

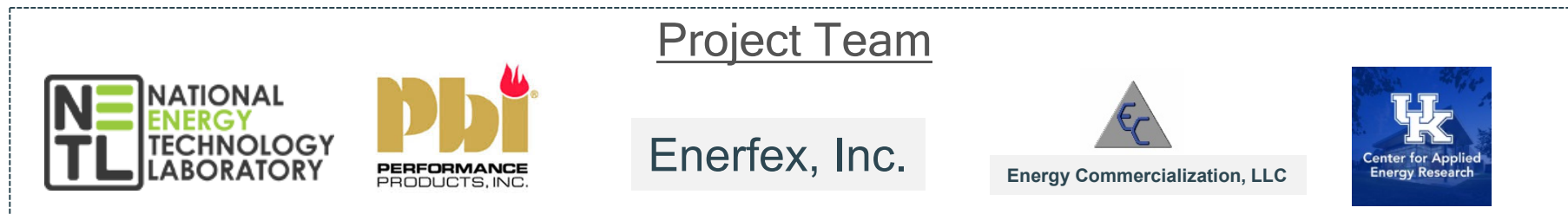


Project Review (FE0031633)

Development and Testing of a High Temperature PBI Hollow-Fiber

Membrane Technology for Pre-Combustion CO₂ Capture

Presented by Indira Jayaweera and Michael Wales
Integrated Systems and Solutions (InSyS) Division
SRI International



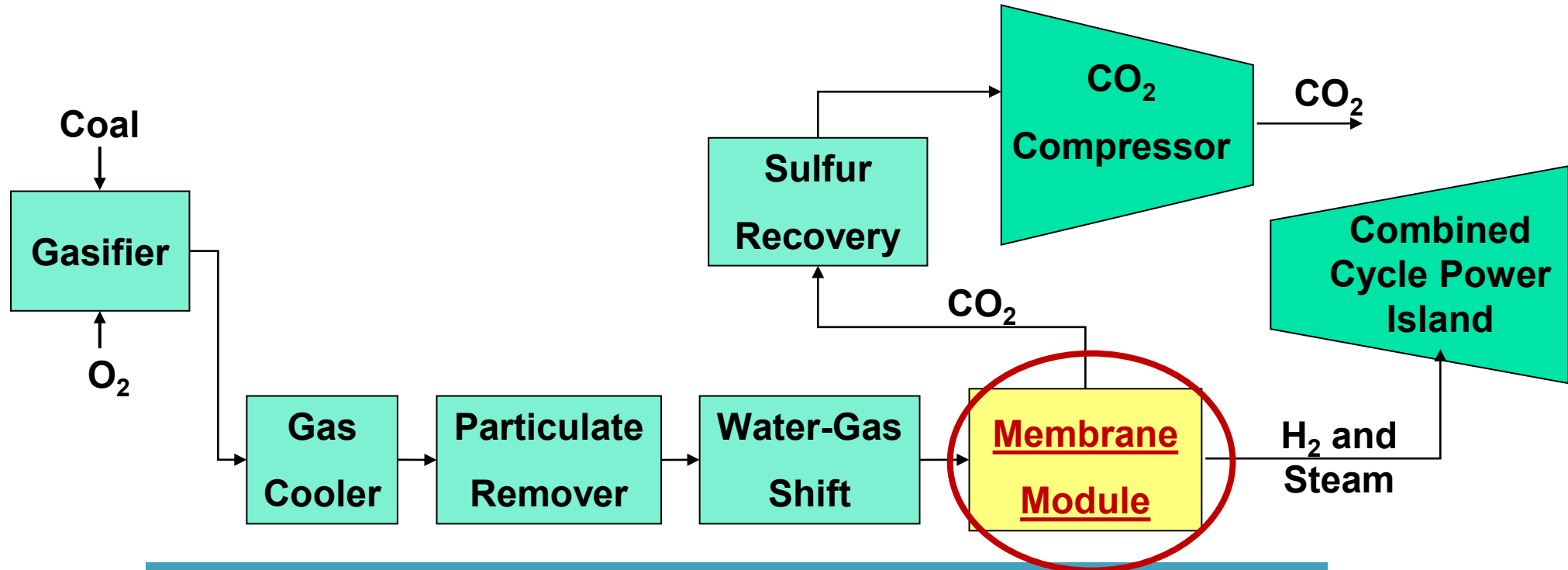
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Technology Background and Previous Projects

Membranes for Pre-Combustion CO₂ Capture

Advantages of High-Temperature Membranes for Separation of CO₂



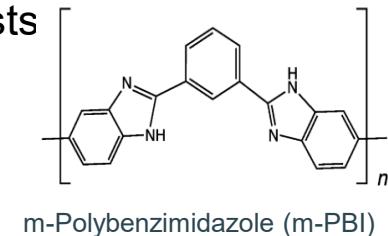
Note: PBI hollow fiber membrane (HFM) is a H₂O and H₂ transporting

Characteristics of PBI Membranes

- Thermally stable up to ~ 300°C and sulfur tolerant
- Tested up to 225°C with simulated gases and with real syngas
- Attractive combination of throughput (permeance) and separation (selectivity)

Advantages of Membrane-Based Separation

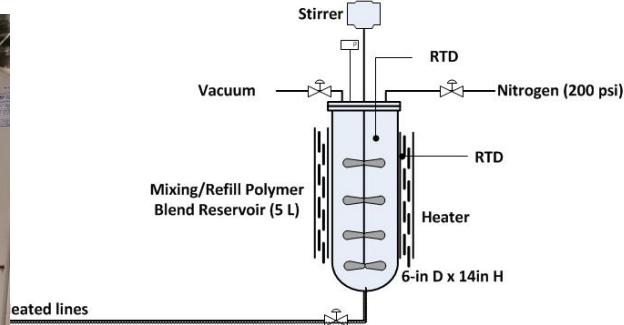
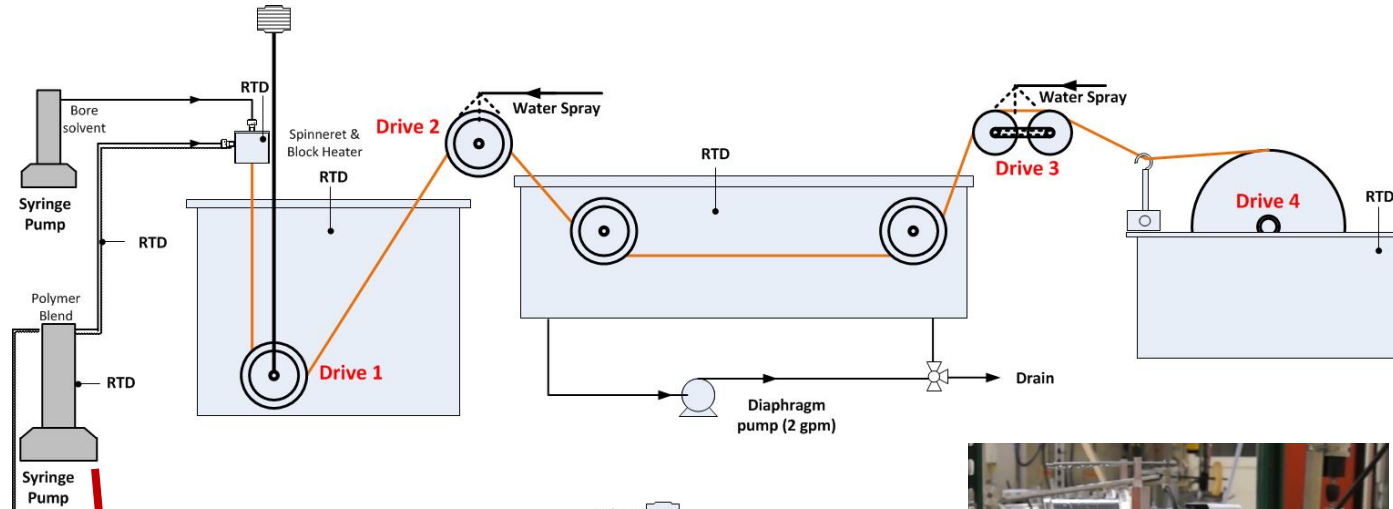
- Reduced costs for syngas cooling
- Reduced CO₂ compression costs
- Emission free, i.e., no solvents
- Decreased capital costs
- Low maintenance
- Modular



