



# Low Cost, Large Area SOEC Stack for $H_2$ and Chemicals

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**Develop and Build an Efficient 5 kW Solid Oxide Electrolyzer and Demonstrate Operation under** Simulated, but Commercially Relevant Conditions

- Develop and build an efficient SOEC and demonstrate operation under simulated, but commercially relevant conditions
- Design electrode cassette modules that include a large 300 cm<sup>2</sup> active area cell, a metal frame and channels for gas flow.
- Develop and employ optimized materials to provide the best possible combination of performance, lifetime and cost.



# **R&D to Reduce Stack Cost and Improve Durability**

## **Technical Barriers and Gaps**

HTE stack performance and durability remains understudied due to industry proprietary R&D: Stack durability is rarely reported Cost at scale is not known Commercially relevant repeat units are not available





PNNL has established cells/stacks fabricating and modeling capabilities and expertise from multiple DOE SOFC R&D programs and private investments



| 5                     |                              |
|-----------------------|------------------------------|
| r Stack Goals by 2025 |                              |
| tal Cost              | \$100/kW                     |
| cy (LHV)              | 98% at 1.5 A/cm <sup>2</sup> |
| Lifetime              | 60,000 hr                    |
|                       |                              |

## **PNNL Testing Approach: Button Cells, Full Size Cells,** and Stacks Pacific Northwest

## High throughput button cell testing (~70 cells)

## Larger size planar cell testing (2+6)

Relevant steam utilizations

Temperature gradients

High currents

Interconnect





active area

is 2-4 cm<sup>2</sup>

- Materials screening
- I-V and EIS measurements
- $pH_2O=1-99\%$ ; impurities

without metal IC

with and



active area is 16 cm<sup>2</sup>



- Seals

- Durability

## 1-5 kW short stack testing (3 platforms)



## Components



Steam delivery and utilization Heat management



# Solid Oxide Cell Manufacturing

Pacific Northwest

## **Powder Synthesis and Processing**

## **Fabrication Techniques**

 Tape casting, screen printing, compression molding, injection molding, isostatic and uniaxial pressing, slip casting, laser cutting, roll lamination

## Thin Film Techniques

• Spin coating, PVD, ALD, PLD, slurry and solution coating, ultrasonic spray coating

## Sintering in air and environment upto 1500°C

## **Seals and Protective Coating**





## *Glycine – nitrate powder synthesis*





## Hot roll laminator







Screen Printer



# **Cell Production of Different Sizes Established**



Pacific

# PNNL produces cells for H2NEW

- Ni-YSZ electrode-supported planar cells have been selected as standard reference cells
- Successfully produced large cells to reduce stack part count, the number of interfaces in stack, and cost
- Decreased YSZ thickness to reduce firing steps, cost, and improve the performance
- Developed a batch fabrication process to minimize the variance between separate cells
- Initiated the development of QA/QC procedures
- Initiated electrode microstructure optimization to improve performance and durability







# **Baseline Performance Obtained at 750°C at 1.3 Volt** in 50% Steam Using Multiple Repeats for 6,000 hours



- Demonstrated in house reproducibility
- Demonstrated cell stability; average degradation rate is below 17 ohm cm<sup>2</sup> per 1,000 hours
- Detailed EIS and DRT analyses attributed degradation during break-in period to two processes in 1 kHz–10kHz and 100 Hz–1 kHz frequency ranges, likely associated with diffusion phenomena in the oxygen electrode



**Probing for Degradation Mechanisms: Post-Test Cell** and Component Characterization by SEM/EDS, **EBSD, STEM, APT** 

# Hydrogen Electrode

# No Ni coarsening or migration after 3,000 hours at 1.3V at 750 and 800°C











**Triple-phase boundary** determination using **PNNL modeling tools** 



**Probing for Degradation Mechanisms: Post-Test Cell and Component Characterization by** SEM/EDS, EBSD, STEM, APT

# **Oxygen Electrode**

## **Co inconsistency**









Fe,Co composition becomes richer in Fe; needs more statistics to confirm

## **Sr migration**



# **Gd diffusion into YSZ**



# Thin Film Deposition of GDC and YSZ



- Tested cells with and without pre-sintered YSZ electrolyte after YSZ and GDC sputtering
- Ohmic losses were reduced with sputtered GDC
- Observing more degradation that needs to be understood
- Not SrZrO<sub>3</sub> related



