



# Pilot Testing of a Modular System for Oxygen Production

DOE Cooperative Agreement DE-FE-0031527  
2021 DOE/FE Spring R&D Project Review Meeting  
May 4, 2021



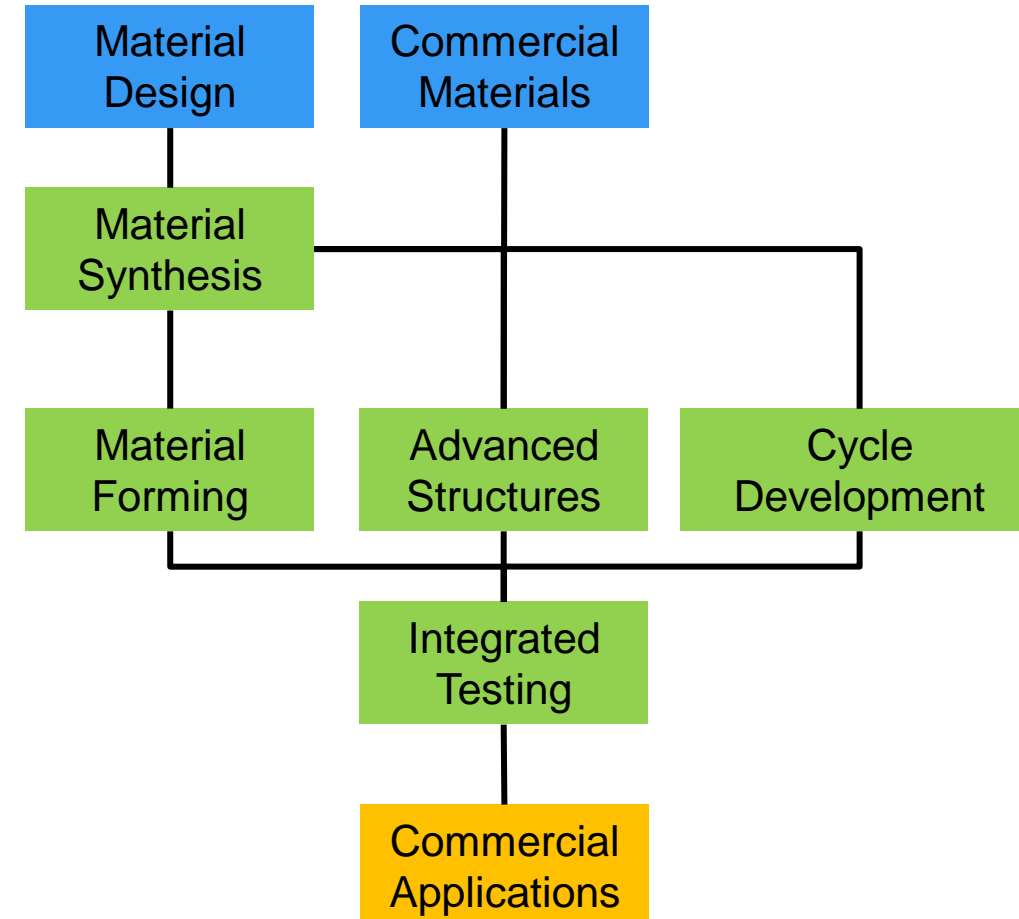
# Project objectives

**Objectives:** The design, fabrication, and testing of a 10 to 20 kg/day modular oxygen (O<sub>2</sub>) production system

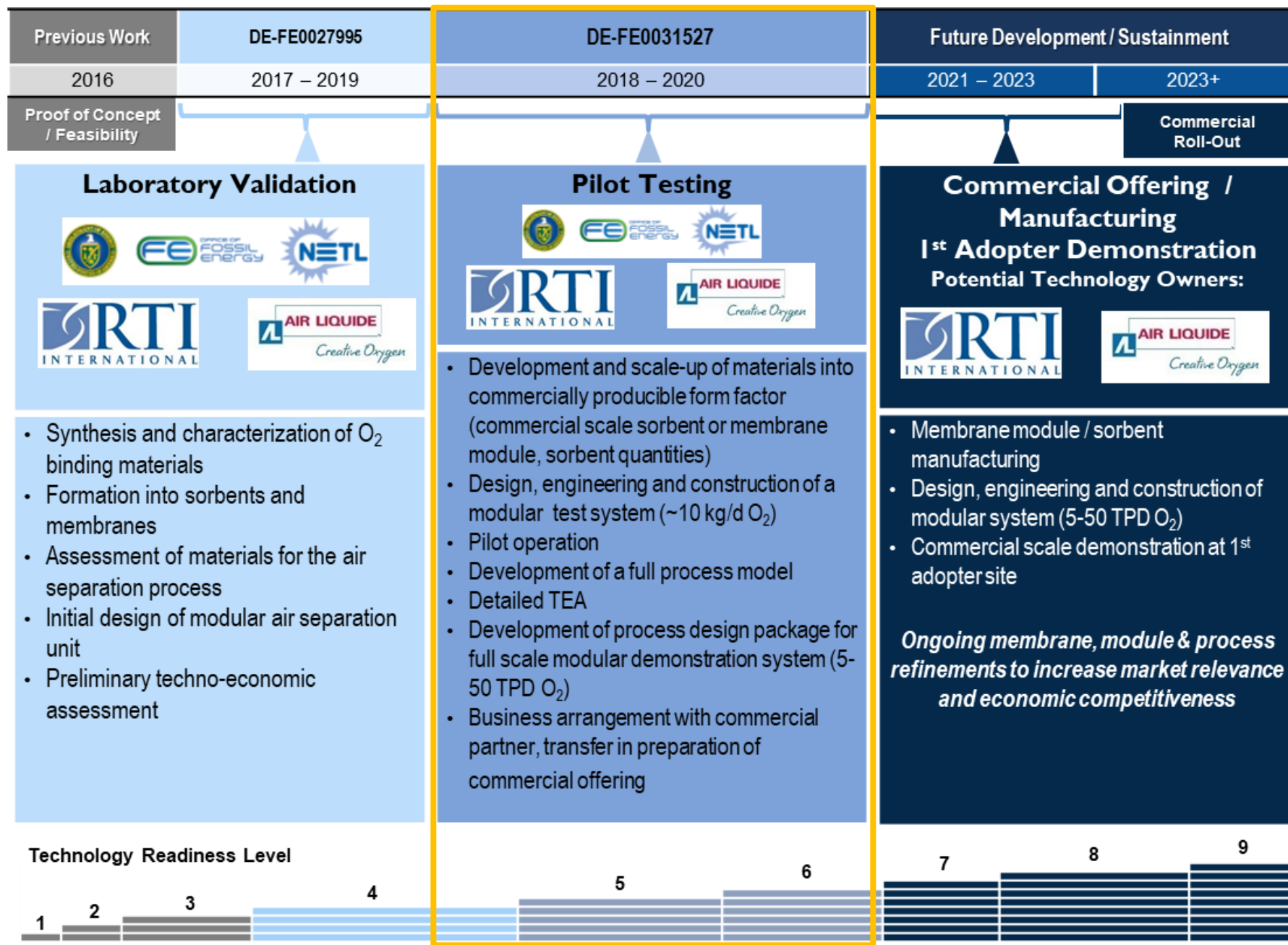
- Be cost competitive with current state-of-art process
- Modular process for small scale oxygen production
- Target lowering sorbent bed-factor

## **Specific Challenges**

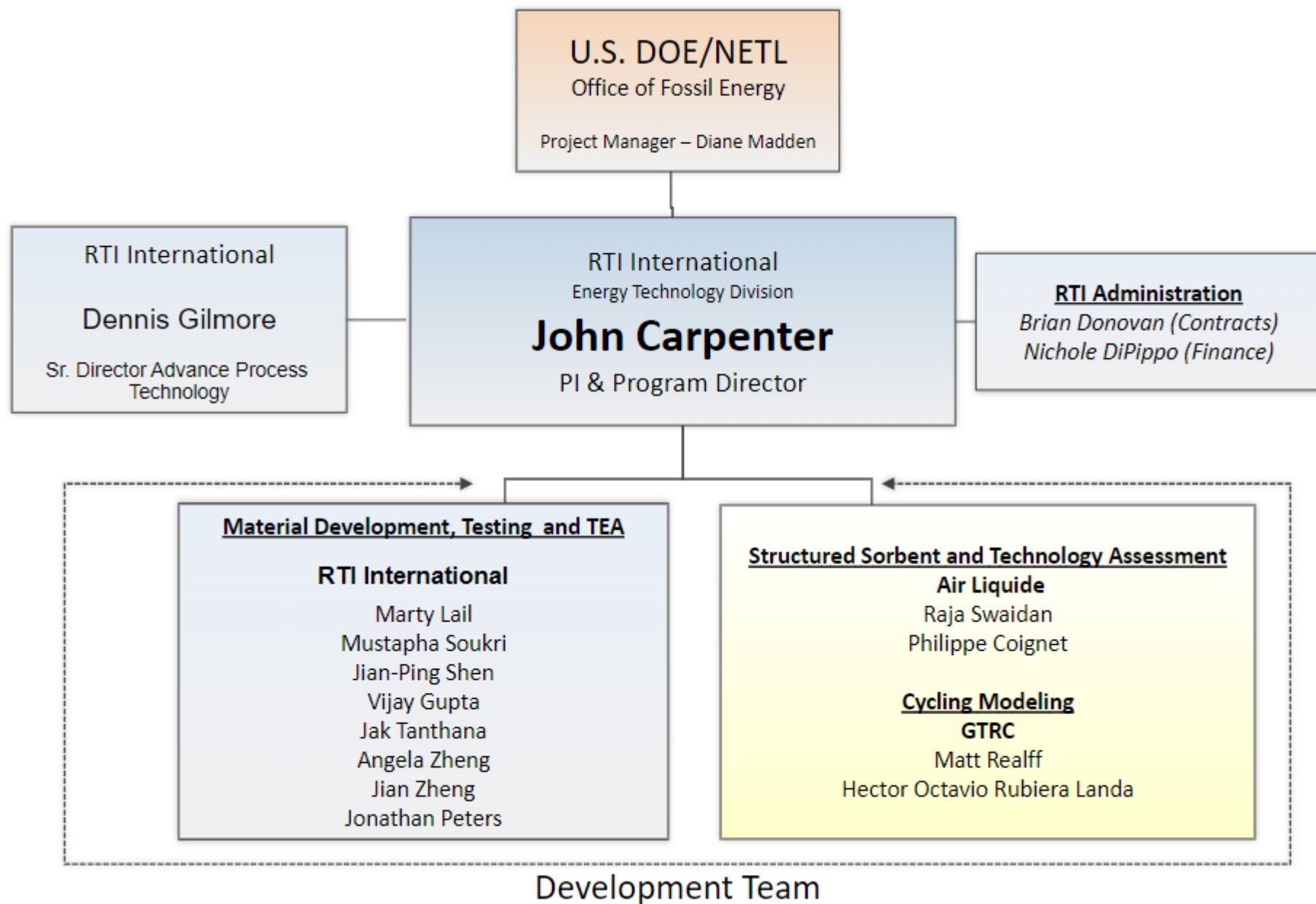
- Rapid PSA cycle development
- Structured sorbent module development
- Rapid cycle modeling tool development and cycle optimization
- Material and module scale up and manufacturing
- Design and fabrication of pilot O<sub>2</sub> production system
- Parametric and long-term testing
- Techno-economic analysis



