

Isolated Single Metal Atoms Supported on Silica for One-Step Non-Oxidative Methane Upgrading

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Presenter: Dongxia Liu

Professor of Chemical and Biomolecular Engineering
University of Maryland, College Park

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Project Overview

- Funding

DOE (\$1.0 M) + Cost Share (\$292,515)

- Overall Project Performance Dates

March 20th, 2020 – March 19th, 2023

- Project Participants

PI: Dongxia Liu, University of Maryland

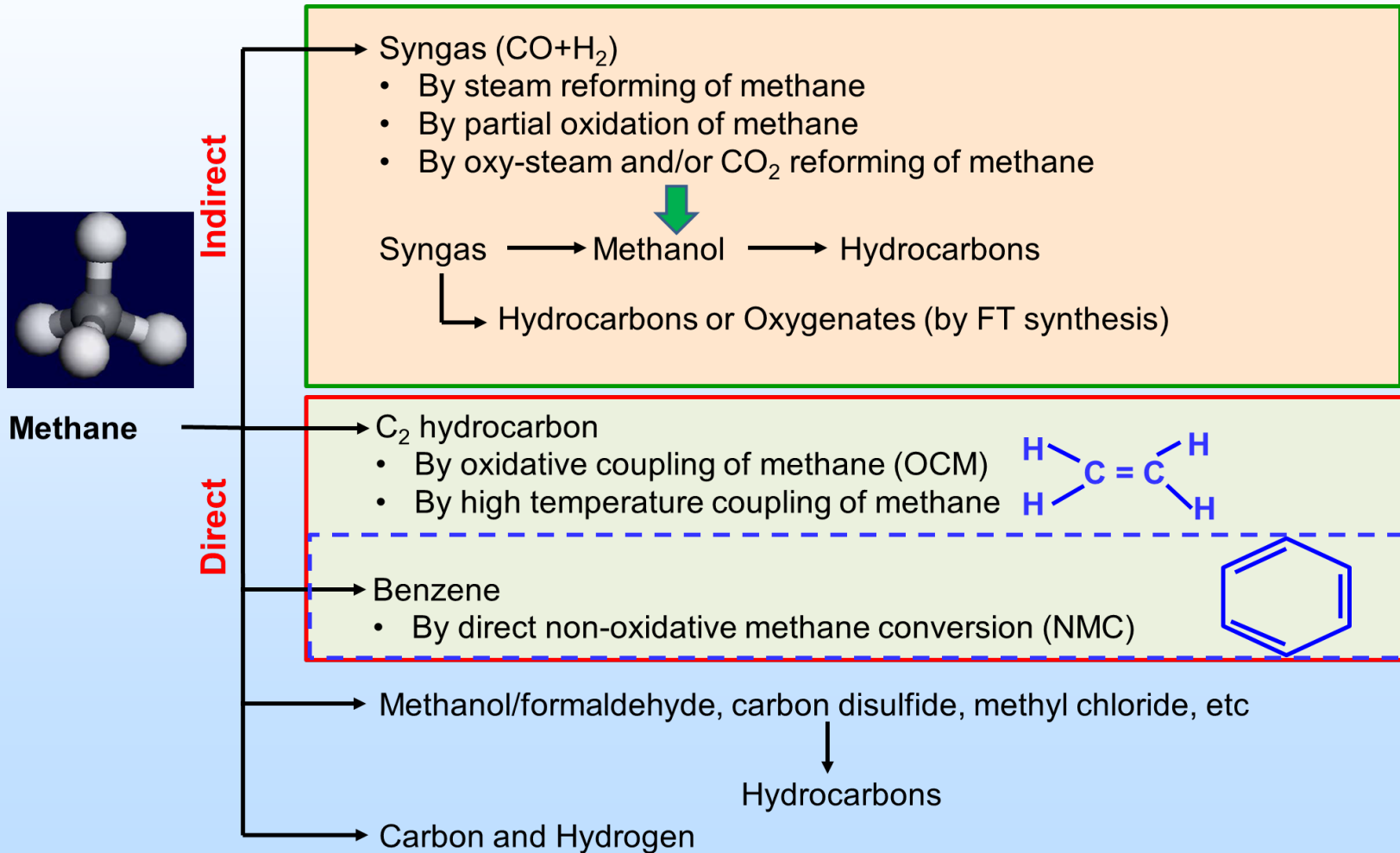
Co-PI: Dionisios G. Vlachos, University of Delaware

- Overall Project Objective

Create new, inexpensive, stable, active and selective catalysts to solve challenges in non-oxidative methane conversion (NMC) to produce hydrogen and higher hydrocarbons, and integrate catalysts in an efficient, scalable, and intensified NMC reactor.

