

# Application of a Transformational UKy 3 Ton/Day CO<sub>2</sub> Capture System at a Steel Process Plant DE-FE0032133

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<https://caer.uky.edu/co2capture/>*

*August 15-19, 2022*

# Project Objective

Demonstrate the UK CO<sub>2</sub> capture process at Nucor Steel Gallatin treating electric arc furnace evolved gas with a CO<sub>2</sub> concentration of ~1.5 vol%.

## BP1

- Design
- Contractor selection

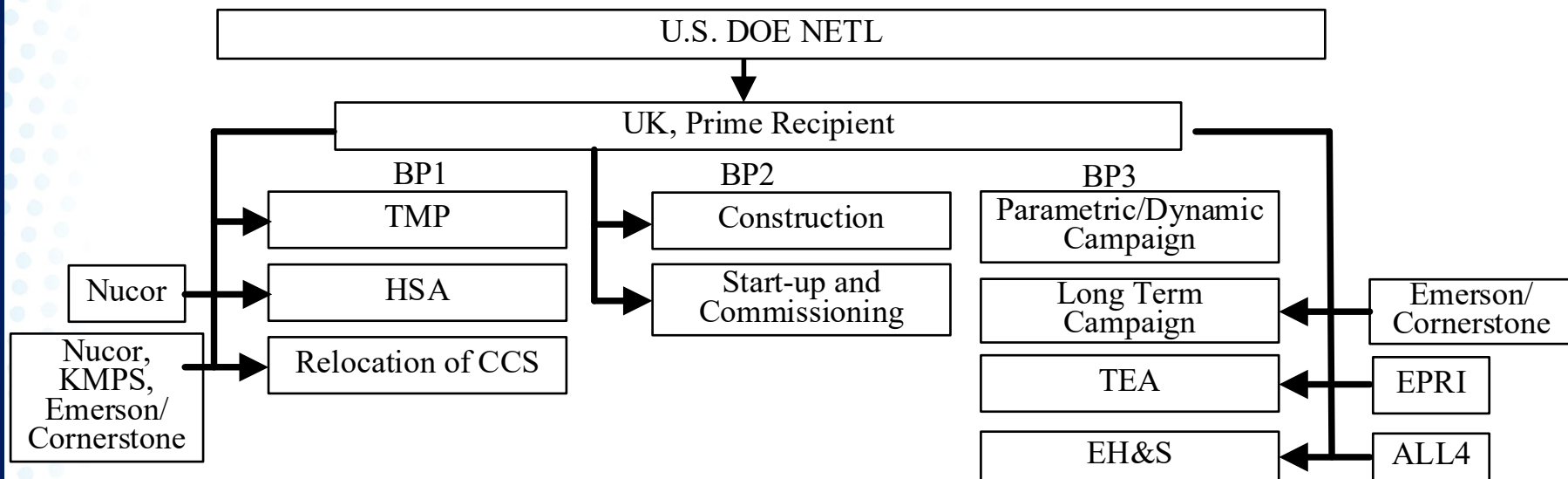
## BP2

- Site Prep
- Module Erection
- Tie-in at Nucor

## BP3

- Evaluation
- Data Analysis
- Reporting

# Project Team and Funding



	DOE-NETL	Cost Share	
<b>Total:</b>	<b>\$4,999,965</b>	<b>\$1,250,523</b>	<b>\$6,250,488</b>
<b>Percent Share:</b>	<b>80%</b>	<b>20%</b>	<b>100%</b>

# Background - Development



## UK Solvent

- <\$5/kg chemical cost
- ~6400 experimental hours at bench and small pilot scales
- NG and coal flue gas evaluations
- 3-20 vol% CO<sub>2</sub> inlet concentration evaluations
- Modeled by small pilot experimentally verified Aspen Plus®
- Solvent regeneration energy as low as 1040 BTU/lb CO<sub>2</sub>
- Make-up rate of 0.6 kg/tonne CO<sub>2</sub>

## H3-1 Solvent Campaign

H3-1 Solvent Performance:  
~27% reduction in solvent regeneration energy, 35-45% reduction in circulation rate, low degradation compared to 30 wt% MEA

