



Pacific  
Northwest  
NATIONAL LABORATORY

# Pressure Driven Oxygen Separation

David Reed, Kerry Meinhardt, Jon Helgeland,  
Greg Coffey, and Pepa Matyas

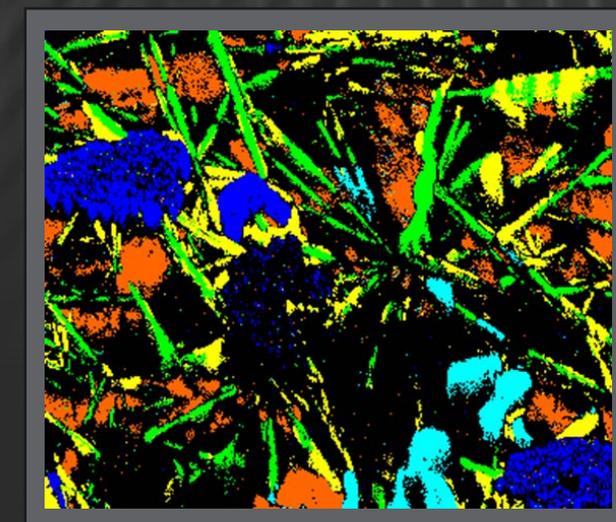
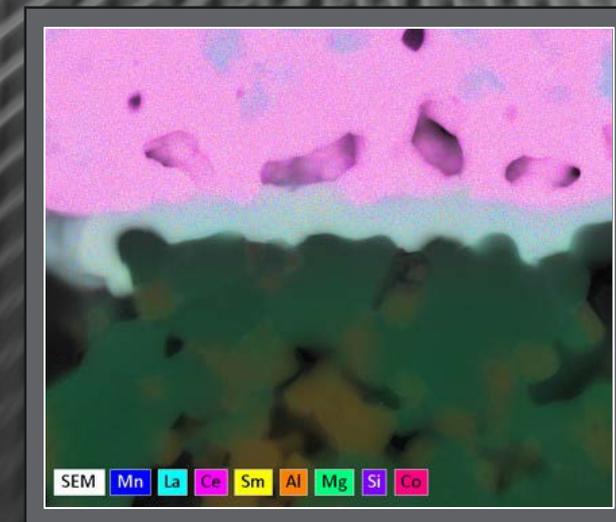
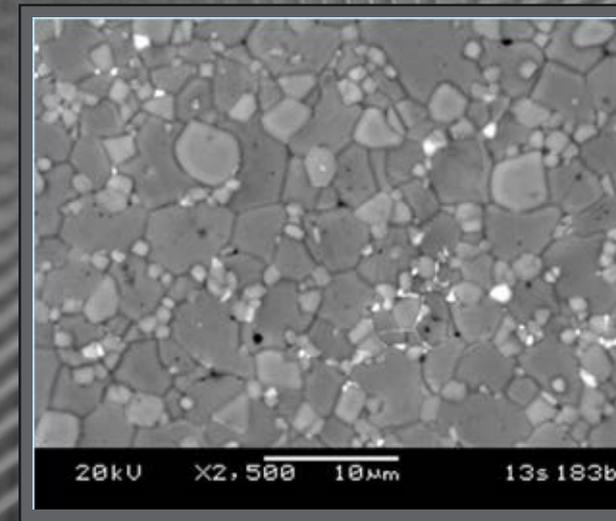
Pacific Northwest National Laboratory  
Richland, WA

2020 Gasification Project Review Meeting

September 2, 2020



PNNL is operated by Battelle for the U.S. Department of Energy



# Pressure Driven Oxygen Separation

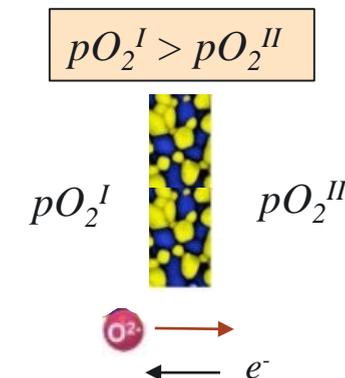
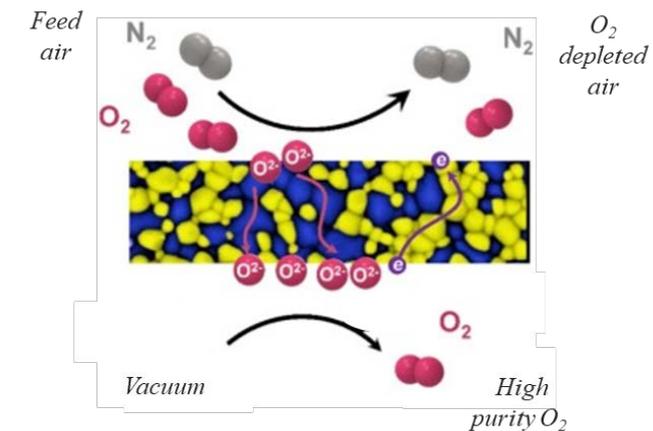
## Outline

- Project Description and Objectives
- Project Background
- Critical Factors for Project Success
- Project Update
- Next Steps

# Project Description and Objectives

*The overall goal of the proposed effort is to develop a small scale, modular air separation unit providing 10-40 tons/day of high purity oxygen to a 1-5 MW gasifier at low cost and high efficiency*

- Mixed conducting two phase material capable of separating oxygen at 700-800°C.
- Planar membrane/support structure
- Utilize the difference in oxygen partial pressure across the membrane to drive oxygen from air, no electrical energy needed for oxygen separation



# Oxygen Separation Techniques

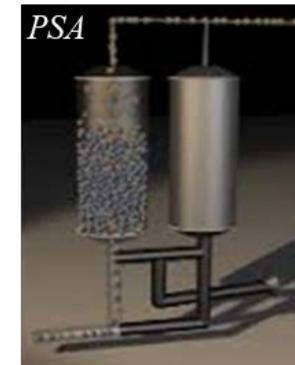
## ➤ Cryogenic Air Separation – mature

- Low energy demand at high capacity (4000 T/day)
- Energy demand very high at low capacity (i.e 10-40 T/day)
- Very high purity (99+)



## ➤ Pressure Swing Adsorption (PSA) – mature

- Economical at lower capacities (i.e. 300-400 T/day)
- Purity ~ 90 - 93%



## ➤ Polymer Membranes – mature

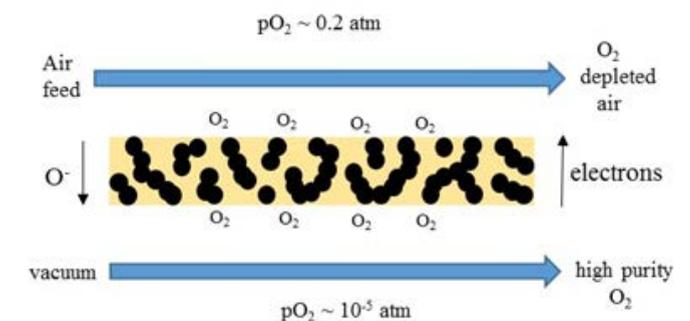
- Low purity (~ 40%)

## ➤ Ceramic Membranes – R&D

- High purity (99+)
- Thermal integration
- Can be economical depending on oxygen permeability
- Examples: OTM (Oxygen Transport Membrane)



ITM (Ion Transport Membrane) 

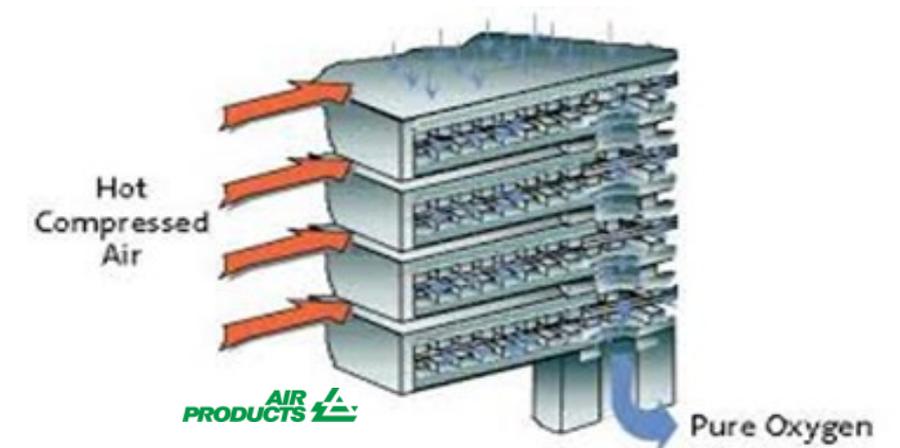


# Proposed Ceramic Membrane Technologies

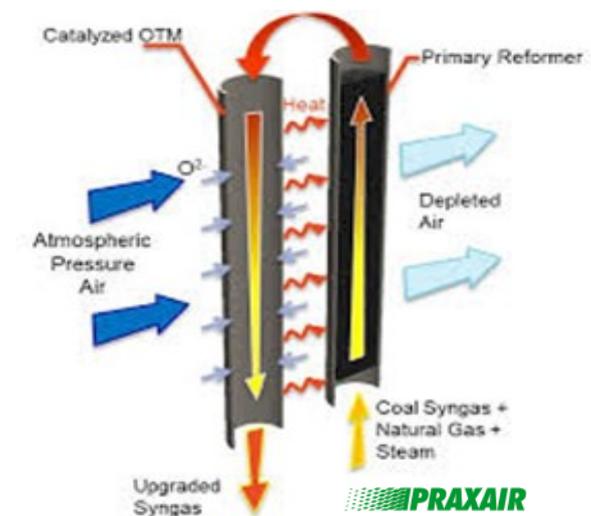
## Planar vs Tubular Design

- Ease of manufacturing
- High surface area
- Increased sealing surface area
- Lower/medium temperature (700-800°C)
- Two phase composite membrane ( $\sigma_i$  and  $\sigma_e$ )
- SOFC design experience at PNNL

