

Piperazine Advanced Stripper (PZAS™) Front End Engineering Design (FEED) Study [on NGCC at Denver City , Tx]

DE-FE0031844

2020 CCUS Integrated Project Review Meeting

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Takeaways

Objective: accurate FEED with benefits

PZAS: a superior capture technology

Mustang Station: space, EOR & cheap energy

Absorber: only 25 ft of solvent packing

Stripper: CO₂ product at 80 psia

Steam: gas-fired boilers with “free” fuel

Compression: 2 reciprocating machines

The Objective: *Accurate installed cost of PZAS™ on NGCC at GSEC Mustang Station*

Complementary Benefits:

- *Develop commercial project at Mustang Station*
- *Qualify PZAS for use on NGCC cogeneration*
- *Provide commercial cost detail*
 - *To optimize PZAS & other 2G capture processes*
 - *To guide R&D of capture technology*

Program Overview

- Funding (DOE and Cost Share)
 - 4.1 MM DOE
 - 1.1 MM cost sharing- ExxonMobil, Total, Chevron
 - 0.3 MM from Honeywell UOP outside DOE
- Performance Dates: 10/2019 – 9/2021
- Project Participants
 - Golden Spread Electric Cooperative (GSEC) - host
 - University of Texas at Austin (UT) - Modeling/ Technology
 - Trimeric – Process Engineering
 - AECOM - EPC

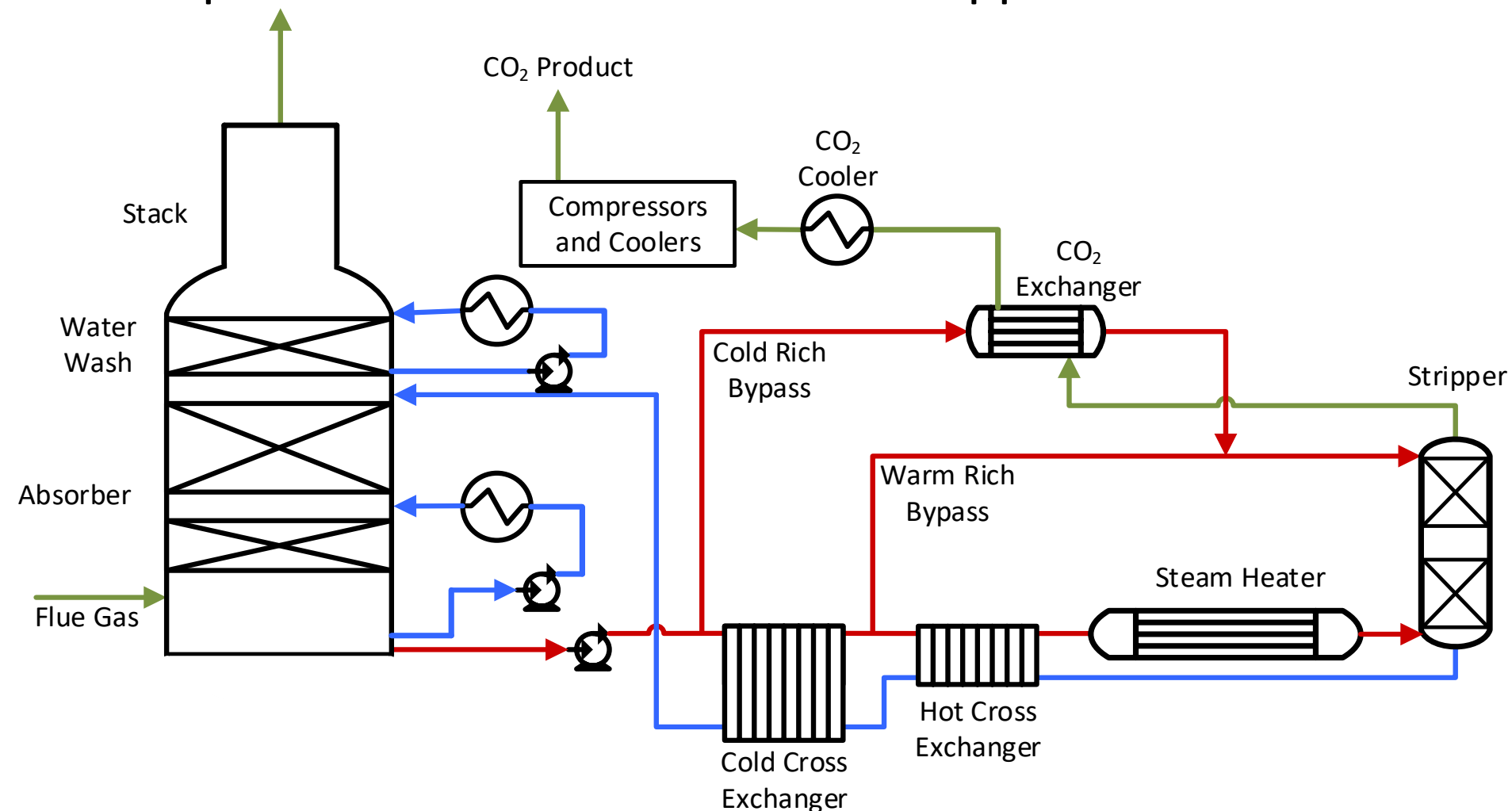
Milestones

2. Kick Off Meeting; DOE	Feb 3, 2020
3. Virtual Kick Off; Mustang Station	Mar 30, 2020
4. Project Design Basis	Aug 14, 2020
5. 2020 DOE-NETL Contractors Mtg	Aug 18, 2020
6. Baseline Process Design	Oct 2020
13. FEED Report	Sept 2021