# **Assembled and Tested 14 SOEC Stacks** Using 300 cm<sup>2</sup> Active Area Cells

- Successfully produced multiple well-sealed cassettes with large 300 cm<sup>2</sup> active area electrode-supported SOEC cells
- Fabricated all other components
- Applied protective coatings to the metal parts and metallic interconnects to prevent corrosion and chromium volatility
- Assembled and tested 14 short stacks of different sizes, ranging from 250 W (1 cell) to 1 kW (4 cells)
  - Optimized cell fabrication and sizing procedures to match the metal window frames
  - Optimized welding and sealing steps
  - Improved air side contacts
  - Addressed cassettes shorting





## 1 kW SOEC stack with 300 cm<sup>2</sup> active area cells



# **Used Predictive Modeling to Address the Initial Stress State in the PEN from Sintering and Sealing**







- ANSYS Initial State process employed
- Assessed principal stresses in anode, electrolyte, and cathode H<sub>2</sub> side stack seal
- Identified elastic strains from the elements in the PEN after running simulations of PEN sintering and PEN sealing



Predict/ID key processing windows & tolerance: tested different plates,

# **EERE HFTO TA**

thicknesses, weights to obtain the best contacts while keeping the weight down



# **Demonstrated Several Full Thermal Cycles**



Elapsed Time Single Repeat Unit Stack 200-250 W in 80% Steam at 750°C Leak rate below the detection limit, hermetic seals OCV=0.893 V, constant throughout the test

## -Voltage -Current



# **Stack 12 Results**

- Good initial performance with some initial degradation with time.
  - 90% steam and ~ 50% steam utilization
- Total run time of about 350 hours
- Successfully thermally cycled
- Developed a short between cell 3 and 4 shortly after the third thermal cycle





Stack 12 Second Heat up Data



# **Sealing Procedure Improvements**

- Issue: low yield after the celllacksquareto-window-frame sealing procedure; about 50% failure rate
- Improvements: replaced dispensed glass by tape casting and improved load uniformity on the cell; yield is now very close to 100%; assemble is easier
- Made many changes to prevent shorting







# **Stack Structural Integrity and Reliability Analysis Predicts Low Failure Probability**

- Designed stack components and validated the design using thermomechanical analysis for structural integrity to predict stack and enclosure level displacements, stresses and investigate any CTE mismatch issues
- Optimized the meshing process of computational grids to reduce the computation time
- The reliability analysis mapped potential failure probabilities concentrated locally to specific areas of the cell depending on operating voltages and operating conditions



J. Bao et al, J. Electrochem. Soc. 2022, 169, 054523





# Investigation of Solid Oxide Co-electrolyzer **Performance with Deep Neural Network**

- The PNNL developed multi-physics solver (SOFC-MP<sup>[1][2]</sup>) for SOFC has been upgraded to support solving co-electrolysis in 2D and 3D scheme.
- The solver predicts the co-electrolysis performance matching the experimental measurement for button cell at various cell operating conditions.



Voltage - current density relationships for six fuel compositions

Current density versus  $CO_2/H_2O$  ratio at five cell voltages

[1]: Lai, K., et al., Journal of Power Sources, 2011. 196(6): p. 3204-3222 [2]: Pan, W., et al., Journal of Power Sources, 2013. 232: p. 139-151.

Bao et al., in preparation

# Pacific Northwest NATIONAL LABORATORY

# Investigation of Solid Oxide Co-electrolyzer **Performance with Deep Neural Network**

## Bao et al., POSTER SESSION

- SOFC-MP is applied to explore the performance of co-electrolyzer at different cell operating conditions with 5000 simulation cases, 300 cm<sup>2</sup> planar cells
- The deep neural network (DNN) is applied to construct the reduced order model (ROM)
- The DNN based ROM provides higher prediction accuracy than the conventional regression approaches
- DNN-ROM helps on understanding the response of the cell performance to the operating conditions

## Multi-Physics Modeling for Identification of Critical Factors in Solid **Oxide CO<sub>2</sub>-Steam Co-Electrolysis System Performances and Durability**

Dewei Wang, Jie Bao, Christopher Coyle, Olga Marina

### Abstract

A multi-physics modeling framework, which includes electrochemical and chemical reactions, mass transfer, and energy balance, has been developed and validated against experimental measurements to investigate the performance of solid oxide CO2-steam co-electrolysis (SOEC) under various operating conditions and cell designs. A deep neural networks (DNN) algorithm was employed to construct reduced-order models (ROMs) according to multi-physics simulations for SOECs to systematically investigate the SOECs' electrochemical performance for both small button cell and large, 100-300 cm<sup>2</sup>, planar cells, It was found that steam is electrolyzed with very high priority over CO2, even if there was only small fraction of steam in the feed

### Methodology

Numerical model SOFC-MP was applied to simulate SOECs with guasi-two-dimensional assumptions. considering three major reactions







Deep Neural Network (DNN) was implemented to construct reduced-order models (ROMs) as an alternative to the numerical model to reduce computational costs.