SRI Fiber Spinning Lines

1st line installed in 2015

2nd line installed in 2019



Fiber Optimization:

- Air gap
- Solvents
- Non-solvents
- Roller speed

Wall thickness
Pore size
Substructure
Dense layer thickness

Variety of Applications:

- Gas Separations¹
- Reverse Osmosis (RO)²
- Ultra Filtrations (UF)³

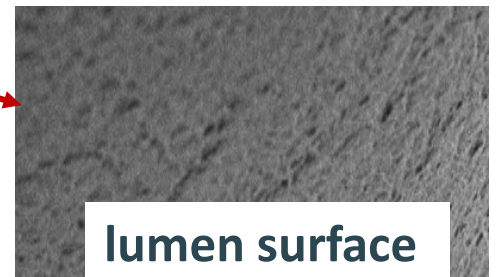
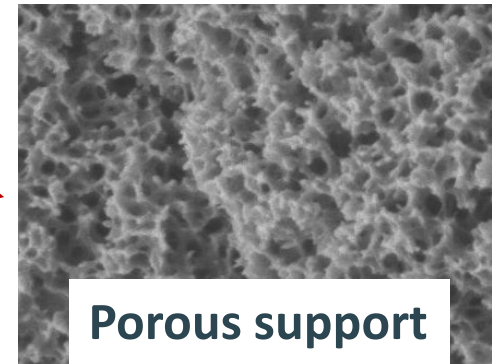
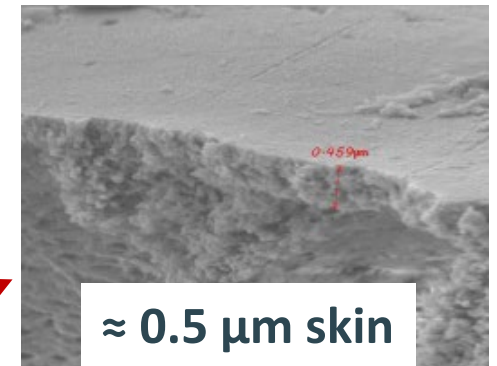
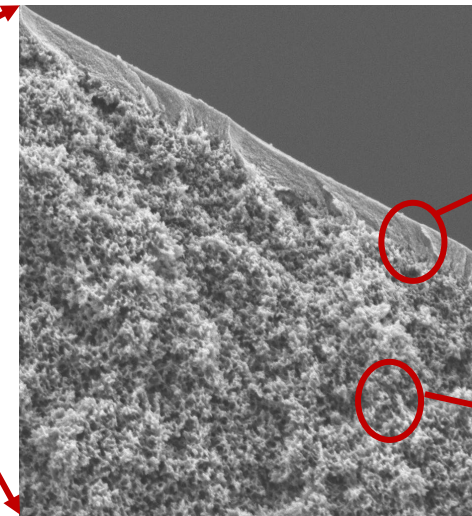
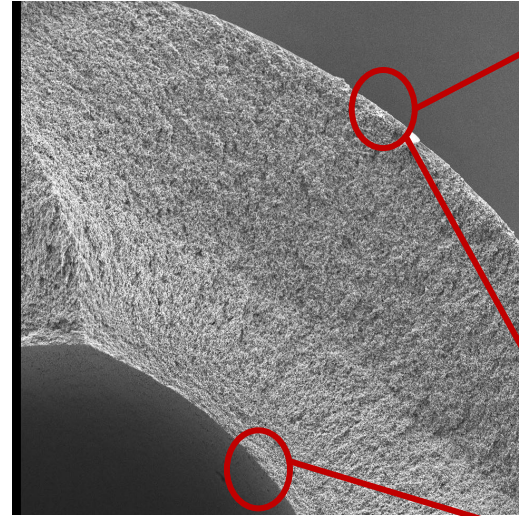
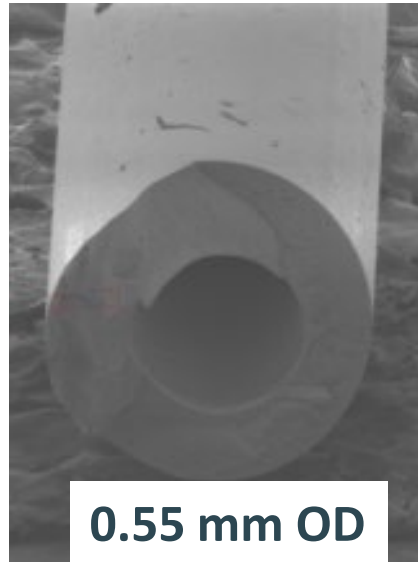
1. Xiao et al. (2018), Membranes, 2018, 8(4), 113;
2. Wales et al. (2021), Membranes, 2021, 11(6), 430;
3. Xiao et al. (2021), Desal and Water Treatment, 2021, 69-78, 229

Syringe Pumps

Drives and Motors

Fabrication of Fibers with Good Reproducibility

Quality Control is the KEY to success when scaling up



SRI Fiber Production – VERY GOOD REPRODUCIBILITY:

- Dense (skin) Layer: 0.3 – 0.5 μm
- OD: 450 – 650 μm
- ID: 120 – 250 μm
- Spun > 500 km

Tunable

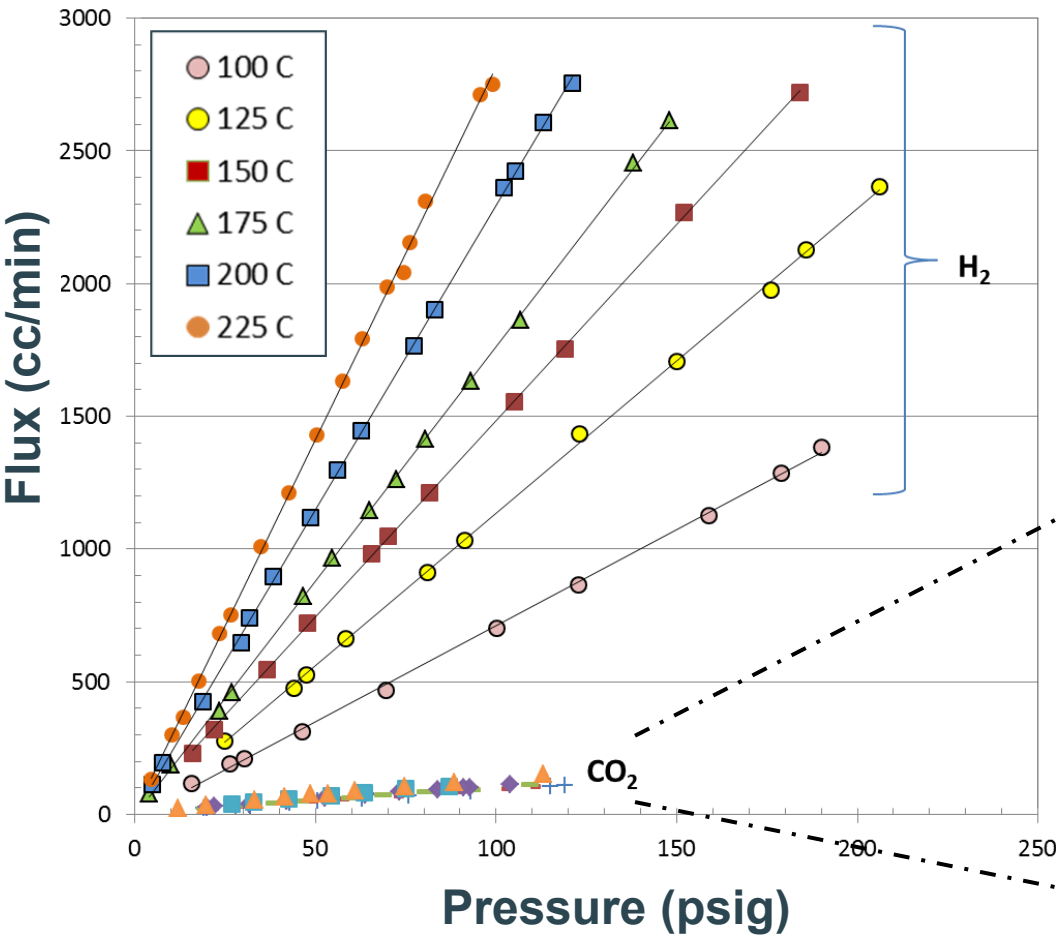
Achievements:

- Dense-layer thickness reduced from 1 μm to < 0.3 μm (Gen-1)
- Fiber diameter reduced from 1 mm to less than 600 μm

Gen-2:

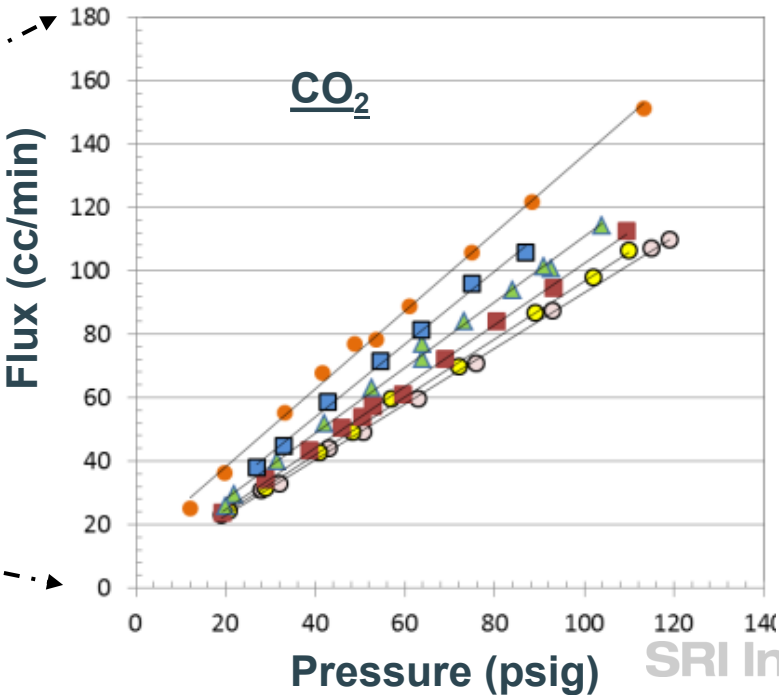
- 0.5 μm dense layer
- Reduce defect, improve reproducibility

PBI H₂/CO₂ Selectivity Increases with Temperature and Pressure



Mixed Gases

	Selectivity
H ₂ /CO ₂	40
H ₂ /N ₂	98
H ₂ /CO	103
H ₂ /H ₂ S	>200
225 °C and 200 psi ΔP	



Critical Asset: Membrane Testing Skid

Field Tested at the National Carbon Capture Center (NCCC)



5,000 fibers (5 m²) arranged for potting



4-inch modules (~5,000 fibers)



Skid installed at the NCCC (April 2017)

50 Kilowatt-Thermal Demonstration:

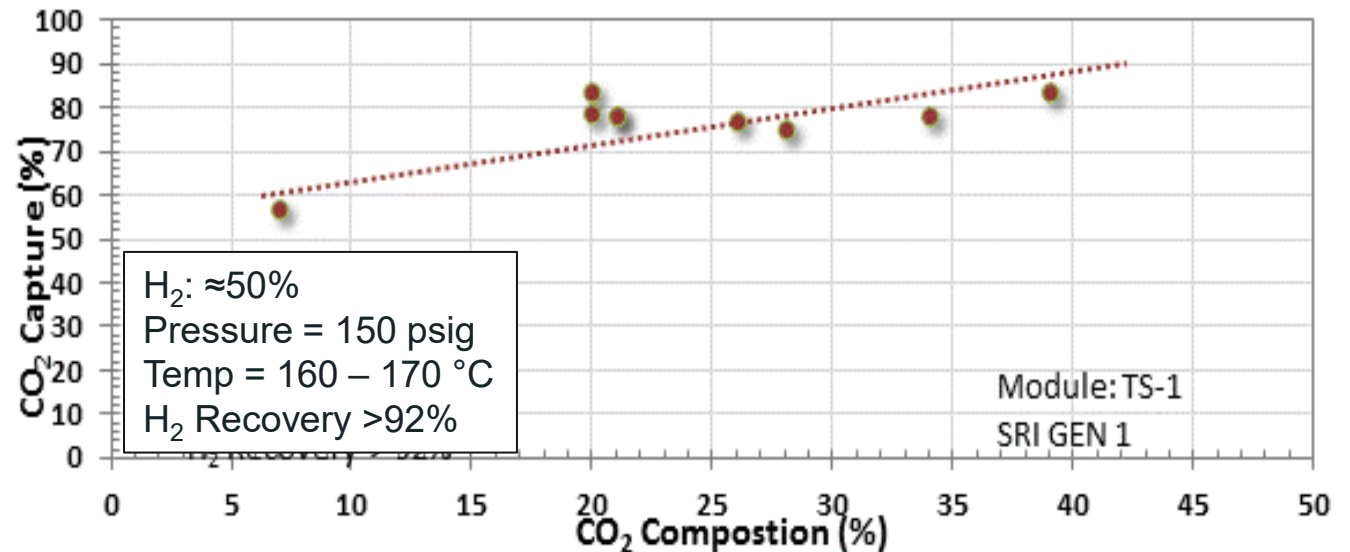
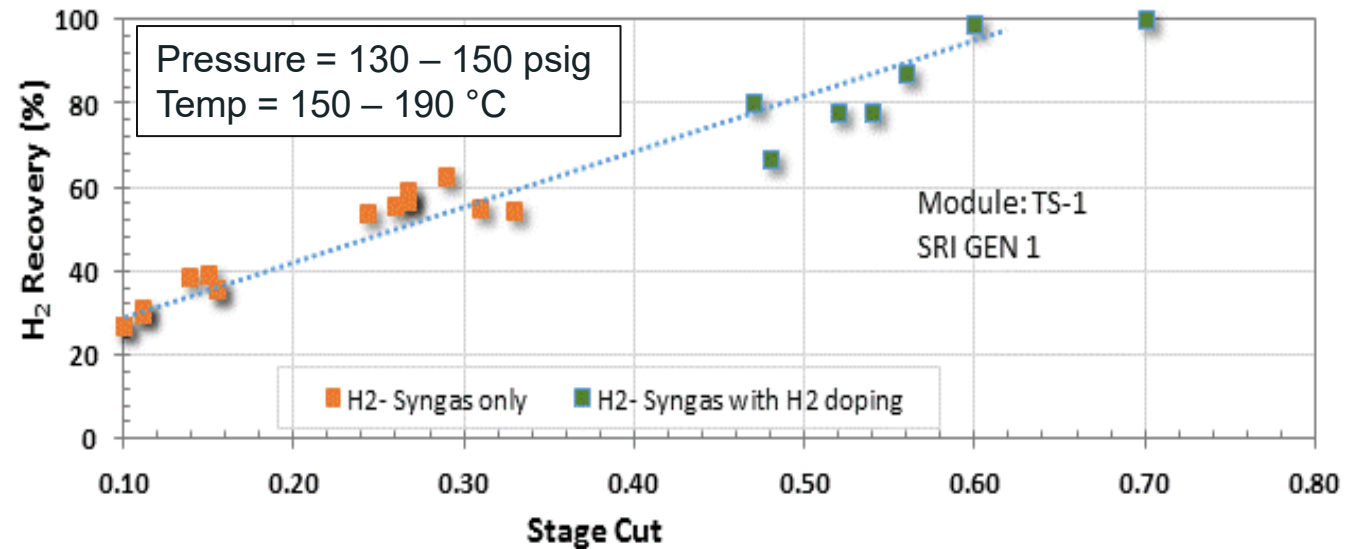
- PBI membrane skid transferred to NCCC in March 2017
- Tested in April 2017 (>600 hours)
- Returned to SRI in March 2018
- Used in current work (with upgrading)

