

# Techno-economic Evaluation of State-of-the-Art and Advanced Post-Combustion Capture Plants

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Office of Program Performance and Benefits

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U.S. DEPARTMENT OF

**ENERGY**

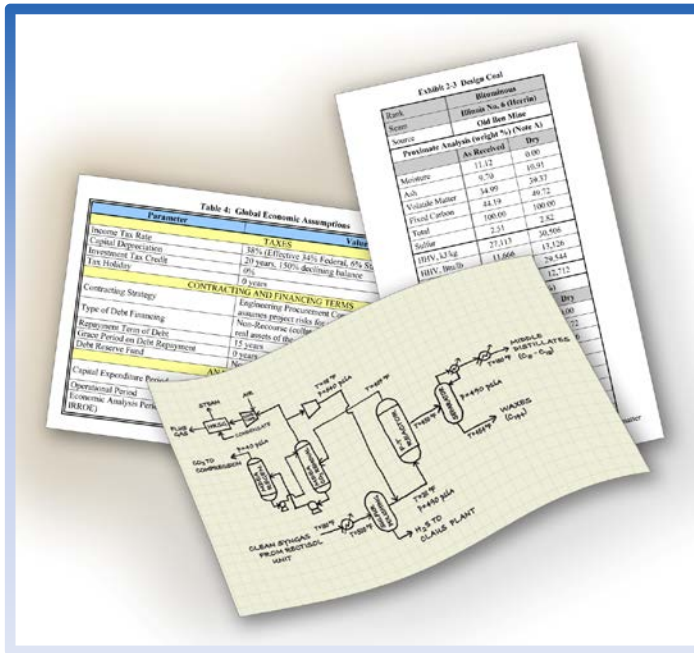
National Energy  
Technology Laboratory

- **Outline**

- Bituminous Baseline Study  
Revision 3
- Clean Coal Research  
Program Goal Review
- NETL Advanced Capture  
Technology Assessments

- **Acknowledgements**

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# BITUMINOUS BASELINE STUDY REVISION 3