## Results

- Sensitivity studies of operating parameters
- Operating parameters' contributions to each output parameters were evaluated by DNN-ROM.
- Current density's variation was mostly contributed by cell voltage and temperature, 38.2% and 42.2%, respectively
- ΔCO/ΔH<sub>2</sub> ratio was highly dependent on CO<sub>2</sub>/H<sub>2</sub>O ratio. 51.64%.



Floure 3: Influence of each operating parameter on each output in a percent;

### Sensitivity studies of cell size & therma boundary

Internal temperature variation showed dependencies on fuel and air flow rates with larger-size planar cells



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### Current density dependencies on temperature, cell voltage and fuel ratio



Floure 4: Current density versus temperature, cell voltage and fuel ratio

## Product ratio $\Delta CO/\Delta H_2$ dependency on CO<sub>2</sub>/H<sub>2</sub>O ratio, temperature, fuel ratio and cell



### Degradation & Boudouard reaction in SOECs

Numerical model SOFC-MP has integrated several degradation mechanisms: Sr/Zr diffusion, Ni-coarsening, sulfur poisoning, and Boudouard reaction





Igure 8: Carbon deposition and n due to Boudouard



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# Investigation of Solid Oxide Co-electrolyzer **Performance with Deep Neural Network**

• DNN-ROM helps on understanding the response of the cell performance to the operating conditions



Current density variations at fuel flow/air rate of 120 and 1200 sccm. (a) versus  $CO_2/H_2O$  ratio and cell voltage at temperature of 750 °C; (b) versus CO<sub>2</sub>/H<sub>2</sub>O ratio at different voltages at temperature of 750 °C; (c) versus temperature and cell voltage with  $CO_2/H_2O$  ratio of 5; (d) versus temperature at different voltages with  $CO_2/H_2O$  ratio of 5.

System efficiency variations at fuel/air flow rates of 120 and 1200 sccm. (a) versus  $CO_2/H_2O$  ratio and cell voltage at temperature of 750 °C; (b) versus  $CO_2/H_2O$  ratio at different voltages at temperature of 750 °C; (c) versus temperature and cell voltage with CO<sub>2</sub>/H<sub>2</sub>O ratio of 5; (d) versus temperature at different voltages with  $CO_2/H_2O$  ratio of 5.

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- Assembled and tested multiple short stacks using 300 cm<sup>2</sup> cells
  - Successfully established stack repeat unit fabrication process
  - Established baseline performance of 1 kW stack in 80% steam at 750°C to understand impact of stack fabrication on performance and life
  - Thermally cycled SOEC stack with large cells
  - Obtained EIS data of a 1 kW stack and separate cells at 50-80% steam utilization.

# SAVE THE DATE



# May 2 - 3, 2023

## 5<sup>th</sup> Annual Advanced Water Splitting Technology Pathways **Benchmarking & Protocols Workshop**

Location: Sky Song: The ASU Scottsdale Innovation Center- Scottsdale, AZ

http://skysong.com/

## **Objectives:**

- Summarize progress over past years and identify opportunities for further collaboration
- Review, refine, identify test protocols and plan for validation
- Review, refine, identify, and resolve issues regarding technology roadmaps
- Identify, leverage, and align related international efforts



# 5<sup>th</sup> Annual AWS Benchmarking Workshop to Engage Technology Experts

- LTE Kathy Ayers, Nel
- **HTE** Olga Marina, PNNL
- **PEC** CX Xiang, Caltech
- **STCH** Ellen Stechel, ASU
- Protocol development for bench-scale, sub-scale and higher levels
- Face-to-face discussions about protocols
- Effective comparison of results
- Leverage international efforts to increase harmony across the field
- Wide community engagement
- Identify Round Robin verification sites
- Understand needs of the community •













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