



**MEMBRANE**  
TECHNOLOGY & RESEARCH

# **Scale-Up and Testing of Advanced Polaris Membranes at TCM (DE-FE0031591)**

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Carbon Management Research Project Review Meeting  
Capture from Power Generation / Pilot-Scale Research  
August 16, 2022

# Project Overview

**Award name:** Scale-Up and Testing of Advanced Polaris Membrane CO<sub>2</sub> Capture Technology (DE-FE0031591)

**Project period:** 8/1/18 to 9/30/22

**Funding:** \$8.2 million DOE; \$2.6 million cost share (\$10.8 million total)

**DOE program manager:** Bruce Lani (BP1), Isaac “Andy” Aurelio (BP1/2), Andy O’Palko (BP3)

**Participants:** MTR, TCM, Trimeric, CCSI2

**Project scope:** Design, build, and operate a system at TCM with Gen 2 Polaris modules

**Project plan:** The project is organized in three phases:

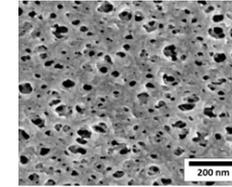
- **Phase 1** – Design system, fabricate membrane modules
- **Phase 2** – Build and install system at TCM
- **Phase 3** – Operate system, analyze results, decommissioning

# Background: This Project in Context

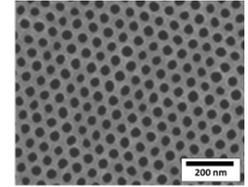


## Self-Assembly Isoporous Supports (DE-FE31596; Hans Wijmans)

- Transformational new membrane (TRL 3 – 4)
- Reduces membrane area and energy use



Surface of Conventional Support

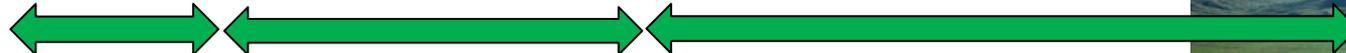


Surface of Isoporous Support



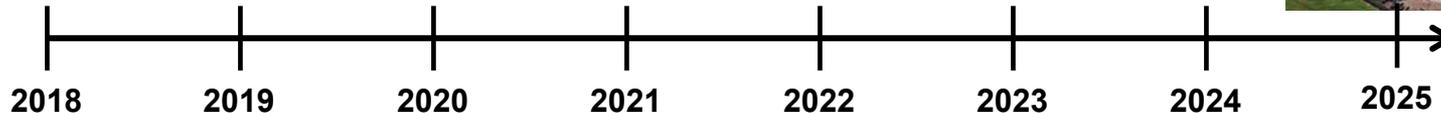
## Pilot Testing at TCM, Norway (DE-FE0031591; Tim Merkel)

- Gen 2 Polaris™ membrane
- Low pressure-drop modules
- Containerized skid, 10 TPD pilot scale



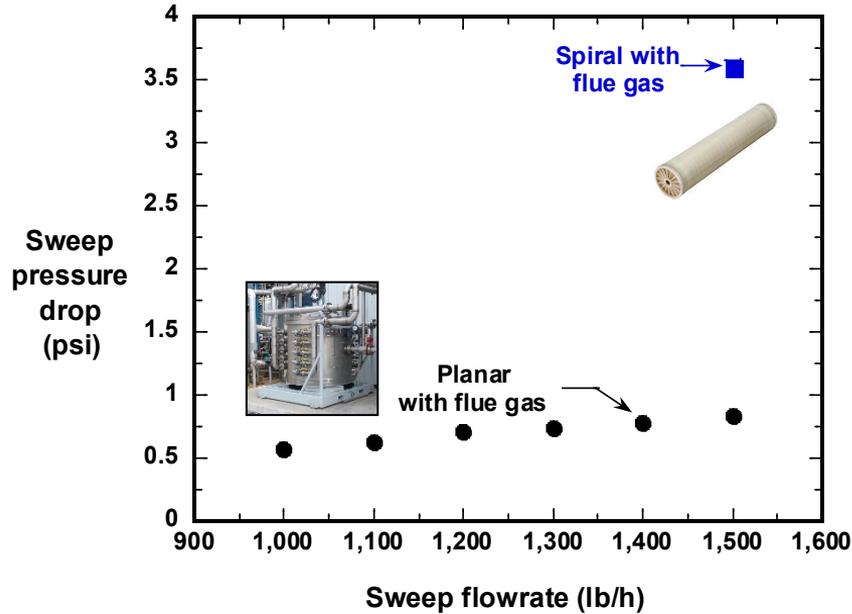
## Large-Pilot Testing at Wyoming ITC (DE-FE31587; Brice Freeman)

- Phase I – Design 150 TPD pilot; secure host site
- Phase II – FEED and permitting
- Phase III – Fabricate, install and operate (TRL 7 – 8)

