



ROTA-CAPtm: An Intensified Carbon Capture System Using Rotating Packed Beds

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Virtual Meetings August 2 through August 31, 2021

Outline

- **Project Overview**
- **Technology Background**
- **Technical Approach Discussion**
- **Progress and Current Status**
- **Summary**

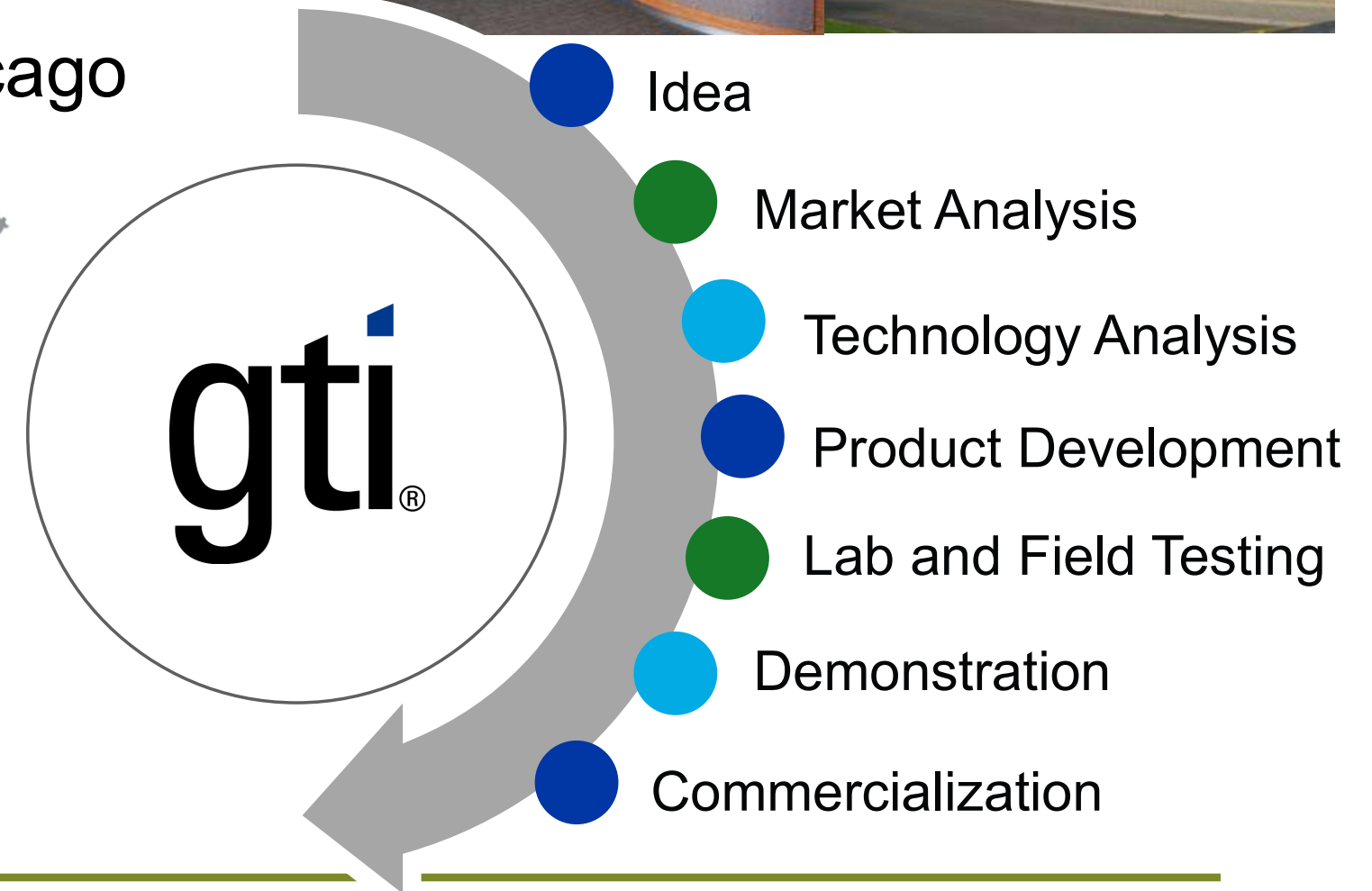
79-year History of Turning Raw Technology into Practical Energy Solutions



World-class piloting facilities headquartered in Chicago area

Introduction to GTI

- Research organization, providing energy and environmental solutions to the government and industry since 1941
- Facilities: 18 acre campus near Chicago



Project Overview

ROTA-CAPtm: An Intensified Carbon Capture System Using Rotating Packed Beds

- **Sponsor**



DE-FE0031630

- **Funding**: \$2,784,222 DOE (\$743,000 co-funding), Duration 42 months
- **Objective**: The objective of this project is to develop and validate a transformational carbon capture technology—ROTA-CAPtm to meet DOE's cost target of $\leq \$30/\text{tonne CO}_2$, 90% capture rate, and product CO₂ purity target of $\geq 95\%$.

BP1: 10/1/2018 – 3/31/2021 BP2: 4/1/2021 – 3/31/2022

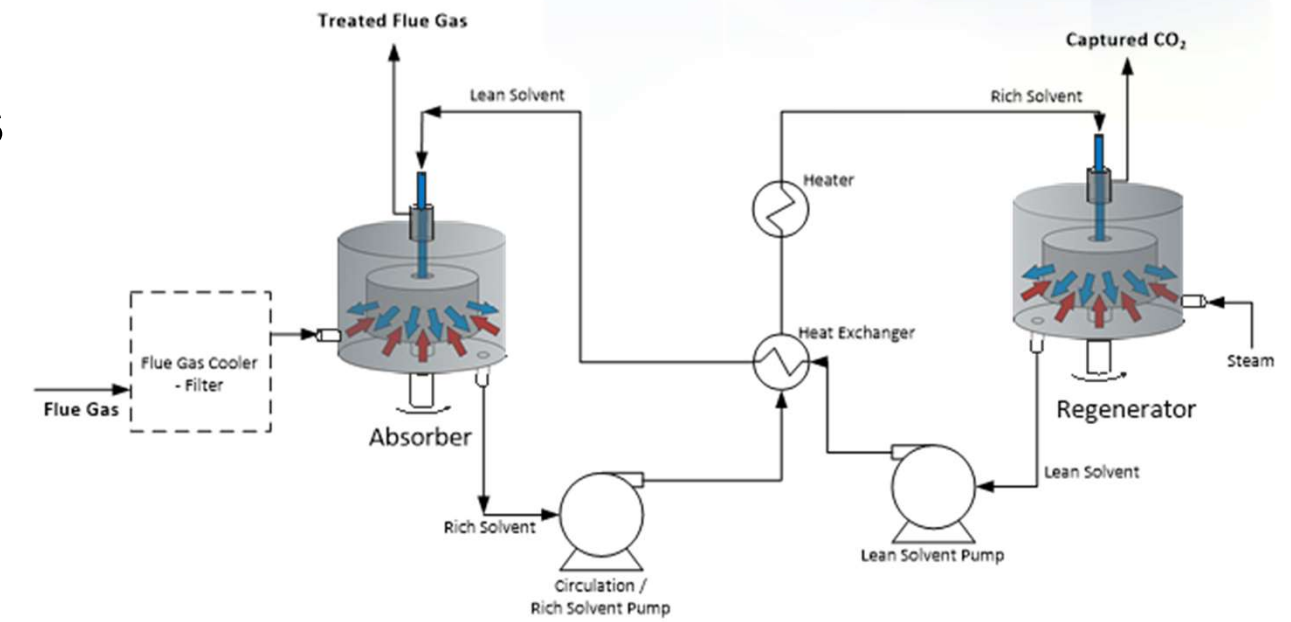
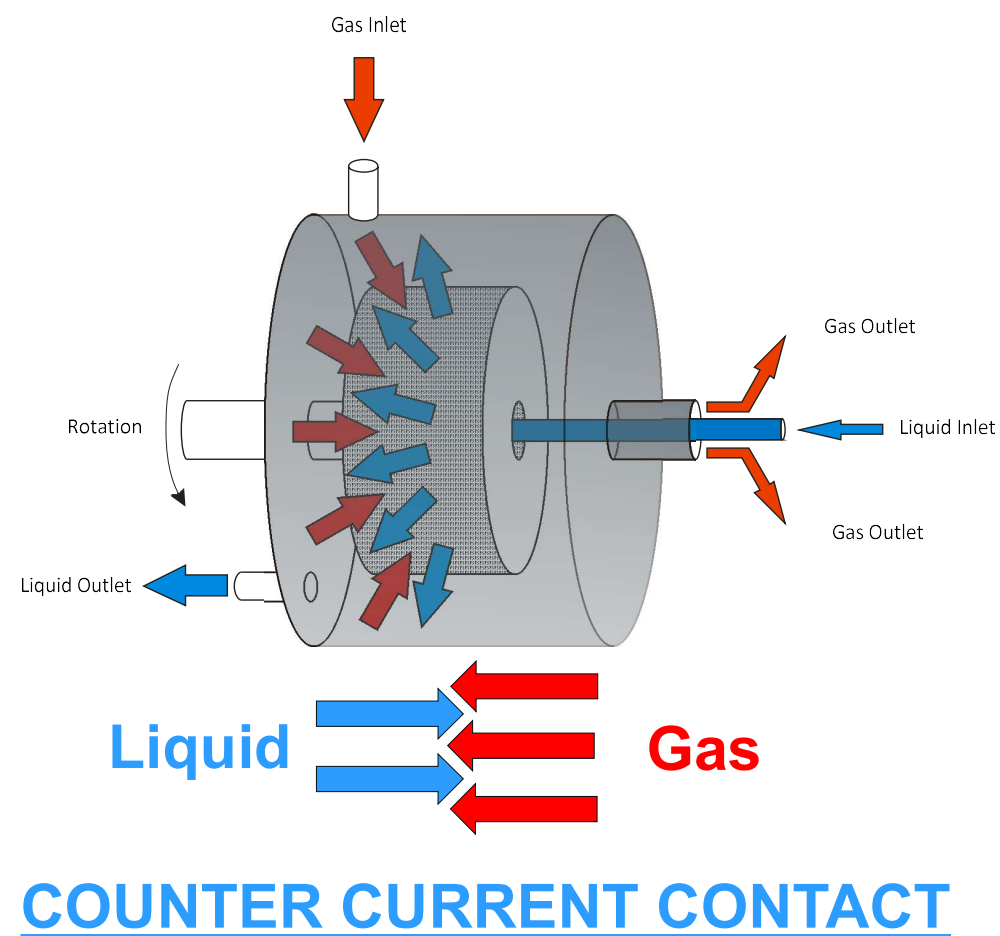
ROTA-CAPtm: DOE/NETL Project Objectives and Members