### *Planar Design*



### *Tubular Design*



# Proposed Ceramic Membrane Technologies

## *Bilayer Structure*



### *Composite membrane*

- Dense
- High  $\sigma_i$  and  $\sigma_e$
- Compatible with glass seal
- Inexpensive fabrication
- No electrodes

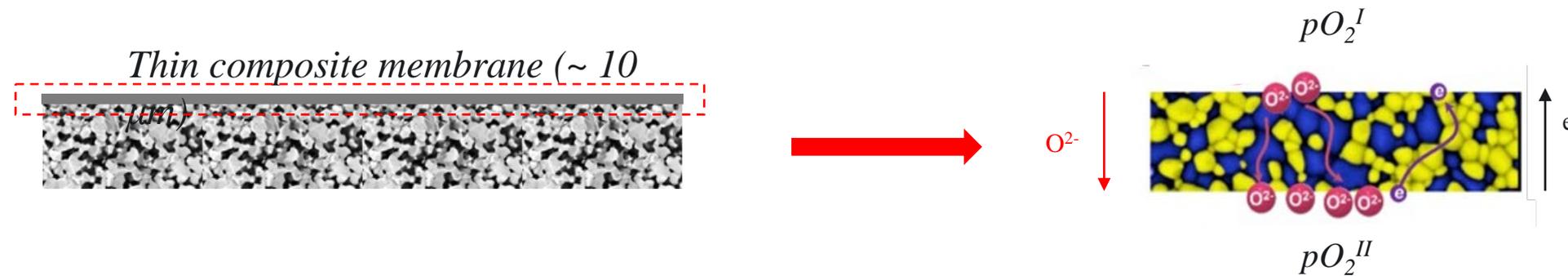
### *Porous Support*

- ~ 50% dense
- TEC match to membrane
- Mechanical integrity
- Co-fired w/ membrane

*Design will leverage SOFC stacks developed at PNNL*

# Proposed Ceramic Membrane Technologies

## Composite Membrane

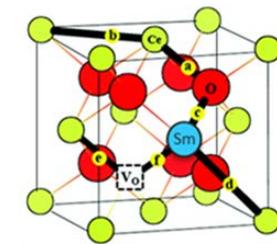


- Two phase composite ( $\sigma_i$  &  $\sigma_e$ )
- Similar TEC
- Limited interaction during firing
- High  $\sigma_i$  phase
- Sufficient  $\sigma_e$  phase
- Compatible with glass seal

### Material Selection

#### Ionic Conductor

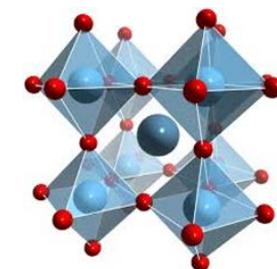
- Doped  $\text{CeO}_2$



Fluorite structure

#### Electronic Conductor

- Doped  $\text{LaMnO}_3$
- Doped  $\text{LaFeO}_3$



Perovskite

# Proposed Ceramic Membrane Technologies

## Composite Membrane O<sub>2</sub> Permeability/Flux Calculations

	Case 1	Case 2	
Ionic conductivity:	0.0233	0.05	S/cm
P(O <sub>2</sub> ) <sub>1</sub> :	0.2	0.2	atm
P(O <sub>2</sub> ) <sub>2</sub> :	1.00E-04	1.00E-04	atm
Temp (°C):	700	800	
Temp (K):	973	1073	
Thickness (um):	10	10	
Thickness (cm):	0.001	0.001	
Flux (A/cm <sup>2</sup> ):	3.71	8.78	
Flux (moles O <sub>2</sub> /cm <sup>2</sup> -s):	9.62E-06	2.28E-05	
Flux (grams O <sub>2</sub> /cm <sup>2</sup> -s):	3.08E-04	7.28E-04	
Flux (grams O <sub>2</sub> /cm <sup>2</sup> -h):	1.11	2.62	
Flux (grams O <sub>2</sub> /cm <sup>2</sup> -day):	26.59	62.93	
Flux (lbs O <sub>2</sub> /cm <sup>2</sup> -day):	5.86E-02	1.39E-01	
Pounds of oxygen required/day:	20000	20000	
Total cell area required (cm <sup>2</sup> ):	341155.97	144162.40	
Cell area(cm <sup>2</sup> ):	420	420	
# of cells required:	812.28	343.24	
Cells/stack:	100	100	
# of stacks required:	8.12	3.43	

### Input Parameters

- $\sigma_i$
- $pO_2^I$  and  $pO_2^{II}$
- Temperature
- Membrane thickness
- lbs. of oxygen/day
- Cell area
- Cells/stack

### Output Value

→ # of stacks required

*# of stacks appears to be very reasonable for a 10 ton/day modular ASU*

# Proposed Ceramic Membrane Technologies

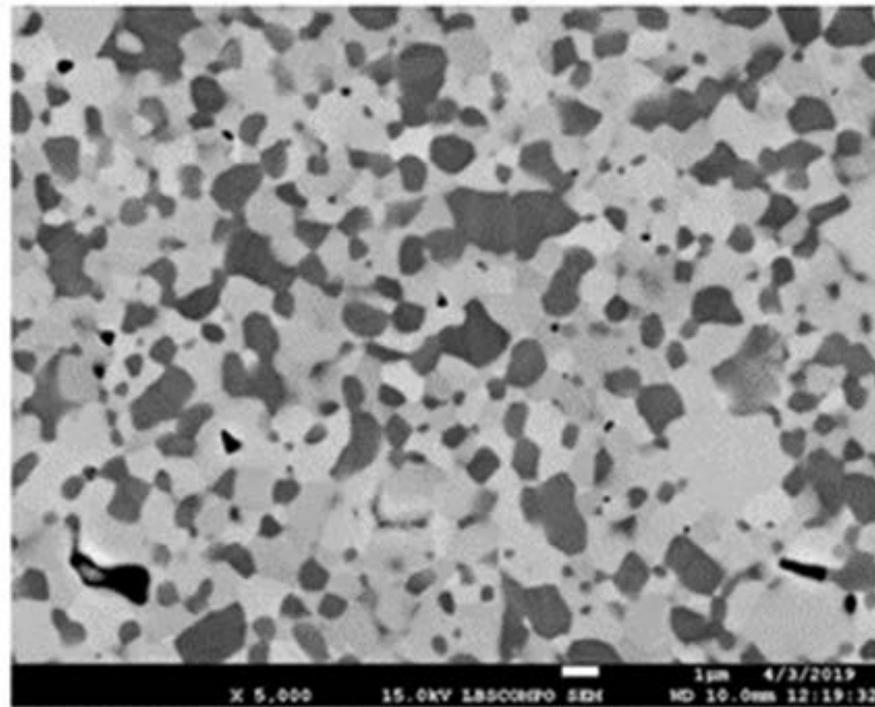
## *Factors Critical for Project Success*

- **Low cost materials** to enable market penetration and maximize energy efficiency
- **Minimize interactions** between ionic and electronic conducting phases
- **Co-sinter thin composite membrane on low cost porous supports** with minimal warping and cracking
- Design a planar stack architecture with **low cost fabrication processes**

# Minimal Interaction within Membrane

70/30 vol%  
Ionic/Electronic phase

SEM micrograph



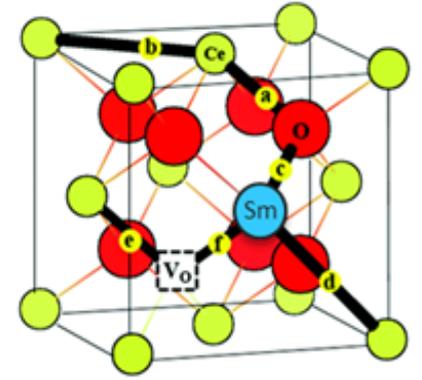
■ Ionic  
Conductor

■ Electronic  
Conductor

**Doped CeO<sub>2</sub>**  
 $\text{Sm}_{\text{Ce}'} \rightarrow 2[\text{V}_{\text{O}}^{\circ\circ}]$

Examples

- Ce<sub>0.8</sub>Sm<sub>0.2</sub>O<sub>2-x</sub> w/1% Co (SDCC)
- Ce<sub>0.8</sub>Gd<sub>0.2</sub>O<sub>2-x</sub> (GDC)
- Ce<sub>0.8</sub>Sm<sub>0.2</sub>O<sub>2-x</sub> (SDC)
  - TC grade (5-8 m<sup>2</sup>/g),  
T<sub>s</sub>~1400°C
  - HP grade (10-14 m<sup>2</sup>/g),  
T<sub>s</sub>~1300°C

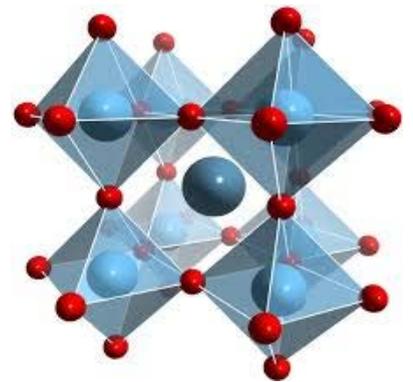


Fluorite structure

**Doped LaMnO<sub>3</sub>**  
Acceptor doped p-type

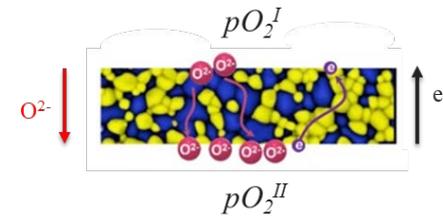
Examples

- La<sub>0.9</sub>MnO<sub>3-x</sub> (LM90)
- La<sub>0.75</sub>Sr<sub>0.2</sub>MnO<sub>3-x</sub> (LSM-20)
  - TC grade (4-8 m<sup>2</sup>/g)
  - HP grade (10-14 m<sup>2</sup>/g)