Project team will request a no-cost extension to Dec 2021

PZAS for NGCC

5 m Piperazine with the Advanced Stripper



PZAS development includes comprehensive research & pilot plant demonstration

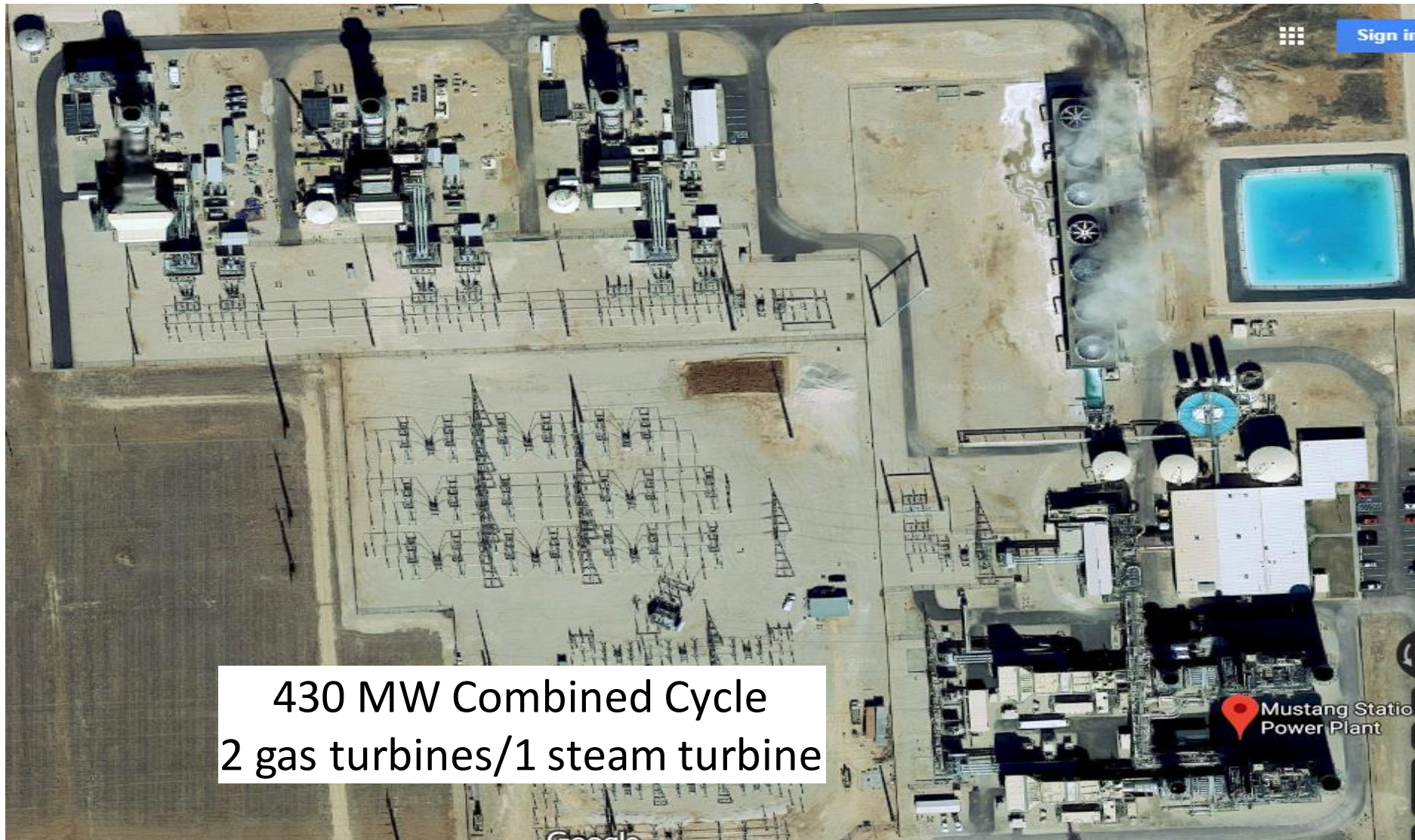
- (2000-20) Research by 43 graduate students
- (2006-09) UT Pilot of K_2CO_3 /Piperazine (PZ)
- PZAS Pilot at 12% CO_2 for coal
 - (2010-18) UT Austin
 - (2018) at NCCC
- PZAS Pilot w 4% CO_2 For NGCC
 - (2016-18) UT Austin
 - (2019) NCCC

PZAS pilot at NCCC with CCP4 funding

- Heat duty 2.4 GJ/t
- Stripping at 302 F/90 psia with little degradation
- 90-95% CO₂ removal with 2 x 20 ft packing
- Pump-around intercooling of hot inlet gas
- Low PZ oxidation, <0.3 kg/t CO₂
- 304 SS works up to 150°C
- PZ emissions < 1 ppm

