

# Energy-Efficient Waste Heat Coupled Forward Osmosis for Effluent Water Management at Coal-Fired Power Plants

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N. Rajagopalan, Ph.D., UIUC

Partners: Trimeric Corporation, IL Power Plant

Project Manager: Mr. Charles Miller

Project: FE-0031551



U.S. DEPARTMENT OF  
**ENERGY**



NATIONAL  
ENERGY  
TECHNOLOGY  
LABORATORY

## Goals

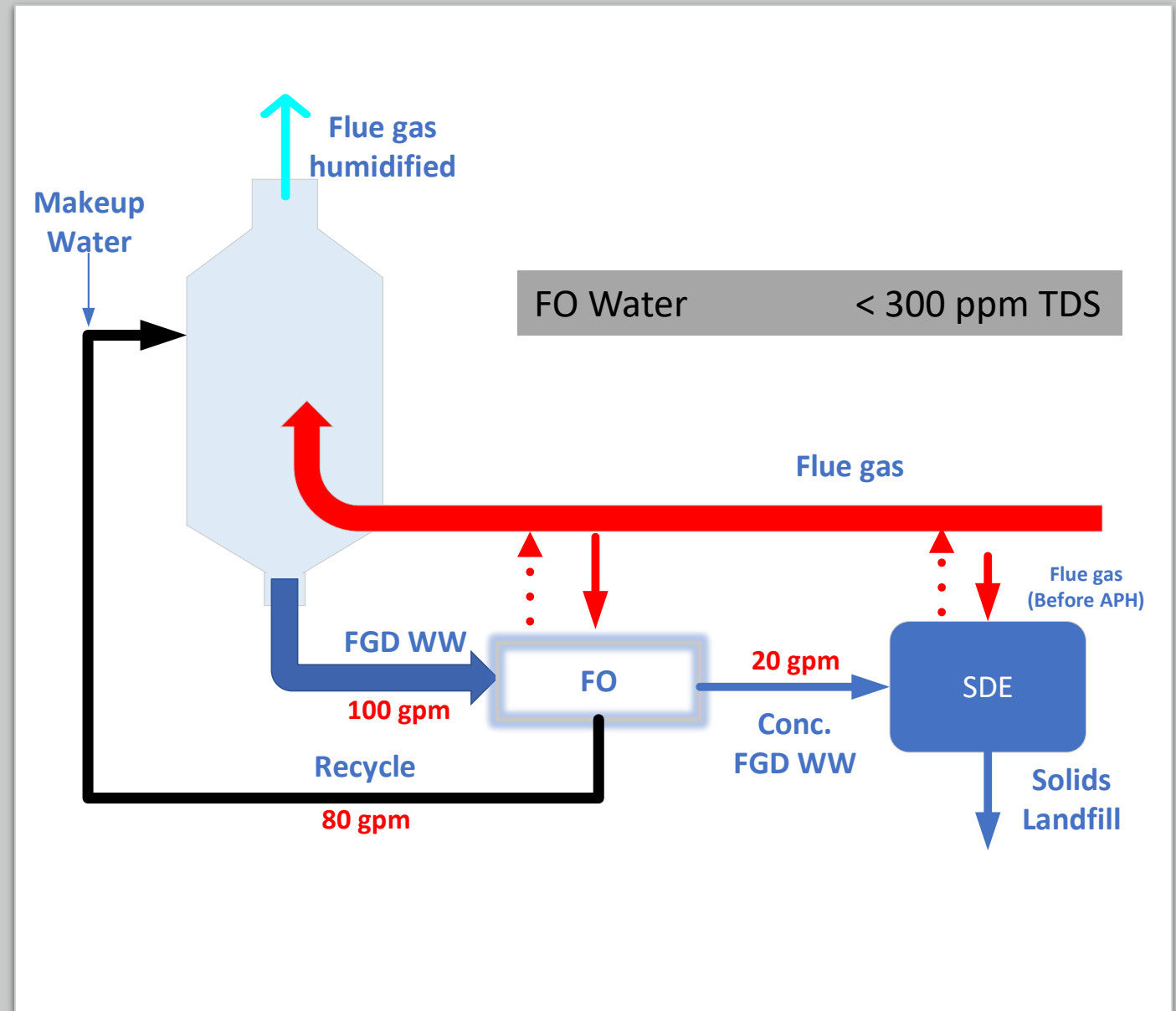
- Recover at least 50% water from problematic power plant effluents such as FGD scrubber blowdown for reuse using FO
- Thermal Energy (200 kJ/kg)
- Electrical Energy (< 3.6 kWh/m<sup>3</sup>)

