Highly Permeable Thin Film Composite Membranes of Rubbery Polymer Blends for CO₂ Capture



Lingxiang Zhu, Victor Kusuma, and David Hopkinson, NETL Research & Innovation Center







- **Project:** High Permeance Blended Rubbery Membranes
- Funding source: NETL-RIC Field Work Proposal Transformational Carbon Capture Task 21
- **Project period**: EY21 EY23 (04/01/2021 03/31/2024)
- Project Objectives: developing a scalable thin-film composite (TFC) membrane for industrial carbon capture that has a CO₂ permeance >3,000 gas permeance unit (GPU) and CO₂/N₂ selectivity of >25. Both the membrane support and selective material will be optimized for scalability, thermal and chemical stability, and anti-aging properties.
- Project participants:

NETL Research & Innovation Center (RIC) Idaho National Laboratory (INL) National Carbon Capture Center (NCCC)







Technology background: the importance of high-permeance membranes



12 COE Reduction (%) 8 **Project objective** 4 Baseline: amine absorption 0 State-ofthe-art CO_2/N_2 selectivity membranes -8 (lab-scale) 25 R&D) 50 -12 2000 1000 3000 4000 5000 6000 0 CO₂ permeance (GPU)

COE: cost of electricity

- Coal flue gas decarbonization: membrane vs amine absorption
- Two-stage membrane process with air sweep (designed by MTR)
- 95% CO₂ purity at a high CO₂ recovery (capture rate) of 90%

For flue gas decarbonization, an increase in CO_2 permeance is more important than a further increase in CO_2/N_2 selectivity when the selectivity is above 25.

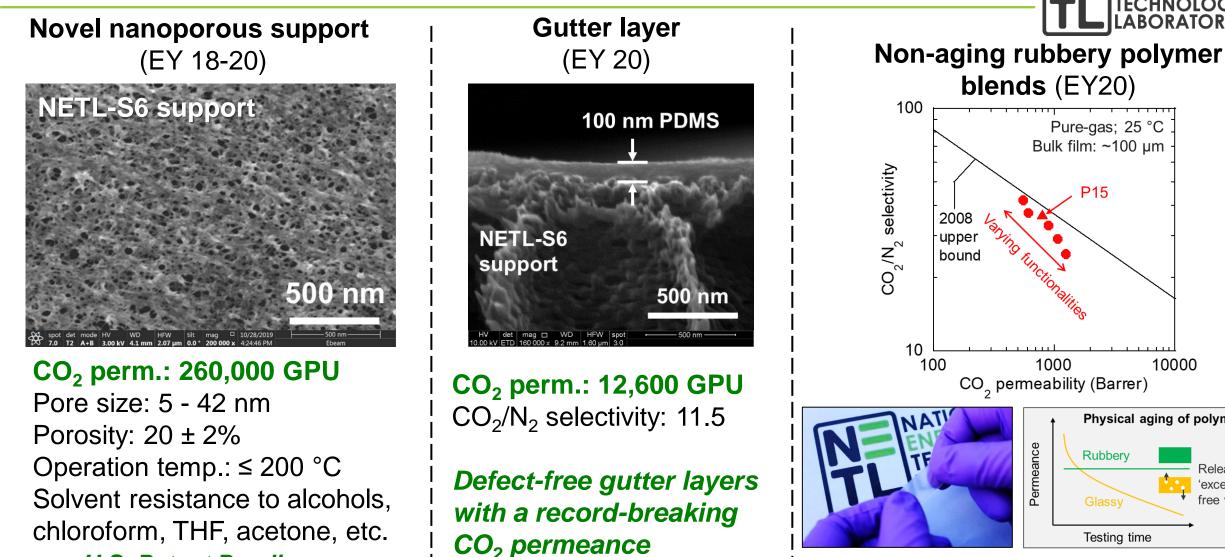
Alex Zoelle et al., Performance and Cost Sensitivities for Post-Combustion Membrane Systems, 2018 NETL CO₂ Capture Technology Project Review Meeting



optimization and thin-film composite (TFC) fabrication Permeability (P) of selective material \uparrow $\mathbf{1}$ Permeance = -**Selectivity** $(> 25) = P(CO_2)/P(N_2)$ thickness of selective layer *Permeance (in GPU) is pressure normalized flux. Permeability (in Barrer) is a material property independent of thickness.* 2. TFC membrane fabrication 1. Selective material optimization Permeability/selectivity tradeoff Selective layer Thickness CO_2/N_2 Selectivity Bulk film reduction $l = \sim 100 \text{ nm}$ Gutter layer $l = \sim 100 \text{ micron}$ Porous support **Selective layer** (< <1 um): CO₂/N₂ separation Robeson's 2008 upper bound plot **Gutter layer** (< 500 nm): preventing pore penetration & 100 10^{4} 0.0001 0.01 smoothening porous support CO_2 permeability (P_{CO_2} , Barrers) **Porous support** (> 20 µm): mechanical reinforcement Robeson, J. Membr. Sci. 320 (2008) 390