## CCSL Solvent Campaign

CCSL Solvent Performance:  
~30% reduction in solvent regeneration energy, 40% reduction in circulation rate, low degradation compared to 30 wt% MEA

## CAER Solvent Campaign

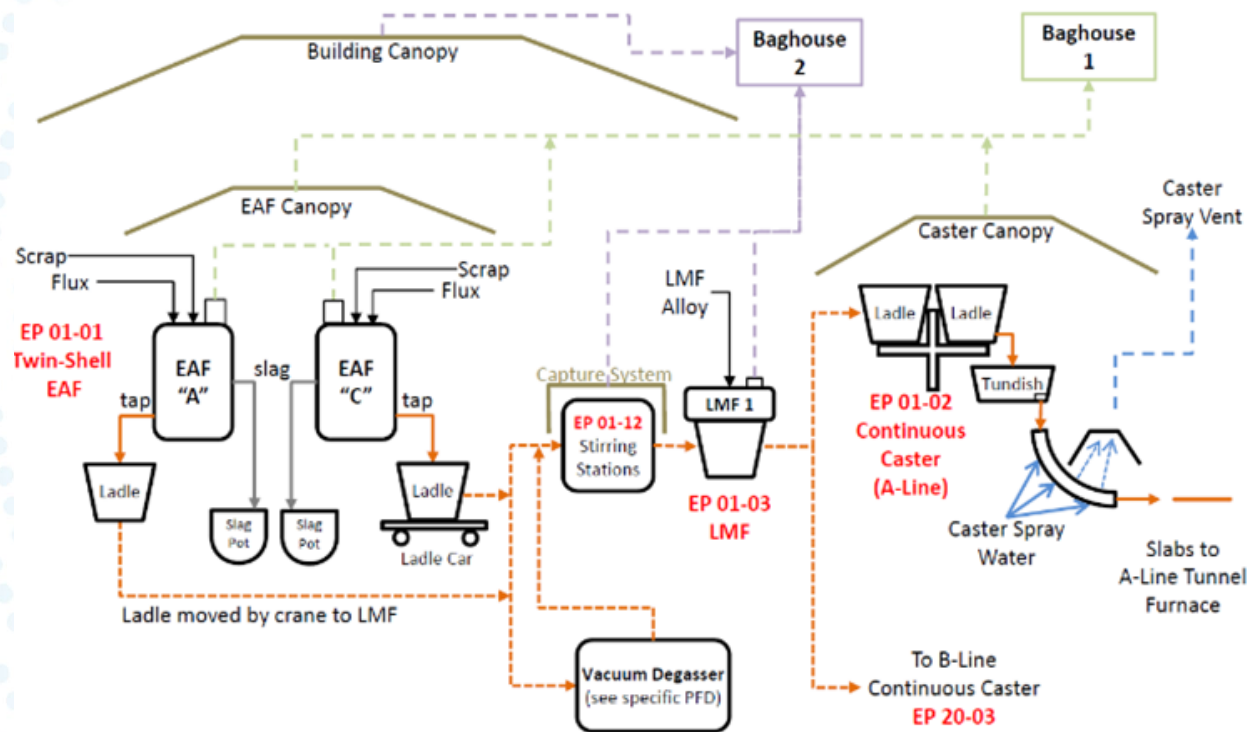
- CAER Solvent Performance: ~20% reduction in solvent regeneration energy, 30% reduction in circulation rate, low degradation compared to 30 wt% MEA
- Solvent Cost <\$5/kg chemical

## Process Modifications

- Absorber Temperature Control via discretized packing
- In-situ liquid redistributor
- Solvent spray with <50 µm droplets leads to 2.6-4.1X increased CO<sub>2</sub> absorption per unit volume
- Staged feed to Absorber and Stripper
- Heat Integration with steam cycle feedwater
- Solids circulation solvent recovery system reduces amine emissions by 50%

# Background – Adaptability and Conditions

- Low CO<sub>2</sub> concentration ~1.5 vol%
- Low SO<sub>2</sub>
- Low H<sub>2</sub>O