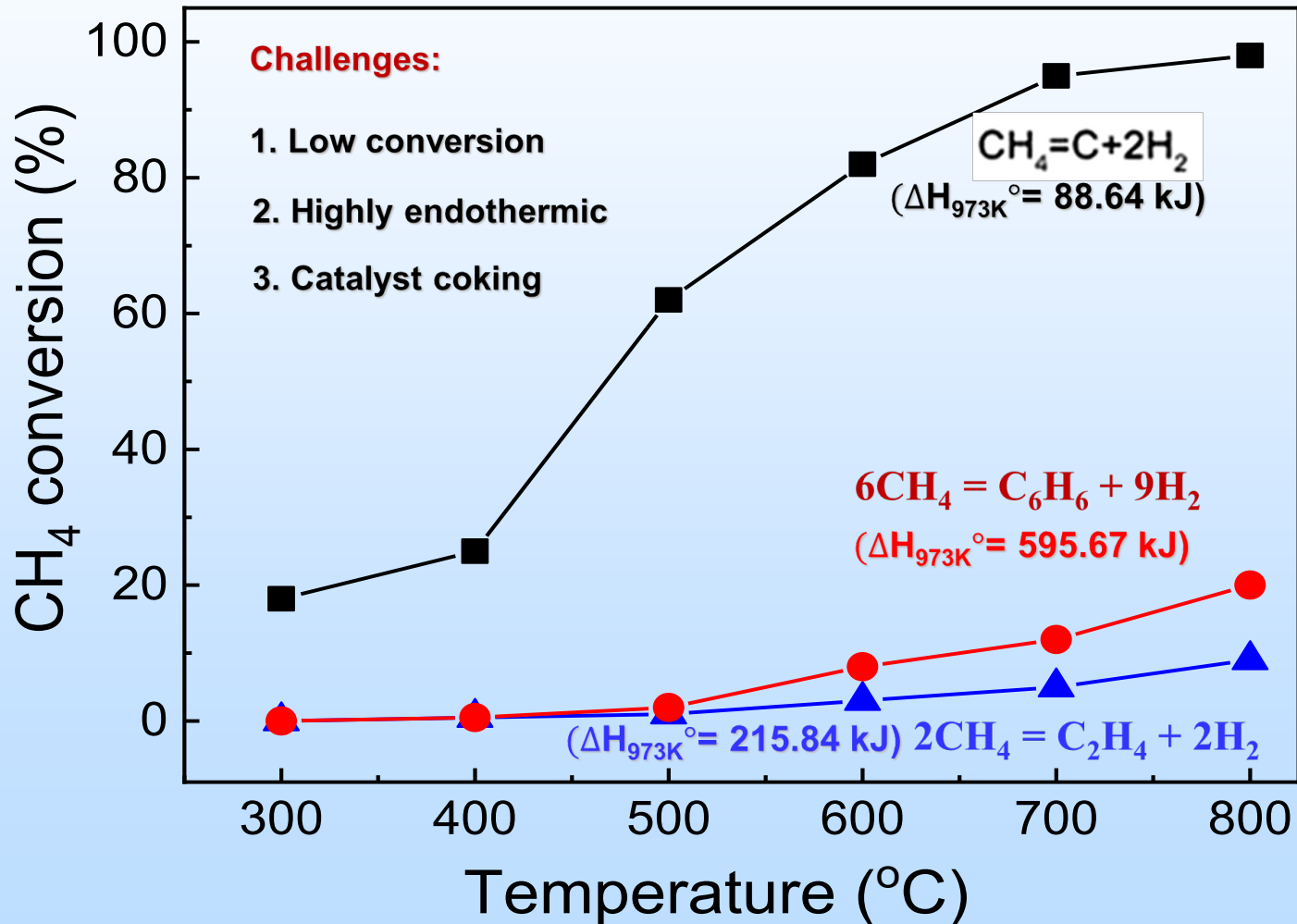
Technology Background

- Different methane conversion pathways



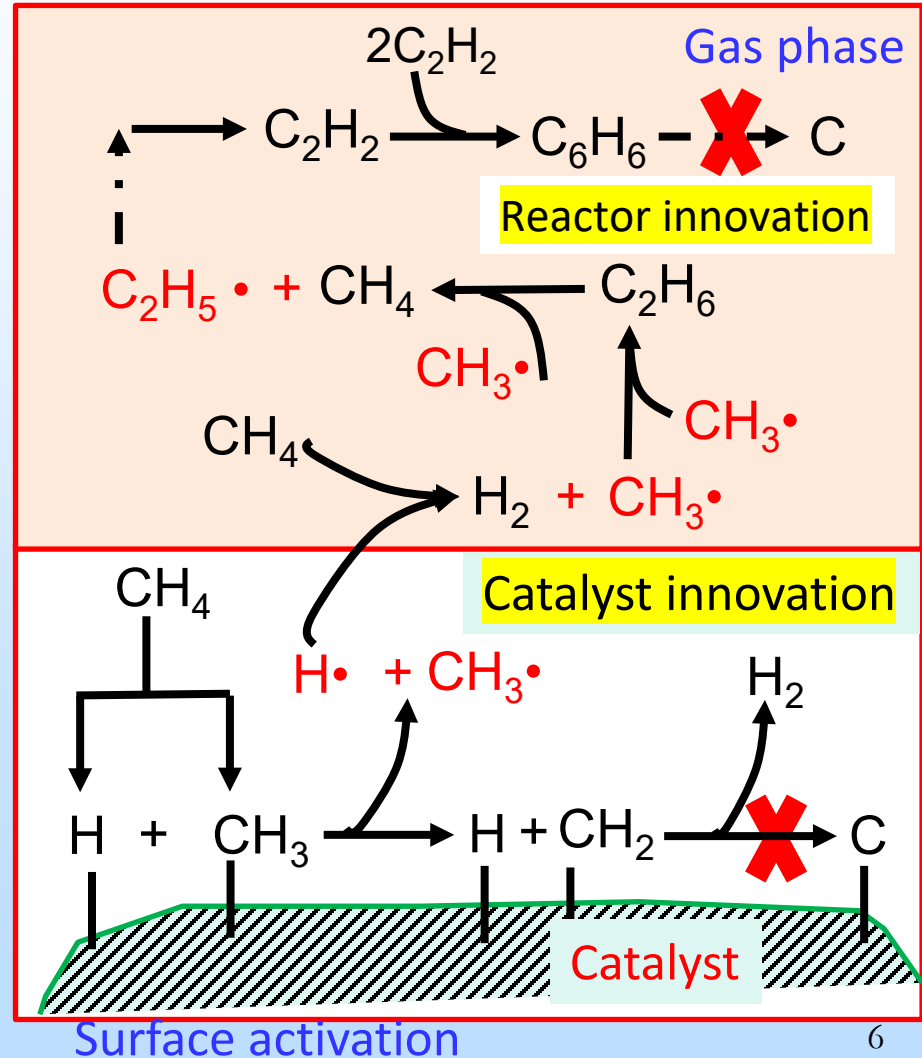
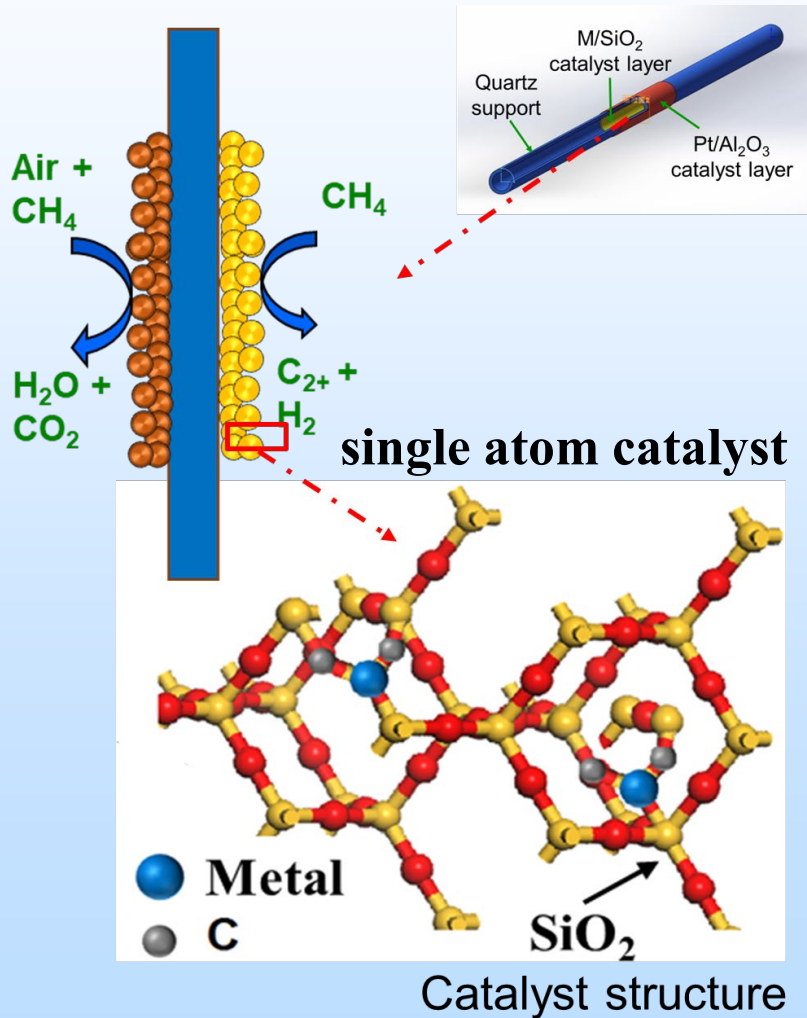
Technology Background

- Scientific challenges in NMC



Technology Background

- Both catalyst and reactor innovation to achieve high NMC performance

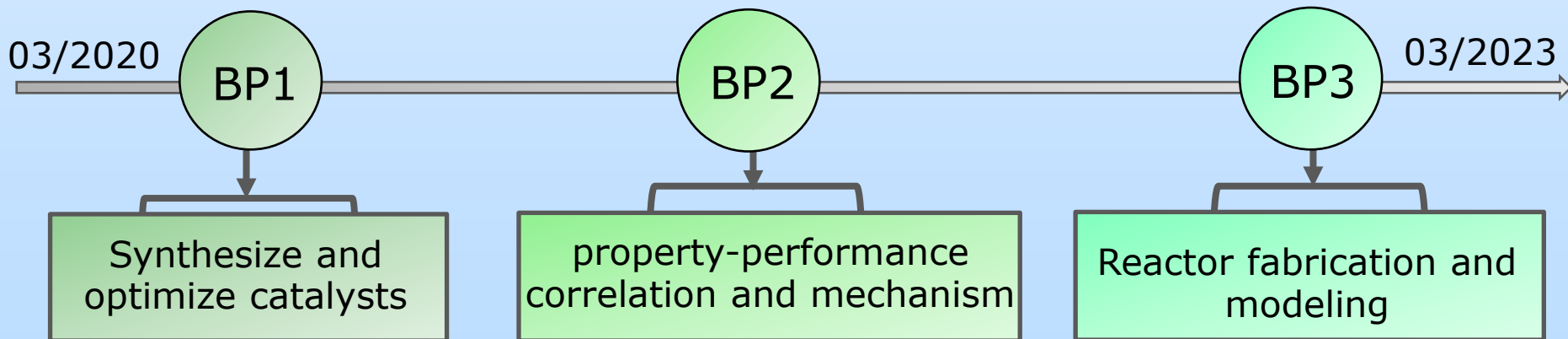


Technical Approach/Project Scope

a. Experimental design (or project steps and work plan)

