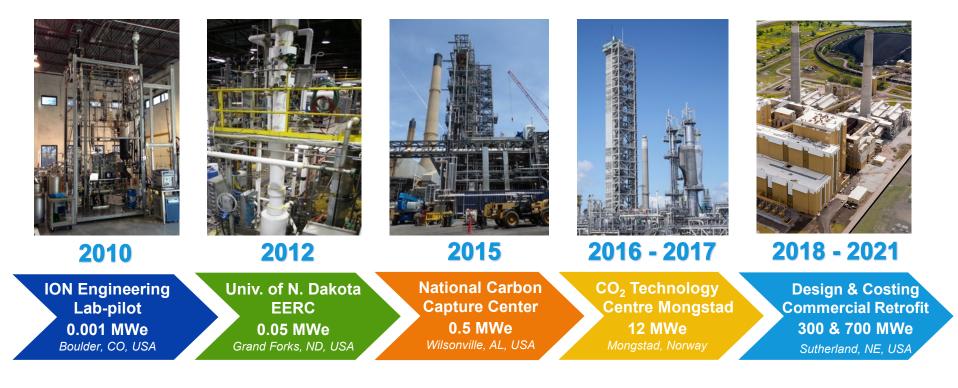
Design and costing of ION's CO₂ capture plant retrofitted to a 700 MW coal-fired power plant

2021 NETL CO₂ Capture Technology Project Review Meeting August 3, 2021

Project: Commercial Carbon Capture Design and Costing: Part 2 (C3DC2) - DE-FE0031840 Andy Awtry, Ph.D. – VP Engineering ION Clean Energy, Boulder, CO, USA

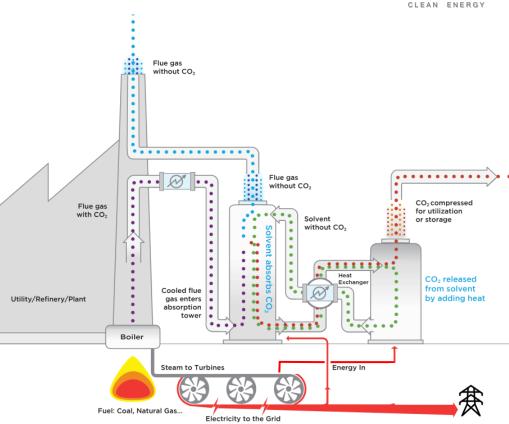
ION's CO₂ Capture Technology Development Accelerated development path leveraging existing research facilities





ION Technology Overview

- Proprietary Solvent-based Technology
 - Liquid absorbent-based capture
 - Low aqueous
 - Worldwide Patents
- Established Engineering Process
 - Learnings from Boundary Dam
 - Learnings from Petra Nova
- Basis of Performance
 - Fast kinetics (on par or faster than MEA)
 - Working capacity (higher than MEA)
 - Low heat capacity (much lower than MEA)
 - < 1,090 Btu/lb CO₂ (2.5 MJ/kg CO₂)



ION Technology Overview Value Added

- High Capture Efficiency
 - Up to 96% CO₂ Capture
- Design System for CAPEX/OPEX savings
 - Smaller absorber column(s) vs higher carrying capacity
 - Pumps/HEXs are smaller due to lower liquid flow rates
- Low regeneration energy requirement
 - Low parasitic load
 - Low steam demand reduction in plant de-rate if integrated into the steam cycle
- Demonstrated lower corrosion rates than MEA
- Demonstrated lower total emission rates than MEA



Nebraska Public Power District Host Site – Gerald Gentleman Station



- Located in Sutherland, Nebraska
- Largest generating station in Nebraska
- Two units with total capacity of 1,365
 MW
 - Unit 1 1979 665 MW



Burns Powder River Basin Coal



Commercial Carbon Capture Design & Costing (C3DC) DE-FE0031595 – Previous Award, Completed Q4 2019



- Objective: Retrofit a Carbon Capture System at a power station
 - Nebraska Public Power District's (NPPD) Gerald Gentleman Station (GGS)
 - 300 MWe Slipstream for carbon capture
 - Ownership model: NPPD owns and operates the capture island
 - Design Basis: CO₂ product for enhanced oil recovery (not regulatory driven)
- Class 3 (AACE) Cost Estimate
 - Cost Estimate is -20% to +30%
 - Completed about 20% of Engineering Effort
- Completed 18mo Project in Q4 of 2019

Commercial Carbon Capture Design & Costing Study

		Value	Units
	Slipstream	300	MWe
	EPC Capital Cost	\$438,000,000	\$
	Loan Term	20	years
	Interest Rate	4.5%	%
	Total OPEX	\$28,200,000	\$/yr
	Total Annual Cost	\$61,800,000	\$/yr
-	Total Annual CO ₂ Production CF	1,900,000	tonne/yr
	Cost of CO₂ Capture	\$32.50	\$/tonne



