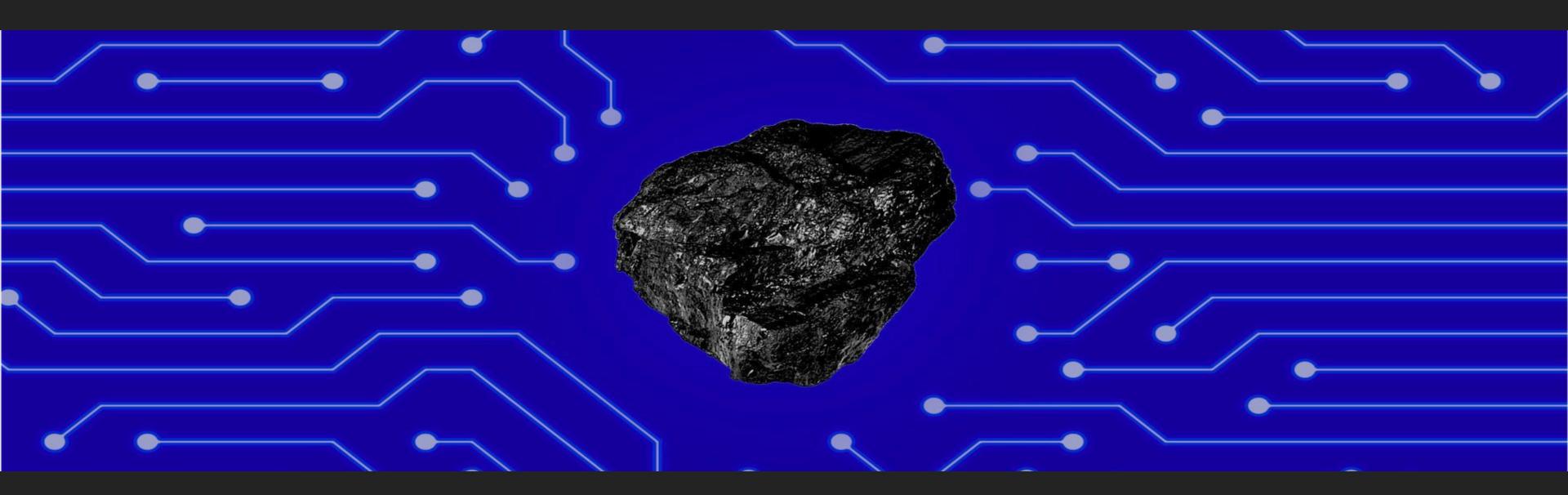
# **Experimental Validation & Continuous Testing of an On-Purpose High-Yield Pitch Synthesis Process for Producing Carbon Fiber from Coal (LSDCL)**



# By Charles Hill and Chris Yurchick — Co-Pls @ Ramaco Carbon

Prepared for the 2020 NETL Annual Coal Processing Project Review Meeting



### Who We Are

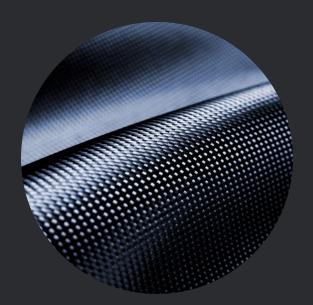
**Ramaco Coal,** founded in 2011, is a coal-based conglomerate with operations in five states. It consists of two main operating companies:



#### Ramaco Resources

A publicly traded met coal producer (METC-Nasdaq) with low cost, high quality production in West Virginia, Virginia and Pennsylvania.

Headquartered in Lexington, Kentucky.



#### **Ramaco Carbon**

The first vertically integrated resource, research and manufacturing coal technology platform focused on creating "Coal to Products".

Headquartered in Sheridan, Wyoming.



www.ramacoresources.com

www.ramacocarbon.com

**Experimental Validation & Continuous Testing of an On-Purpose High-Yield Pitch Synthesis Process for Producing Carbon Fiber from Coal (LSDCL)** 

Experimental Validation & Continuous Testing of an On-Purpose High-Yield Pitch Synthesis Process for Producing Carbon Fiber from Coal (LSDCL) DE-FE-00310801

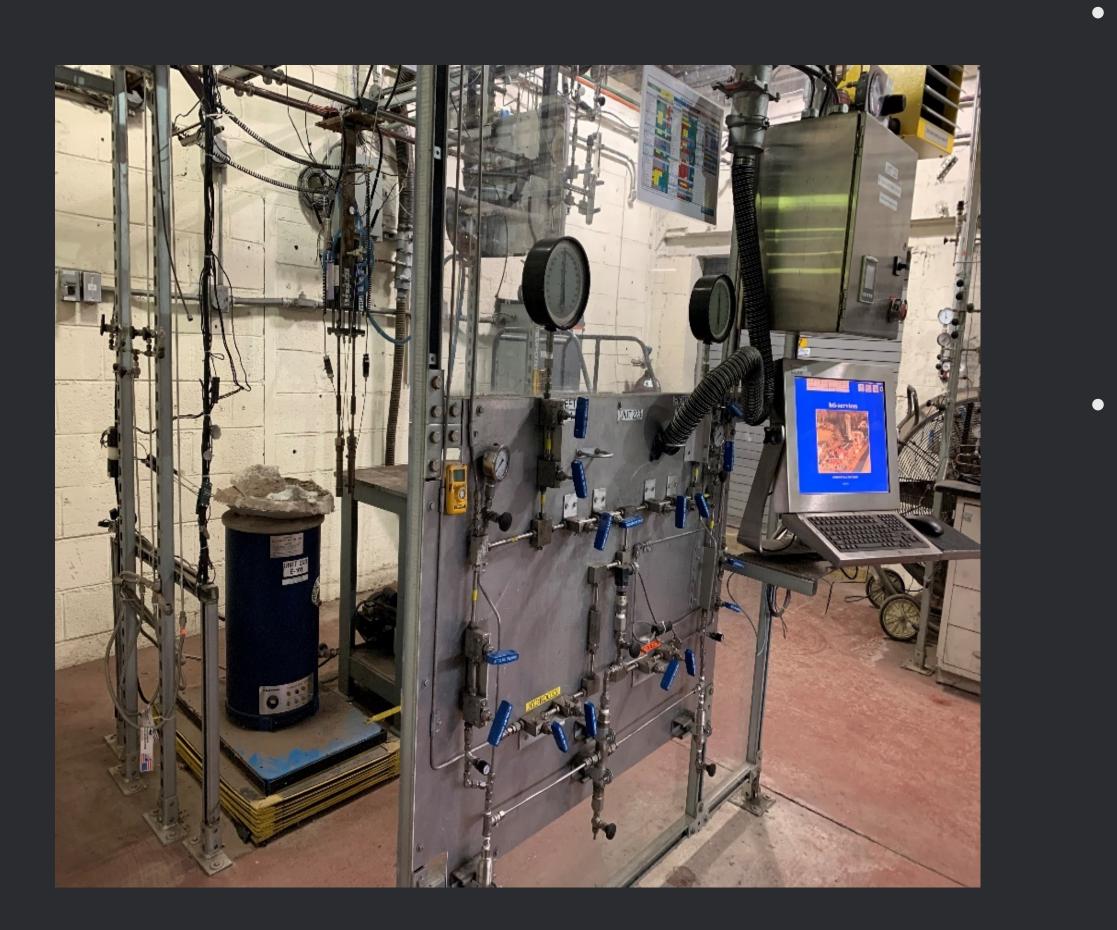
- Produced over 100kg of high-quality isotropic pitch.
- Much lower cost than PAN and more ecologically sound (greener)
- Demonstrated mesophase conversion at acceptable yields.
- Demonstrated initial fiber production with good draw down ratios.



#### DOE Funding: \$883,365 Cost Share: \$220,842 Total Value: \$1,104,207

Budget Period 1: 1-12 months Budget Period 2: 2-12 months

ic pitch. gically sound (greener) eptable yields. good draw down ratios.





Develop a process to create highquality carbon fiber precursor material from U.S. coal using **lowseverity direct coal liquefaction** (LS-DCL) techniques in the synthesis of coal tar pitch.

 Project could lead to cost reductions to take advantage of a secure, plentiful domestic coal feedstock, and may significantly expand the market for pitch-based carbon fiber.



Direct Coal Liquefaction Technology – HTI H-Coal<sup>®</sup> Development History:

• Same development path/pilot units as H-Oil®.

• Pilot plant development started in 1960's.

• DOE-supported scale-up to demonstration scale (200 TPD) in 1980s. This Catlettsburg, KY facility is pictured on the right.

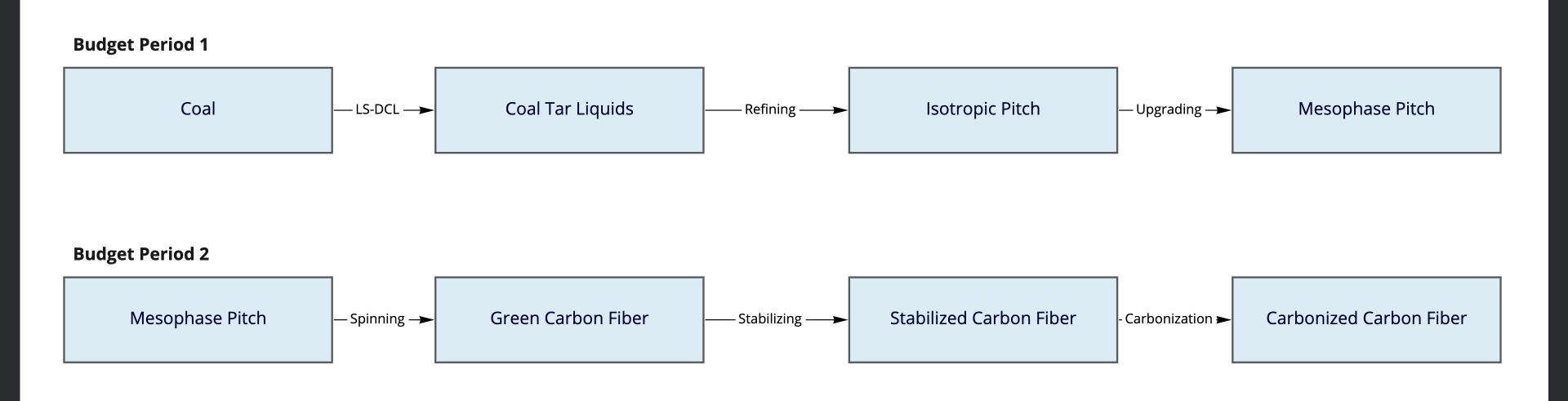
• License/Basic engineering design and provided start-up support for Shenhua Direct Coal Liquefaction Plant, a successful start-up in 2008 with a capacity of 6000 tons per day of coal.