## Flue Gas Conditions

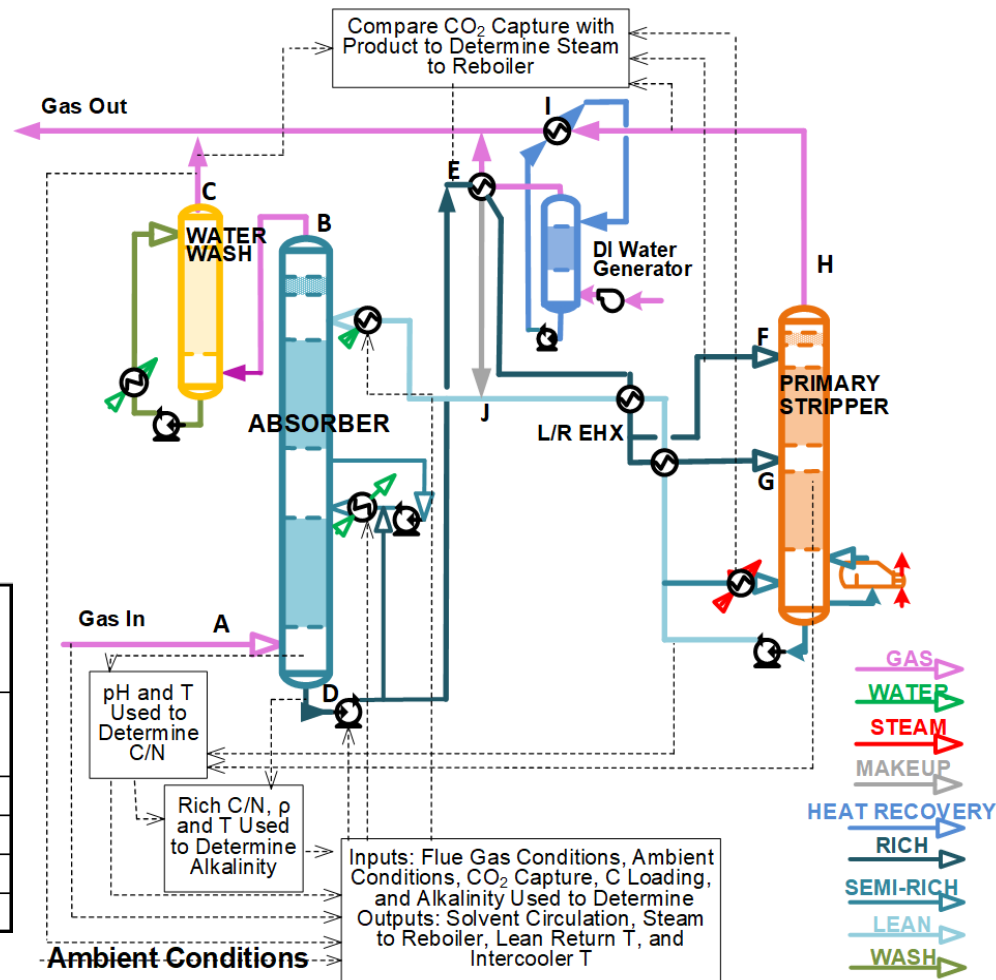
Gas Component	Value
CO <sub>2</sub> , vol%	0.5-1.5
O <sub>2</sub> , vol%	19-20
H <sub>2</sub> O, vol%	<5
SO <sub>2</sub> , ppm	0.23-4.5
NO <sub>x</sub> , ppm	1.6-5.2
N <sub>2</sub> +Ar	Balance
Flowrate, cfm	1,000,000
Temperature, °F	80-100
Pressure, psi	14.6



# Technical Approach

- Process Simplified
- Low L/G
- Specialized absorber packing
- Auto-set points for input energy minimization
- Lower specific reboiler duty via split rich stripper feed