## Achievements

- ✓ **80% achieved /90% possible**
- ✓ **Achieved**
- ✓ **2.2 kWh/m<sup>3</sup>**

# DOE Alignment

- DE-FOA-0001686/ AOI 5
  - innovative effluent water management
  - developing water treatment and reuse methods that employ low energy or waste heat solutions
  - reduce overall treatment requirements



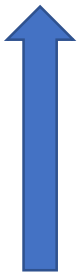
# Summary

- Met project goals of low energy requirement, waste heat utilization and reuse of power plant effluent
- FO can treat FGD wastewater with minimal pretreatment to achieve wastewater volume reduction
- Currently limited to 80% water recovery to avoid gypsum precipitation
- 90% reduction in wastewater volume possible with intermediate gypsum desaturation/other process variations
- Process scale-up and testing in power plant required to further advance TRL level; reduce uncertainties (e.g., membrane lifetime)
- Membrane residuals treatment costs can and must be reduced further- several pathways exist to achieve mid-single digit \$/m<sup>3</sup> total treatment costs

## This Project

5

Laboratory scale,  
similar system validation  
in relevant environment

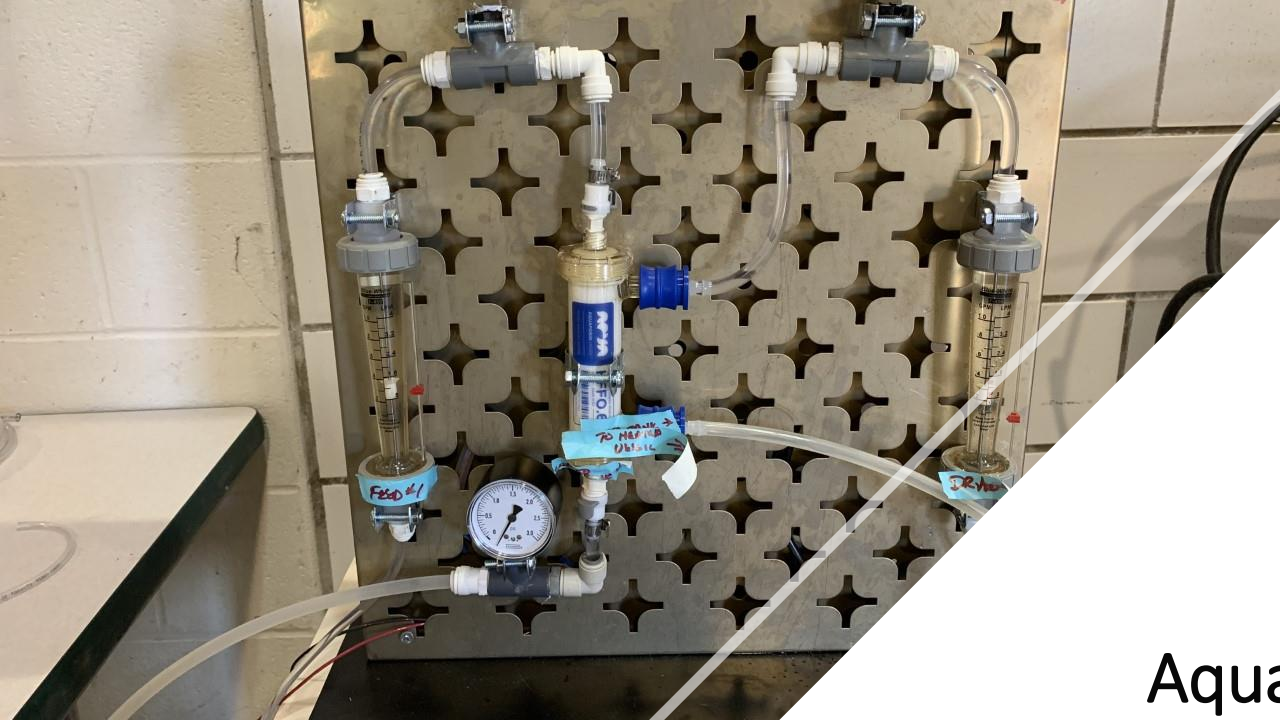


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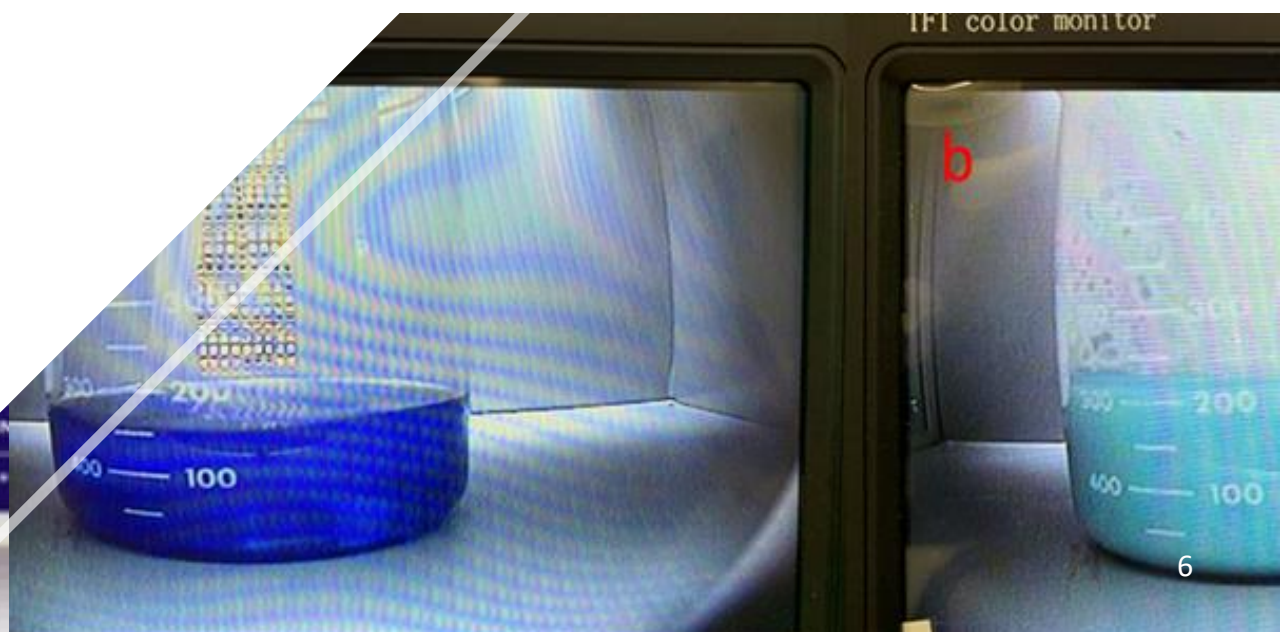
Research to prove  
feasibility

## Next Steps

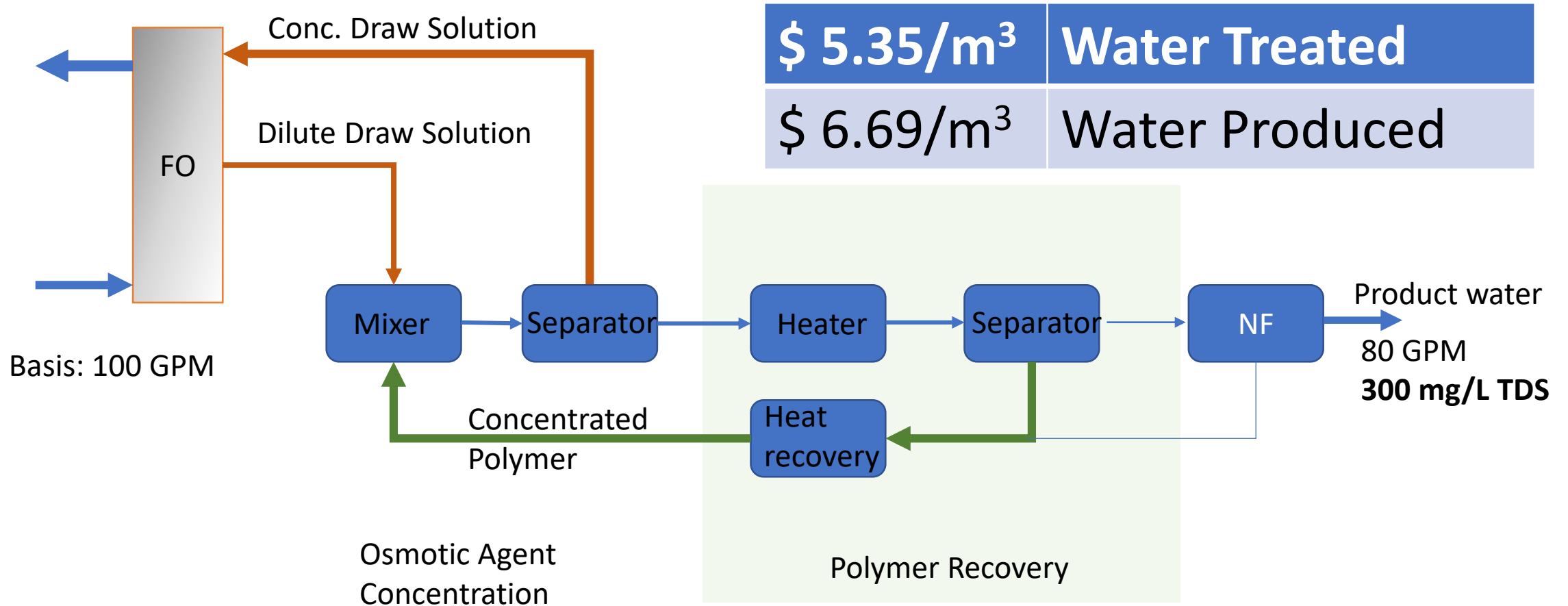
- Long-term membrane module stability testing;  
3 modules/3 – 6 months
- Test scaled-up system at power plant (~1 gpm)
- Conduct proof-of-concept of very ***low energy/low-cost residuals management approach***