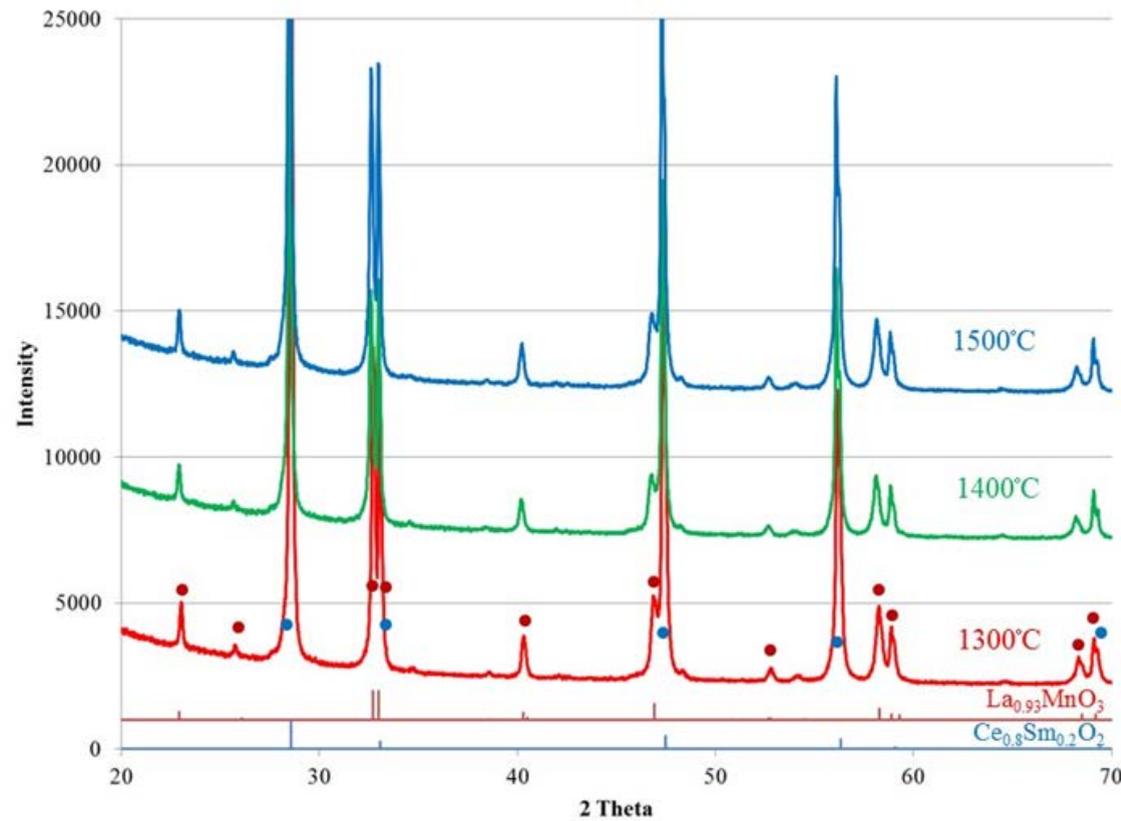


Perovskite

# Composite Membrane Characterization



## Interaction Studies



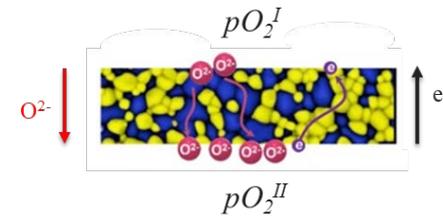
- Limited interaction, no 2<sup>nd</sup> phase formation
- Potential interdiffusion, Mn & Sr into fluorite structure

## Composite Dilatometry

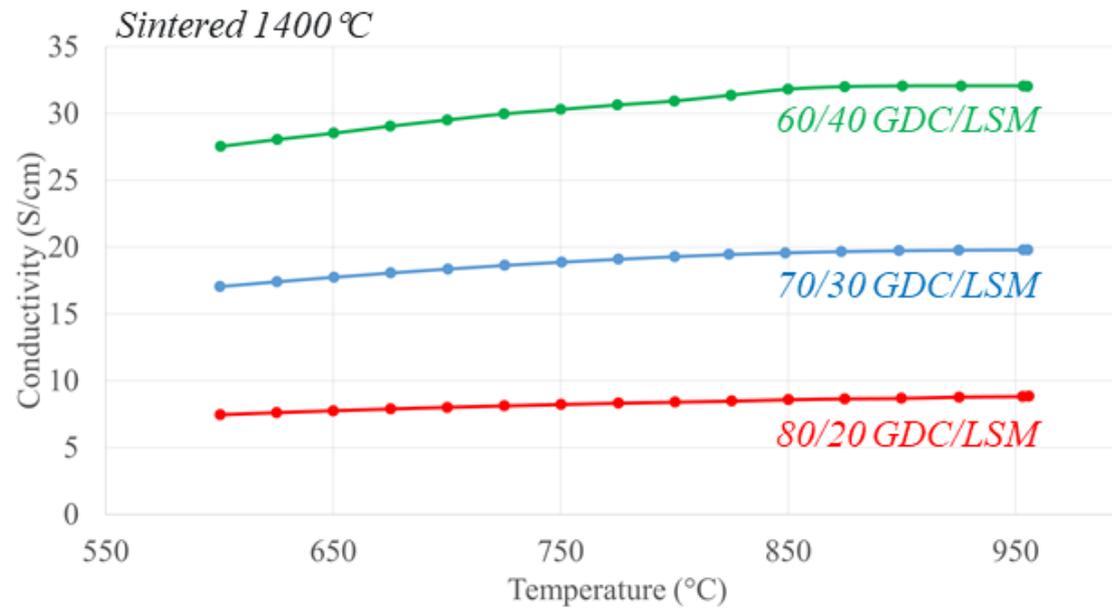
Material	$\alpha$ (x 10 <sup>-6</sup> )
SDCC-LM90 50/50	11.11
SDCC-LM90 60/40	11.57
SDCC-LM90 70/30	12.02
GDC20-LSM20 50/50	11.83
GDC20-LSM20 60/40	11.89
GDC20-LSM20 70/30	12.09
SDCC-LSM20 60/40	11.93
SDCC-LSM20 70/30	11.91

- Typical values of  $\alpha$  are  $\sim 12 \times 10^{-6}/^{\circ}\text{C}$

# Composite Membrane Characterization

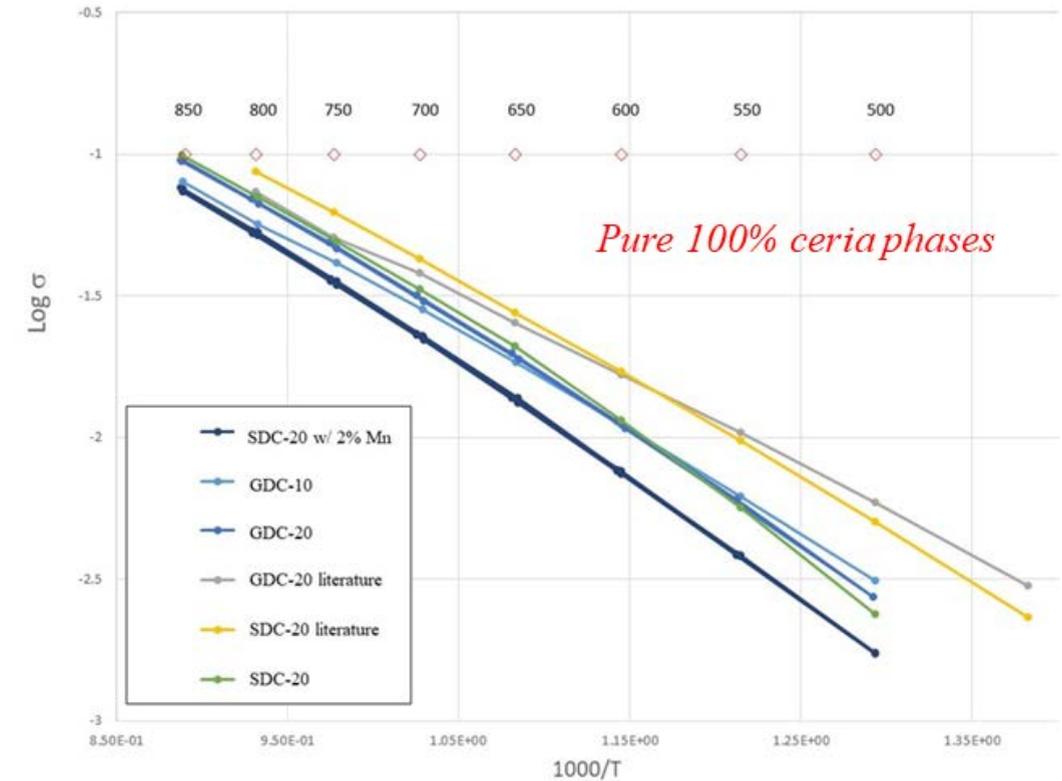


## Electrical Conductivity



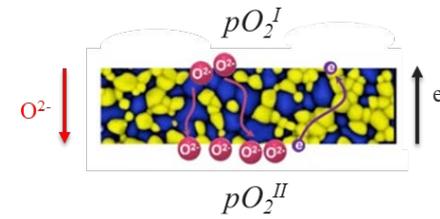
- Electrical conductivity ( $\sigma_e$ ) controlled by perovskite phase
- $\sigma_e \sim 3$  orders of magnitude greater than ionic conductivity ( $\sigma_i$ )
- Percolation in perovskite phase

