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NATIONAL LABORATORY

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PARAMETRIC TESTING OF CO₂-BINDING ORGANIC LIQUIDS (CO₂BOLs) TO ENABLE INDUSTRY ADOPTION (FWP-76270)

[NETL/DOE Project Manager: Dustin Brown]

U.S. DEPARTMENT OF ENERGY
NATIONAL ENERGY TECHNOLOGY LABORATORY
CARBON MANAGEMENT AND NATURAL GAS & OIL RESEARCH PROJECT REVIEW MEETING
VIRTUAL MEETINGS AUGUST 2 THROUGH AUGUST 31, 2021

"This material is based upon work supported by the U.S. Department of Energy under Field Work Proposal FWP-76270."

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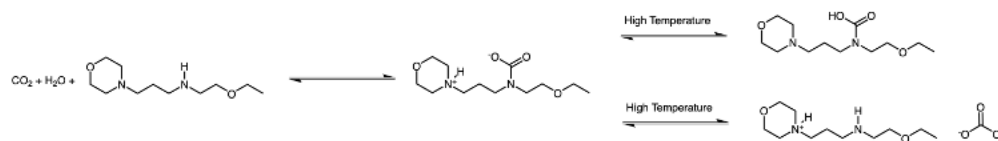
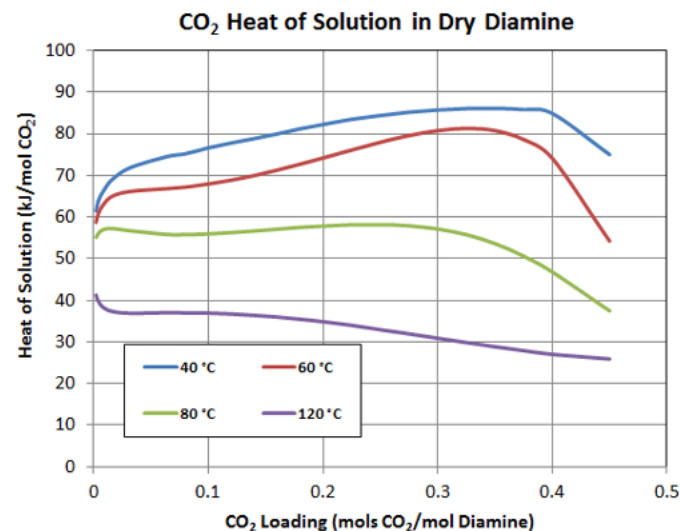
Engineering-Scale Test of a Water-Lean Solvent for Post-Combustion Capture

▶ DE-FE0031945

EEMPA can achieve low specific reboiler duties

The favorable thermal performance is attributable to

- The low water content (around 2 wt.% or less) meaning less water to vaporize
- A shift in the ionic character of the solvent with higher temperature, disfavoring the CO₂-bound ionic species
- SRDs down to 2.0 GJ/tonne have been observed in experiments. Cost-optimal designs for coal indicate 2.34 GJ/tonne is achievable.

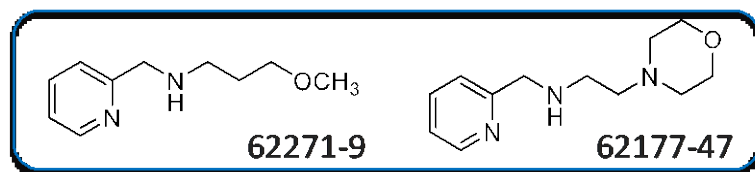


Project Overview

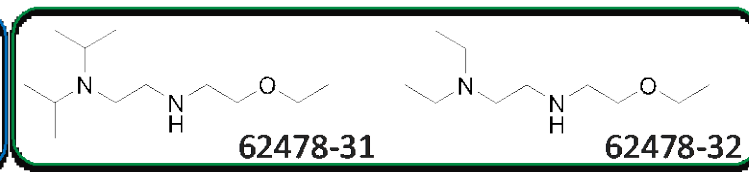
Project Period: 5/1/2020-2/28/2022

Funding: \$1,827,000

Aminopyridines



Diamines



Project Objectives:

- ▶ Provide critical data needed to project performance of three 3rd generation CO₂BOL single-component water-lean formulations (diamine, 2 aminopyridines)
- ▶ Measure essential physical and thermodynamic properties and demonstrate >90% capture of CO₂ on simulated flue gas for 40+ hours in steady-state operation
- ▶ Assess chemical durability of 3rd Generation CO₂BOL diamines and aminopyridines on simulated flue gas.
- ▶ Prime viable solvents for slip-stream testing and engage industrial partners for industry handoff.