Host Site - Mustang Station

Golden Spread Electric Cooperative, Denver City, TX

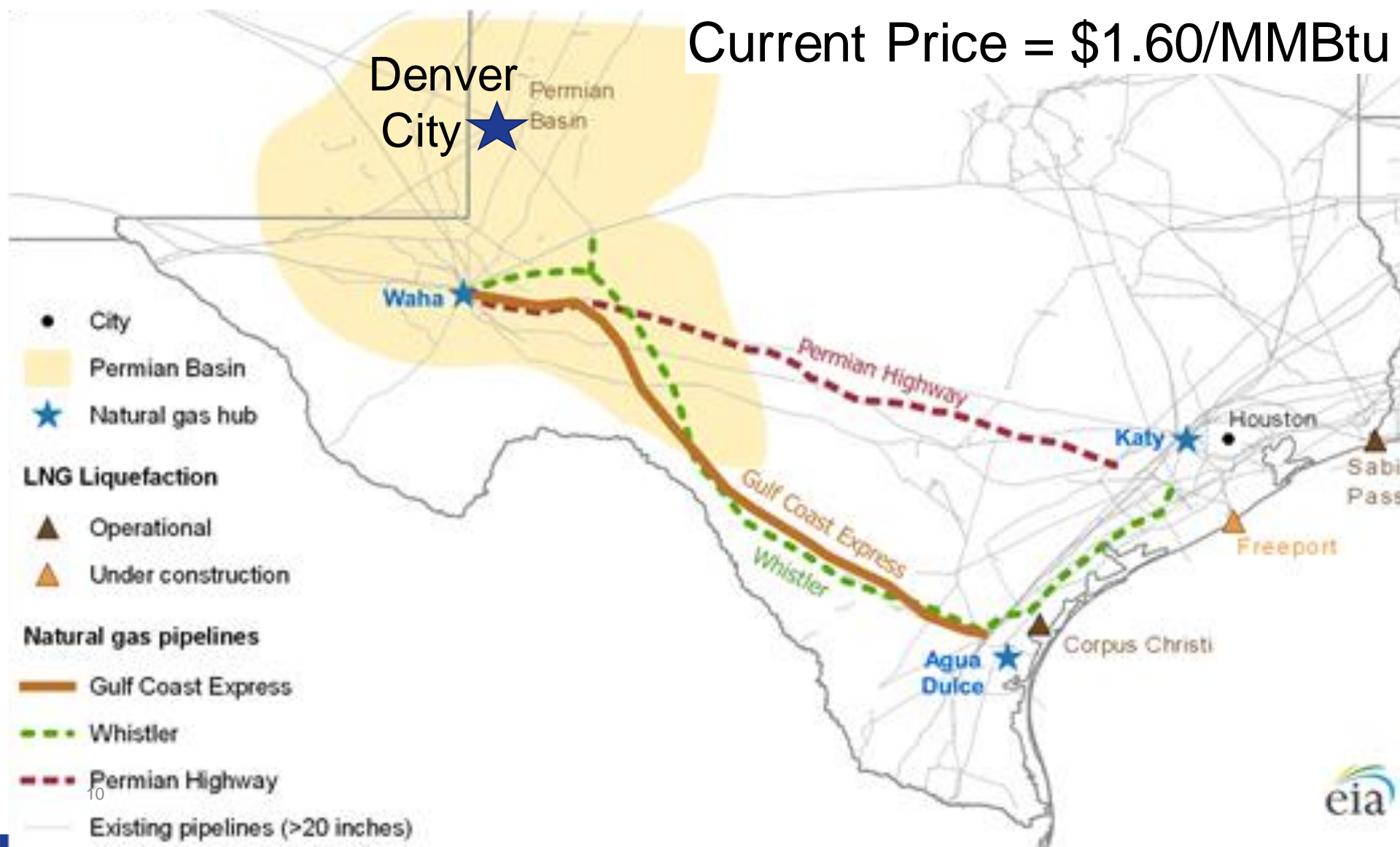


430 MW Combined Cycle
2 gas turbines/1 steam turbine

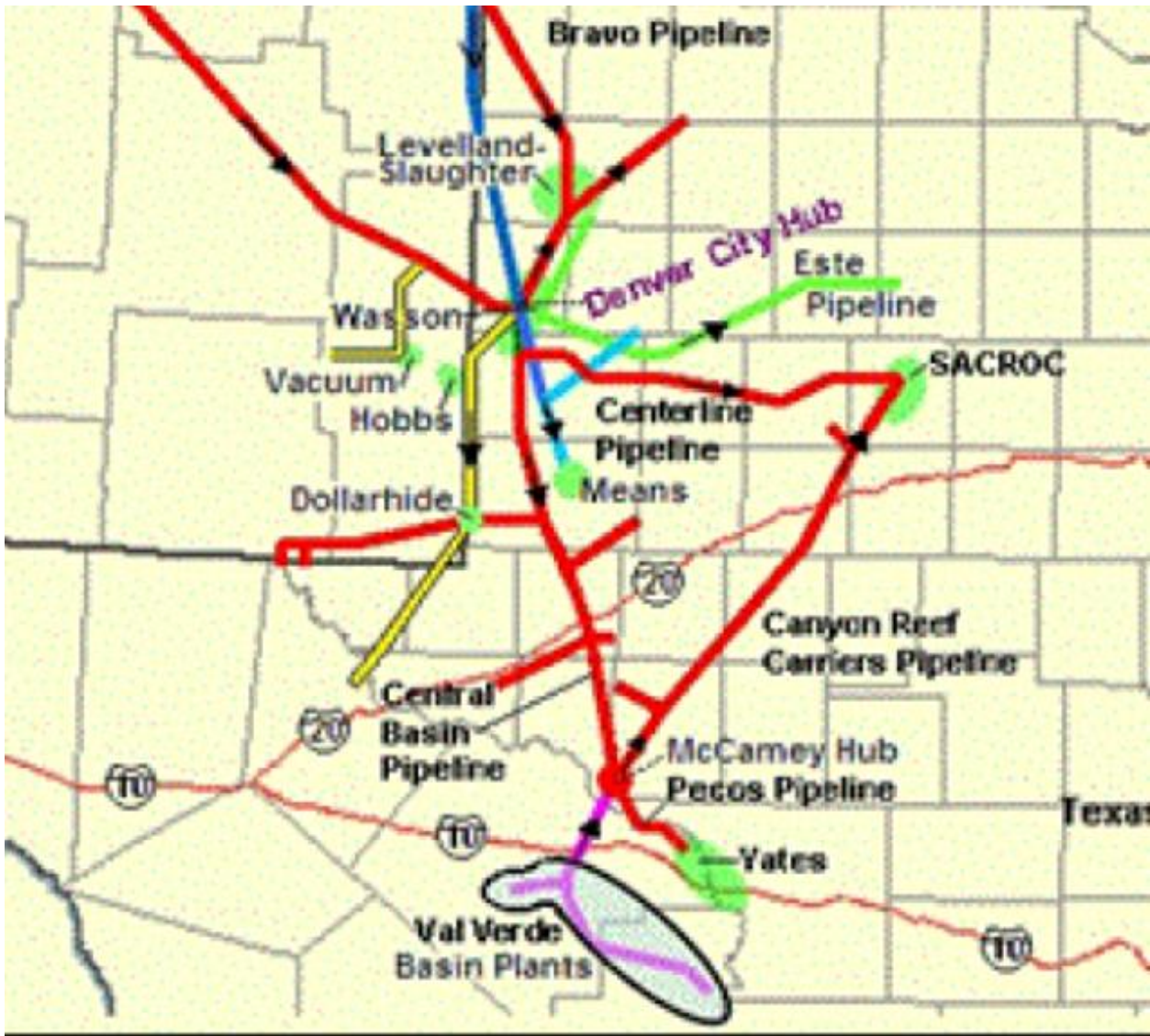
Cheap, Stranded Gas available from Waha Hub