- Design, construct, test and model novel rotating packed bed (RPB) absorbers and regenerators
- Assess the performance of the integrated hardware and solvent under a range of operating conditions
- Test with simulated flue gas at GTI
- Long term test with real flue gas at the National Carbon Capture Center (NCCC)



ROTA-CAPtm: Process Intensification (PI) by Using Rotating Packed Bed Reactors to Replace Conventional Absorber and Regenerator

ROTA-CAPtm uses rotating packed bed (RPB) absorbers and regenerators for contacting flue gas with an advanced solvent such as Carbon Clean's CDRMax[®] for carbon capture



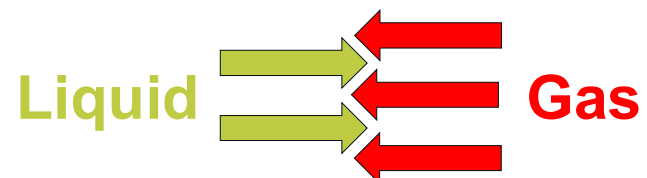
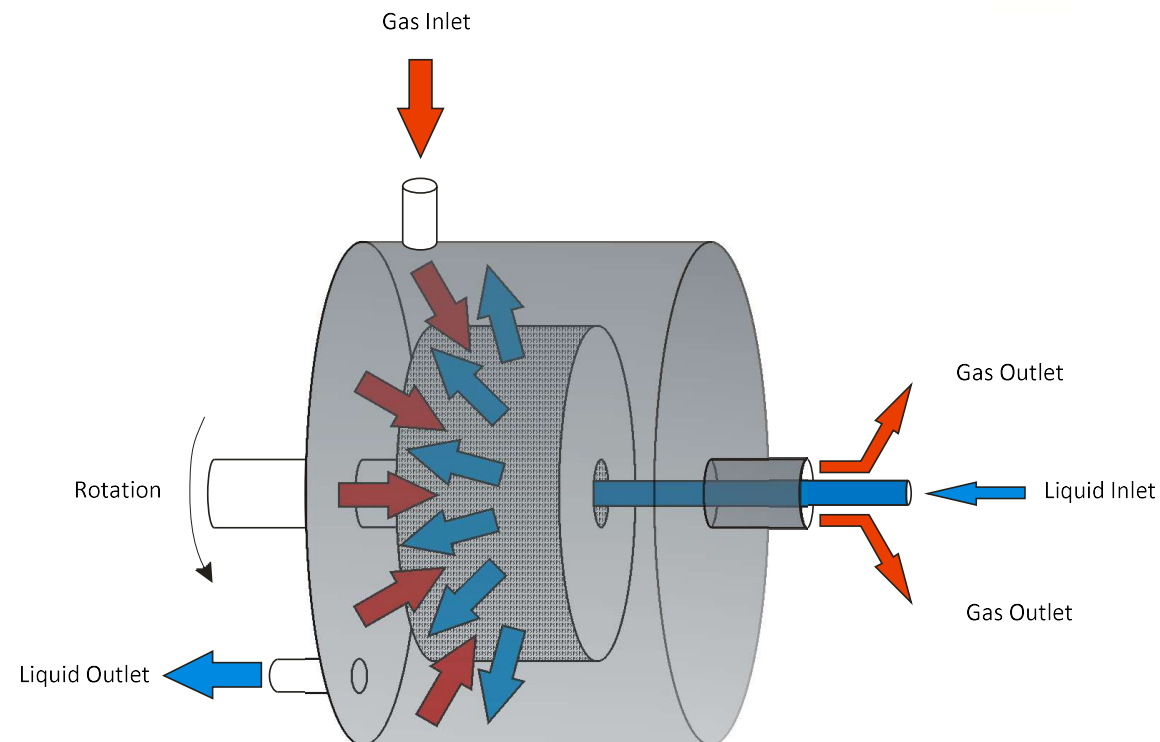
Simplified ROTA-CAPtm flow diagram



ROTA-CAPtm Absorber and Regenerator RPBs

Technology Background

RPB Absorber Background

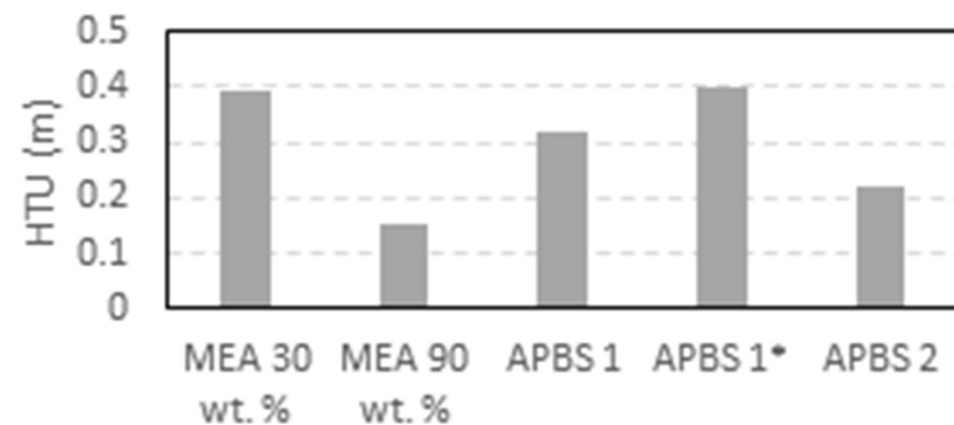


COUNTER CURRENT CONTACT

- Initial tests (UK) on laboratory prototype absorber performance measured mass transfer of CO₂ (12 vol.%) into 4 solvent systems.
- Counter current contact:
 - Solvent distributed from inner radius to outer radius under centrifugal force generated by rotation of the packed bed.
 - Gas flows from outer radius to inner radius of packed bed.
- Absorber tests measurements:
 - Inlet and outlet gas phase CO₂ concentrations
 - Inlet, outlet and sump solvent temperature
 - Gas and liquid flow rates
 - Speed of rotation

Solvent Background

- Intensified solvents have been developed to achieve higher CO₂ loadings than those used in conventional systems – these are more viscous than conventional solvents.
- Intensified solvents (MEA 90 wt.% and APBS 2) exhibited higher mass transfer rates (low HTU) than non-intensified solvents (MEA 30 wt.% and APBS 1).
- Simulation determined a conventional absorption process with 30 wt.% MEA requires packing height of 0.94 m to achieve equivalent mass transfer of CCSL's intensified solvent in RPB with 0.11 packing height – leading to close to 90% size reduction

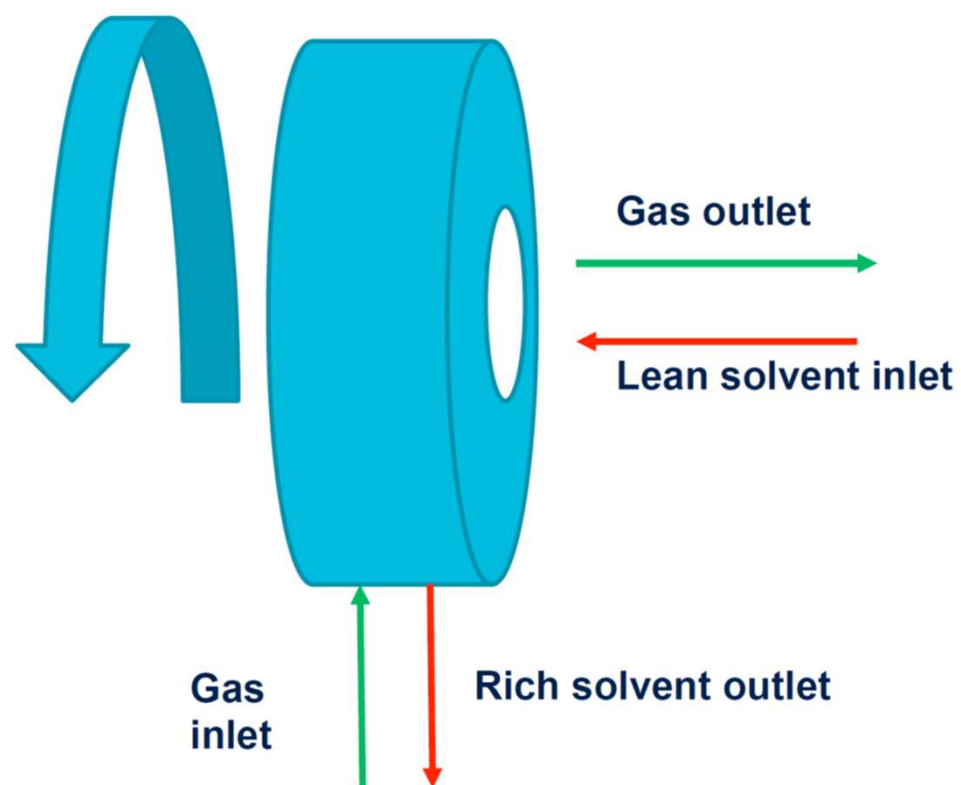


Solvent	30 wt.% MEA	APBS 2
Absorber Type	Static	RPB
CO ₂ in (mol.%)	12.0	12.0
CO ₂ out (mol.%)	7.2	7.2
Packing Height (m)	0.94	0.11
Relative Size Reduction	Base	8.5