Project Milestones

Completed dates underlined.

No.	BP	Task/ Subtask	Milestone Description	Initial Planned Completion
M1.1	1	1	Updated Project Management Plan.	<u>6/1/2020</u> (completed)
M1.2	1	1	Go-No Go Presentation at NETL.	<u>2/28/2021</u>
M1.3	1	1	Delivery of final report to NETL	<u>1/31/2022</u>
M2.1	1	2	3-5L EEDIDA synthesized for testing. Synthetic costs of ~\$10/kg of compound.	9/30/2020 (completed)
M3.1	1	3	EEDIDA kinetics and VLE measured. k'g values comparable to MEA, VLE confirms heat of solution between -75 to -85 kJ/mol (enabling 90% capture).	<u>1/31/2021</u>
M4.1	1	4	Continuous Flow Testing on EEDIDA completed. At least 40 hours of steady state 90% capture from simulated flue gas (15% CO ₂ , 85 % N ₂ with SO _x , NO _x , O ₂) with and without PSAR.	<u>2/28/2021</u>
M4.2	1	4	Final TEA of EEDIDA completed with costs targets at or below \$40/tonne CO ₂	<u>2/28/2021</u>

Success Criteria- BP1

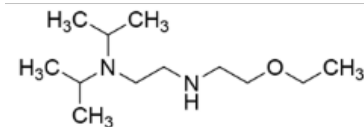
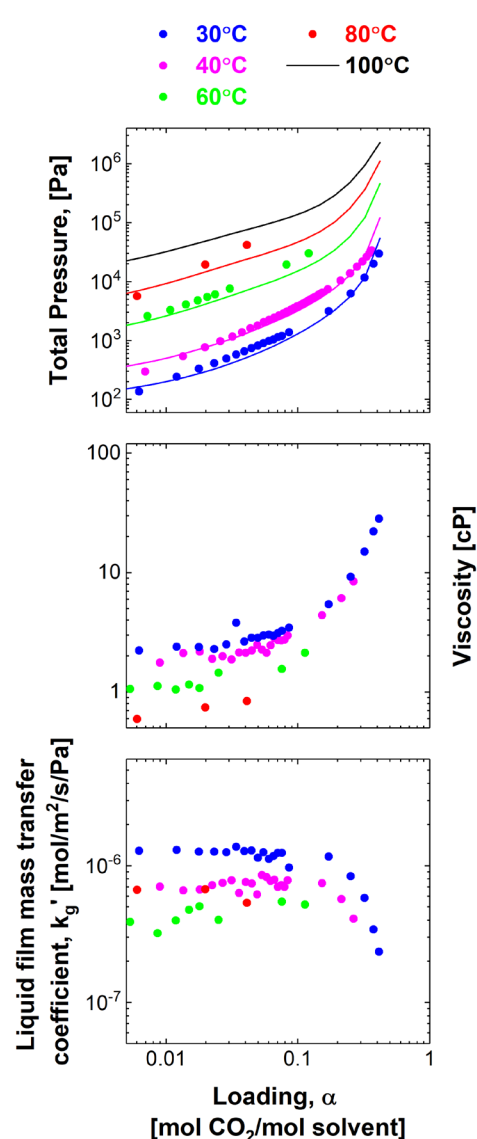
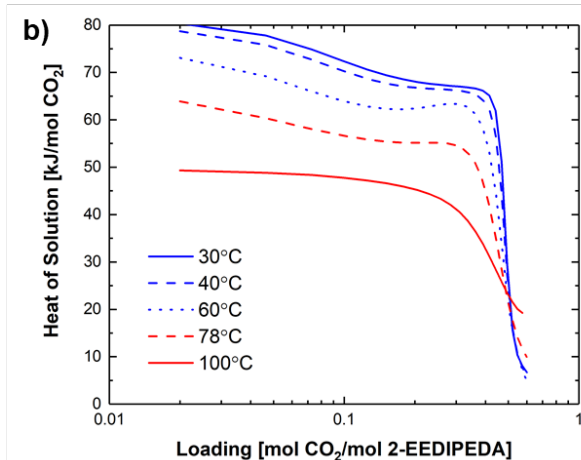
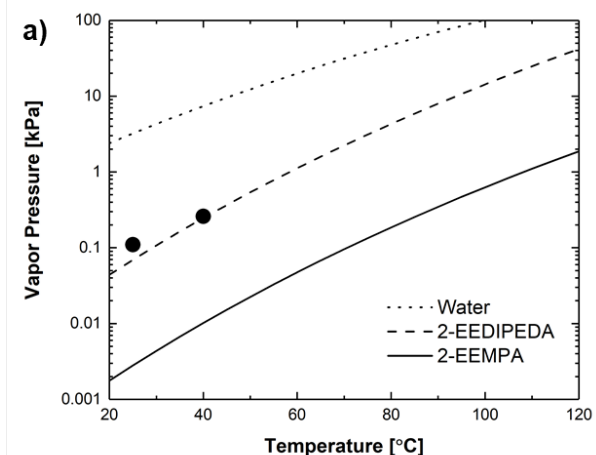
All criteria for BP1 were met by 2/28/2021.