Limited pipeline capacity from the Permian Basin

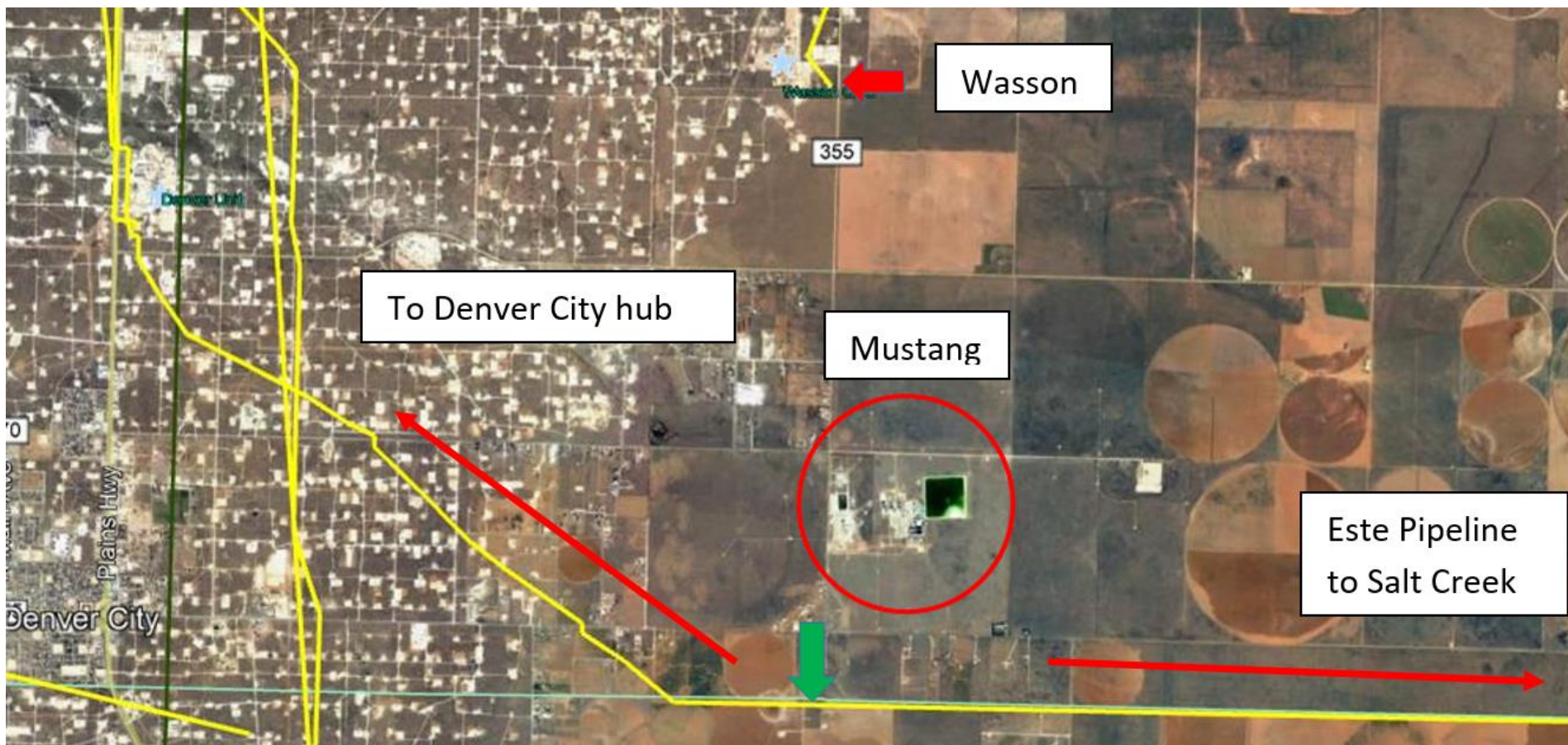
Current Price = \$1.60/MMBtu



CO₂ pipelines converge on Denver City, TX

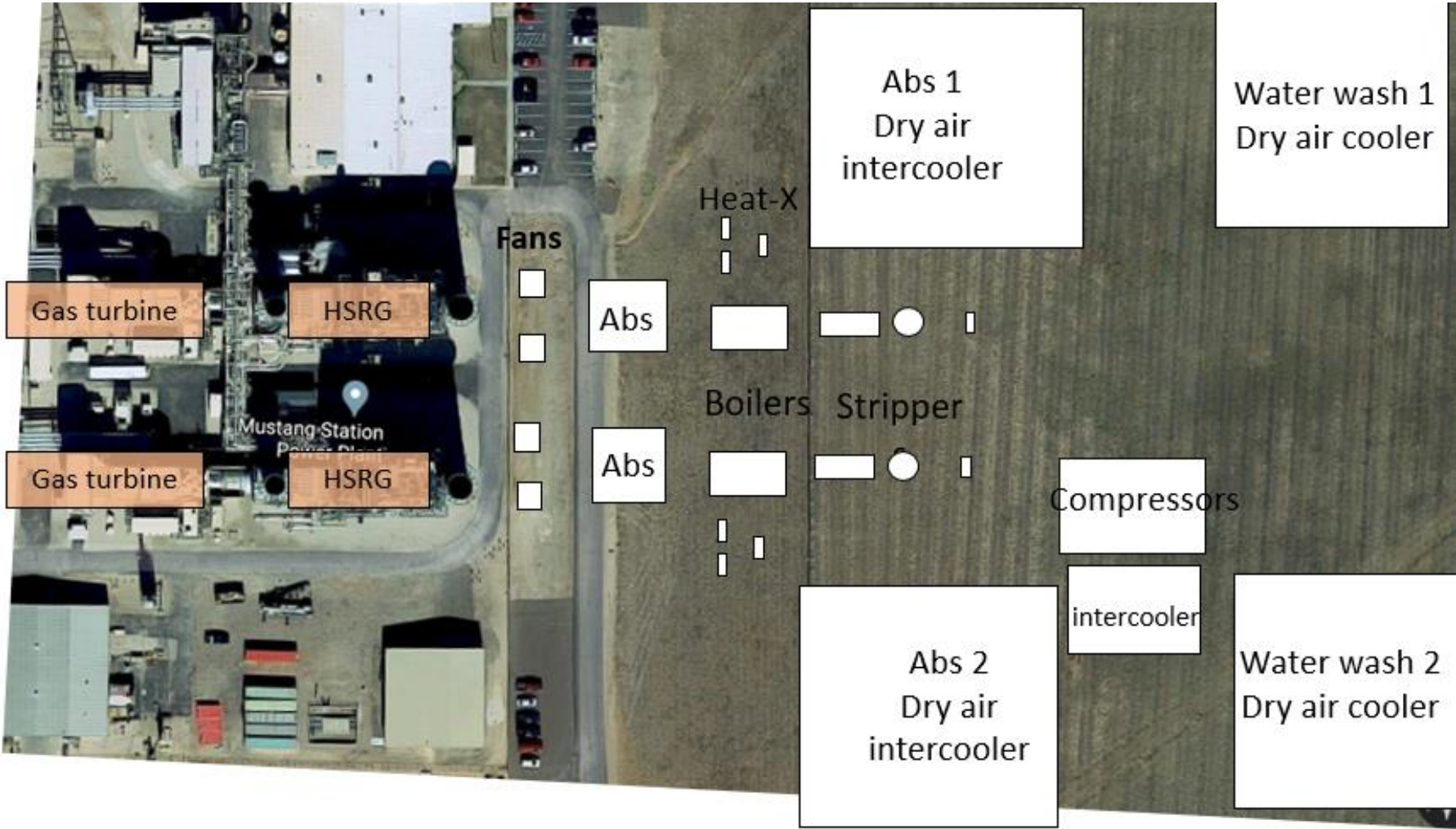