# Update to the Bituminous Baseline Study

## Overview

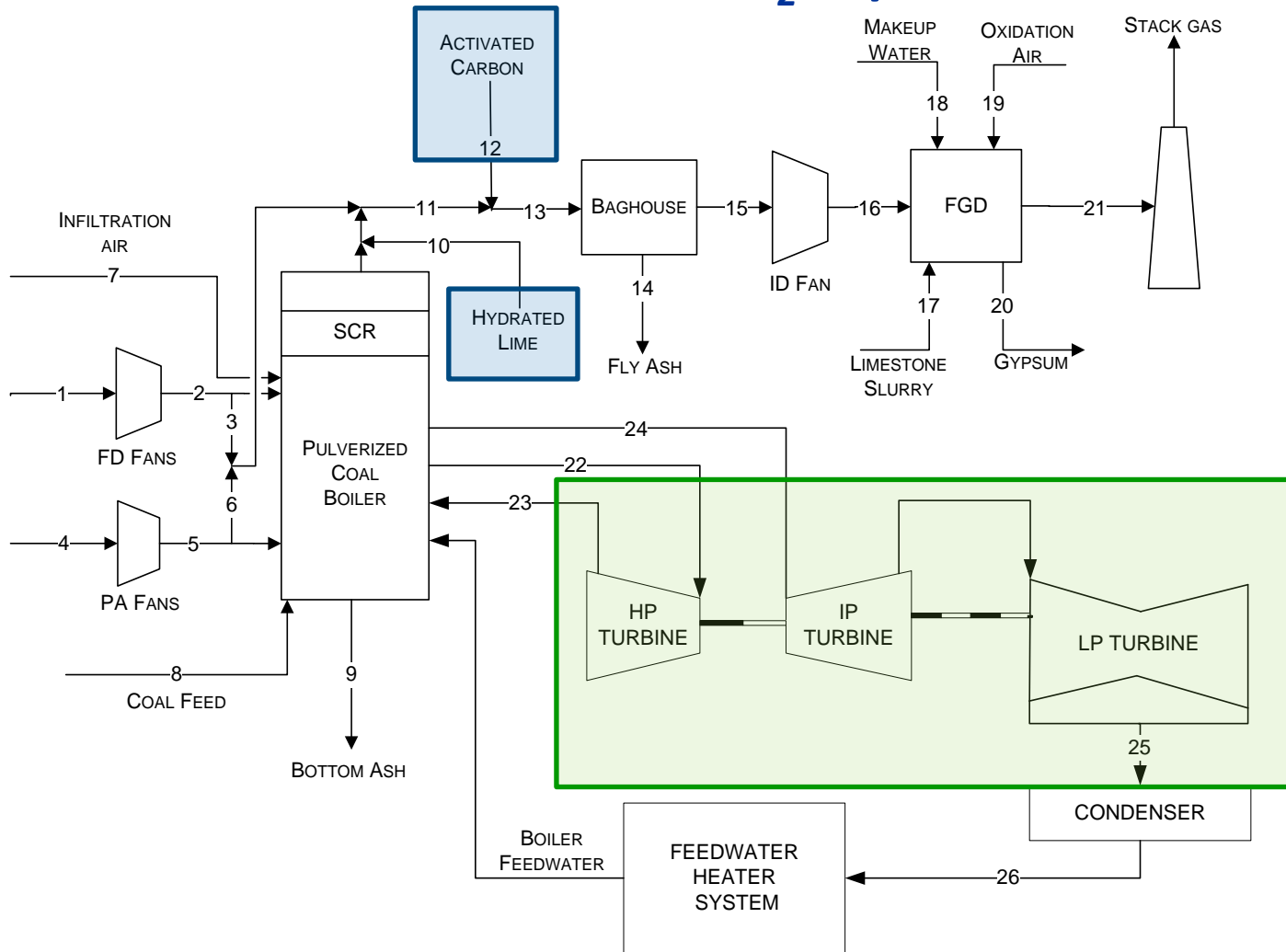
**Full Title: *Cost and Performance Baseline for Fossil Energy Plants, Volume 1: Bituminous Coal and Natural Gas to Electricity, Revision 3, Fall/Winter 2014***

**Purpose: *to provide a basis for evaluation of advanced technologies on a consistent set of technical and economic assumptions***

- Major change summary
  - Updated basis for performance and cost for CO<sub>2</sub> capture system, CO<sub>2</sub> compression, steam turbines, natural gas turbines
  - Update of all cases to 2011\$
  - Updated environmental control train to address EPA regulations
  - Updated tables to include additional data
  - New case numbering system (conforms with Low Rank study)
  - Minimal changes to IGCC cases (further updates coming soon!!)

