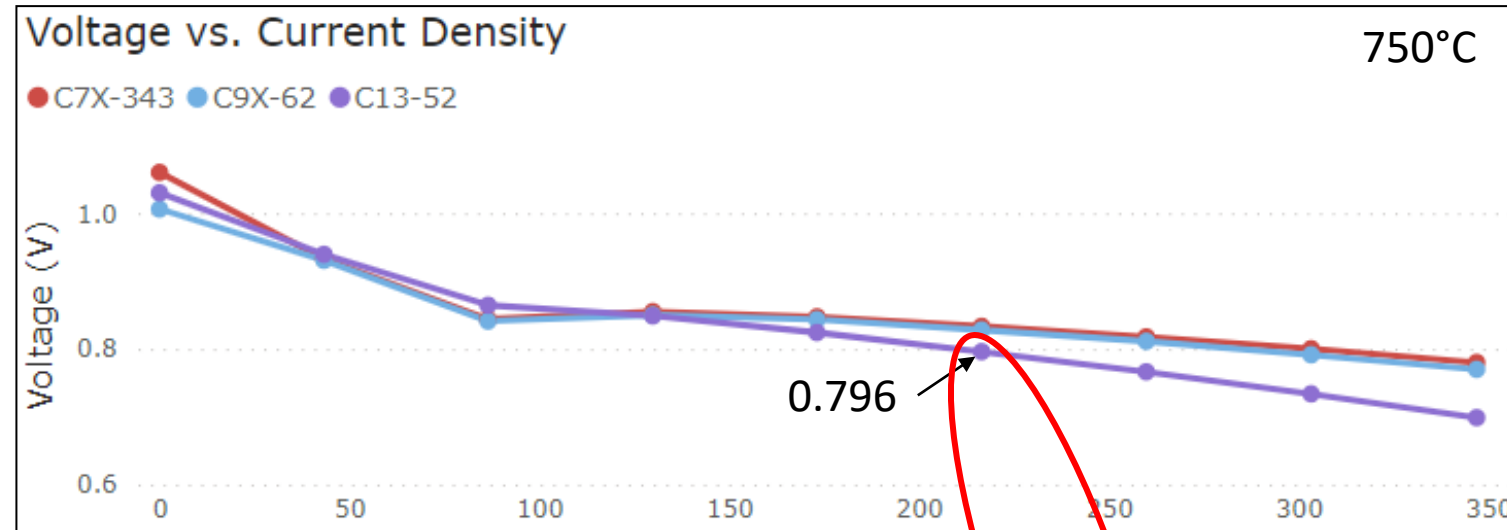
Bundle configuration being implemented

Task 2.6 Result of Combined Effects

Final Process

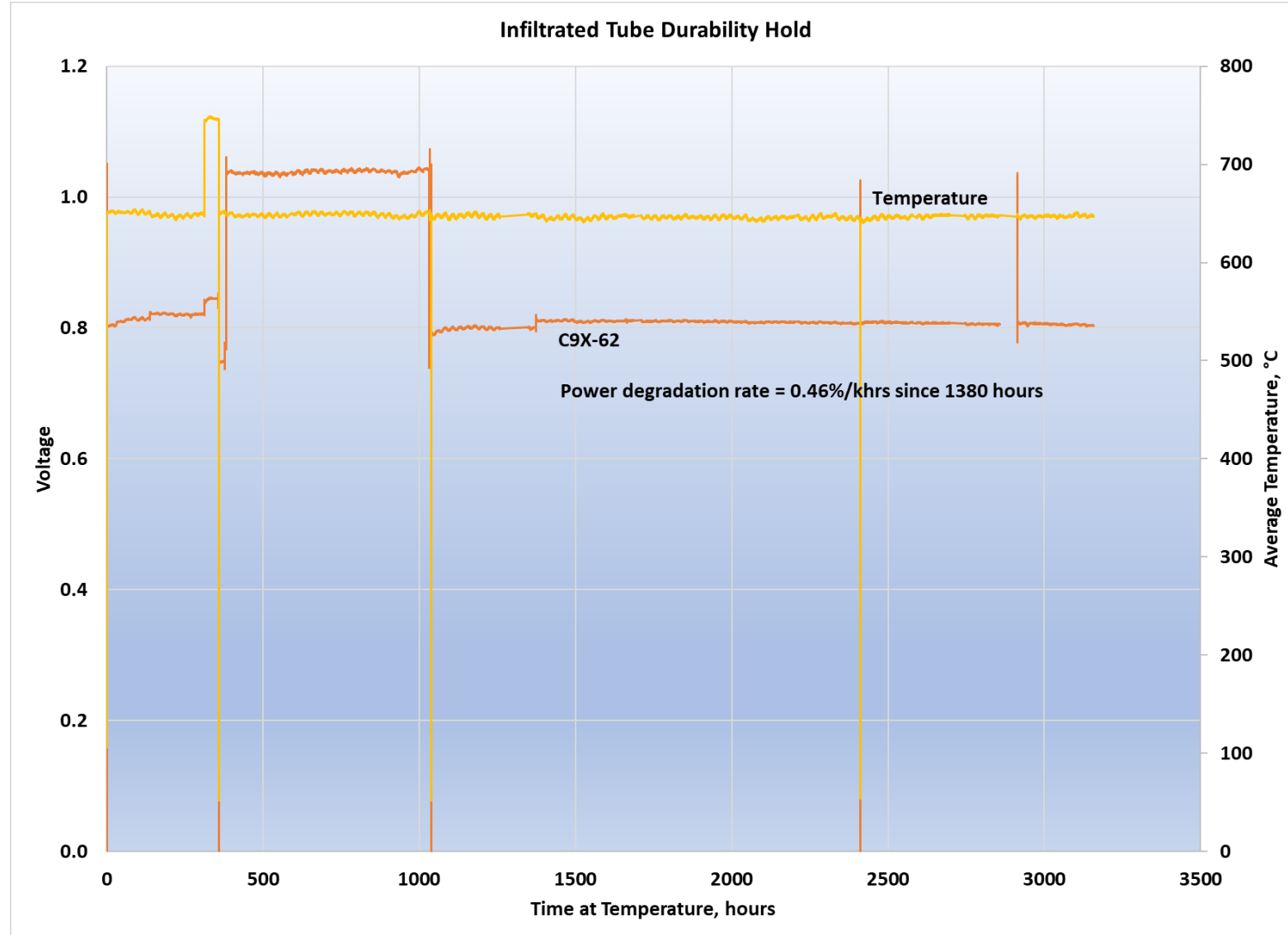
- Cells reduced
- Anode/Cathode infiltration
- Thermal treatment to 400C
- Anode Cu wash
- CCC screen print

Improved tubes generate 20% more power than standard tubes at same voltage, yet at 100°C lower temperature