# Development Roadmap

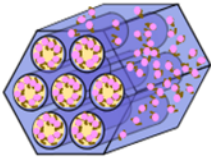
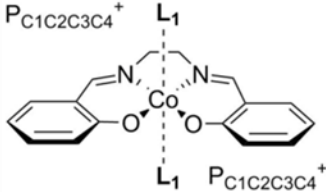
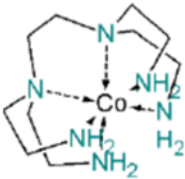
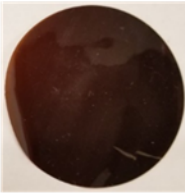
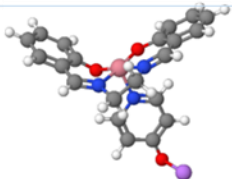


# Project team

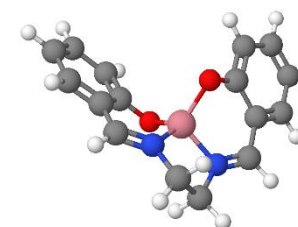
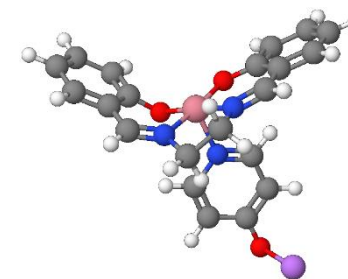
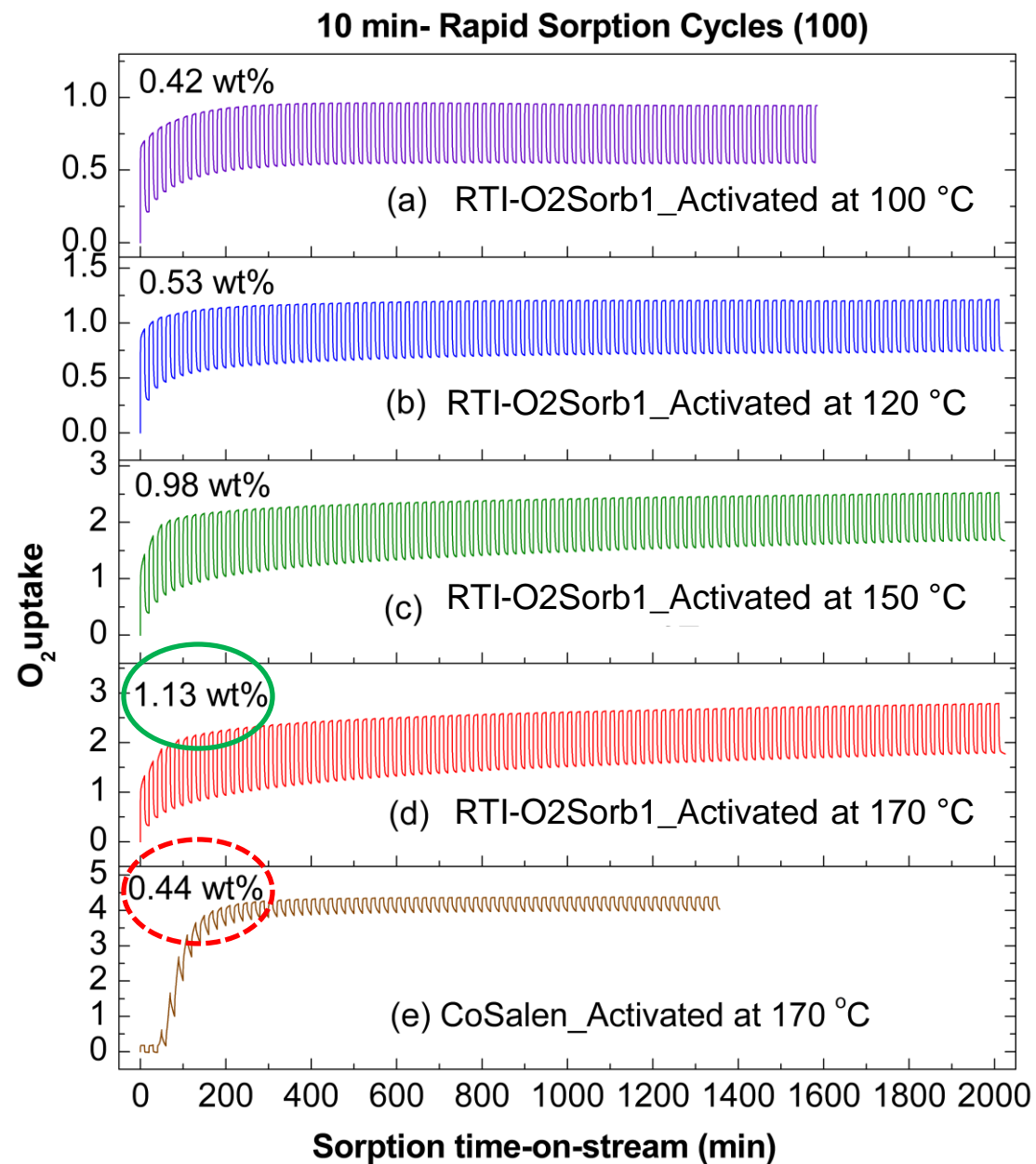


# Materials Scale-up

# Bio-Inspired O<sub>2</sub> Sorbent Material Development Summary

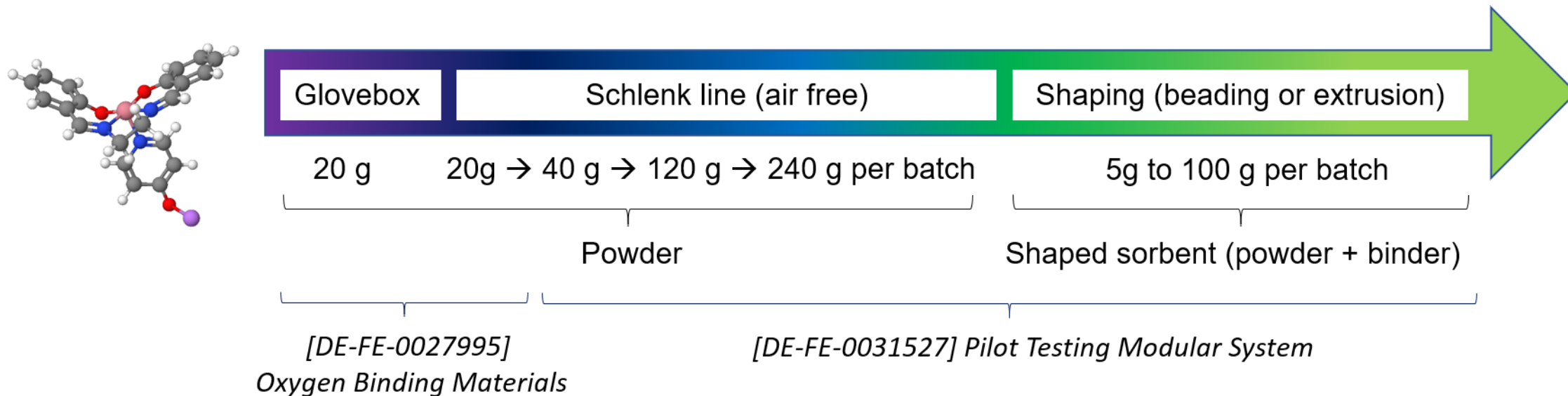
Material type	Structure/ Illustration	Material form	Material performance
Co-organometallic complex/silica		Solid	<ul style="list-style-type: none"> <li>Moderate O<sub>2</sub> sorption capacity (as high as 1.2 wt%)</li> <li>Slow O<sub>2</sub> sorption/ desorption kinetics</li> <li>Low O<sub>2</sub>/ N<sub>2</sub> selectivity</li> </ul>
Co Complex – Ionic Liquid		Ionic liquid	<ul style="list-style-type: none"> <li>Moderate O<sub>2</sub> sorption capacity (as high as 1.1 wt%)</li> <li>Slow O<sub>2</sub> sorption/ desorption kinetics</li> <li>High O<sub>2</sub>/ N<sub>2</sub> selectivity</li> </ul>
Co Complex/ porous support	<ul style="list-style-type: none"> <li>Complex on Mesoporous silica or zeolites</li> <li>O<sub>2</sub> binding metal organic frameworks</li> </ul>	Solid	<ul style="list-style-type: none"> <li>Low-moderate O<sub>2</sub> sorption capacity</li> <li>Slow O<sub>2</sub> sorption/desorption kinetics</li> <li>Low O<sub>2</sub>/ N<sub>2</sub> selectivity</li> </ul>
Co-PEI		Solid/ Solution	<ul style="list-style-type: none"> <li>High O<sub>2</sub> capacity, solid vs. liquid (3-6 wt% vs. 0.2 wt% in solution)</li> <li>Low O<sub>2</sub>/ N<sub>2</sub> selectivity</li> </ul>
Co Complex- O <sub>2</sub> membrane	 10 wt% Co Complex in Matrimid film	Solid membrane	<ul style="list-style-type: none"> <li>Low O<sub>2</sub>/ N<sub>2</sub> selectivity</li> </ul>
★ RTI-O2Sorb		Solid	<ul style="list-style-type: none"> <li>✓ High O<sub>2</sub> sorption capacity (as high as 3.0 wt%)</li> <li>✓ Fast O<sub>2</sub> sorption kinetics (rapid cycle &lt;10 min)</li> <li>✓ High O<sub>2</sub>/ N<sub>2</sub> selectivity</li> </ul>

# TGA Cyclic O<sub>2</sub> Sorption of RTI's RTI-O2Sorb1 vs. Commercial Co-Salen





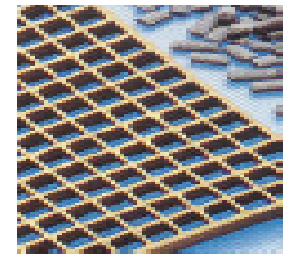
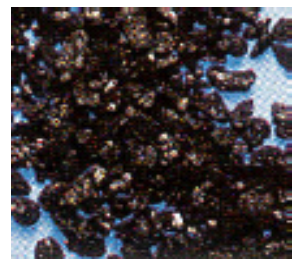
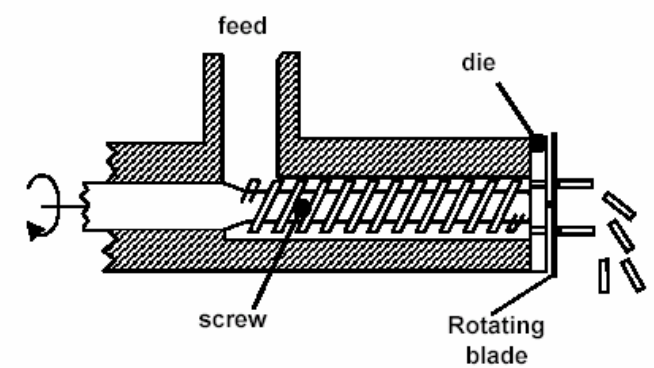
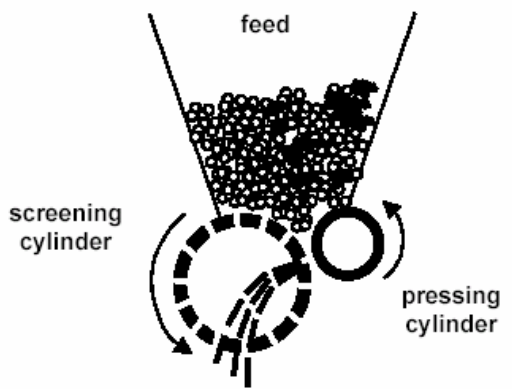
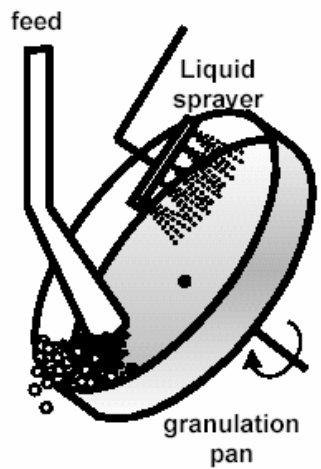
# Progress on Scale-up of RTI-O2Sorb