Technology background: achieving high permeance via selective material

Prior technology development efforts



U.S. Patent Pending



Release of

'excessive'

free volume

ATIONAL

P15

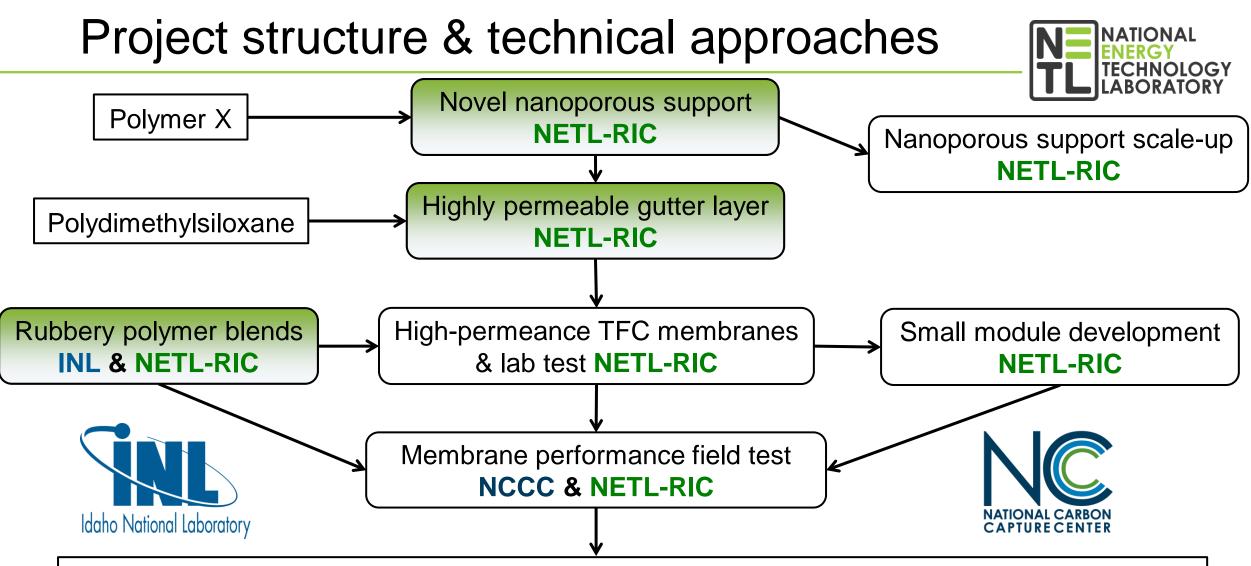
Rubberv

Testing time

TECHNOLOGY ABORATORY

10000

Physical aging of polymers



Project objective (03/2024): demonstrating a TFC membrane module with CO_2 permeance of >3,000 GPU and CO_2/N_2 selectivity >25 in a long-term (>500 hrs) field test.