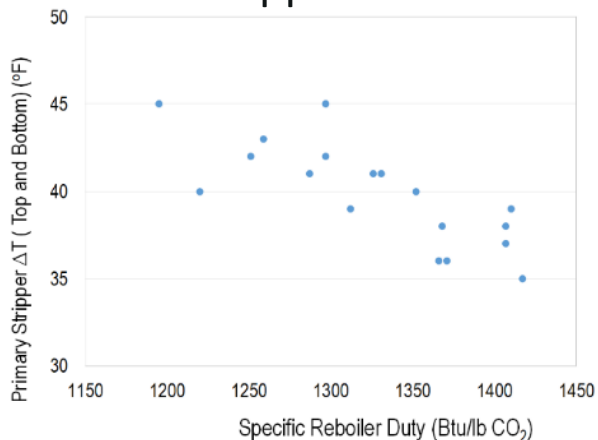
Split Flow % (Warm/ Hot)	CO <sub>2</sub> %	Solvent Flow (lb/hr)	% Capture	BTU/lbC O <sub>2</sub>	Lean Loading	Rich Loading
		DP (inH <sub>2</sub> O)			Alkalinity (mol/kg)	Alkalinity (mol/kg)
20%/ 80%	4%	100.1	86.8	945	0.66	1.72
		2.3			4.906	4.874
0/100%	4%	95.1	83.8	1073	1.09	1.89
		2.3			5.068	4.894



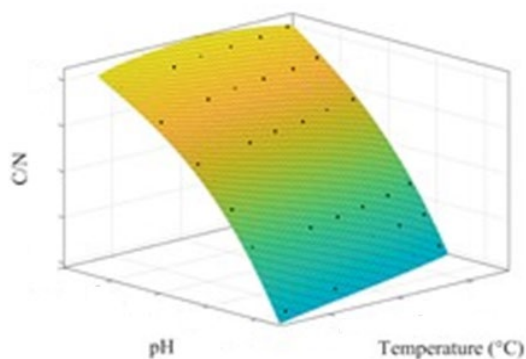
# Technical Approach

Just-in-time optimal operation via feed-forward process control strategy, collaborating with Emerson

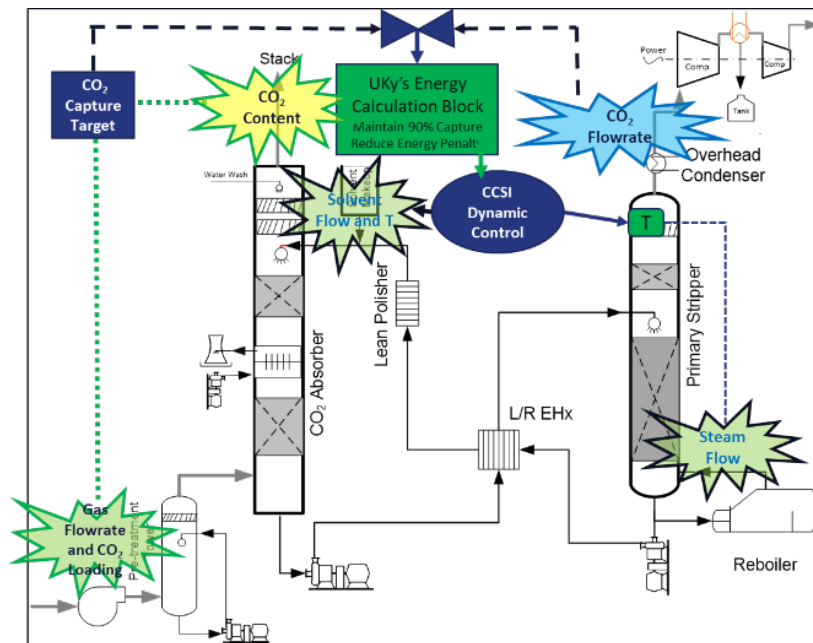
Energy Reduction with Higher Stripper  $\Delta T$