Ample open land CO₂ to Este Pipeline for EOR



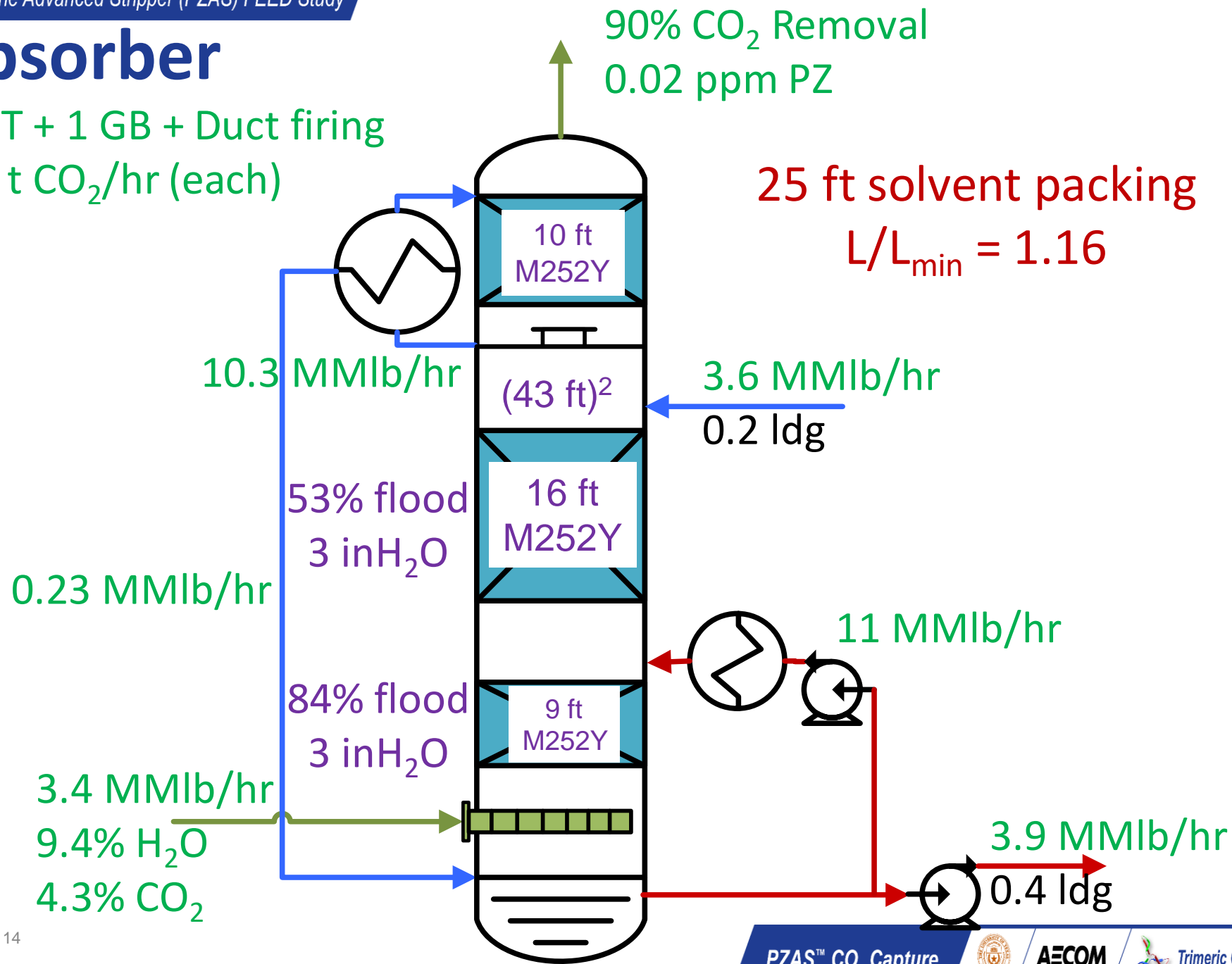
Two trains: Plot Space dominated by air coolers

[Preliminary unvetted layout by UT]