Results from NCCC Field Test

Air-Blown Gasifier

Sample parametric matrix

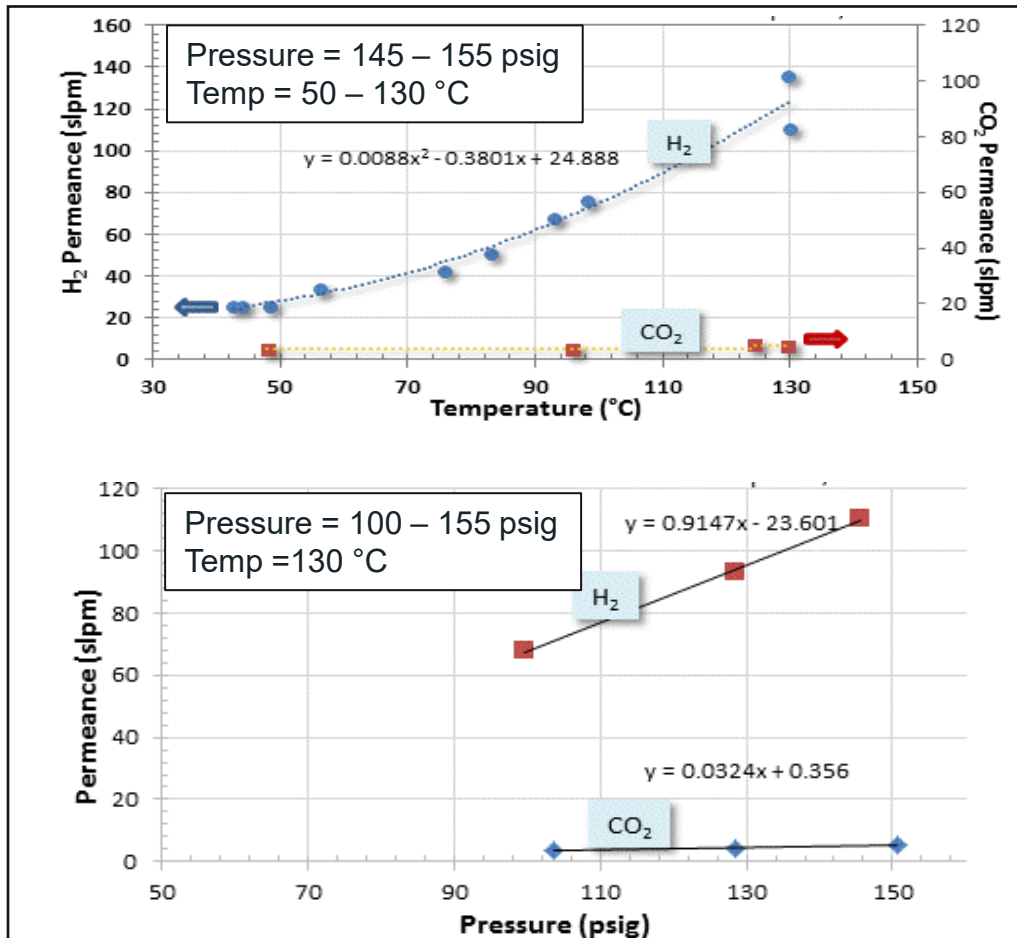
Test Parameter	Range	Unit
Temperature	80 – 215	°C
Pressure	50 – 170	psig
Gas composition	Variable	slpm
Stage cut	0.2 – 0.7	
H ₂ in syngas	12 – 50	%
CO ₂ in syngas	5 – 40	%



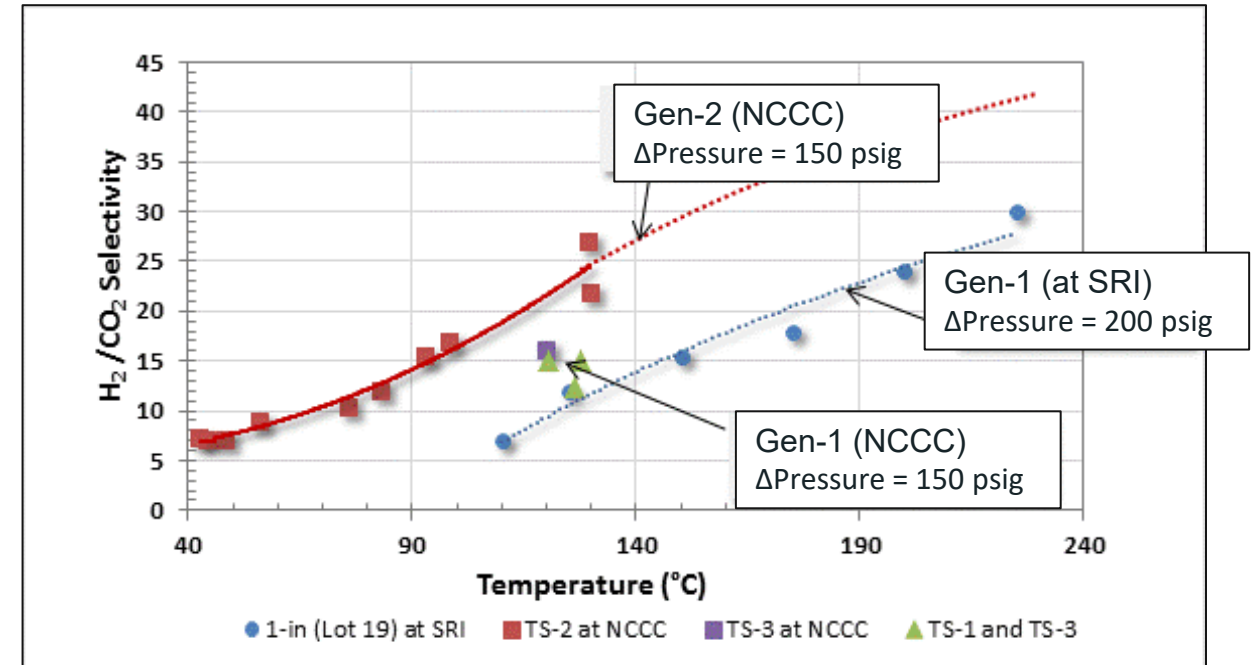
600 Hours of Data Collected

Gen-2 Results from NCCC Field Test

Air-Blown Gasifier



H₂ and CO₂ permeances as a function of temperature (top), function of pressure (bottom)



Gen-1 and Gen-2 selectivities as a function of pressure

Selectivity of PBI Gen-2 > PBI Gen-1:

- Gen-2 has better selectivity than Gen-1
40 compared to 25
- Gen-1 has higher flux (150 GPU compared to 100 GPU)
- Selectivity is more important than Flux (TEA)

Case Name	IGCC-B1A Baseline No Capture	IGCC-B5B ¹ Baseline CO ₂ Capture	SRI PBI GEN-1 Membrane CO ₂ Capture	SRI PBI GEN-2 Membrane CO ₂ Capture
CO ₂ removal	No	Selexol	PBI membrane	
CO ₂ purification	No		Yes	
Sulfur removal	Sulfinol	Selexol		
Performance and Economic Summary				
H ₂ /CO ₂ Selectivity	n/a	n/a	40	50
H ₂ GPU	n/a	n/a	80	80
CO ₂ capture	n/a	92.25%	90.04%	90.02%
CO ₂ purity	n/a	99.48%	95.62%	95.57%
H ₂ recovery	n/a	99.98%	96.10%	99.64%
HHV plant efficiency	42.10%	32.60%	32.61%	34.39%
LHV plant efficiency	43.70%	33.80%	33.81%	35.65%
COE w/o T&S (\$/MWh)	\$107.10	\$135.30	\$120.76	\$117.74
COE w/ T&S (\$/MWh)	\$107.10	\$144.50	\$129.96	\$126.94
% Increase in COE	0.00%	34.92%	21.34%	18.52%