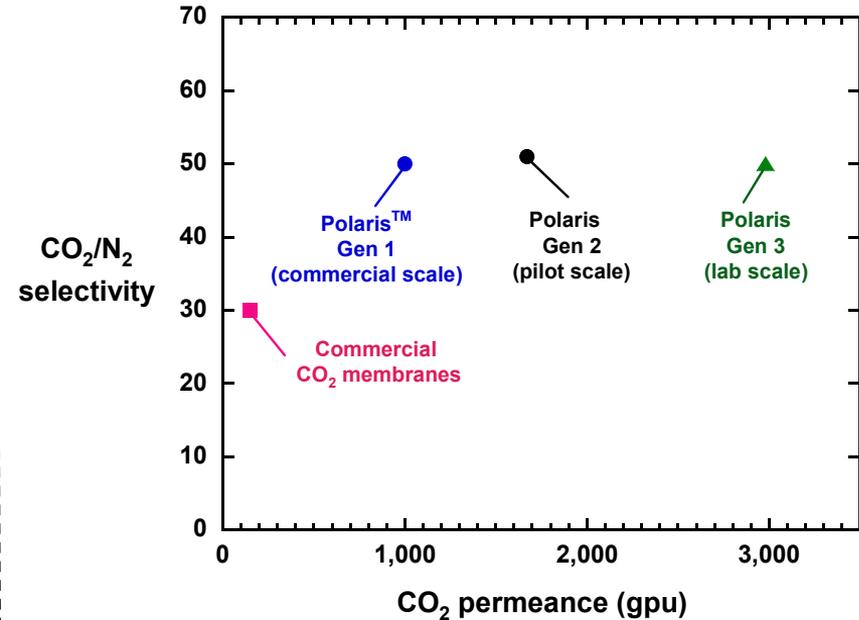


# Background: Membrane and Module Improvements

## Planar Modules



## Polaris™ Membranes



- Moving from Gen 1 to Gen 2 Polaris cuts membrane area by ~50% (~\$12/tonne CO<sub>2</sub>)
- Lower pressure drop of new modules saves 10 MW<sub>e</sub> fan power on 500 MW<sub>e</sub> system

# Project Objectives

- Scale-up Gen 2 Polaris membrane packaged in low-pressure-drop, low-cost module stacks and test at TCM
- Demonstrate “containerized” skid as final form factor for future large-scale systems
- Test pilot system (~10 TPD) over range of CO<sub>2</sub> capture rates and feed CO<sub>2</sub> content for TEA input
- Update overall process TEA

# Primary Objective: Module-Scale Up

Plate-and-Frame Prototype with Gen-1 Polaris  
(Tested at NCCC/B&W/UT-Austin 2015-18)



Verified low-pressure drop in field testing

Containerized Module Stacks with Gen-2 Polaris  
(2021/22 TCM Field Test)



Low pressure drop, plus optimized flow distribution and reduced cost (valves, etc)

# TCM Site Preparations

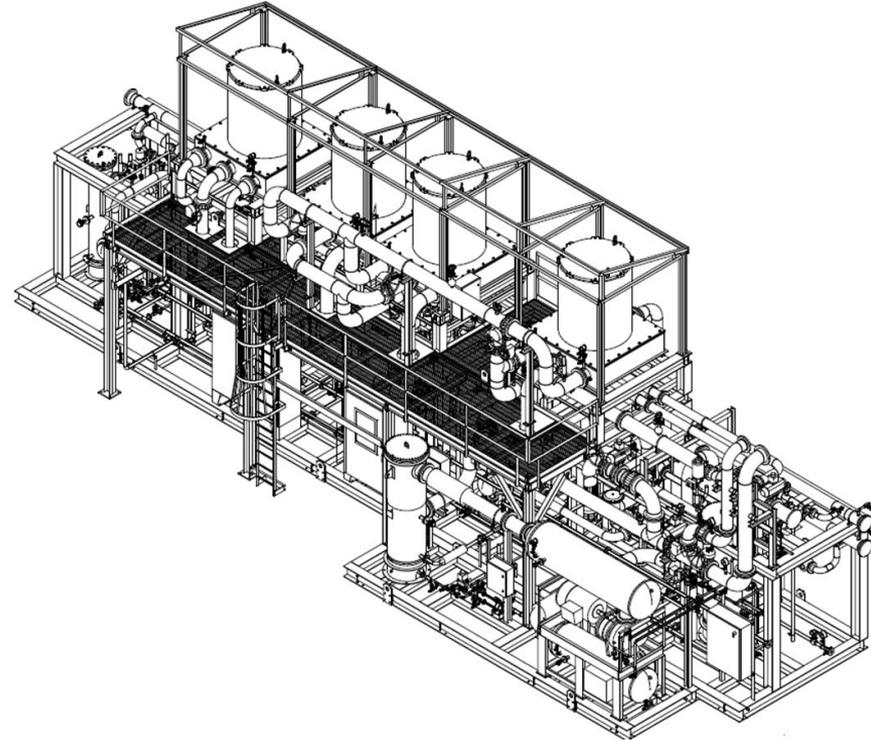
View of TCM with 3<sup>rd</sup> site in foreground