COMMERCIAL CARBON CAPTURE DESIGN & COSTING STUDY: PART 2

DE-FE0031840

- Retrofit a Carbon Capture System at an existing power station
 - Nebraska Public Power District's (NPPD) Gerald Gentleman Station (GGS)
 - 700 MWe carbon capture system (2x 350 MWe trains)
 - Ownership model: Capture System is 3rd Party Owned and Operated
 - Design Basis: CO₂ product for EOR (not regulatory driven)
- Class 2 (AACE) Capital Cost Estimate
 - Estimate Accuracy Range: -15% to +20%
 - Complete about 50-60% of Engineering Effort
- 18-month project; to be completed in Q1 of 2021
- \$5.8M project budget
 - \$4.6M DOE-NETL
 - \$1.2M ION & Partners

C3DC2 Study Project Team and Roles



ION Clean Energy

- Technology Developer
- Process Design and Project Management



Koch Modular Process System

- Carbon Capture pilot
 experience and expertise
- Capture Process
 Oversight, Design and
 Costing



Nebraska Public Power District

- Host Site (GGS)
- Power Generation Engineering,
 Operational and Financial Expertise

Sargent & Lundy

Sargent and Lundy

- Balance of Plant (BOP)
 - Engineering
- Overall Cost Estimate Development
- Constructability Review
- Construction Cost Estimating

SIEMENS Siemens Ingenuity for Life

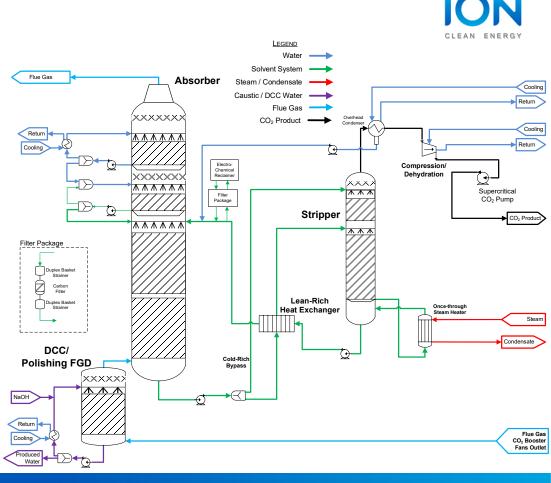
Compressor Vendor

ProTreat[®] Process Model *ION CO*₂ *Capture Process*

Key features of ION process compared to 'common' MEA-designed plant

- Cold-Rich By-pass
- Optimized lean rich cross exchanger (LRXC) design
- Caustic addition to DCC to act as SO_x
 Polishing Scrubber
- Compressor Selection

ProTreat output provides stream tables, key performance indices, and steam, cooling and electrical duties



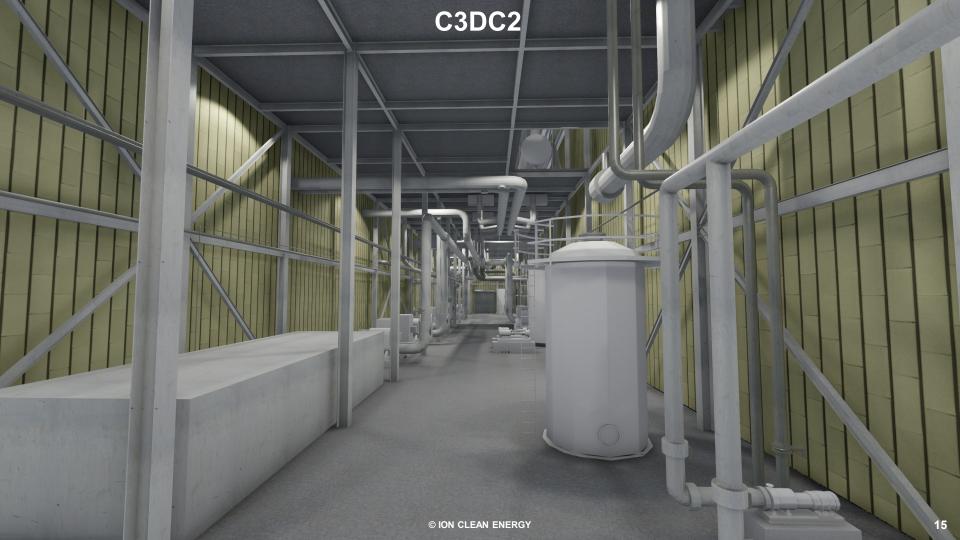
System Design 700MWe CO₂ Capture Plant



- Capture System Design
 - 2x 50% trains for the Capture Island
 - 2x 50% on major pieces of equipment to assist in turndown and provide some risk mitigation
 - Designed for operation at full load, and track plant load to maximum turndown
 - Designed for 90% capture of CO_2 ; resulting in >95% capture at turndown
 - CO₂ product at historic plant CF (2018-2019): 4.3M tonnes of CO₂/yr
- BOP Design
 - Steam sourcing from GGS2 steam cycle
 - Cooling water from a hybrid system