% Increase in Cost of Electricity (COE)



Current Project Details

Objectives

Demonstrate that Gen-2 PBI based HFM provide a pathway to achieve DOE's pre-combustion capture targets:

- Targets: 90% CO₂ capture and 95% purity
 >99% H₂ recovery
 30% reduction in COE
- Field test 50 kWth fiber skid
- University of Kentucky Center for Applied Energy Research (UK-CAER), Oxygen Blown Gasifier
- Techno-Economic Analysis from field data

Leverage assets, technology, and knowledge from previous projects:

- Spin 100 km of SRI PBI fibers
- Improved potting and module construction
- Modifications/improvements to fiber skid

Project Budget and Team for DE-FE0031633

Cooperative agreement grant with U.S. DOE Period of Performance:

- BP1: 10-1-2018 to 03-31-20
- BP2: 04-01-20 to 09-30-21

Funding:

- U.S. Department of Energy: \$2.007 million
- Cost share: \$0.505 million (20.1%)
- Total: \$2.512 million

NETL Project Manager:

- Krista Hill
- Andrew Jones (former)

NETL

- Funding and technology oversight

SRI

- Gen-2 PBI membrane Spinning
- Module fabrication
- Skid installation & testing

PBI Performance Products, Inc.

- PBI Dope and industry perspective

Enerfex, Inc.

- Membrane system modeling and Techno-economic analysis

Energy Commercialization

- Commercialization analysis

UKy CAER

- Gasifier facility test site

Project Objectives and Tasks

Budget Period 1 (10-01-2018 → 03-31-2020)

Task #	BP	Task	Status
1	1	Project Management and Planning	Completed
1	1	Preliminary Technology Maturation Plan Program Management Plan Preliminary TEA	Completed
1	1	Installation of Partner Agreements and Sub-awards	Completed
2	1	Modification of the 50 kWth Test Unit - Refurbish and upgrading of the existing skid system - Fabrication of 100 km of SRI PBI Fibers - Module design and installation of the Modules (4 to 6-in diameter) - Membrane performance testing at SRI - HAZOP and PI&D Review at UK-CAER	Completed
3	1	Modeling - Modeling of the Module arrangement - Modeling of the skid performance - Preliminary TEA	Completed

Project Objectives and Tasks

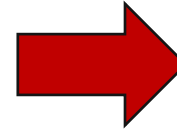
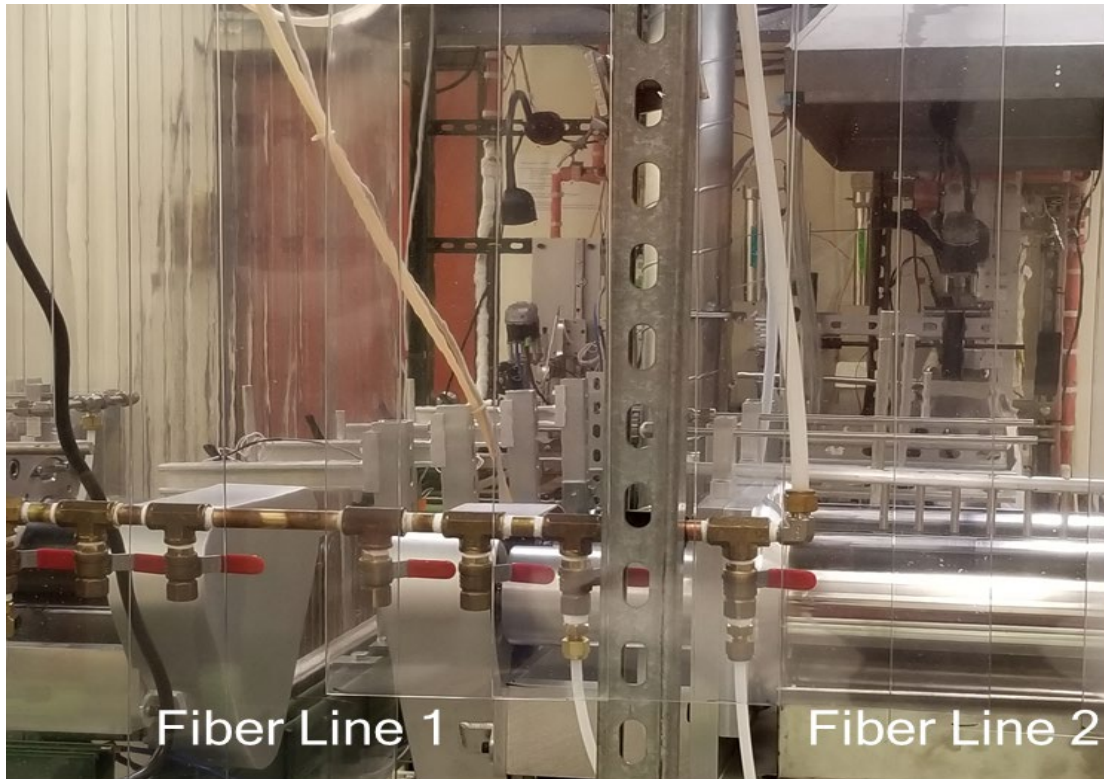
Budget Period 2 (04-01-2020 → 09-30-2021)

Task #	BP	Task	Status
4	2	Operation of the Test Unit at a Field <ul style="list-style-type: none">- Skid Transport and Installation at the Site- Development of a test plan- Operation of the skid and data collection- Analysis of the data form the skid	Started
5	2	EH&S, TEA and other Related Reports <ul style="list-style-type: none">- Techno-Economic Analysis- Update the State Point Data Table- Technology Gap Analysis- Preparation of Technology Maturation Plan- Environmental Health and Safety Assessment (EH&S)	Not Started (Post-UK CAER)
6	2	Skid Decommissioning <ul style="list-style-type: none">- Skid decommissioning and Transport- Skid Postmortem and Storage	Not Started (Post-UK CAER)

2nd Spinning Line Installed in 2019

Budget Period 1

New = Fiber Line 2 (right):



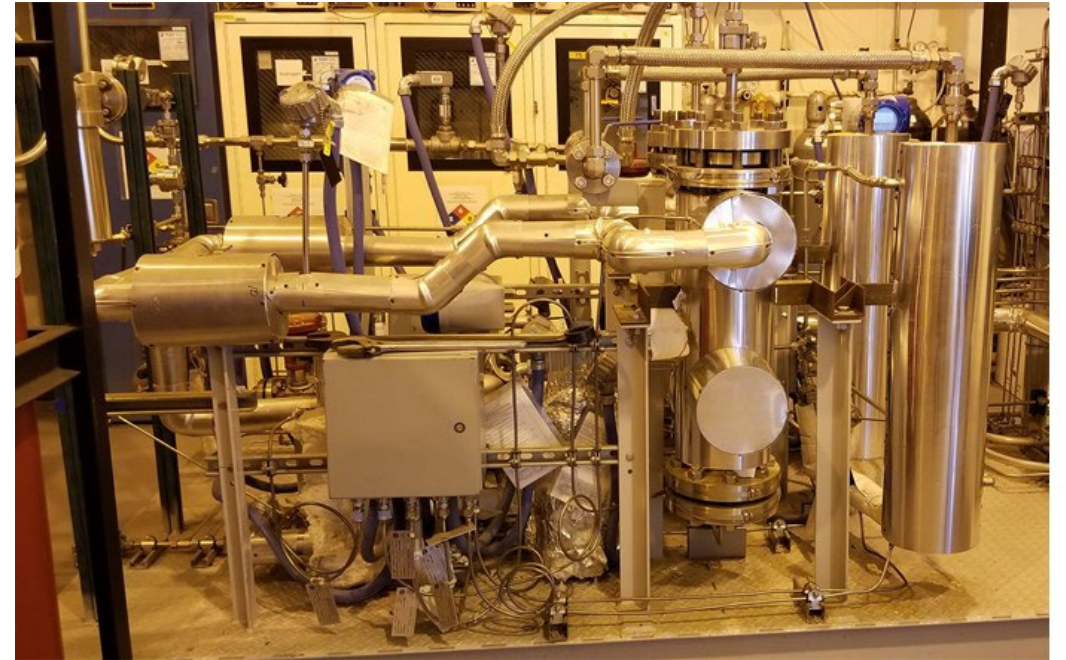
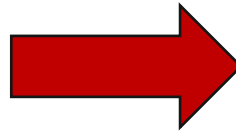
Spin 150 km of fibers (BP-1):