## Aquapod Process



# FO Lifetime Cost Estimates



Total Plant Costs	\$7,361,542
PEC	\$1,372,398

# Operating Cost Estimates

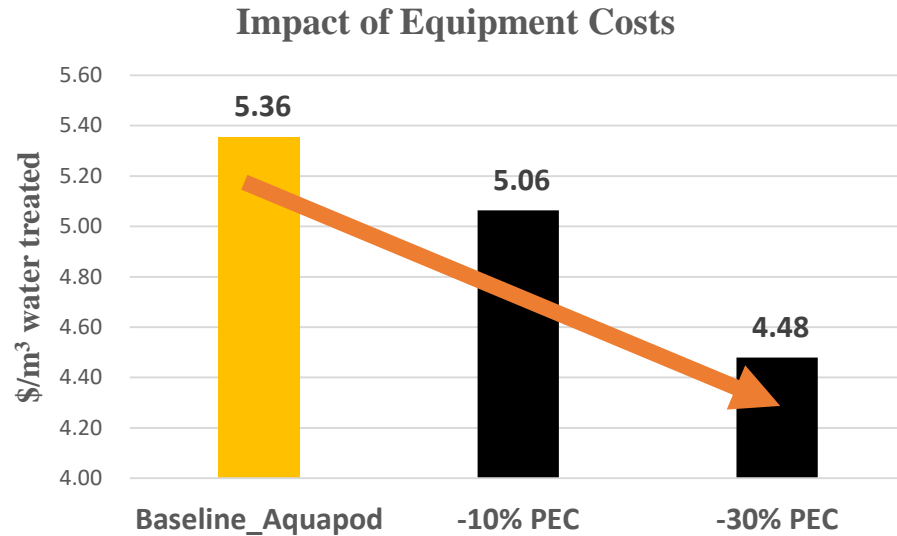
Variable O&M Costs

<b>\$ 1.50/m<sup>3</sup></b>	<b>Water Treated</b>
\$ 1.88/m <sup>3</sup>	Water Produced

