



Pilot Testing of a Modular System for Oxygen Production

DOE Cooperative Agreement DE-FE-0031527
2021 DOE/FE Spring R&D Project Review Meeting
May 4, 2021



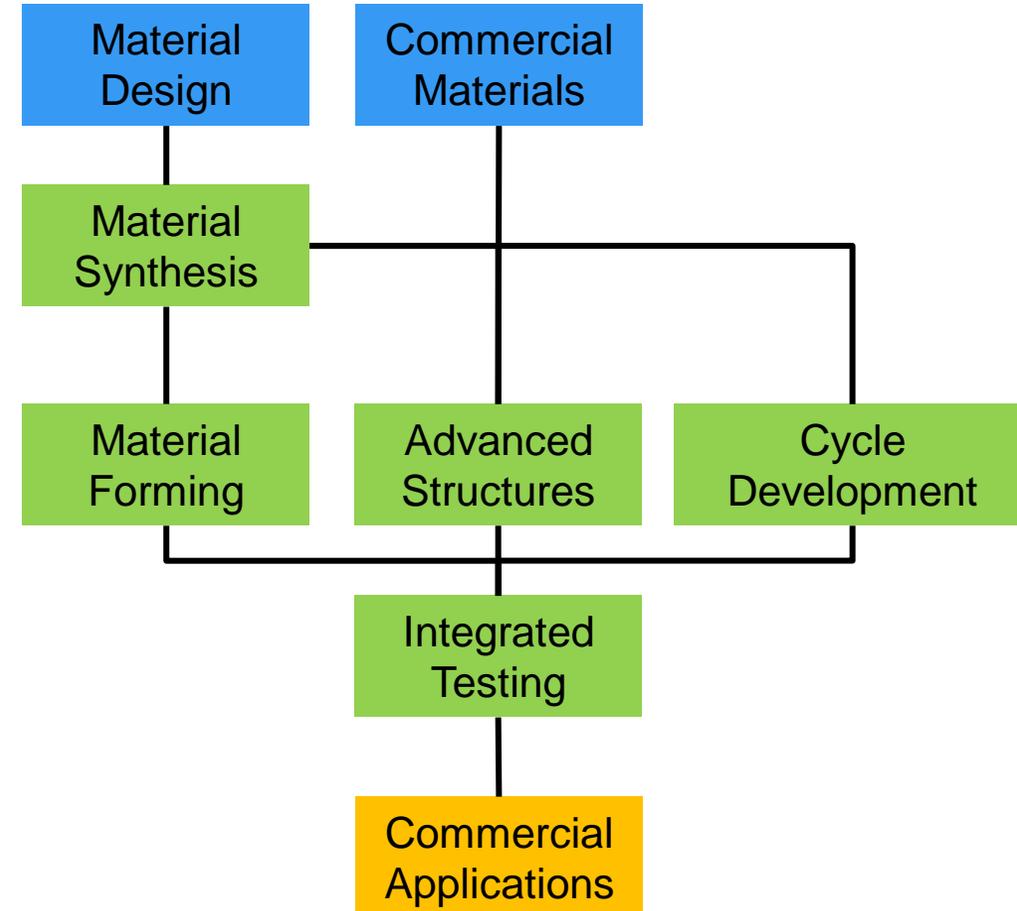
Project objectives

Objectives: The design, fabrication, and testing of a 10 to 20 kg/day modular oxygen (O₂) production system

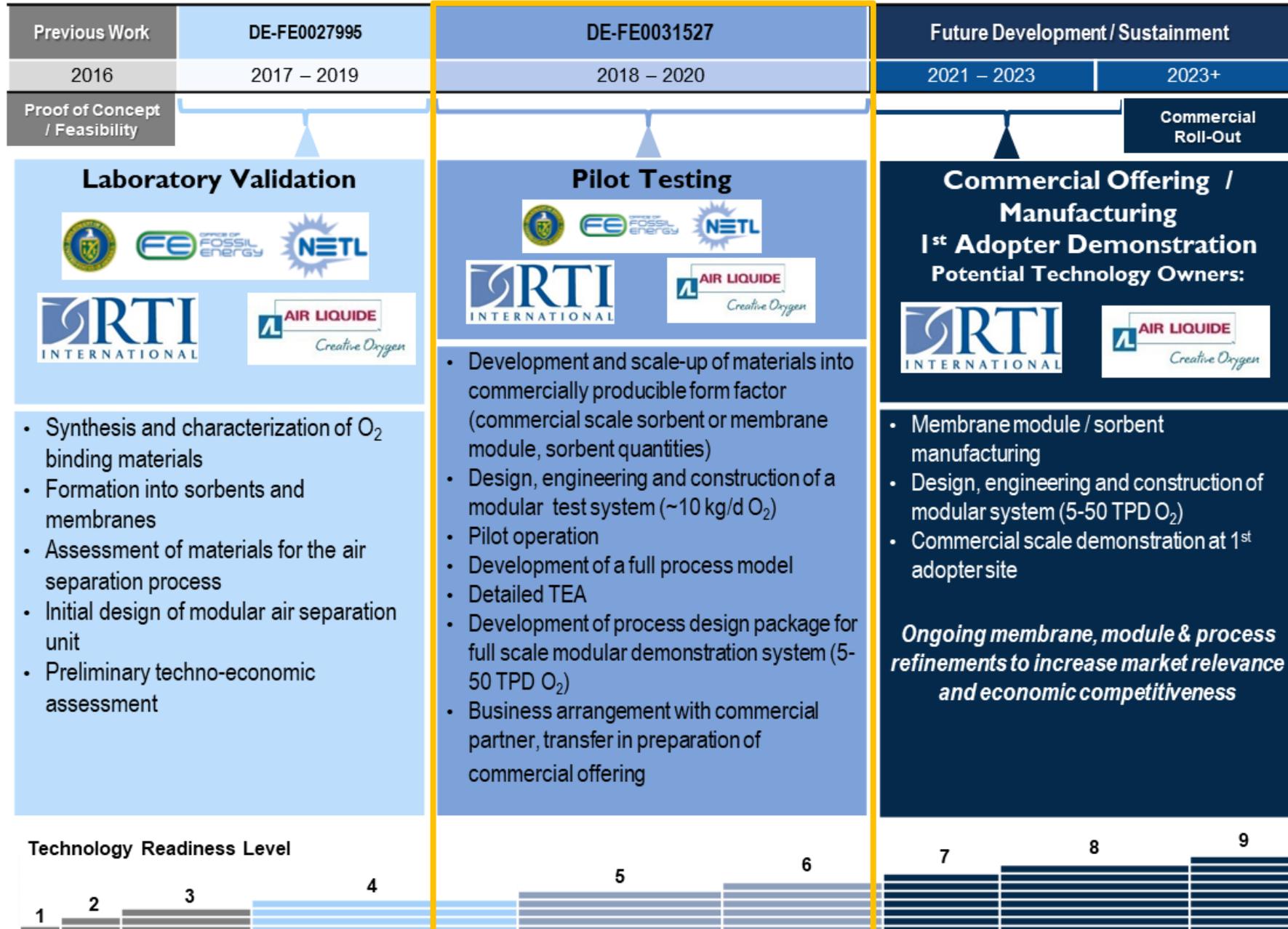
- Be cost competitive with current state-of-art process
- Modular process for small scale oxygen production
- Target lowering sorbent bed-factor

Specific Challenges

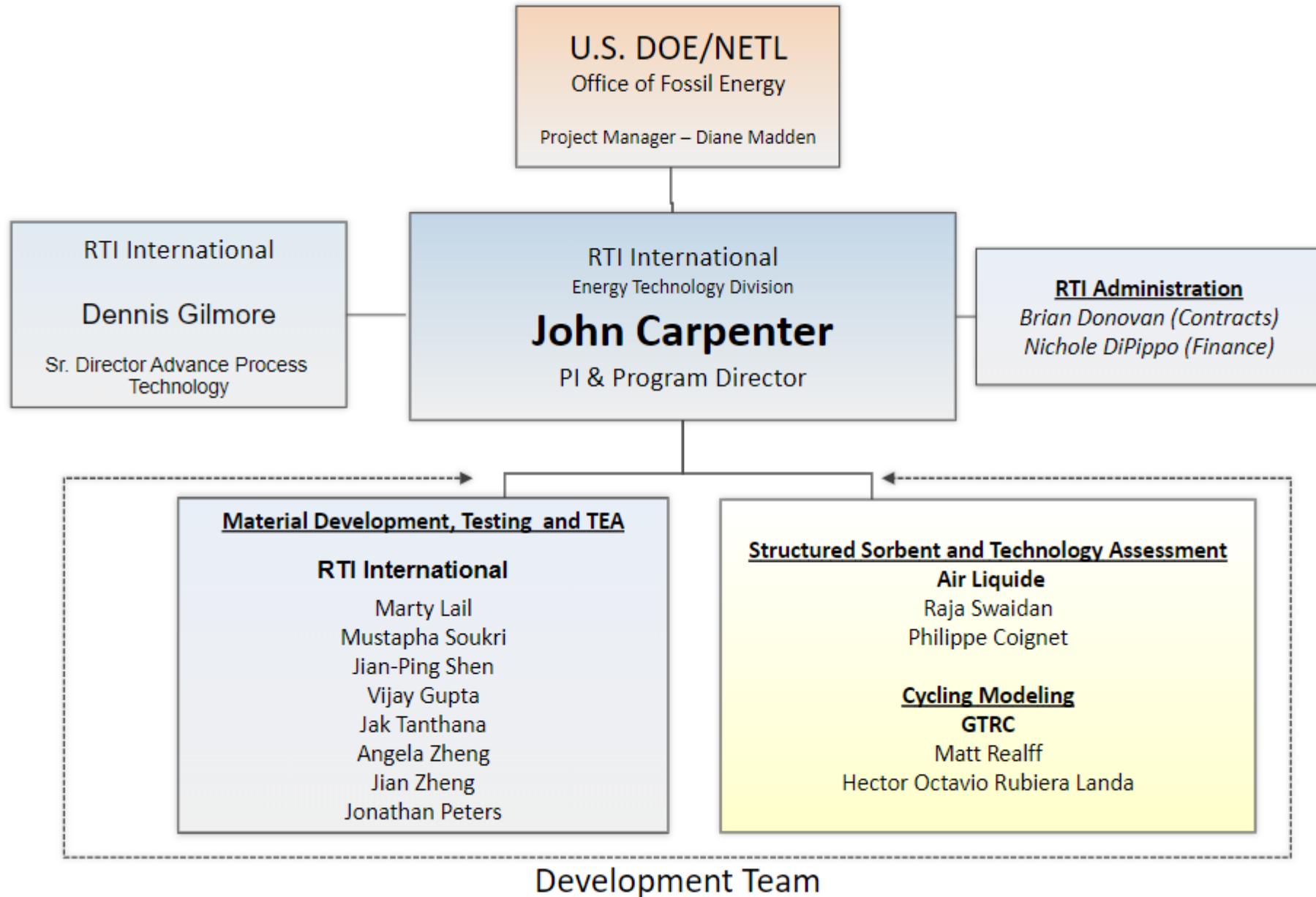
- Rapid PSA cycle development
- Structured sorbent module development
- Rapid cycle modeling tool development and cycle optimization
- Material and module scale up and manufacturing
- Design and fabrication of pilot O₂ production system
- Parametric and long-term testing
- Techno-economic analysis