ROTA-CAPtm

ROTA-CAP EQUIPMENT

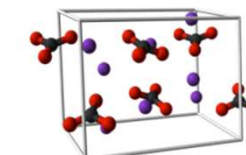
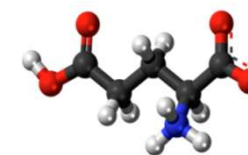
RPB equipment improves mass transfer leading to up to 90% volume reduction from a conventional static column.



INTENSIFIED SOLVENT

CCS's advanced solvents (Amine Promoted Buffer Solutions or APBS) remove CO₂ from a variety of gas streams – for use in new and existing industrial facilities.

SOLVENTS:
Fast reaction,
High energy

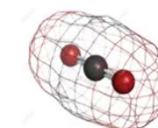
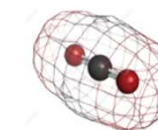


SALTS:
Slow Reaction,
Low energy

Advanced Solvents (APBS 1)

Intensified solvent leads to a reduction in energy and equipment size.

Intensified Solvents (APBS 2)

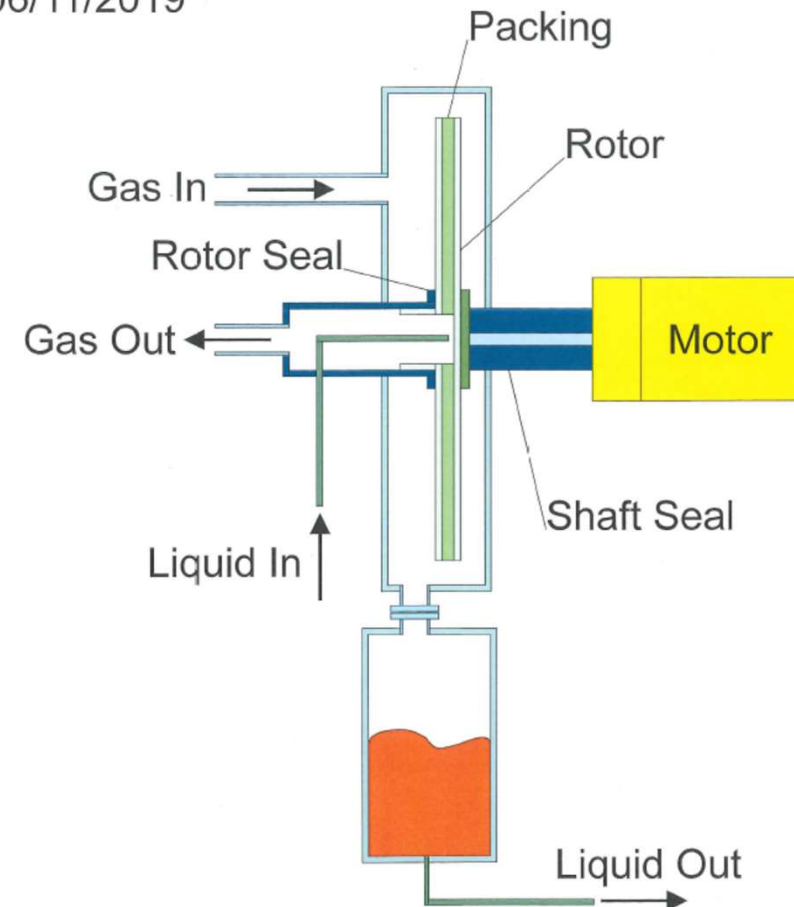


RPB equipment with intensified solvent will improve typical economics

ROTA-CAPtm: Rotating Packed Bed Design

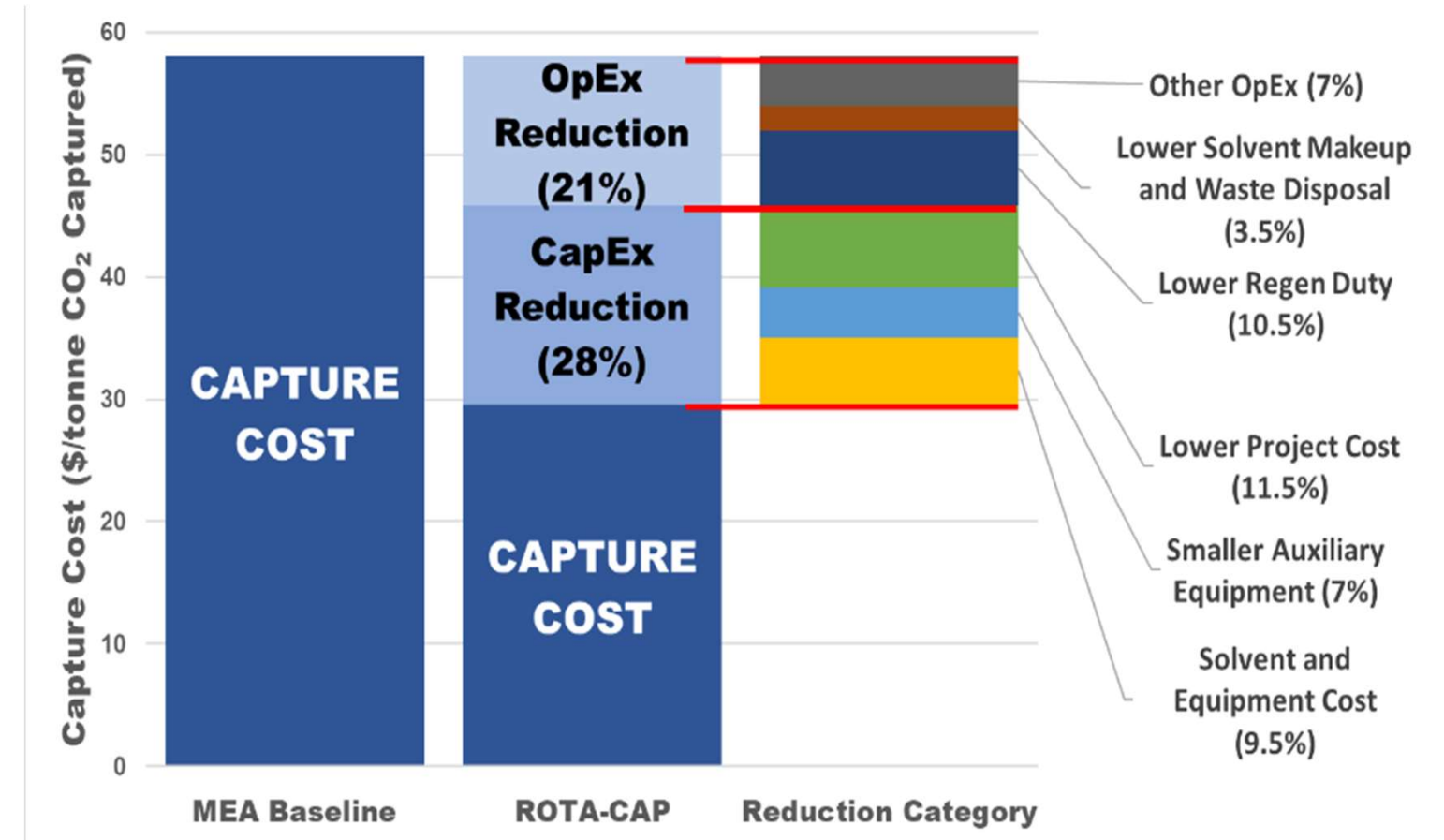
- GTI and its predecessor institutions GRI and IGT has experience on RPB process technology for natural gas dehydration and bulk acid gas removal process design and operation
- GTI Engineering Team reviewed mechanical requirements of the RPB sizing submitted by Carbon Clean.
- GTI prepared initial RPB design concept and mechanical design for rotating packed beds.
- Packing for RPB's are provided by Montz, Germany.