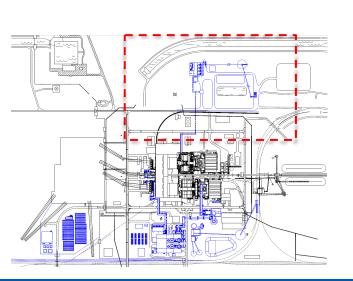
Bioenergy w/ Carbon Capture & Sequestration (BECCS) 700MWe (4.3M TPA) CO₂ Capture Plant

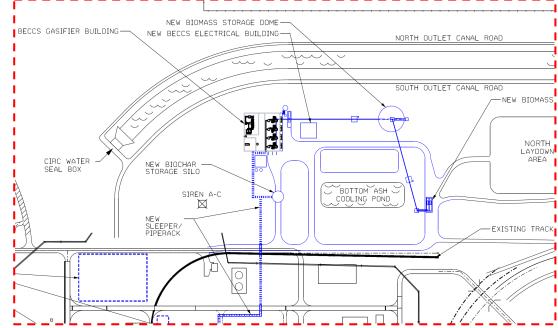
- Overall cost evaluation for potential net zero and net negative emissions
- Engineering Design
 - Biofuel Sourcing
 - Corn Stover vs Eastern Red Cedar
 - Pellets vs Bales
 - Gasifier Design
 - Design for 10-15% coal offset
 - Evaluate boiler performance
 - Balance of Plant Design
 - Evaluation of capture performance on the existing CO₂ capture process design



Bioenergy w/ Carbon Capture & Sequestration (BECCS) BECCS General Arrangement Drawing

- Corn Stover Pellets delivered by truck
- Gasifier converts pellets to syngas
- Boiler mods and resulting flue gas by B&W





Bioenergy w/ Carbon Capture & Sequestration (BECCS)

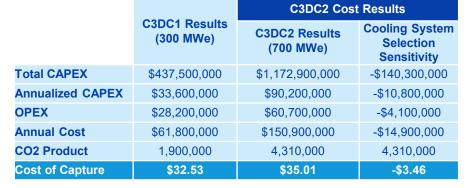
Flue Gas Comparison and CCS Performance

- Max Design is the Base Design Case, assuming full load of the power plant
- BECCS case replaces 10% of the coal with the syngas from the gasifier
 - 5.5% reduction in CO₂ flow to the capture island
 - Increase in capture efficiency to 93.3% (holding steam consumption constant)
 - 1.6% reduction in CO₂ product flow
 - Reduced CO₂ by 98% relative to coal emissions
 - CO₂ reduction >100% with 10% increase in packing and 23% more plates in LRXC

Parameter	Units	Max Design Value	BECCS (Corn Stover)	BECCS (Corn Stover)
DCC Inlet Conditions (1x50% train)				
Temperature	°F	145	144	144
Pressure	psia	13.75	13.75	13.75
O ₂ Concentration	vol %	4.34	5.43	5.43
CO. Data	vol %	11.5	10.78	10.78
CO_2 Rate	lb/hr	711,831	672,890	672,890
Flue Gas Flowrate	acfm	1,107,000	1,114,000	1,114,000
	lb/hr	3,973,000	4,003,000	4,003,000
CO ₂ Capture Performance (1x50% train)				
Capture Efficiency	%	90	93	95
CO ₂ Captured	lb/hr	638,000	628,000	640,745
L/G	lb/lb	1.93	1.81	1.81
Electrical Duty	kW	31,900	31,700	31,700
SRD	MJ/kg CO2	2.51	2.55	2.55
Steam Consumption	lb/hr	765,100	765,100	765,100

Cost of CO₂ Capture Costing Basis

- Designed to produce a reliable CO₂ product stream for EOR/Sequestration; not regulatory driven CO₂ capture
- Used historical data for the unit to model cumulative captured CO₂ based on observed power plant load factor, capture plant uptime, and ambient conditions
- Calculated the cost with and without the additional flue gas pre-conditioning to isolate the cost of CO₂ capture for comparison to sites that may already have this equipment
- BECCS evaluation was performed as a sensitivity study and its incremental capital and operating expenses are separate
- 3rd Party Ownership impact on overall costing being further investigated





Acknowledgement and Disclaimer



Acknowledgement

This material is based upon work supported by the Department of Energy National Energy Technology Laboratory under cooperative award number DE-FE0031840.