- (1) **synthesize** isolated single atoms of various metals in a silica matrix to prove universality of these catalysts in CH_4 activation, provide data for catalyst optimization, and select the best one;
- (2) **probe** in situ and operando the surface and bulk structure of NMC catalysts using a wide range of experimental and ab initio thermodynamic techniques;
- (3) **understand** the reaction mechanism and kinetics by an integrated experimental and computational effort to quantify species and temperature, and use this information to create performance windows in an ideal reactor;
- (4) **demonstrate** an efficient prototype reactor that integrates knowledge and data from the above steps for NMC.

b. Project schedule



Technical Approach/Project Scope

c. Project success criteria

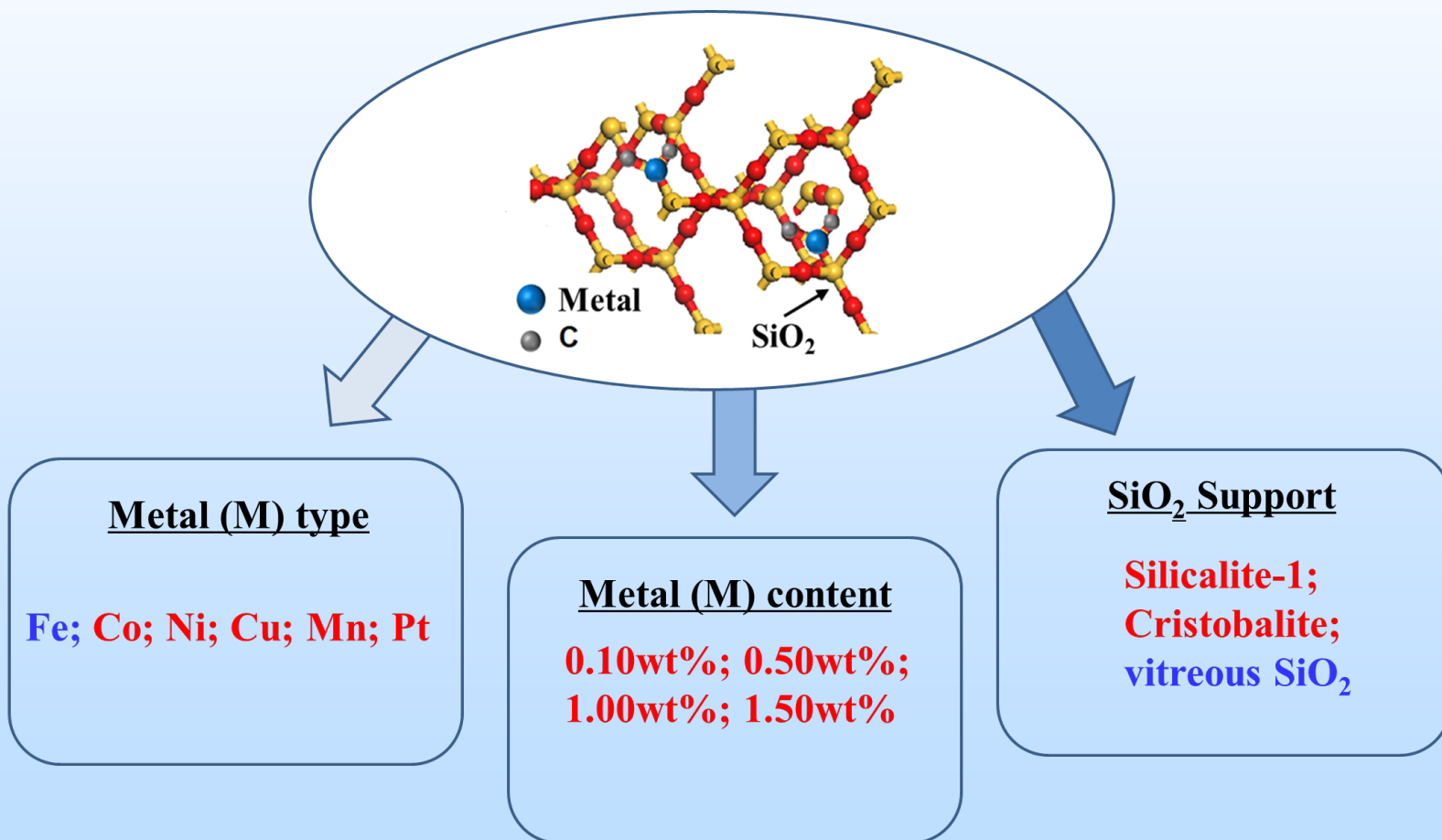
- (1) Make M/SiO₂ catalysts and obtain synthesis-structure-performance correlations;
- (2) Attain surface and gas phase reaction mechanism and kinetics by an integrated experimental and computational effort to create performance windows in reactor operation;
- (3) Demonstrate an efficient prototype reactor. The proposed catalyst/reactor system attains single-pass CH₄ conversion and C₂₊ yields of >25%, with > 90% C₂₊ selectivity, lifetime of >1000 h, and a low cost of catalyst and reactor materials.

d. Project risks and mitigation strategies

Risk	Mitigation strategy
Poor chemical/physical stability of M/SiO ₂ catalyst and microreactor	(1) Operate reaction at medium high temperature conditions; (2) Employ standard thermally stable support and metal catalyst materials in synthesis.
Measurement for real active sites in both catalyst surface and gas-phase reactions	Develop spatially resolved microprobe mass spectrometry equipment for in-situ measurement; Run co-feed experiments to probe NMC performance and reaction mechanisms.
Proper kinetic model for chemistry coupling both surface and gas phase reactions	Rely on first-principles models and use local computational resources and supercomputers to overcome this barrier.

Progress and Current Status of Project

1a. Prepared various silica supported single atom catalysts



Progress and Current Status of Project

1a. Representative M/SiO₂ catalysts synthesized for NMC

Metal (M) precursors



Fe₂SiO₄



Co₂SiO₄



Ni₂SiO₄



CuSiO₃

M/SiO₂ catalysts with different metal type



Fe/SiO₂



Co/SiO₂



Ni/SiO₂



Cu/SiO₂

Progress and Current Status of Project

1a. Representative M/SiO₂ catalysts synthesized for NMC

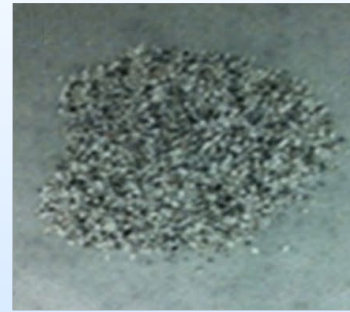
Fe/SiO₂ catalyst with different Fe content



0.05wt%



0.1wt%

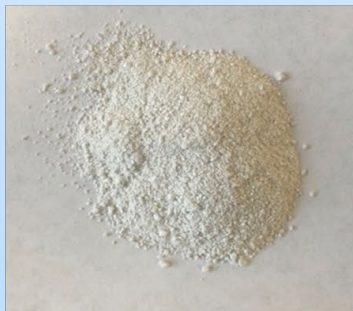


0.5wt%



1.50wt%

Fe/SiO₂ catalyst with different SiO₂ crystalline phase



silicalite-1



α-quartz



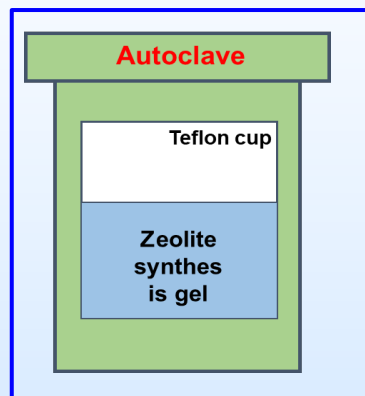
quartz-melt



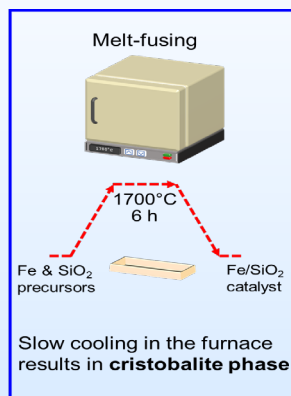
cristobalite

Progress and Current Status of Project

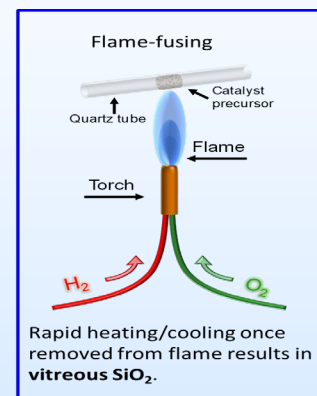
1b. Employed three different routes to synthesize catalysts