- Technology Centre Mongstad (TCM) is a world-leading site for evaluation of carbon capture technologies
- TCM began development of the “3<sup>rd</sup>” site for testing of emerging capture technologies in 2019
- TCM assisted MTR with installation of the pilot system at the site in spring/summer 2021, and with operation in fall 2021/winter 2022

# MTR System General Arrangement

- Membrane system general arrangement drawings finalized in BP2 (June 2020)
- Membrane “container” with 4 stacks on top floor (full container would be 6-8 stacks); blower/pumps on bottom floor
- Factory Acceptance Test (FAT) of system completed in March 2021
- Skids shipped to Norway in spring 2021, and installed at TCM in summer 2021



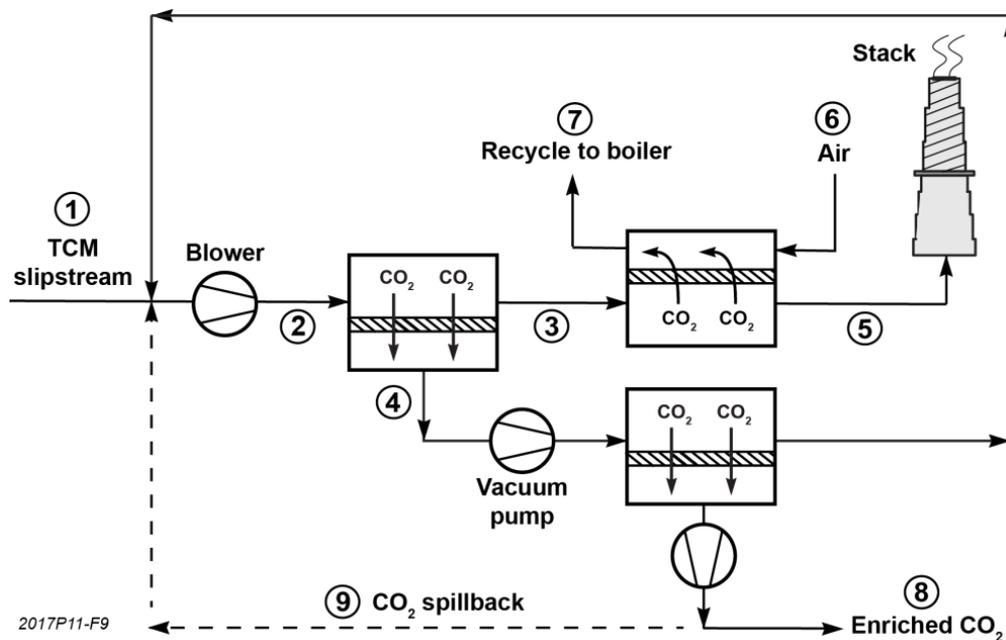
# MTR System at TCM



- System has a single membrane container. Future larger systems will have multiples of this unit building block