- ✓ **Successfully repeated batch synthesis for maximum O<sub>2</sub> sorption performance**  
(reversible O<sub>2</sub> uptake of 1~1.5 wt% with powder sample after activation at 170 °C)
- ✓ **Successfully synthesized powder material with same performance using Schlenk line**  
(which allows large batch synthesis)
- ✓ **Successfully scaled up powder material synthesis with same sorption performance**  
(20g → 40 g → 120 g → 240 g per batch)



# Agglomeration of Powder into Structured Form

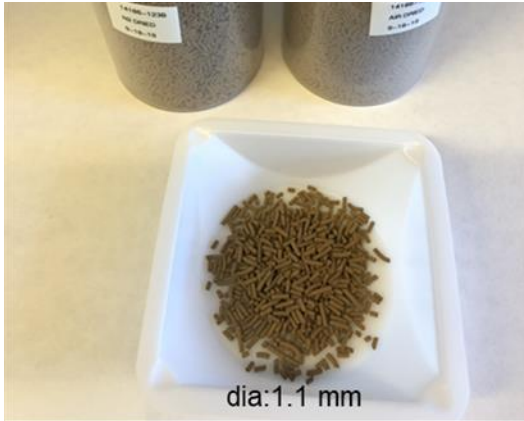
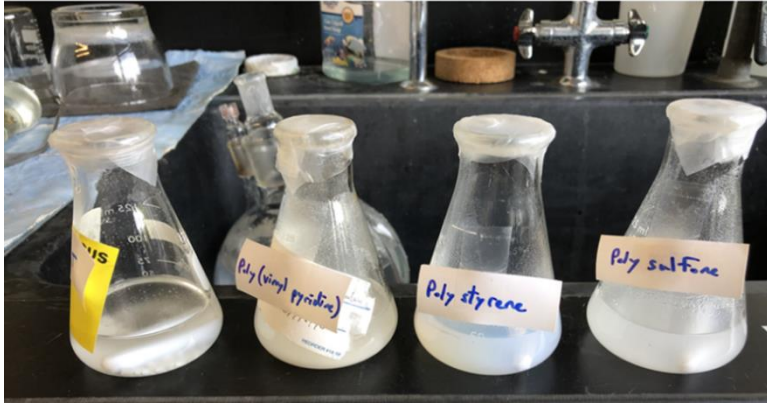


Granulation

Pelletization

**Extrusion**

# Optimization of Extrudate Formulation



After exposed in 100% O<sub>2</sub>  
@ 100°C 0.5hr,  
and continued for 100 N<sub>2</sub>-O<sub>2</sub> cycles

After normal N<sub>2</sub>-O<sub>2</sub> 100 cycles

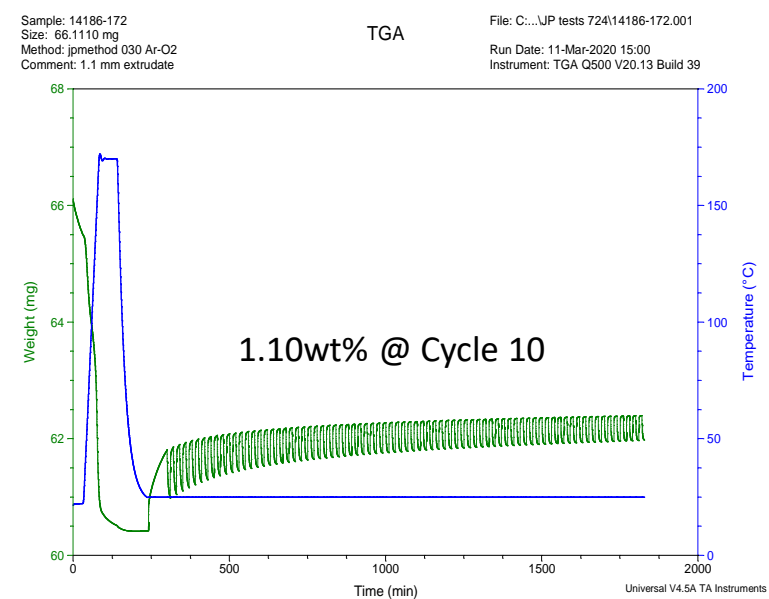
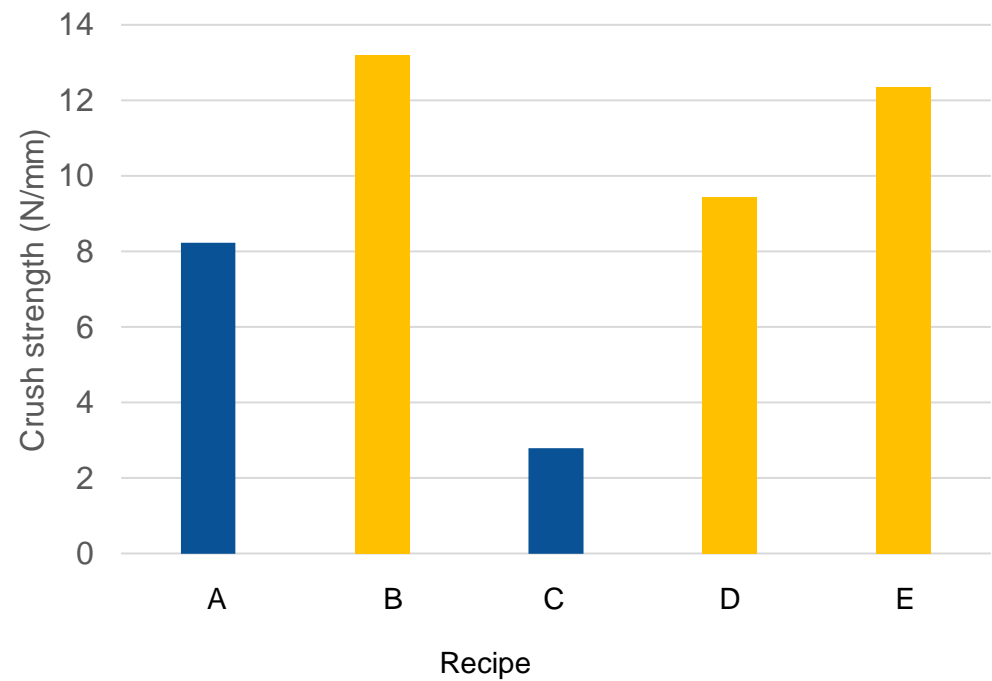
# Extrudate Formation Characteristics

## Key characteristics of Forming Extrudate:

- O<sub>2</sub> capacity, mechanical strength, size

## Key variables of Forming Extrudate:

- binder ratios and solvent
- extrusion pressure and temperature, drying temperature



Dia (in)	Dia (mm)	N	N/mm
0.054	1.3716	13.6	9.915427
0.053	1.3462	21.4	15.8966
0.055	1.397	12.9	9.234073
0.052	1.3208	15.4	11.6596
0.052	1.3208	15.4	11.6596
0.054	1.3716	17.6	12.83173
0.052	1.3208	11.9	9.009691
0.053	1.3462	16.8	12.47957
0.052	1.3208	12.1	9.161114
0.055	1.397	11.8	8.446671
		Avg	11.02941

Binder (wt%)	Density (g/cc)	Dia. (mm)	Length (mm)	Crush strength (N/mm)	Dynamic oxygen capacity (wt%)
16.7	0.55-0.62	1.2-1.5	2.0-10.0	8.0-12.0	0.8-1.2

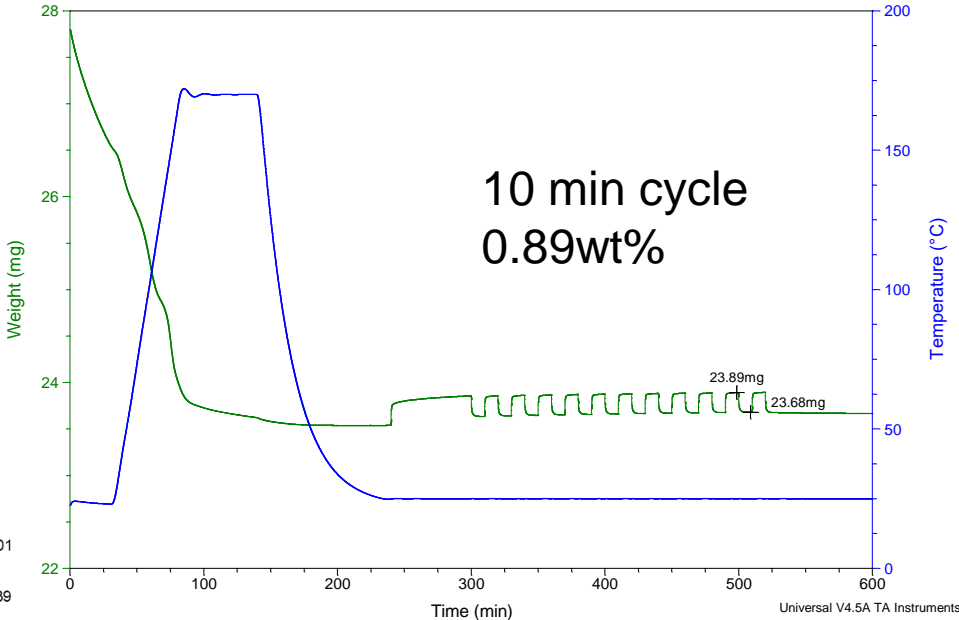
# TGA Profile of Extrusion Shaped RTI-O2Sorb (crushed to 300~425 μm)



Sample: 14186-123B  
Size: 27.7990 mg  
Method: jpmethod 030 Ar-O2  
Comment: extrudate and crushed sieved 14186-123B N2 dried

TGA

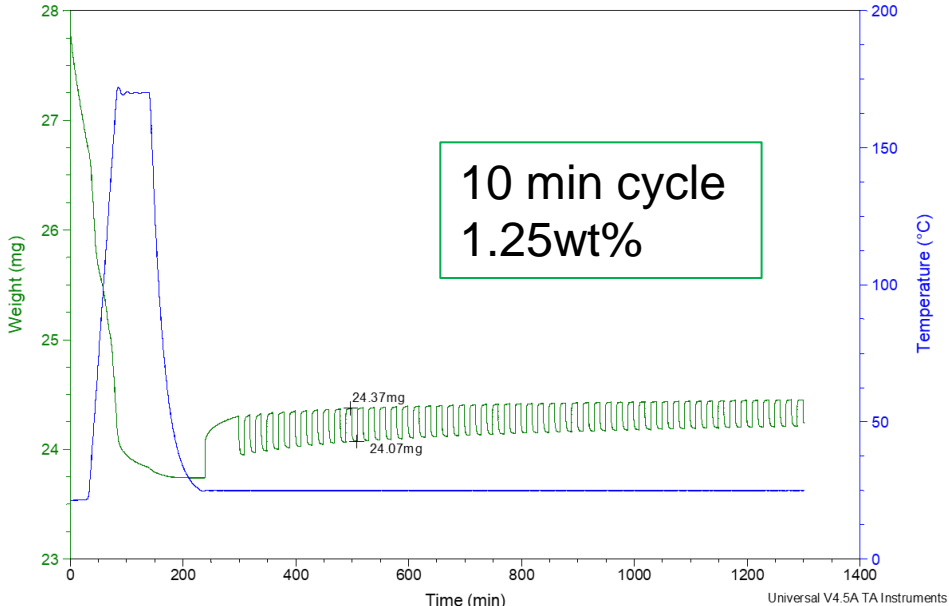
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Instrument: TGA Q500 V20.13 Build 39