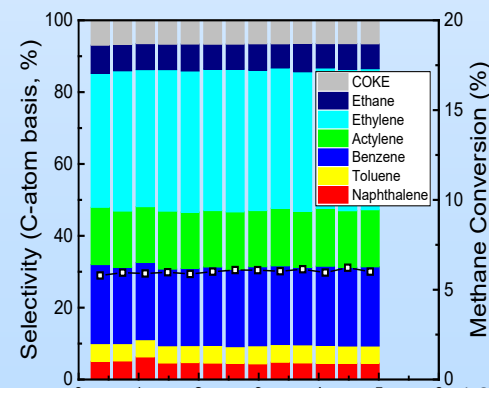
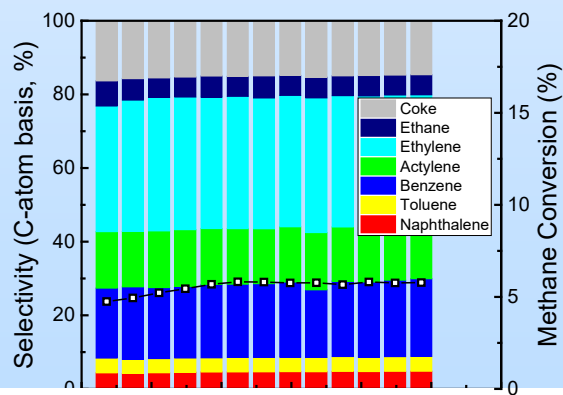
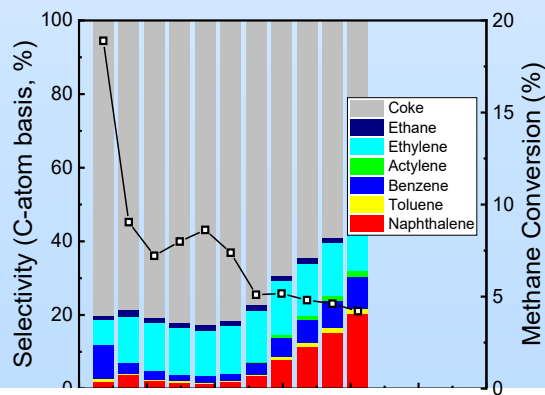
Fe/Silicalite-1



Fe/SiO₂-CRS (Cristobalite)

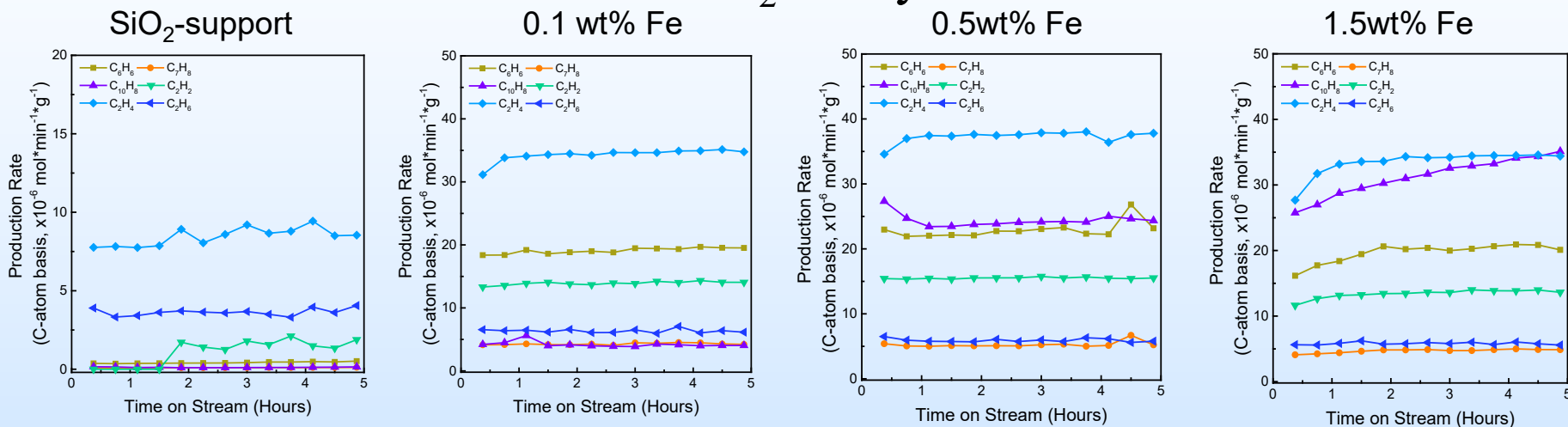


Fe/SiO₂-VS (Vitreous)