Development Roadmap

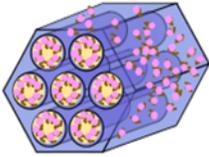
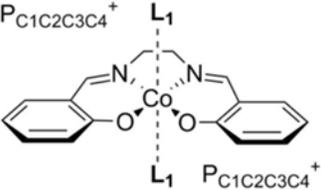
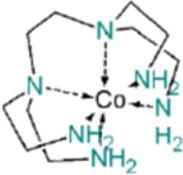
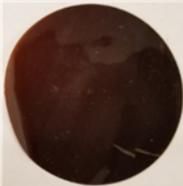
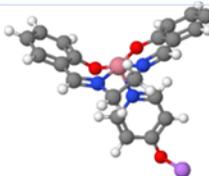


Project team

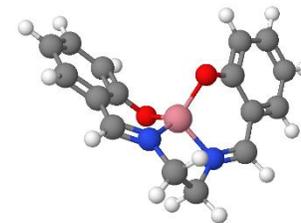
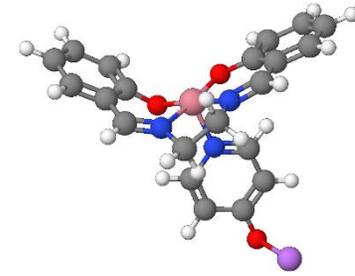
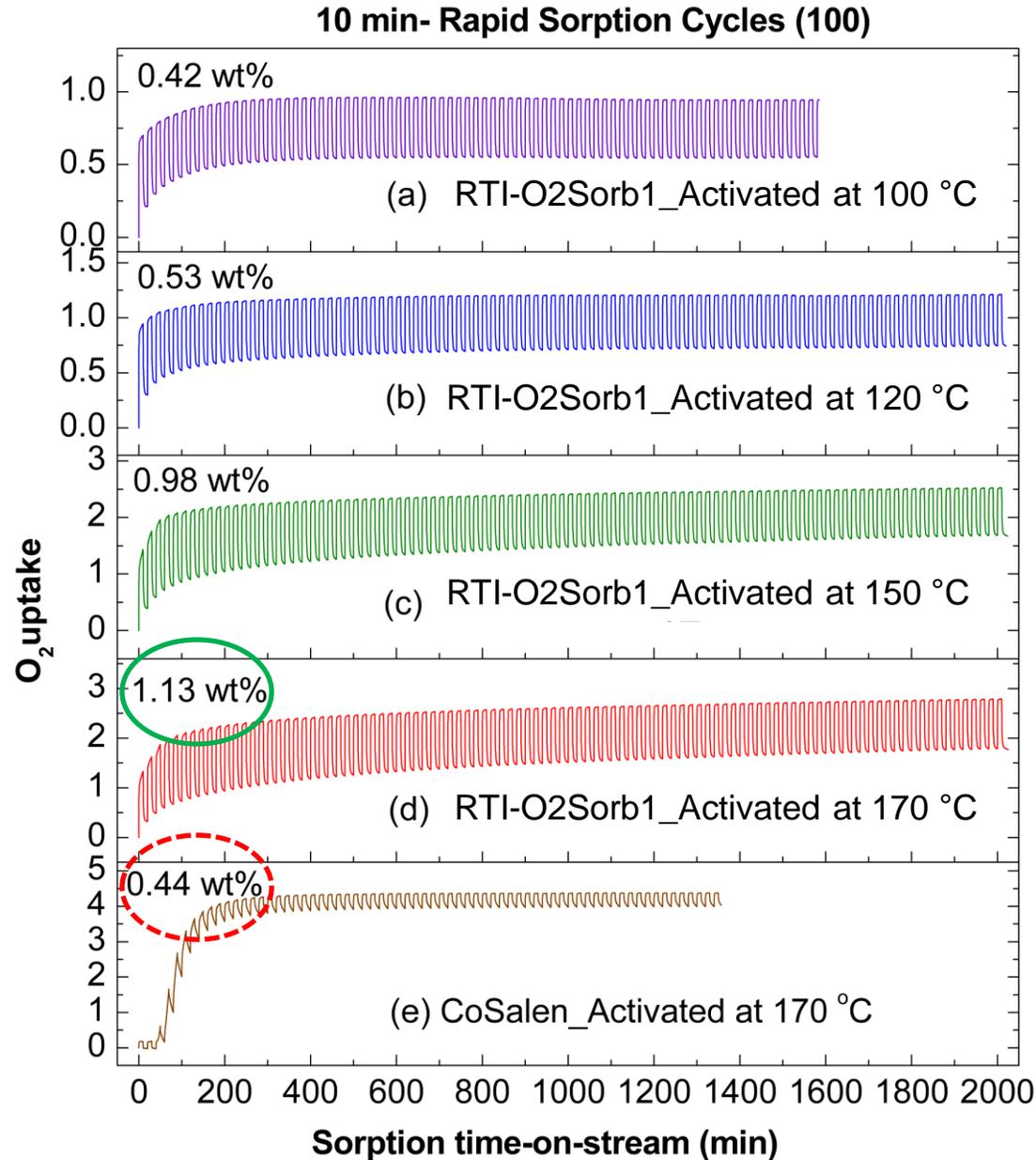


Materials Scale-up

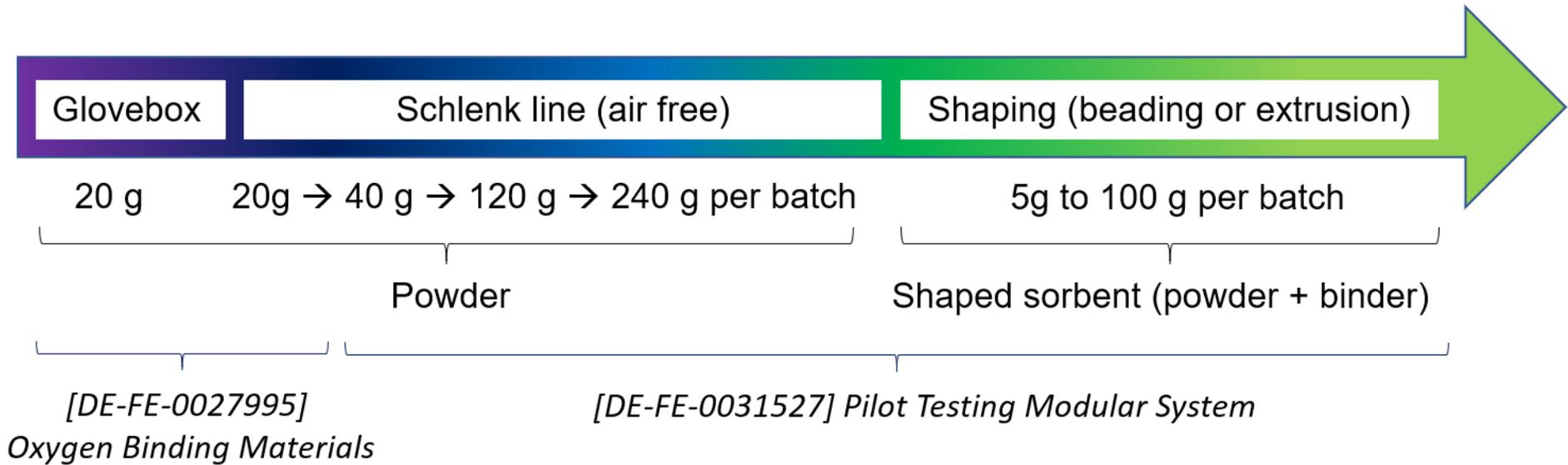
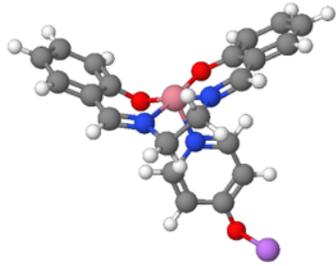
Bio-Inspired O₂ Sorbent Material Development Summary

Material type	Structure/ Illustration	Material form	Material performance
Co-organometallic complex/silica		Solid	<ul style="list-style-type: none"> Moderate O₂ sorption capacity (as high as 1.2 wt%) Slow O₂ sorption/ desorption kinetics Low O₂/ N₂ selectivity
Co Complex – Ionic Liquid	 <p>P_{C1C2C3C4}⁺ L₁</p> <p>L₁ P_{C1C2C3C4}⁺</p>	Ionic liquid	<ul style="list-style-type: none"> Moderate O₂ sorption capacity (as high as 1.1 wt%) Slow O₂ sorption/ desorption kinetics High O₂/ N₂ selectivity
Co Complex/ porous support	<ul style="list-style-type: none"> Complex on Mesoporous silica or zeolites O₂ binding metal organic frameworks 	Solid	<ul style="list-style-type: none"> Low-moderate O₂ sorption capacity Slow O₂ sorption/desorption kinetics Low O₂/ N₂ selectivity
Co-PEI		Solid/ Solution	<ul style="list-style-type: none"> High O₂ capacity, solid vs. liquid (3-6 wt% vs. 0.2 wt% in solution) Low O₂/ N₂ selectivity
Co Complex- O ₂ membrane	 <p>10 wt% Co Complex in Matrimid film</p>	Solid membrane	<ul style="list-style-type: none"> Low O₂/ N₂ selectivity
★ RTI-O2Sorb		Solid	<ul style="list-style-type: none"> ✓ High O₂ sorption capacity (as high as 3.0 wt%) ✓ Fast O₂ sorption kinetics (rapid cycle <10 min) ✓ High O₂/ N₂ selectivity