# Flowsheet Changes

## B11A and B12A – No CO<sub>2</sub> Capture

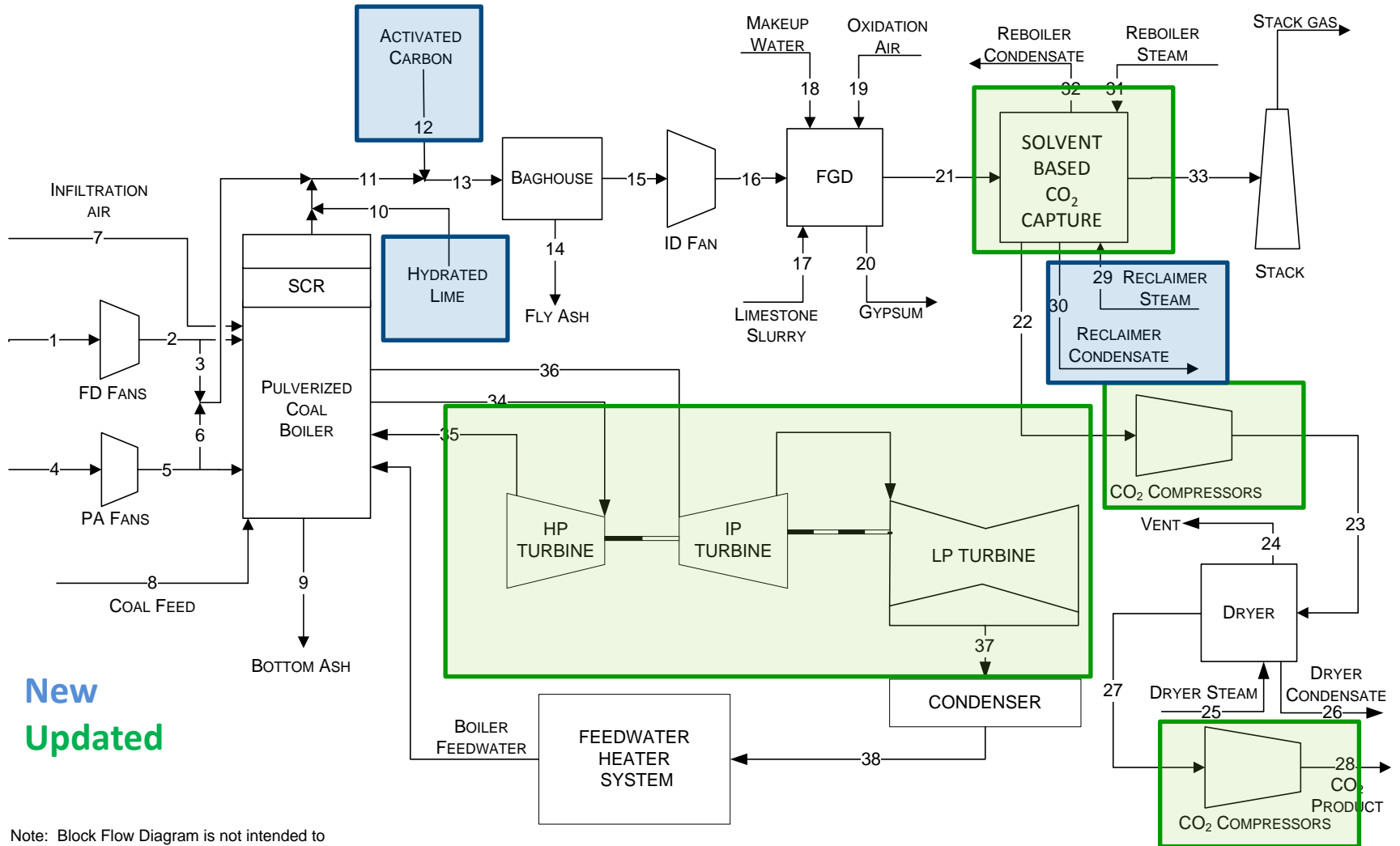


New  
Updated

Note: Block Flow Diagram is not intended to represent a complete material balance. Only major process streams and equipment are shown.