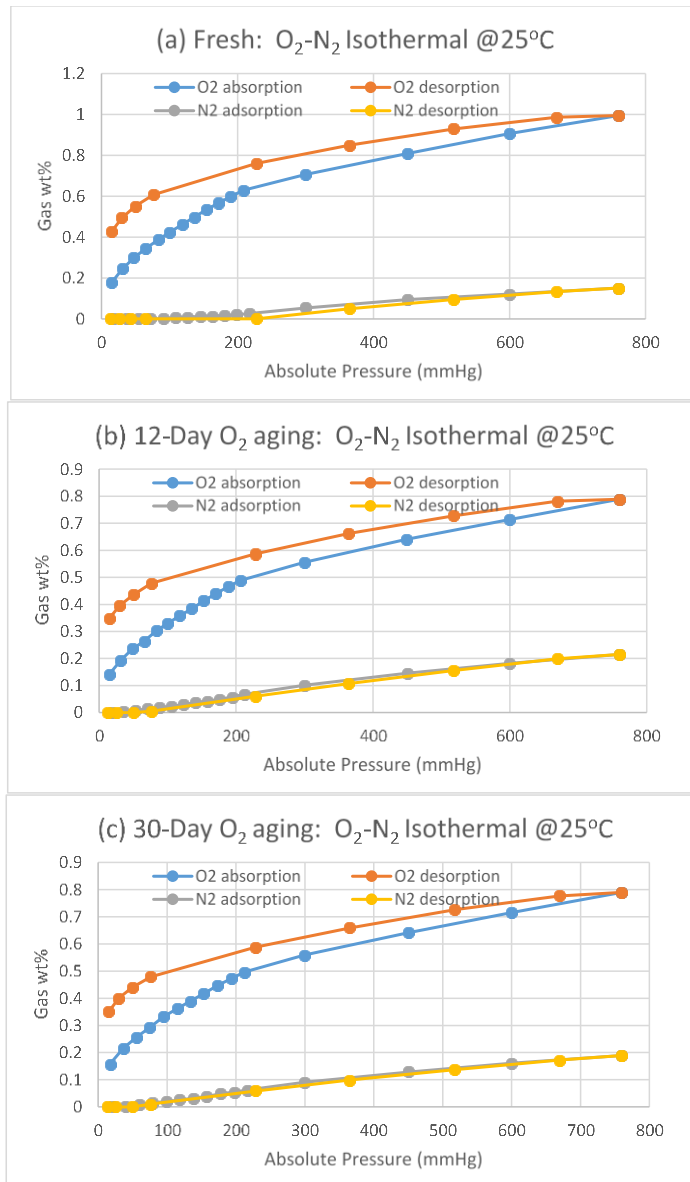
Sample: 14186-124A  
Size: 27.8430 mg  
Method: jpmethod 030 Ar-O2 long  
Comment: extrudate crushed sieved N2 comp dried

TGA

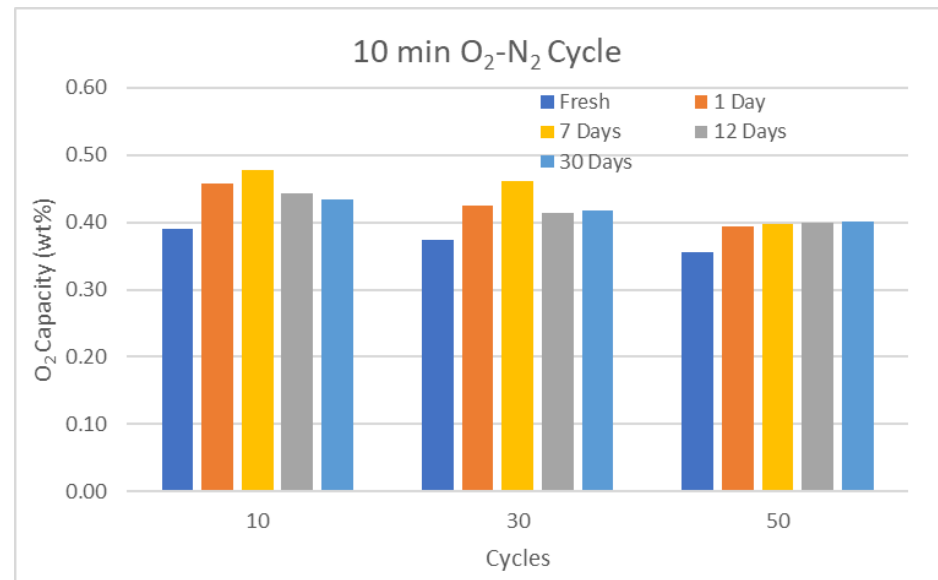
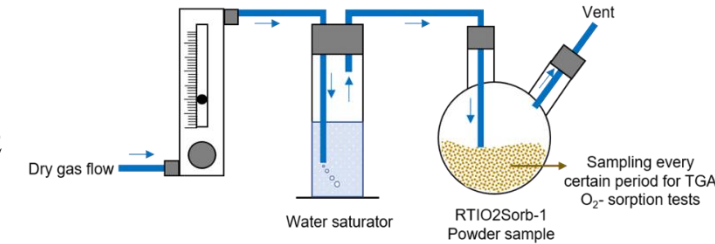
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Instrument: TGA Q500 V20.13 Build 39



# Exposure/Aging Testing



- 2.62 vol% H<sub>2</sub>O (g), balance N<sub>2</sub>
  - 45d exposed, similar to long term cycling
- 1.5% O<sub>2</sub>, 19.5 CO<sub>2</sub>, balance N<sub>2</sub>
  - Exposed 36d – no degradation
- 2.62 vol% H<sub>2</sub>O (g), 20.40% O<sub>2</sub>, balance N<sub>2</sub>
  - Similar to long term cycling in TGA
- 99% vol% O<sub>2</sub>, , balance N<sub>2</sub>
  - Some degradation through day 12,
  - day 30 similar to day 12 ( See graphic to left)





## Forming of Structured Sorbents



### *Air Liquide Objectives:*

- Develop novel structured adsorbents production techniques using conventional sorbent materials
- Apply and adapt the techniques developed on conventional adsorbents to the novel oxygen-binding adsorbent materials
- Manufacture and ship 2 to 4 structured adsorbers for pilot testing based on novel oxygen-binding adsorbent
- Support activities (e.g. Pilot design, Techno-Economic Analysis)

## ***Focus on Traditional Materials***

- Air Liquide BP1 objectives successfully met on time (*by June 30<sup>th</sup>, 2019*)
- Formulations were developed and characterized for (1) air dehumidification and (2) for conventional nitrogen (N<sub>2</sub>)-binding adsorbent
- Activation protocols for each adsorbent formulation were developed
- Forming techniques to produce structured beds were developed

## ***Adapting Method to RTI Sorbent***

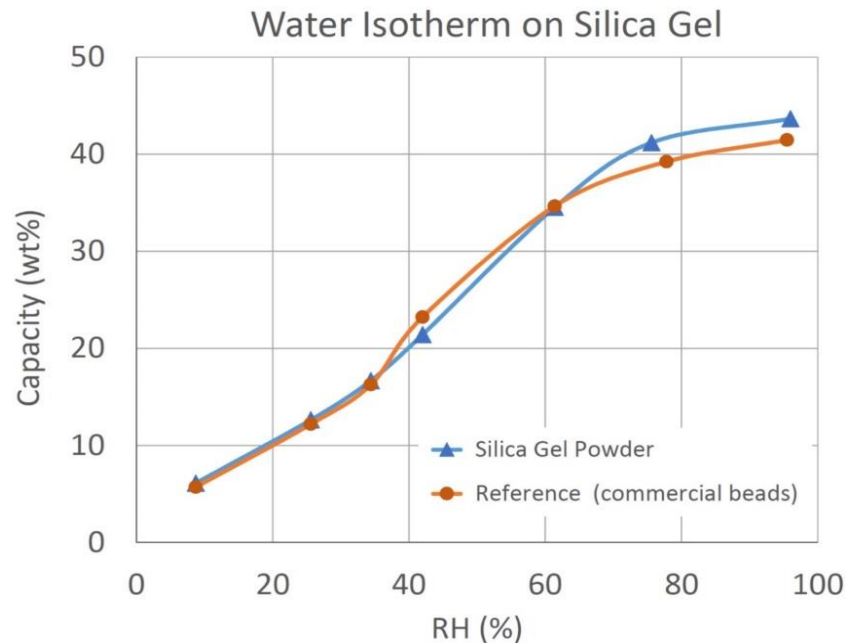
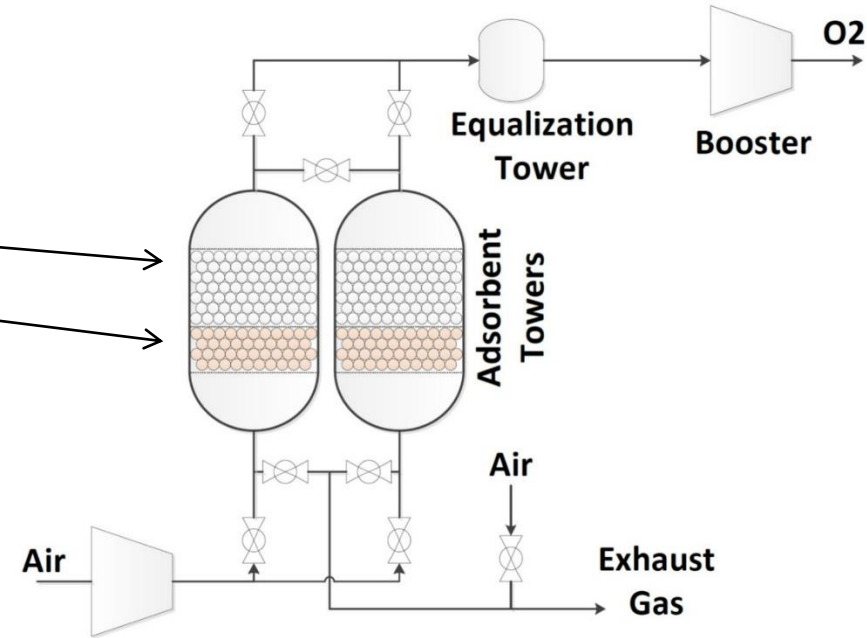
- Forming techniques and activation tool were scaled up for beds of up to 1 kilogram
- Reviewed and provided feedback on the pilot design
- Explored adapting formulation and forming techniques to novel oxygen-binding adsorbent. Multiple samples were received from RTI, characterized and used to support adaptation-work on formulation and forming



# Sorbent and Structured Sorbent Module Development and Characterization

## Overall Approach

- Conventional O<sub>2</sub> VSA → uses 2 adsorbents
- Top adsorbent used to capture N<sub>2</sub>
- Bottom adsorbent used for air drying
- Structured beds made of elementary shapes
- Elementary shapes produced by combining adsorbent powder and binder

