#### Oxygen Production for Gasification



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# **Advanced Reaction Systems**

New Approach - Tasks



- Task 1 Project Coordination/Management
- Task 2 Gasification Test Facility
- Task 3 Advanced Gasifier Design
- Task 4 Advanced Manufacturing Technologies for Gasification
- Task 5 Oxygen Production for Gasification
- Task 6 Microwave Reactions for Gasification
- Task 11 Catalytic and Non-Catalytic Processes for Hydrogen Production
- Task 12 Biomass Gasification Assessment
- Task 13 Gasification Polygeneration Assessment
- Task 14 Syngas Conversion to Industrial Chemicals



## **Oxygen Carrier Studies**

Project Goal: Linking Atomic and Process Scales









### Perovskite Materials

Background

- Perovskites are a well studied type of oxide with the general formula ABO<sub>3</sub>
- The first identified Perovskite was CaTiO<sub>3</sub>
- A-site cation has a dodecahedral coordination
- B-site cation sits in the center of BO<sub>6</sub> octahedra
- "Ideal" structure is cubic though the size of the A-site cation can create distortions

- Applications
  - Chemical looping combustion
    - Potential CLOU candidates, if oxygen is released into the gas phase
  - Pollution remediation
    - NO<sub>x</sub> decomposition
  - Replacement of noble metal catalysts in automobiles
  - Syngas production via reforming reactions
  - High Temperature Gas Sensors
  - Solid Oxide Fuel Cells
  - Photovoltaics
- Potentially Interesting Properties
  - Superconductivity
  - Magnetoresistance
  - Ferromagnetism









#### Perovskite Materials Chemical Substitution

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High-resolution, rapid collection synchrotron powder in situ XRD

- Time-resolved *in situ* XRD
  - Determine structural changes in relation to oxygen release
  - Synchrotron source (APS 17-BM) high-energy, rapid acquisition









#### Thermal expansion, possible oxygen release



TPD: Determination of maximum O<sub>2</sub> storage capacities and desorption temperatures

MS response / gram

#### • Experiment:

- Systematic priming at 850°C in air flow for O<sub>2</sub> uptake for 1 hour
- Cool to RT
- 10 deg/min ramp to 1050°C in He flow and monitor  $O_2$  release

#### • Findings:

- As x increases,  $T_{des, max}$  decreases
- As x increases, max O<sub>2</sub> release decreases
- As x increases, α & β oxygen desorption distinctions merge





TGA: All samples show cyclable O<sub>2</sub> uptake and release

- Samples demonstrate durability and cyclability
  - 4 uptake/release cycles
    - Shorter cycle timeframe used for higher temperatures
    - Gas flow (75 sccm)
  - Samples aged 6+ mo. in air

#### • Findings:

- As x increases, max O<sub>2</sub> capacity decreases (agrees with O<sub>2</sub>-TPD)
- As x increases, max uptake temperature increases
- As x increases, rate of O<sub>2</sub> release at 800°C increases
- If  $x \ge 0.30$ , sharp decrease in oxygen storage at 450-500°C exists
  - x = 0.20, less abrupt at 550-700°C





Popczun, E.J.; Tafen D.; Natesakhawat, S.; Marin, C.M.; Nguyen-Phan, T.-D.; Zhou, Y.; Alfonso, D.; Lekse, J.W. J. Mater. Chem. A, 2020, 8, 2602.



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TGA: Oxygen storage capacities and time to reach 90% released

- As temperature increases, max OSC decreases
  - Instability of oxidized species under air flow
  - Ex: x = 0.30 at 550°C 0.54 wt% O<sub>2</sub>

			Temperature (°C)						
<b>^</b> 0			400	450	500	550	600	700	
wt <sup>0</sup>	Ca <sup>2+</sup> ratio (x)	0.00	0.84	0.82	0.95	1.06	1.30	1.40	
		0.05	0.81	0.91	1.19	1.37	1.69	1.55	
D		0.10	0.93	1.08	1.91	2.04	1.90	1.50	
<b>OSCs</b> i		0.15	1.35	2.17	2.26	2.04	1.83	1.44	
		0.20	2.10	2.37	2.19	1.99	1.78	1.36	
		0.25	2.41	2.35	2.13	1.84	1.43	0.49	
		0.30	2.41	2.21	1.77	0.54	0.24	0.14	
		0.35	2.13	1.90	0.46				
		0.40	1.72						