Absorber

1 GT + 1 GB + Duct firing
95 t CO₂/hr (each)



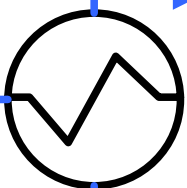
Absorber T's

$T_{amb} = 65\text{ F}$

0.23 MMlb/hr
+0.11 net H₂O

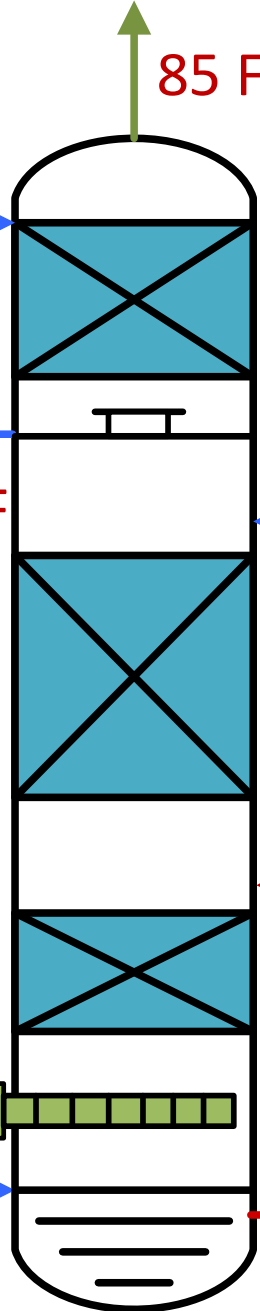
No DCC
233 F

Air Cooling



85 F

112 F



85 F

143 F No Trim Cooler

85 F

Air Cooling



111 F

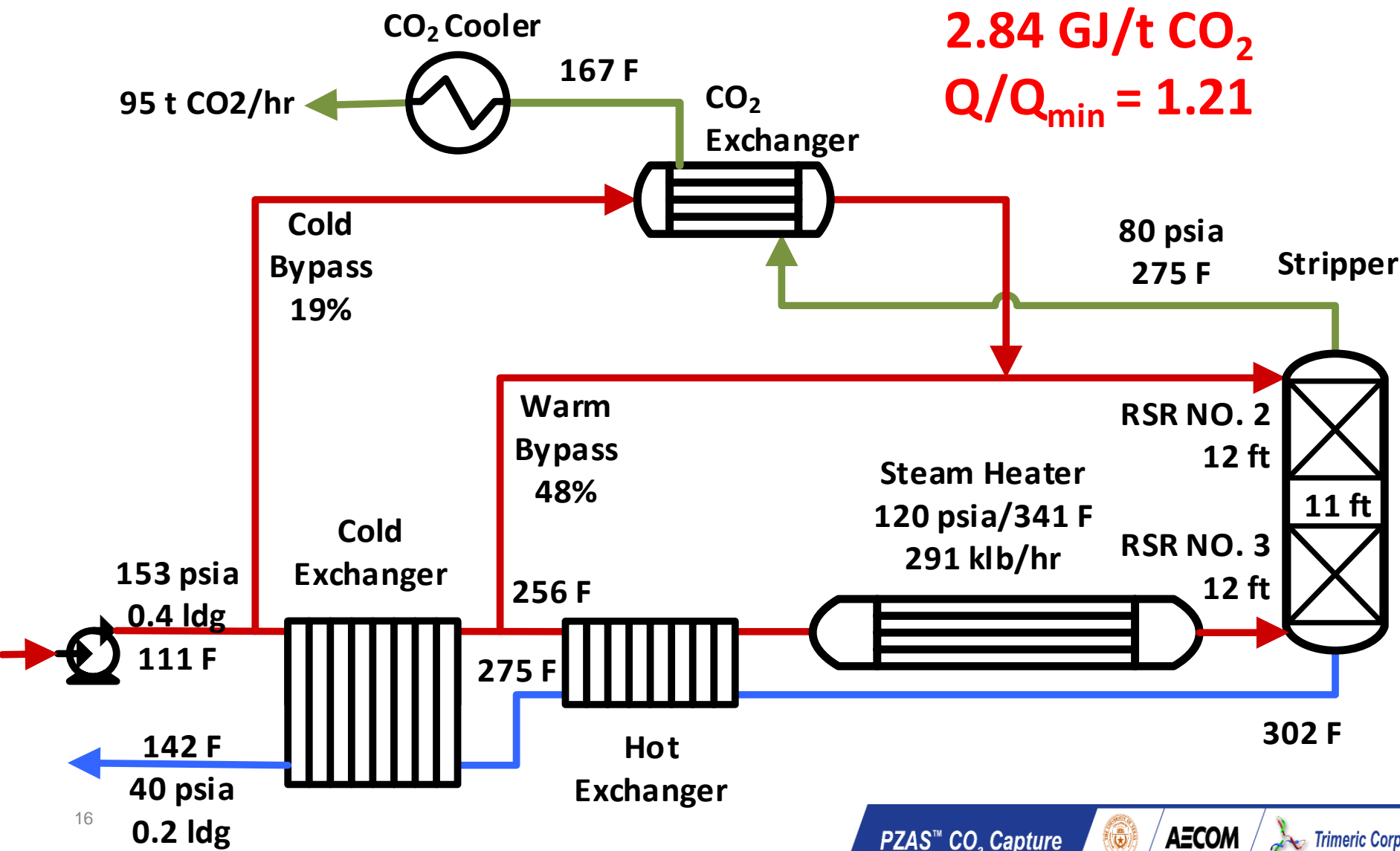


Advanced Stripper (for 1 GT+ 1 GB)