Relationship Among pH, T and C/N



Feed Forward Control



# Project Milestones

Task	Milestone Title/Description	Planned Completion Date
1.0	Project Kickoff Meeting Held	8/24/2022
1.2	TMP Complete	8/24/2022
2	Host Site Agreement (HSA) Complete	10/24/2022
3	PDP Complete	10/24/2022
3.2	Boiler Procurement Decision Point Meeting	8/24/2022
3.6	General Contractor Selected	4/24/2023
4.1	Nucor Site Prepared for Installation	6/24/2023
4.3	CCS Installed at Nucor	10/24/2023
5	Test Plan Complete	10/24/2023
6	Commissioning Complete	4/24/2024
7	Parametric/Dynamic Campaign Complete (Demonstrate 95% CO <sub>2</sub> capture efficiency and CO <sub>2</sub> product stream purity of ≥95%; quantify absorber performance and reboiler duty)	9/24/2024
8	Long-term Campaign Complete (1000 hours showing optimized process conditions, dynamic stability and operability)	12/24/2024
9	TEA Complete	1/24/2025
10	EH&S Complete	1/24/2025



# Project Success Criteria

Decision Point	Date	Success Criteria
Completion of BP1	4/24/2023	<ol style="list-style-type: none"> <li>1) Contract in place with engineering design firm for CCS reconfiguration and relocation</li> <li>2) Boiler specified and procured</li> <li>3) Contract in place with general contractor for relocation of CCS</li> </ol>
Completion of BP2	4/24/2024	<ol style="list-style-type: none"> <li>1) Commissioned CCS at Nucor Steel Gallatin Site</li> <li>2) Acceptance of test plan</li> </ol>
Project Completion	4/24/2025	<ol style="list-style-type: none"> <li>1) At least 2 months of engineering-scale testing campaign of three transformational CO<sub>2</sub> capture technologies at the Nucor Steel Gallatin Site.</li> <li>2) Demonstrated <math>\geq 95\%</math> CO<sub>2</sub> capture efficiency</li> <li>3) Demonstrated CO<sub>2</sub> product stream purity of <math>\geq 95\%</math></li> <li>4) Techno-economic analysis showing Cost of Capture and Cost of CO<sub>2</sub> Avoided, calculated for gross CO<sub>2</sub> captured and net CO<sub>2</sub> captured</li> <li>5) Attainment of TRL 6 of the three proposed transformational CO<sub>2</sub> capture technologies</li> </ol>