- Main technical focus area is on the LS-DCL step
- LS-DCL is derived from long established process technologies, H-Coal<sup>TM</sup>/H-Oil<sup>TM</sup>, originally commercialized for liquid transportations fuels
- LS-DCL constitutes an incremental, lower severity, change in process conditions to produce **on-purpose isotropic pitch** and valuable co-products
- Other processing steps are to be practiced by conventional means





#### **Project Objectives & Success Criteria**

- 1. Demonstrate that coal tar pitch-based isotropic pitch can be made in **high yield** >35% in a low severity DCL process.
- 2. Illustrate techno-economic viability of producing mesophase pitch at \$1.50/lb.
- 3. Validate that the resulting **mesophase** pitch is a suitable carbon fiber precursor, satisfying the most basic physical property criteria, such as:
  - Softening point (300°C –375°C).
  - Sufficiently high mesophase content (35% -90%). •
  - Sufficiently low QI content.
  - Ability to spin continuous monofilament fiber.



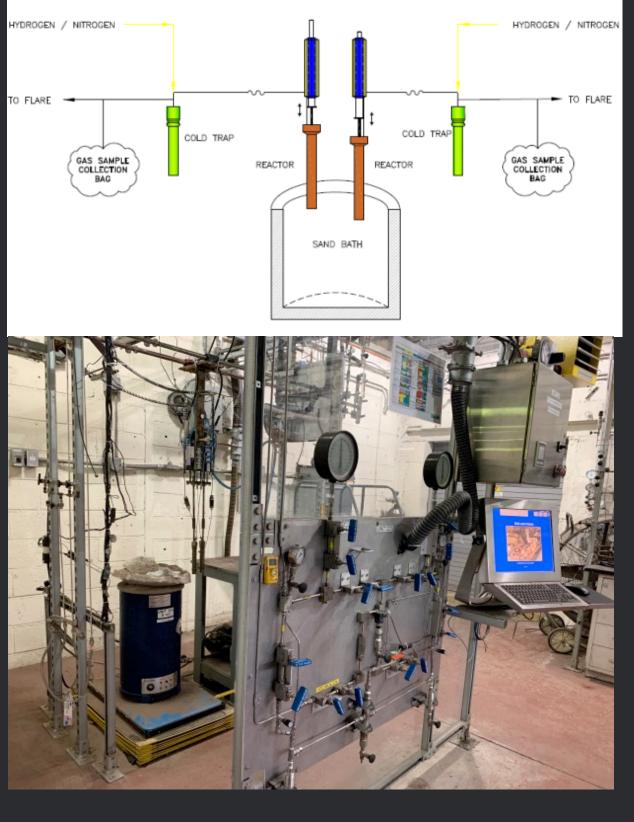


#### Micro-autoclave (Unit 223) Coal Reactivity Testing To Determine Conditions for Pilot Operations

Unit 223 has side-by-side reactors to allow parallel testing. The reactors were charged with coal (4 g) and solvent (16 g) and were threaded onto the shaker arm assembly. The reactors were pressurized to the desired test pressure with hydrogen, nitrogen, or other gas via 3-mm tubing that was welded into the reactor cap.

Run# 223- 28-	Reactor #	Time @Temperature Minutes	Temperature deg C	Starting Pressure	Coal g	Solvent g
6	K-1	60	400	6.90 MPa/H2	4.00	16.00
6	K-2	60	400	3.45 MPa/H2	4.00	16.00
7	K-1	90	400	6.90 MPa/H2	4.00	16.00
7	K-2	90	400	3.45 MPa/H2	4.00	16.00
8	K-1	45	413	6.90 MPa/H2	4.00	16.00
8	K-2	45	413	3.45 MPa/H2	4.00	16.00
9	K-1	60	413	6.90 MPa/H2	4.00	16.00
9	K-2	60	413	3.45 MPa/H2	4.00	16.00
10	K-1	30	407	6.90 MPa/H2	4.00	16.00
10	K-2	30/30	407/418	6.90 MPa/H2	4.00	16.00