GTI-RPB
concept Rev. 1
06/11/2019



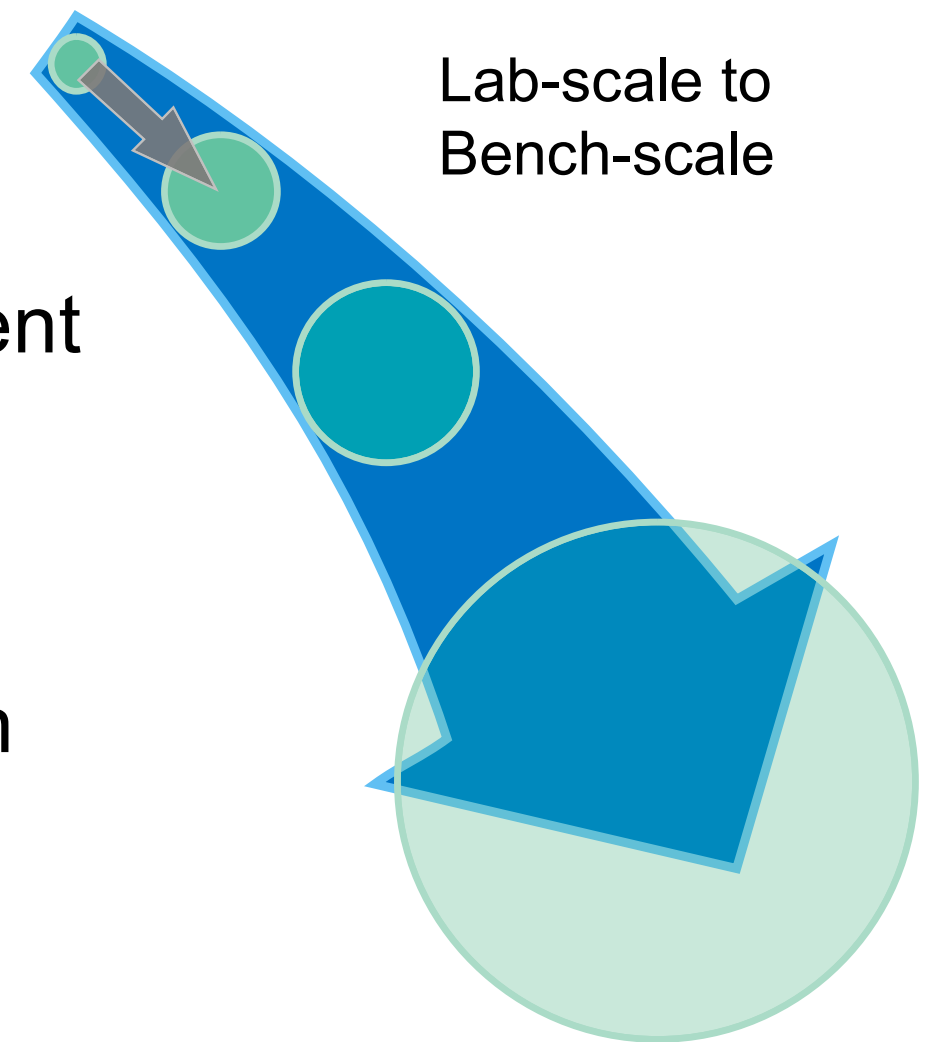
Advantages Over Traditional Processes

- RPB technology reduces the size and therefore cost of the absorber. RPB regenerator size reduction is comparable to that of an RPB absorber
- Lower circulation rate reduces sizing requirements of heat exchangers, pumps, and coolers by up to 50%
- Lower residence time of the solvent in the absorber and lower reboiler duty reduces oxidative and thermal degradation by up to 77%



Technical and Economic Challenges

- The integrated use of RPBs as both absorber and regenerator in a single system
- The mechanical design parameters of rotating equipment
- Solvent stability performance during operation
- Integrating and achieving required solvent regeneration using an RPB regenerator



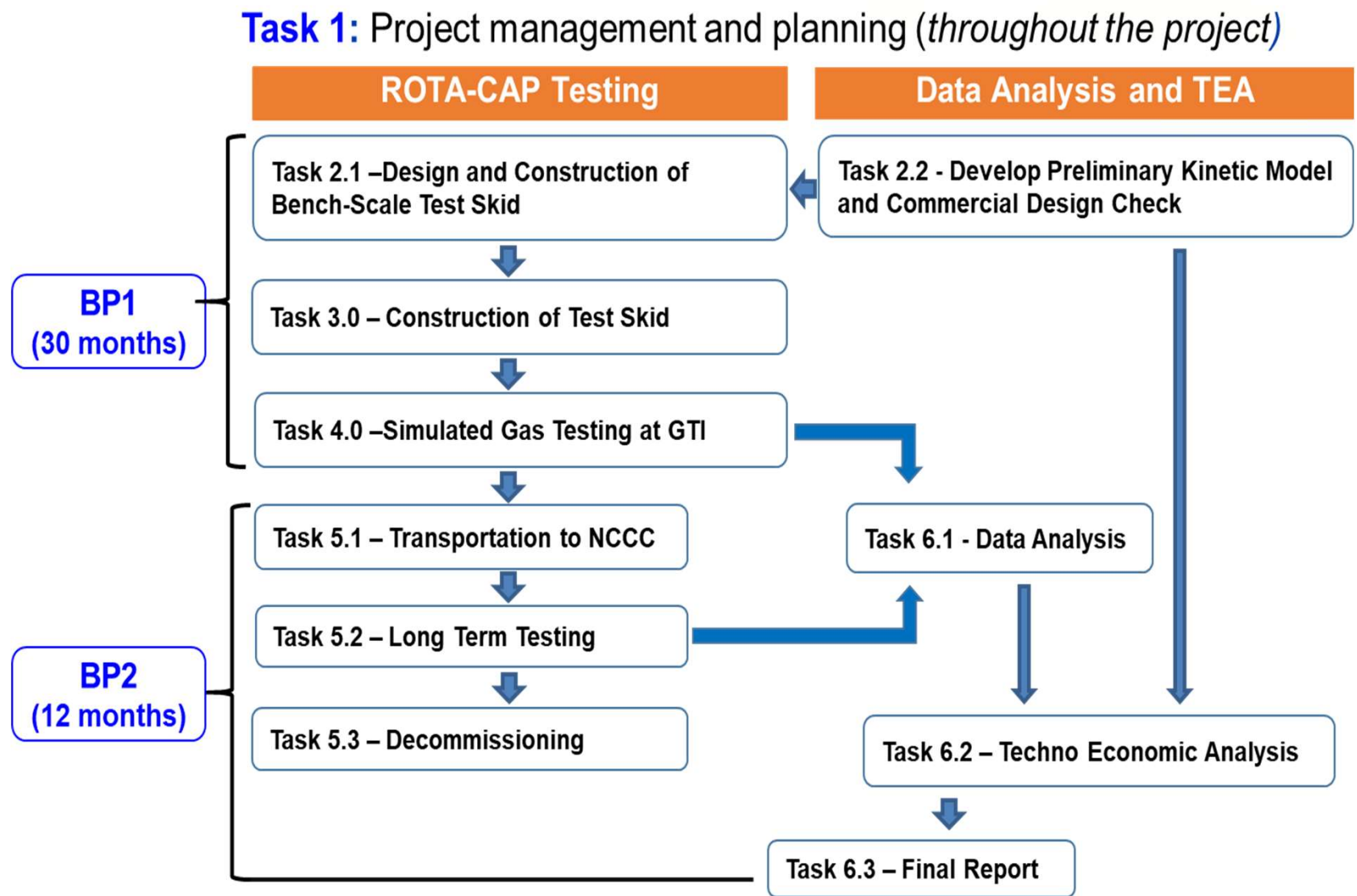
Technical Approach

Test Plan and Key Experimental Parameters

Parameter	Range
Rotational Speed	100–500 RPM
Absorber Liquid/Gas ratio	0.5–5.0 kg/m ³
Solvent Circulation Rate	30–150 kg/h
Solvent Concentration & Viscosity	35–70 wt.% & 5–80 cP
Regenerator Operating Pressure & Temperature	0.0–1.0 bar(g) & 100–130°C
Flue gas composition	Synthetic - Natural gas-fired - Coal-fired

- 50kWe (1000kg/day CO₂ removal) scale integrated carbon capture skid
- Design, construct, test and model novel rotating packed bed (RPB) absorbers and regenerators
- Assess the performance of the integrated hardware and solvent under a range of operating conditions
- Test with simulated flue gas at GTI
- Long term test with real flue gas at the National Carbon Capture Center (NCCC)
- Test conventional column performance using NCCC's Slip Stream Test Unit (SSTU)

Project Schedule and Milestones



Milestones	Planned	Actual
Finish Construction of Test Skid	2/8/21	2/12/21
Start Parametric Testing	2/15/21	2/28/21
Develop Preliminary Kinetic Model	8/1/19	6/1/19
Update Kinetic Model Based on Experimental Data	5/31/21	5/31/21
Transport Skid to Host Site	8/31/21	
Start Long-Term Testing	10/15/21	
Verify Kinetic Model with Real Flue Gas Data	3/31/22	

Summary Schedule:

2019 Q1 – Q3	Design Test Skid
2019 Q4 – 2020 Q3	Construct RPBs
2020 Q4 – 2021 Q1	Coplete Test Skid
2021 Q1 – 2021 Q2	Testing at GTI
2021 Q3	Transport to NCCC
2021 Q3 – 2022 Q1	Testing at NCCC

Success Criteria

Decision Point	Date	Success Criteria
Go / No-Go	3/31/2021	<ul style="list-style-type: none"> Complete design for bench scale ROTA-CAPtm skid utilizing continuous absorption-regeneration operation. Viable design for a commercial scale unit verified. Successful testing of the ROTA-CAPtm bench scale skid with RPB absorber and regenerator using simulated gas and natural gas burner flue gas: <ol style="list-style-type: none"> Continuous operation with absorber and regenerator coupled together. Quick startup and shutdown duration for the skid.
Completion of the project	3/31/2022	<ul style="list-style-type: none"> Successful long duration testing: <ol style="list-style-type: none"> Cumulative 1000 hr testing with real flue gas. Minimal solvent carryover and degradation.