Date	Success Criteria
2/28/2021	Projected reboiler duty for EEDIDA in a simple stripper configuration is <2.0 GJ/tonne CO ₂ or lower.
2/28/2021	Total costs of capture for EEDIDA are <\$50/tonne CO ₂ , with potential to meet DOE's \$40/tonne target in future efforts.
2/28/2021	Two new potential commercialization partners have been engaged to potentially partner on subsequent scale-up testing.



Physical Property Measurements

2-EEDIDA is comparable to 2-EEMPA, with lower viscosity and higher selectivity.

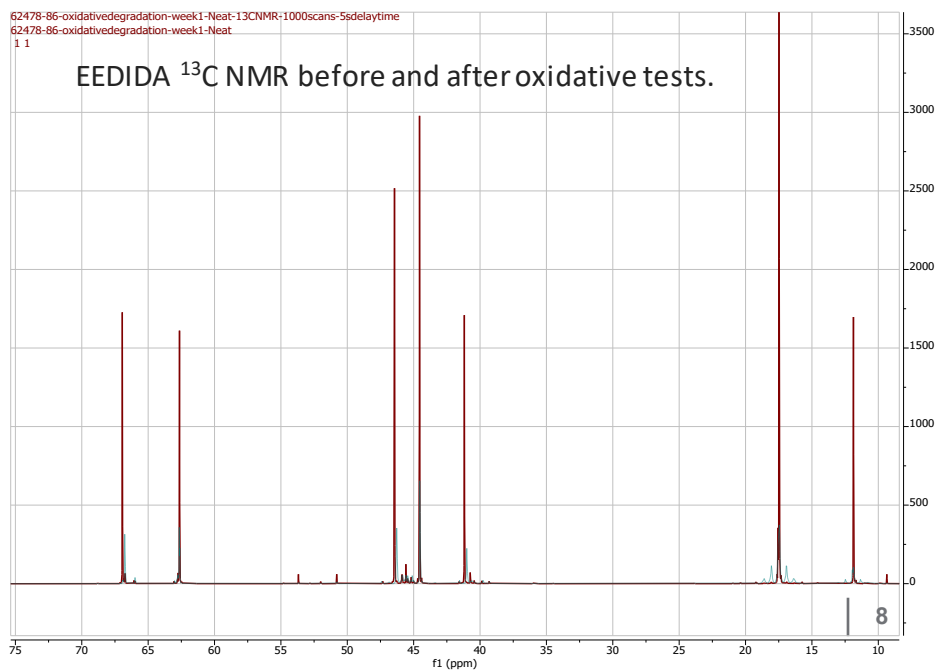
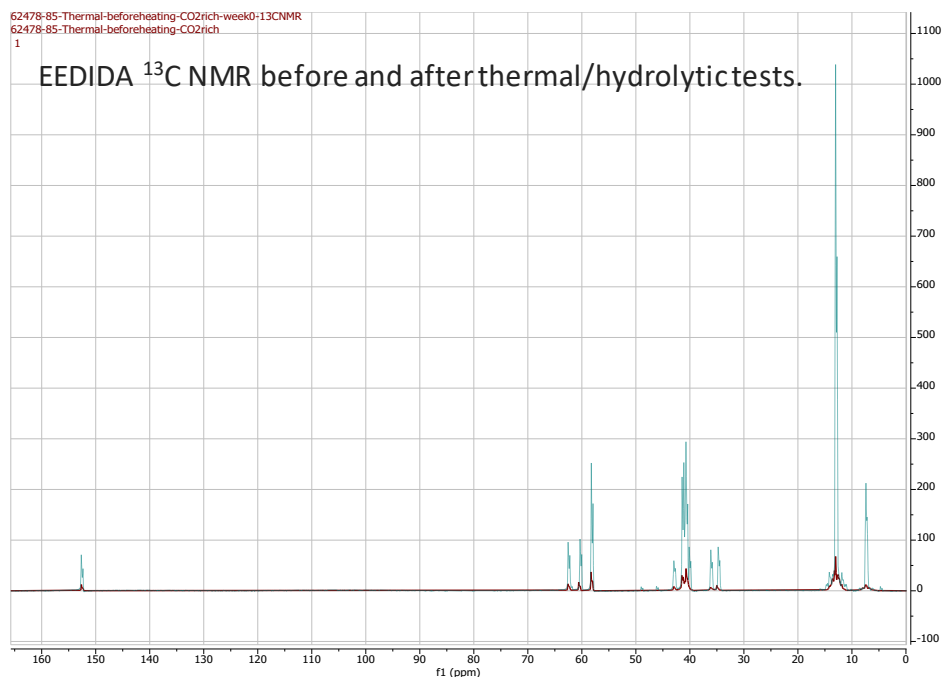