TGA Cyclic O₂ Sorption of RTI's RTI-O2Sorb1 vs. Commercial Co-Salen

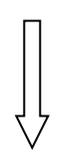
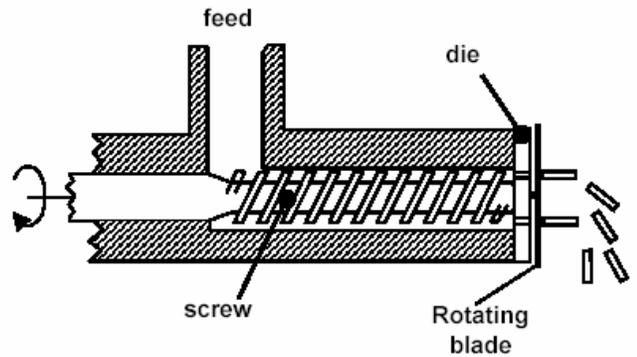
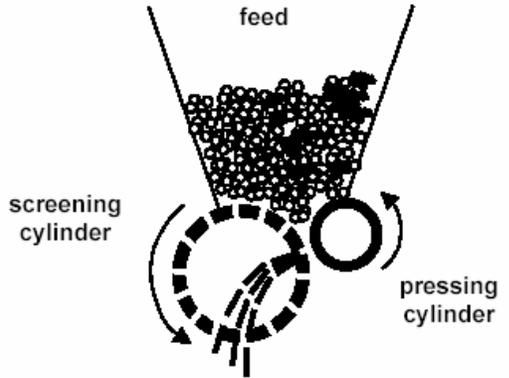
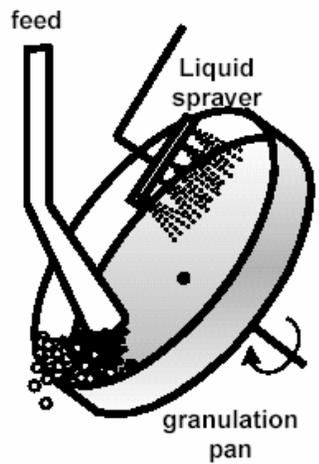


Progress on Scale-up of RTI-O2Sorb

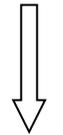


- ✓ **Successfully repeated batch synthesis for maximum O₂ sorption performance**
(reversible O₂ uptake of 1~1.5 wt% with powder sample after activation at 170 °C)
- ✓ **Successfully synthesized powder material with same performance using Schlenk line**
(which allows large batch synthesis)
- ✓ **Successfully scaled up powder material synthesis with same sorption performance**
(20g → 40 g → 120 g → 240 g per batch)

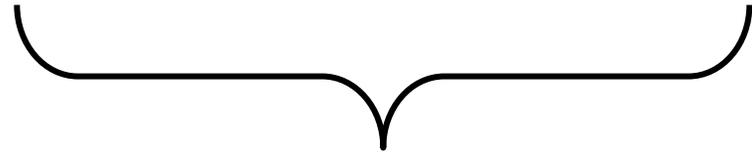
Agglomeration of Powder into Structured Form



Granulation

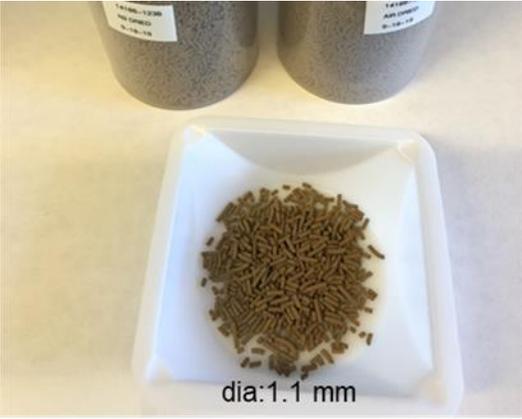
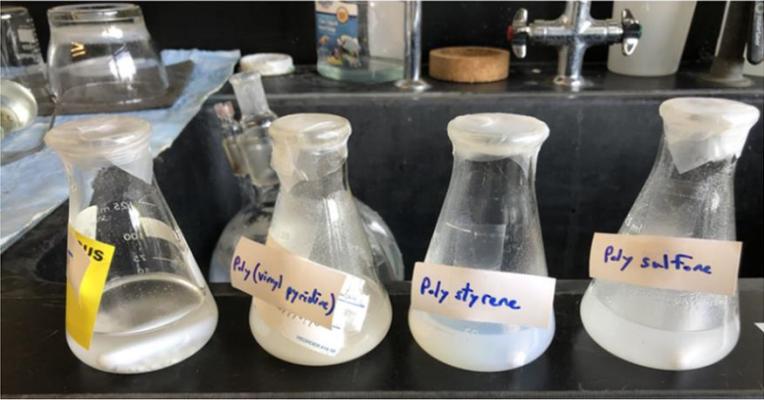


Pelletization



Extrusion

Optimization of Extrudate Formulation



After exposed in 100% O₂
@ 100°C 0.5hr,
and continued for 100 N₂-O₂ cycles

After normal N₂-O₂ 100 cycles

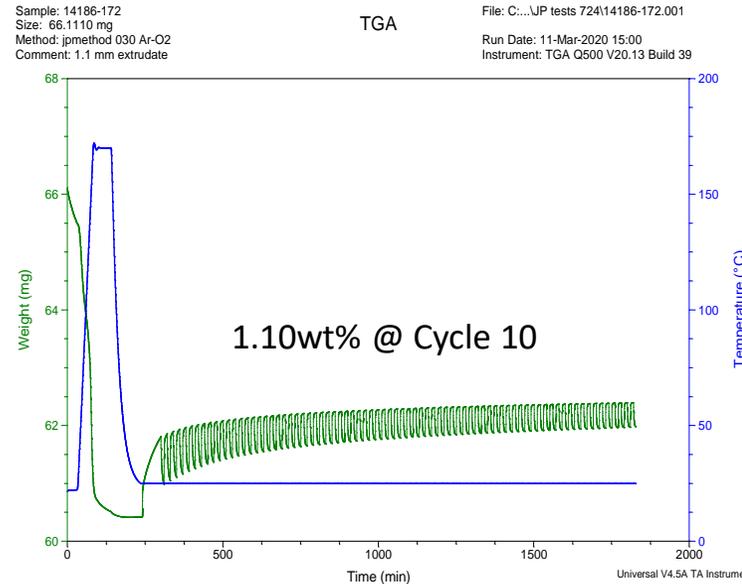
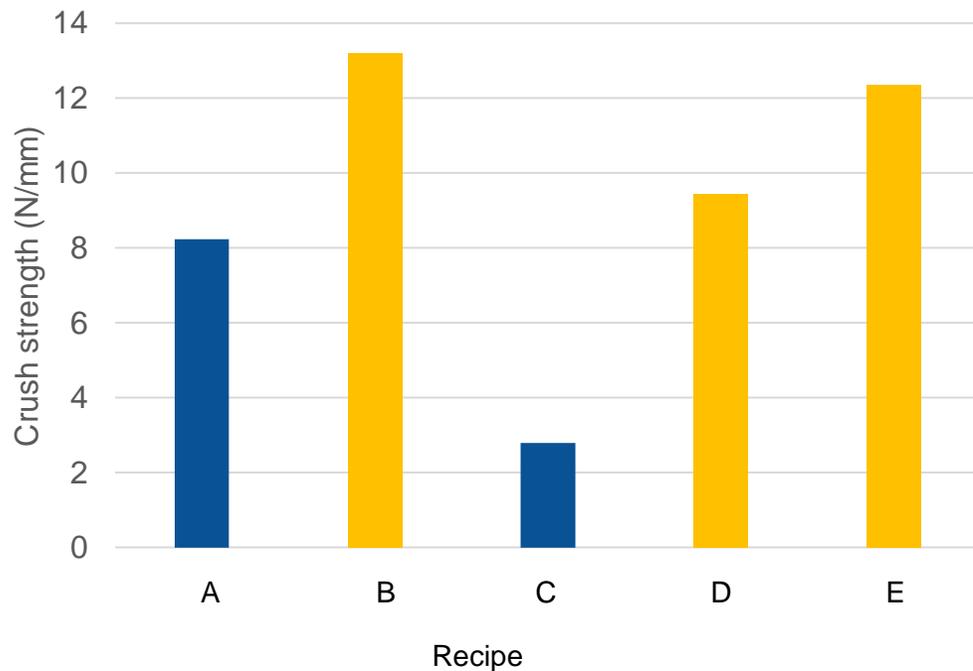
Extrudate Formation Characteristics

Key characteristics of Forming Extrudate:

- O₂ capacity, mechanical strength, size

Key variables of Forming Extrudate:

- binder ratios and solvent
- extrusion pressure and temperature, drying temperature



Dia (in)	Dia (mm)	N	N/mm
0.054	1.3716	13.6	9.915427
0.053	1.3462	21.4	15.8966
0.055	1.397	12.9	9.234073
0.052	1.3208	15.4	11.6596
0.052	1.3208	15.4	11.6596
0.054	1.3716	17.6	12.83173
0.052	1.3208	11.9	9.009691
0.053	1.3462	16.8	12.47957
0.052	1.3208	12.1	9.161114
0.055	1.397	11.8	8.446671
		Avg	11.02941

Binder (wt%)	Density (g/cc)	Dia. (mm)	Length (mm)	Crush strength (N/mm)	Dynamic oxygen capacity (wt%)
16.7	0.55-0.62	1.2-1.5	2.0-10.0	8.0-12.0	0.8-1.2

TGA Profile of Extrusion Shaped RTI-O2Sorb (crushed to 300~425 μm)



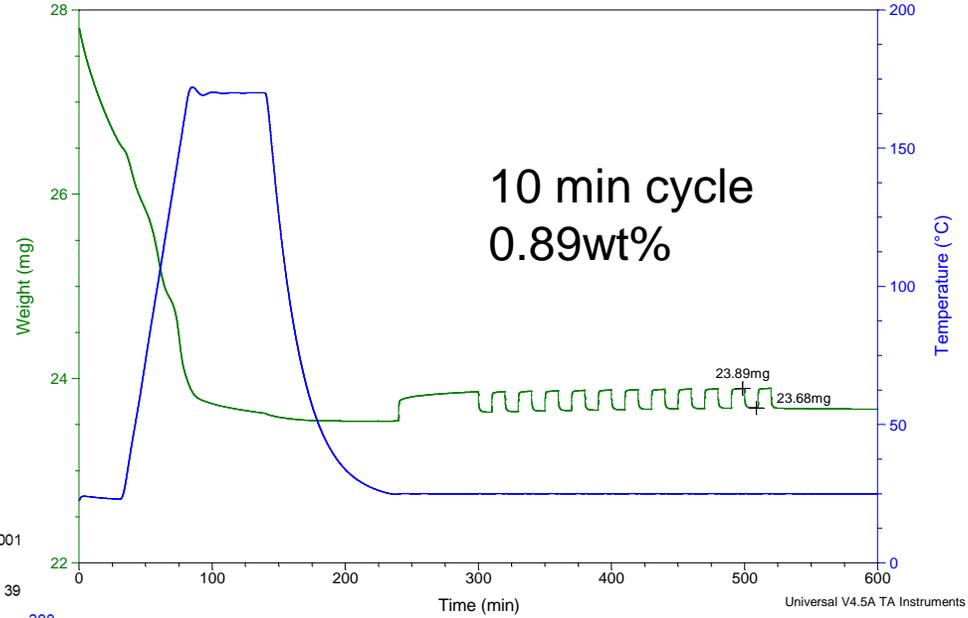
dia:1.1 mm

Sample: 14186-123B
 Size: 27.7990 mg
 Method: jpmethod 030 Ar-O2
 Comment: extrudate and crushed sieved 14186-123B N2 dried