# Test System Design

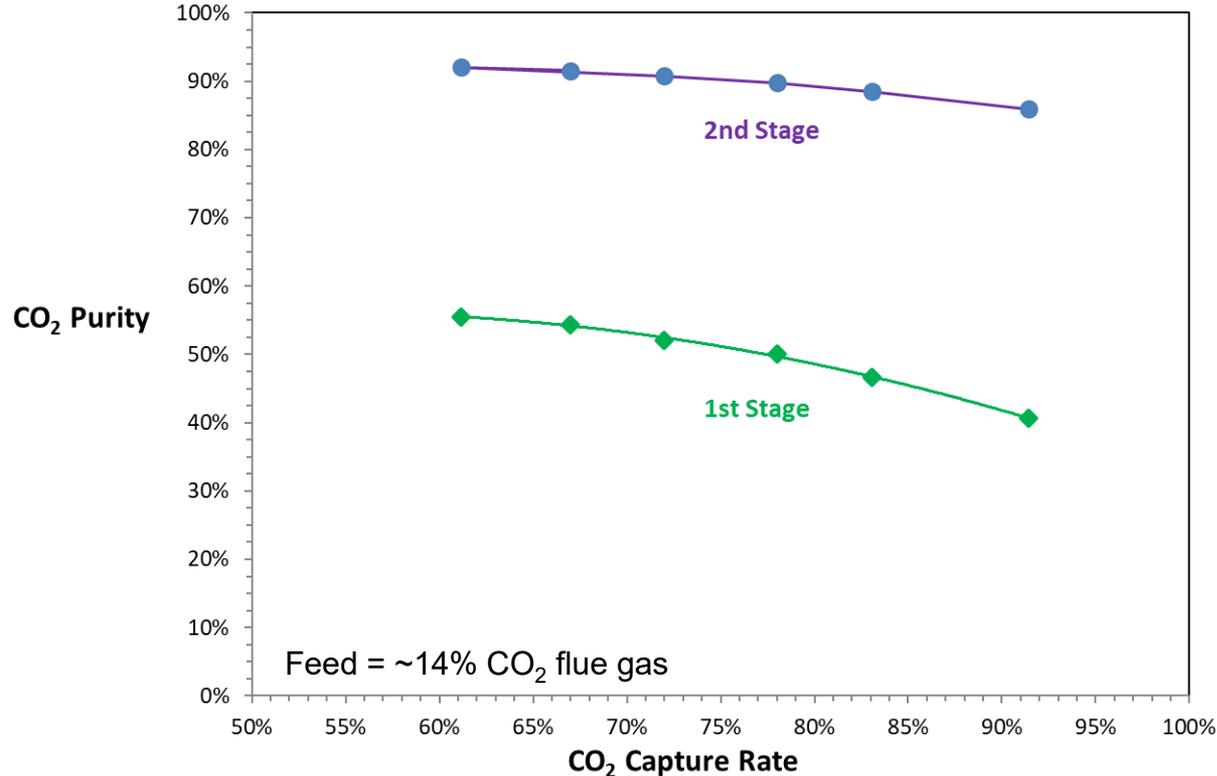
- 2 stage system with air sweep step (stream 6) and varying feed CO<sub>2</sub> content using recycle (stream 9)
- TCM slipstream flow rate of 800 to 2,400 Nm<sup>3</sup>/h
- 50% to >90% CO<sub>2</sub> capture rates possible
- Tests the membrane portion of the capture process, but not the CO<sub>2</sub> purification unit (CPU)



# Test Plan for TCM Campaign

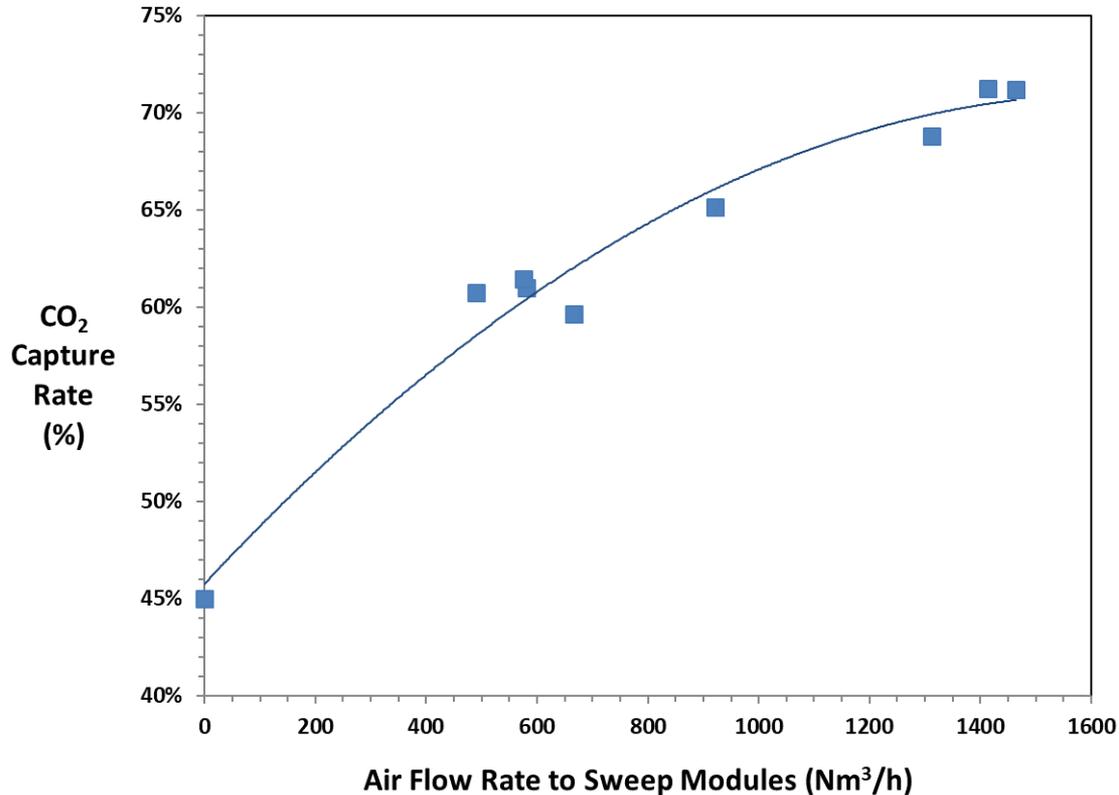
- Received input from DOE, TCM and CCSI2 team on test plan
  - Adjustable test parameters included: flue gas flow rate, sweep air flow rate, and CO<sub>2</sub> concentration to 1<sup>st</sup> stage membrane
  - Used these variables to explore capture rates from 50% to >90% and to evaluate pressure drop in planar modules
  - Two different module configurations with different pressure drop characteristics were examined
  - Metal coupon testing of membrane generated streams also conducted: carbon steel, Ni plated CS, 304 SS, 316 SS, Al 6061, etc