Fiber Skid Modifications/Improvements

Budget Period 1

Refurbished existing Skid:



Fiber Skid Modifications/Improvements

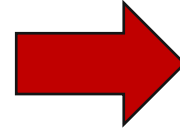
Budget Period 1 – Ensure maximum up-time at UK-CAER (max data collection)

Converted 2x existing modules:

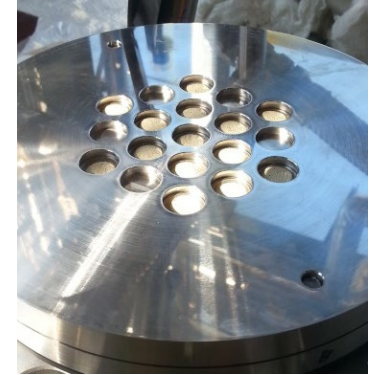
- ~6.5 m² each
- Only need to replace damaged cartridge
- Faster replacement than repairing the 4-inch bundle



4-inch



19x modular



Installed 2x new modules:

- ~4 m² each
- Faster module swapping than converted modules
- Reduce gas bypass
- Designed to allow sweep gas



2x-new modules



19x modular

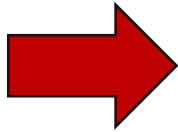


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Fiber Spinning and Potting

Budget Period 1 & 2

Spin 150 km of fibers (BP-1)

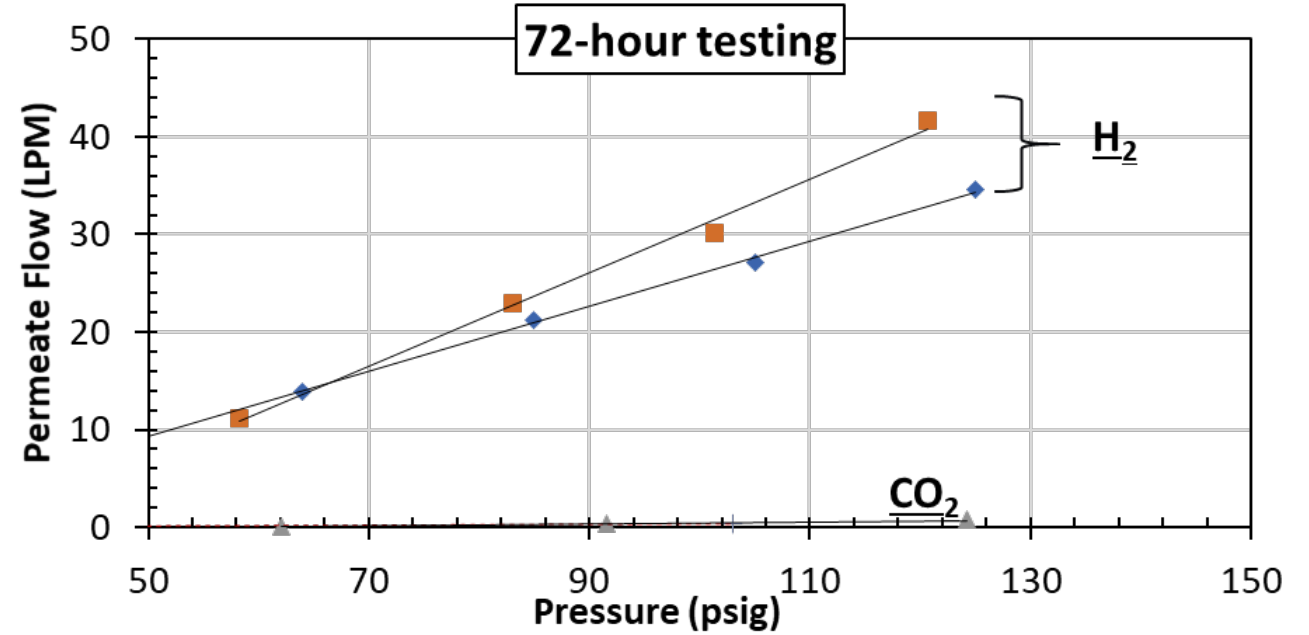
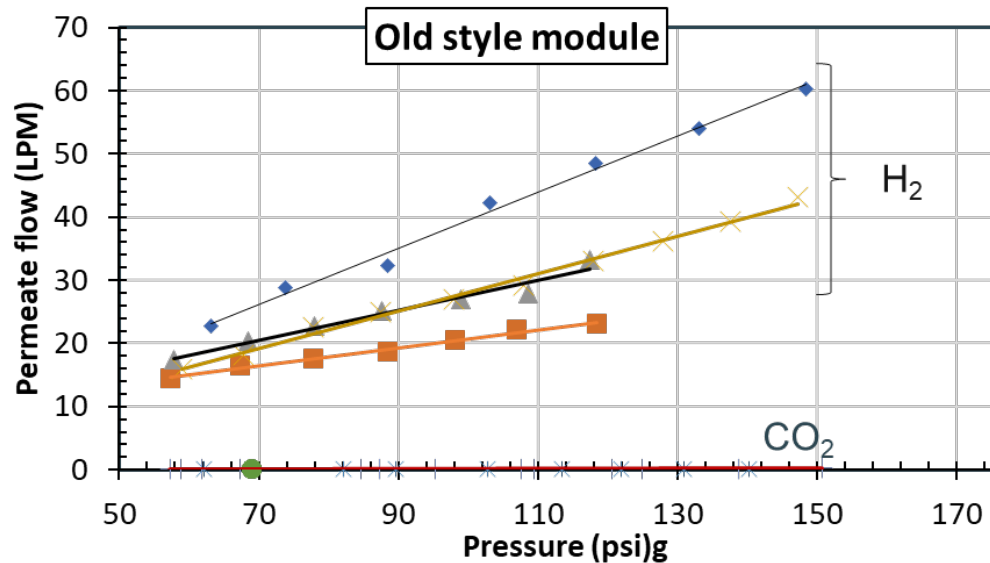
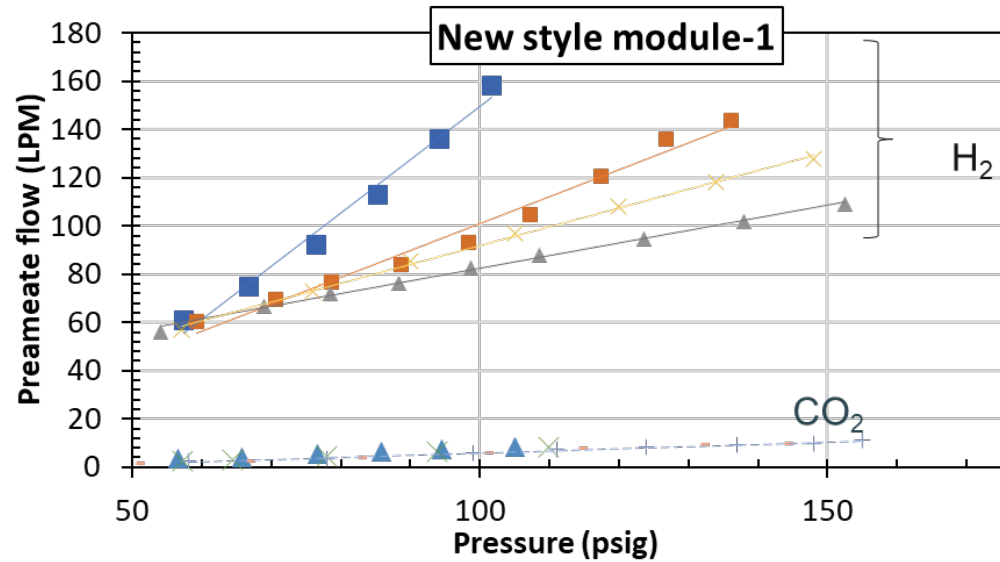