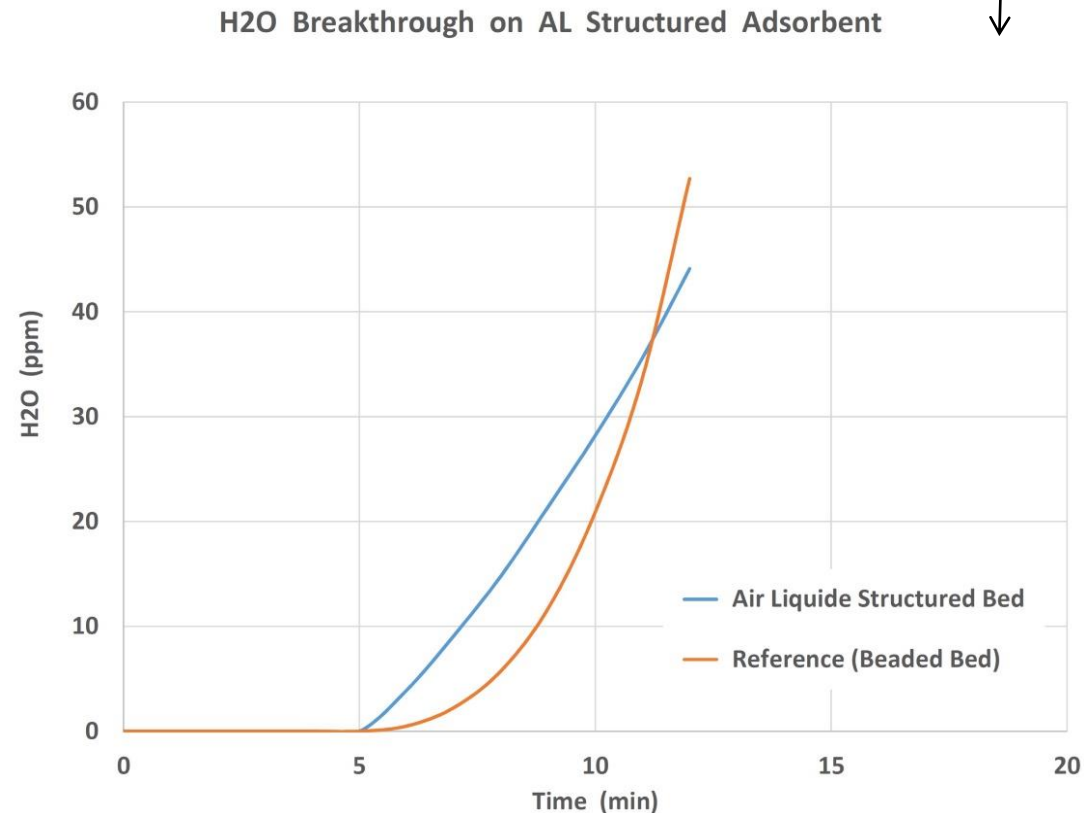


## Air Drying / Multi-Steps Approach

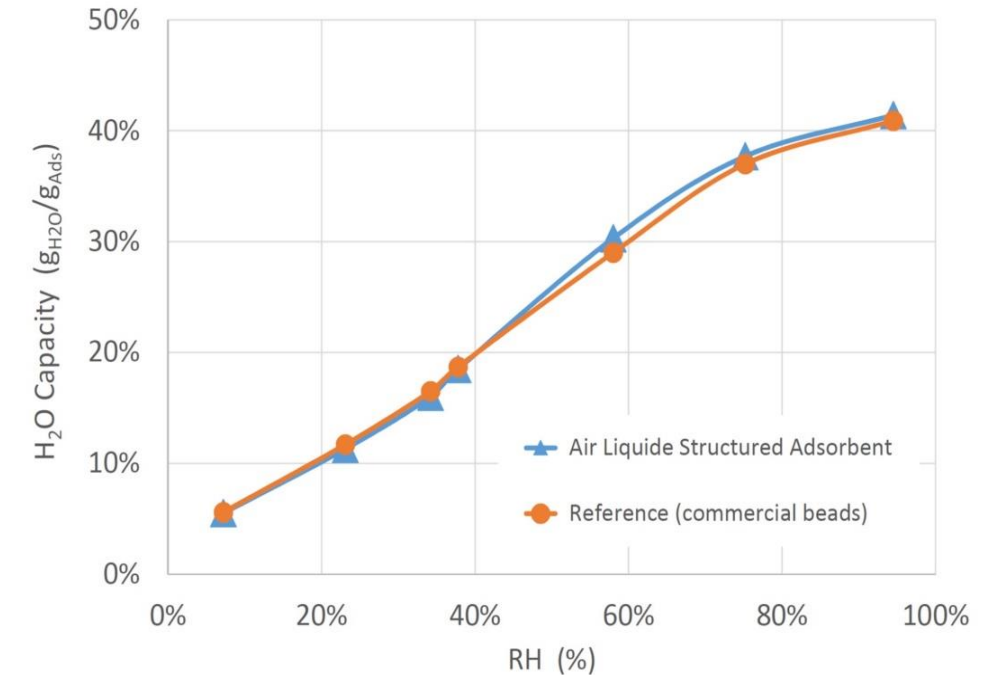
- 2 options: activated alumina (AA) or silica gel (SG)
- SG powder selected based on its highest water capacity
- SG powder formed with a binder into elementary shapes

## Air Drying / Multi-Steps Approach

- H<sub>2</sub>O capacity of SG elementary shapes meets expectations
- Small scale structured SG-bed formed and characterized
  - H<sub>2</sub>O breakthrough curve comparable to conventional beaded bed
  - Pressure drop comparable to conventional beaded bed

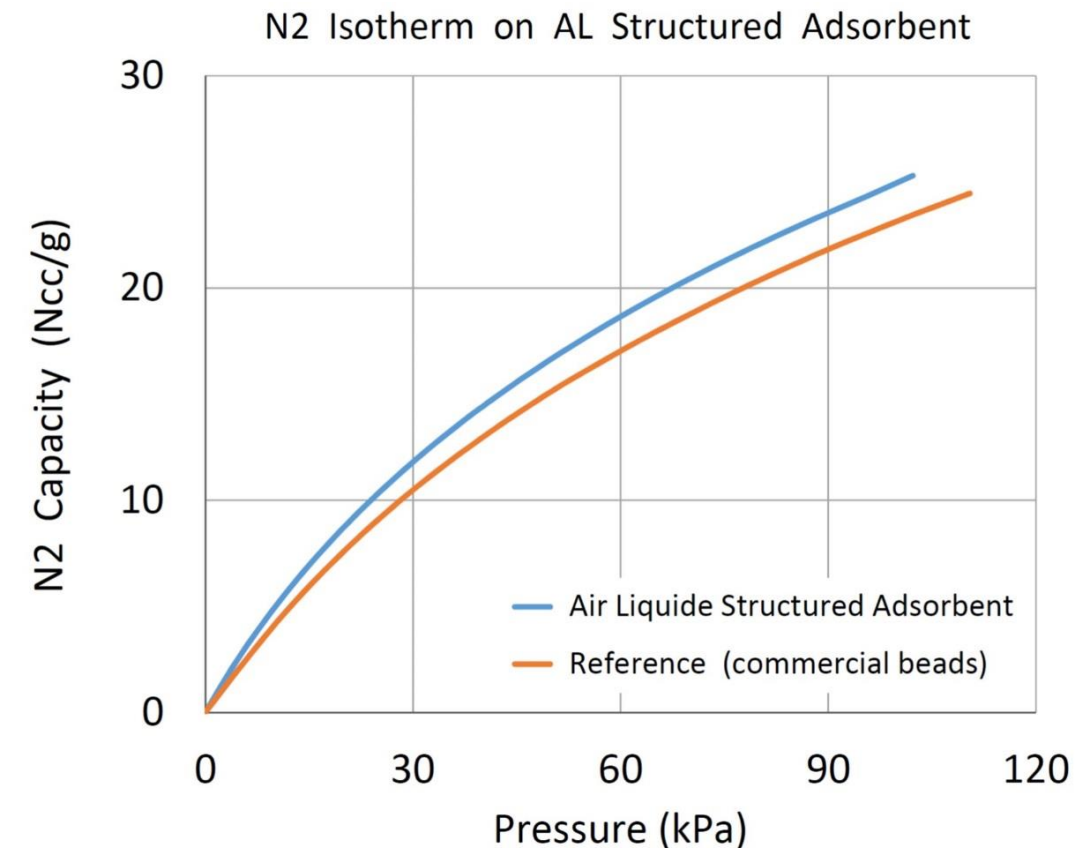


Water Isotherm At 22°C on Silica Gel



## *N<sub>2</sub> Adsorbent / Multi-Steps Approach*

- Various zeolites typically used as N<sub>2</sub> binding adsorbents
- Selection of zeolite powder
- Forming with binder
- High temperature activation
- Similar N<sub>2</sub> capacity & selectivity compared to commercial adsorbents
- Faster kinetics



## ***Adaptation Work on Novel O<sub>2</sub> Binding Adsorbent***

- Goal: form structured bed with novel adsorbent by adapting techniques developed with traditional sorbents
- Focused on producing an advantageous elementary shape while managing specific limitations of novel adsorbent
- An advantageous elementary shape is fast to produce and can yield low pressure drop once formed into a structured bed
- Performance of the formed adsorbent is checked by running N<sub>2</sub>/O<sub>2</sub> isotherms on elementary shapes
- Forming of the novel O<sub>2</sub> binding adsorbent was unable to achieve mechanical strength for full module forming
- Focused on extrudate formations



*Novel powder of O<sub>2</sub> binding adsorbent*

## Cycle Modeling



# Development of a vacuum pressure-swing adsorption (VPSA) full-order solver

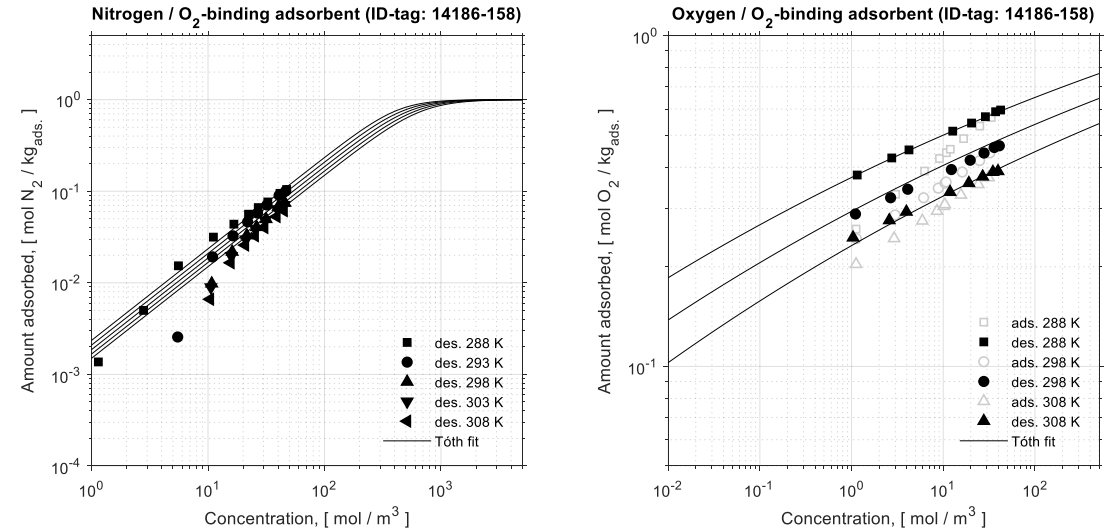
## Process modeling

- 1D PDE system describing transient fixed-bed adsorber equations for 7 state variables: gas-phase compositions, adsorbed-phase concentrations, pressure, bed & casing temperatures
- Competitive **adsorption equilibria** modeled w/ IAST
- Linear driving-force (LDF) approximation for mass transfer
- First-principles heat transfer modeling considered
- Solved numerically w/ Finite Volume Method (FVM)
- Coded in MATLAB