## Ionic Conductivity

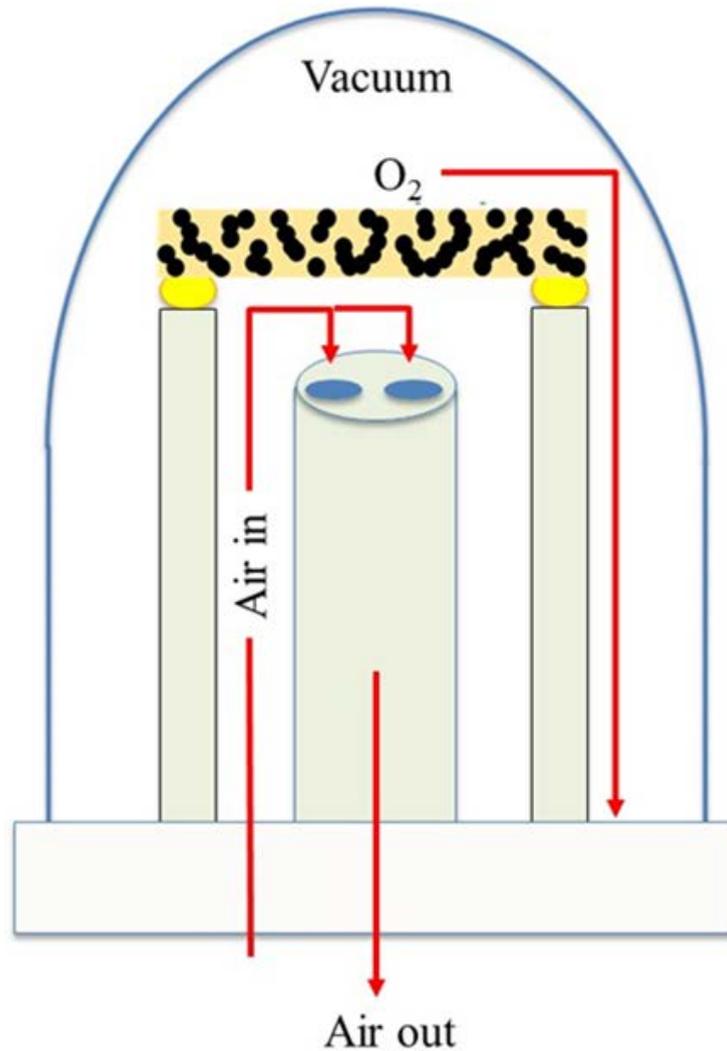


- $\sigma_i \sim 0.07$  at 800°C and 0.03 at 700°C
- $\sim 2/3 \sigma_i$  value used in composite calculations
- Percolation in both phases

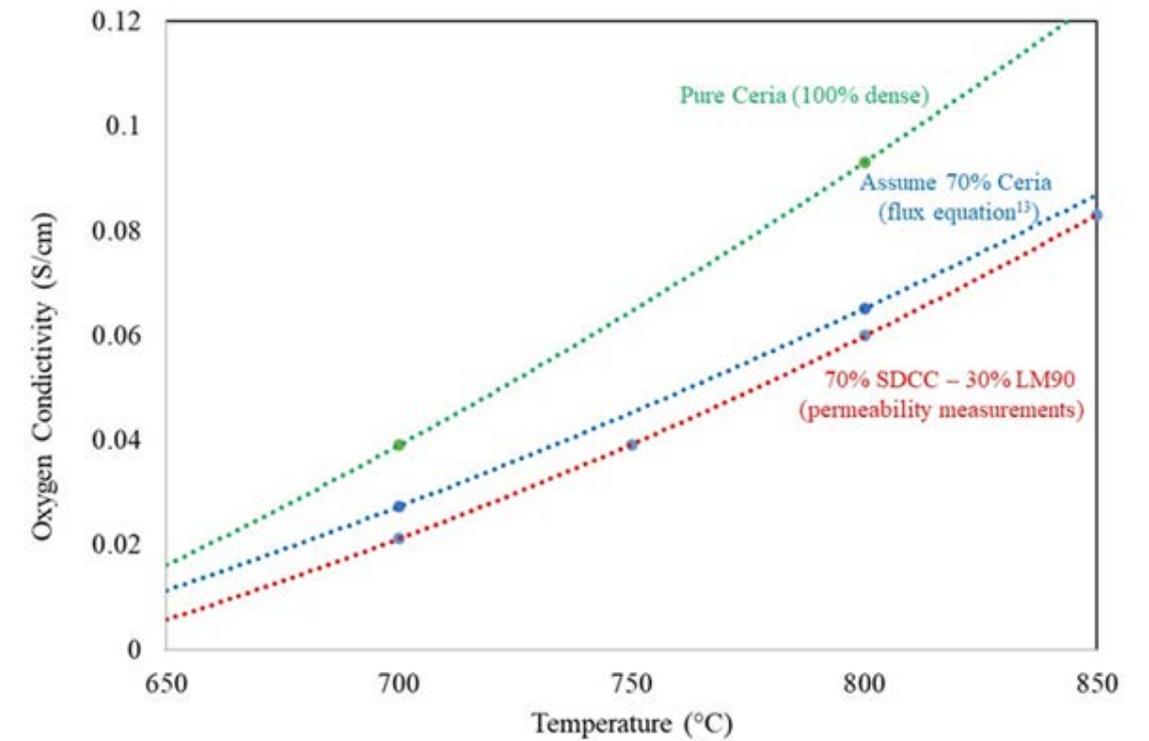
# Composite Membrane Characterization



## Permeability Measurements

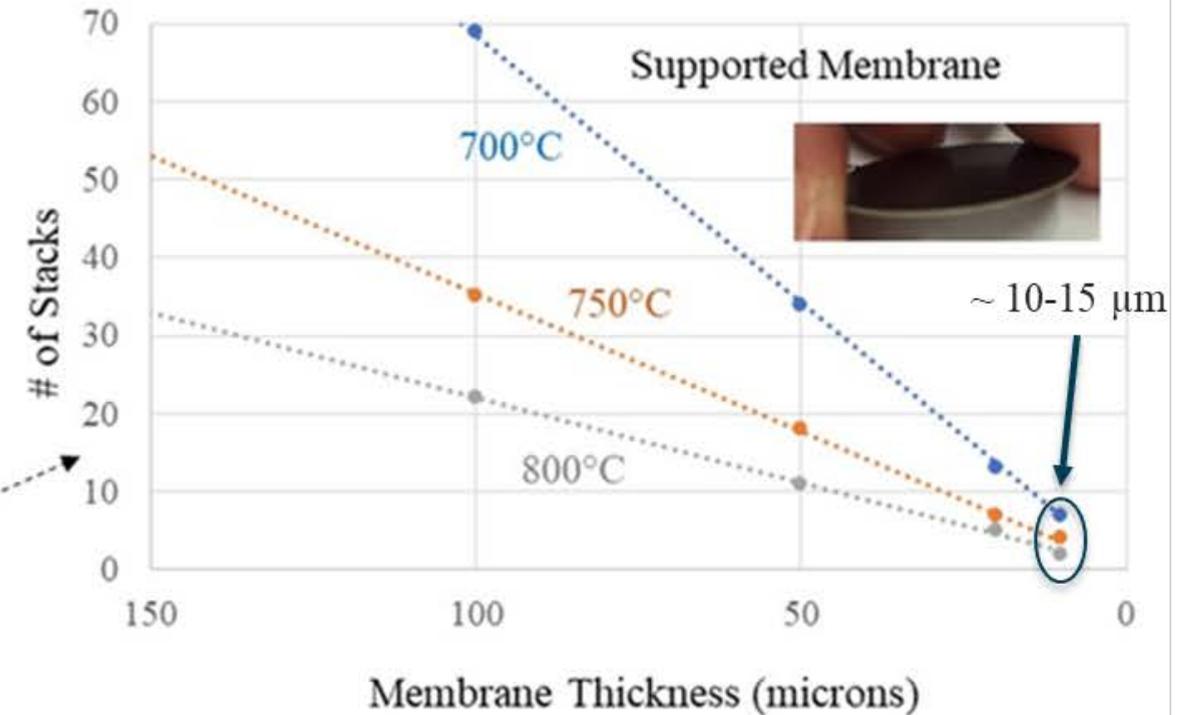
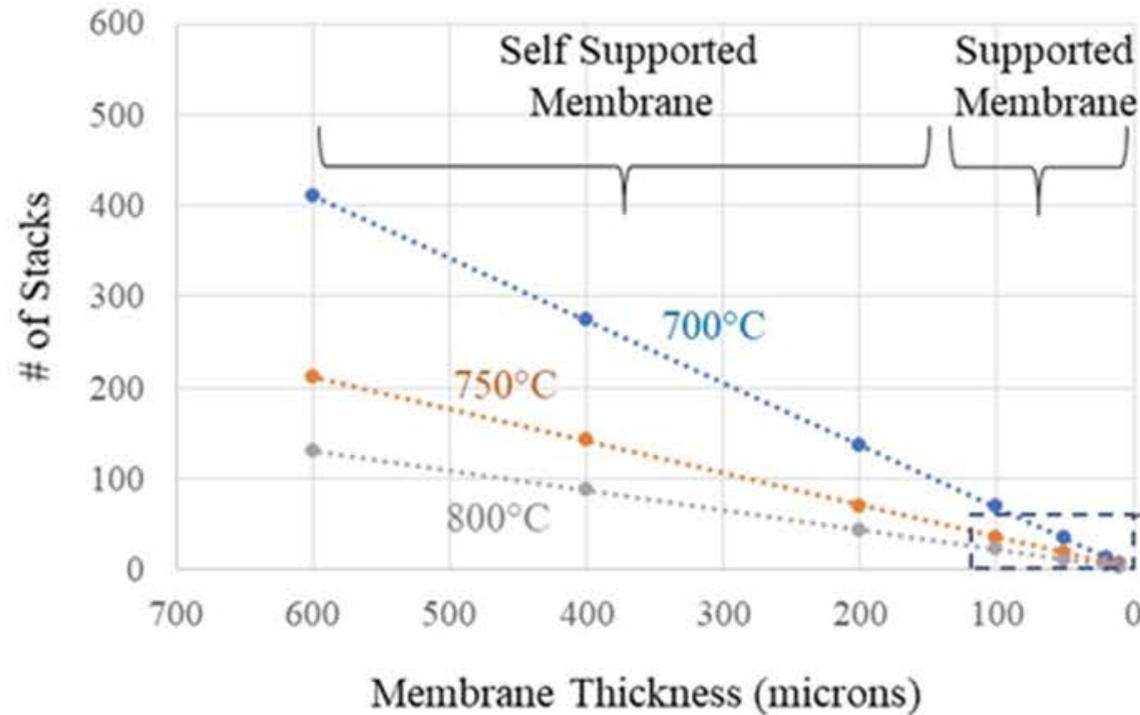
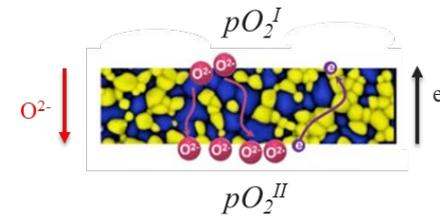