Potted 160+ cartridges (old + new style), BP-1&2



Skid Acceptance Testing

Budget Period 2



Performance meets expectations:

- Selectivity: 19 – 50
- GPUs: 130 (150 °C)
- Up to 72 hours of testing

Skid Acceptance Testing

Budget Period 2

Summary:

- Over 150 hours of Skid testing at SRI
- Over 150 membrane cartridges tested in skid (last step of QC)
- Longer testing up to 72 hours
- Selectivity: 19 – 50
- GPUs: 130 (150 °C)



Fiber Skid Shipped and Installed at UK CAER

Budget Period 2

Shipped to UK CAER July 2021



Fiber Skid Shipped and Installed at UK CAER

Budget Period 2

Installed at UK CAER July 2021



Gas lines going from CAER facility into Container



Skid inside Container



Gas lines going into Skid Container

UK-CAER Pilot Facility

Gasification Unit

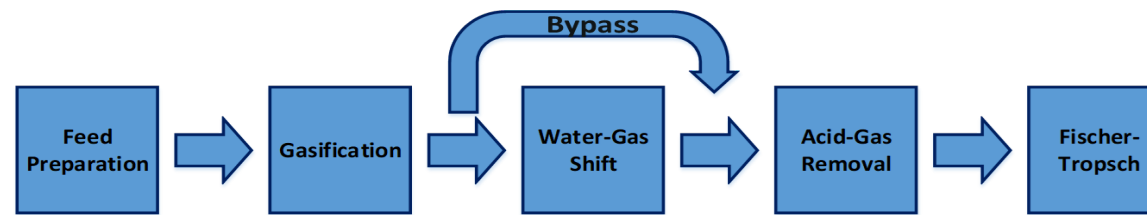
- Multi-burner, entrained flow, oxygen blown, slagging type
- 1 ton/day coal consumption
- Syngas production rate: $\sim 80 \text{ m}^3/\text{hr}$
- H_2/CO : $\sim .80$

Water-Gas Shift

- Packed bed
- Sulfur tolerant sour shift catalyst
- H_2/CO : up to 11/1

Syngas Compressor

- Metal Diaphragm Compressor
- 450 psi max outlet pressure



Gasifier



WGS



Compressor



Gasifier Operating Parameters	
Temperature ($^{\circ}\text{C}$)	1350
Pressure (MPag)	0.1
CWS Solid (%)	53.0
Syngas (vol%)	
H_2	24.51
N_2	2.93
CO	28.94
CO_2	40.89
H_2O	2.54
H_2S	0.18
COS	0.02

Test Plan and Schedule

Budget Period 2

Parametric matrix

Parameter	Range/Value	Unit
Temperature	80 - 225	°C
Pressure	50 - 200	psig
Gas Composition	Variable	
Stage Cut	0.2 – 0.7	
H ₂ in syngas	40-45	vol%
CO ₂ in syngas	40-42	vol%

Testing Schedule: Starting September 7th, 2021

Week #	Days/week	Hours/day	Total Hours
1	5	10	50
2	5	10	50
3	Test Data Analysis		
4	5	10	50
5	5	10	50
6	Test Data Analysis		
7	5	10	50
8	5	10	50
9	Test Data Analysis		