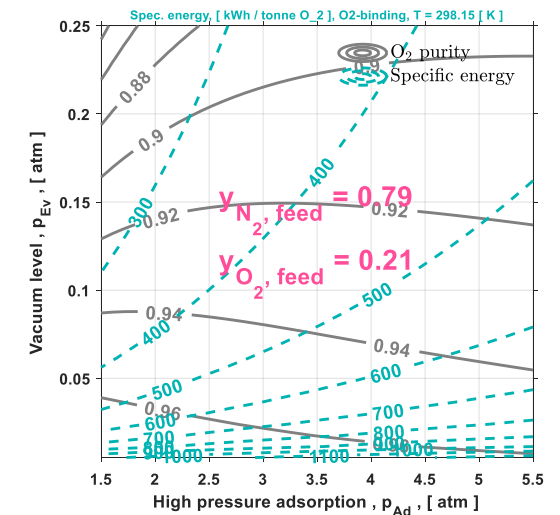
## Optimization

- Multi-objective optimization of relevant VPSA performance variables using genetic & surrogate-based algorithms

## Adsorption equilibria

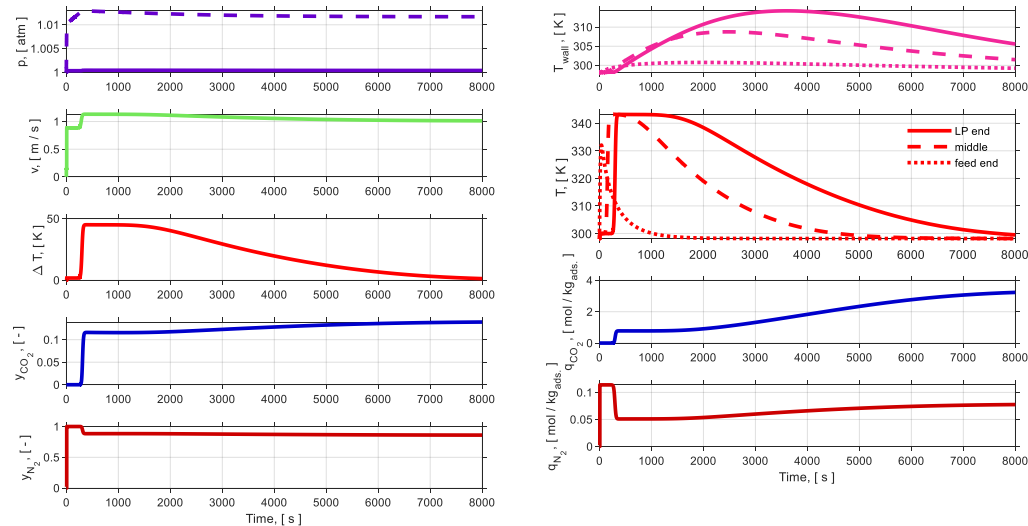


- Applied a short-cut method to test IAST implementation and obtain preliminary assessment for the oxygen-binding adsorbent

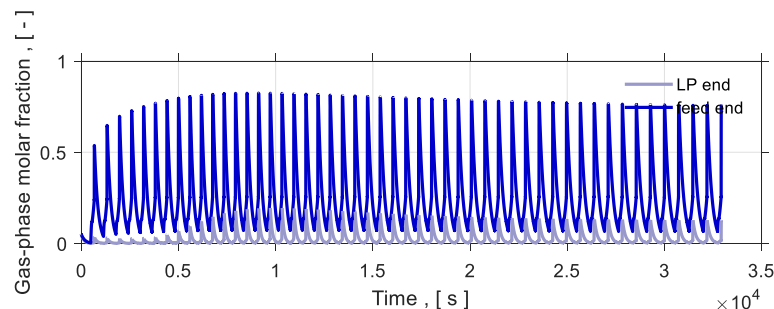


## Flue-gas separation results for model validation

- Dynamic column breakthrough (DCB)

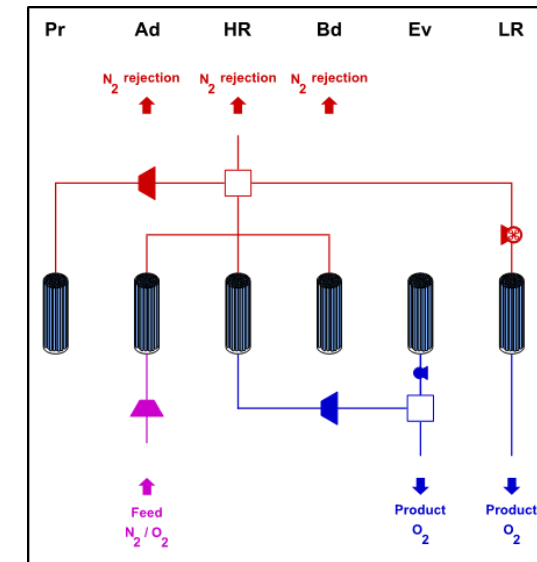


- 4-step VPSA w/ LPP for heavy-product recovery



## On-going sub-tasks

- Implementation of 6-step cycle to simulate the operation of the air separation skid under construction

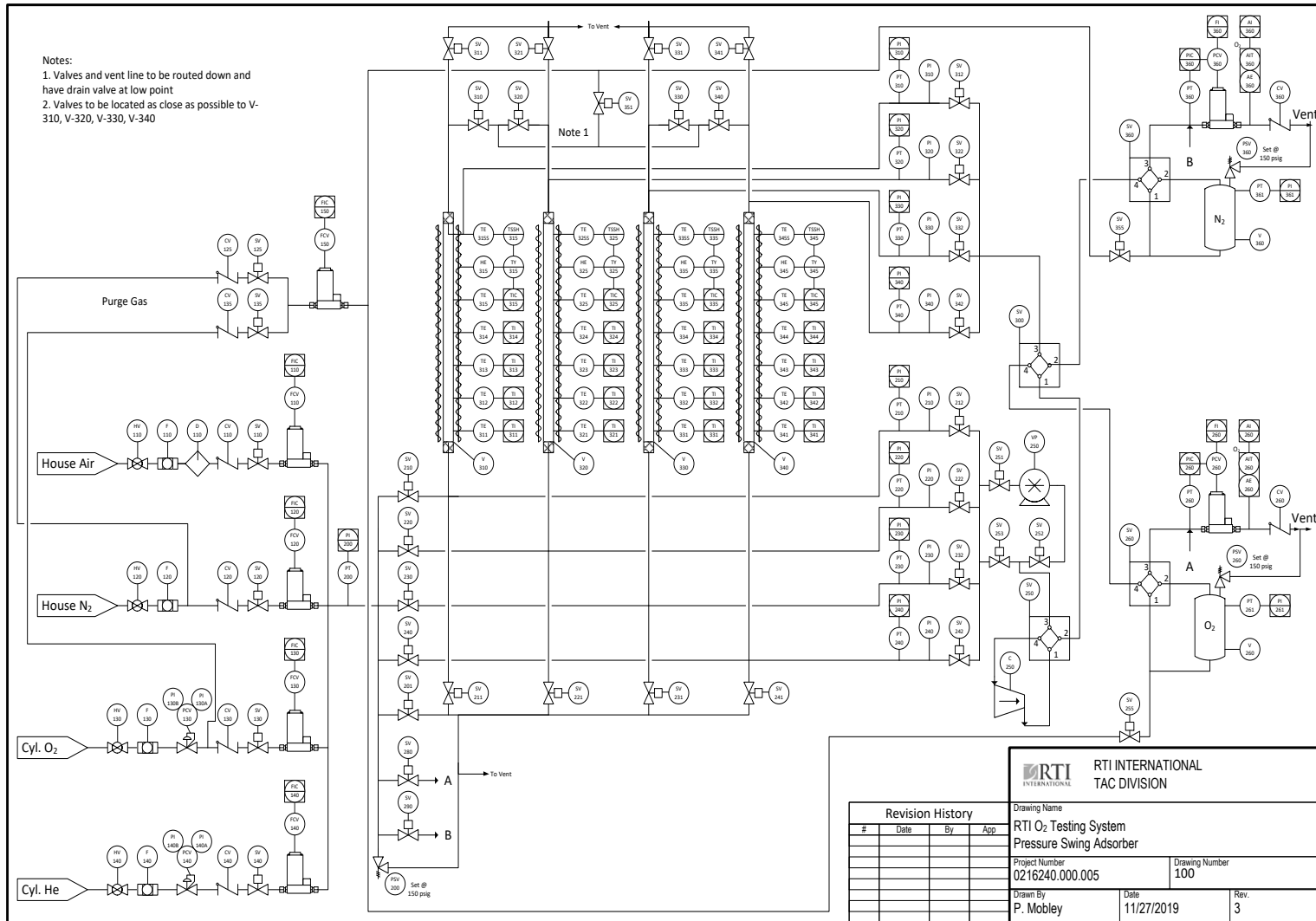


- Efficiency improvements of IAST calculations to speed-up optimization runs
- Implementation & execution of multi-objective optimization runs for 4-step and 6-step cycles to identify suitable operating conditions



## Integrated Test Skid

# 10 kg Pilot Modular System Process Flow Diagram



- O<sub>2</sub> production rate
- O<sub>2</sub> purity
- Cycle optimization
- Bed size factor
- Unit power consumption
- Material stability

- Techno-economic analysis for O<sub>2</sub> cost projection

## Steps

- HMB
- Sizing
- Safety Review Internal
- AL feedback
- Order Key Instruments
- Fabrication\Controls Commissioning
- Testing

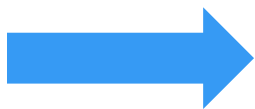
# Kg Extrudate Production

Produced 2.4 kg of O<sub>2</sub> Sorb in extrudate form

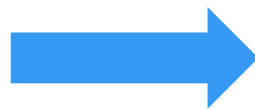
- Due to size limitations of equipment this was performed in 150-250 gm batches