## Self-supporting composite membranes (~ 600 μm)



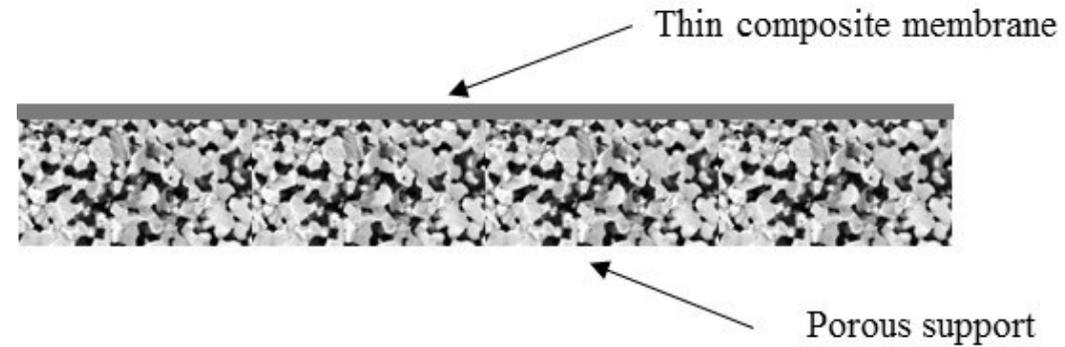
- $\sigma_i$  calculated from oxygen permeability measurements
- Similar to predicted value

# Composite Membrane Characterization

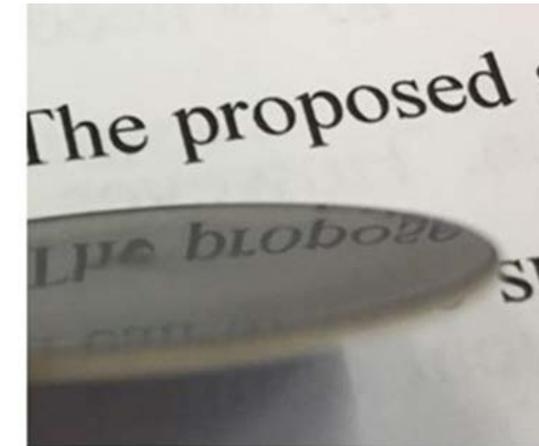
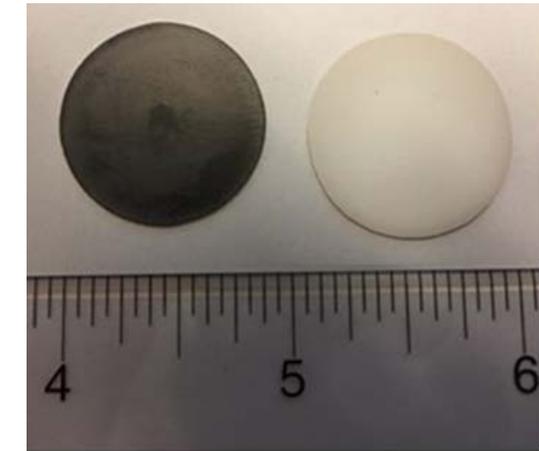


- To have a realistic number of stacks for producing 10 T/day of O<sub>2</sub> → the membrane thickness needs to be on the order of 10-15 μm.
- Membrane will need to be supported → Bilayer Structure

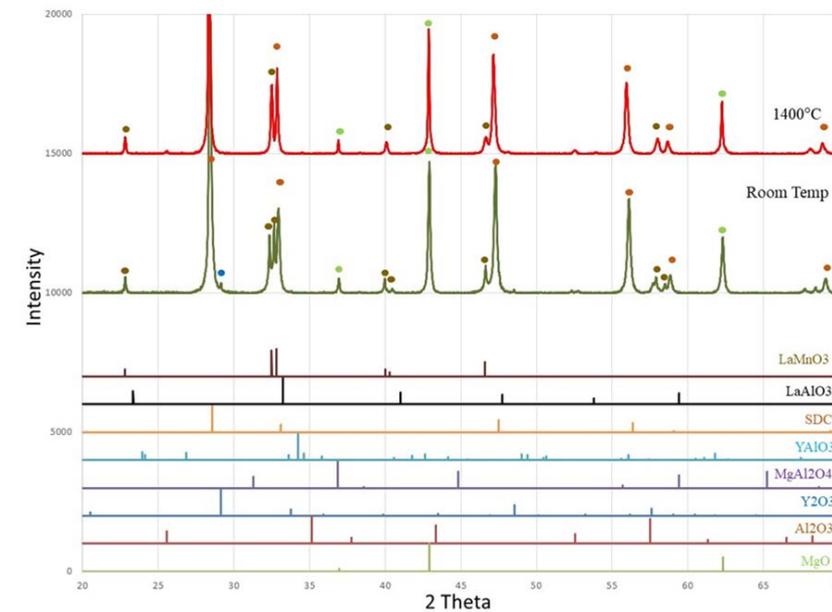
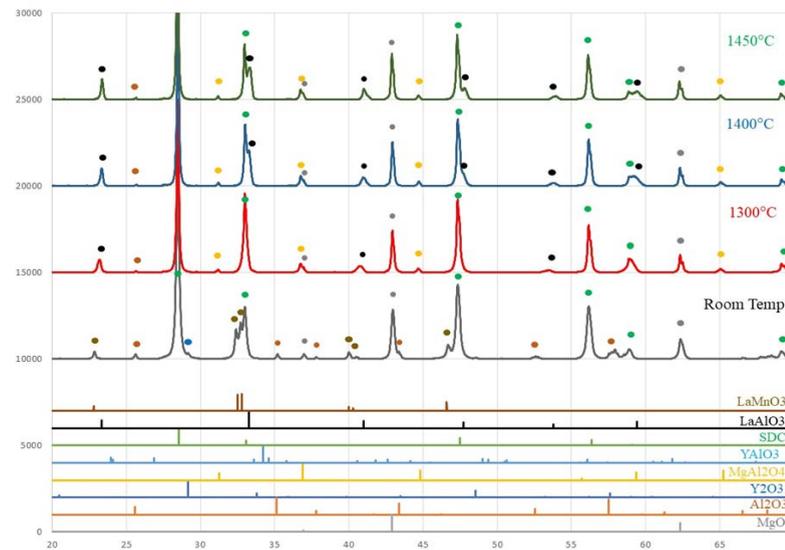
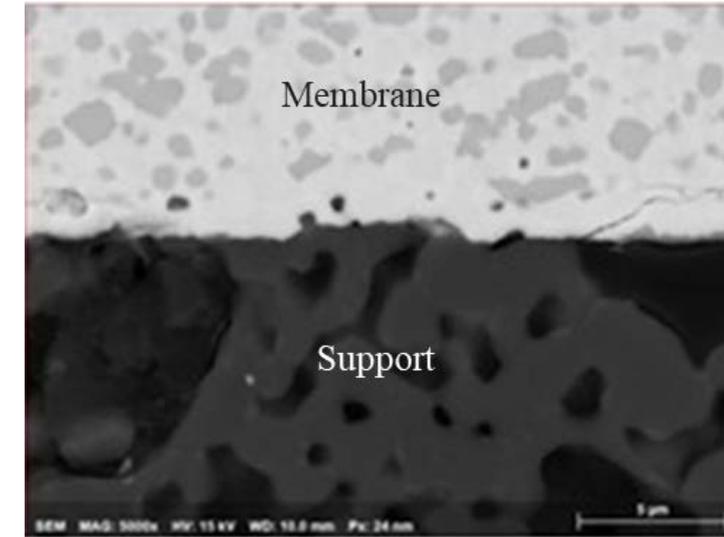
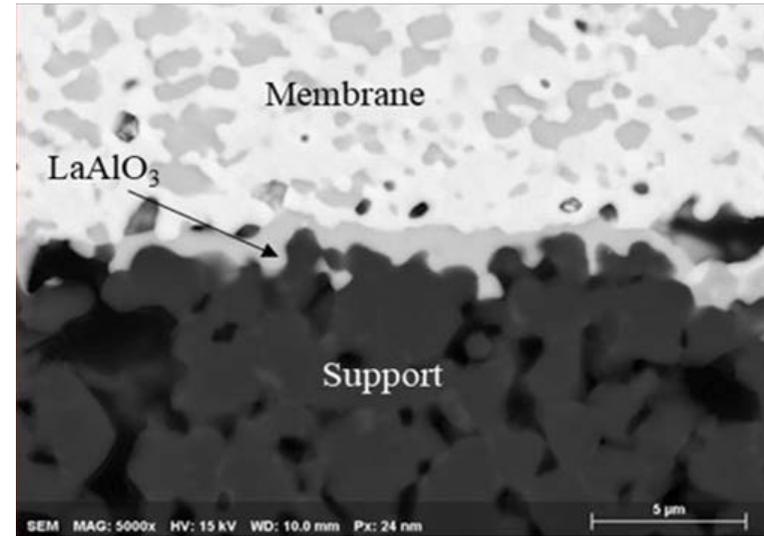
# Co-sintered bilayers