TGA

File: C:\...JP tests 724\14186-123B.001

Run Date: 18-Sep-2019 17:37
 Instrument: TGA Q500 V20.13 Build 39

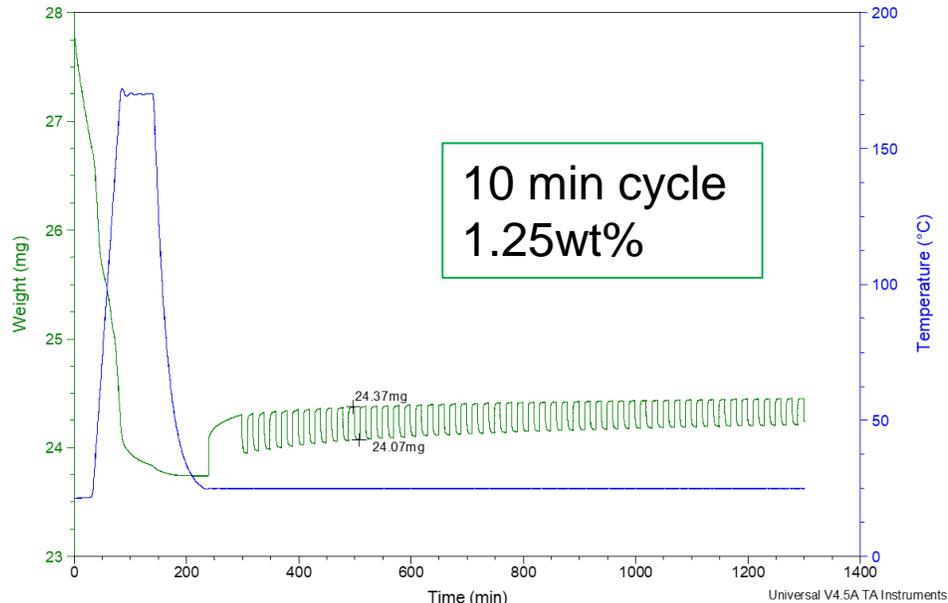


Sample: 14186-124A
 Size: 27.8430 mg
 Method: jpmethod 030 Ar-O2 long
 Comment: extrudate crushed sieved N2 comp dried

TGA

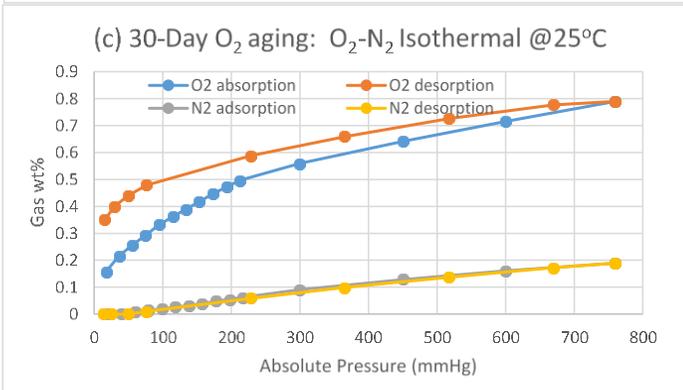
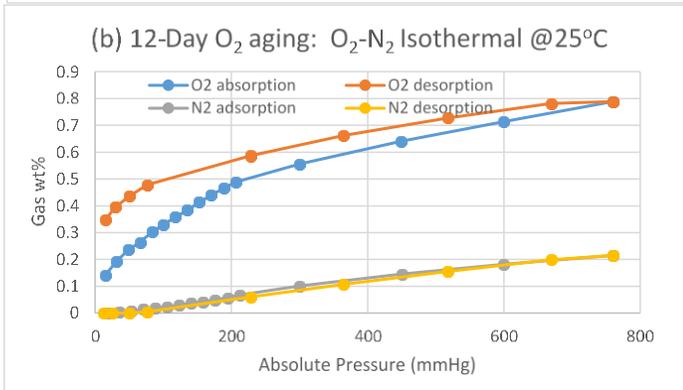
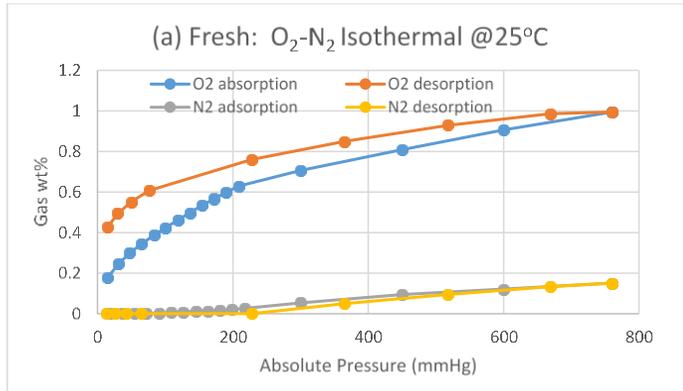
File: C:\...JP tests 724\14186-124A.001

Run Date: 22-Sep-2019 12:51
 Instrument: TGA Q500 V20.13 Build 39

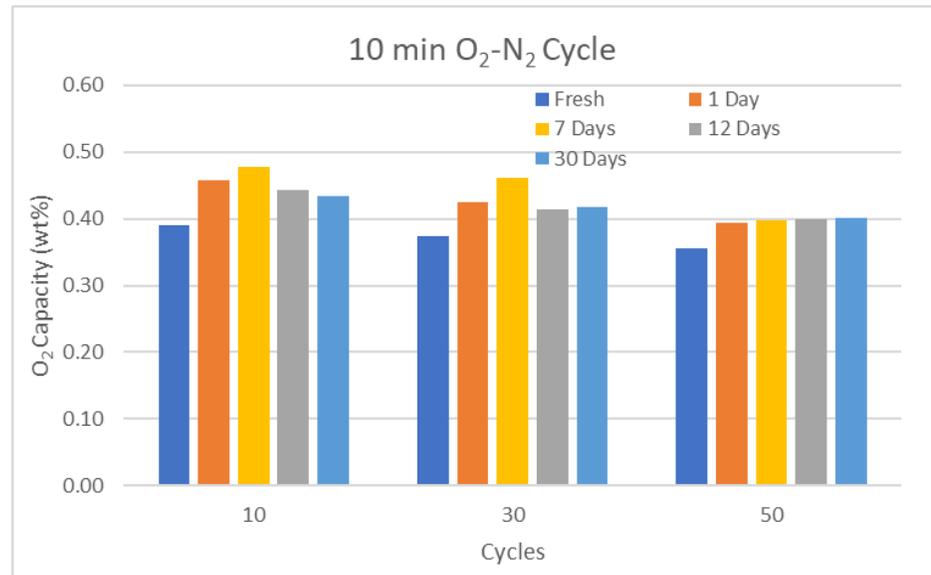
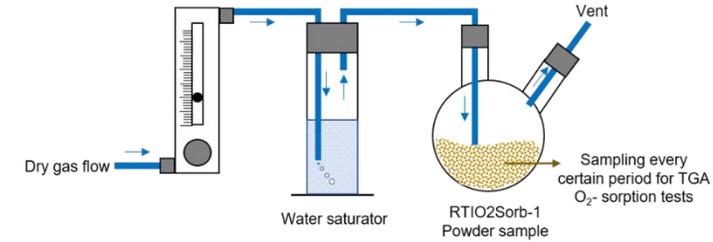


dia:2.2 mm

Exposure/Aging Testing



- 2.62 vol% H₂O (g), balance N₂
 - 45d exposed, similar to long term cycling
- 1.5% O₂, 19.5 CO₂, balance N₂
 - Exposed 36d – no degradation
- 2.62 vol% H₂O (g), 20.40% O₂, balance N₂
 - Similar to long term cycling in TGA
- 99% vol% O₂, , balance N₂
 - Some degradation through day 12,
 - day 30 similar to day 12 (See graphic to left)



Forming of Structured Sorbents



Air Liquide Objectives:

- Develop novel structured adsorbents production techniques using conventional sorbent materials
- Apply and adapt the techniques developed on conventional adsorbents to the novel oxygen-binding adsorbent materials
- Manufacture and ship 2 to 4 structured adsorbers for pilot testing based on novel oxygen-binding adsorbent
- Support activities (e.g. Pilot design, Techno-Economic Analysis)

Focus on Traditional Materials

- Air Liquide BP1 objectives successfully met on time (*by June 30th, 2019*)
- Formulations were developed and characterized for (1) air dehumidification and (2) for conventional nitrogen (N₂)-binding adsorbent
- Activation protocols for each adsorbent formulation were developed
- Forming techniques to produce structured beds were developed