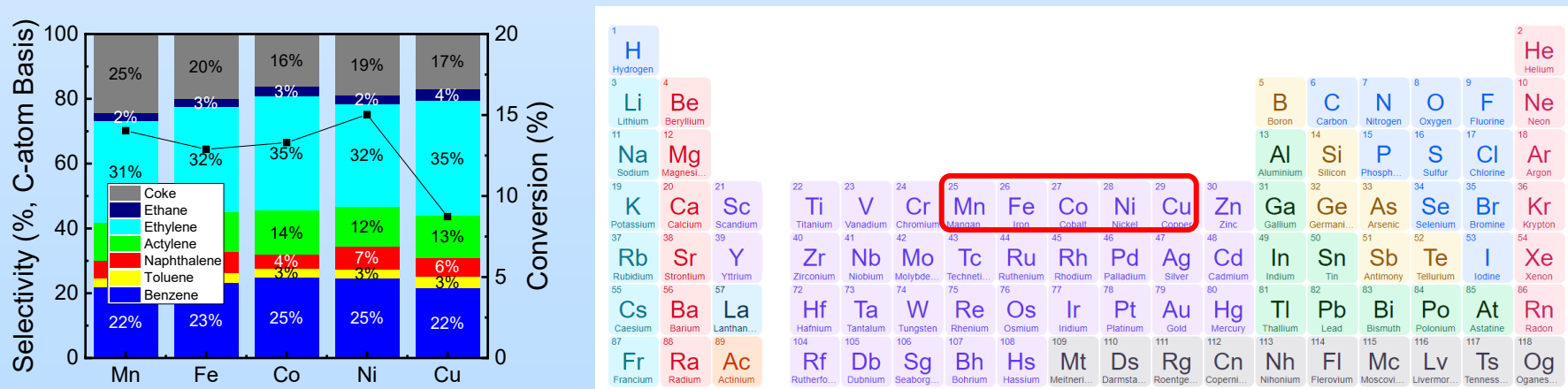


Progress and Current Status of Project

1c. Effect of metal conc. in M/SiO₂ catalysts on NMC

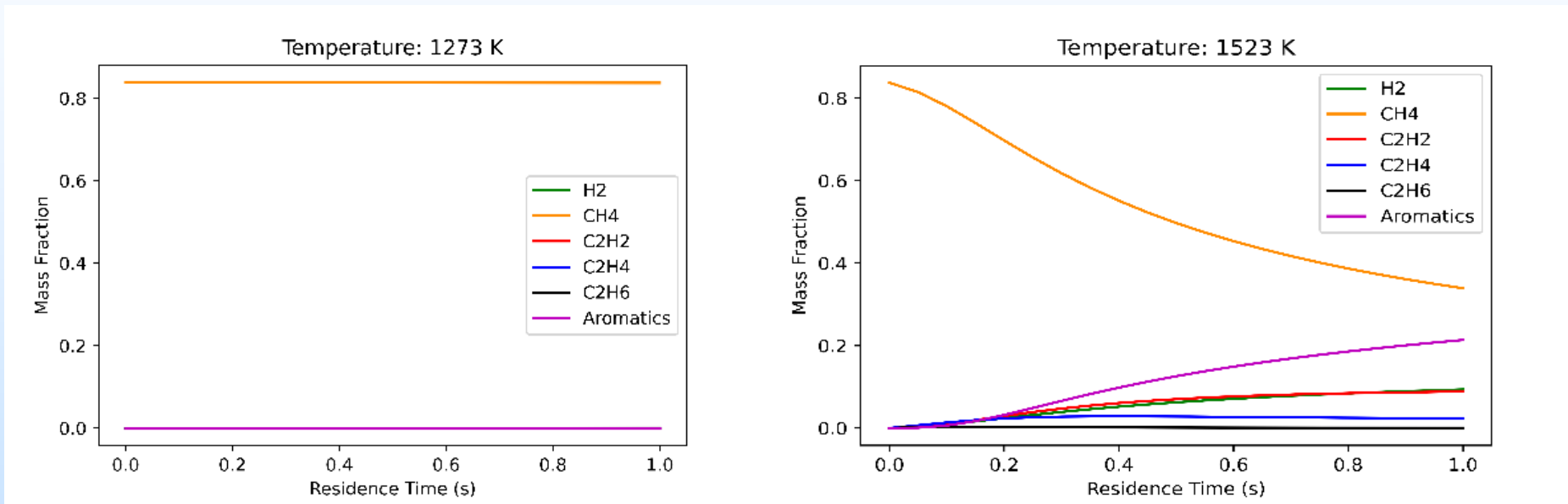


1d. Effect of metal type in M/SiO₂ catalysts on NMC



Progress and Current Status of Project

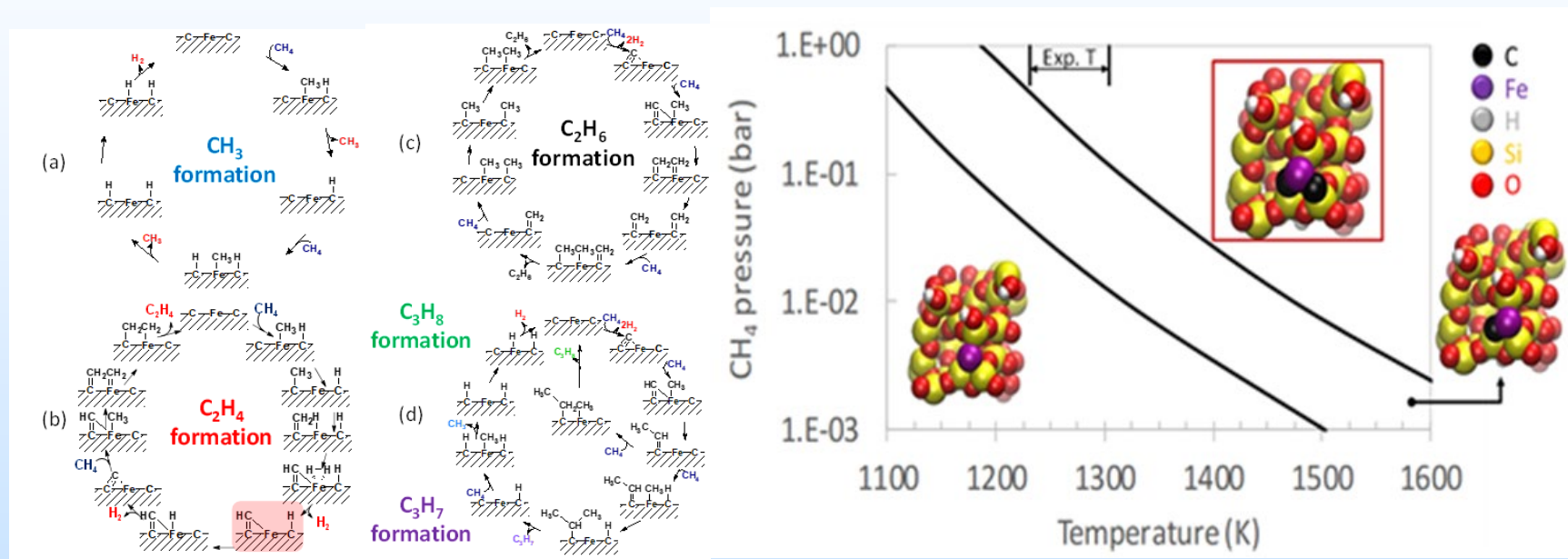
1e. Simulated conversion with only gas-phase chemistry (90% CH₄+10% inert)



- (1) CH₄ does not readily couple in the gas phase at typical reactor temperatures;
- (2) >1473 K is required for a direct conversion of methane, form aromatics and acetylene with little ethylene;
- (3) High temperature requirement for methane coupling in the gas phase suggests that methane coupling occurs primarily on the surface to form ethylene.
- (4) Ethylene formed on the surface readily reacts further in the gas phase to form compounds like aromatics. This agrees with the expectation that gas phase chemistry is detrimental to ethylene selectivity.

Progress and Current Status of Project

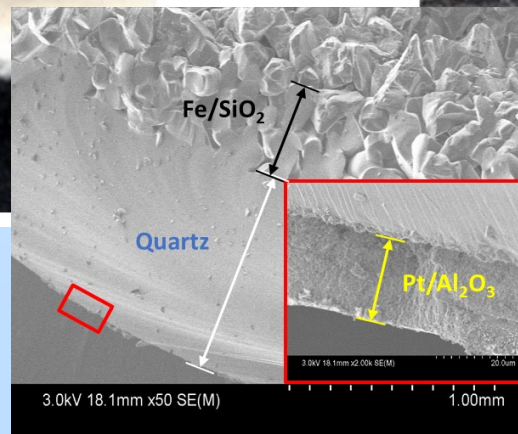
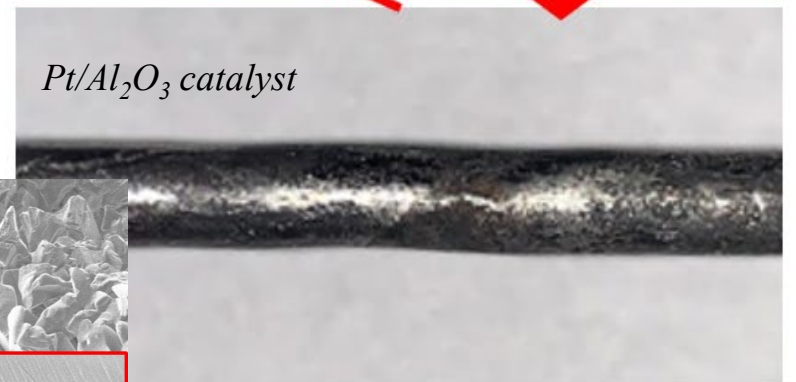
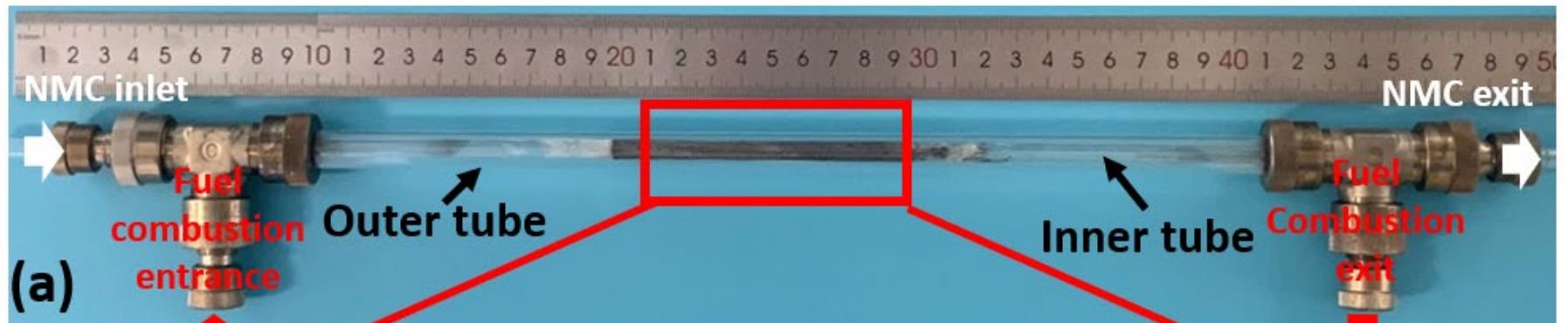
1f. Simulation of CH₄ activation mechanism on Fe/SiO₂ catalyst



- (1) Ab initio phase behaviour of isolated iron atoms on amorphous silica. Thermodynamic analysis is done for $\text{FeO}_3/\text{SiO}_2 + x\text{CH}_4 \leftrightarrow \text{FeC}_{x-3}/\text{SiO}_2 + 3\text{CO} + 2x\text{H}_2$ with $x = 3, 4, 5, 6$, $P_{\text{H}_2} = 10^{-3}$ bar, and $P_{\text{CO}} = 10^{-8}$ bar. At typical reaction temperatures and methane partial pressures, carburization of the catalyst occurs.
- (2) Catalytic reaction network for C1-C3 species formation from methane over isolated iron carbide species. The steps leading to the formation of coked iron carbide active site are common in all C2-C3 species formation cycles and are shown for ethylene only.