2.6 Combined Testing – Single Cell

- Operation at 650°C
- Current = 50 amps
- FU = 75%
- Power degradation: <0.5%/1000 hours





2.6 Combined Testing 5000-hour System Test

Commercial bundles operation 750-775°C
Targeting low temperature operation 650C-700°C

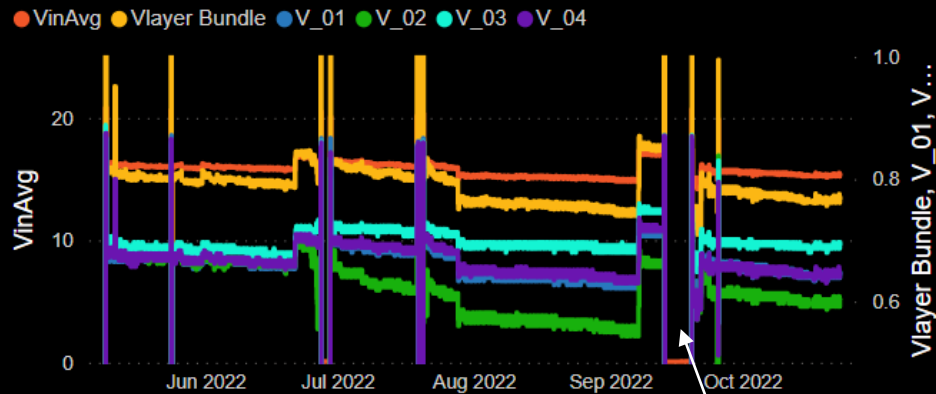
Test started week of 5/9/2022
Scheduled completion of 5000 hrs Dec 5, 2022