# TCM Test Data: Purity/Recovery



- With ~14% CO<sub>2</sub> feed gas, a single stage membrane produces 40-55% CO<sub>2</sub> and a second stage yields >85% CO<sub>2</sub>
- Purity/recovery tradeoff is typical membrane behavior; details are useful for future system design
- In a complete system, the second stage permeate would be sent to the CPU for liquefaction producing >99.9% CO<sub>2</sub> ready for pipelines

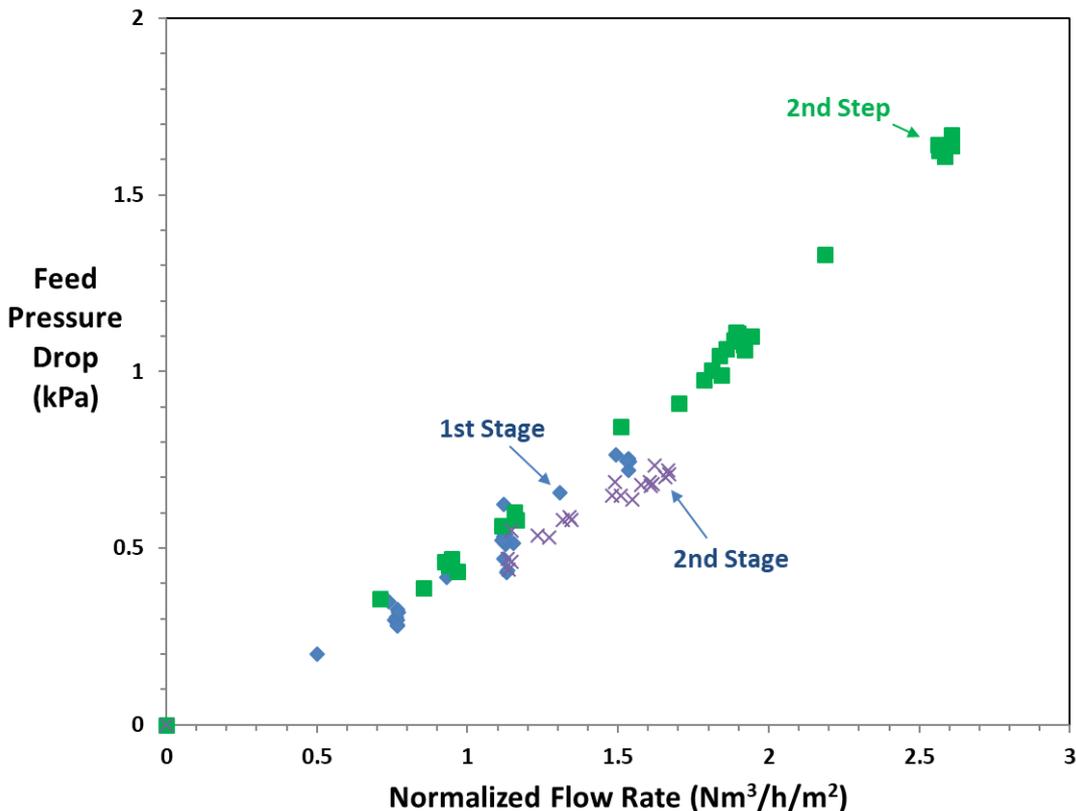
# TCM Test Data: Effect of Air Sweep



Feed = 1800 Nm<sup>3</sup>/h of ~14% CO<sub>2</sub> flue gas

- Air sweep on a 2<sup>nd</sup> step membrane module can be used to increase capture rate at low cost
- The TCM campaign was slipstream testing, so the CO<sub>2</sub>-laden air was measured and vented; in a real system, it would be recycled to the combustion process
- Results are consistent with prior sweep testing at B&W and NCCC