Forming



Drying



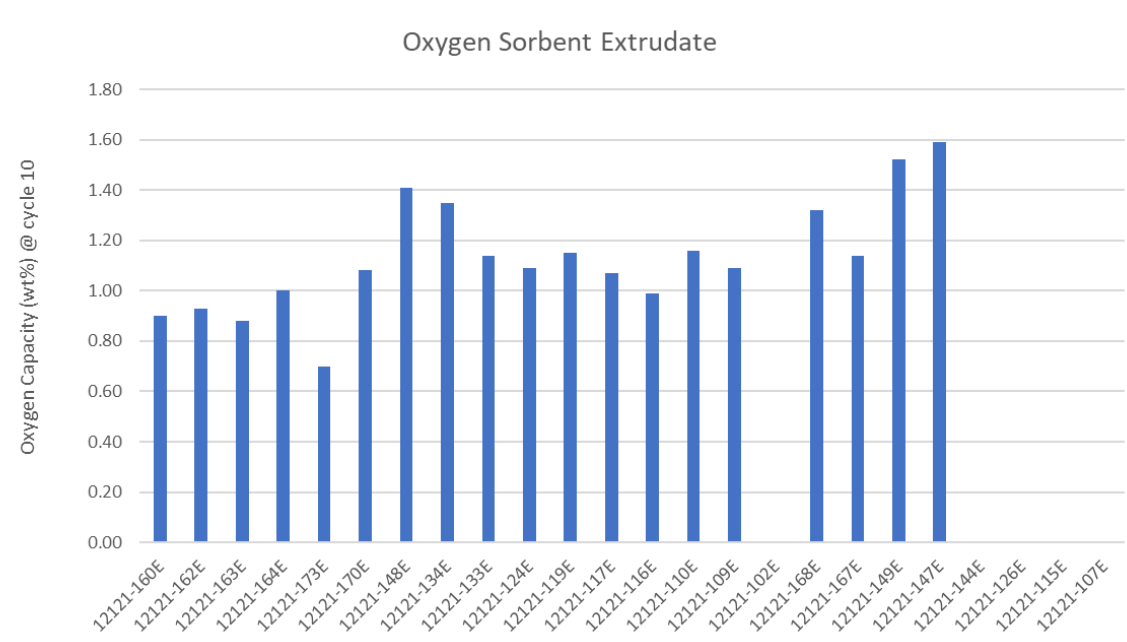
Sizing



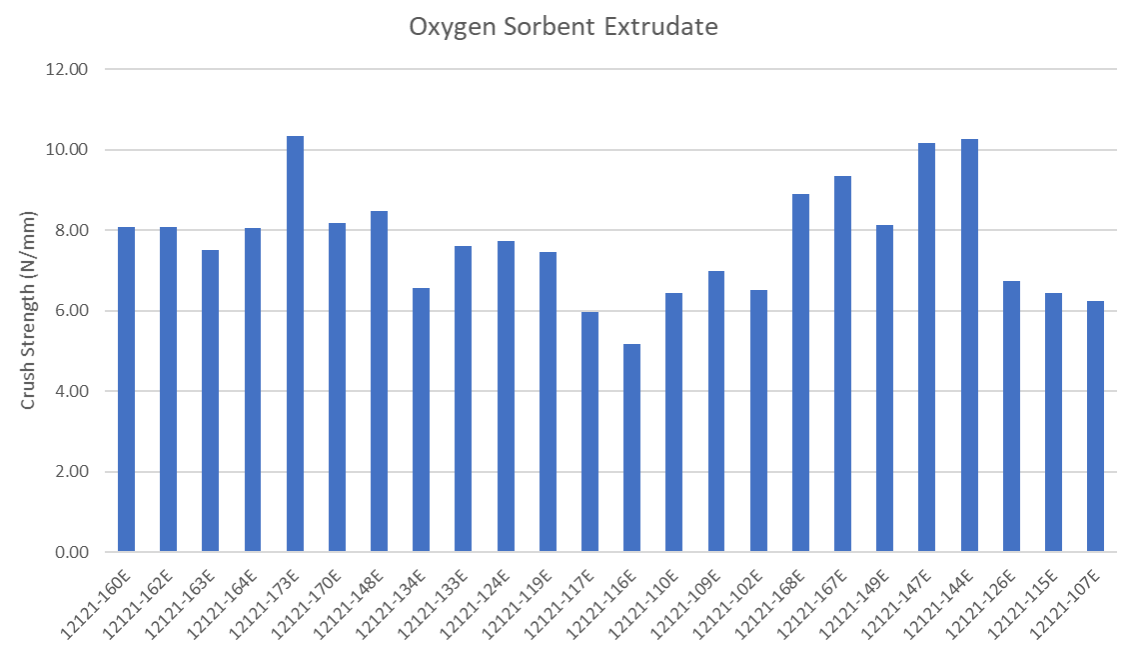
# Kg Extrudate Characterization

Key characterizations were O2 capacity under standard TGA test and crush strength

- Some variation from batch to batch



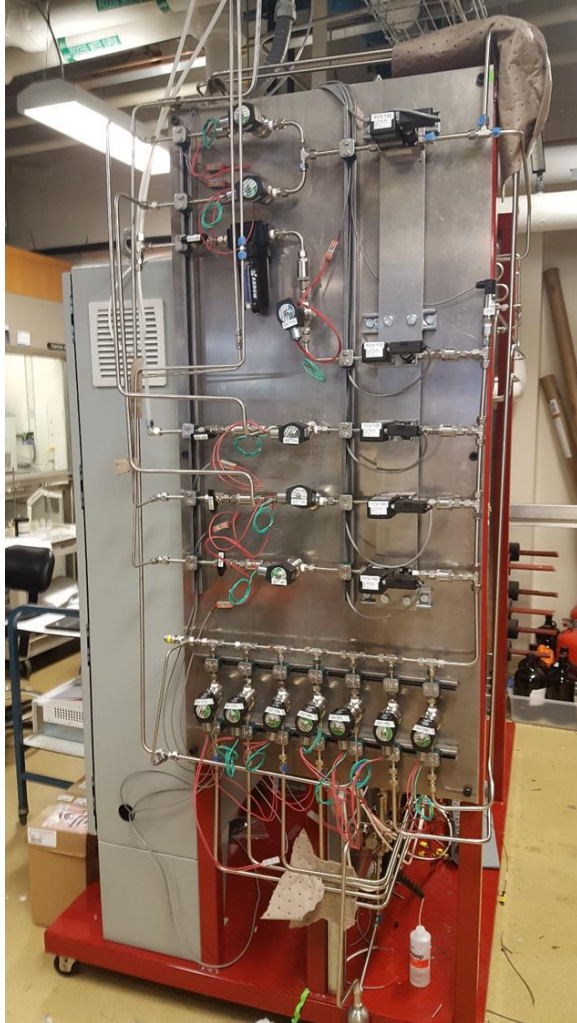
Target was > 1.0 wt% in TGA testing for goal of achieving > 0.5 wt% working capacity



Target was > 5 N/mm in axial crush strength similar to commercial materials of similar structure

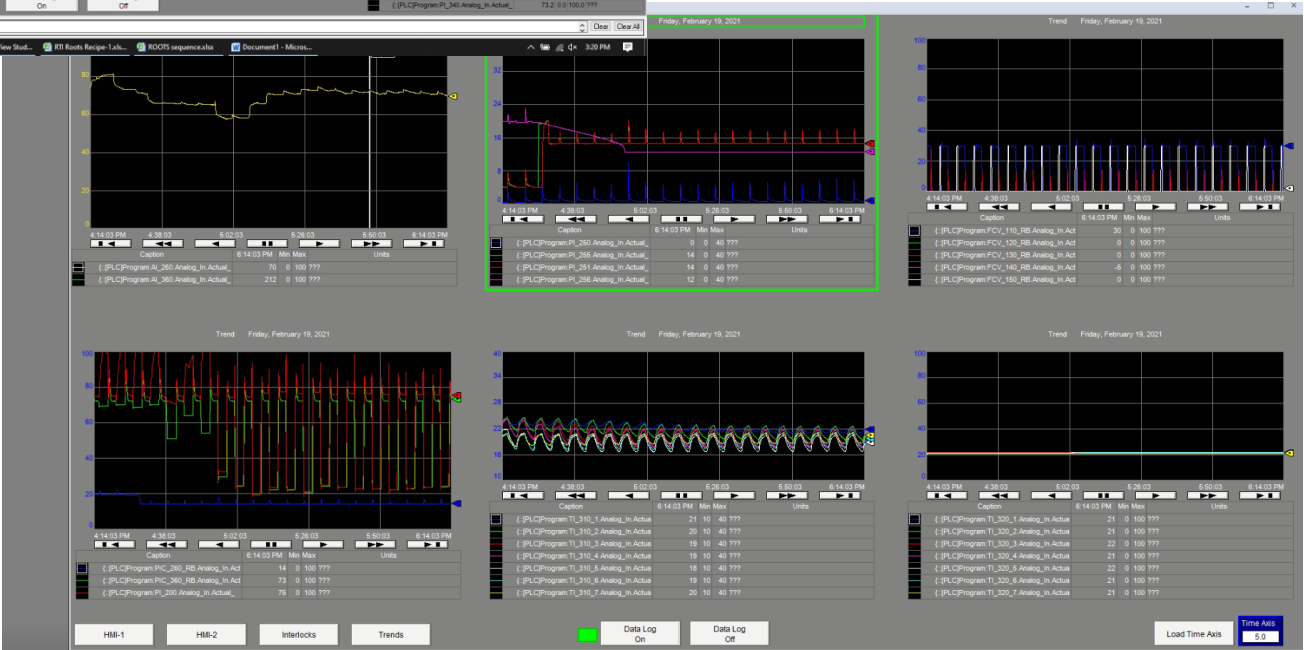
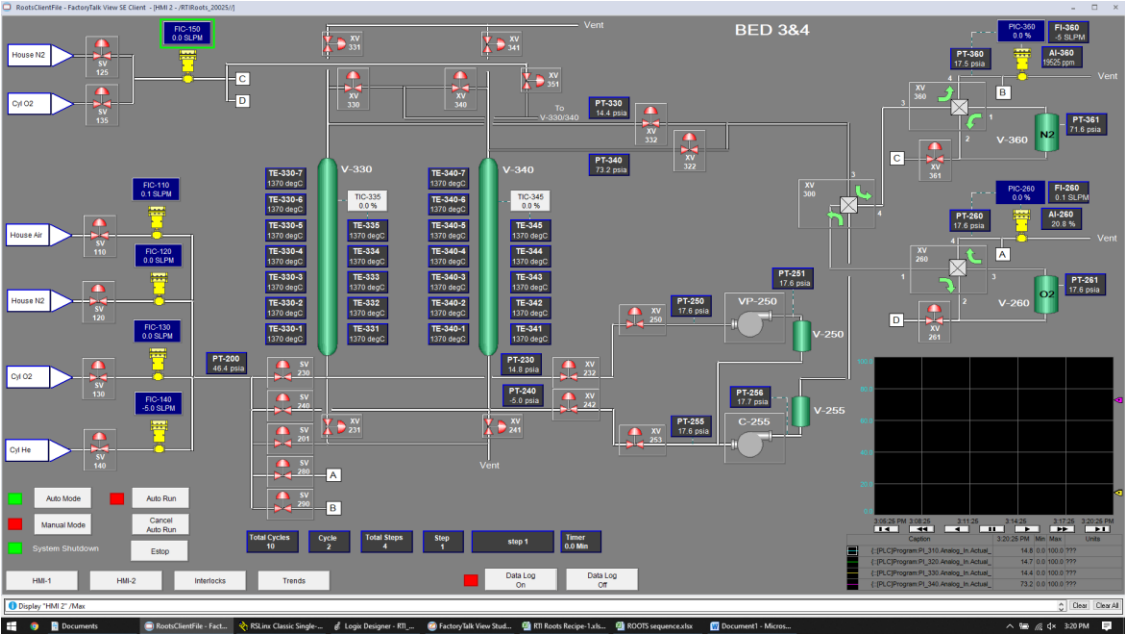