20 tube bundle in a full system
Capable of 625W rated power

DC efficiency > 40%

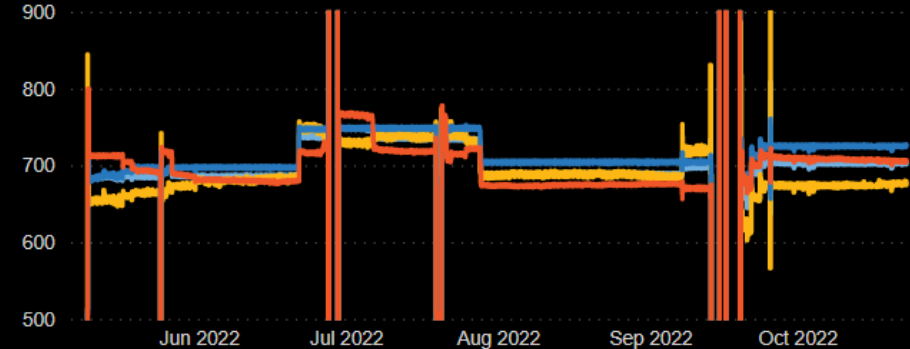
5000 Hour System Test Progress

Bundle Voltages ~3800 hours on load

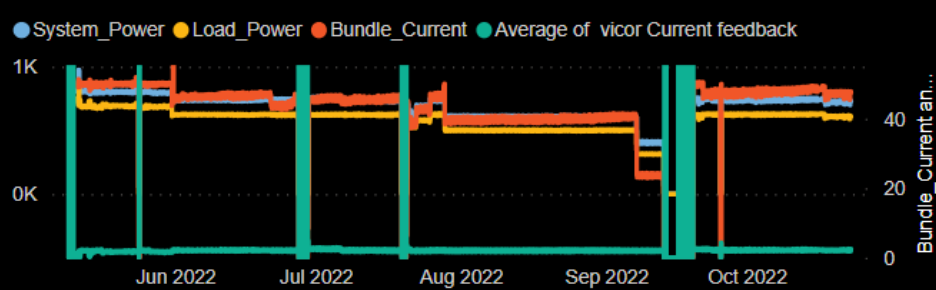


Bundle Temperatures

687 - 700°C Average

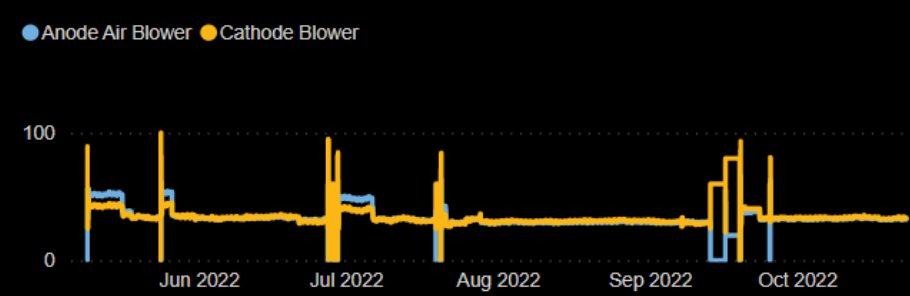


System_Power & Load Power

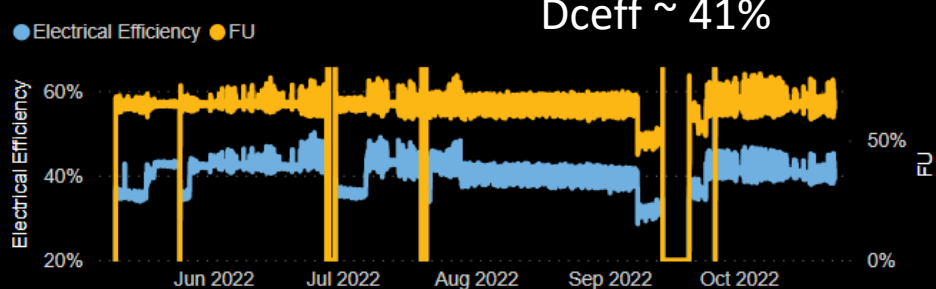