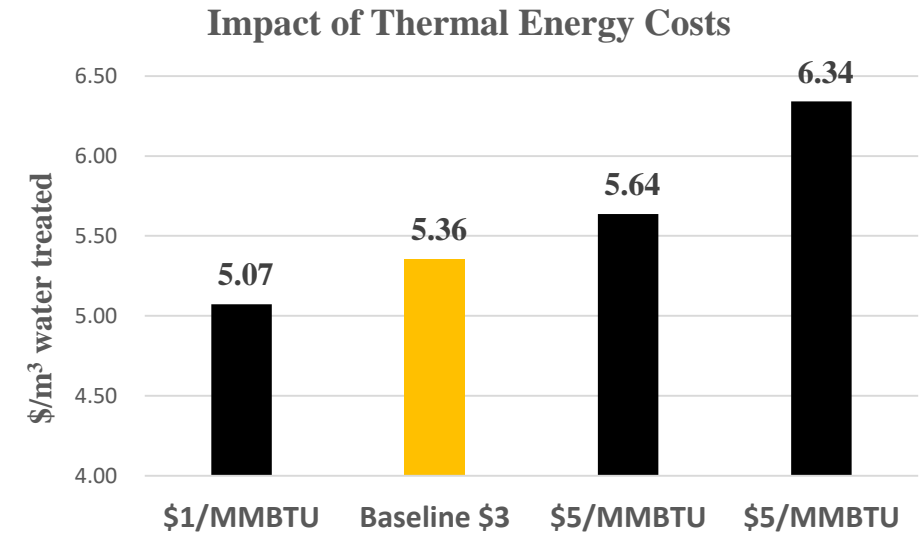
Fixed O&M Costs

<b>\$ 1.87/m<sup>3</sup></b>	<b>Water Treated</b>
\$ 2.34/m <sup>3</sup>	Water Produced

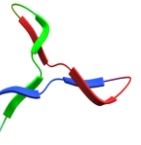




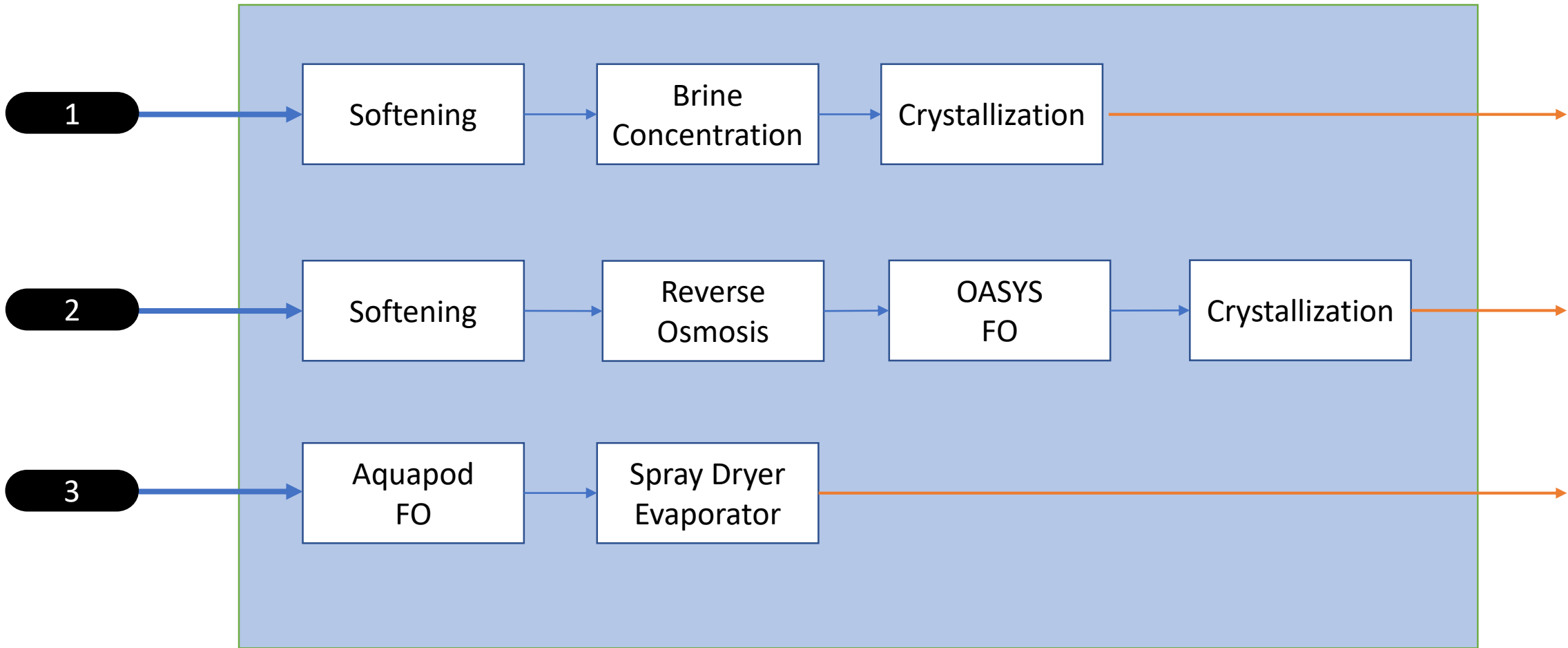
- -30% PEC reduction target for second iteration
- Cost reductions possible due to derisking, lower FO costs, engineering optimization