# Flowsheet Changes

## B11B and B12B – with CO<sub>2</sub> Capture

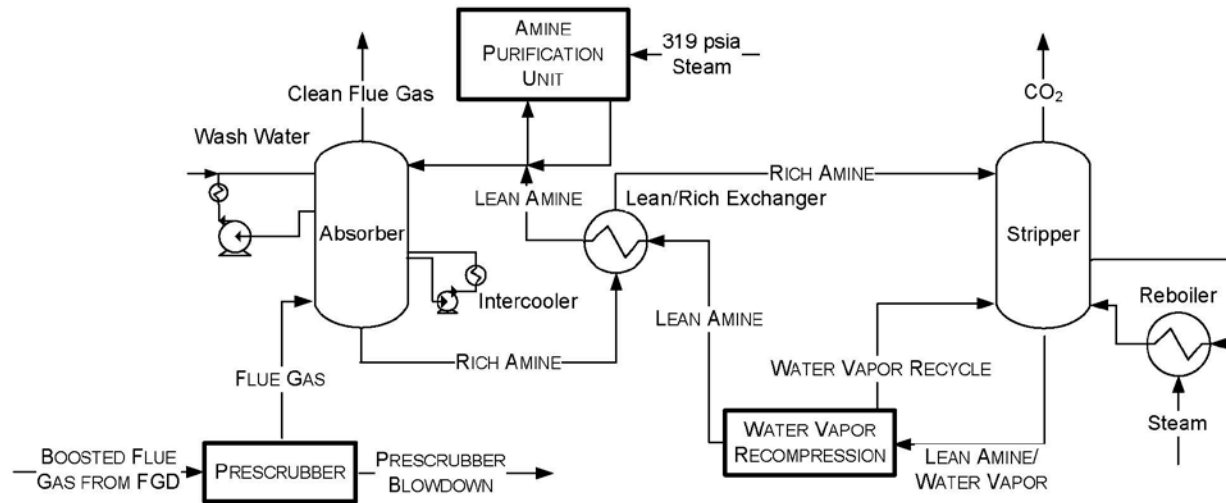


New  
Updated

Note: Block Flow Diagram is not intended to represent a complete material balance. Only major process streams and equipment are shown.