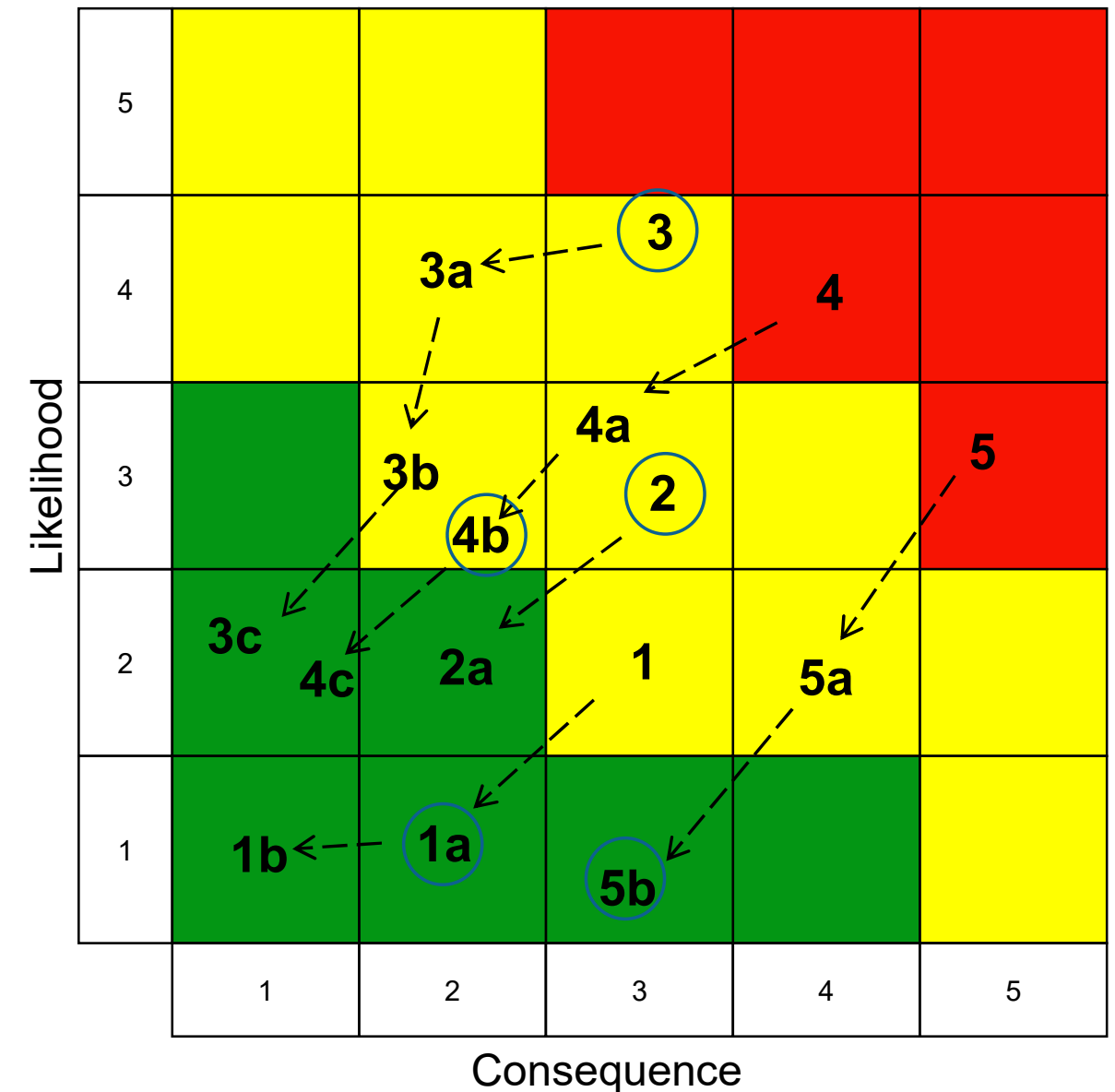
Project Risks and Mitigation Strategies

Technical Risks:

1. **Scale up of rotating packed bed reactor is too problematic**
 - 1a. GTI's experience on evaluation of high-efficiency gas-liquid contactors for natural gas processing including RPB reactors
 - 1b. CCSL's previous and current projects involving RPB reactors and other process equipment
2. **Energy use by RPB reactors is too high**
 - 2a. Reactor design will balance the size of reactor and energy use to achieve economic scale up
3. **Flue gas contaminants degrade solvent or solvent aerosols form on RPB reactor exit**
 - 3a. Solvent analysis to monitor degradation
 - 3b. Liquid carryover measurement
 - 3c. Include a water wash
4. **Not high enough capture efficiency**
 - 4a. CCSL solvent matched MEA performance using RPB
 - 4b. Modify operating conditions to achieve desired capture efficiency
 - 4c. Modify solvent concentration as necessary

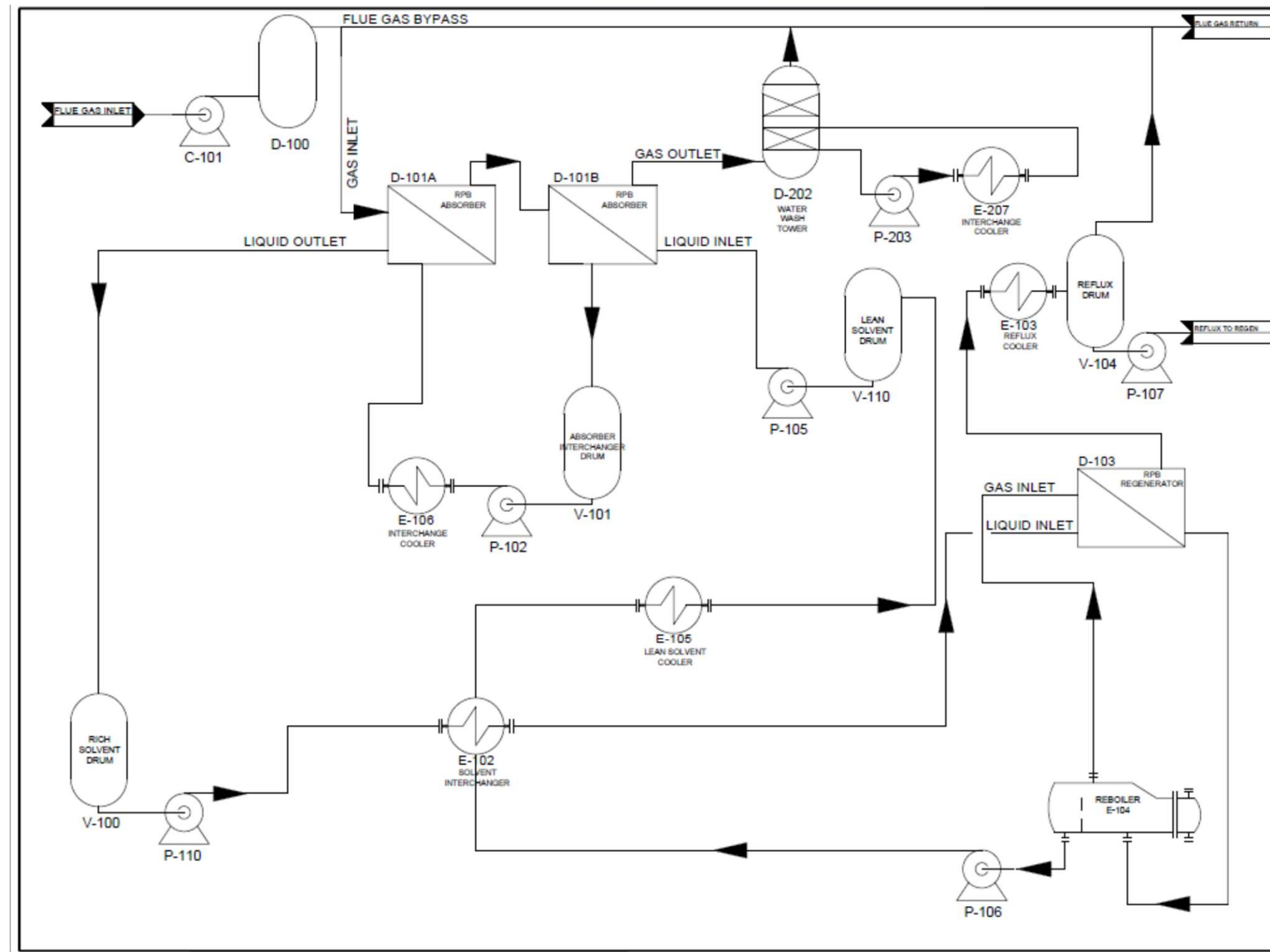
Safety Risk:

5. **Rotating equipment related safety**
 - 5a. GTI Engineering Team has the tools and expertise to design and evaluate rotating equipment requirements.
 - 5b. GTI has access to prototype/one off design engineering facilities for design evaluation. RPB's use GTI's inhouse mechanical design.