- Dense and thin membrane to maximize the oxygen permeability
- Thick and porous support to provide mechanical integrity and maximize gas diffusion
- Limited interaction during co-sintering



# Co-sintered bilayers

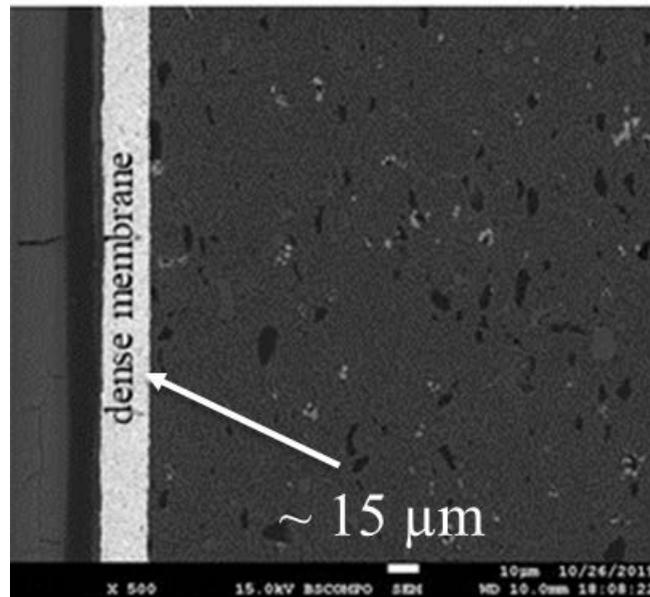


Insulating  $\text{LaAlO}_3$  formation at membrane/support interface – extremely low oxygen flux

No interfacial reaction w/ compositional change – future direction

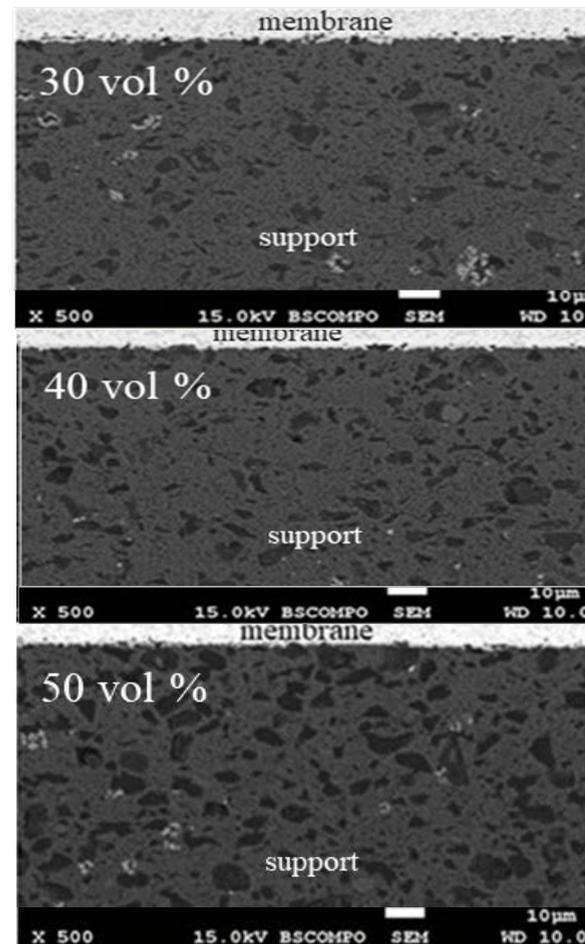
# Bilayers with Controlled Microstructures

## Membrane Thickness



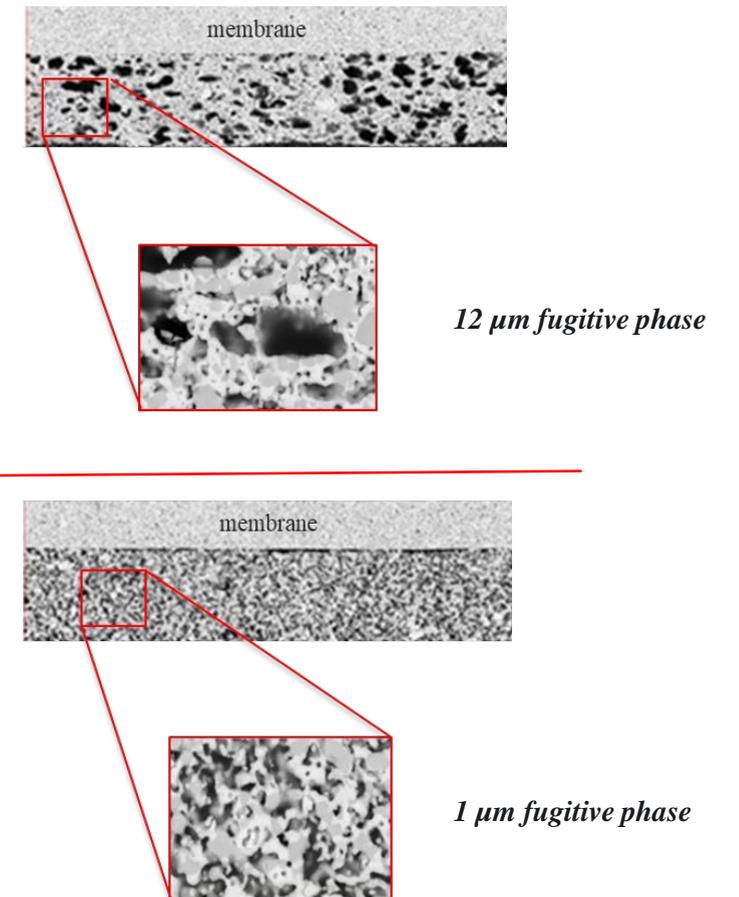
Tailor the membrane thickness by controlling the casting thickness

## Vol % Porosity



Tailor porosity by controlling the amount of fugitive phase used in tape cast suspension