Progress and Current Status of Project

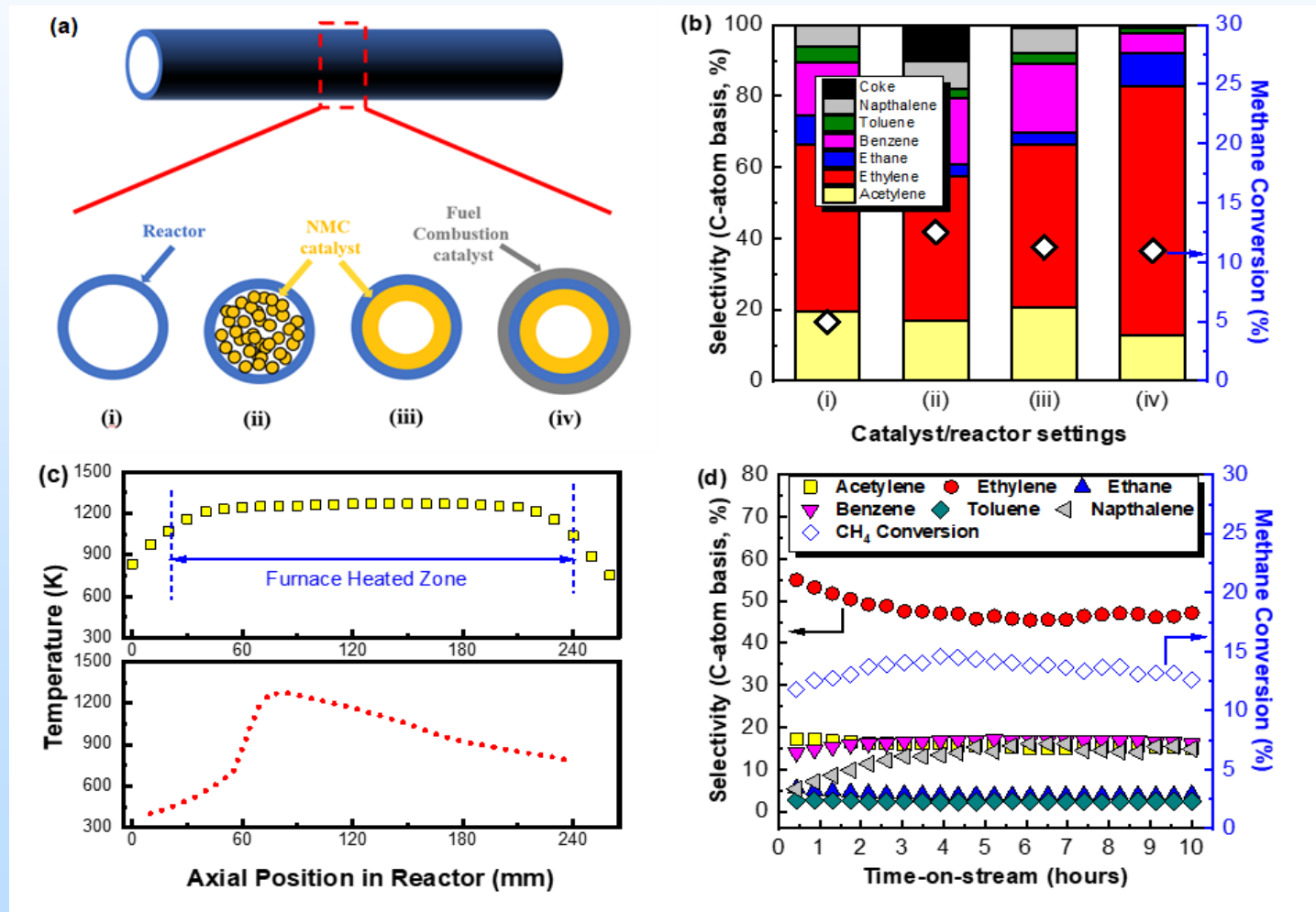
2a. Design/fabrication of catalytic wall reactor



Provisional patent filed.

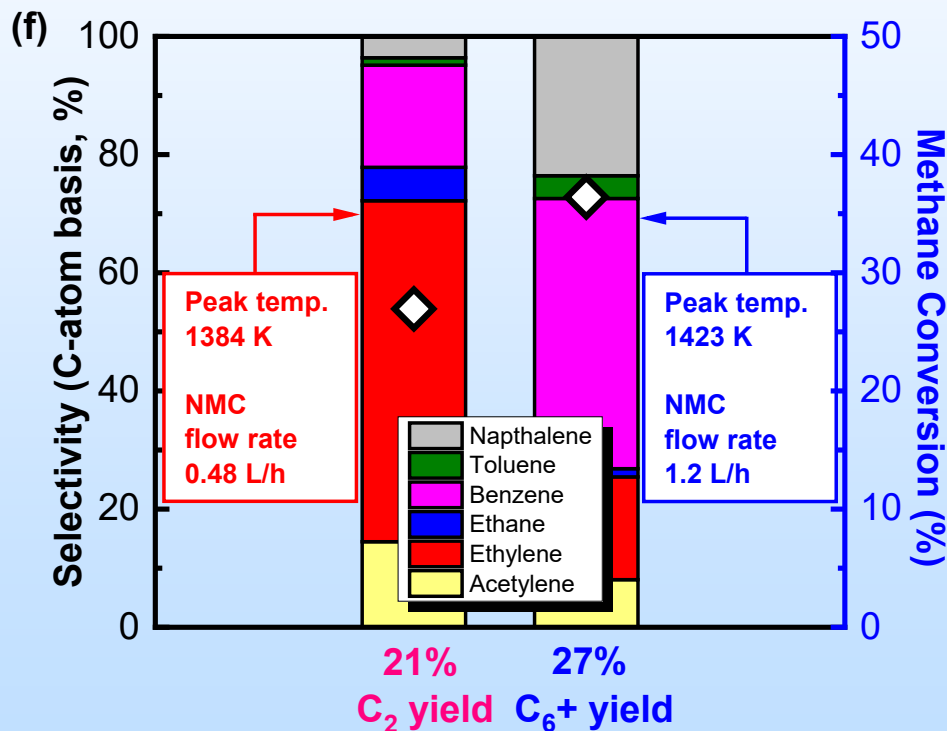
Progress and Current Status of Project

2b. Effect of catalyst layout in reactor on NMC

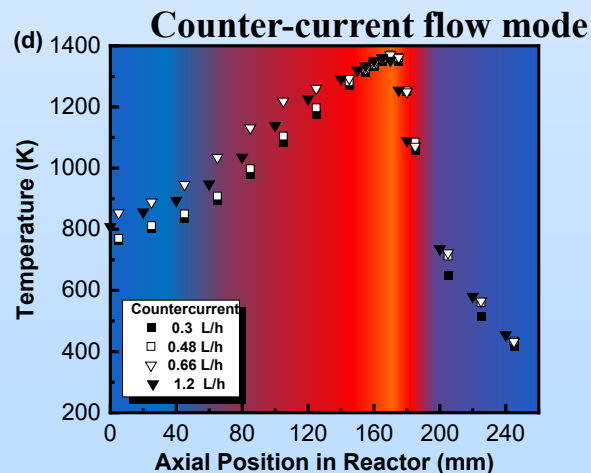
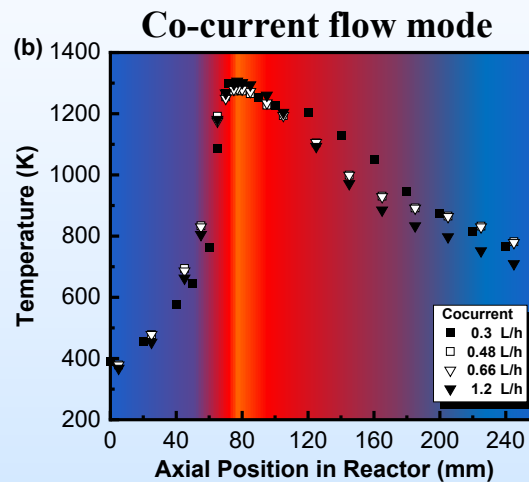