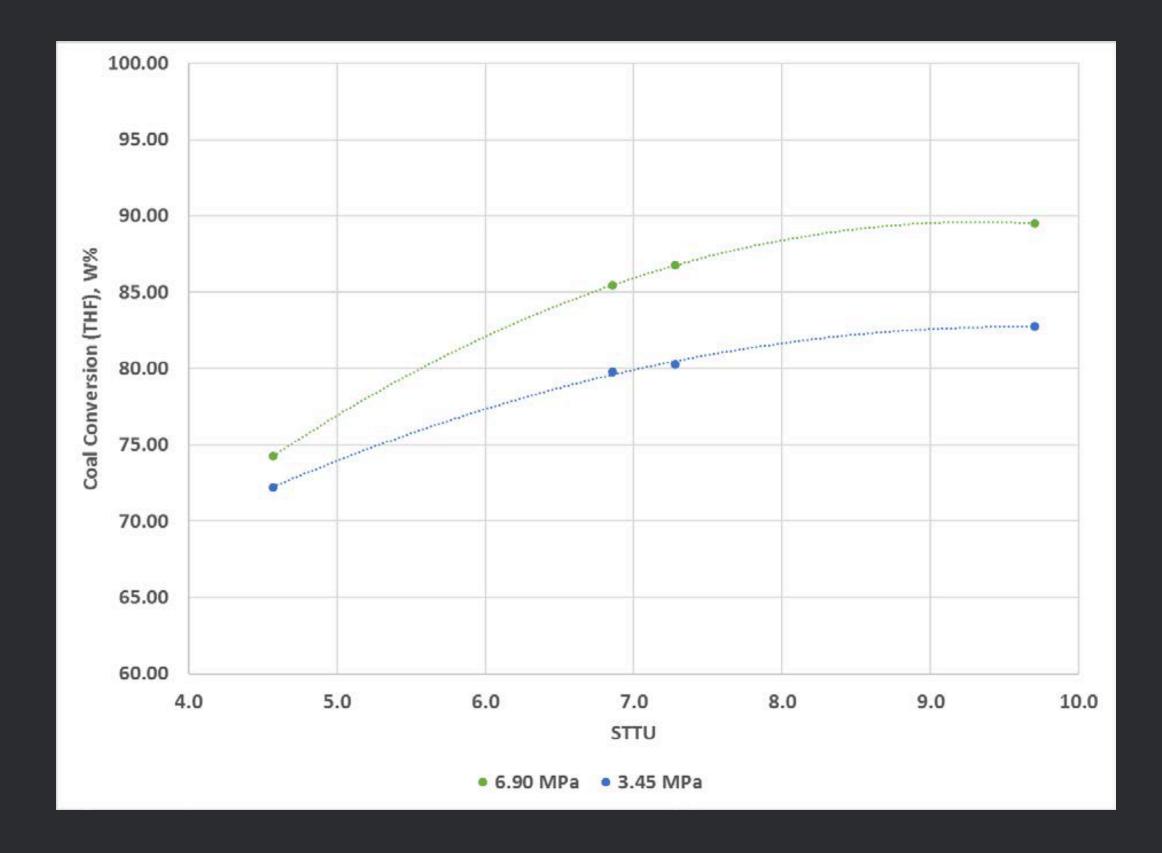






# Micro-autoclave (Unit 223) Coal Reactivity Testing Results

Coal Conversion H2 Pressure Effect

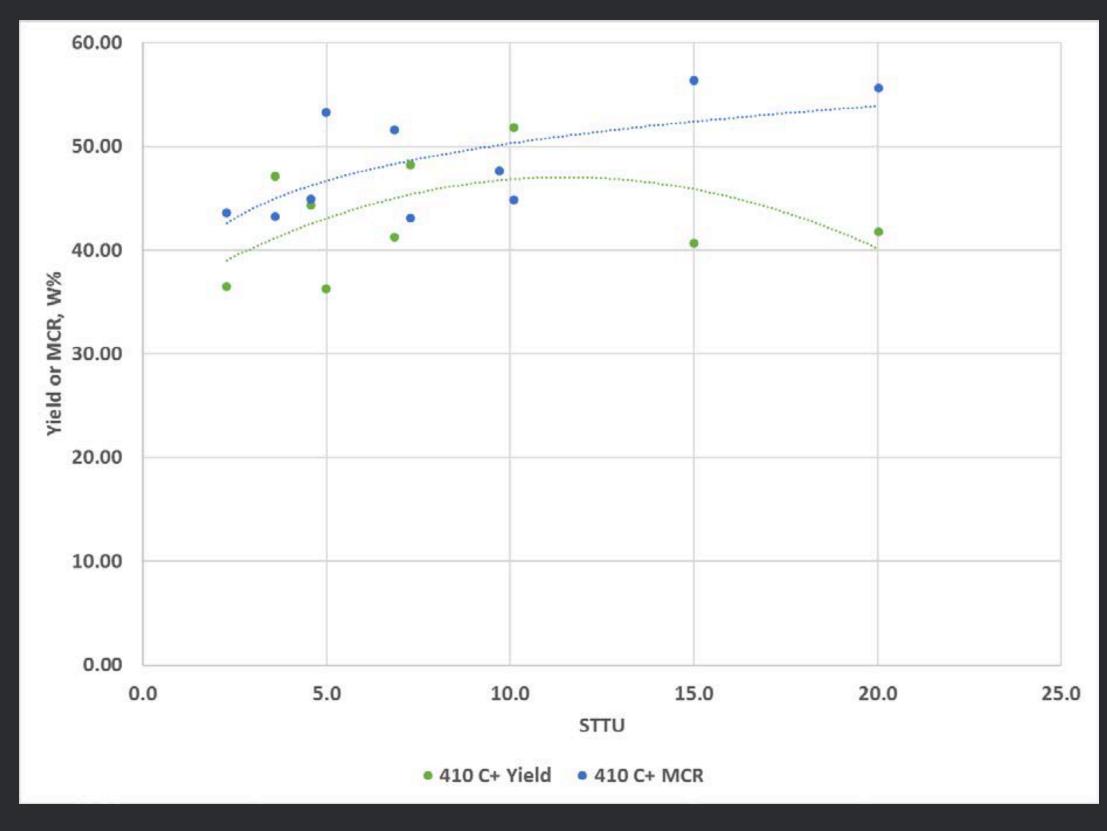






#### Micro-autoclave (Unit 223) Coal Reactivity Testing Results

#### Pitch Yield and Quality at 6.9MPa







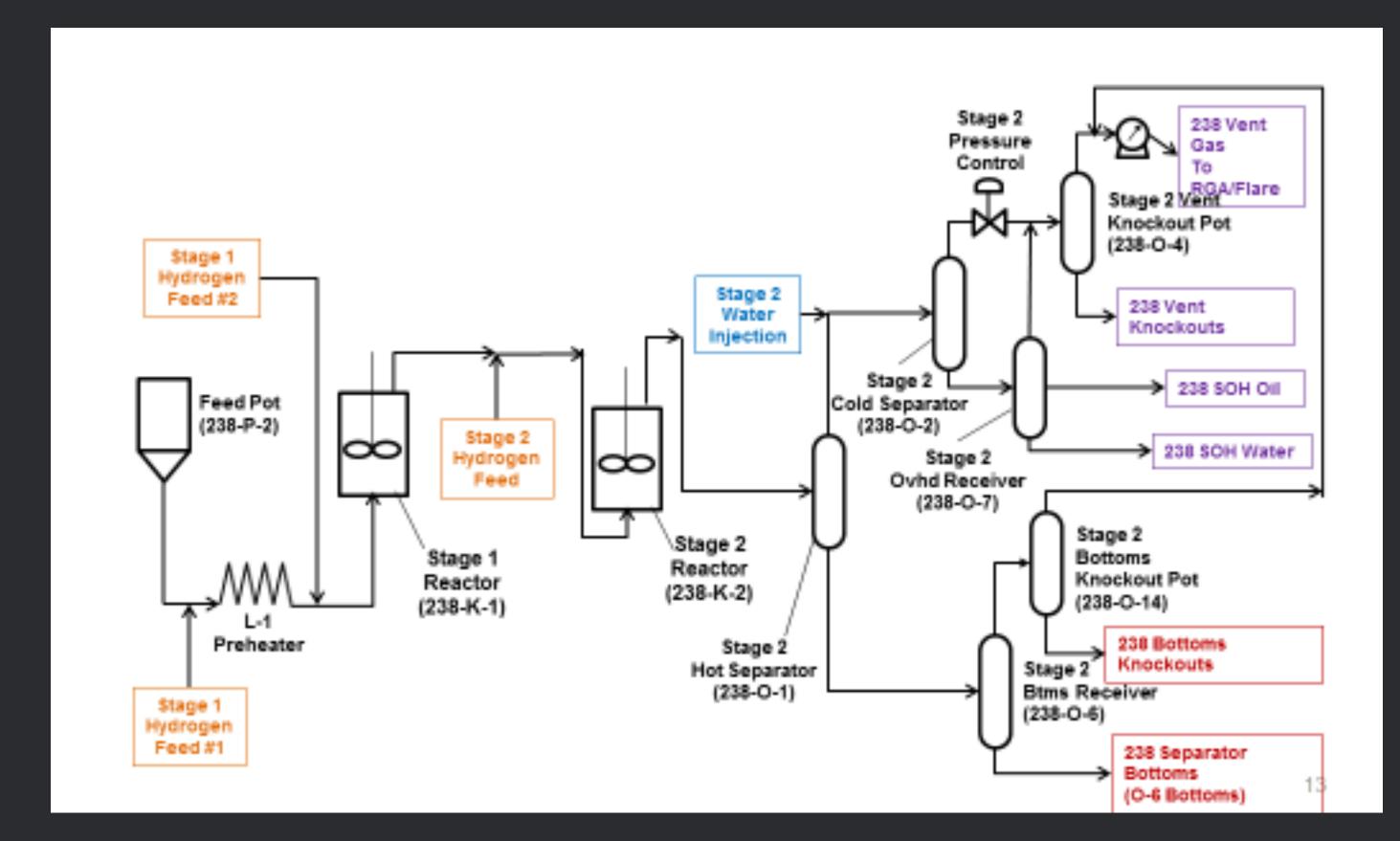
### Micro-autoclave (Unit 223) Coal Reactivity Testing

- The last test performed (Test 10) in K2 simulated a 2-stage operation ullet
- Reaction time of 30 minutes in each stage ullet
- Temperatures of 407°C and 418 °C respectively. igodol
- Results from this last test are excellent with: igodol
  - 90 % coal conversion,
  - 35 % 525 C+ pitch yield
  - MCR:Asphaltene ratio of 1.9
- These conditions were selected for continuous operation in the pilot (Unit 245). ullet





#### Pilot Operations (Unit 245) Processing

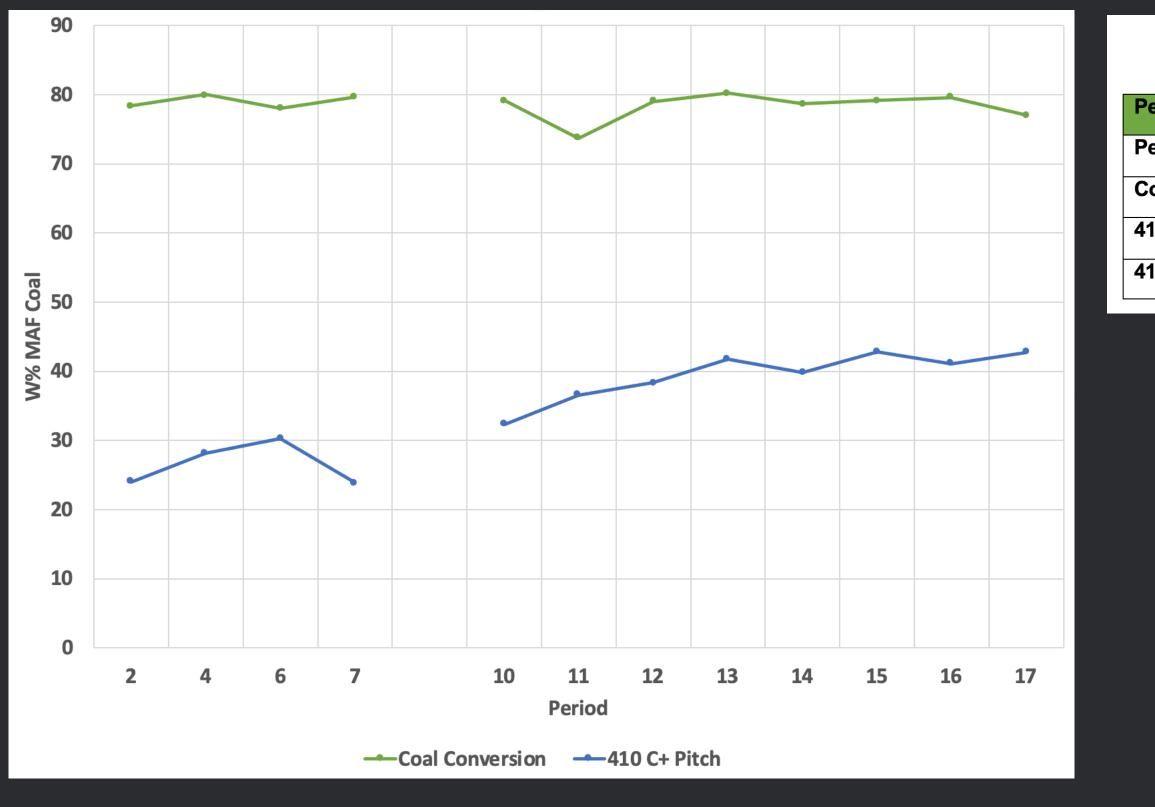






#### Pilot Operations (Unit 245) Processing

Coal Conversion & Pitch Yield (%)





#### Table 1 – Average Performances

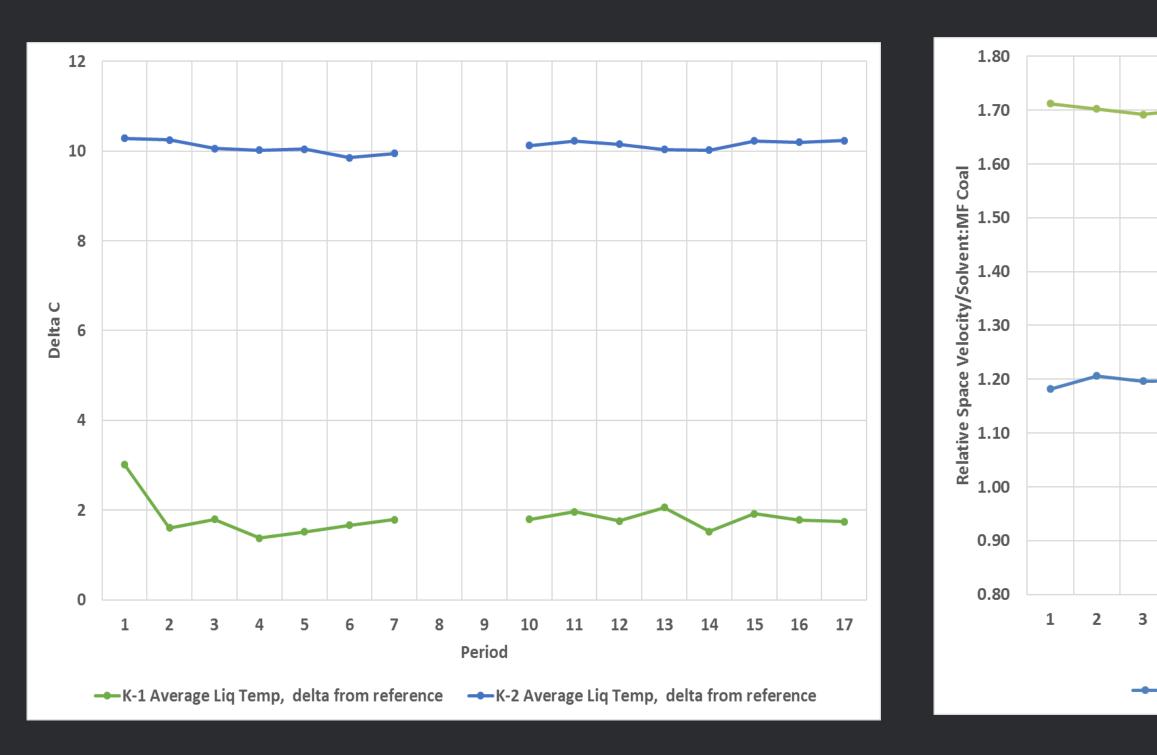
eriods	1-7	10-17			
eriods Averaged	2,4,6,7	10-17			
oal Conversion, W% MAF Coal	79.0	78.9			
10 °C+ Pitch Yield, W % MF Coal	25.2	37.3			
10 °C+ Pitch, MCR	41.2	42.1			