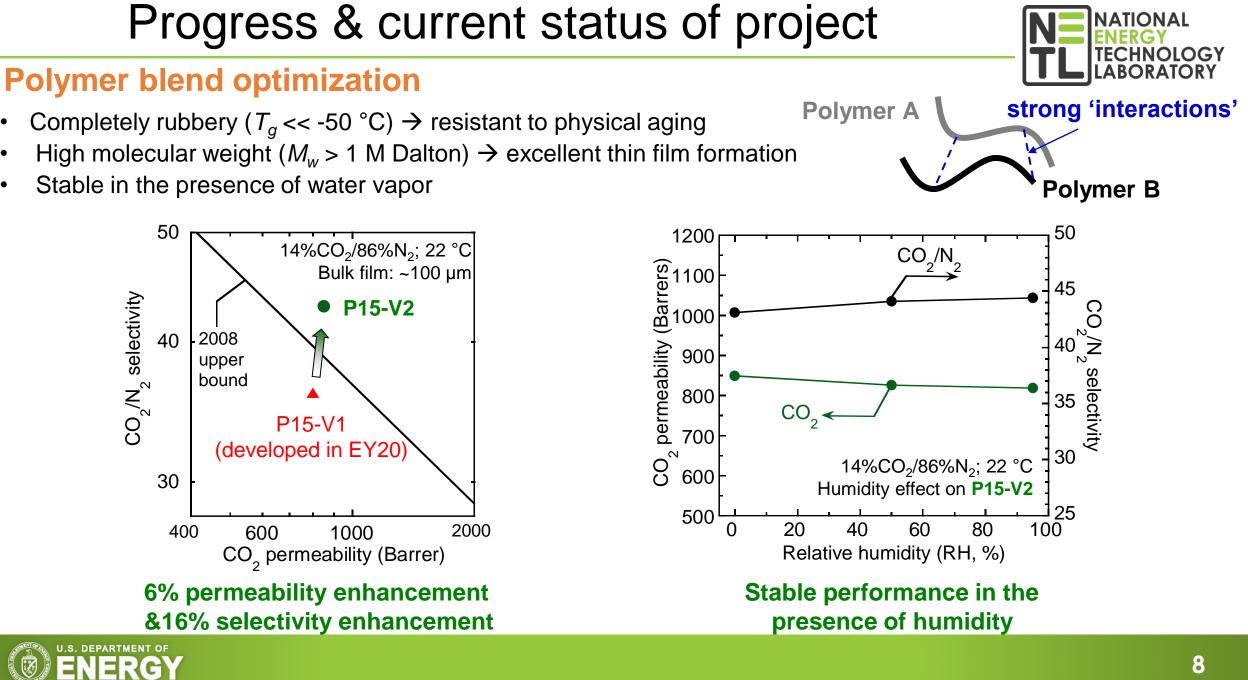


Project schedule and milestones



Schedule	Milestones		
EY21 : 04/01/2021 - 03/31/2022	Demonstrate a functioning 100 cm ² TFC with CO ₂ permeance of > 3,000 GPU and CO ₂ /N ₂ selectivity of > 25 targeted for industrial flue gas and showing no significant aging for 1,000 hours.		
EY22: 04/01/2022 - 03/31/2023	Demonstrate a bench-scale 100 cm ² plate-and-frame module of TFC membranes with CO_2 permeance of > 3,000 GPU and CO_2/N_2 selectivity of > 25 using real or simulated flue gas.		
EY22: 04/01/2022 - 03/31/2023	Demonstrate a roll-to-roll fabrication of flat-sheet membrane support at a size of 30 cm \times 10 m.		
EY23: 04/01/2023 - 03/29/2024	Demonstrate a TFC membrane module with CO_2 permeance of > 3,000 GPU and CO_2/N_2 selectivity of >25 in a long-term (> 500 hours) field test.		

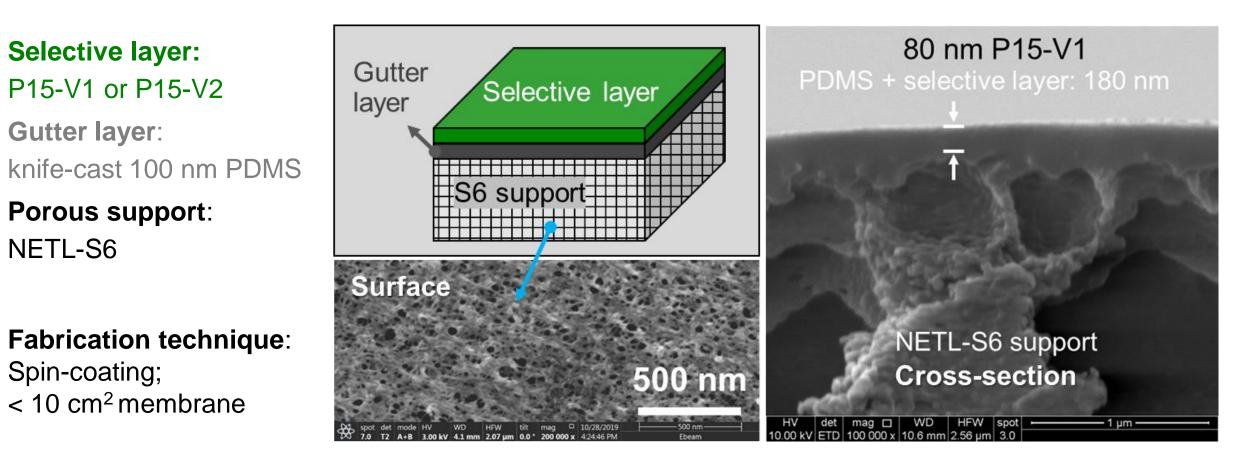




Progress & current status of project



Influence of polymer blend optimization on TFC membranes - Coupon-size TFC fabrication