# PC & NGCC Cases

## *CO<sub>2</sub> Capture System*



### Amine-based capture system

#### Features:

Absorber – acid brick lined concrete structure

90 % CO<sub>2</sub> Capture

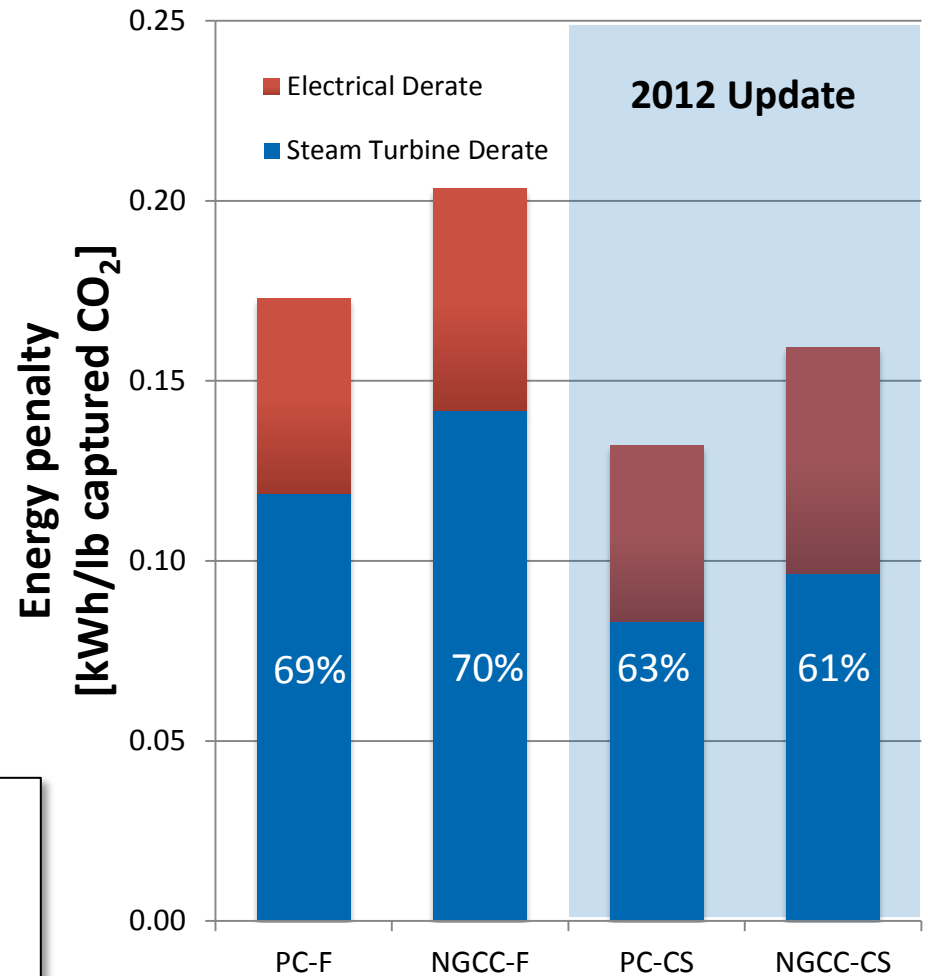
Pre-scrubber used in coal cases only

# Baseline Greenfield Capture and Compression Technology Update

PC Plants	Quote Vintage	
Metric	2005	2012
Net Energy Penalty [kWh <sub>net</sub> /lb CO <sub>2</sub> Captured]	0.17	0.13
Reference Capital Cost [\$2011/tpd CO <sub>2</sub> Capt. @ full load]	\$45,000	\$47,900
CO <sub>2</sub> Capture Basis [tpd]	11,210	11,210

**PC:** ~25% reduction in regeneration energy penalty

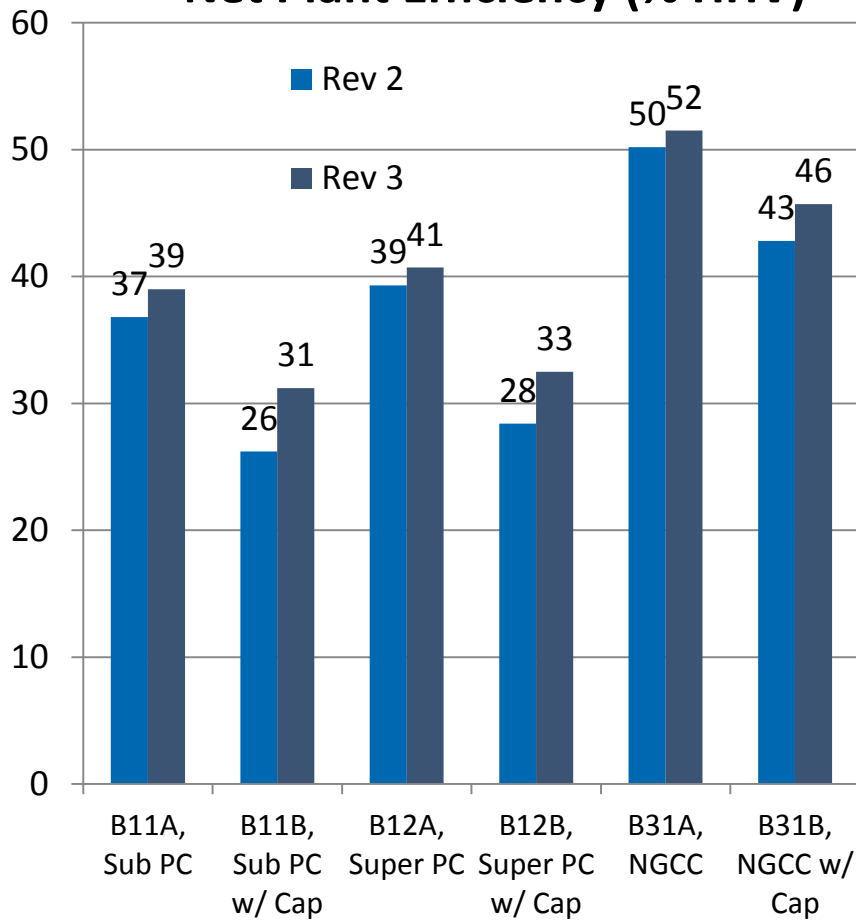
**NGCC:** ~20% reduction in regeneration energy penalty