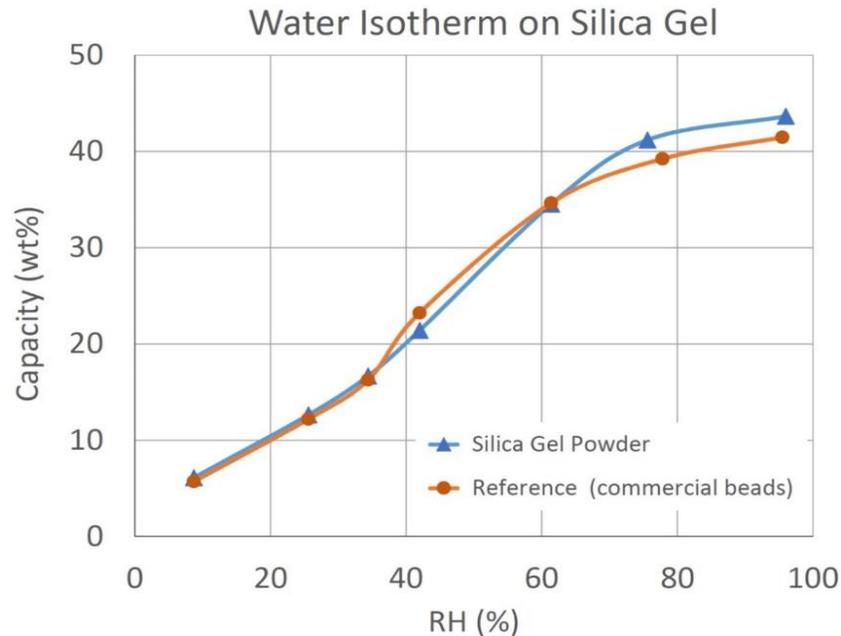
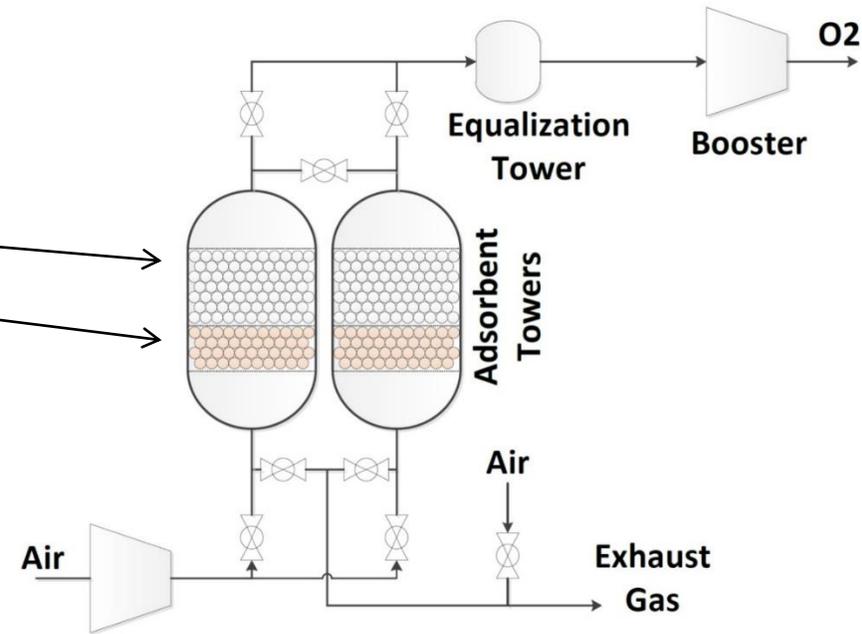
Adapting Method to RTI Sorbent

- Forming techniques and activation tool were scaled up for beds of up to 1 kilogram
- Reviewed and provided feedback on the pilot design
- Explored adapting formulation and forming techniques to novel oxygen-binding adsorbent. Multiple samples were received from RTI, characterized and used to support adaptation-work on formulation and forming

Sorbent and Structured Sorbent Module Development and Characterization

Overall Approach

- Conventional O₂ VSA → uses 2 adsorbents
- Top adsorbent used to capture N₂
- Bottom adsorbent used for air drying
- Structured beds made of elementary shapes
- Elementary shapes produced by combining adsorbent powder and binder

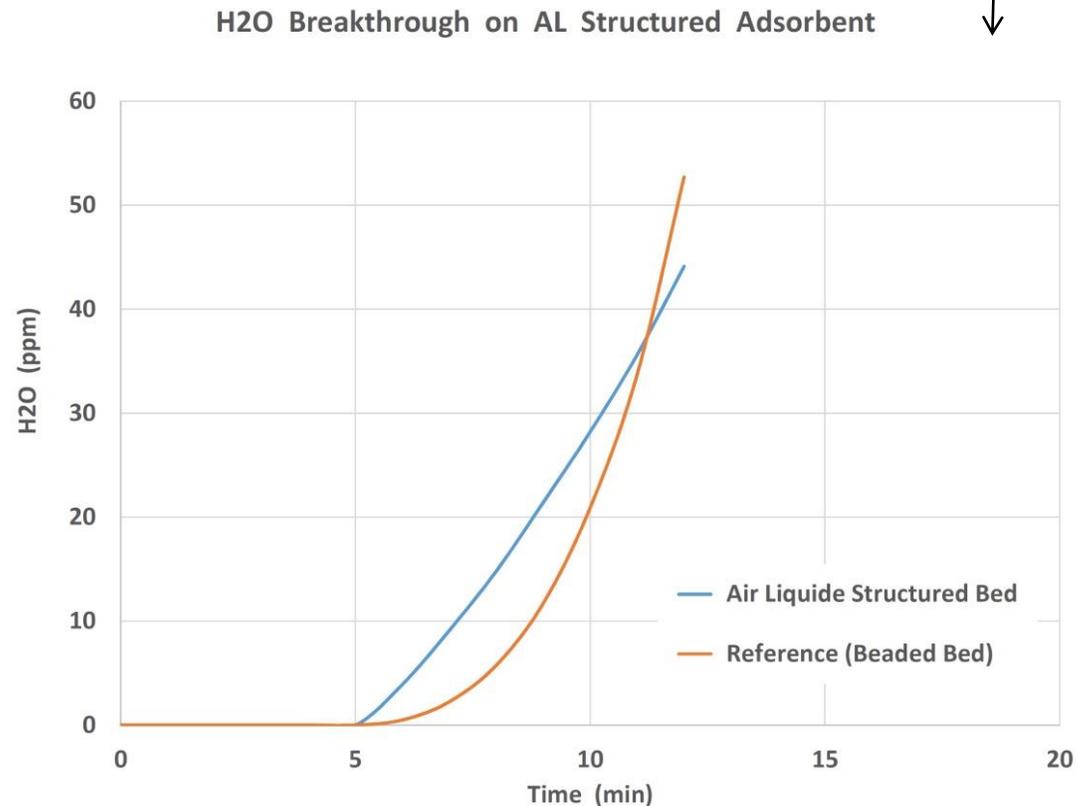


Air Drying / Multi-Steps Approach

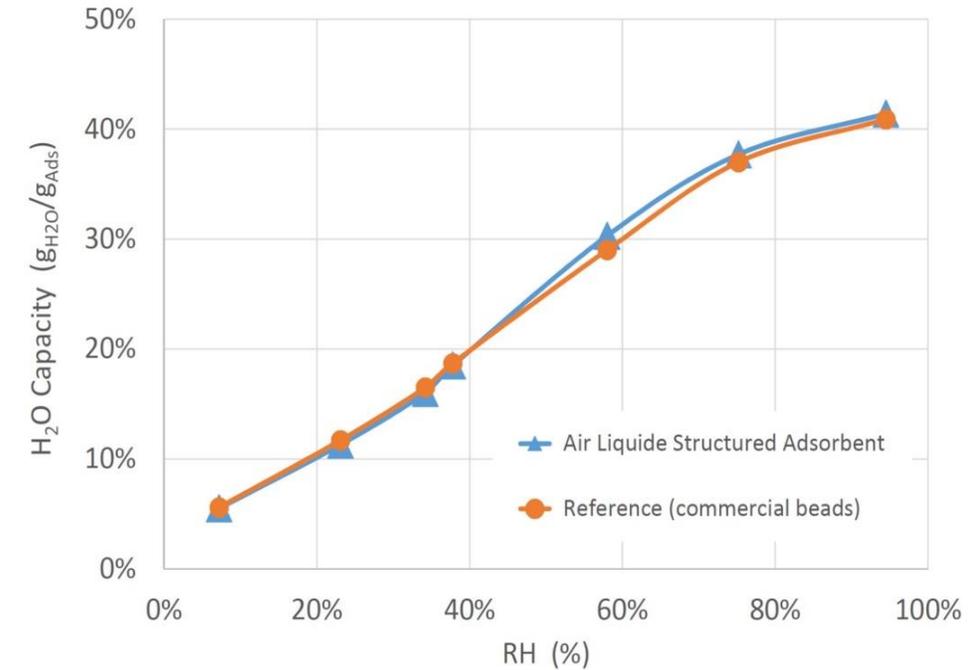
- 2 options: activated alumina (AA) or silica gel (SG)
- SG powder selected based on its highest water capacity
- SG powder formed with a binder into elementary shapes

Air Drying / Multi-Steps Approach

- H₂O capacity of SG elementary shapes meets expectations
- Small scale structured SG-bed formed and characterized
 - H₂O breakthrough curve comparable to conventional beaded bed
 - Pressure drop comparable to conventional beaded bed

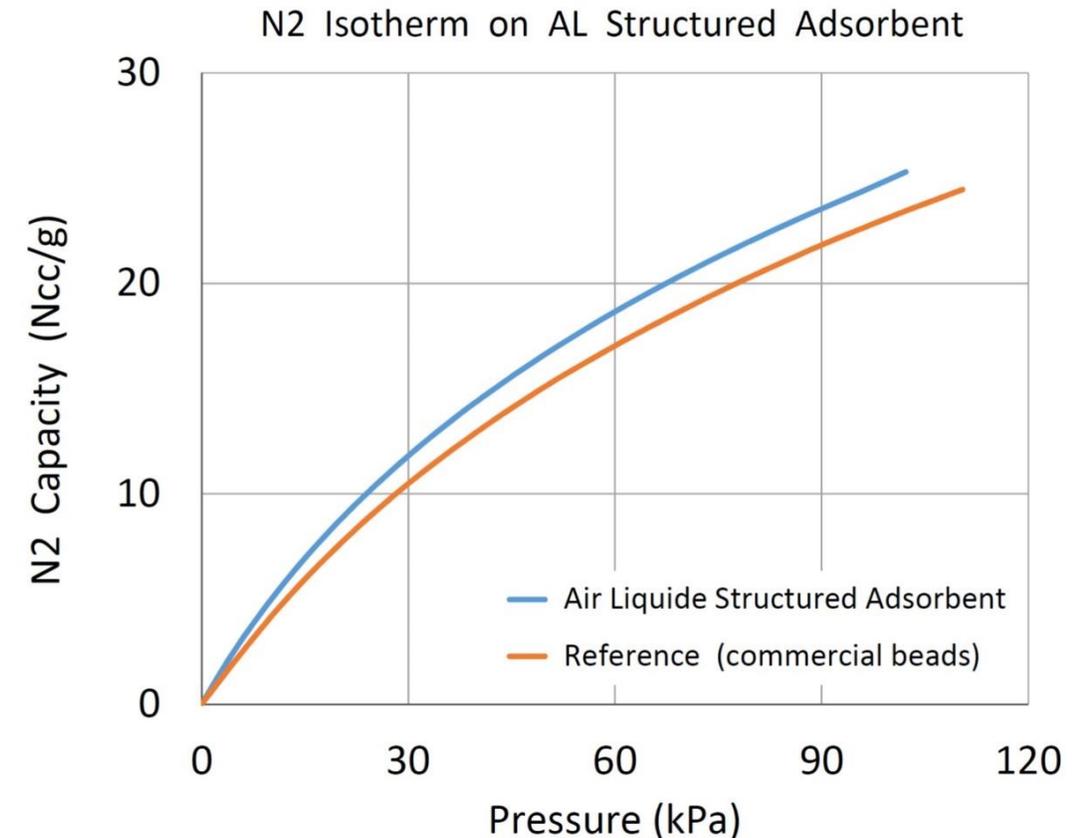


Water Isotherm At 22°C on Silica Gel



N₂ Adsorbent / Multi-Steps Approach

- Various zeolites typically used as N₂ binding adsorbents
- Selection of zeolite powder
- Forming with binder
- High temperature activation
- Similar N₂ capacity & selectivity compared to commercial adsorbents
- Faster kinetics