Progress and Current Status

ROTA-CAPtm Process Flow Diagram (PFD)

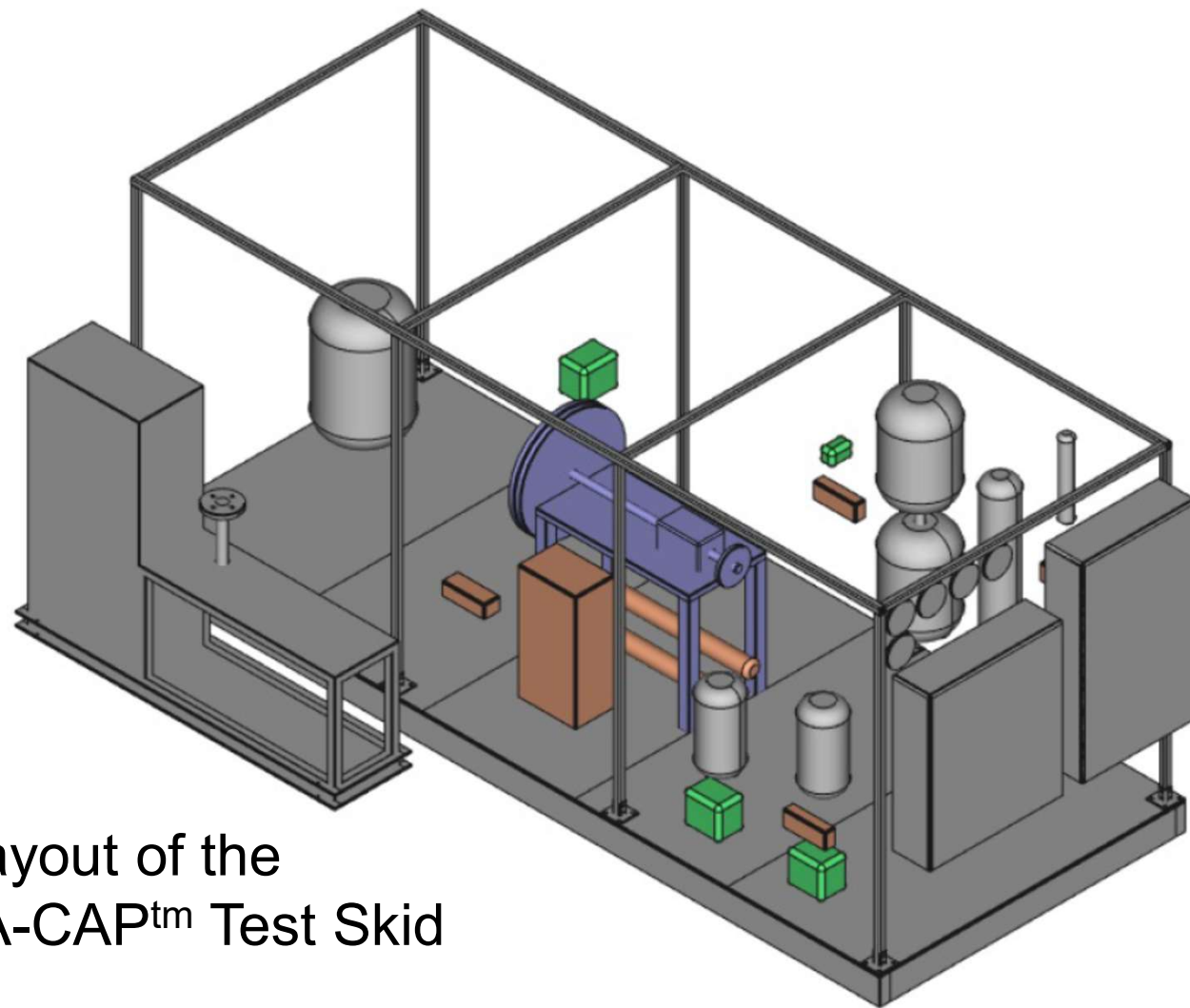


Simplified
ROTA-CAPtm PFD

ROTA-CAPtm has two stages of absorber RPB and one regenerator RPB with a separate reboiler.

ROTA-CAPtm Test Skid and Layout

ROTA-CAPtm Power and Control Panels



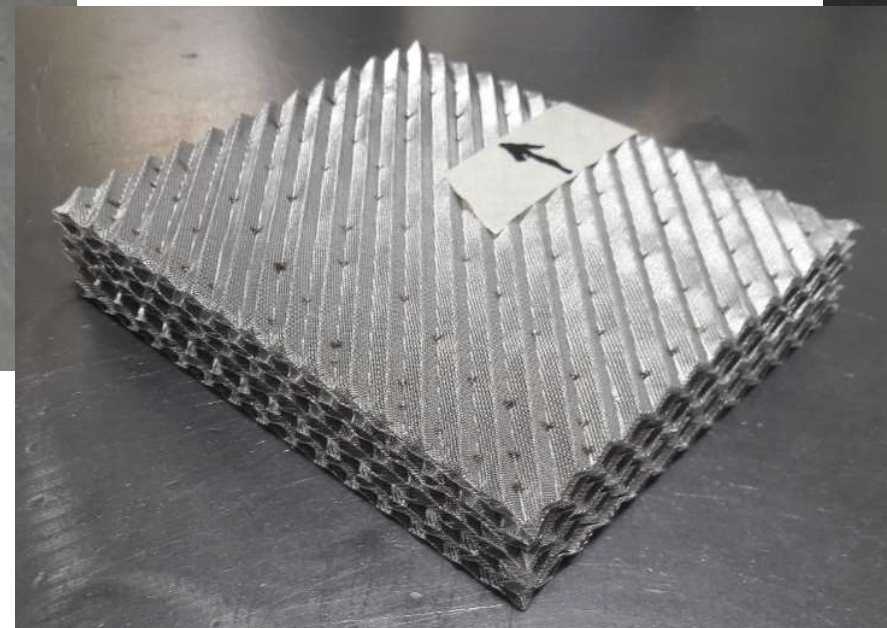
3D Layout of the
ROTA-CAPtm Test Skid



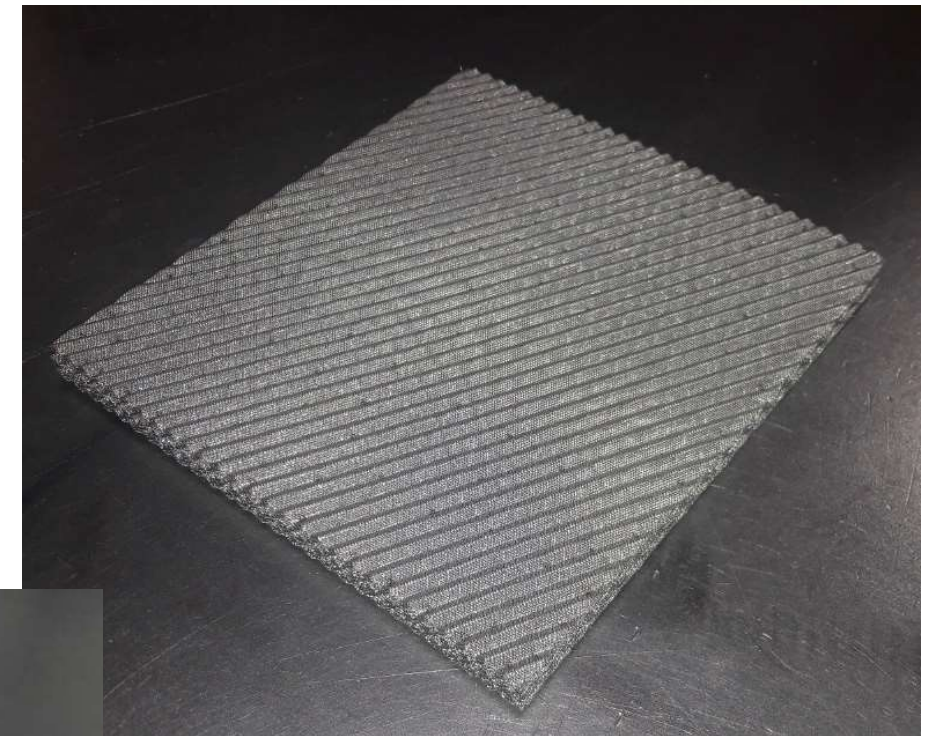
RPB Packing Material by Montz



Novel Packing Material for RPB
manufactured by Montz
(Low Density)