NTU = 8, 24 ft packing

2.84 GJ/t CO₂

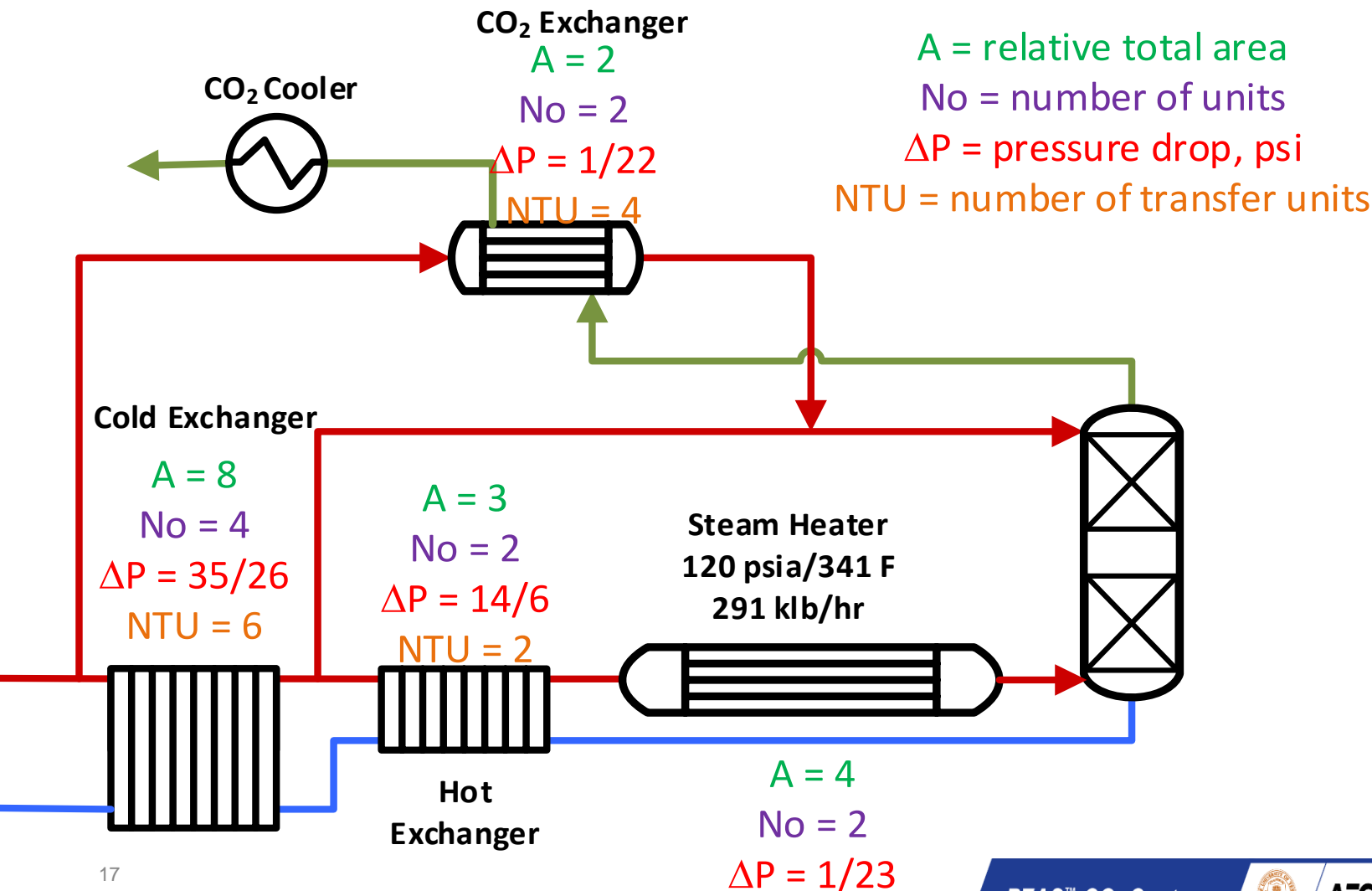
Q/Q_{min} = 1.21



Exchangers for both trains

low cost energy \rightarrow less area, larger ΔP

Total Exchanger purchase cost = \$3.6 MM



Steam provided by 2 gas-fired boilers

- 2 x 290,000 lbs/hr, one for each absorber
 - Saturated steam at 140 psia
 - Air preheater to reduce flue gas to 250 F
 - Flue gas fed to absorber for 90% removal
- @ \$50/t CO₂ for 45Q and EOR, the C in natural gas is worth \$2.66/MMBtu.
- @ 29 t CO₂/hr - \$13 MM/yr
- With 90% removal the incr fuel cost < zero if gas < \$2.4/MMBtu.
 - Current gas price is 1.2 – 2 \$/MMBtu

Design: One Reciprocating Compressor/Absorber

- Recip consistent with high inlet P
- Recip provides better turndown than centrifugal
- Purchase Cost about \$700/hp
- Cost Comparison with 1 machine per absorber

	Reciprocating	Integrally Geared Centrifugal
Power per machine, HP	9,075	8,708
Relative Cost	1.0	1.3

1 IGC machine for 2 absorbers: relative total cost = 0.85

Profitability

- Cash Flow w capture, \$65 MM/yr
 - Fuel cost, \$2/MMBtu, \$18/MWh
 - Variable maintenance & operating, \$5/MWH
 - 45Q tax credit, \$35/t CO₂, \$14/MWh
 - EOR value, \$15/t CO₂, \$6/MWh
 - Electricity sales price, \$18/MWh
 - Annual load factor, 75%
- Total cash flow w/o capture, \$15 MM/yr
 - 50% annual load factor
- Net cash flow created by capture, \$50 MM/yr
- With \$300 MM investment, 6 yr payout