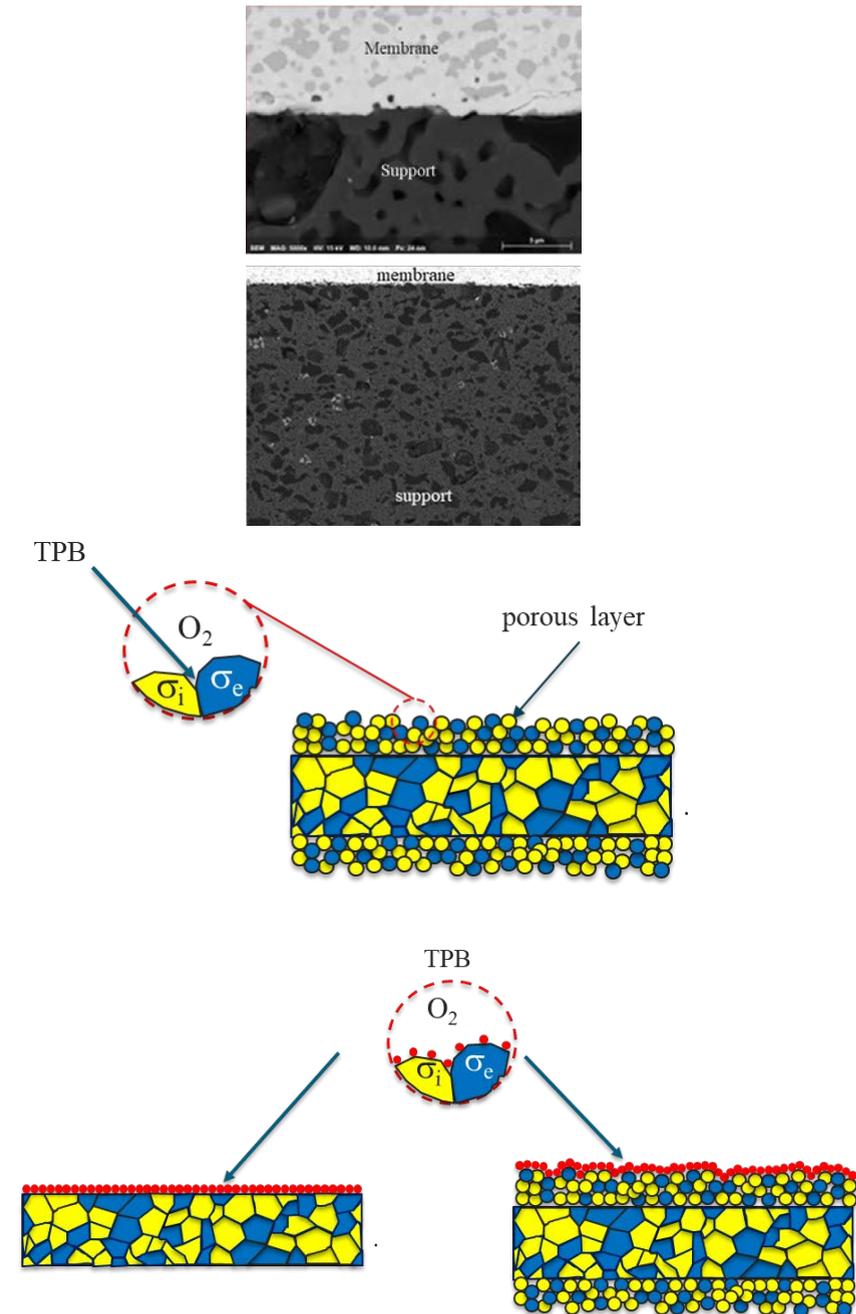
## Size of Porosity



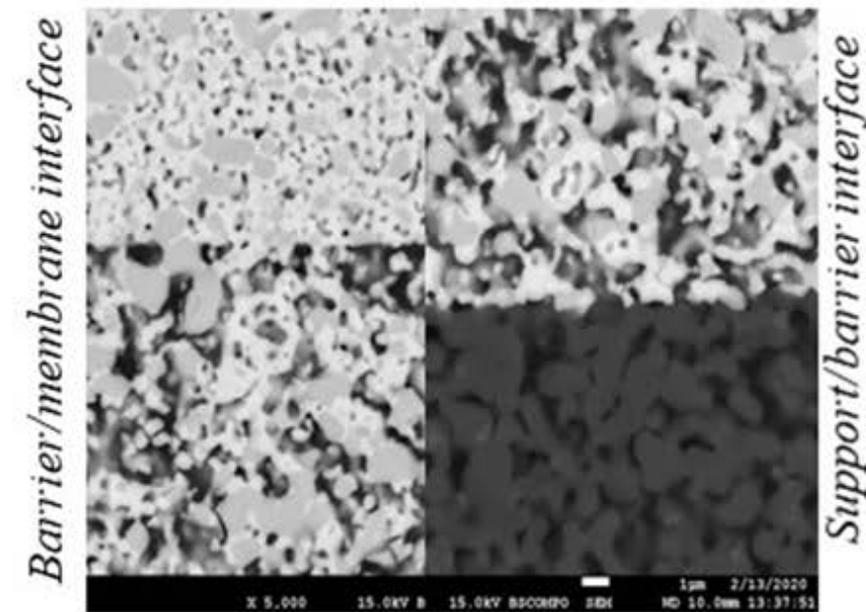
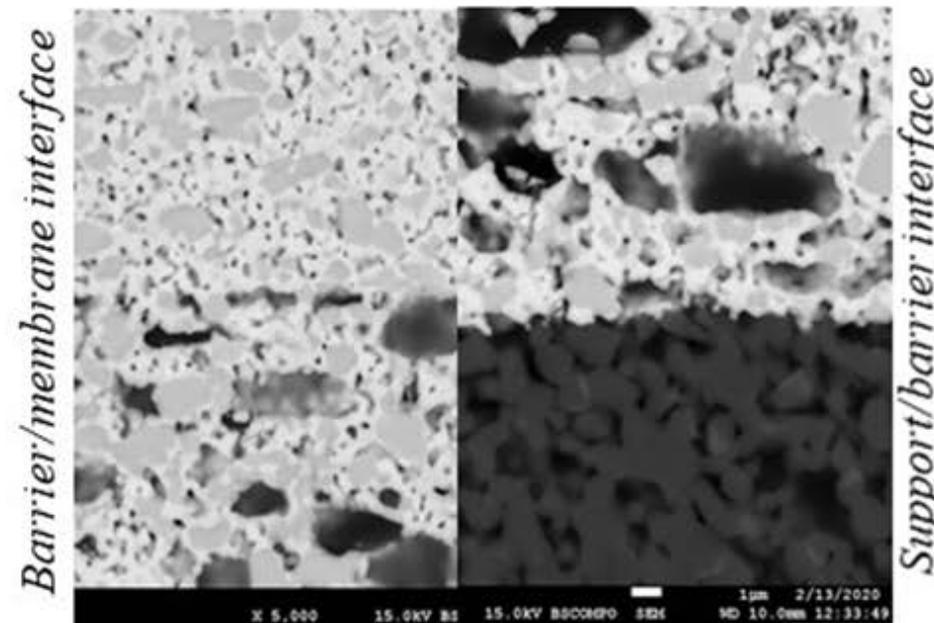
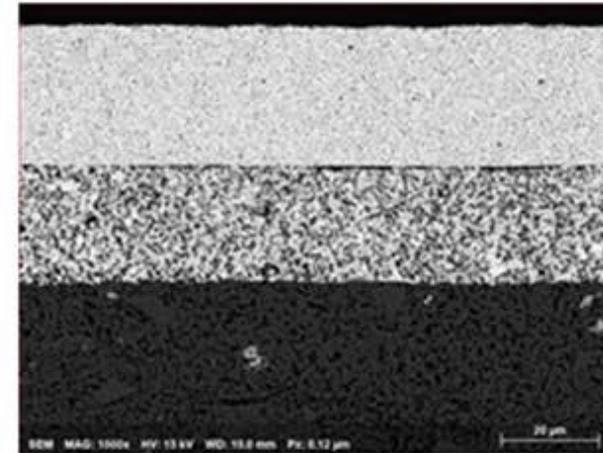
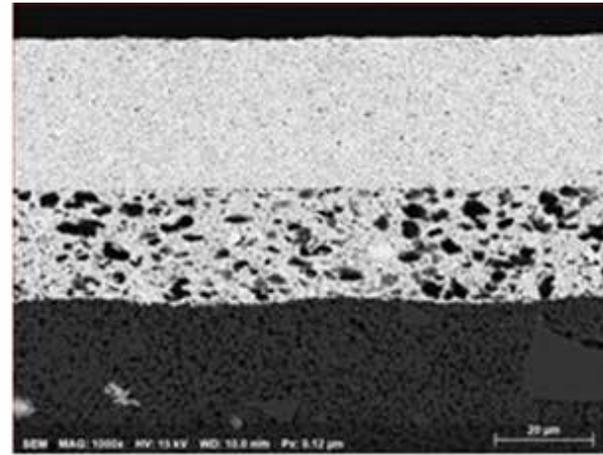
Tailor size & distribution of porosity by controlling size of the fugitive phase

# Bilayers with Maximum Oxygen Permeability

- Limited interaction during sintering of membrane and support (no 2<sup>nd</sup> phase formation)
- Thin, dense, crack-free membrane
- Porous support with controlled microstructure
- Expansion of the reaction area into three dimension  $\rightarrow$  improve the reaction kinetics by increasing the effective area of the three-phase boundary (TPB) at both reaction sites
- Increase the reaction kinetics by utilizing a known catalysts at the three phase boundaries

