## Electrochemically-Driven Carbon Dioxide Separation DE-FE0031955

Brian P. Setzler University of Delaware

U.S. Department of Energy National Energy Technology Laboratory **Direct Air Capture Kickoff Meeting** February 24-25, 2021

## **Program Overview**

Funding: \$800,000 federal + \$200,000 cost share

Period of Performance: 10/1/2020 – 3/31/2022

Participants: University of Delaware

Project Objectives:

- Develop electrochemically-driven  $CO_2$  separator with 0.4 mol/m<sup>2</sup>-hr air capture at <235 kJ/mol<sub>CO2</sub> (1.5 MWh/t)
- Characterize poly(aryl piperidinium) (PAP) properties to support future development

## **Technology Background**

### Principles of operation

- 1. Generate OH<sup>-</sup>
- 2. Scrub  $CO_2$  as  $CO_3^{2-}$
- 3. Transport  $CO_3^{2-}$
- 4. Consume OH<sup>-</sup>
- 5. Release  $CO_2$

### Technical advantages

- Continuous separation
- Strong binding by OH<sup>-</sup>
- Electrically driven
- Ambient temperature



# Technical Approach/Project Scope

- 1. Project management and planning
- 2. Membrane fabrication Make flow-through PAP porous absorbers
- **3. Polymer/membrane characterization** Characterize dense and porous PAP polymer properties necessary to predict EDCS performance
- 4. Membrane electrode assembly testing Integrate absorber, membranes, and electrodes in small single cells (25 cm<sup>2</sup>) and test EDCS performance
- 5. **Process development** High-level process design and analysis

Mile- stone	Sub- task	Milestone Description	Planned Completion
4	3.1	<b>Membrane anion transport:</b> Establish operating window where conductivity is $\geq 5$ mS/cm.	3/31/2021
5	3.2	<b>Membrane CO<sub>2</sub> capture and release:</b> Establish operating window where first-order rate constant is $\geq 1000 \text{ s}^{-1}$ and where thick-film mass transfer coefficient is $\geq 1 \text{ mm/s}$ .	9/30/2021
6	4.3	<b>Initial cell testing and performance:</b> Demonstrate basic level of performance: $\leq 320$ kJ/mol (2 MWh/t <sub>CO2</sub> ), 0.1 mol/m <sup>2</sup> -hr CO <sub>2</sub> production (25 cm <sup>2</sup> )	9/30/2021
7	4.3	<b>Final cell performance:</b> Characterize wide range of operating parameters. Final targets: $\leq 235 \text{ kJ/mol} (1.5 \text{ MWh/t}_{CO2}), 0.4 \text{ mol/m}^2\text{-hr CO}_2 \text{ production} (25 \text{ cm}^2)$	3/31/2022
8	5.1	<b>Process flowsheet:</b> Complete flowsheet showing high-level process design and calculate mass and energy flows	3/31/2022

Success criteria:- Characterize PAP properties to enable modeling and analysis- Demonstrate technical feasibility at moderate performance level

4

## **Team and Facilities**



Yushan Yan (PI)

Thank you to our many colleagues whose foundational work made this project possible:

- Junhua Wang
- Yun Zhao
- Teng Wang
- Stevi Matz
- Lin Shi
- David Yan
- Rohan Razdan
- Catherine Weiss
- Santiago Rojas-Carbonell
- Junwu Xiao



Brian Setzler (co-PI)





James Buchen



Membrane and cell test stations

## Progress and Current Status of Project

### Equipment constructed / adapted

• Polymer conductivity apparatus controlling temperature, humidity, and CO<sub>2</sub> concentration

#### **Accomplishments**

- Fabricated porous absorbers
- Ni(OH)<sub>2</sub> electrodes with polymer electrolyte

### Performance achieved

- Electrodes (affect cell voltage and reversal losses): 0.32 V full cycle overpotential, 100 mAh/g
- Cell: 0.05 mol/m<sup>2</sup>-hr at 100 kJ/mol (0.6 MWh/t)
- Target: 0.40 mol/m<sup>2</sup>-hr at 235 kJ/mol (1.5 MWh/t)





• 90% RH

# **Opportunities for Collaboration**

- Standardization of methods to characterize kinetics and thermodynamics of  $CO_2$  in anion exchange polymers
- Fabrication of porous polymer films
  - Structural properties are critical to device performance
  - Project will cover only a small fraction of the possible fabrication methods
- Development of CO<sub>2</sub> hydration catalysts
  - Accelerate CO<sub>2</sub> capture
  - Lower energy consumption (smaller pH swing)
- Technoeconomic analysis and manufacturing cost estimates