Bundle Repair

Blower %

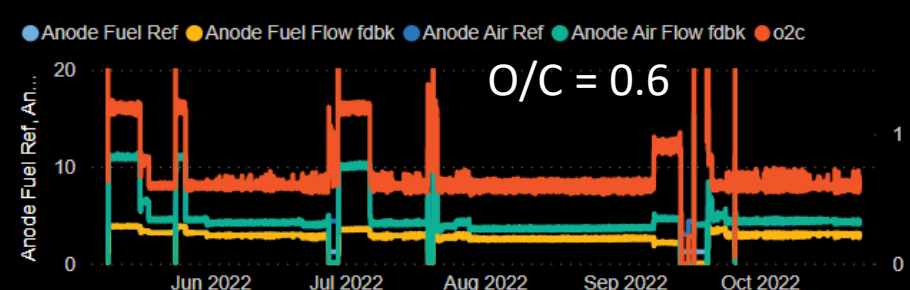


Efficiency & Utilization



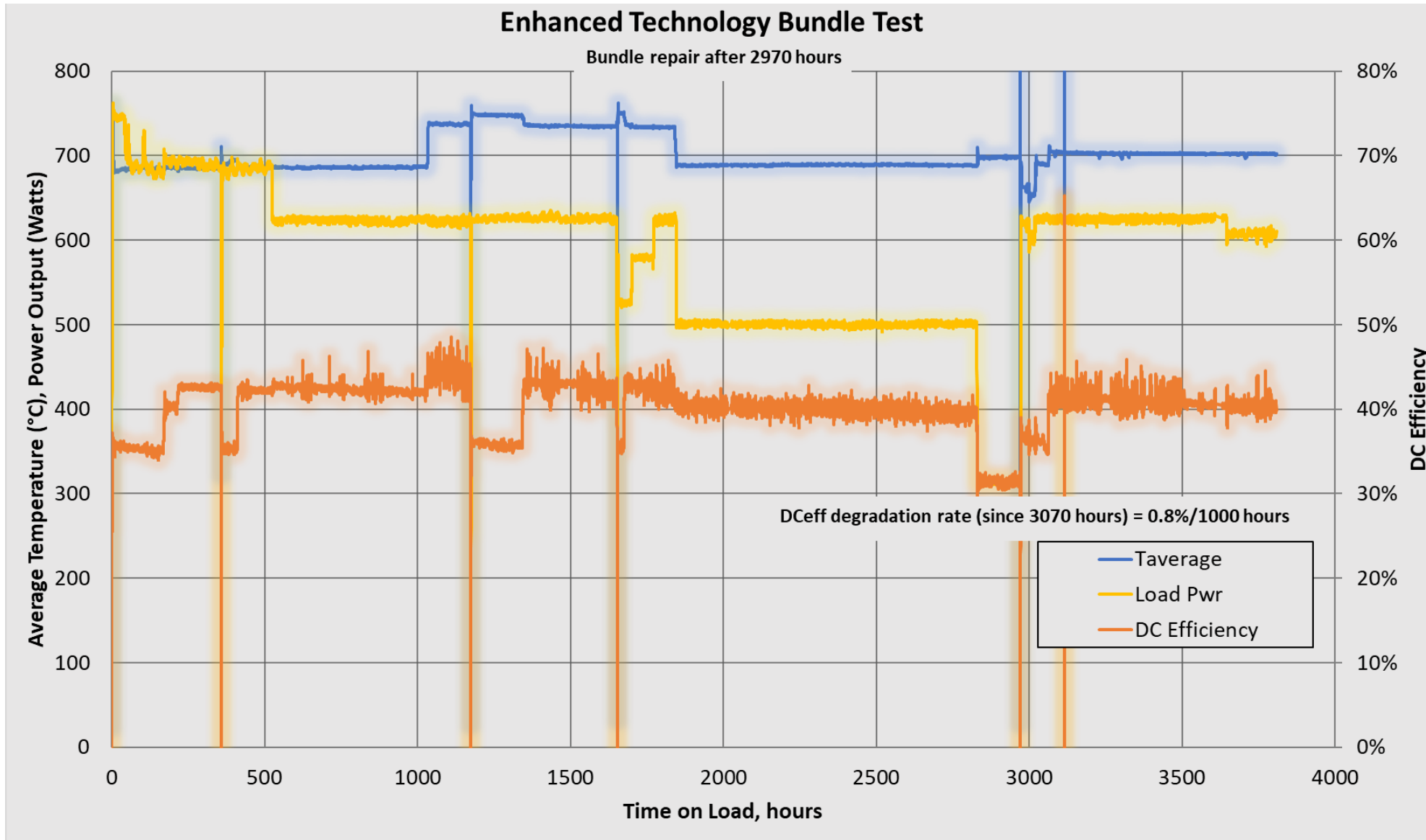
Dceff ~ 41%

Anode Fuel Flow fdbk



O/C = 0.6

5000-hr System Test Performance Summary



5000-hour System Test Plan

500 hours at max load (50 amps) ✓

1000 hours at 100% load (625W) ✓

500 hours at 100% load, FU = 75% (625W)