Mid Density Packing



High Density Packing

Project DE-FE0031630 – Technical Updates



Project DE-FE0031630 – Technical Updates



Project DE-FE0031630 – Technical Updates



Project DE-FE0031630 – Technical Updates



Absorber RPB's and Flue Gas Piping



ROTA-CAP™ Skid Before Shakedown

ROTA-CAPtm: Bench Scale Test Unit

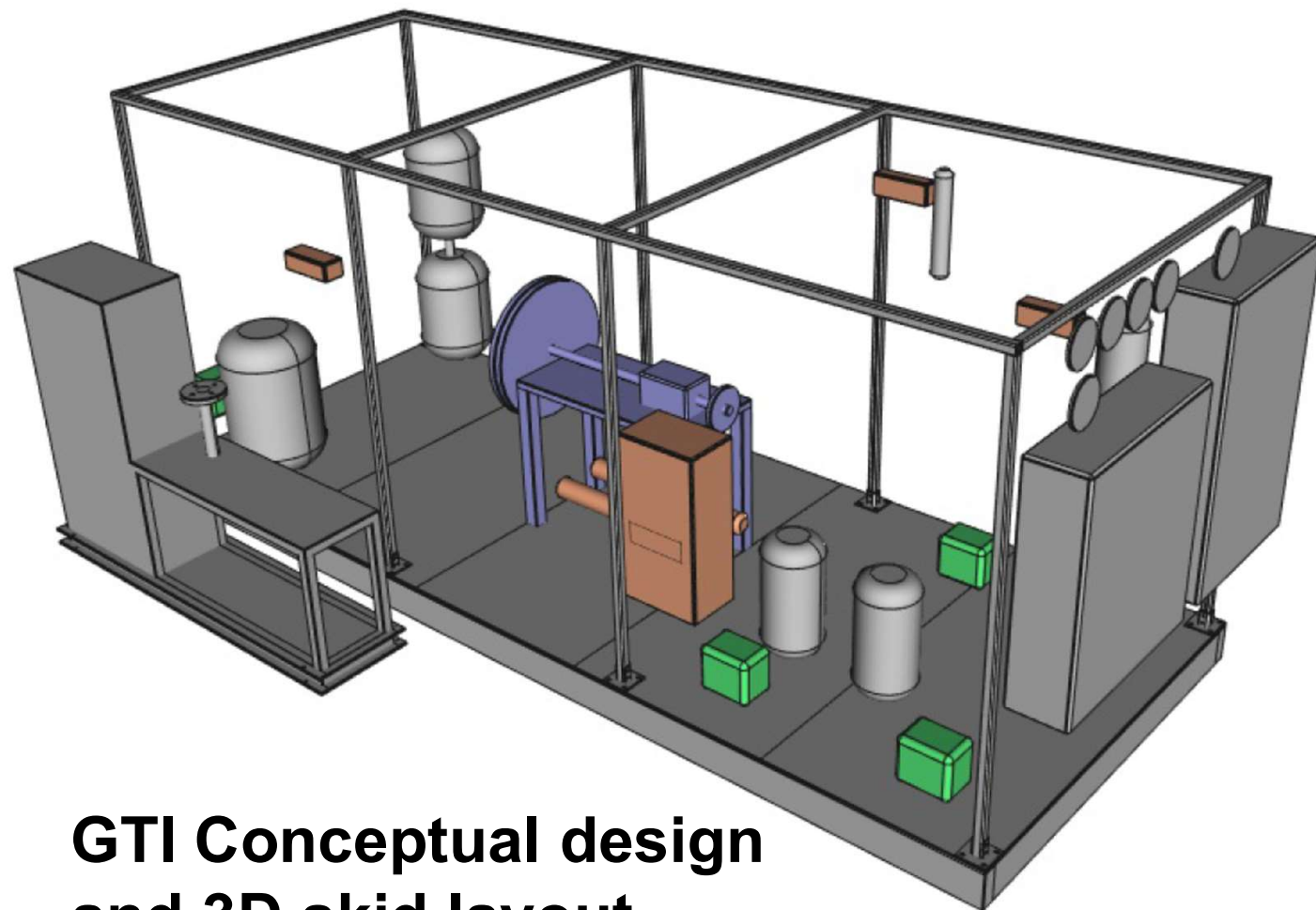
Experimental Development Unit

- 1 ton CO₂ per day removal capacity
- Skid size is 20 feet x 8 feet x 8 feet (NOT OPTIMIZED)
- RPB diameter is about 1 meter



ROTA-CAPtm: Bench Scale Test Skid Design

Integrated (RPB absorber and RPB regenerator),
Continuous, Bench-scale, 1 TPD test skid at GTI



**GTI Conceptual design
and 3D skid layout**



Operational ROTA-CAPtm skid at GTI

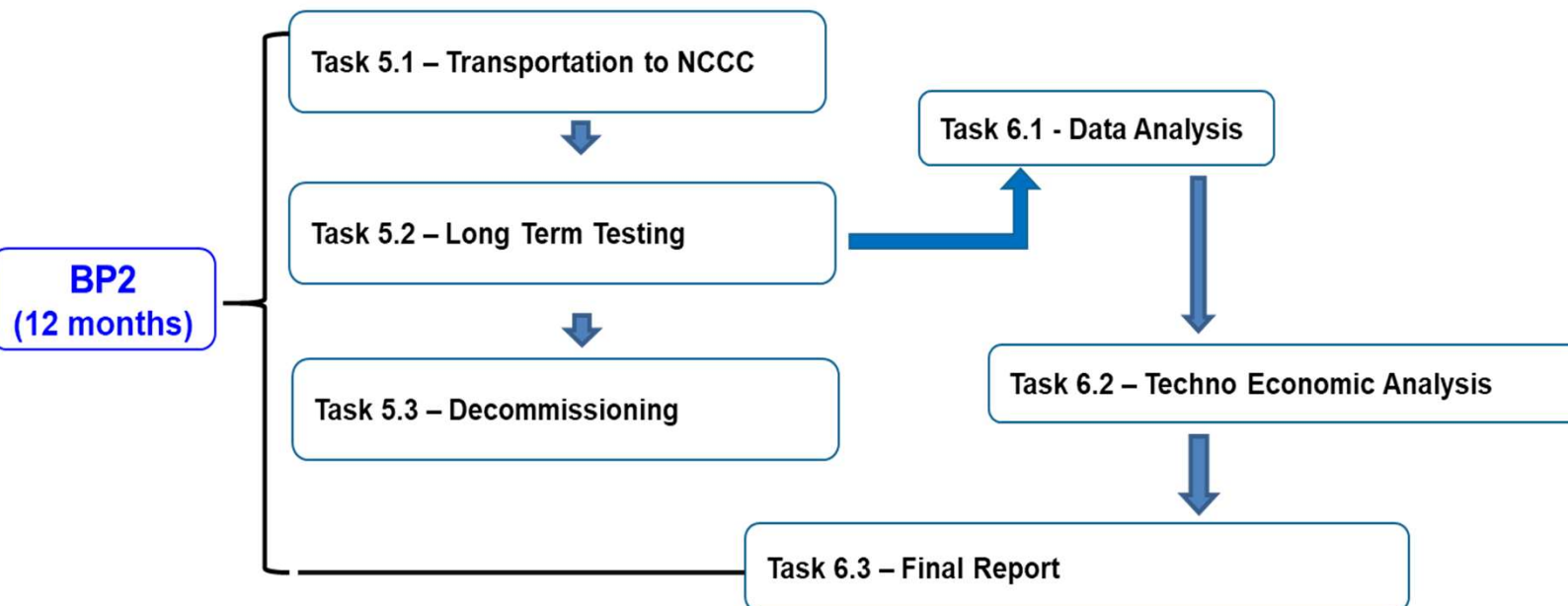
Plans for Future Testing / Scale-Up

Current Project BP2 Overview

Task 1: Project management and planning (*throughout the project*)

ROTA-CAP Testing

Data Analysis and TEA



Success Criteria	Completion Date
Complete design for bench scale ROTA-CAP skid utilizing continuous absorption-regeneration operation.	12/31/2019
Viable design for a commercial scale unit verified.	10/1/2020
Successful testing of the ROTA-CAP bench scale skid with RPB absorber and regenerator using simulated gas: <ul style="list-style-type: none"> Continuous operation with absorber and regenerator coupled together. Quick startup and shutdown duration for the skid. 	5/31/2021

ROTA-CAPtm: Future Projects and Scale Up Plan

- Evaluating different industrial emission sources for ROTA-CAPtm applications.
 - Steel
 - Concrete
 - Petrochemical
- Engineering scale development unit at 2.5 TPD proposed
- Next Scale-Up unit at 10 TPD is designed
- Modular expansion to 100 TPD commercial unit