Adaptation Work on Novel O₂ Binding Adsorbent

- Goal: form structured bed with novel adsorbent by adapting techniques developed with traditional sorbents
- Focused on producing an advantageous elementary shape while managing specific limitations of novel adsorbent
- An advantageous elementary shape is fast to produce and can yield low pressure drop once formed into a structured bed
- Performance of the formed adsorbent is checked by running N₂/O₂ isotherms on elementary shapes
- Forming of the novel O₂ binding adsorbent was unable to achieve mechanical strength for full module forming
- Focused on extrudate formations



Novel powder of O₂ binding adsorbent

Cycle Modeling



Development of a vacuum pressure-swing adsorption (VPSA) full-order solver

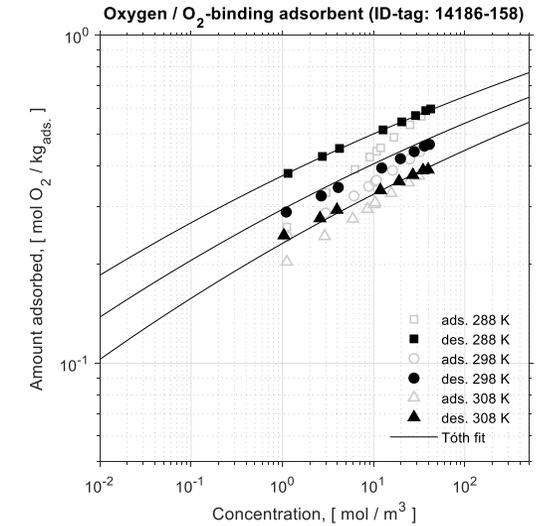
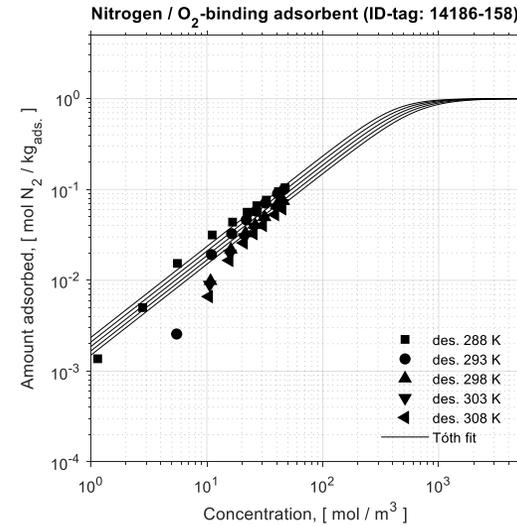
Process modeling

- 1D PDE system describing transient fixed-bed adsorber equations for 7 state variables: gas-phase compositions, adsorbed-phase concentrations, pressure, bed & casing temperatures
- Competitive **adsorption equilibria** modeled w/ IAST
- Linear driving-force (LDF) approximation for mass transfer
- First-principles heat transfer modeling considered
- Solved numerically w/ Finite Volume Method (FVM)
- Coded in MATLAB

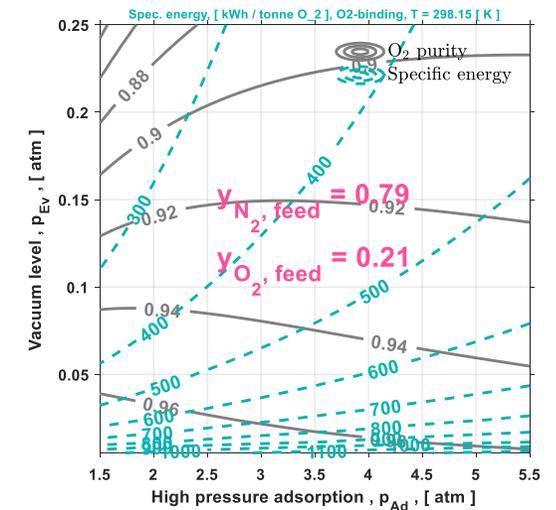
Optimization

- Multi-objective optimization of relevant VPSA performance variables using genetic & surrogate-based algorithms

Adsorption equilibria

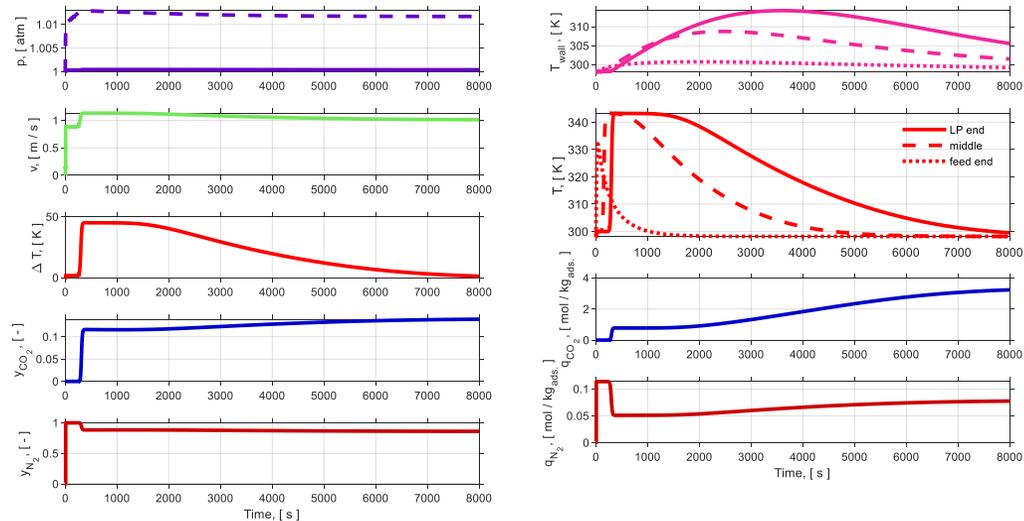


- Applied a short-cut method to test IAST implementation and obtain preliminary assessment for the oxygen-binding adsorbent

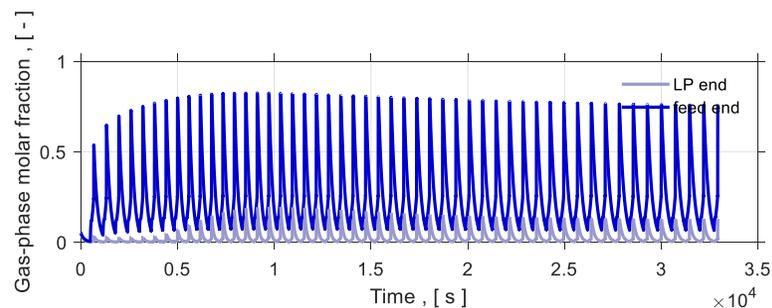


Flue-gas separation results for model validation

- Dynamic column breakthrough (DCB)

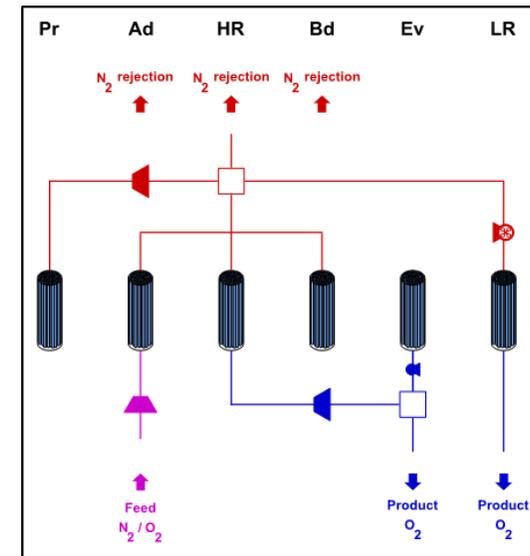


- 4-step VPSA w/ LPP for heavy-product recovery



On-going sub-tasks

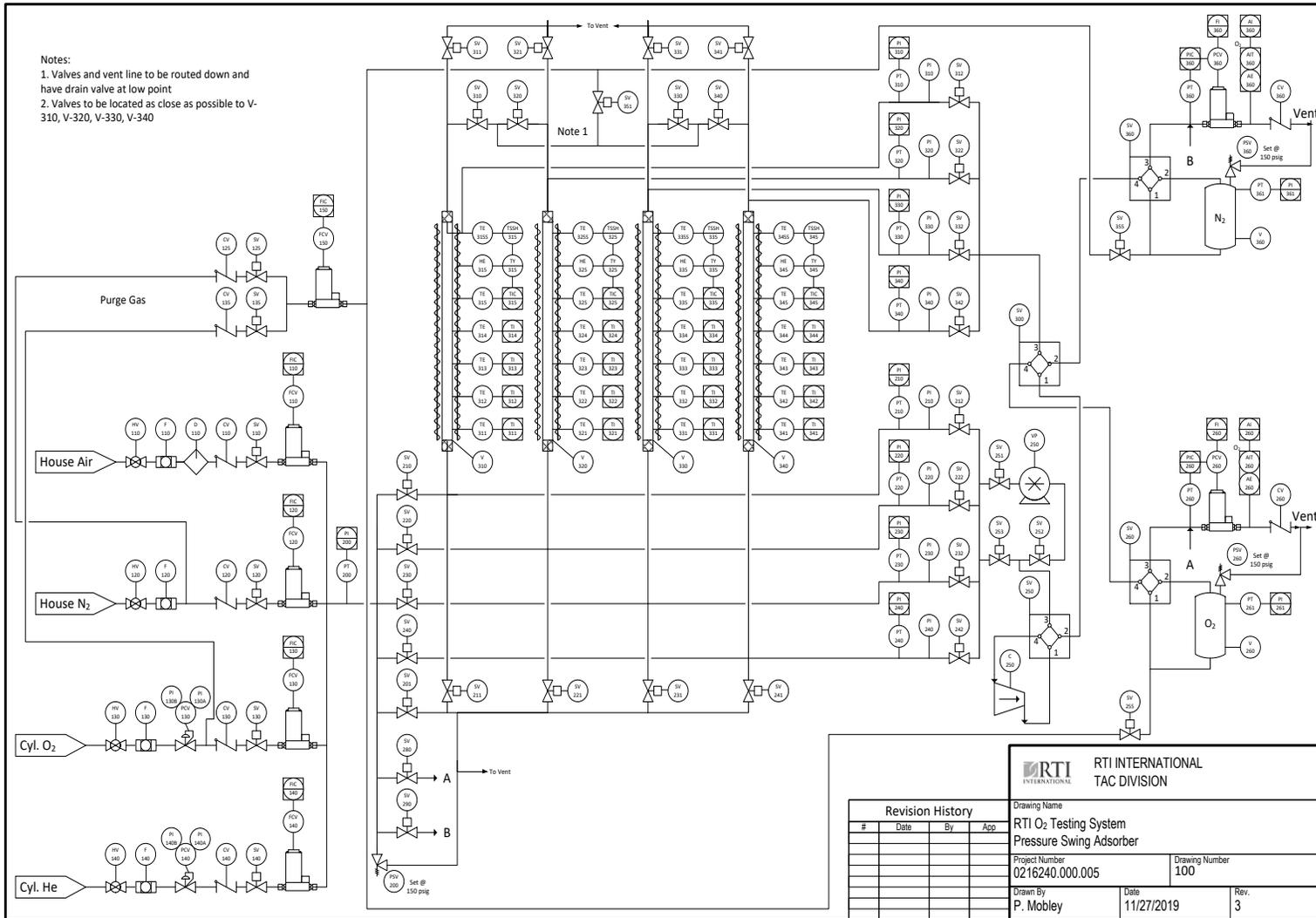
- Implementation of 6-step cycle to simulate the operation of the air separation skid under construction