# TCM Test Data: Pressure Drop



- A key feature of the MTR planar modules is lower pressure drop compared to other module configurations
- Lower pressure drop means less fan power is needed to push gas through the membrane modules
- Pressure drop used in TEA is 1.5 psi (10.4 kPa); actual performance is much lower!
- Data for different modules falls on a single trendline indicating good flow distribution

# Current Project Status

- Testing at TCM finished March 1, 2022
- Decommissioning of the system was completed in June
- The system is now being stored at the port of Bergen awaiting future industrial test opportunities

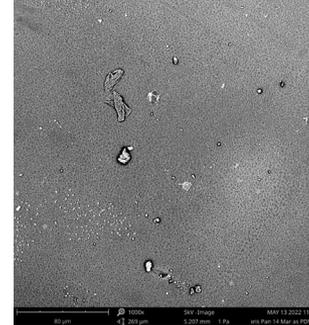


- Currently, we are working on the project TEA with Trimeric
- This study, as well as the technology gap analysis and the EH&S reports, are on schedule for Sept 30 completion

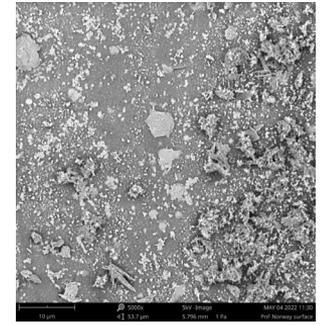
# Lessons Learned

- Because of supply chain issues, module housings were aluminum instead of plastic or stainless steel (prior systems)
- After running at TCM, housings showed significant aluminum sulfate corrosion presumably due to water + SO<sub>2</sub> condensate
- Surface analysis of membranes (SEM/EDS, XPS, ICP-MS) confirmed the presence of aluminum and ammonium (bi)sulfate, which lowered membrane permeance
- Running in parallel at TCM, the TDA/MTR hybrid system with all SS housings showed no membrane fouling;
- Also, a new module installed mid-campaign with fouling-resistant Polaris formulation was unaffected by the corrosion

Fresh Polaris

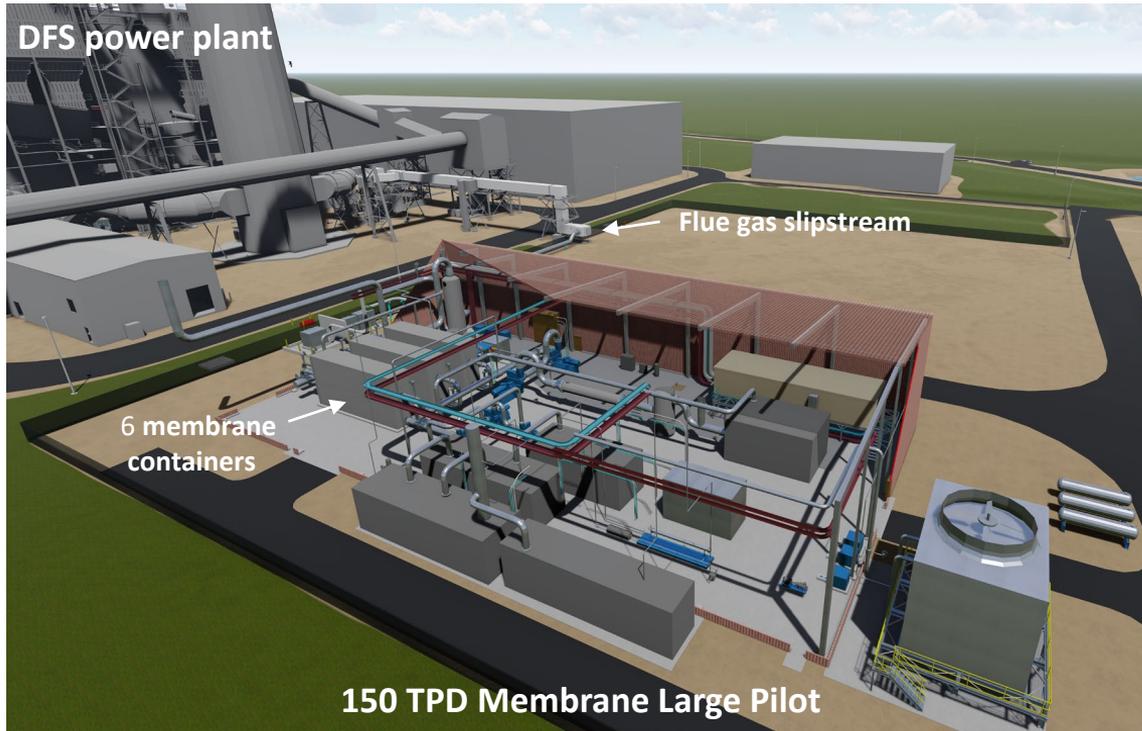


After TCM Testing



# Next Steps

## Conceptual Drawing of MTR Large Pilot at WITC



- The modular membrane capture approach demonstrated at TCM will be used on the larger 150 TPD MTR system under construction at the Wyoming Integrated Test Center (WITC) - Dry Fork Station (DFS) power plant