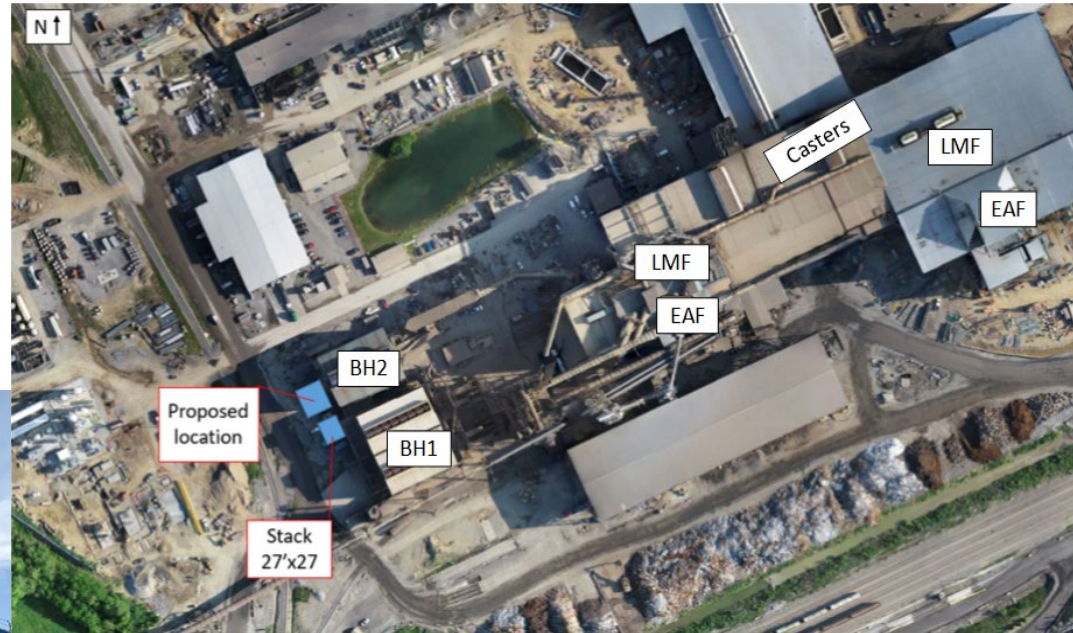
# Progress: Relocation Activities

BP1 Task		Progress
2	Host Site Agreement (HSA)	Communication between UK and Nucor
3	Unit Reconfiguration and Relocation Planning	<p>Quote for CO<sub>2</sub> capture unit reconfiguration received from KMPS.</p> <p>Quote for BOP and bid package preparation received from B&amp;M.</p>
3.1	Reconfiguration	
3.1.1	Absorber Internals	
3.1.2	Split Rich Stripper Feed	
3.1.1	Advanced Control Strategy	
3.1.4	Process Simplification	
3.2	Steam Generator Procurement	
3.3	Site Survey and Prep	Initial meeting with UK Purchasing held.
3.6	General Contractor Selection	
3.7	HAZOP	

Capital Project request defined by UK is in the process

- Board of Trustee approval
- Establishing plant account
- Issuing RFP for engineering firm selection
- Solicit public bid for BOP preparation and module relocation