Chemical Durability Testing

2-EEDIDA is durable under absorber and stripper conditions, comparable to 2-EEMPA.

- ▶ Hydrolysis tests at simulated stripper conditions: 5-weeks, 117°C, 5 wt% water, CO₂ saturated, in tubular reactors with periodic sample analysis.
- ▶ Oxidative degradation tests at simulated absorber conditions: 0.5 mol-CO₂/mol in autoclave, 55°C, 2% CO₂/air mixture gas, 3 weeks, with periodic liquid analysis.
- ▶ ¹³C NMR, LC/MS and MS analysis suggests negligible degradation



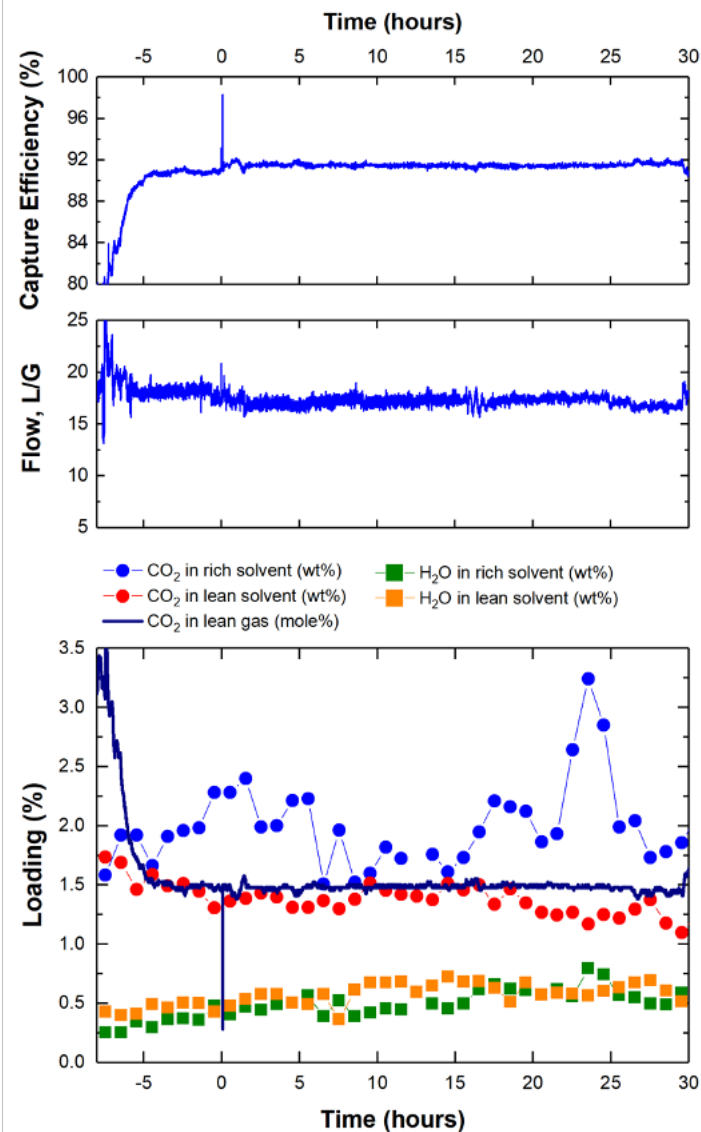
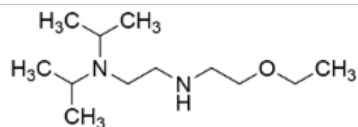