- Efficiency improvements of IAST calculations to speed-up optimization runs
- Implementation & execution of multi-objective optimization runs for 4-step and 6-step cycles to identify suitable operating conditions

Integrated Test Skid

10 kg Pilot Modular System Process Flow Diagram



- O₂ production rate
- O₂ purity
- Cycle optimization
- Bed size factor
- Unit power consumption
- Material stability

- Techno-economic analysis for O₂ cost projection

Steps

- HMB
- Sizing
- Safety Review Internal
- AL feedback
- Order Key Instruments
- Fabrication\Controls Commissioning
- Testing

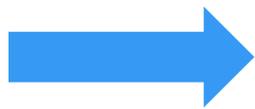
Kg Extrudate Production

Produced 2.4 kg of O₂ Sorb in extrudate form

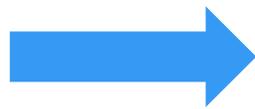
- Due to size limitations of equipment this was performed in 150-250 gm batches



Forming



Drying

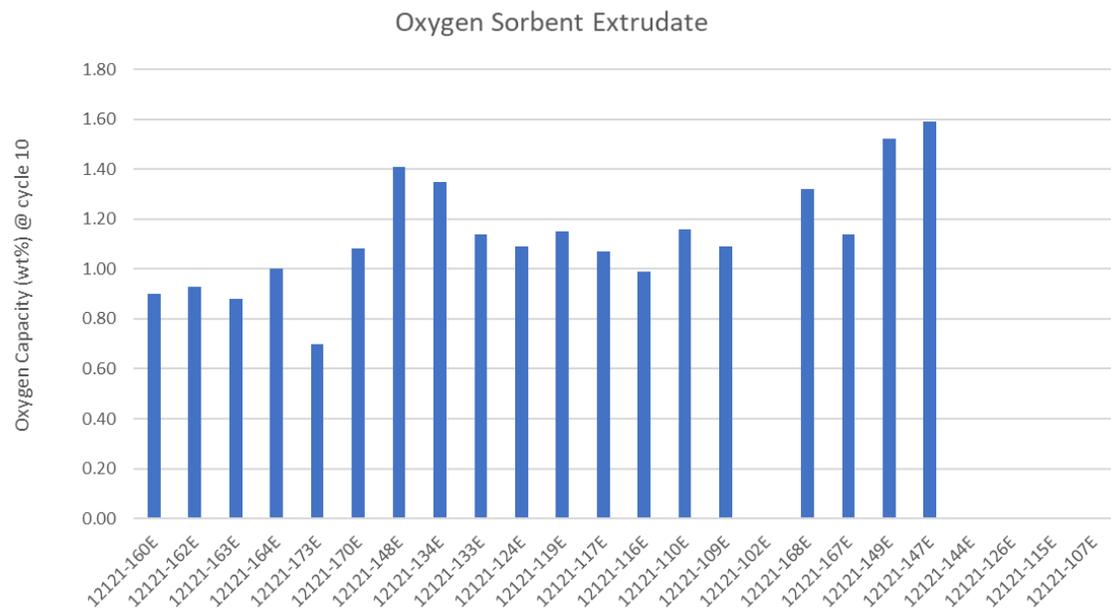


Sizing

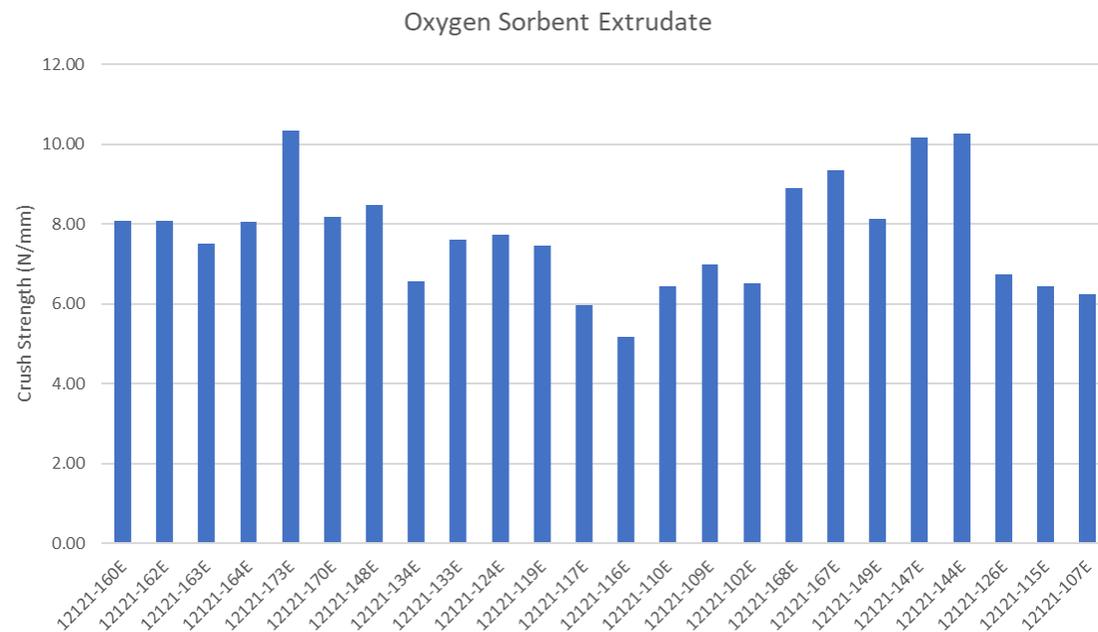
Kg Extrudate Characterization

Key characterizations were O₂ capacity under standard TGA test and crush strength

- Some variation from batch to batch



Target was > 1.0 wt% in TGA testing for goal of achieving > 0.5 wt% working capacity

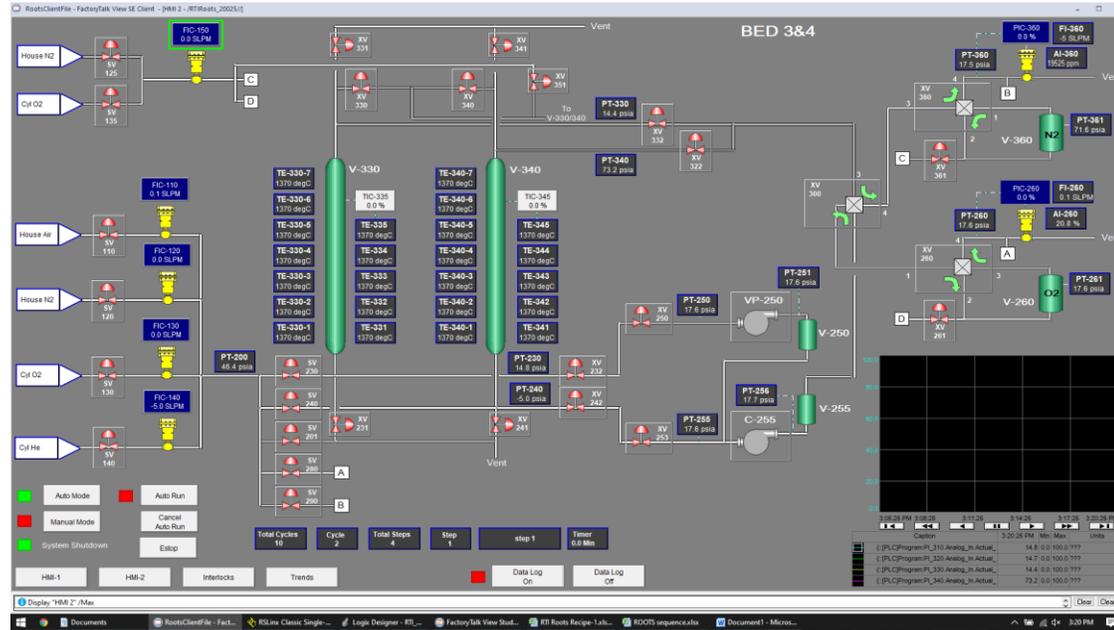


Target was > 5 N/mm in axial crush strength similar to commercial materials of similar structure