# Location at Nucor Steel Gallatin





# Module Arrangement

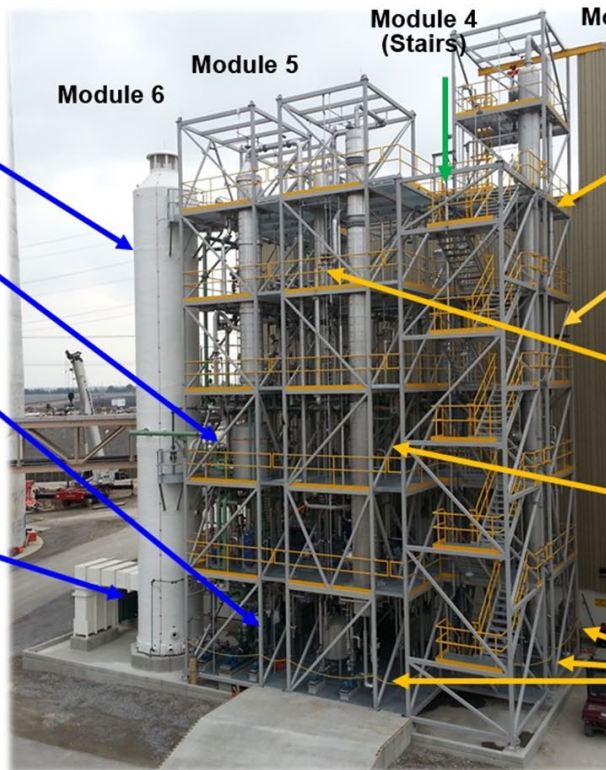
## Cooling Water Loop

Two-stage  
Cooling Tower

Cooling Water  
Holding Tank

Cooling Water  
Circulation  
pump

Cooling Tower  
Blower



## Amine Loop

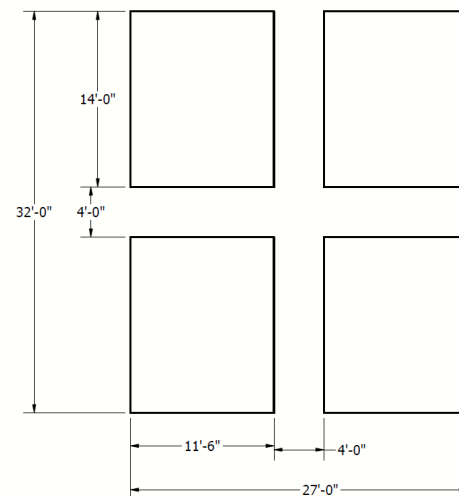
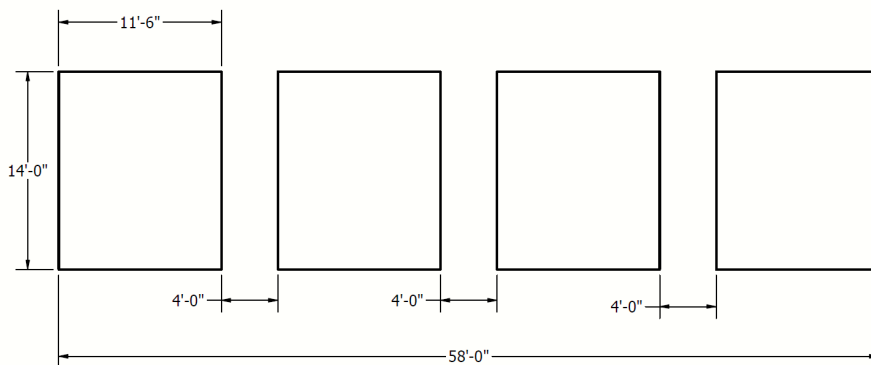
Absorber

Activated  
Carbon Filter

Primary  
Stripper

Secondary Air  
Stripper

Several Pumps



# Summary – Expected Output

- Firsthand experience and knowledge on low concentration CO<sub>2</sub> capture – performance, solvent management and dynamic operability
- Control strategy automatically maintains the target CO<sub>2</sub> capture efficiency while continuously minimizing the solvent regeneration energy.
- Full-scale deployment if the post-combustion CO<sub>2</sub> capture is feasible and cost effective

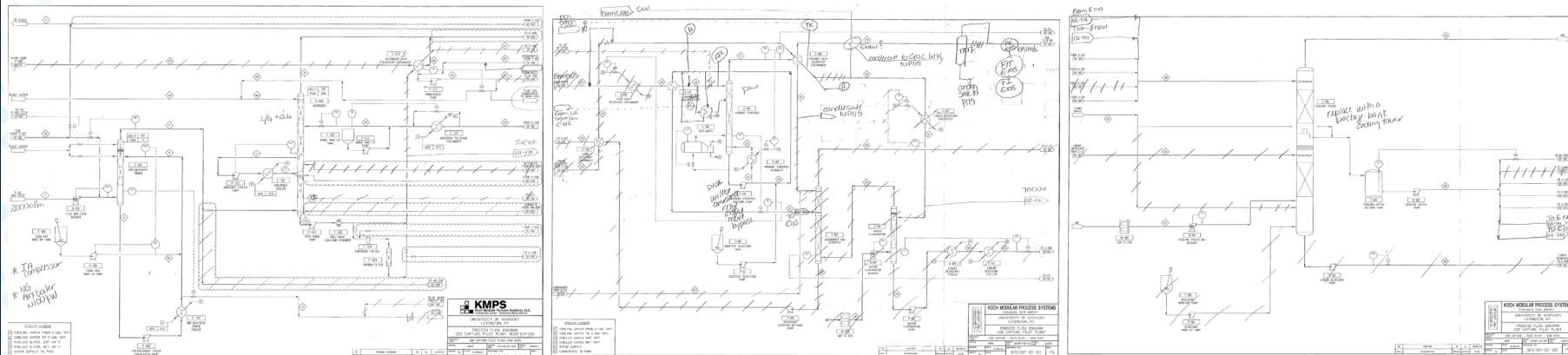
# Capture Process Simplification and Relocation

**Update:** PFDs, P&IDs, utility summary, 3-D model, piping isometrics, BOM, piping support details, heat tracing, stripper lead sheet for nozzle modification