#### Pilot Operations (Unit 245) Processing

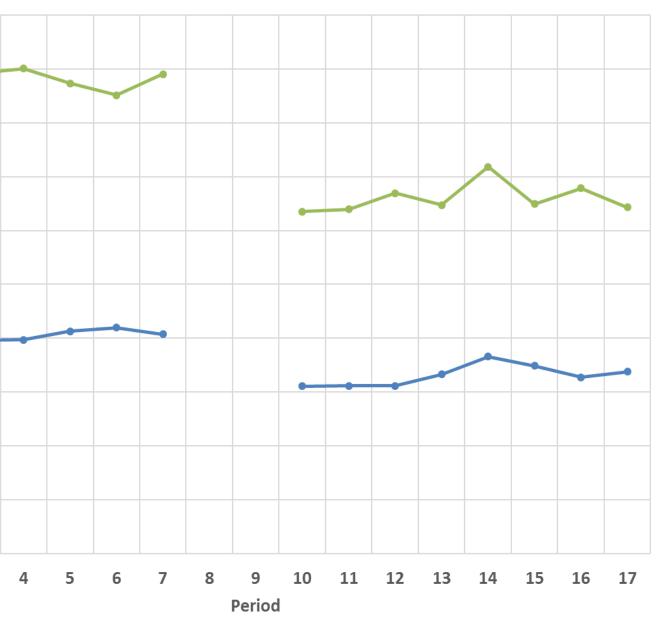
#### **Reactor Temperatures**

#### Reactor Space Velocity/Solvet:MF Coal Ratio



Carbon Fiber Precursor Pitch from Low-Cost Powder River Basin Coal





---Solvent:MF Coal Ratio

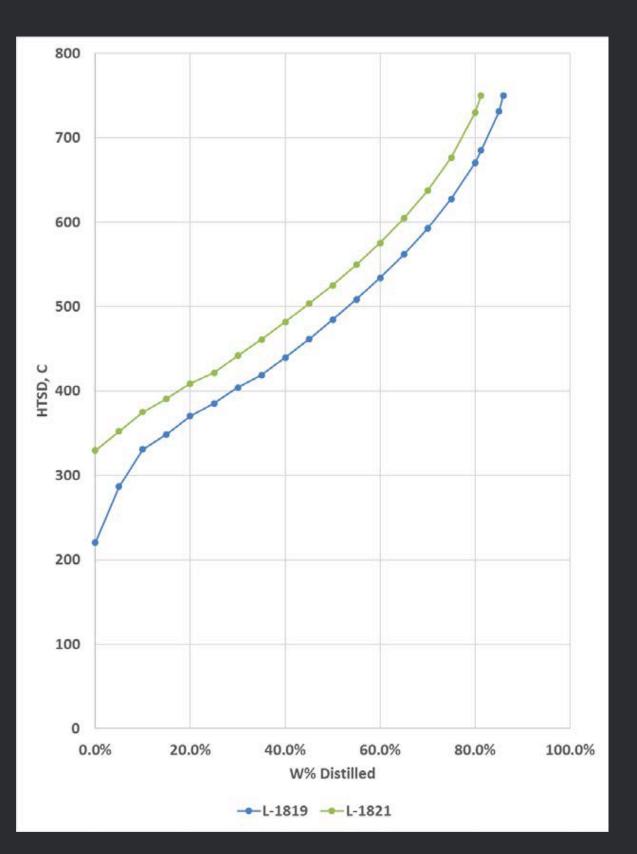


#### **Batch Vacuum Distillation**











#### **Pressure Filter Solids (PFS)**



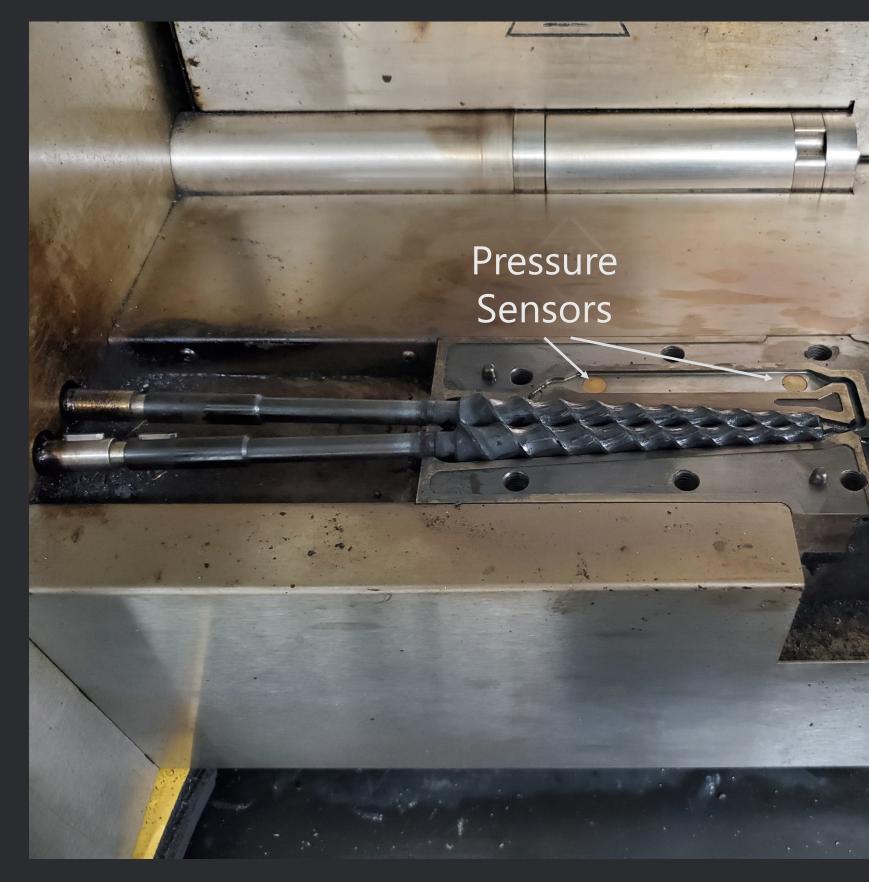
#### Investigating Product Value for REE Extraction



Period	Filter Solids, g
1B	1843
2A	2948
2B	2258
3A	3428
3B	3297
4A	4142
4B	2216
5A	3713
5B	2602
6A	3686
6B	2593
7A	3799
7B	3899
Total	40424



#### **Conversion of Pitch to Mesophase by Ramaco**



#### Pitch recirculates during thermal treatment and is extruded after completion

Carbon Fiber Precursor Pitch from Low-Cost Powder River Basin Coal





Extrusion

Port

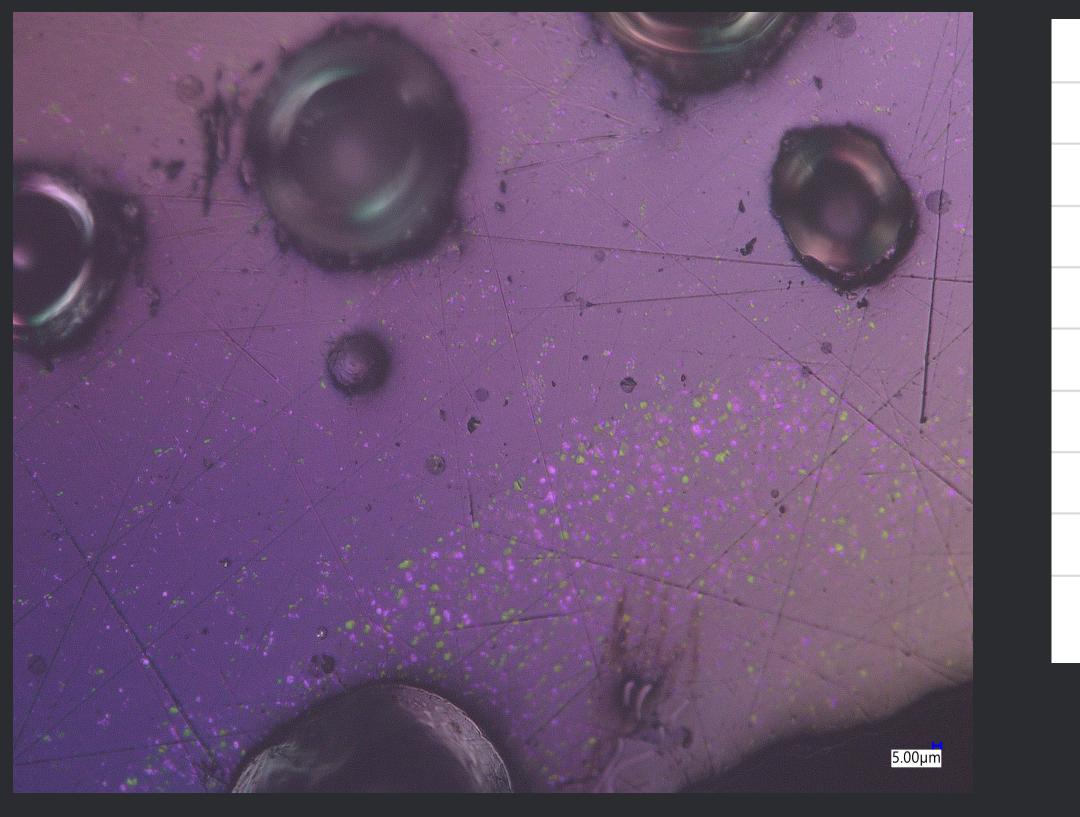
#### **Conversion of Pitch to Mesophase by Ramaco**