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Lab-Scale Testing on Simulated Flue Gas

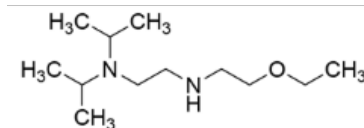
2-EEDIDA achieved 40 hours steady-state CO₂ capture with no foaming, aerosols or LLE.





Techno-Economic Analysis

2-EEDIDA is projected to be 20% cheaper than B12B Baseline, and \$1.1/tonne cheaper than 2-EEMPA.*

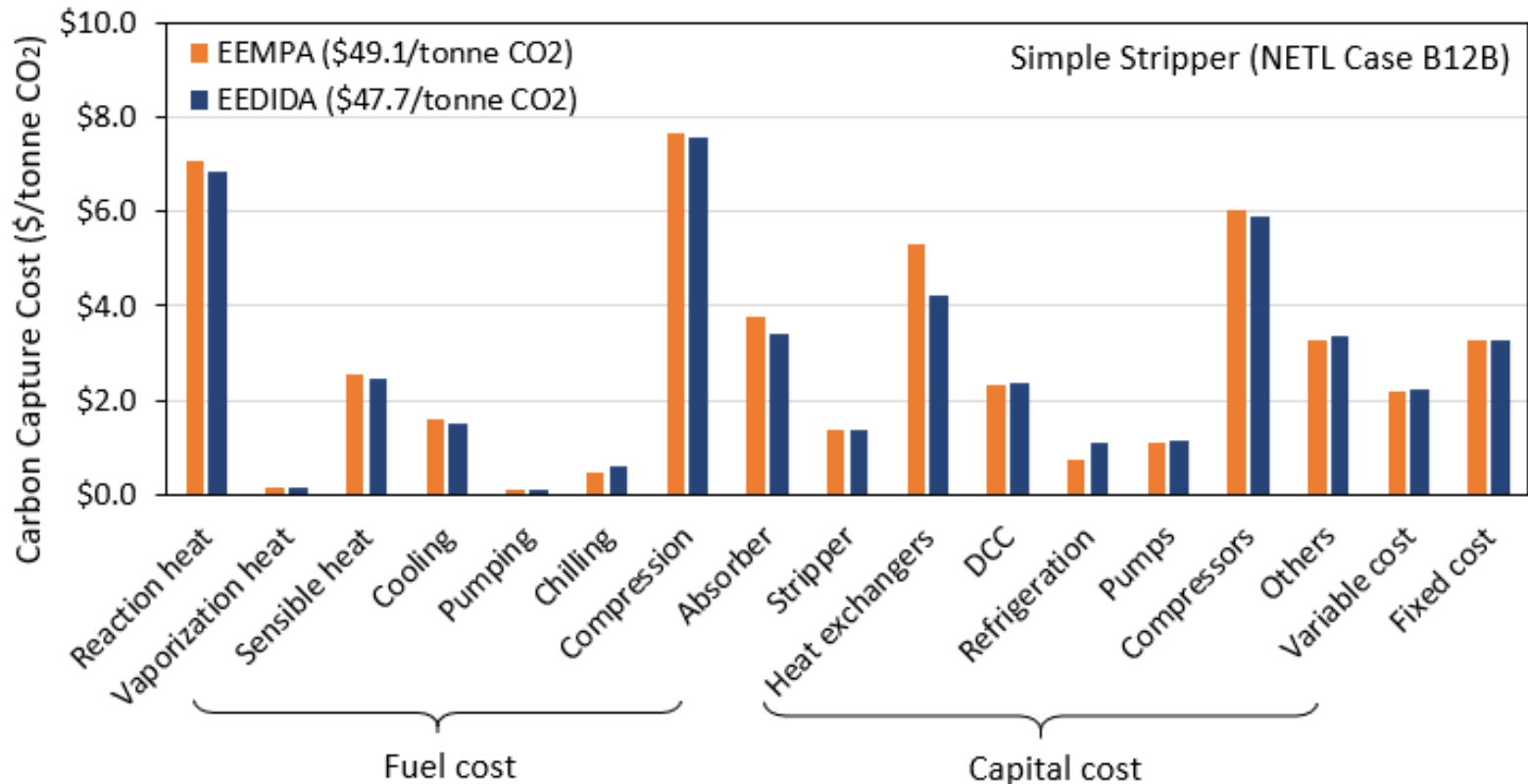
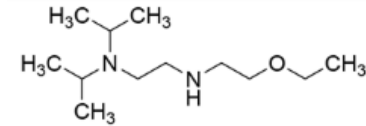