- FO Membrane Costs of \$75/m<sup>2</sup> HF in <1 year (\$25/m<sup>2</sup> available NOW in different chemistry)



# Membrane Residuals Treatment/ZLD



1, 2, 3

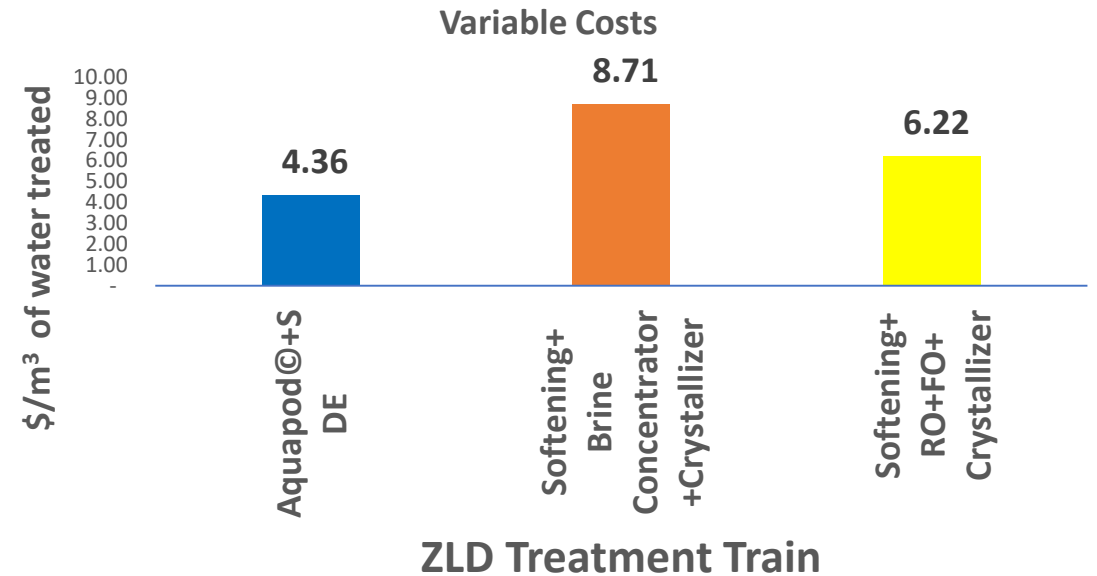
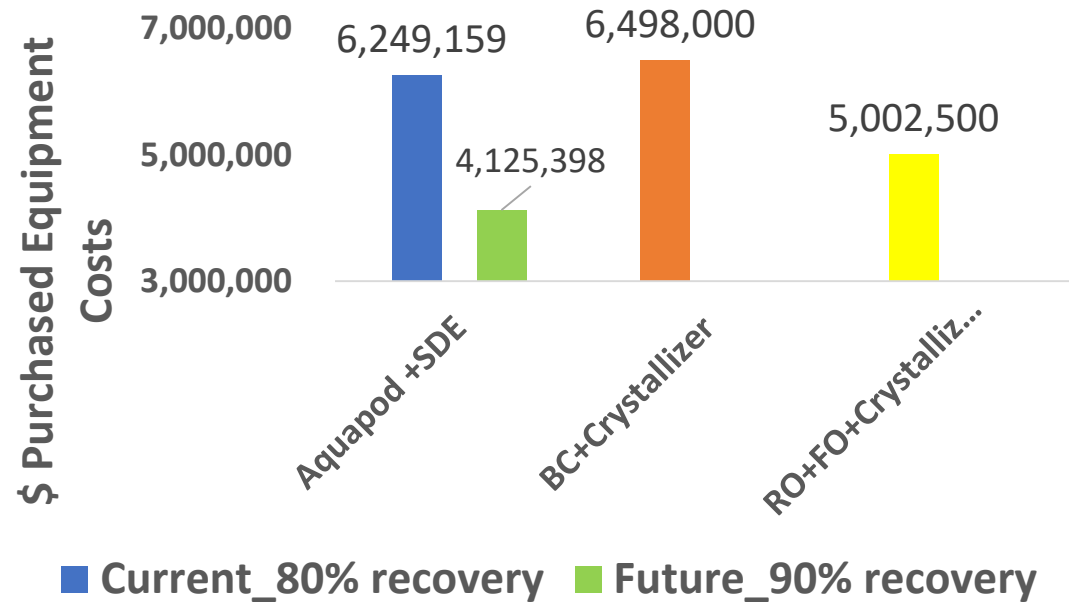
FGDWW desaturated and treated to remove metals, Hg, etc..