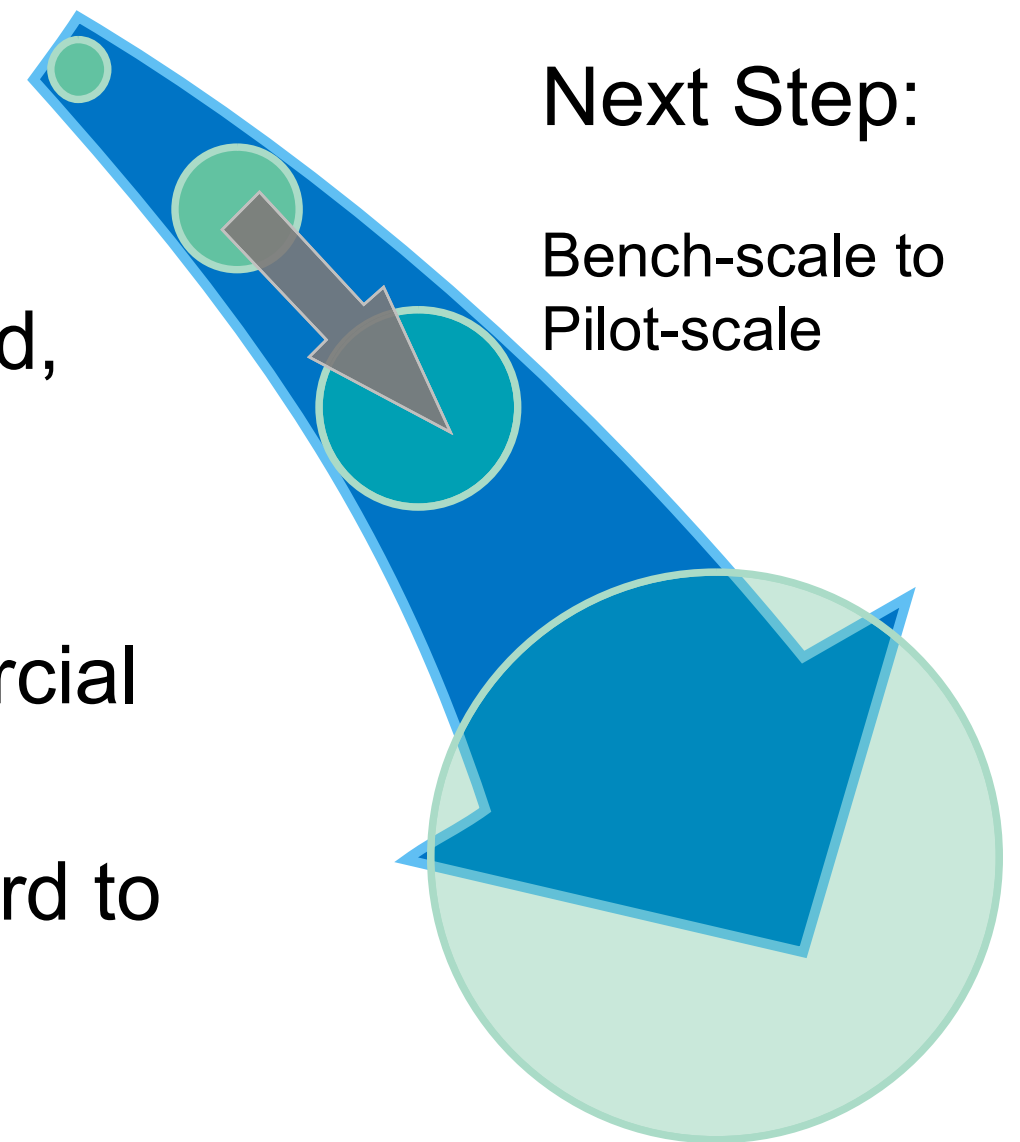


Summary of BP1 Work

- ROTA-CAPtm process design was developed
- Packing material for RPBs fabricated and installed
- 2 stage RPB absorber and 1 stage RPB desorber designed and constructed
- ROTA-CAPtm skid constructed, commissioned and operated
- Parametric testing with simulated gas performed at GTI

Summary:

- ROTA-CAPtm : More versatile process compared to other next generation CO₂ capture technologies
- RPB reactors are agnostic to the solvent used
- First RPB absorber AND RPB regenerator integrated, continuous, bench-scale CO₂ capture skid
- Challenges of scale up from bench-scale to commercial scale; Maybe limited to modular design approach
- Design of seals, wall effects and area affects are hard to determine for commercial scale



Acknowledgements

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Dan Hancu

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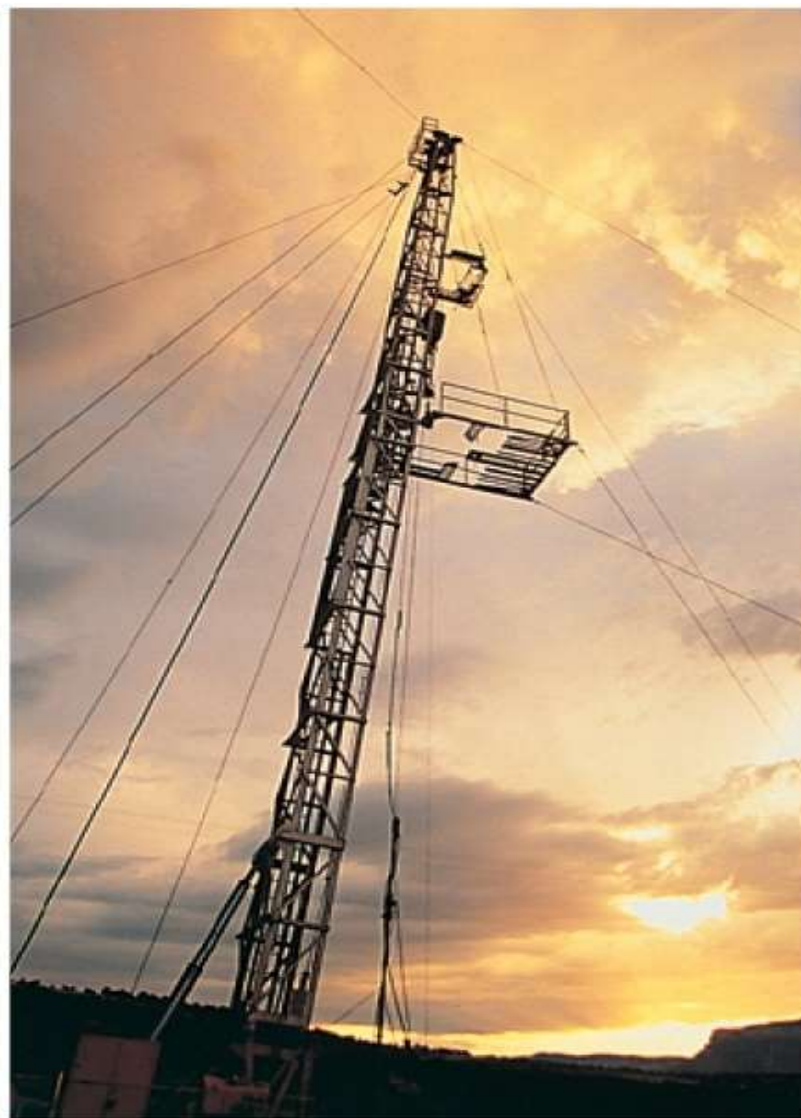


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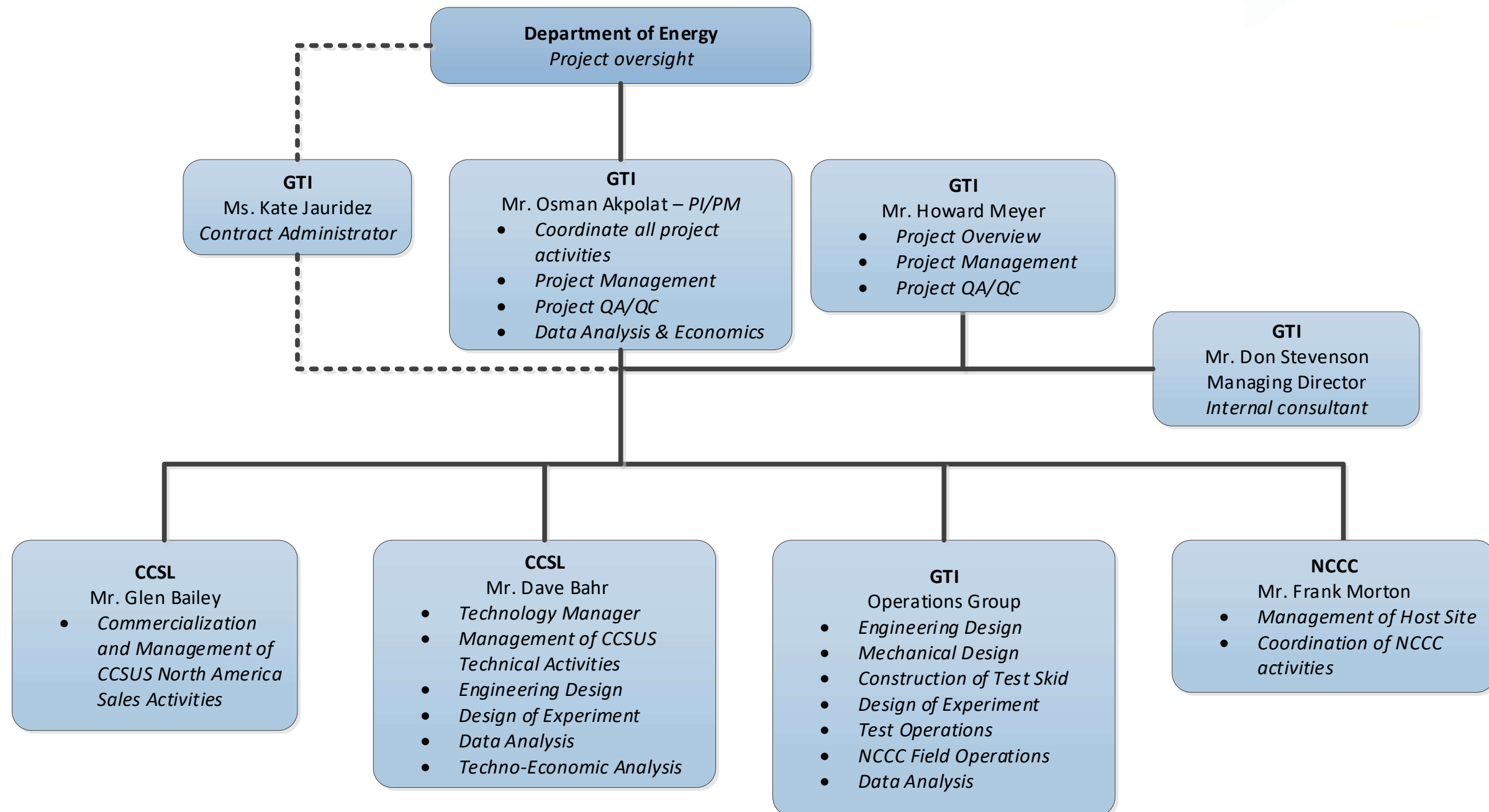
Turning Raw Technology into Practical Solutions

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Appendix

Planned Project Team



Project Schedule - Project DE-FE0031630