Variable	MEA	Cansolv	2-EEMPA		2-EEDIDA	
NETL Reference	Case 12	Case B12B	Case B12B		Case B12B	
Configuration	SS	LVC	SS	TSF	SS	TSF
Lean Loading [mol CO ₂ / mol solvent]	0.27	-	0.113	0.113	0.113	0.113
Rich Loading [mol CO ₂ /mol solvent]	0.50			0.328	0.328	0.344
Water Loading [wt%]	70	-	1.6	1.6	1.7	1.7
Regeneration Temp [°C]	115	-	96	98	98	103
Regeneration Pressure [bar]		1.98	1.98	2.32	5.2/2.3	2.32
Reboiler Duty [GJ _e /tonne CO ₂]	3.55	2.48	2.35	2.36	2.22	2.30
Total Plant Cost [MM\$, 2011]	-	632	530	497	505	488
Cost of Capture [\$ /tonne CO ₂]	-	58.3	49.1	47.1	47.7	46.6

***All costs are in 2012 dollars using NETL REV3 pricing.**

Techno-Economic Comparison With 2-EEMPA

2-EEDIDA is \$1.4/tonne cheaper than 2-EEMPA due to lower viscosity and higher selectivity.



► Squeezing the lemon with respect to viscosity.

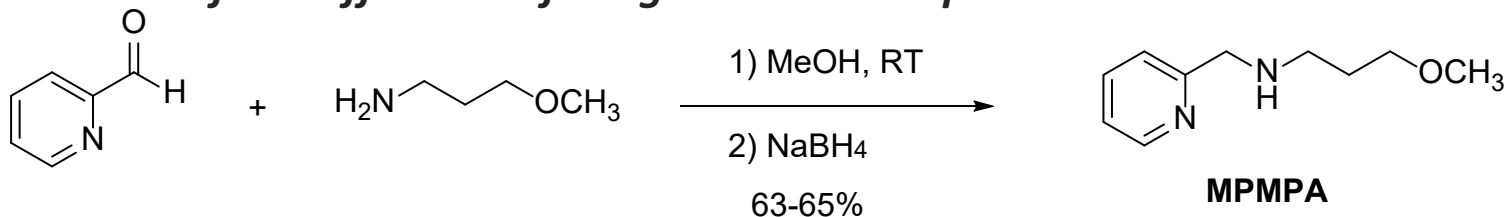


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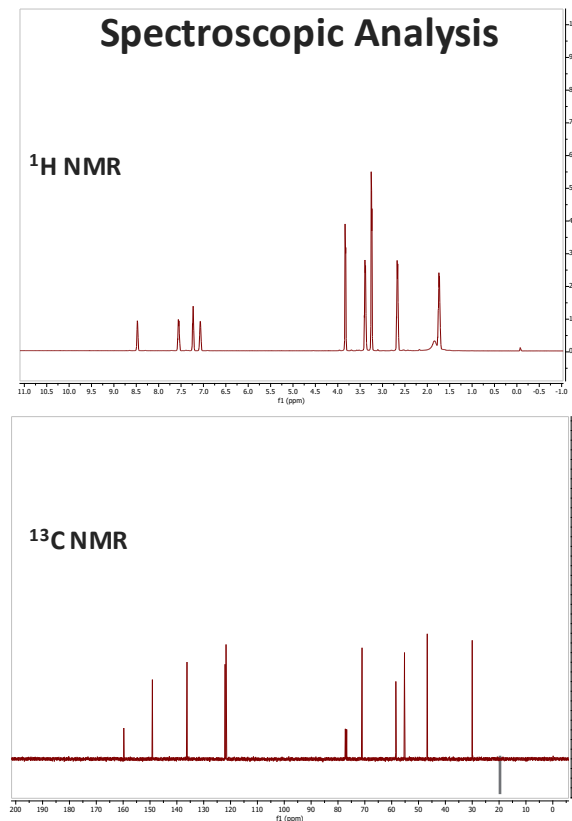
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Synthesis of MPMPA solvent