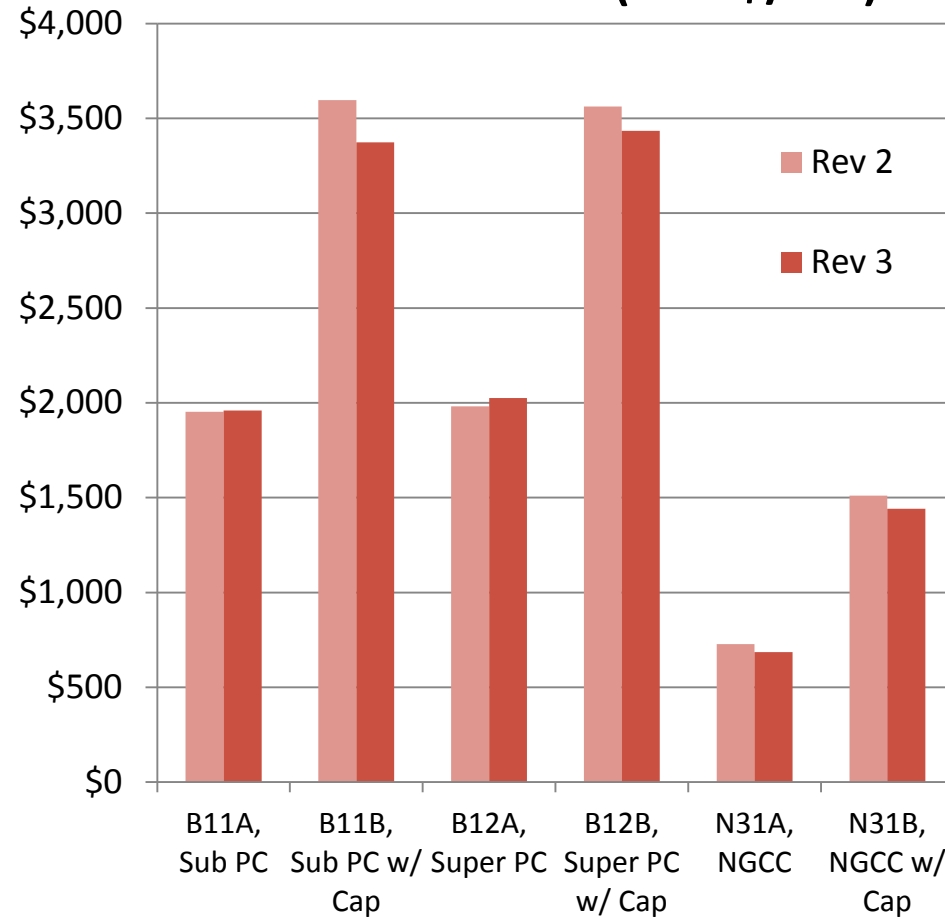


# Bituminous Baseline Revision Comparisons

## Net Plant Efficiency (% HHV)

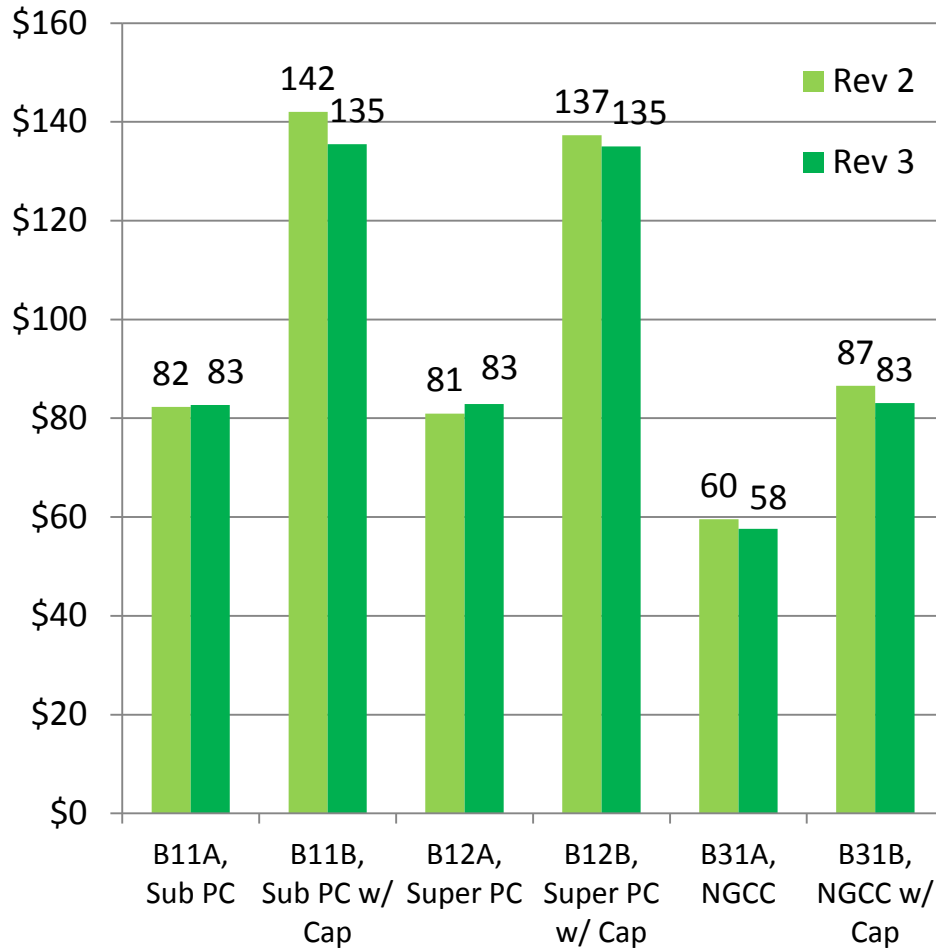


## Total Plant Cost (2011\$/kW)