#### Added Box for Nitrogen Purge at Inlet and Exit Ports



#### **Conversion of Pitch to Mesophase by Ramaco**

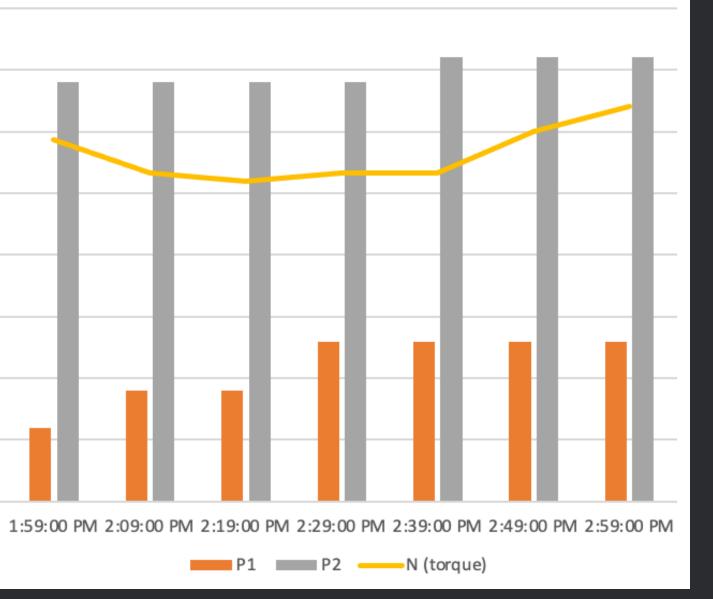


#### Mesophase Formation after 60m at 400C Image 500X

Carbon Fiber Precursor Pitch from Low-Cost Powder River Basin Coal

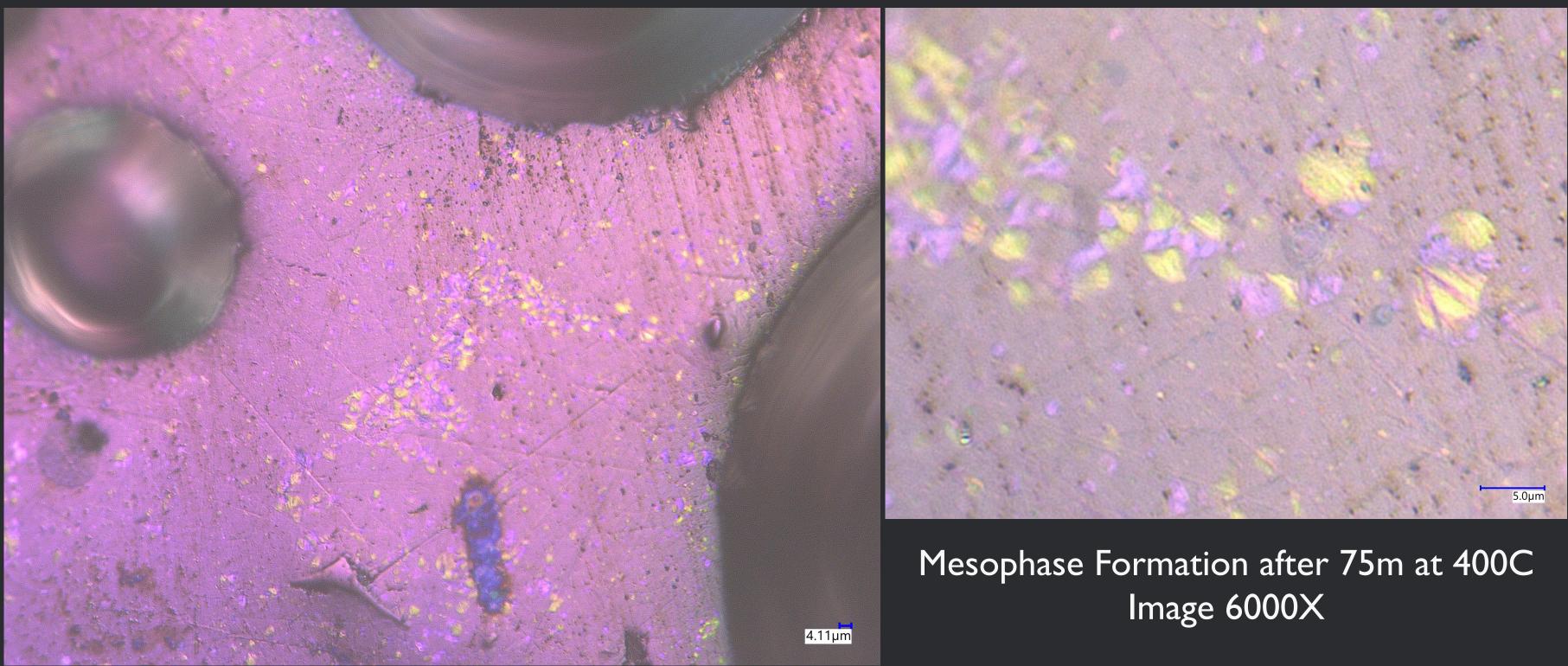


#### Pressure and Torque During Thermal Treatment



# In-line flow pressures and torque recorded during conversion

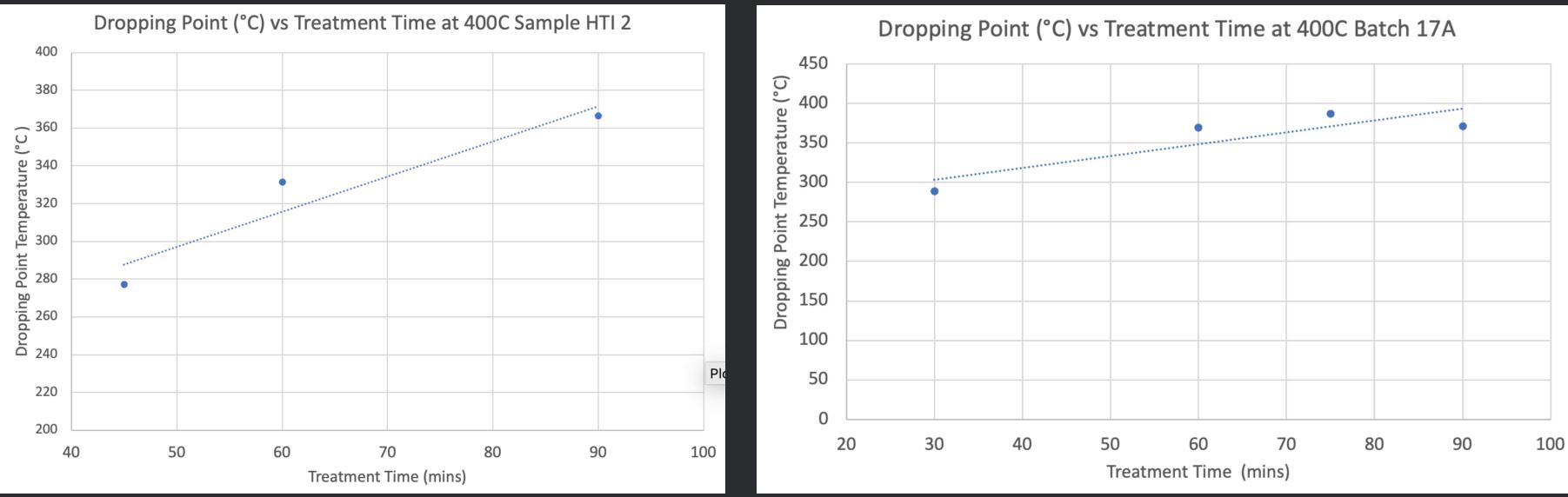
#### **Conversion of Pitch to Mesophase by Ramaco**



#### Mesophase Formation after 75m at 400C Image 500X



#### **Conversion of Pitch to Mesophase by Ramaco**



Dropping Point of Starting Materials. ullet

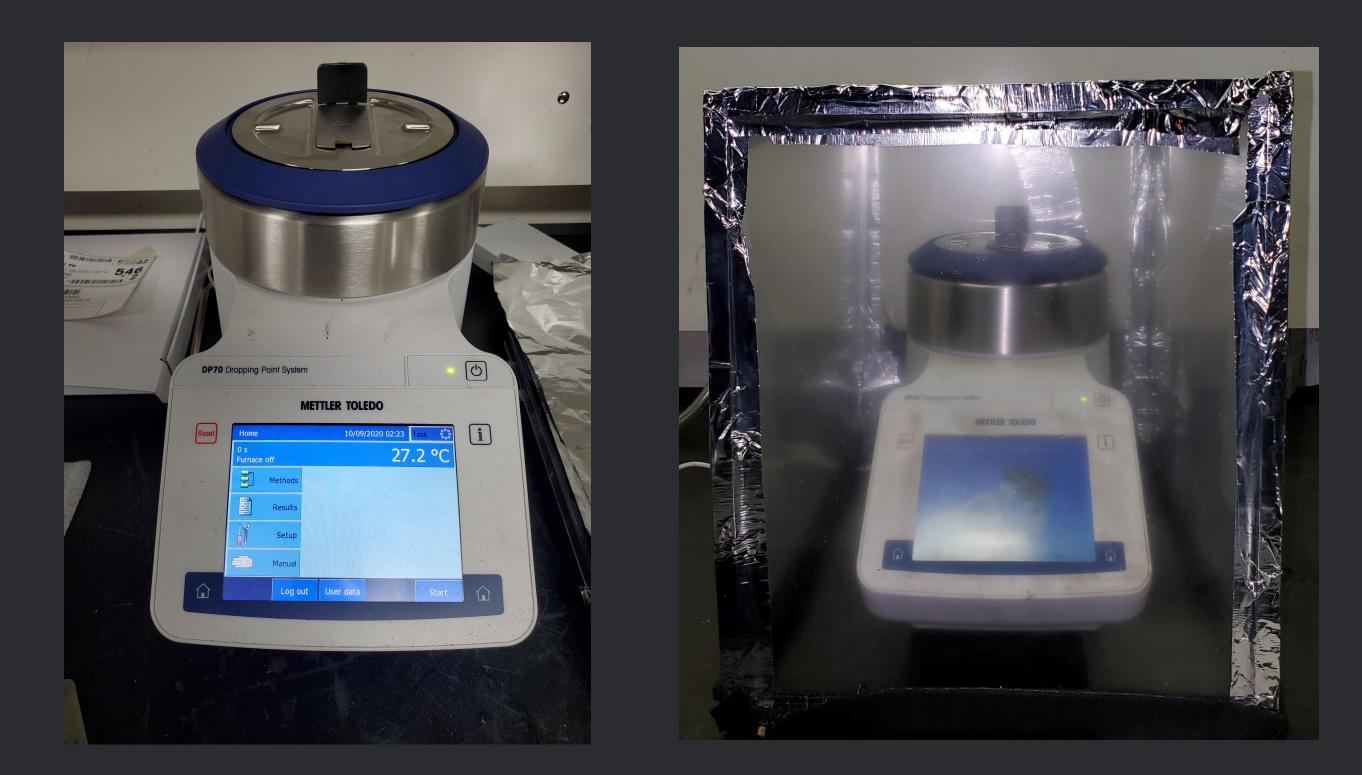
- HTI 2 DP is 114.7°C
- Batch I7A is I44.7°C