Future Work

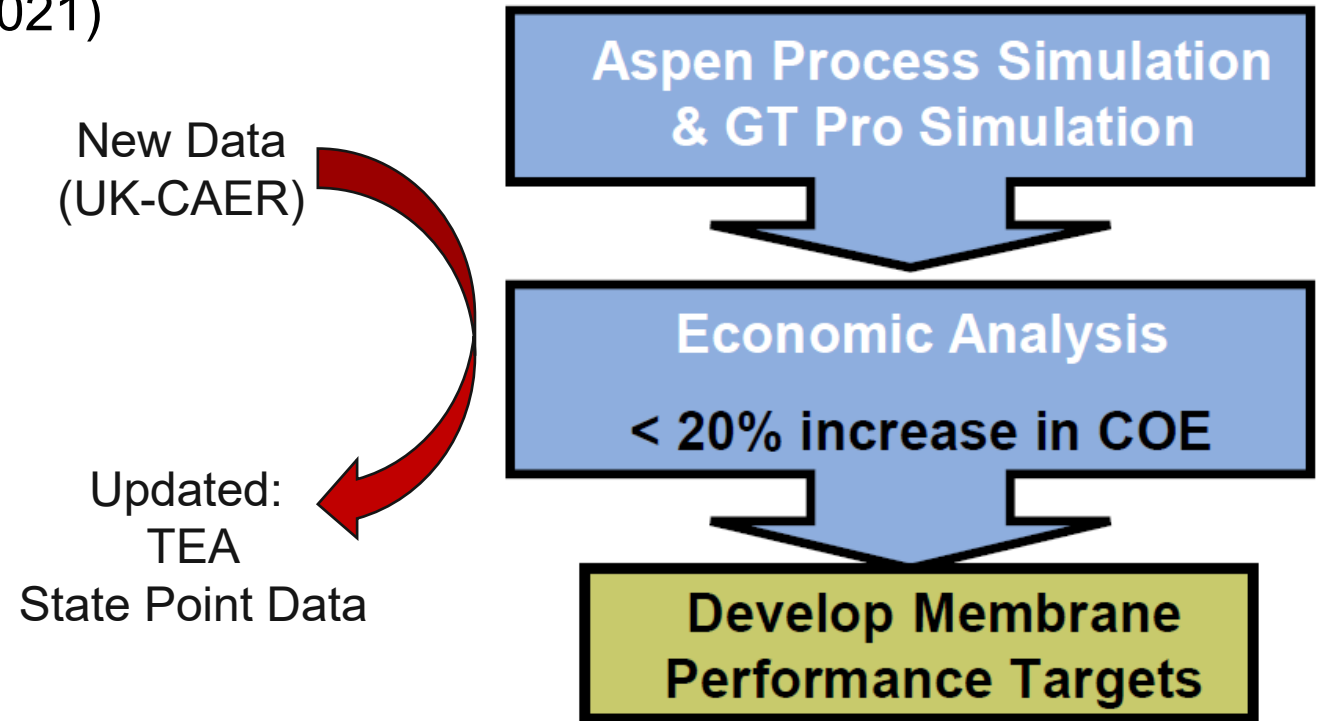
Budget Period 2 Final Tasks

1. UK-CAER:

- 6-weeks of Testing (start date 09-07-2021)
- Generate high fidelity data

2. Post UK-CAER:

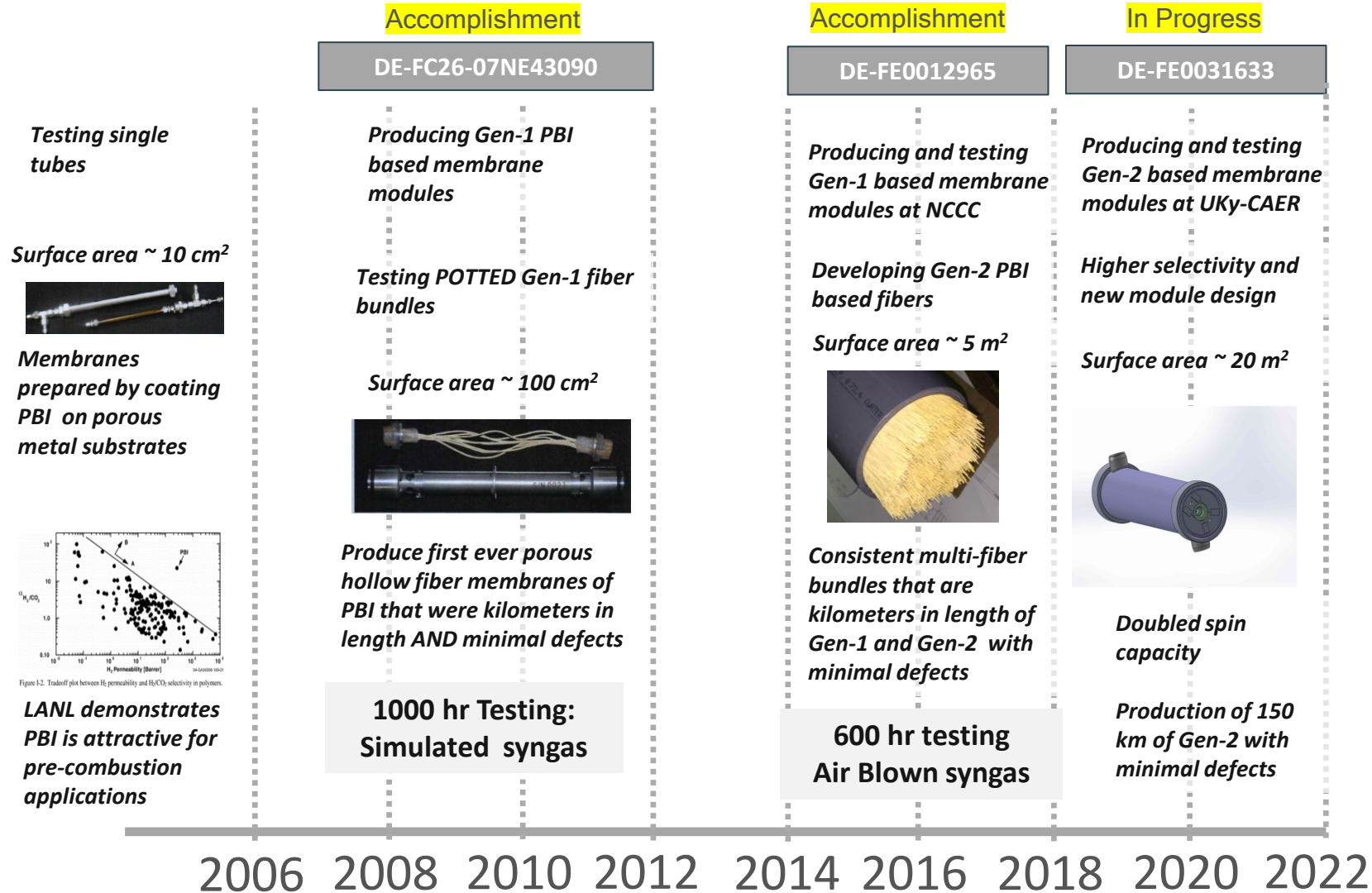
- Update Techno-Economic Analysis
- Technology Gap
- Technology Maturation Plan
- State Point Data Table



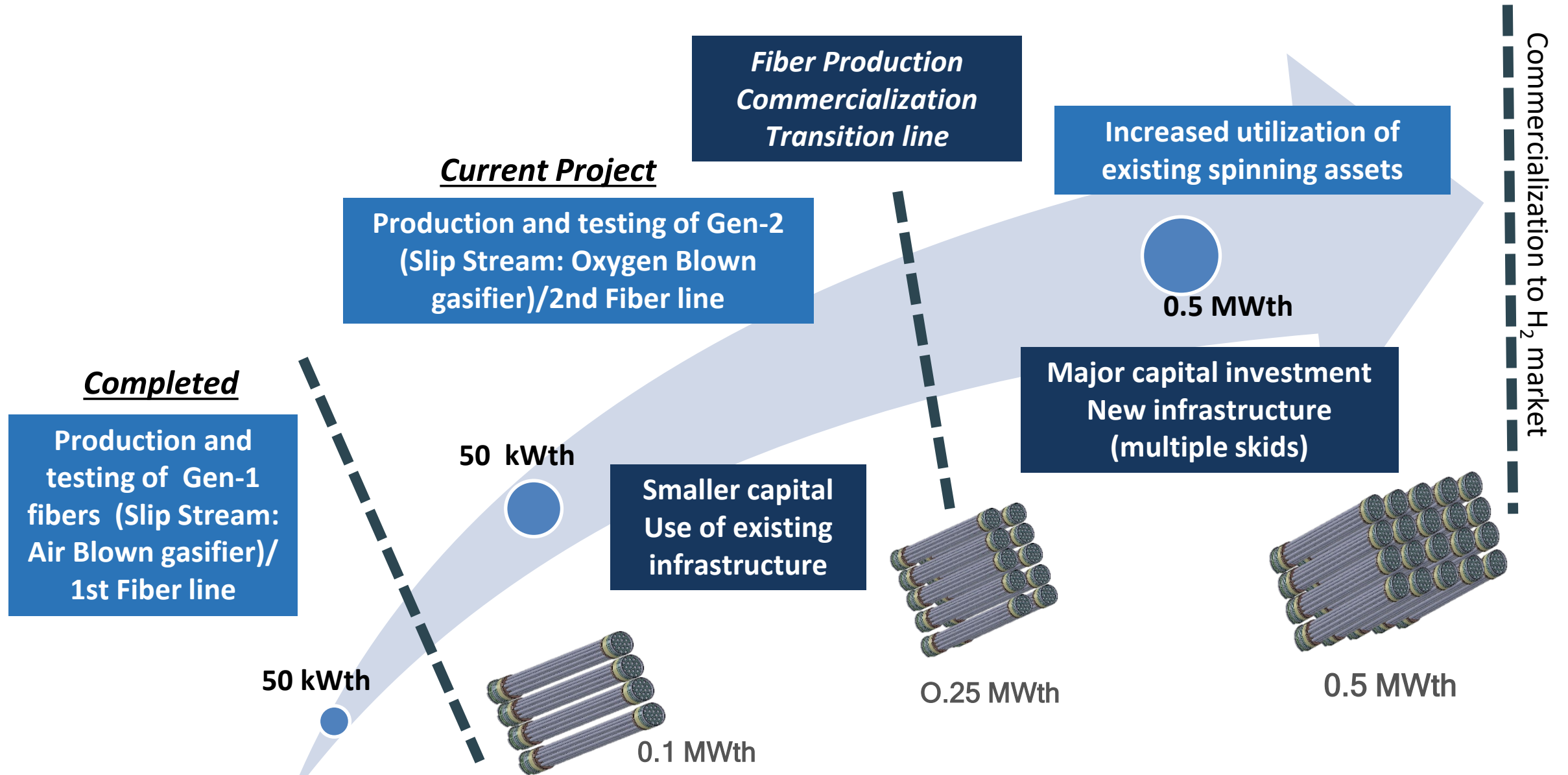
Technology Maturation

DOE Funding Critical to Technology Maturation

DOE enabled “first-of a kind” hollow fiber membranes of PBI in kilometer lengths



Roadmap to Small and Large Pilot Scale



Acknowledgements

- **Krista Hill, Andrew Jones, Jose Figueroa, Elaine Everitt, Lynn Brickett, and others at NETL**
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- **Kevin O'Brien (Energy Commercialization, LLC)**
- **Greg Copeland and Mike Gruender (PBI Performance Products)**
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- **John Jensvold and his team (Generon IGS)**
- **The staff at the NCCC**

Thank You

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