Plot estimates the speed of oxygen release:  $rate = OSC_{90\%}/time_{90\%}$ 

> (Larger rates do not specifically suggest use of that material)

- Rates increase as x and temperature increase
  - Disparities due to very low OSCs

(min)

[ime

Only SrFeO<sub>3</sub> stays constant

			Temperature (°C)								
			400	450	500	550	600	700			
90% release	Ca <sup>2+</sup> ratio	0.00	9.56	16.53	17.38	13.93	15.58	15.15			
		0.05	31.77	18.33	20.70	16.03	15.65	11.67			
		0.10	36.03	22.08	25.08	15.47	8.85	4.93			
		0.15	51.35	24.22	11.83	5.35	3.02	1.68			
		0.20	45.17	17.85	6.53	3.00	1.70	0.90			
		0.25	36.13	7.00	2.18	1.00	0.53	1.05			
		0.30	25.83	4.10	1.17	0.70	4.72	17.32			
		0.35	16.03	3.00	1.07						
		0.40	10.30								

Stability Testing and Comparison to Known Materials

- NETL Perovskite samples were tested in collaboration with ThermoSolv
- NETL sample demonstrated stability over >10,000 cycles
- NETL Perovskite outperformed an LSCF sample in multiple cycle structures











#### **Perovskite Modelling**

Atomistic Modelling

**Vacancy Formation Energy** 3.5 3.0 2.5 2.0 Energy (eV) 1.5 1.0 0.5 relax 0.0 -0.5 -1.0 -1.5 0.3 0.4 0.0 0.1 0.2 0.5

x in Sr<sub>1</sub>, Ca, FeO<sub>3</sub>



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**Electronic Density of States** 





## **Perovskite Modelling**

Ellingham Diagram Calculation





- Differential Scanning Calorimetry used to determine enthalpy of oxidation/reduction for each sample at each temperature from cycling experiments
- Decreasing enthalpy as both calcium content and temperature increase
- Agreement between computational models and DSC experiments



### **Perovskite Modeling**

MFiX-DEM Verification of TGA Data





For each case, the 2<sup>nd</sup> TGA cycle was used to calculate kinetic constants.





## **Current and Future Work**

MFiX Validation and Reactor Design





For each temperature and perovskite composition, a

CFD Model Demonstration for 300s  $O_2$ absorption sweep

22mm x 559mm tube •

Validated TGA data

will contribute to the

final MFiX CFD

**Reactor Design** 

 $Ba_{1-x}Sr_{x}Co_{0.8}Fe_{0.2}O_{3-\delta}$  data from He (2009) ullet





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numerical matching of TGA data is necessary.

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- Synthesized more than 24 perovskite materials
- Achieved more than 2.4 wt %  $O_2$  capacity
- Achieved control of desorption temperature
- Sr<sub>1-x</sub>Ca<sub>x</sub>FeO<sub>3-d</sub> found to outperform LSCF
- Sr<sub>1-x</sub>Ca<sub>x</sub>FeO<sub>3-d</sub> found to be stable over >10,000 cycles
- Experimentally validated Ellingham Diagrams
- Initiated CFD design and model validation





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### **Future Work**

- Larger surface areas obtained by changing synthesis technique and temperature
- Particle synthesis based on literature precedent from Dou
  - Use of citric acid and ethylene glycol allows lower temperature synthesis (at 1000 °C)
  - Show increased activity versus their solid-state materials
- Did not alter temperature to synthesize different particle sizes or morphologies
  - NETL: 700-1000 °C

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- BET surface areas: 8.2-15.0 m<sup>2</sup>/g depending on synthesis temperature
- Mesoporous sample observed at 800 °C

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Multiphase Flow with Interphase eXchanges





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# **Questions?**