**Evaluate equipment sizing:** pumps, P&F heat exchangers, B-101 with new specification if required

**Specify:** package cooling tower, air compressor, steam boiler,

**Verify:** in-line instrumentation for lower L, PSV relief scenarios





# Acknowledgements

U.S.DOE NETL: Krista Hill, Jose Figueroa, Dan Hancu and  
Lynn Brickett

Nucor Steel Gallatin: Gordon Ewell and Roy Syrmanske

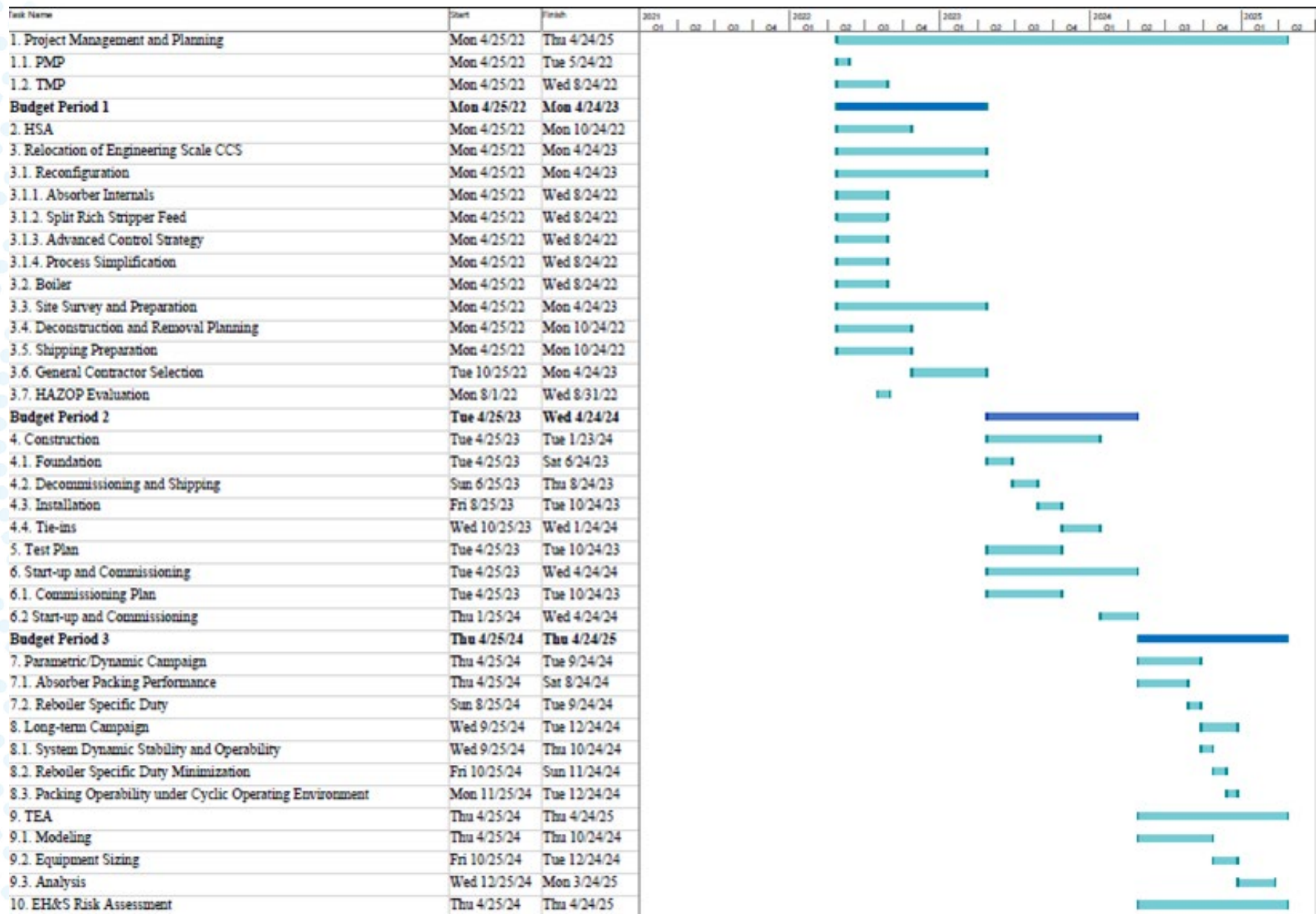
EPRI: Abhoyjit Bhowm

Emerson/Cornerstone: Vigen Biglari

ALL4: Clayton Whitney



# Appendix: Gantt Chart



# Appendix: Organizational Chart