MPMPA is made from off the shelf-reagents in a 1-step condensation.

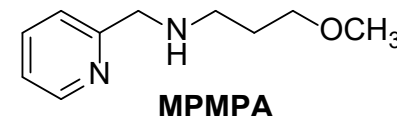


- ▶ Completed the synthesis of 3L of MPMPA solvent
- ▶ The estimated cost of MPMPA solvent production is ~ \$9/Kg
- ▶ MPMPA is stable up to 200 °C under vacuum distillation



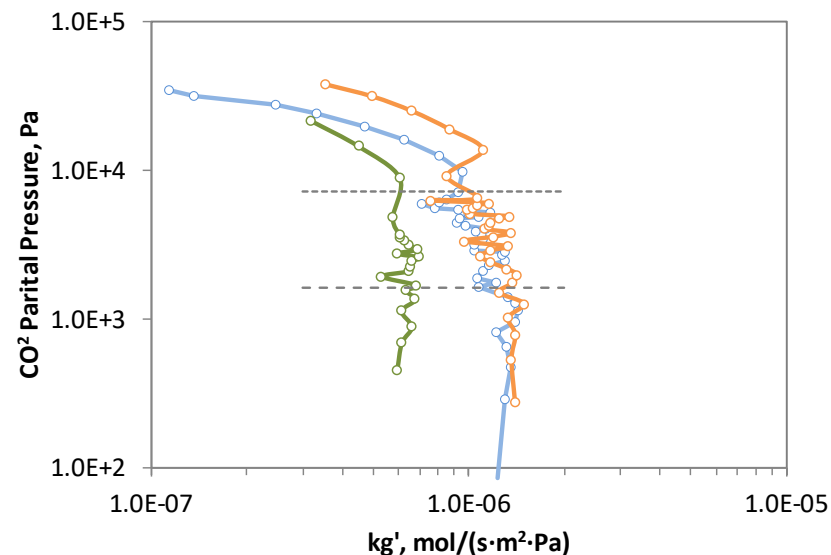
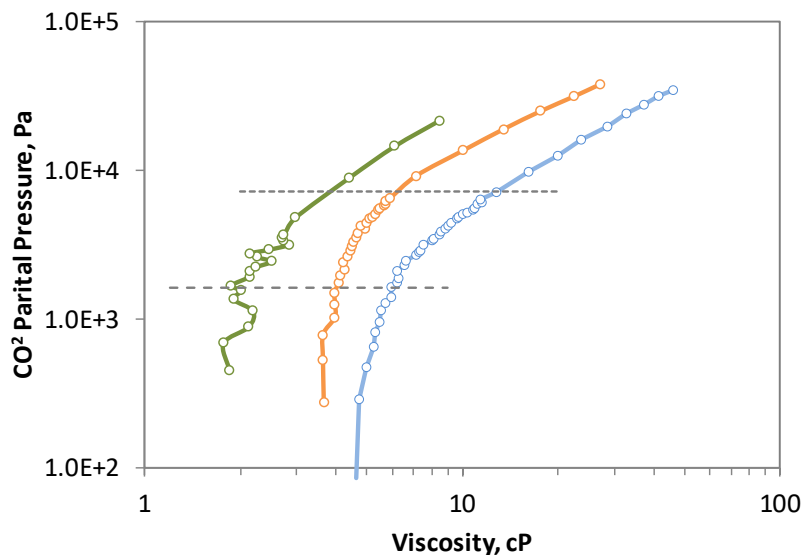
Physical Property Measurements

MPMPA has comparable properties to 2-EEMPA and 2-EEDIDA.



