

FE0026334: ADVANCED CONTROL ARCHITECTURE AND SENSOR INFORMATION DEVELOPMENT

FOR PROCESS AUTOMATION, OPTIMIZATION, AND IMAGING OF CHEMICAL LOOPING SYSTEMS

Andrew Tong (PI), Umit Ozgunner (Co-PI), Arda Kurt (Co-PI)

Department of Chemical and Biomolecular Engineering

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Syngas Chemical Looping (SCL) Process for H₂ Production



Summary of DE-FE0026334



- Objective: develop an advanced process automation control architecture and imaging and optimization sensor information for the OSU chemical looping process
 - Develop HLC-SMC control scheme for process automation (OSU ECE)
 - Establish sensor algorithm for high temperature ECVT (Tech4Imaging)
 - Integrate process performance parameters with FocalPoint Optimization System (B&W)
 - Prepare and test process control and optimization concepts in 25 kW_{th} sub-pilot test unit (OSU CBE)



- OSU chemical looping technology: advanced solid and gaseous fuel conversion process for H₂ and electricity cogeneration with in-situ CO₂ capture
- Phase I: test control concept in an integrated sub-pilot test unit at high temperature, reactive conditions
- Phase II: demonstrate control concept at commercially applicable pilot scale test unit at high temperature, high pressure, reactive conditions



Autonomous Process Control Concept

The Ohio State University

Sliding Mode Controller (SMC)

- Advantage: State trajectory control, robustness
- Controller changes behavior as the state trajectory crosses the surface
- Exemplary mathematical form:

 $\ddot{x} + a_2 \dot{x} + a_1 x = u,$

$$u = -Msign(s), s = cx + \dot{x}, a_1, a_2, M, c - const$$

- Two stages:
 - Reaching mode: to get to the sliding surface
 - Sliding mode: reduced order motion on the surface
- Disadvantage: chattering →
 - actuator wear-and-tear
 - potential plant excitement





Utkin, V., "Variable structure systems with sliding modes," *Automatic Control, IEEE Transactions on*, vol.22, no.2, pp.212,222, Apr 1977

Matlab simulation of a sliding mode controller design for pressure control

- Control law: rate of valve opening change
- $u = \frac{dx}{dt}$ • S2 Controller: • $u = M_2 \cdot sign(S_2)$ • $S_2 = \frac{dP}{dt} - RR$ • RR = 1 psi/min• S3 Controller: • $u = M_3 \cdot sign(S_3)$ • $S_3 = \frac{dP}{dt} + (P - P_{sp}) \cdot K$ • $P_{sp} = 30psig, K = \frac{1}{2}min^{-1}$



Phase Plane



SCL Pilot Unit Pressurization/Depressurization

Ramp surface:

$$u = M_2 \cdot sign(S_2)$$
$$S_2 = \frac{dP}{dt} - RR$$
$$RR: Ramp \ rate$$

SS surface:

$$u = M_{3} \cdot sign(S_{3})$$

$$S_{2} = \frac{dP}{dt} + (P - P_{sp}) \cdot K$$

$$P_{sp} = setpoint, K = const$$

$$u = \frac{dx}{dt}$$





Design of adaptive M





Implementation of automatic start-up algorithm

- Pre-set operation goals
- HLC-SMC structure
- 1-click startup for fluidization, entrainment and maintaining circulation during heat-up
- Fuel injection upon reaching reaction temperatures and operation 1-click acknowledgement

Automatic Operation Sequence	Heater Power	OFF	
Manual Step 1: Start Fluidization	Auto Combustor Air	OFF	
Step 2: Start Circulation Step 3: Heating Step 4: Establish Pressure Balance	Auto L-Valve	OFF	
Step 5: Fuel Injection Step 6: Stop Fuel Injection	Auto Temperature Ramp	OFF	Reaction Temperature 0 C Temperature Ramp Rate 0 C/min
Step 7: Shutdown	Auto Capacity Control	OFF	Syngas Capacity 0.0 kW
Start Automatic Operation			Narogen 1:1 H2 CO
Start Fuel Injection			
Shutdown			Home Coal Inj. Manifold Pressure Temps Reactive Gas Manifold Gas Analysis

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	<pre>(* Calculate Ut based on riser top temperature, latm correlation *) AIR_UTS_R:=((TZ243/10)*2/10**6+(TZ243/10)*0.0041+1.7669)/10**5; (* The unit of TE tags in AIR_DEN_R:=653.32/(TZ43/10)+273.15); Ut:=0.154*(0.0015*1.6+2500*9.8/AIR_UTS_R**0.6+AIR_DEN_R**0.4)**(5/7); Ut:=1.74*8207(10.0015*2500*9.8/AIR_DEN_R); Ut:= Ut; else Ut:= Ut; end_if; Ft_ent:= Ut/(273+TE234/10)*298*0.002*60000; (* Decide whether combutor gas flow is sufficient to start L-valve*) if PII0*(273+TE234/10)/298/0.002/60000-0.5 >= Ut then IERT:= 0; end_if; (* Decide whether the bed is circulating based on riser DP fluctuation *) if PDI7261[STD>=1 then IsCirc := 1; end_if; ************************************</pre>
	IsCirc := 0; end_if;



Start-up sequence test drive

- Achieved automatic startup with zero operator intervention
- Maintained oxygen carrier circulation at minimal solid flow rate using self-regulating aeration and entrainment gases



Circulation rate control



Fuel injection mode



Fuel injection mode



- Simultaneous control actions correctly executed by all SMCs with no operator intervention
- Achieved ~99% syngas conversion
- No gas breakthrough was observed in either reactor



SMC Response to Capacity Change



Combustor Performance Investigation - ECVT







Combustor Performance Investigation - ECVT

Image Reconstruction:



Image reconstruction frame rate: 80 Hz ~ 260 Hz

Combustor Performance Investigation - ECVT

Slug Velocity vs. Gas Velocity



Slug Frequency vs. Gas Velocity





23 C, 600 slpm

Additional Work

- Continued sub-pilot demonstration
 - Tuning adaptive SMC
 - Comparative testing with conventional controls
- FocalPoint Integration
 - HLC Performance
 - Sensor fault detection
 - Thermodynamic Optimization parameters
- ECVT Solid flow control development
 - Moving bed flow characterization
 - Electrical characterization of ceramic and oxygen carrier material

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