- **Observations**
- igodol



Increasing Trends in Dropping Point Large Variability and Two-Phase Behavior at Longer Treatment Times

# **Conversion of Pitch to Mesophase by Ramaco**



Mettler DP70

- Large Variability in Dropping Point
- Observed Oxidation of Pitch Surface

# • Added Cover and Nitrogen Purge on Mettler DP70



#### **Conversion of Pitch to Mesophase by Ramaco**

Scale to larger batches in traditional stirred/sparged reactor

- Produce quantities adequate for filtering and spinning igodol
- Improve consistency and repeatability ightarrow



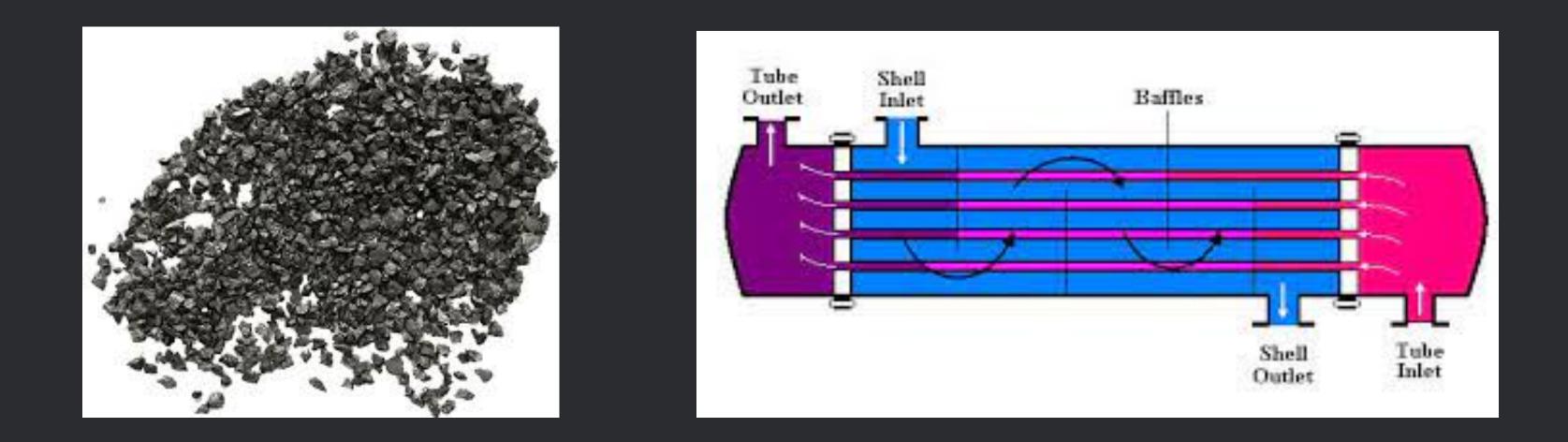
1L Parr Reactor, Gas Entrainment Impeller, and Solids Charging Port (expected delivery 4/30)





#### **Recovery of Liquid Volatiles from Mesophase Reaction**

- Various coal-derived volatile fractions are emitted in the vapor form  $\bullet$ from the mesophase reaction by controlling the pitch composition and process variables
- Volatile composition varies as the reaction progresses ullet
- The volatile recovery system will condense and collect the volatiles ulletand permit volatile fractions to be separated and analyzed at various points throughout the reaction.





#### **Spinning of Fiber by Ramaco**

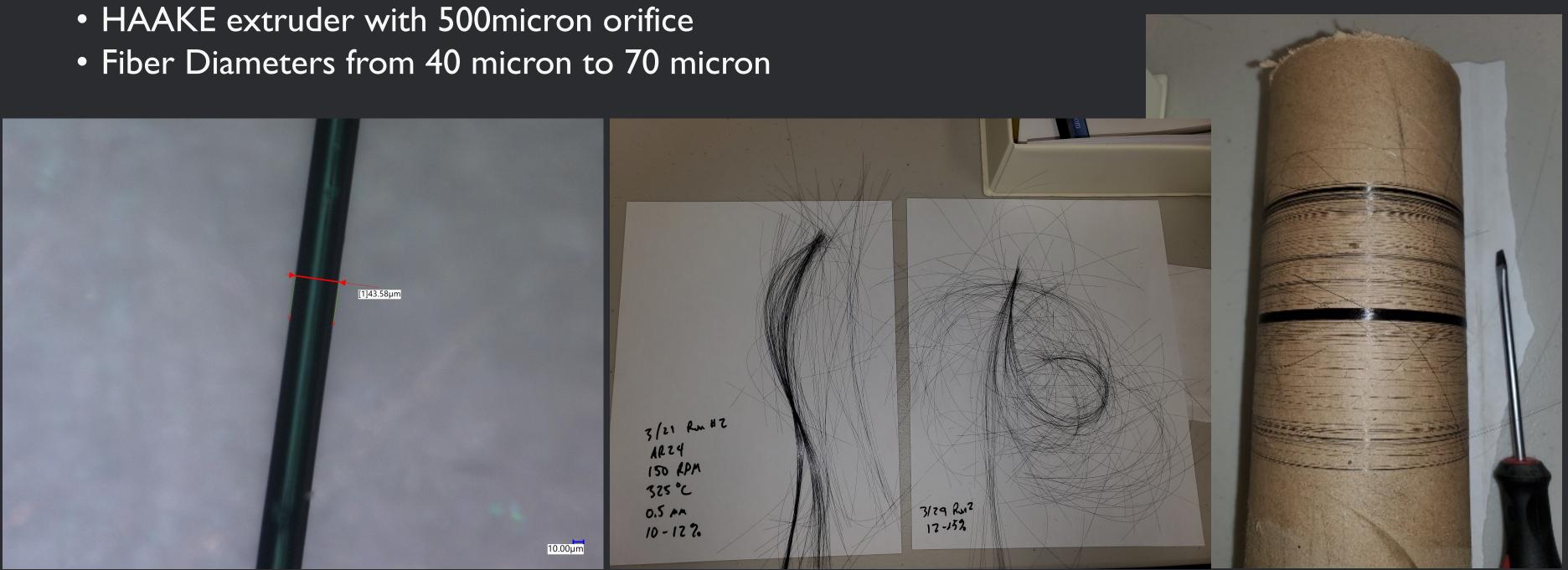


#### HAAKE on Hinged Rack Enables Spinning of 5g Samples



### **Spinning of Fiber by Ramaco**

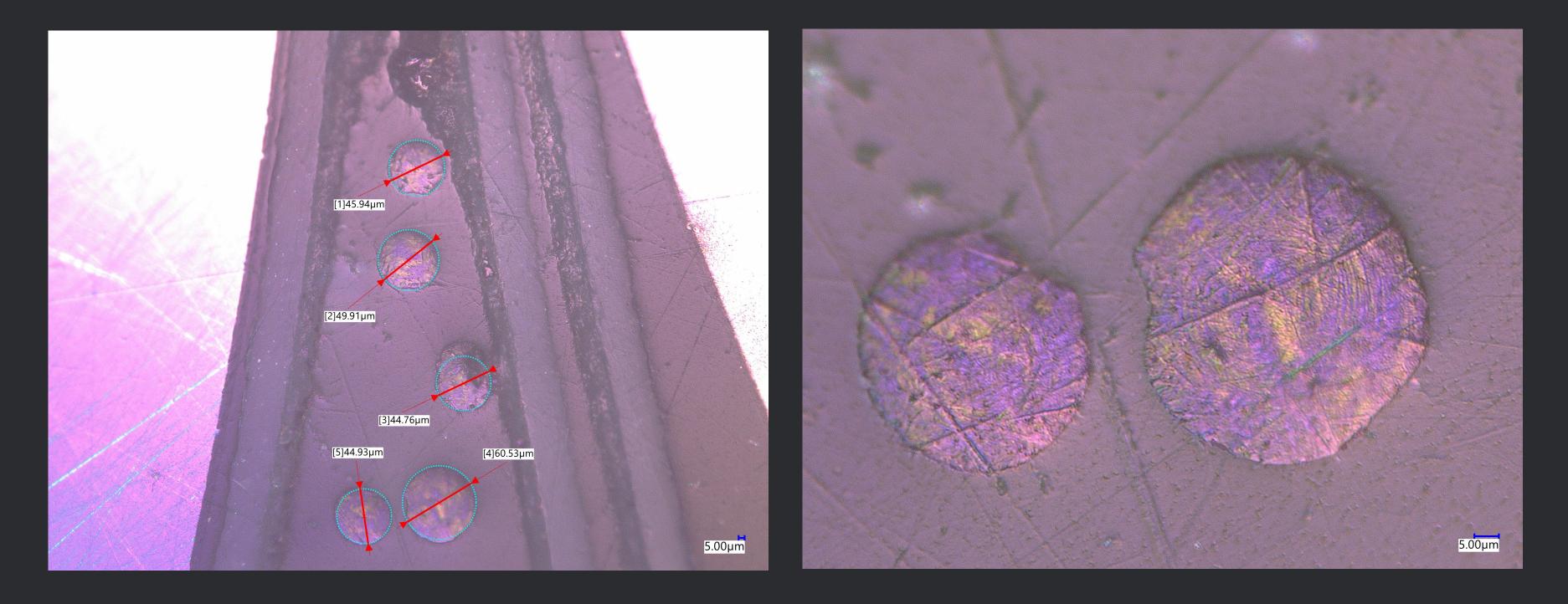
- Fiber Spinning Initiated 3/26
  - Establish Baseline and Verify Equipment
  - Achieved Stable Spinning AR24 Synthetic Mesophase