# Summary

- A planar module test system was designed, built, installed and operated at the new TCM 3<sup>rd</sup> site
- ~6 months of testing was focused on varying capture rates and evaluating different module configurations; completed in March 2022
- Performance confirmed expected purity/recovery tradeoff and low pressure drop of planar modules
- Lessons learned included need to protect membranes from capture system corrosion; component and membrane material solutions
- Project is nearing completion with TEA and other reports on schedule for Sept 30 end date

# Acknowledgements

This material is based upon work supported by the Department of Energy under Award Number DE-FE0031591.

## **Disclaimer**

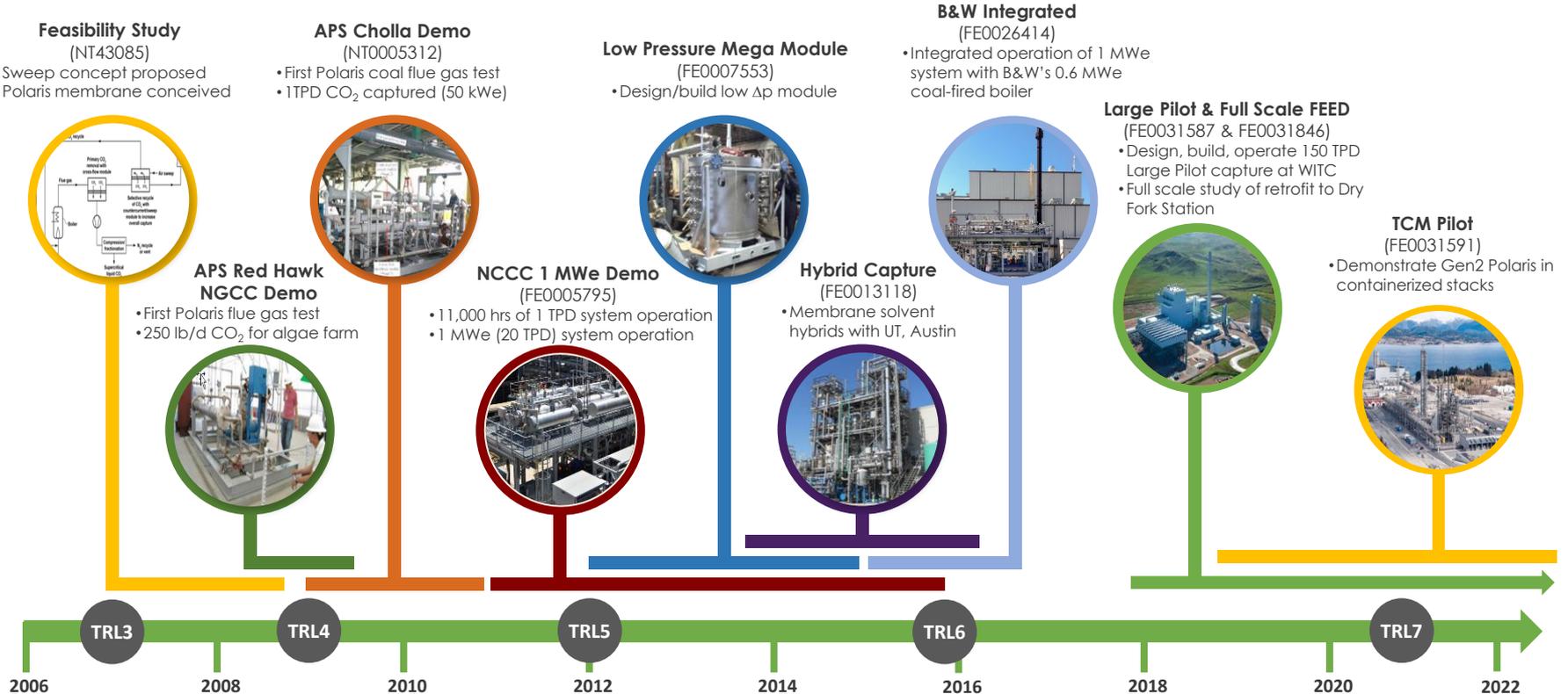
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# EXTRA SLIDES

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# Background: Development Timeline



# Presentation Outline

- Project overview
- Background and objectives
- Progress to date
- Future plans
- Summary