500 hours at 80% load (500W), 680C ✓

100 hours at 50% load – O/C = 1.2 (313W) ✓

Bundle layer 2 repaired after 2970 hours

500 hours at 100% load (625W) ✓

→ 500 hours at 100% load, FU = 75% (625W)

500 hours at 80% load (500W), 680C

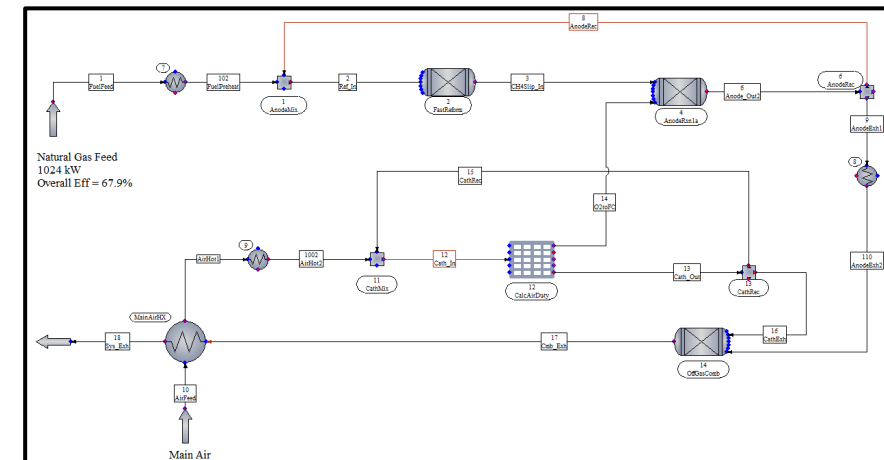
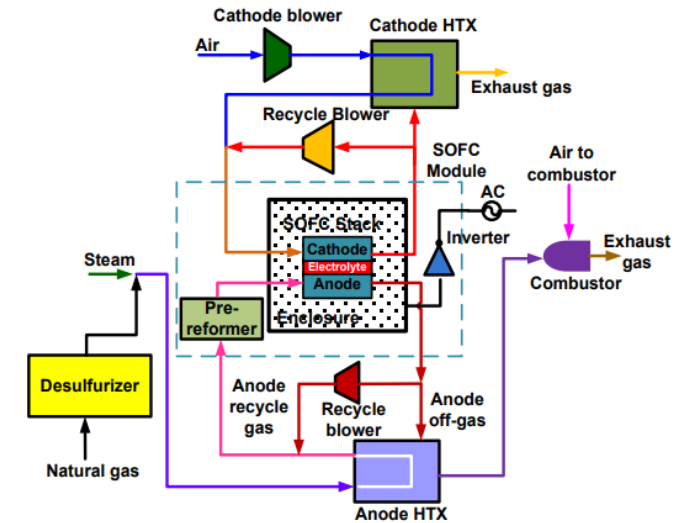
100 hours at 20% load – O/C = 1.2, FU < 50%

500 hours at 100% load (625W)

On track to complete 5000 hours by end of 2022

Task 4.4 – Megawatt Performance, Cost, and Reliability Feasibility

- Modeling 1 Megawatt using ChemCad
 - Modeling based in DOE system. “Distributed Generation as a Potential Market for SOFC”
 - Simulate DOE baseline case as benchmark
 - **Chem-Cad Model successfully matched fuel utilization at specified efficiency.**
- Mechanical Design of 5 to 10 KW Module
 - Building block for 1 MW system
 - Use for costing purposes