## ZLD Treatment Train

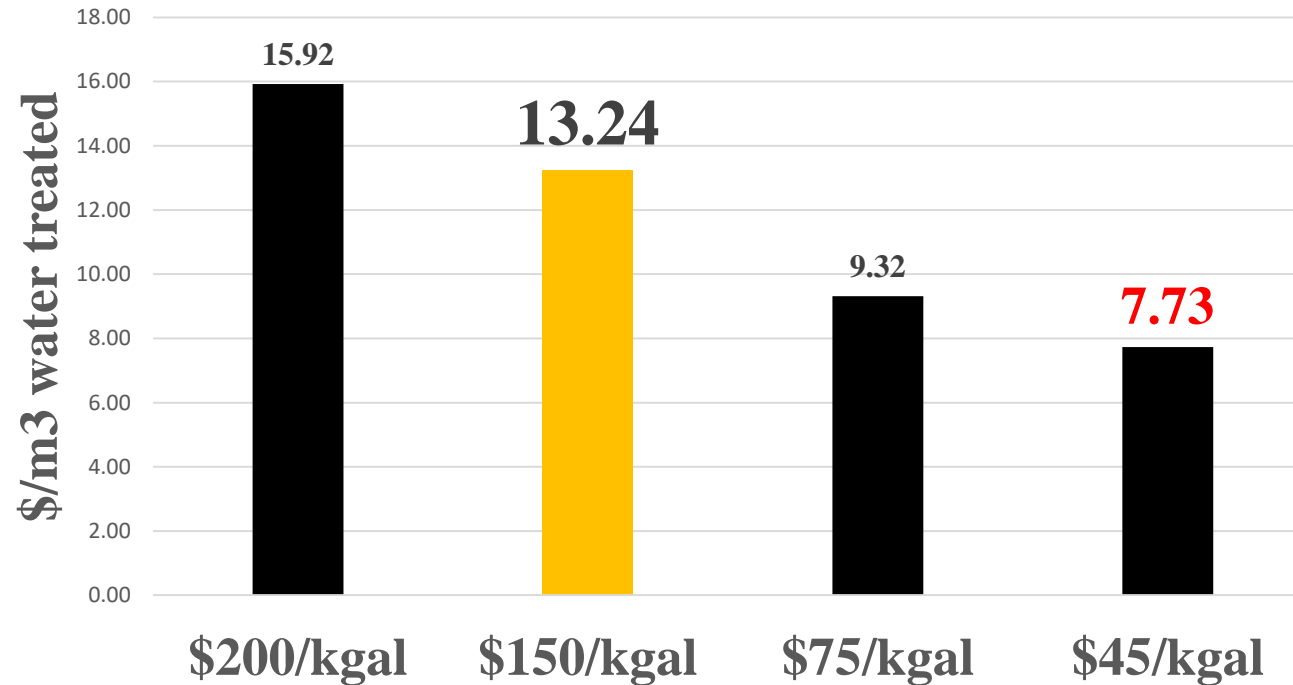
## FOR CURRENT PROCESS FLOWSHEET

**Aquapod+SDE Variable Costs Are LOWER**

**But Capital Costs are INTERMEDIATE at 80% recovery & LOWER at 90% recovery**



## Impact of Residuals Treatment Costs on Overall Costs



~\$8/m<sup>3</sup> achievable in power plant at current Aquapod costs with new residuals treatment approach in development at ISTC; Simulations completed- prototype design in progress.

For reference, PP spends between \$4-\$9/m<sup>3</sup> currently for discharge.

MVC+crystallizer costs in literature are ~\$20/m<sup>3</sup>

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# Team

## UIUC

- K C OBrien
- Chinmoy Baroi
- Martina Del Cerro
- Sriraam Chandrasekaran
- DongHao Chen
- Mariah Muhsinah
- Vinod Patel
- John Scott
- Xuesong Zhang

## Trimeric

- Katherine Dombrowski
- Ray McKaskle
- Kevin Fisher

## IL PP

- P.J. Becker
- Brandon Powell
- Eric Staley