Progress & current status of project



- Influence of polymer blend optimization on TFC membranes
- TFC coupons' performance at 22 25 °C in pure-gas

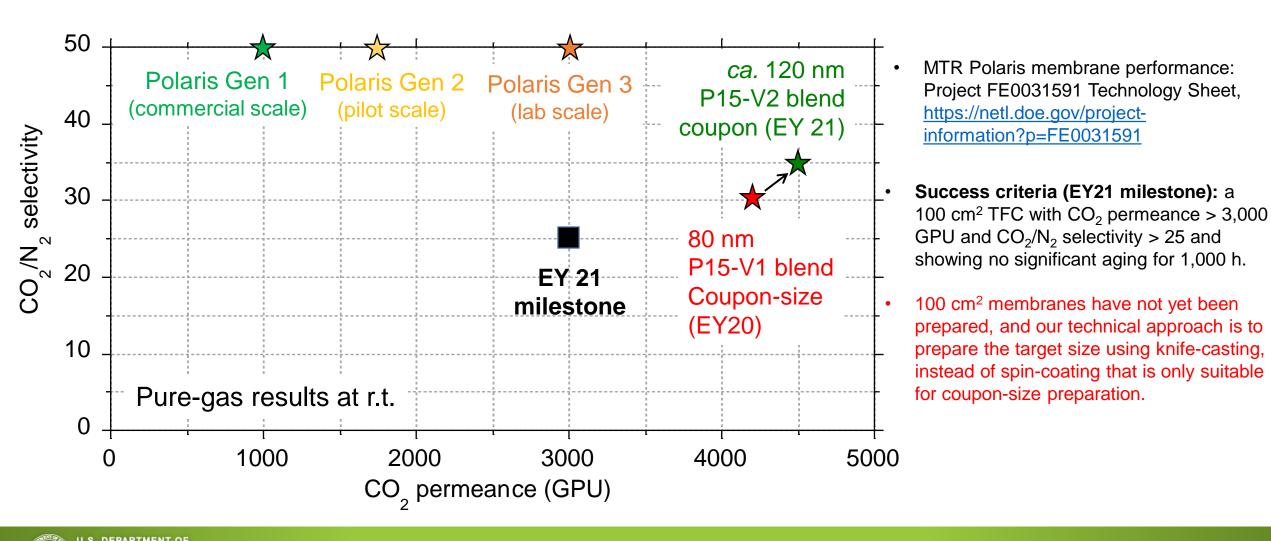
Selective material	Selective layer thickness (nm)	CO ₂ permeance (GPU)	CO ₂ /N ₂ selectivity
P15-V1 (developed in EY20)	80	4200	30
P15-V2 (newly optimized)	120 (est.)	4500 / 7%	34 / 13%

- Higher CO₂ permeance and selectivity in the P15-V2 TFC than the P15-V1 TFC though the P15-V2 layer is thicker.
- No permeance drop was observed on the P15-V2 TFC after aging for 300 hrs.



Comparison of the polymer blend TFC membranes with the leading membranes for CO_2/N_2 separation





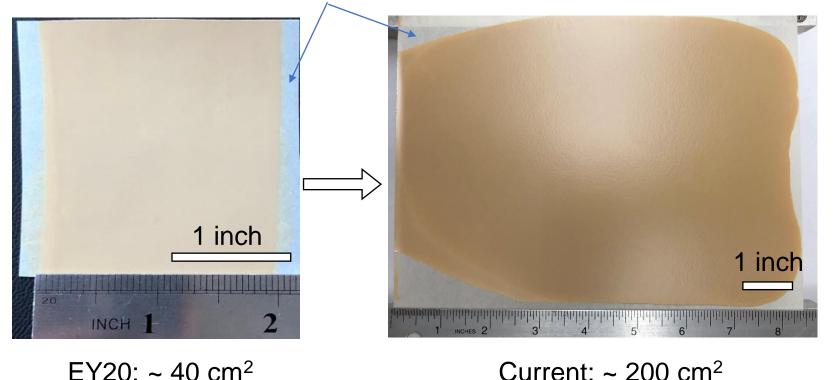
11

Progress & current status of project

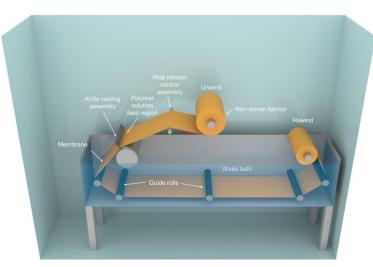
Scale-up activities on NETL-S6 support

to accommodate the P15-based TFC membrane scale-up (to 100 cm² in EY21)

Non-woven fabrics



Roll-to-roll fabrication



Machine customization in progress

A non-provisional patent application was filed on the NETL-S6 support fabrication in July 2021.



Future plans



TFC fabrication and lab test (the rest of EY21)

- Fabrication of 100 cm² P15-V2 based-TFC membranes;
- Dry/wet mixed-gas testing of P15-V2 based-TFC membranes using 10 30% CO₂ balanced with N₂ that simulates gas streams emitted from coal power plants (14% CO₂), cement plants (20-30% CO₂) or steel mills (20-30% CO₂).

Membrane modulation and porous support scale-up (EY22)

- Small plate-and-frame membrane module fabrication and testing in lab and at NCCC;
- Procurement, installation, shakedown, and operational test of a roll-to-roll membrane fabrication machine. Pilot-scale (30 cm × 10 m) production of NETL-S6 support.

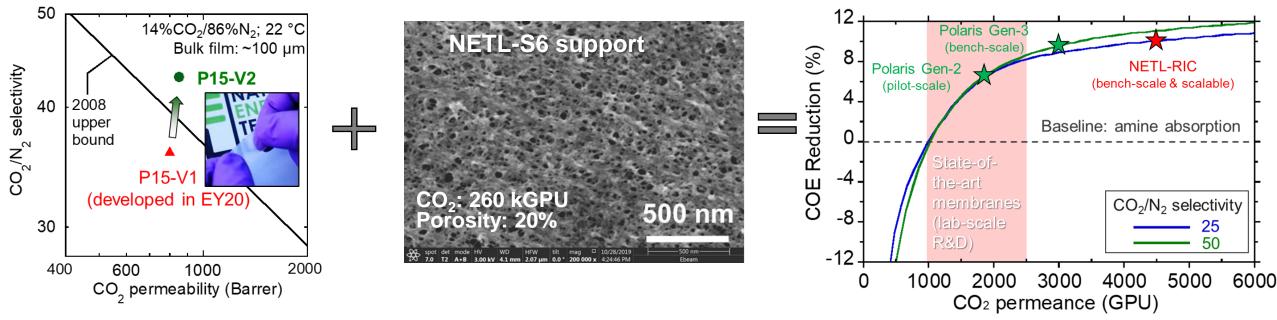
TFC scale-up and field test (EY23)

- TFC membrane scale-up, module optimization, and a long-term field test of the membrane modules



Summary: NETL has taken a well-designed and fruitful approach to high-permeance TFC membranes for low-cost CO₂ capture.





Lower-cost CO₂ capture (10% decrease) *vs.* amine absorption

1. Alex Zoelle *et al.*, <u>Performance and Cost Sensitivities</u> for Post-Combustion Membrane Systems, 2018 NETL CO₂ Capture Technology Project Review Meeting 2. MTR Polaris membrane performance: Project FE0031591 Technology Sheet, https://netl.doe.gov/project-information?p=FE0031591

Selective material optimization

(U.S. patent application in preparation)

Novel porous membrane support (U.S. patent pending)

<u>m:p=re</u>



Acknowledgements



Team leads: David Hopkinson (david.hopkinson@netl.doe.gov) Kevin Resnik

Program management: Lynn Brickett Dan Hancu

Simulation team: Janice Steckel Samir Budhathoki Wei Shi Surya Tiwari

ENERGY

Membrane team:

James Baker Sameh Elsaidi Victor Kusuma Patrick Muldoon Ali Sekizkardes Zi Tong Fangming Xiang Shouliang Yi Lingxiang Zhu (lingxiang.zhu@netl.doe.gov)

Collaborators:

Josh McNally (INL) Tony Wu (NCCC/Southern Co.) Robert Lambrecht (NCCC/Southern Co.)





Disclaimer



This project was funded by the United States Department of Energy, National Energy Technology Laboratory, in part, through a site support contract. Neither the United States Government nor any agency thereof, nor any of their employees, nor the support contractor, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof.



NETL Resources

VISIT US AT: www.NETL.DOE.gov







@NationalEnergyTechnologyLaboratory

CONTACT:

Lingxiang Zhu lingxiang.zhu@netl.doe.gov David Hopkinson (Team Lead) <u>david.hopkinson@netl.doe.gov</u>