### Spinning of Fiber by Ramaco

#### Establishing Baseline with Synthetic Mesophase

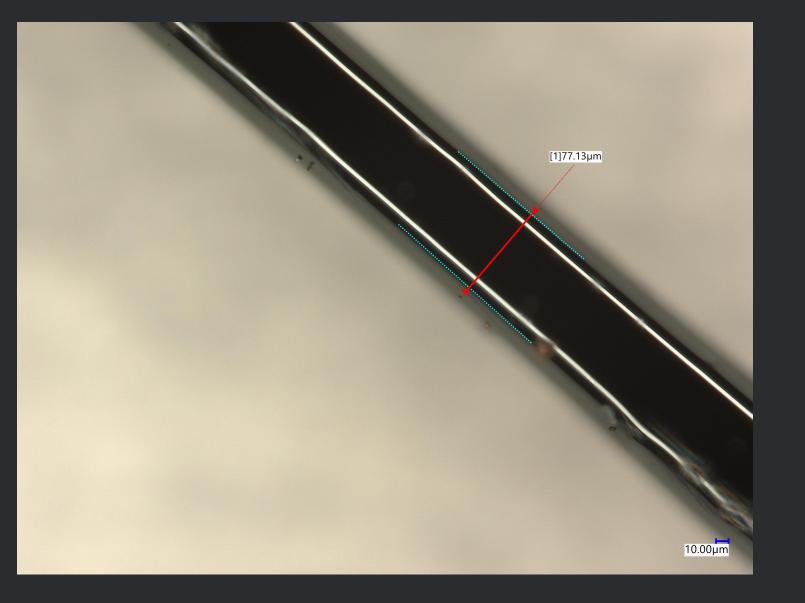


#### AR24 Fibers Spun at 325C AVG DIA 48um Observed Orientation of Mesogens

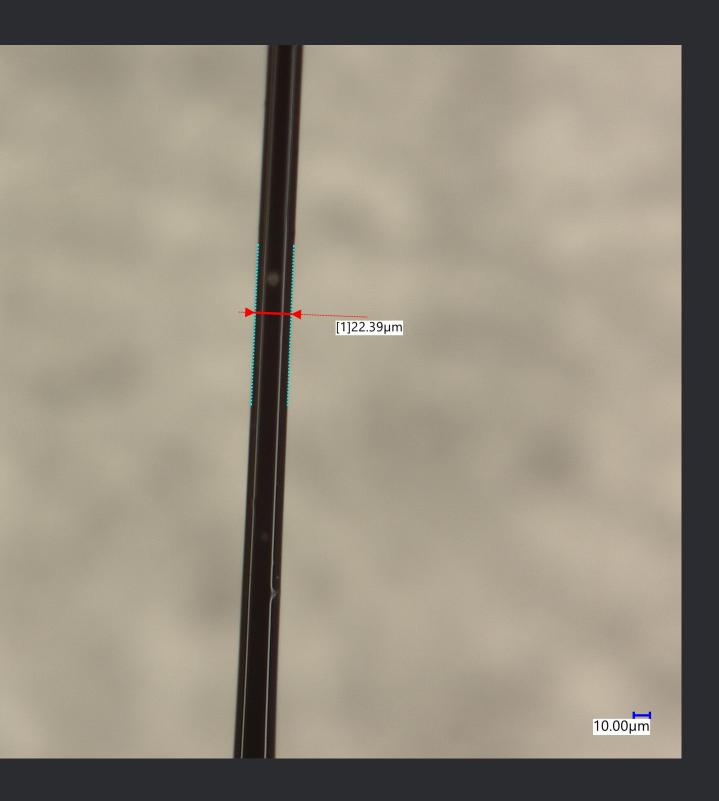


### Spinning of Fiber by Ramaco

- Fiber Spinning HTIVSB As-Received Isotropic Pitch
  - Easy to Spin
  - HAAKE extruder with 500micron orifice
  - Fiber Diameters Observed
    - 77 micron at 50RPM
    - 22 micron at I50RPM

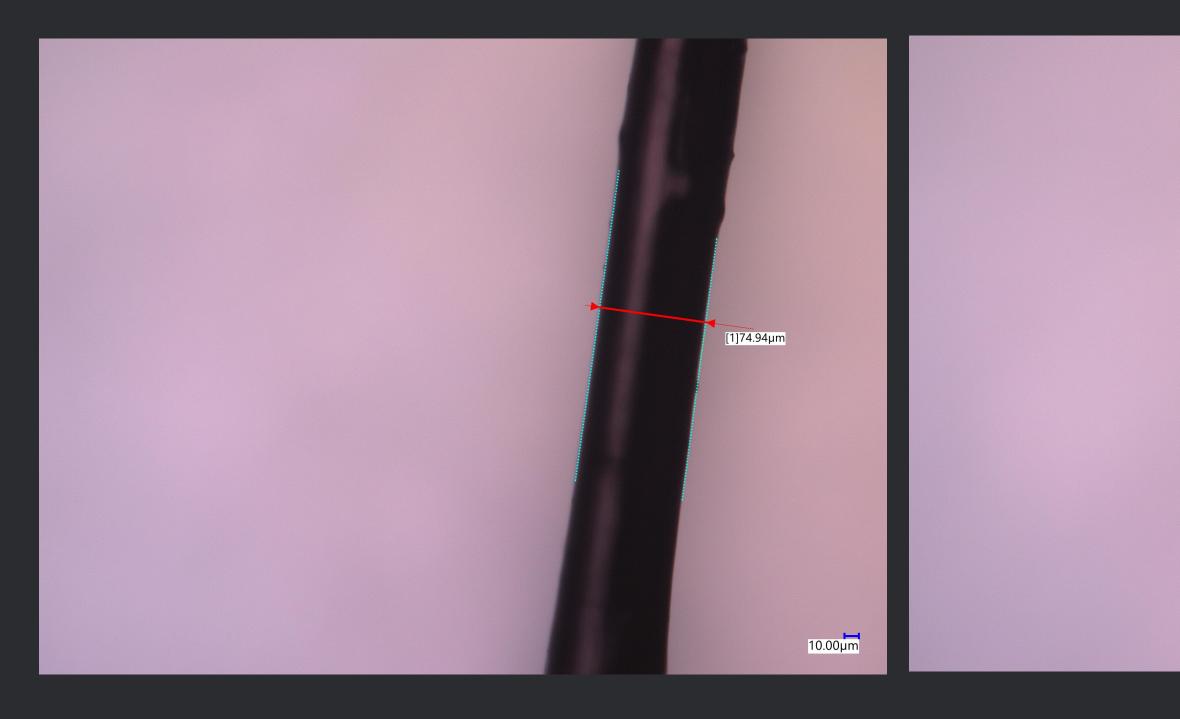






### Spinning of Fiber by Ramaco

- Fiber Spinning Thermally Treated Pitch 60mins at 400C
  - Difficult to Spin due to Clogs
  - HAAKE extruder with 500micron orifice
  - Fiber Diameters Inconsistent Averaged 70microns