# 10 kg Pilot Modular System Build

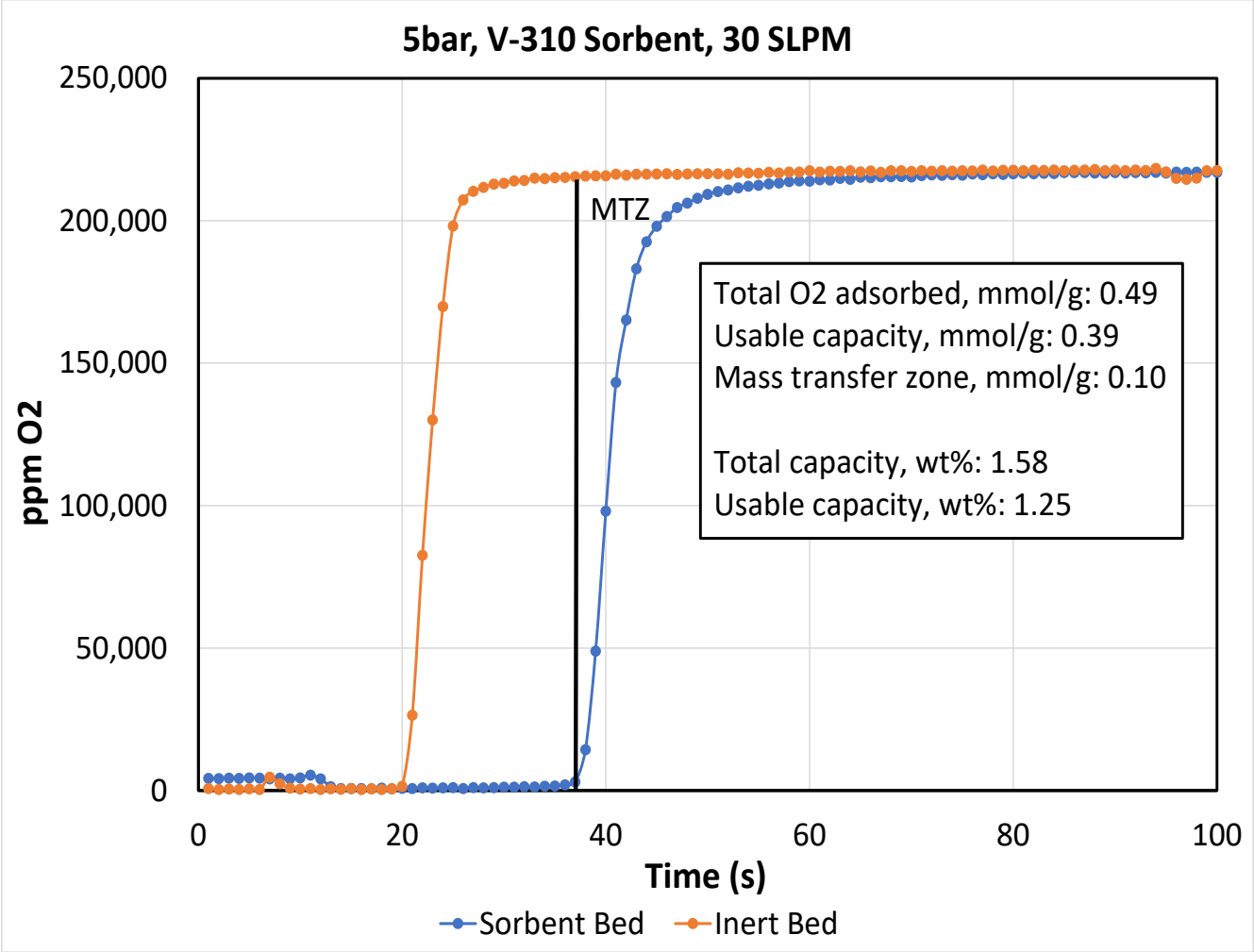




# 10 kg Pilot Modular System Controls



# System Characterization – Breakthrough Testing



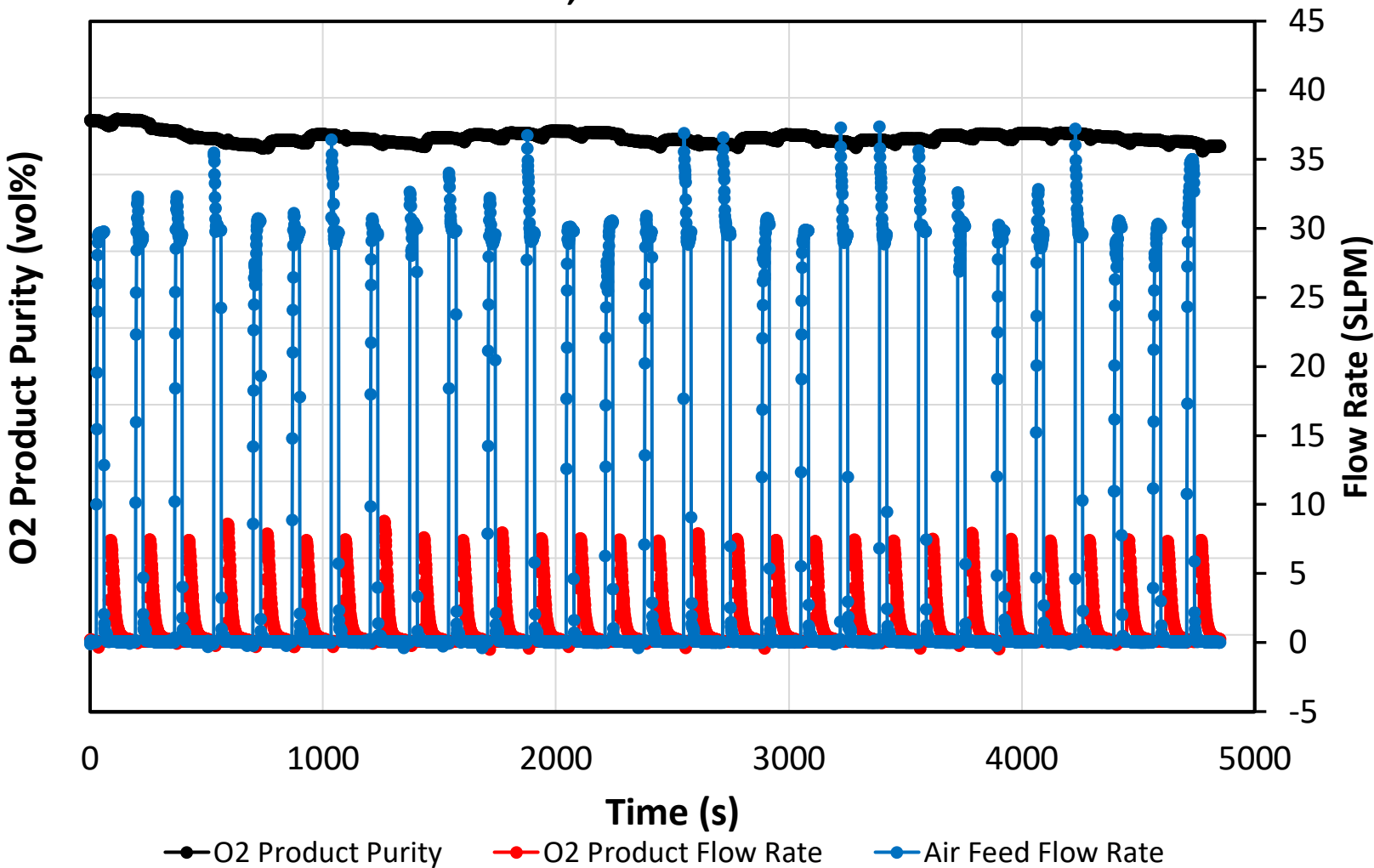


# Example Parameter Set Test

5bar, V-310 Sorbent

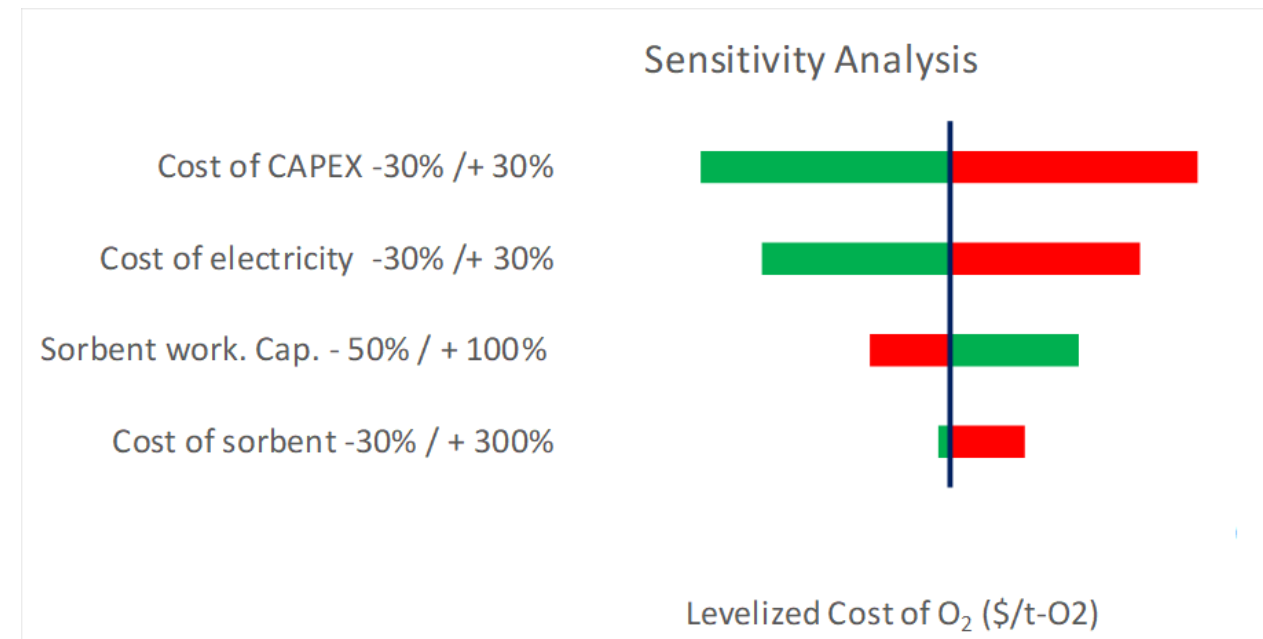
**Valve Sequence**

- 1-Pressurization
- 2-Adsorption
- 3-Blowdown
- 4-Product Reflux
- 5-Evacutination



# TEA Refinement

- Data from the 10 kg/d test bed will provide key data for sorption/desorption kinetics at relevant conditions
  - O<sub>2</sub>-binding sorbent data will be used for cycle modeling and optimization by GTRC
  - N<sub>2</sub>-binding, if tested, will be modeled by Air Liquide
- Air Liquide will provide input module costs
- System design will be updated from DE-FE0027995 (10 TPD design) to incorporate
  - Refined sizing and utilities
  - Update utilities and equipment cost
  - Update modular construction costs
  - Determine overall O<sub>2</sub> production cost



## Results

- Converted RTIO2Sorb synthesis from glove box to scalable protocol
- Developed structured sorbent modules with N2 sorbents
- Developed O2 sorbent VPSA cycle model
- Design and fabricated of 10 kg/d testing system

## Next step

- Integrated 10 kg/d system testing
- Refining process modeling for large scale design and cost

## Future

- Focus on improving performance qualities of extrudate
- Sorbent powder properties improvement for structure formation
- Catalyst manufacturing development
- Large pilot-scale testing or 1 TPD prototype

*Enable small-scale applications of oxygen such as 10-30MW gasifiers or 1 to 10 TPD systems by providing air separation at small-scale matching air separation cost of larger cryogenic separation systems.*

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## **RTI International**

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Dr. Jak Tanthana  
Dr. Paul Mobley  
Dr. Jian Zheng  
Dr. Vijay Gupta  
Dr. Mustapha Soukri  
Jonathan Peters

## **DOE\NETL**

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## **Air Liquide**

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Philippe Coignet

## **GTRC**

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