Model Result: FC Condition @ 90% Utilization

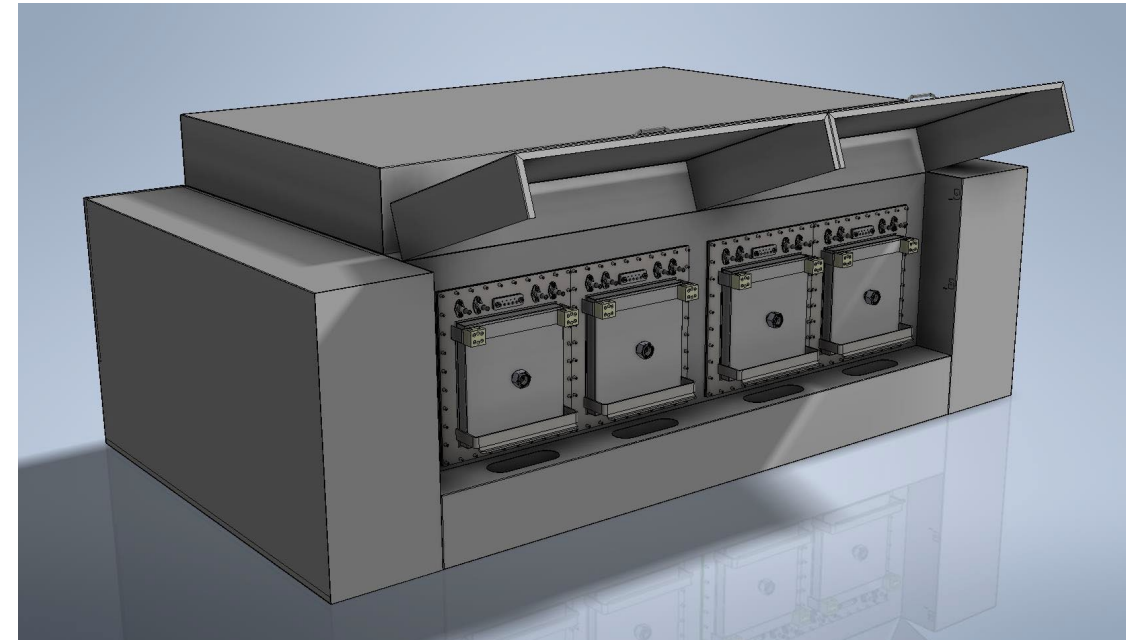
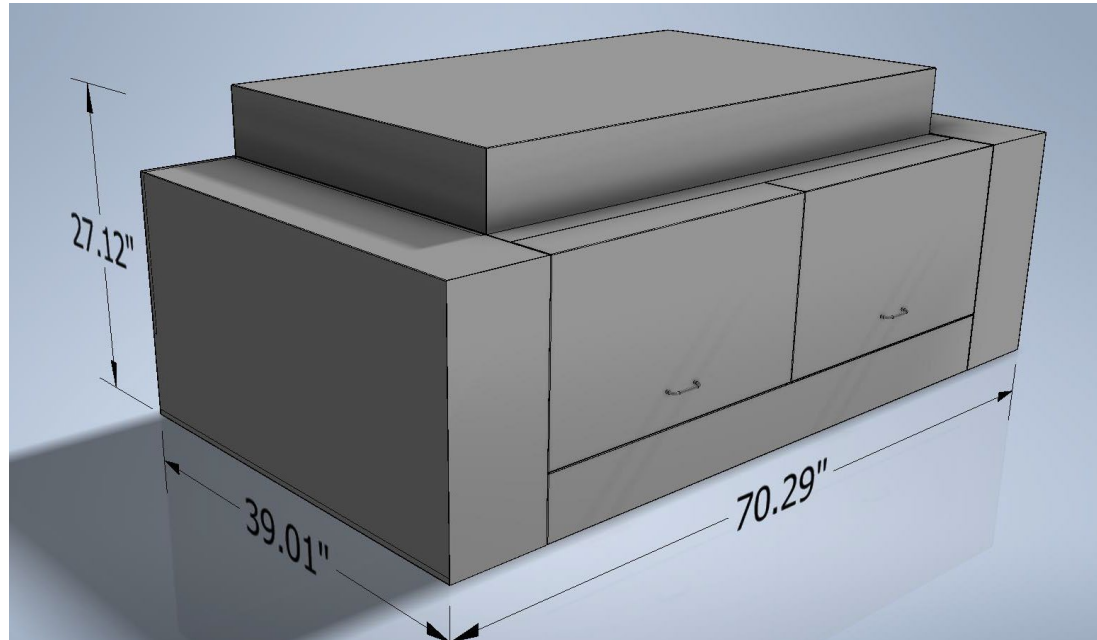


Property	Inlet	Outlet
Composition		
N2	0.53	0.52
CO	16.17	4.44
CO2	17.70	29.53
H2	38.54	12.55
H2O	26.77	52.96
CH4	0.29	0.001
Average Temperature, °C		750
Current Density, mA/cm ²		400
Vop, volts		0.83
Average Vrev, volts		0.927
Average ASR, ohm-cm ²		0.242