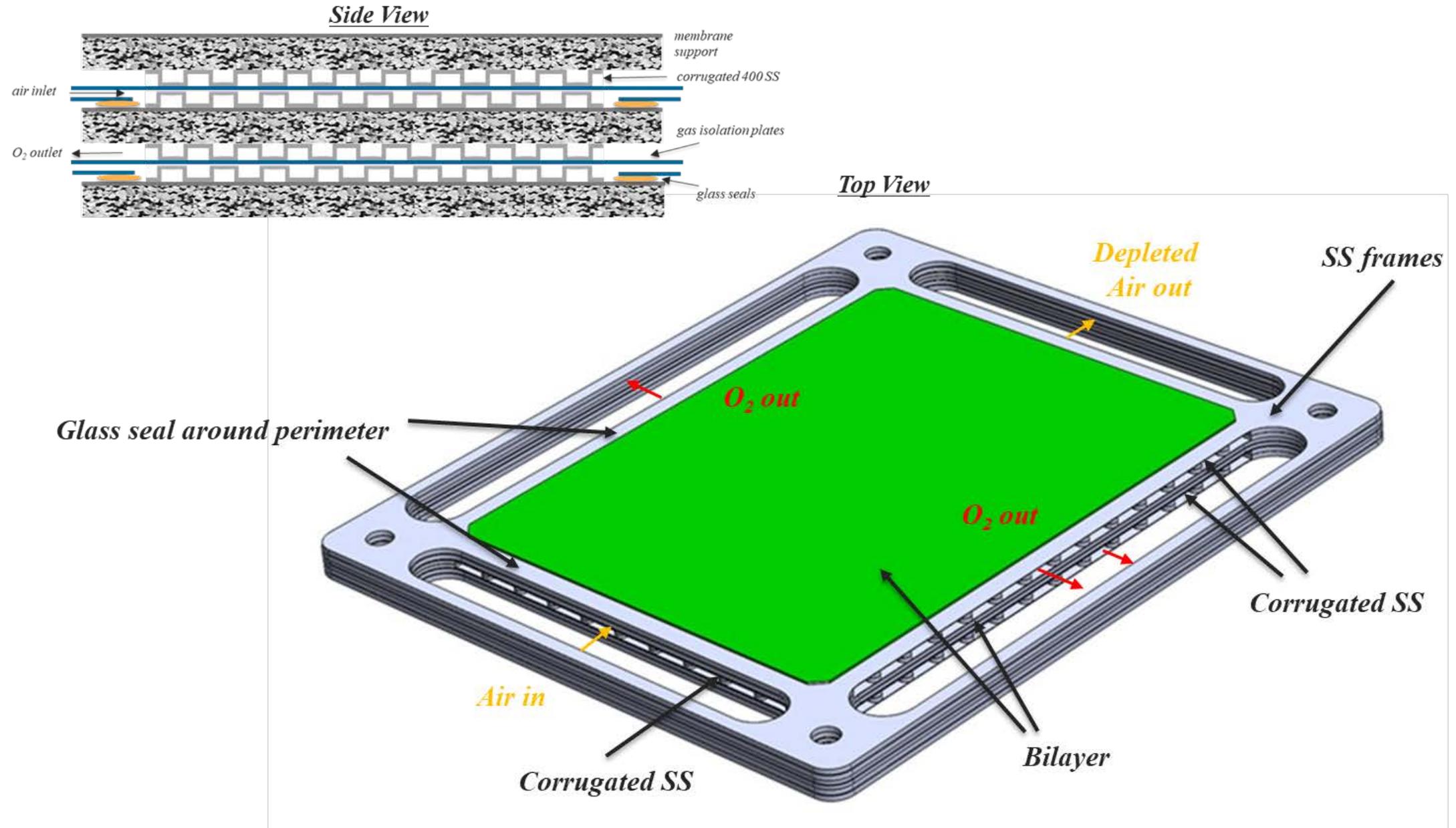


# Barrier Layer for Maximum Oxygen Permeability

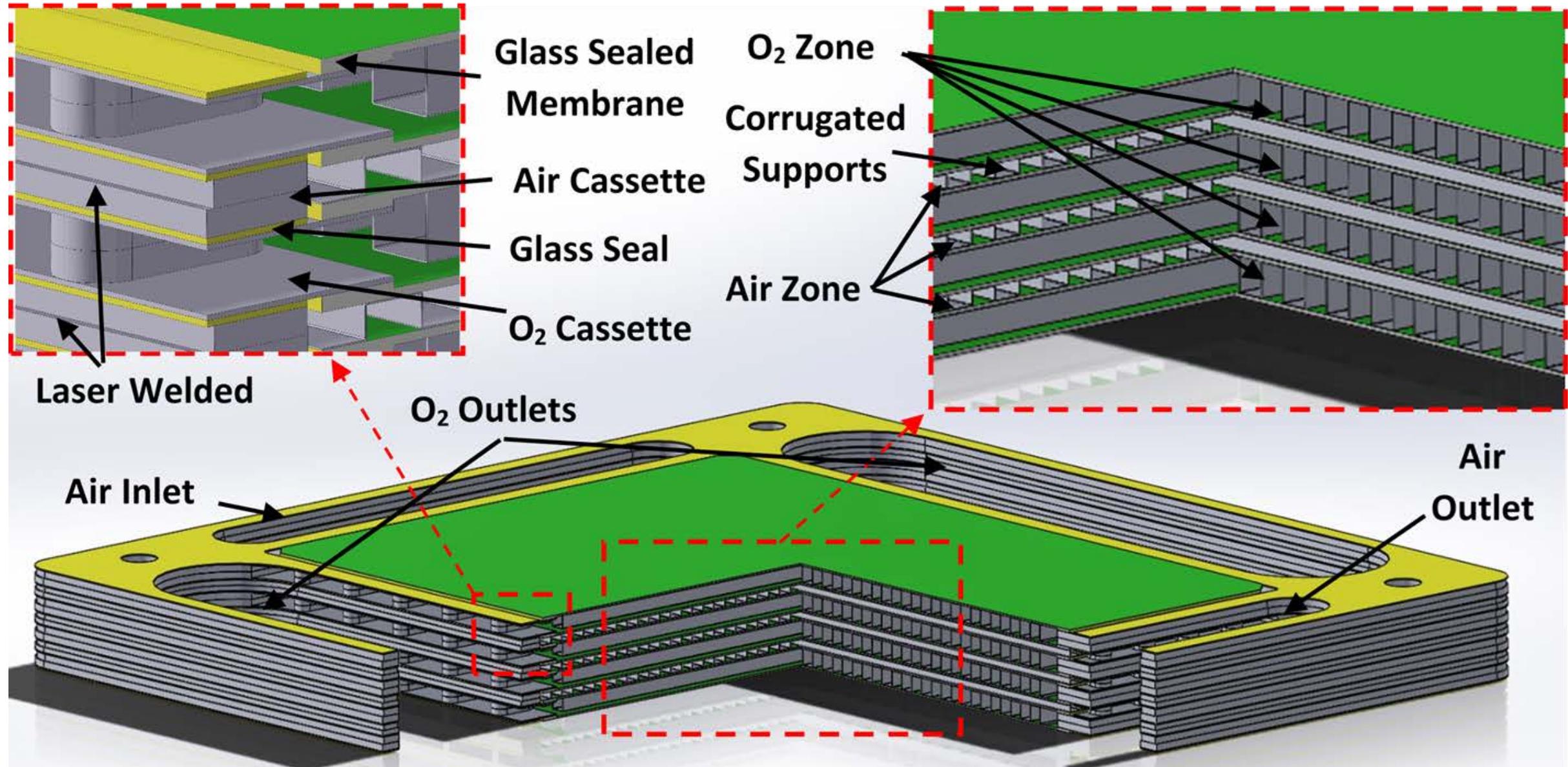


- Barrier layer provides 3-D surface to improve reaction kinetics

# Stack Design



# Stack Design



# Low Cost Materials and Processes

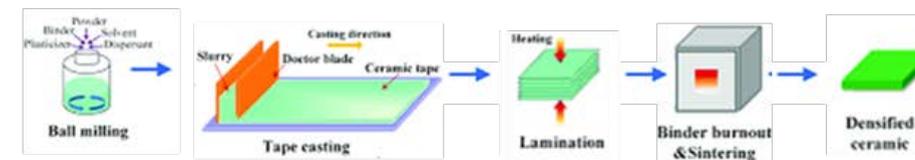
## Materials

- Membrane (least amount of material used ~ 10-15  $\mu\text{m}$  thick)
  - Ionic conductor -  $\text{Ce}_{1-x}\text{Gd}_x\text{O}_{2-x}$
  - Electronic conductor –  $\text{La}_{0.75}\text{Sr}_{0.2}\text{O}_{3-x}$
- Support – MgO
- Glass seal ( $\text{BaO-Al}_2\text{O}_3\text{-SiO}_2$ )
- Frames, gas isolation plates and corrugated supports
  - 400 series stainless steel

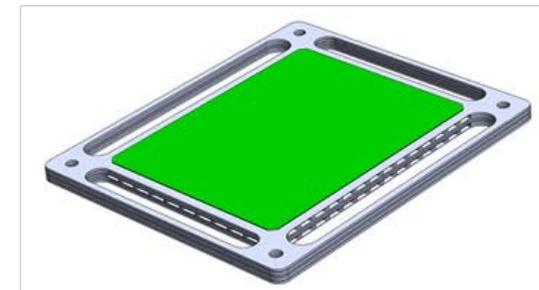
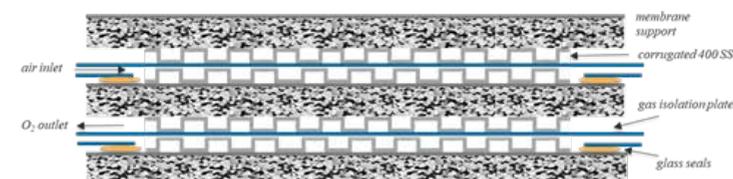
## Fabrication processes

- Membrane and support used traditional thick film processing

- Tape casting
- Screen printing



- Stainless steel frames, gas isolation plates and corrugated supports will be stamped



# Accomplishments

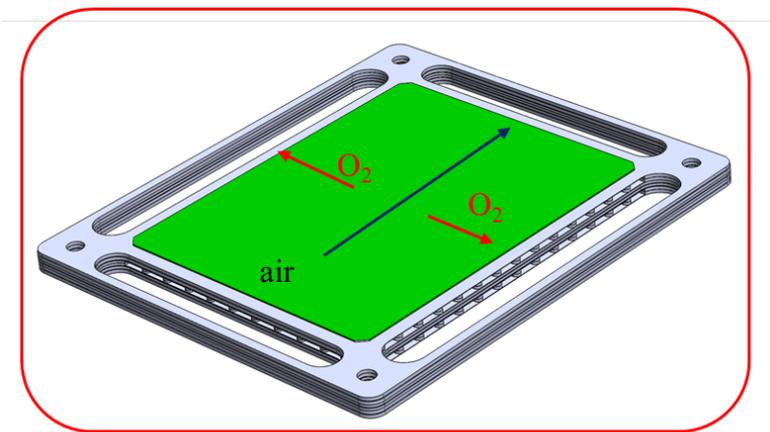
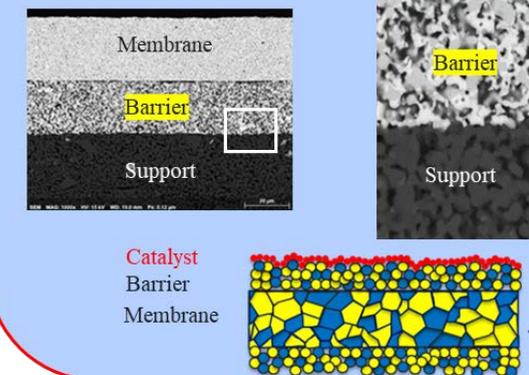
- Reduced sintering temperature during co-firing to reduce interactions (~1300°C)
- Limited interactions at the membrane/support interface
- Good membrane conductivity – significant oxygen flux can be achieved in composites for designing an economic modular oxygen separation unit
- Thermal expansion match between all components (composite membrane, composite support, glass-ceramic seal, 400 series stainless steel frame)
- Inexpensive materials of construction
- Good mechanical strength in porous support
- Ability to fabricate very thin dense membrane (10-15 μm) on flat, crack free porous supports
- Ability to control tape cast composite microstructures such as density, % porosity, size of porosity, shrinkage, etc.
- Ability to scale technology using traditional inexpensive thick film techniques

# Project Milestones

Fiscal Year	ID	Description	Planned/ Expected Completion Date	Actual Completion Date	Verification Method
2	M1	Reduce interfacial reactions at membrane-support interface	5/31/2020	3/31/2020	Reduce interfacial interactions via sintering temperature and/or alternative materials to improve the oxygen permeability in the bilayer structure
2	M2	Optimize oxygen flux for 1-2" diameter bilayer structures using barrier layers and catalysts	11/30/2020		Oxygen flux values will be compared to theoretical values calculated at various temperatures on bilayer structures
2	M3	Demonstrate scale up of bilayer structure (10 cm x 10 cm)	2/28/2021		Bilayer structure will be flat and crack free with a dense membrane co-sintered on a porous support using bilayer structures in M2
2	M4	Propose stack Design capable of producing 10 tons/day of oxygen	2/28/2021		Design will use oxygen flux values found on bilayer structures in M2 utilizing low cost frames and glass seals.

## Maximize Oxygen Permeability

- Tailor microstructure
- Barrier layer to increase reaction area
- Catalysts to improve reaction rates



# Acknowledgements

The authors wish to thank Venkat Venkataraman, David Lyons, and Jai-Woh Kim from DOE Office of Fossil Energy for their support of this project.