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Nebraska Public Power District

Sargent & Lundy LLC







ION

Thanks

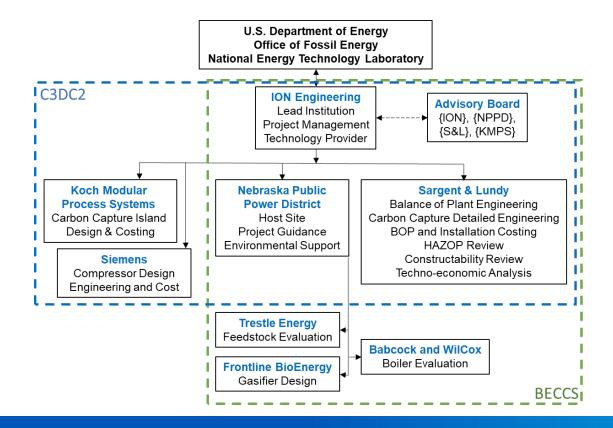
C3DC2 Team: ION, NPPD, S&L, KMPS, Siemens

BECCS TEAM:

Trestle Energy, Frontline BioEnergy, Babcock & Wilcox

Department of Energy:

#	Task	Milestone Title / Description	Completion Date	Verification Method
M1	1.0	DOE Kickoff Meeting	12/5/2019	Meeting Held
M2	M2 1.0 Updated PMP		11/7/2019	PMP Transmitted to DOE FPM
М3	2.0	Basis of Design for Project Finalized	1/10/2019	Meeting Held w/ Results Project SharePoint Site; Completion Memo to DOE
M4 3.0 Preliminary Design Review Complete		3/30/2020	Meeting Held w/ Results Project SharePoint Site; Completion Memo to DOE	
M5 4.0 Critical Design Review Complete		9/30/2020	Meeting Held w/ Results Project SharePoint Site; Completion Memo to DOE	
M6	5.4	HAZOP Complete	11/24/2020	HAZOP Report Completed
M7	M7 6.0 Overall Cost Estimate and Cost of Capture		1/12/2021	Meeting Held w/ Results Project SharePoint Site; Completion Memo to DOE
M10	4.2	BioMass Co-firing BOP Design	4/1/2021	Meeting Held w/ Results Project SharePoint Site; Completion Memo to DOE
M8 7.0 Front-End Engineering Design (FEED) Report		9/1/2021	Report Delivered to DOE/NETL	
M9 7.0 Final DOE Report & Presentation		9/30/2021	Report Delivered to DOE/NETL	



					Half 2, 2019 Half 1, 2020 Half 2, 2020 Half 1, 2021 Half 2, 202
	Task Name	- Duration	🗕 Start	🗕 Finish	JASONDJFMAMJJASONDJFMAMJJASO
	⊿C3DC2 Project - FEED Study	526 days	Mon 9/2/19	Thu 9/30/21	
	1.0 Project Management and Planning	460 days	Mon 9/2/19	Wed 6/30/21	
20	2.0 Overall Project Design Basis	361 days	Thu 10/31/19	Tue 4/13/21	
51	43.0 Process Design - CO2 Capture Island Design	290 days	Mon 9/30/19	Wed 11/25/20	
52	Preliminary Design - CO2 Capture Island	254 days	Mon 9/30/19	Tue 10/6/20	
103	M4: Preliminary Design Review	0 days	Fri 4/24/20	Fri 4/24/20	♦ 4/24
104	Detailed Design - CO2 Capture Island	159 days	Thu 4/16/20	Wed 11/25/20	
136	4.0 Engineering & Design - Integration and BOP	340 days	Fri 12/20/19	Fri 4/30/21	
137	Detailed Design - Integration and BOP	340 days	Fri 12/20/19	Fri 4/30/21	
383	M5: Critical Design Review	10 days	Wed 9/16/20	Tue 9/29/20	
384	BECCS - Biomass Co-firing	121 days	Thu 11/5/20	Thu 4/29/21	
430	5.0 Studies and Investigation	412 days	Tue 12/3/19	Fri 7/23/21	
540	6.0 Cost Estimate	199 days	Tue 7/21/20	Fri 4/30/21	
574	₄7.0 Reporting	158 days	Tue 2/23/21	Thu 9/30/21	
575	M8: Front-End Engineering Design (FEED) Report	137 days	Tue 2/23/21	Wed 9/1/21	
583	M9: Final DOE Project Report	71 days	Thu 6/24/21	Thu 9/30/21	
589	BECCS Reporting	70 days	Thu 4/1/21	Wed 7/7/21	