SPS legacy cells operate at 210 mA/cm² nominally

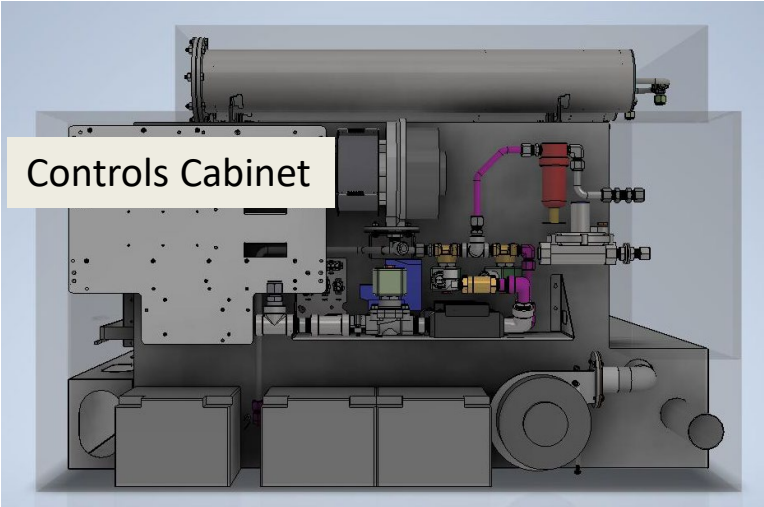
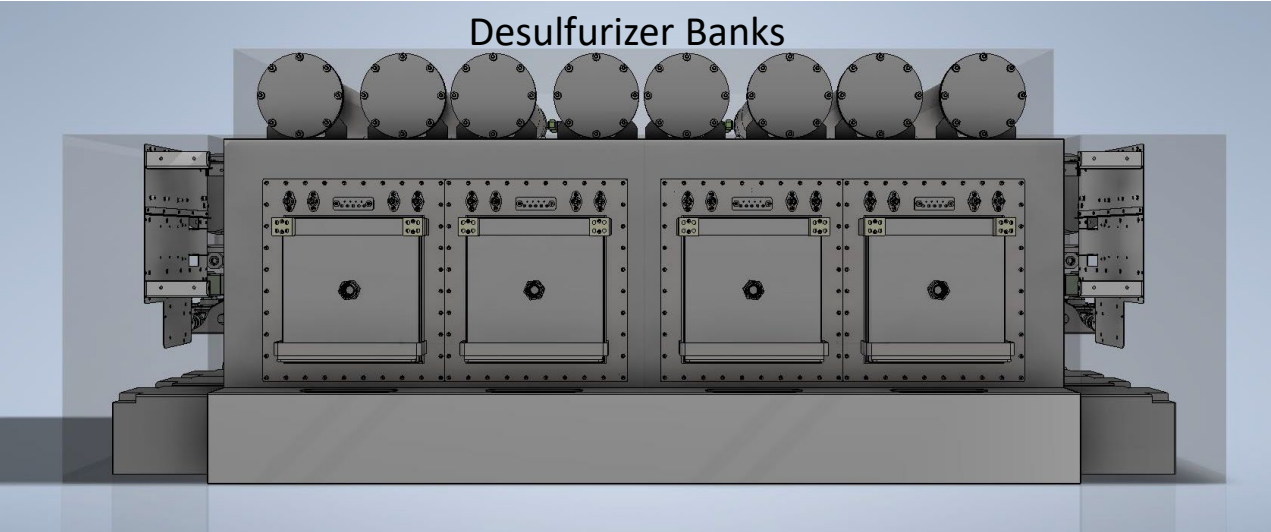
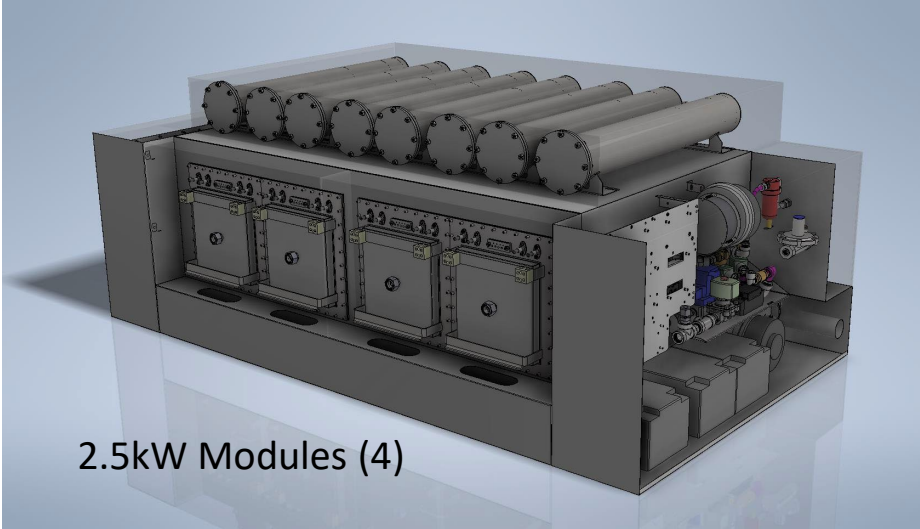
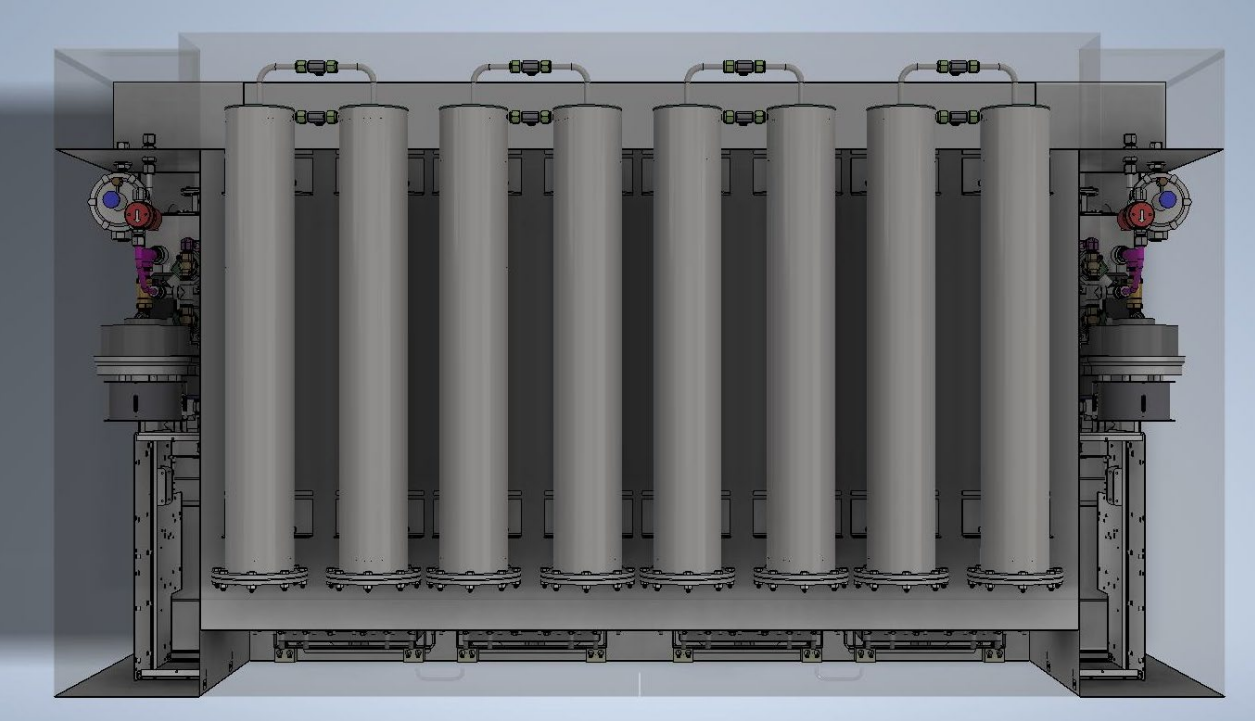
Projected voltage of 0.75V at 400 mA/cm² based on enhanced performance cells

SPS 10kW System Concept



**Concept based on 2 (two) parallel 5kW system, each using 2 (two) 2.5kW modules
Desulfurization on the top, Controls on the side**

SPS 10kW System Concept



Summary

- Improved fundamental cell technology has been demonstrated at single tube and system scales which has improved power output by 20% while operating at 100°C lower temperature.
- SPS patented internal recycle arrangement has been further developed to operate heavier hydrocarbon fuels directly in a compact, high efficiency system.
- System testing is ongoing to prove out long-term durability of cell improvements.
- System designs at 5 and 10kW are being developed for cost study and will form the basis for near-term commercial opportunities.

Acknowledgement



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