Conclusions

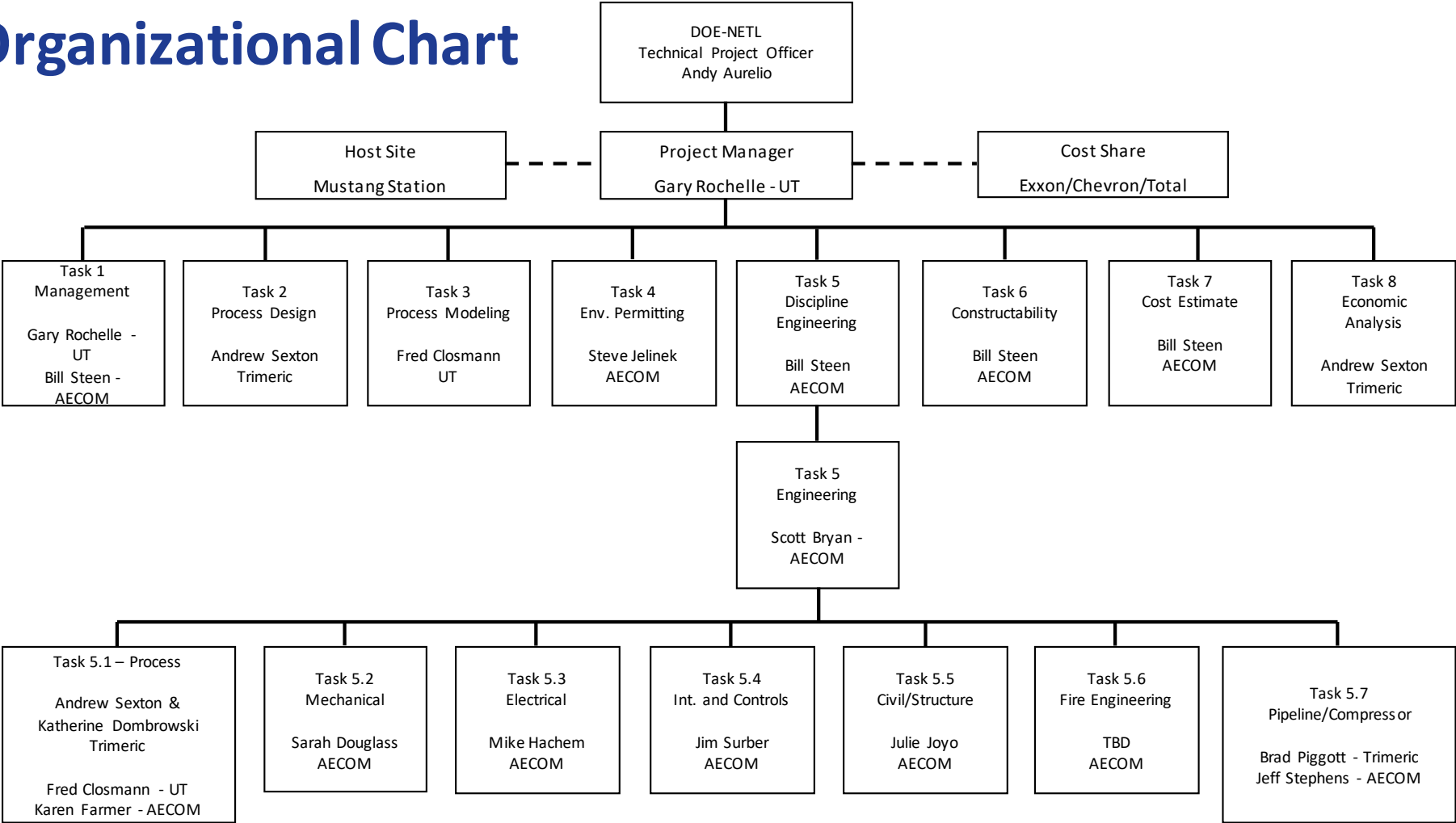
- PZAS uses 25 ft of absorber packing even w no DCC
- Air cooling feasible, even with swings in T_{amb}
- 80 psia stripper permits reciprocating compressors
- With cheap energy, PZAS uses 2.84 GJ/t CO₂
- With cheap gas, gas boiler provides zero incr fuel cost
- 6 year payout expected
- Detailed FEED on schedule for Fall 2021

Appendix

Project Team and Key Personnel

Party	Person	Role
NETL	Isaac Aurelio	Technical Project Officer
UT-Austin	Dr. Gary Rochelle	Principal Investigator
	Dr. Fred Closmann	Technical Proj Manager
AECOM	Dr. Bill Steen	AECOM Proj Manager
	Scott Bryan	Project Engineer
	Karen Farmer	AECOM Process Lead / Dept Project Manager
Trimeric	Dr. Andrew Sexton	Trimeric PjM
	Katherine Dombrowski	Process Lead

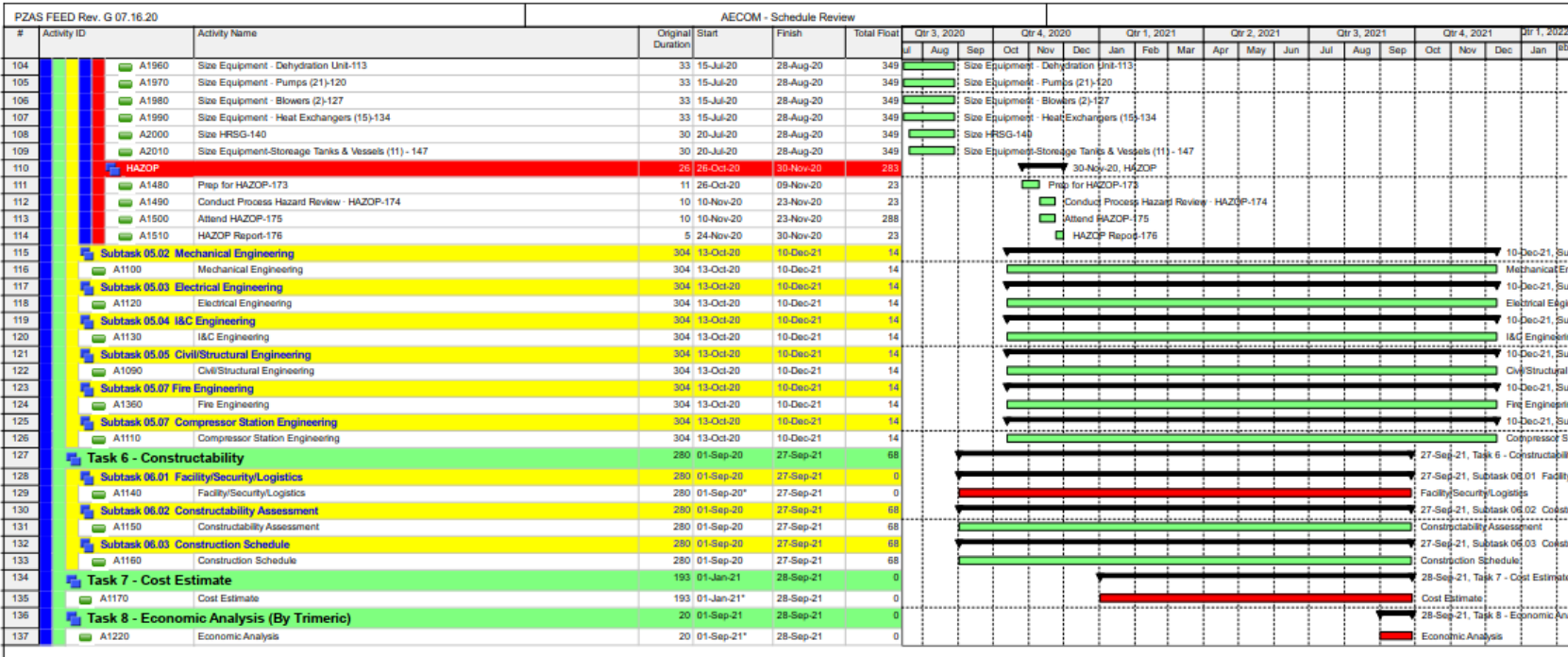
Organizational Chart







Gantt Chart



Still working to add fragments & detail to discipline engineering tasks