Progress and Current Status of Project

2c. Maximized NMC performance in autothermal catalytic wall reactor

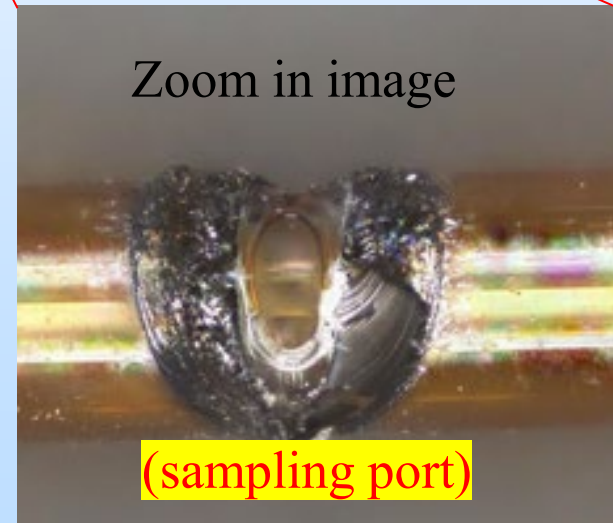
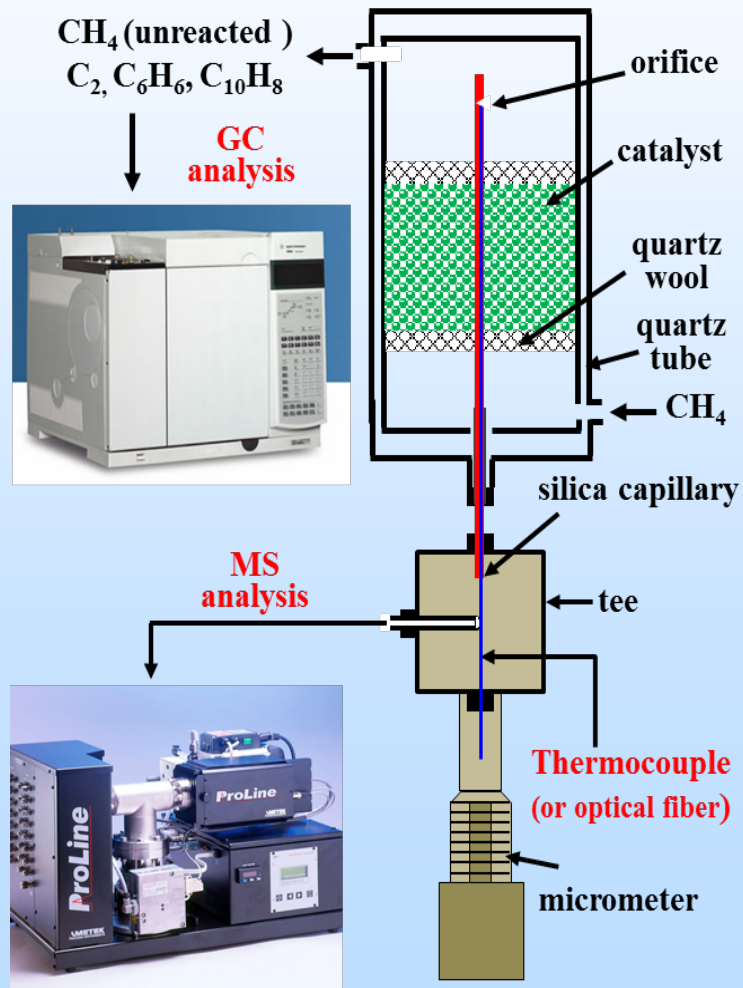


Tune process conditions towards target products



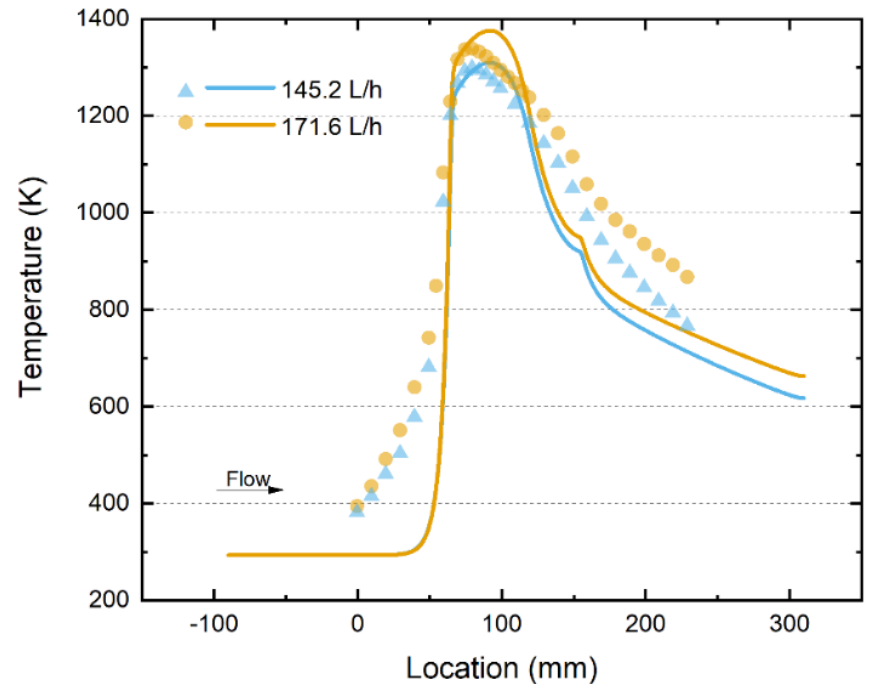
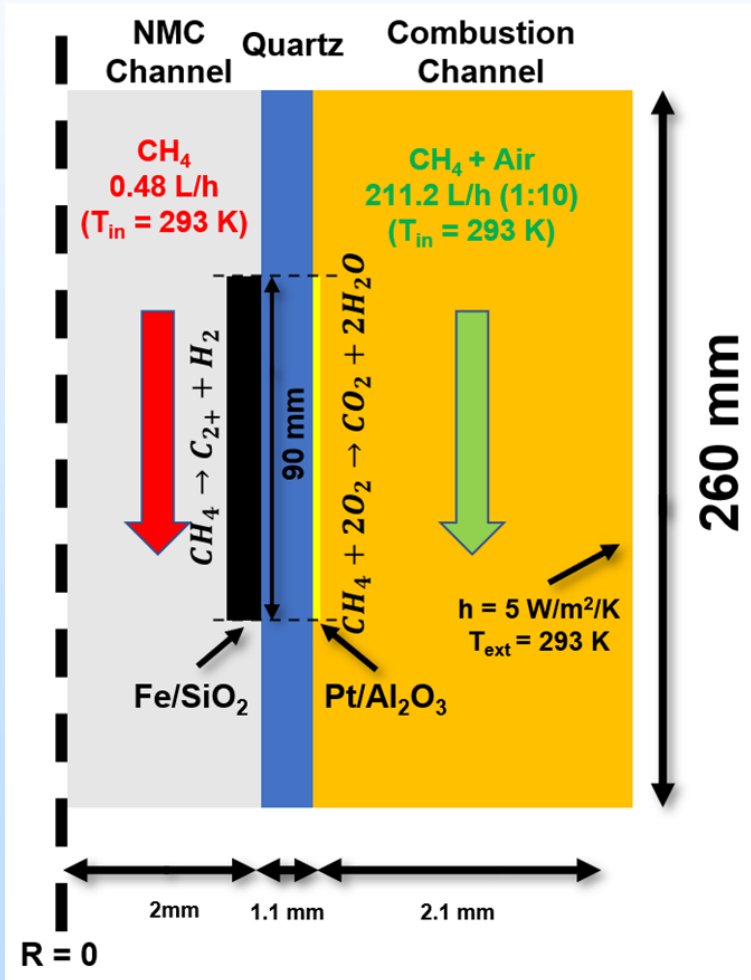
Progress and Current Status of Project