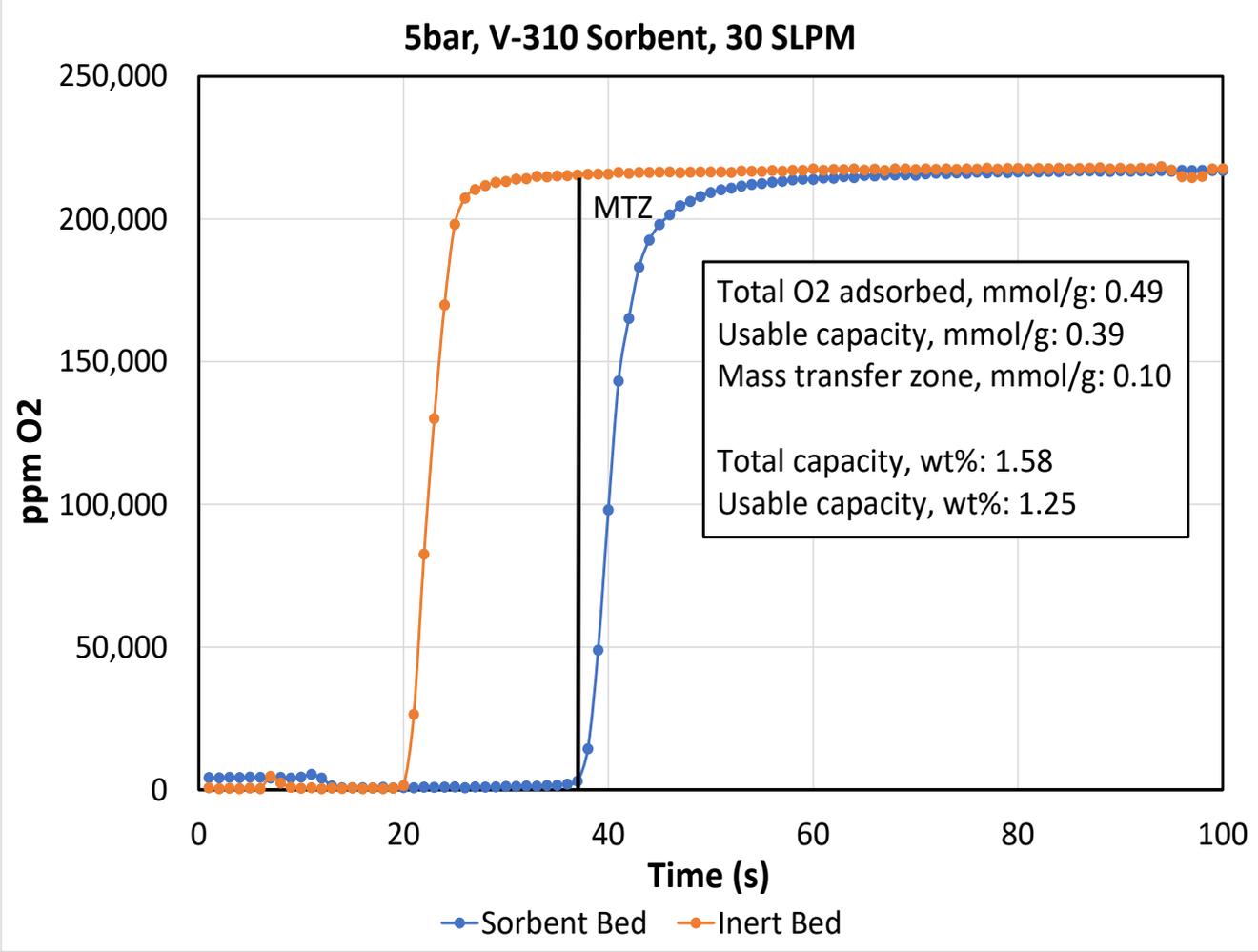
10 kg Pilot Modular System Build



10 kg Pilot Modular System Controls



System Characterization – Breakthrough Testing

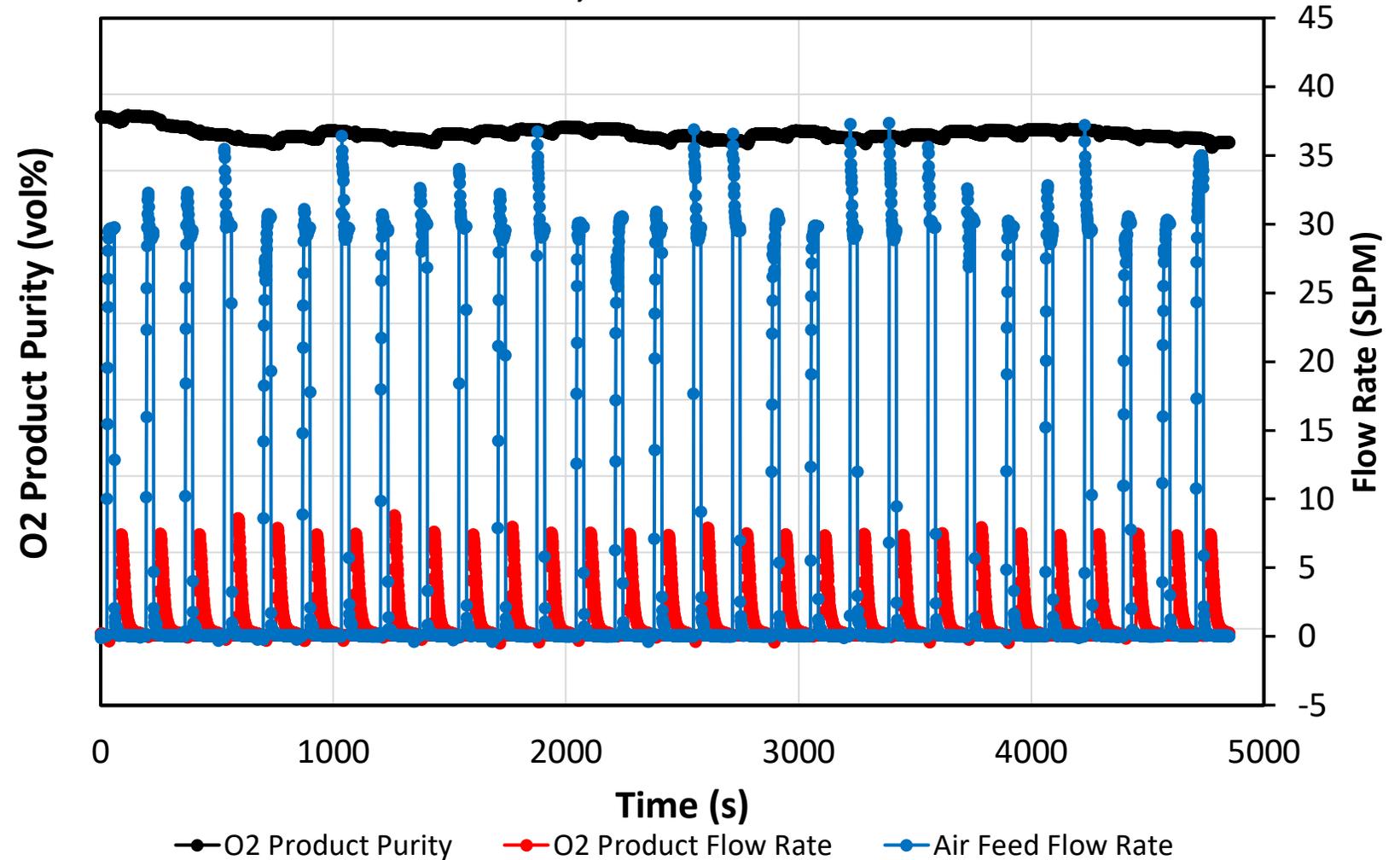


Example Parameter Set Test

5bar, V-310 Sorbent

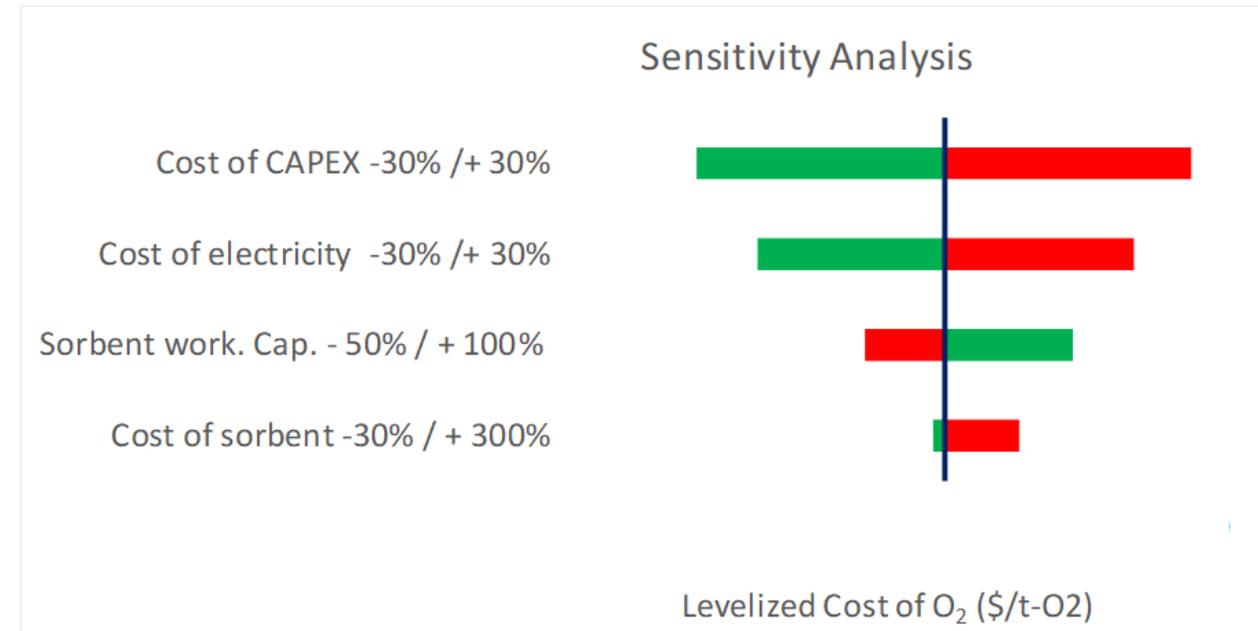
Valve Sequence

- 1-Pressurization
- 2-Adsorption
- 3-Blowdown
- 4-Product Reflux
- 5-Evacuation



TEA Refinement

- Data from the 10 kg/d test bed will provide key data for sorption/desorption kinetics at relevant conditions
 - O₂-binding sorbent data will be used for cycle modeling and optimization by GTRC
 - N₂-binding, if tested, will be modeled by Air Liquide
- Air Liquide will provide input module costs
- System design will be updated from DE-FE0027995 (10 TPD design) to incorporate
 - Refined sizing and utilities
 - Update utilities and equipment cost
 - Update modular construction costs
 - Determine overall O₂ production cost



Results

- Converted RTIO₂Sorb synthesis from glove box to scalable protocol
- Developed structured sorbent modules with N₂ sorbents
- Developed O₂ sorbent VPSA cycle model
- Design and fabricated of 10 kg/d testing system

Next step

- Integrated 10 kg/d system testing
- Refining process modeling for large scale design and cost

Future

- Focus on improving performance qualities of extrudate
- Sorbent powder properties improvement for structure formation
- Catalyst manufacturing development
- Large pilot-scale testing or 1 TPD prototype

Enable small-scale applications of oxygen such as 10-30MW gasifiers or 1 to 10 TPD systems by providing air separation at small-scale matching air separation cost of larger cryogenic separation systems.



Contact Information:
Dr. John Carpenter
919.541.6784
jcarpenter@rti.org

RTI International

Dr. John Carpenter
Dr. Jianping Shen
Dr. Qinghe (Angela) Zheng
Dr. Jak Tanthana
Dr. Paul Mobley
Dr. Jian Zheng
Dr. Vijay Gupta
Dr. Mustapha Soukri
Jonathan Peters

DOE\NETL

Diane Madden

Air Liquide

Raja Swaidan
Philippe Coignet

GTRC

Dr. Matther Realff
Dr. Hector Octavio Rubiera Landa

Acknowledgment: This material is based upon work supported by the Department of Energy Award Number DE-FE0031527.

Disclaimer: This report was prepared as an account of work sponsored by an agency of the United States Government. Neither the United States Government nor any agency thereof, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof.