

#### Development of Self-Assembly Isoporous Supports Enabling Transformational Membrane Performance for Cost Effective Carbon Capture (DE-FE0031596)

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# **Project Overview**

- Award Name: Development of Self-Assembly Isoporous Supports Enabling Transformational Membrane Performance for Cost Effective Carbon Capture (DE-FE0031596)
- **Project Period:** June 1, 2018 November 30, 2022
- Funding: \$2,905,620 DOE; \$726,805 cost share (MTR and University of Buffalo)
- DOE Project Manager: Carl Laird
- Participants: Membrane Technology and Research, Inc., University of Buffalo, University of Texas at Austin
- Project Objectives:
  - Develop supports for composite membranes with highly regular surface pore structures that eliminate the restriction on diffusion in the selective layer that is present with current generation supports
  - Develop improved selective materials with higher permeance and/or higher selectivity compared to the current generation Polaris material
- Project Plan:
  - BP1: Lab-scale support development, screening of novel selective materials
  - **BP2:** Lab-scale support development, scale up of selective materials, composite membrane optimization
  - BP3: Commercial-scale composite membrane development, lab-scale module testing at MTR, bench-scale module test at NCCC

#### Current Status: - BP2 nearly completed

- BP3 Continuation Application underway



# **Project Background**

- MTR has developed the **PolarCap<sup>TM</sup>** carbon capture process
- Key component is the highly permeable **Polaris<sup>™</sup>** membrane
- Higher permeance membranes will reduce cost of capture
- Higher selectivity, but lower permeance, membranes will reduce cost of capture, particularly in industrial capture where CO2 source may be available at elevated pressure
- Higher permeances are typically achieved by making composite membranes with thinner selective layers.
- Our previous work has established that the surface pore structure of the support membrane is a limiting factor for thin selective layers, because:

**Reducing** the selective layer thickness by a factor of two **does not increase** the permeance by a factor of two, even though the support membrane has negligible resistance.



CFD analysis has shown that the pore structure of the support changes the diffusion path in the selective top layer.

## **Project Objectives, Success Criteria**

- 1. Produce Support Membranes with improved surface structures by
  - 1. Using block copolymers to create support membranes with isoporous surfaces
  - 2. Employ a dual-slot die casting technique to make "two-layer" support membranes
- 2. Demonstrate that these support membranes allow composite membranes to be produced with higher permeances
- 3. Investigate new selective materials to produce higher selectivity membranes
- 4. BP2 Success Criteria:
  - 1. Composite membranes prepared with CO2 = 3,000 gpu and CO2/N2 = 20 (mixed gas)
  - 2. New selective materials demonstrated to have improved selectivity
- 5. BP3 Success Criteria
  - 1. Composite membranes prepared with CO2 = 4,000 gpu and CO2/N2 = 25 (mixed gas)
  - 2. Composite membranes prepared with CO2 = 2,000 gpu and CO2/N2 = 50 (mixed gas)
  - 3. Small modules tested at NCCC



# **Effect of Support Membrane Surface**



Computational Fluid Dynamics simulations show that non-uniform distribution of surface pores is a major contributor to the reduction in measured permeance.  $\rightarrow$ 

# Isoporous membranes are ideal supports for composite membranes.



200 nm

Surface of Isoporous Support



#### – Variations in BCP surfaces obtained at MTR –



Surface of Conventional Support

Conclusion:

Reproducible preparation of isoporous surfaces on a large scale is difficult.





### **Isoporous Surface prepared at MTR**

**Scanning Electron** Microscope









- The AFM profile shows that remnants of six micelles • surround the pore at the surface
- Confirms the hypothesis that a pore is created by ٠ assemblies of six spherical micelles



#### Nano-IR + PiFM reveals distribution of the Blocks

Nano-IR

PiFM



- Polystyrene (PS) forms the bulk of the support
- Polyvinylpyridine (P4VP) lines the pores, indicating that P4VP makes up the outer layer of the micelles
- Top surface shows traces of P4VP which is consistent with a top surface covered by a P4VP layer of about 5 nm thickness (Nano-IR depth penetration is about 20 nm)

820 cm<sup>-1</sup> (**P4VP**) 1027 cm<sup>-1</sup> (**PS**)





#### PS based Block Copolymer (Polymer Source, Inc.)

- Uncoated permeance of support is 162,000 gpu
- CO2 permeance of PDMS coated support is 11,800 gpu
- PDMS thickness is 143 nm
- Sample too small to be coated with Polaris layer
- Confirms that a better surface results in an increase in permeance





#### **UT Austin Block Copolymer: Hand-Cast Support**

- UT Austin developed an alternative approach to making block copolymers
- "Simplified block copolymer"
- Hand-cast dual layer supports with the PEI-b-PEO block copolymer as top layer
- Excellent support membranes, even though the surface is not truly isoporous:







PEI-b-PEO block copolymer N2 permeance = 95,000 gpu

# **Support Casting Techniques**

#### Blade Casting (conventional):

- Common method for membrane casting
- Simple equipment, simple operation
- Allows for deposition of only one layer

#### Slot Die Casting (this project):

- Possible to deposit multiple layers
- Better control of thicknesses
- More complicated, but used on large scale in many casting and coating operations











### **Conventional Polymer, Dual Slot Die**

- Dual Slot Die in stalled on MTR R&D casting machine
- Advantage of Dual Slot Die is that the top and bottom layers can be made with different casting solution formulations
- This allows optimization of top layer for surface properties
- And allows optimization of the bottom layer for mechanical strength
- Dual Slot Die produces a better support
- Casting runs sufficiently long that Polaris coating runs can be made on MTR R&D coating machine.





#### **Current Best Polaris Membrane Performance**





#### **Polaris Performance with Wet Gas**





#### **Effect of Membrane Improvement**

Initial Techno-Economic Analysis:

- Effect of improved membrane.
- No optimization of operating pressures.





#### **Novel Selective Materials**

We confirmed that the novel materials made by the University of Buffalo have high selectivities, but also discovered that it is very difficult tailoring the MTR Polaris coating techniques to these new materials.



34 membranes 4 monomer batches

Difficulty in producing defect-free top layers → multiple coatings

The approach developed for BP3 is to combine the polymer synthesis and chemistry expertise of the University of Buffalo and UT Austin to solve this problem.



### **Planned BP3 Activities**

- Scale up PEI-b-PEO block copolymer manufacture to 1 kg scale (UT Austin)
- Synthesize alternative block copolymers (UT Austin)
- Install 40" wide dual slot die on MTR commercial casting machine
- Manufacture block copolymer based support membranes on commercial machine
- Prepare Polaris composite membranes on commercial coater
- Test Polaris membranes with pure gases and gas mixture
- Develop methods to turn the NYUB novel selective materials into suitable coating solutions (Buffalo and UT Austin)
- Prepare composite membranes with novel selective materials
- Prepare lab-scale modules with improved Polaris composite membranes
- Test modules with pure gases and gas mixture
- Build test system for small modules and operate at NCCC
- Perform Techno-Economic Analysis, Technology Gap Analysis and EH&S Risk Analysis



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Haiqing Lin

• University of Texas at Austin









#### **Thank You**

Questions?







#### **Self Assembly**

Amphiphilic block copolymer: A is hydrophobic, B is hydrophilic.

Separately A and B are not compatible, but in the block copolymer they are connected.

This leads to assembly into a range of different morphologies, depending on composition.



# Self Assembly → Isoporous

Asymmetric superstructure formed in a block copolymer via phase separation

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- Amphiphilic Block Copolymer in mixed solvent, evaporation step followed by immersion precipitation
- Block copolymers consist of two blocks, each block has a controlled molecular weight (mono disperse): Expensive



- Method creates top surface with highly ordered porous structure
- Literature working hypothesis is that the pores are formed via assembly of micelles, which have the majority blocks at the center and the minor block at the surface

(2007)

 Structure below top layer has a "tendril" like structure, and is different from the porous structure in conventional porous supports



#### Nano-IR + PiFM

#### Nanoscale InfraRed Spectroscopy + Photo-induced Force Microscopy

- Atomic Force Microscopy scans the surface of the sample by measuring the attractive force between the AFM Tip and the sample
- A laser with variable wavelength is used to polarize the sample which increases the attraction with the AFM Tip.
- The degree of polarization depends on the laser frequency and the chemical nature of the sample, much like is seen in an FTIR spectra.
- Sample area is about 10 nm by 10 nm
- Laser penetrates sample by about 20 nm



Image courtesy of Molecular Vista, San Jose, CA www.molecularvista.com



#### PS-b-P4VP block copolymer: PS and P4VP areas

#### PolyStyrene



491 μV

50 μV



Poly-4-VinylPyridine





Looking into the pore openings: No polystyrene, all poly-4-vinylpyridine In between pores: Mostly polystyrene, but also some poly-4-vinylpyridine 91 µV

# Isoporous Surface prepared at MTR with PS based block copolymer (Polymer Source)

Scanning Electron Microscope

Atomic Force Microscope







#### **Solvent System for PEI-b-PEO**

DMAC 100

- Developed solvent systems that dissolved the PEI-b-PEO block copolymer
- DMAc is a good solvent for the block copolymer
- THF is a good solvent for the PEO block, but does not dissolve the block copolymer
- Small amounts of THF are used to facilitate the selfassembly of the PEO blocks

- Successfully produced a porous support in hand casting experiments
- Uncoated support has permeance of 68,000 gpu.
- Pore radius is 38 nm





#### **Structure of the Project**





### **Computational Fluid Dynamics**



CFD results for uniform pore distribution are very accurately correlated by:



#### **Slot Die Casting**

Slot One



Slot Two



Top Layer Solution Bottom Layer Solution



#### **Slot Die Casting**







#### **Alternative to "Perfect" Block Copolymers**





# **UT Austin block copolymer**

The approach is to attach a Poly-ethylene-oxide block (M=5k) to the commercially available engineering polymer Ultem 1000 (poly-ether-imide):



### **Two Layer Approach: Dual Slot Die**

- Two separate layers created in a single step
- Top layer can be very thin (10 micron or less)
- Makes it possible to reduce block copolymer usage
- Independent optimization of two layers
- Dual slot die installed on MTR R&D caster
- Installation, pump system, completed in Sep 2019
- Each run requires at least 20 gram of polymer (top layer)
- Initial work on dual layer supports was carried out with conventional polymers







### Materials with High Oxygen/Carbon Ratio

(University of Buffalo)

i. Synthesis of PDXL Macromonomers (CROP)  $\begin{array}{c}
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Successful preparation of high permeance composite membranes requires an intermediate step.



ii. Preparation of Polymers (Photo-Polymerization)





PDXLEA

34

#### **Novel Selective Materials**





#### **Block Copolymer, Dual Slot Die**

Dual Slot Die Casting Block, Bottom Layer is PEI Homopolymer, 11" wide, Top layer is PEI-b-PEO block copolymer, 4" wide



#### **Polaris Composite Membranes**





#### **Polaris Composite Membrane on BCP**



#### **Polaris Composite Membrane on BCP**

January 20, 2021:



#### Gas Mixture Data, hand cast support

Feed gas: 20% CO2 in N2 50 psig

> CO2/N2 Selectivity (-)

Permeance advantage of the composite membrane prepared on a block copolymer based support membrane is maintained in gas mixture experiments at elevated temperature.





### Gas Mixture Data, machine cast support

- Decrease in selectivity from pure gas to ٠ mixed gas at RT is as expected
- Decrease in selectivity from RT to 50C is ٠ also as expected

CO2/N2

(-)

- Increases in CO2 permeance are less ٠ expected.
- To be investigated further