2d. Design/fabricate spatial/temporal measurement equipment



Progress and Current Status of Project

2e. 2D-axisymmetric steady-state COMSOL simulation

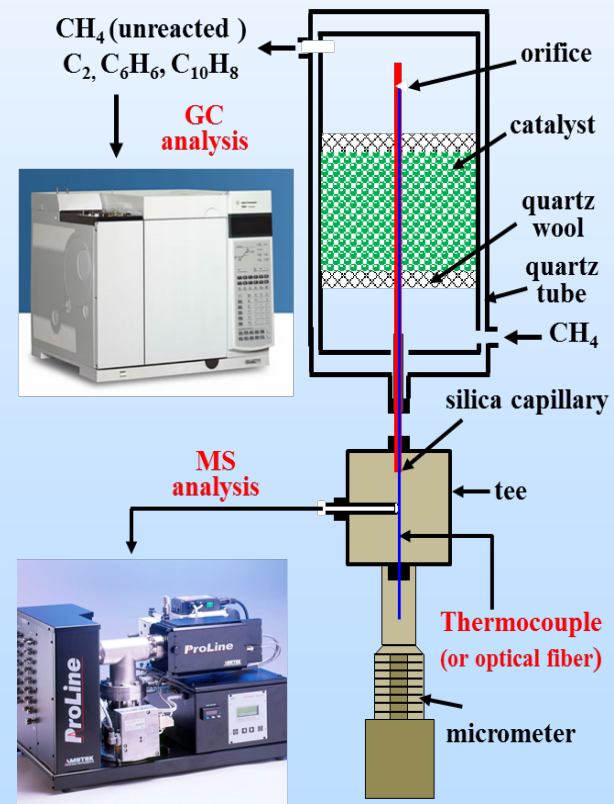
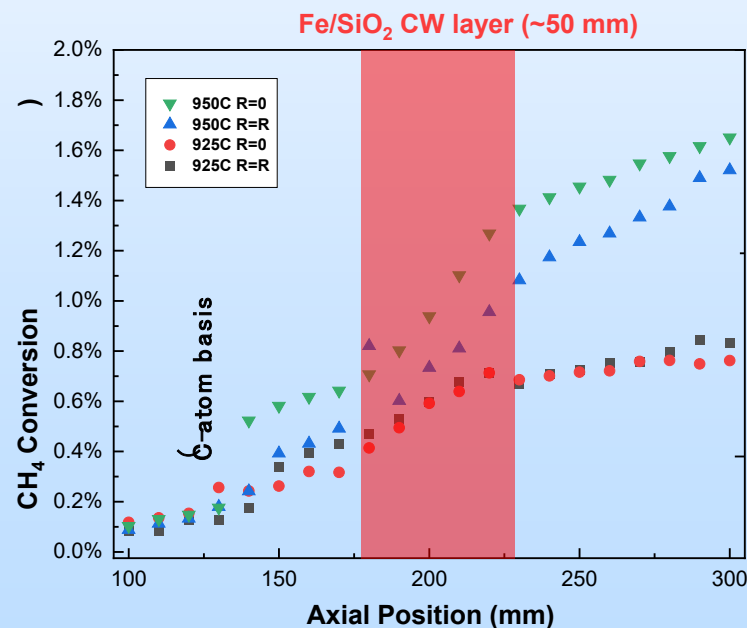


High flow rate → high peak temperature
Model and experiment fits each other

Plans for future testing/development/ commercialization

a. In this project

- (1) continue to measure spatial/temporal species concentrations;
- (2) develop coupled surface and gas phase mechanism for NMC optimization;
- (3) long-term test for reactor.

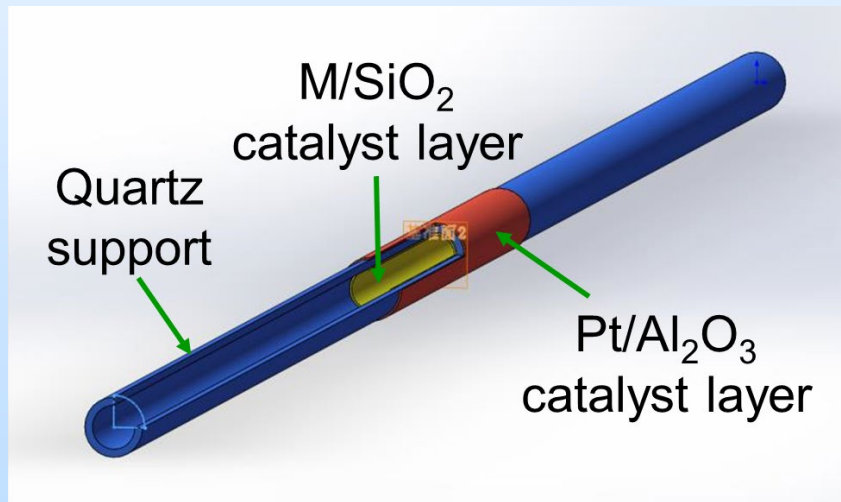


Plans for future testing/development/ commercialization

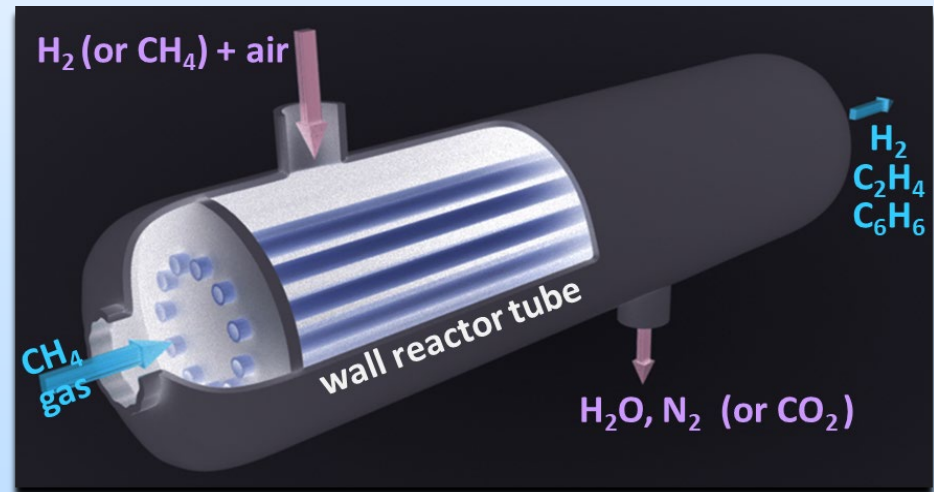
b. After this project

Scale up the catalytic reactor design/fabrication and catalyst for high TRL-level research for NMC

Singe reactor tube



Reactor bundle



Outreach and Workforce Development Efforts or Achievements

- Outreach: Hosted undergraduate students in ENES240, the intro to science, technology, ethics, and policy (STEP) every semester
Students' feedback: **There was just so much "magic" happening there...** I'm glad I went... It was good to see so many projects' people were working on and the kind of inspirations they drew on to get there. In my extremely humble opinion, **science is as much about finding out what doesn't work as finding out what does.** The students encouraged each other to keep going and try new methods. The prof even stated that it was best to just go through a couple failures as quickly as possible to get used to it and the idea of persisting notwithstanding."
- Workforce Development: Trained 3 undergraduate and 3 graduate students, and 1 postdoc fellow; integrate research findings into courses that the PIs teach to educate broad student body in STEM field.

Summary Slide

- a. Single atom M/SiO₂ catalysts with variable metal type, metal concentration and support are synthesized by high temperature synthesis routes;
- b. NMC performance depends on metal type, concentration and silica support properties. Among all studied catalysts, Co/SiO₂ and Fe/SiO₂ are the most promising ones for scale up;
- c. NMC over M/SiO₂ catalyst involves surface activation of C-H bond in CH₄, and gas phase chemistry to produce larger C_xH_y products. Suppression of gas phase chemistry is needed to improve ethylene selectivity;
- d. Reactor engineering is a strategy to control gas phase reaction to tailor product selectivity. Innovations in both catalyst and reactor engineering are needed to maximize NMC performance.

Appendix

- These slides will not be discussed during the presentation **but are mandatory.**

Organization Chart