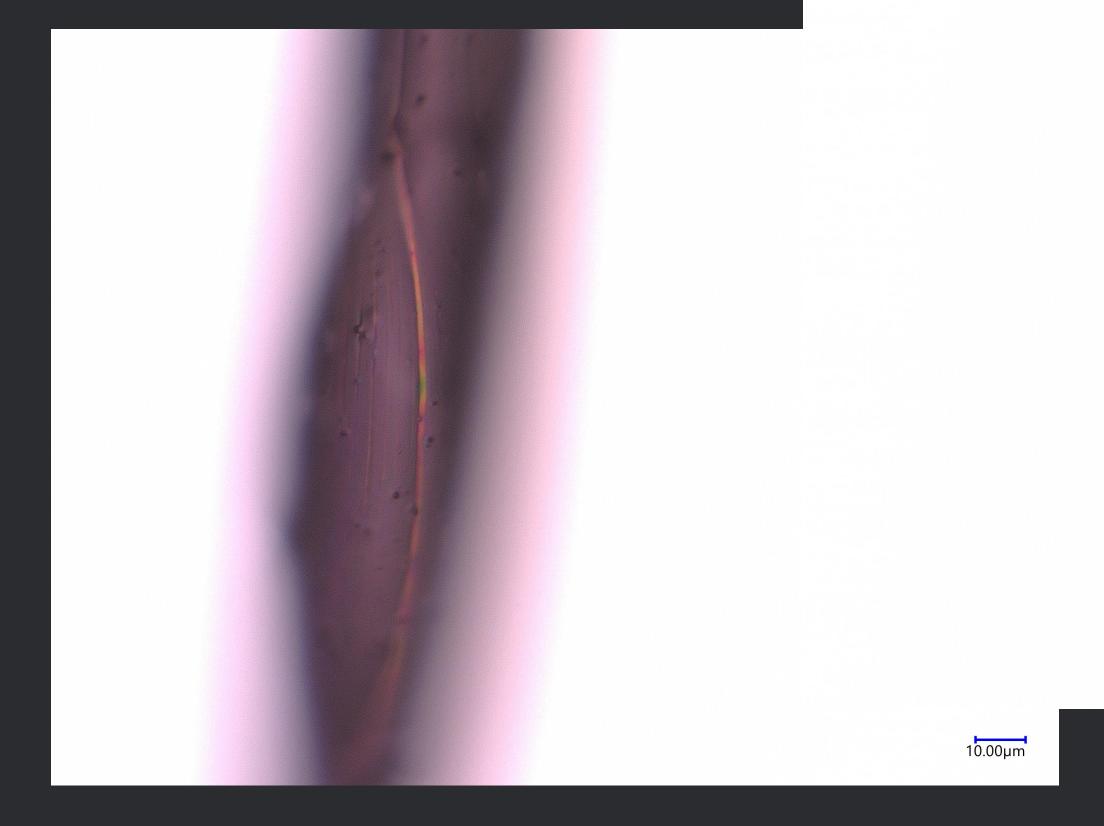




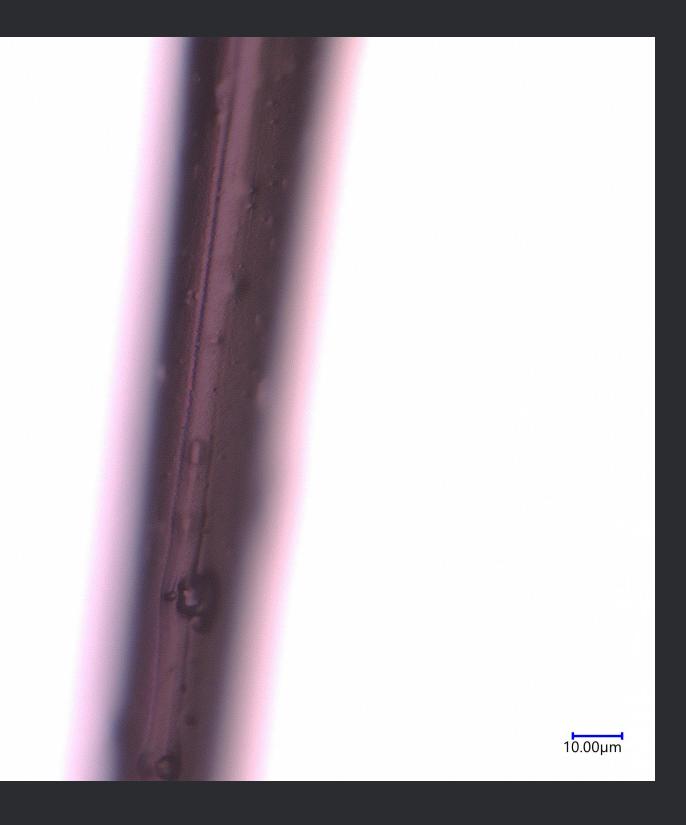
### Spinning of Fiber by Ramaco

• Fiber Spinning Thermally Treated Pitch 60mins at 400C

• Mesophase Observed in Fibers

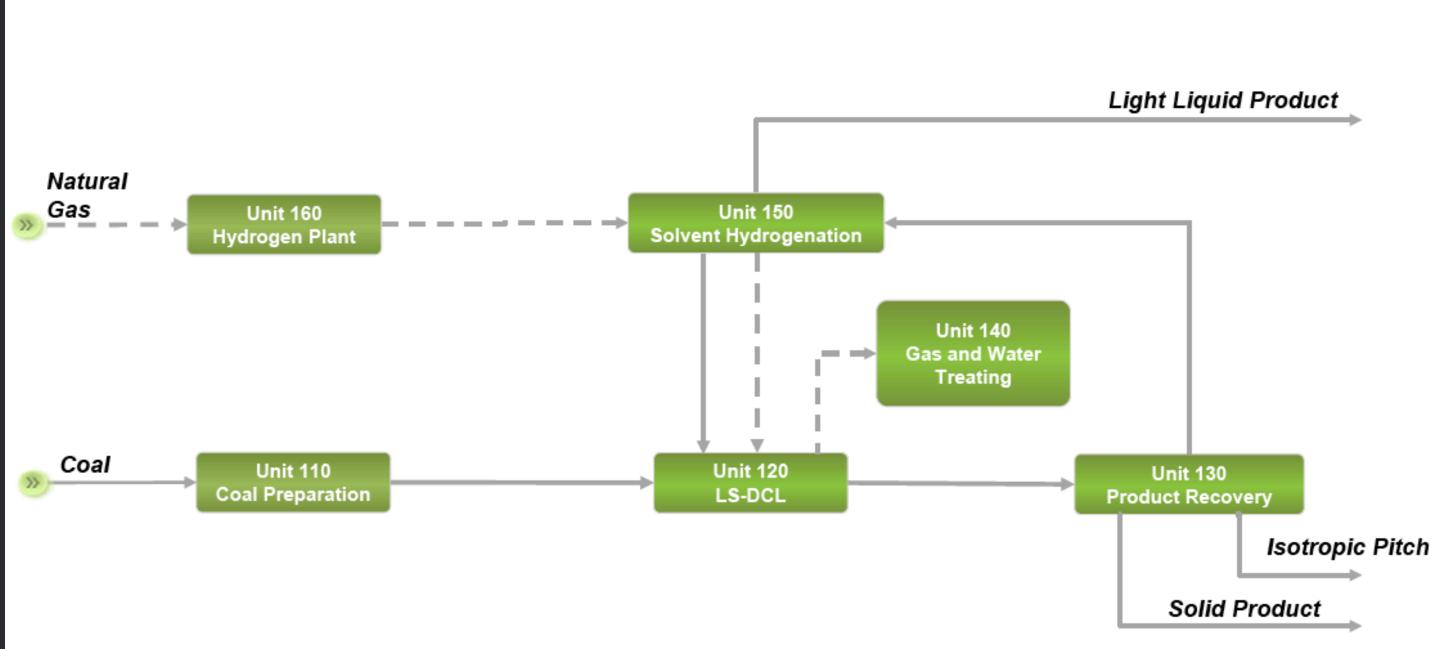




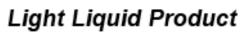


#### Commercialization and Economic Analysis







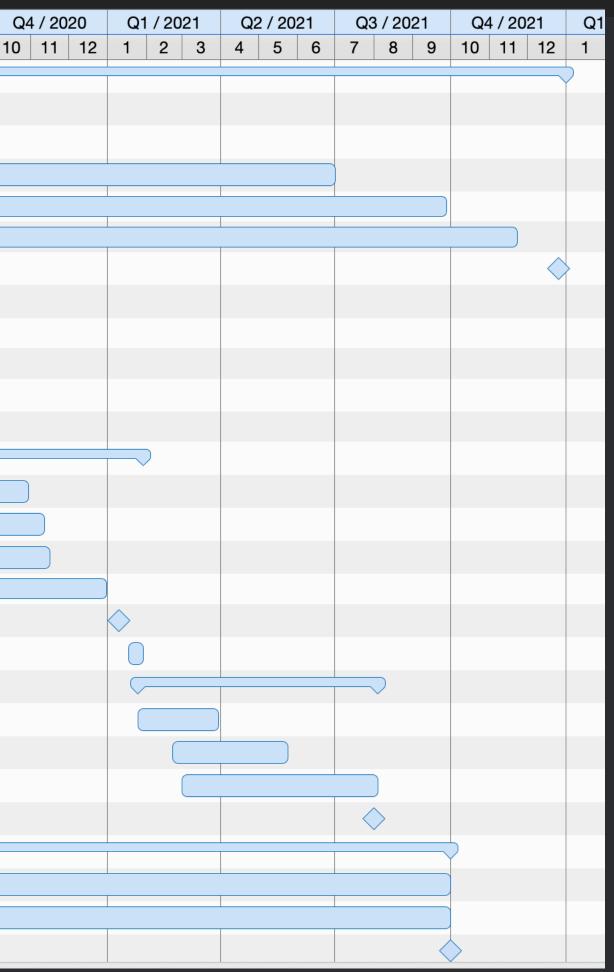




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Fiber from US Domestic Coal	9	10	11	12	1		2 3	4	5	6	7	8	9	
▼ Task 1 Project Management														
Finalize Teaming Agreement between Ramaco and Sub-Recipient														
Update Project Management Plan			$\diamond$											
Quarterly Reports														
► Topical Reports														
Briefings/Technical Presentations														C
Final Report														
▼ Task 2 Coal/Conversion Screening								$\rightarrow$						
Subtask 2.1 Extraction/Shipping/Recieving of Coal														
Subtask 2.2 Preparation of Coal														
Milestone 2 Completion of Task 2							$\diamond$							
Task 2 > Task 3 Decision Planning Point								þ						
Task 3 Feedstock Production														
Subtask 3.1 LSDCL Processing														
Subtask 3.2 Liquid Distillation to Isotropic Pitch														
Subtask 3.3 Delivery of Pitch to Ramaco														
Subtask 3.4 Conversion of Isotropic Pitch to Mesophase														C
Milestone 3 Completion of Feedstock Production														
Task 3 > Task 4 Decision Planning Point														
▼ Task 4 Carbon Fiber Production														
Subtask 4.1 Carbon Fiber Spinning Preparations														
Subtask 4.2 Set-up of Mesophase to Fiber Forming Equipment														
Subtask 4.3 Carbon Fiber Formation Testing														Γ
Milestone 4 Complete Carbon Fiber Formation Testing														
▼ Task 5 Commercialization Plan								<b></b>						+
Subtask 5.1 Determination of Overall Process Yields														
Subtask 5.2 Integrated System Capital Cost Estimation														1
Milestone 5 Completion of Feasibility Assessment														

# COVID-19 Impacts March-May 2020, Equipment Delivery Delays Revised Schedule for Task 4 Extended to July 31





# Conclusions

- Produced over 100kg of high-quality isotropic pitch.
- Much lower cost than PAN and more ecologically sound (greener)
- Demonstrated mesophase conversion at acceptable yields.
- Demonstrated initial fiber production with good draw down ratios.



# opic pitch. ogically sound (greener) cceptable yields. good draw down ratios.

Thank You



www.ramacocarbon.com

Acknowledgements

RAMACO: Charlie Atkins Grant Hazle Luke Adsit

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DOE PM: Mike Fasouletos