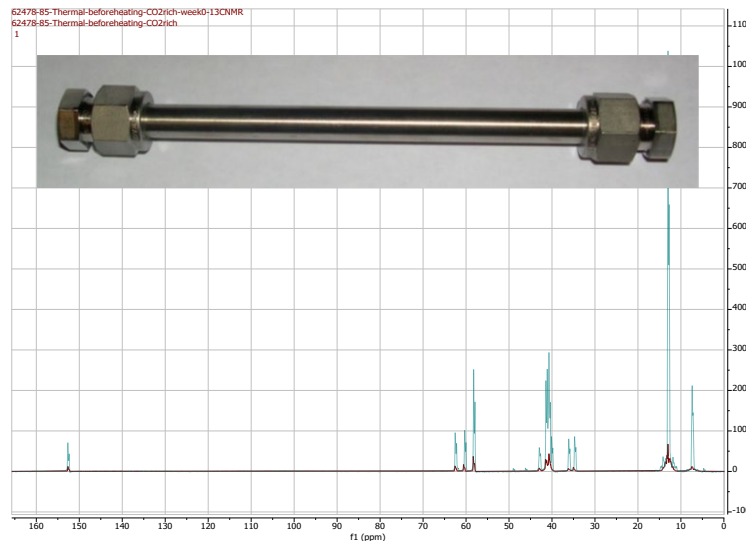
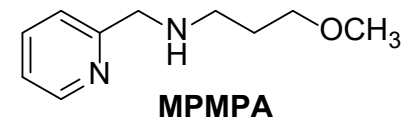
ΔH -71.6 to -78.0 kJ/mol

Vapor pressure <0.02 torr at 40 °C



Current and Future Work

MPMPA is set to undergo thermal and oxidative stability and testing on WWC and LCFS.





Project Schedule and Major Tasks – BP2

	BP-1					BP2																
	FY20					FY21										FY22						
	M	J	J	A	S	O	N	D	J	F	M	A	M	J	J	A	S	O	N	D	J	F
Budget Period 2 (BP2)																						
1b. Project Management																						
5. Solvent Scale-up (AP: 1)																						
5.1 Develop solvent synthesis methodology with scale-up projections																						
5.2 Initial solvent scale-up production																						
5.3 Solvent physical property measurements (e.g. VP, flash point, density)																						
5.4 Solvent durability and chemical degradation assessment																						
6. Solvent Testing (AP: 1)																						
6.1 Vapor-liquid equilibrium, viscosity and other properties																						
6.2 Wetted-wall kinetics testing																						
6.3 Preliminary TEA																						
7. Laboratory Continuous Flow System Testing (AP: 1)																						
7.1 Parametric testing																						
7.2 Long duration testing on realistic flue gas																						
7.3 Data analysis and reporting																						
7.4 Final TEA																						
8. Solvent Scale-up (AP: 2)																						
8.1 Develop solvent synthesis methodology with scale-up projections																						
8.2 Initial solvent scale-up production																						
8.3 Solvent physical property measurements (e.g. VP, flash point, density)																						
8.4 Solvent durability and chemical degradation assessment																						
9. Solvent Testing (AP: 2)																						
9.1 Vapor-liquid equilibrium, viscosity and other properties																						
9.2 Wetted-wall kinetics testing																						
9.3 Preliminary TEA																						
10. Laboratory Continuous Flow System Testing (AP: 2)																						
10.1 Parametric testing																						
10.2 Long duration testing on realistic flue gas																						
10.3 Data analysis and reporting																						
10.4 Final TEA																						
Total - BP2																						

Conclusions and Future Work

Key Findings:

- ▶ 2-EEDIDA is a viable solvent for post-combustion capture
 - 20% cheaper than Case 12B baseline (CANSOLV)
 - \$1.4/tonne CO₂ cheaper than 2-EEMPA
 - Chemically durable

- ▶ MPMPA preliminary analysis suggests comparable properties as 2-EEMPA and 2-EEDIDA

Upcoming efforts:

- ▶ Full kinetics and continuous flow testing for MPMPA on simulated flue gas

- ▶ Update all pricing and TEA to REV4 (2018 \$)

Acknowledgements



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Greg Whyatt



Andy Zwoster

Parametric Testing
and Analysis
Process Modeling



David Heldebrant



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Deepika Malhotra



Kat Grubel

Solvent Design
Synthesis & Scaleup
Chemical Durability