# Role of Participants

- MTR (Tim Merkel, Jay Kniep, Thomas Hofmann) – project lead and liaison with DOE; responsible for membrane system design, construction, installation and operation; will lead data analysis and all reporting to DOE
- TCM (Kjetil Hantveit, Sundus Akhter) – host site for the field test; with MTR, will coordinate system installation, operation, and data analysis
- Trimeric (Ray McKaskle) – Responsible for membrane capture process techno-economic analysis (TEA)

# Budget Period 3 Milestones

Milestone Number	Task/ Subtask No.	Milestone Description	Planned Completion Date (*)	Verification Method
Phase 3 / Budget Period 3				
11	8.1	Test System Commissioned on Flue Gas	7/31/21	Quarterly Report
12	8.3	Parametric Tests Completed, Long Term Performance Testing Begins	12/31/21	Quarterly Report
13	8.4	Long Term Performance Testing Completed	2/28/22	Quarterly Report
14	10	Complete Techno-Economic Analysis Report	9/30/22	Topical Report
15	11	Complete Technology Gap Analysis Report	9/30/22	Topical Report
16	12	Complete Environmental Health and Safety Risk Assessment Report	9/30/22	Topical Report
17	M1	Submit Final Report	12/31/22	Final Report

# Budget Period 3 Scope of Work

- Main objective of BP3 is operation of the test system; tasks include:
  - Task 8: Operate Membrane Test System
  - Task 9: Decommissioning and Site Clean-Up
  - Task 10: Refine Techno-Economic Analysis
  - Task 11: Technology Gap Analysis
  - Task 12: Environmental Health and Safety Risk Assessment
- BP3 budget: \$2,614,694
  - \$1,333,694 Federal, \$1,281,000 Cost Share

# TCM Site Preparations

3<sup>rd</sup> site with MTR and TDA skids

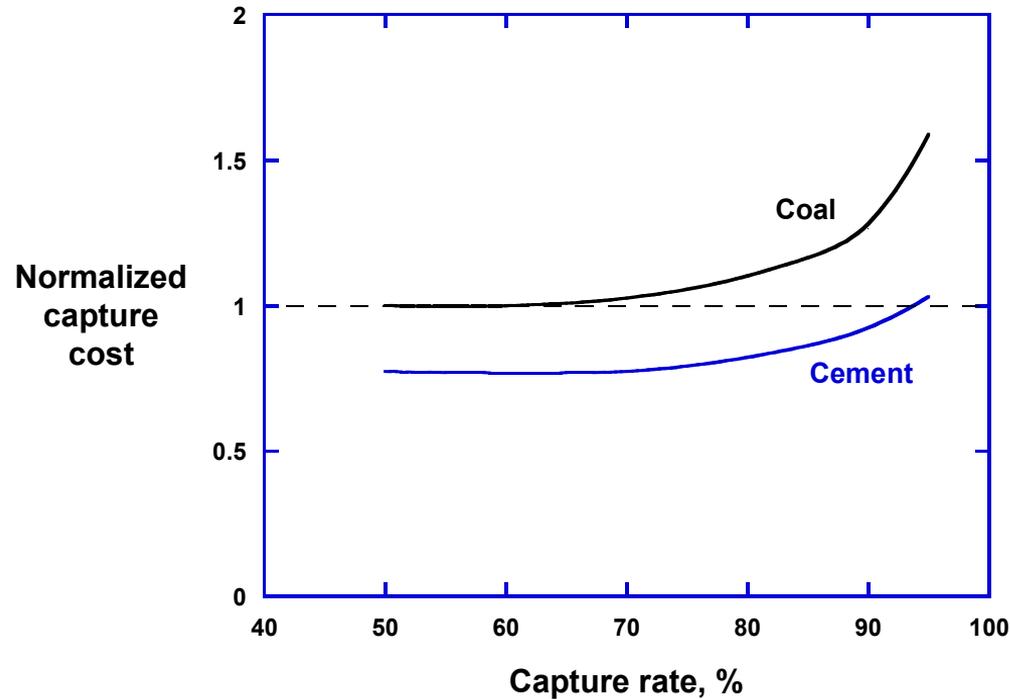


Close up view of 3<sup>rd</sup> site foundation



- TCM approved development of the “3<sup>rd</sup>” site for testing of emerging technologies in 2019
- The site was ready for system installation by Fall 2020

# Capture Cost vs Rate and CO<sub>2</sub> Content



Capture cost is normalized to 60% capture from coal using today's Polaris membranes

- TEA will quantify the impact of capture rate and CO<sub>2</sub> content on costs
- Membrane costs are sensitive to the feed CO<sub>2</sub> content
- Minimum cost is about 20% lower for cement compared to coal
- Membrane cost is less sensitive to capture rate for higher feed CO<sub>2</sub> content; higher capture is more affordable for cement

# Primary Objective: Module-Scale Up

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