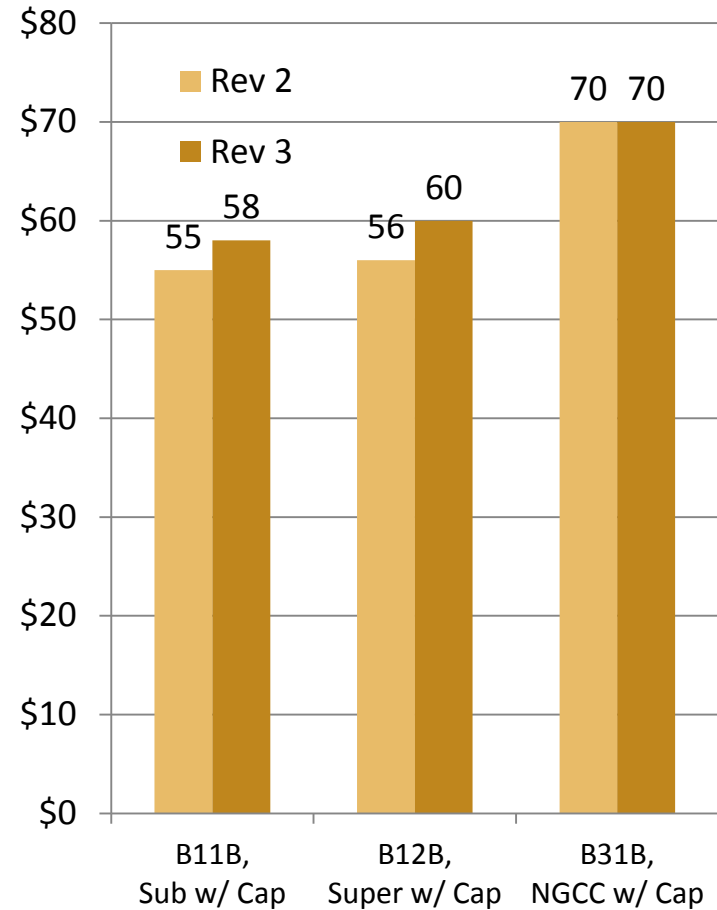


# Bituminous Baseline Revision Comparisons (con't)

**Total COE w/o T&S  
(2011\$/MWh)**



**CO<sub>2</sub> Capture Cost w/o T&S  
(2011\$/tonne)**

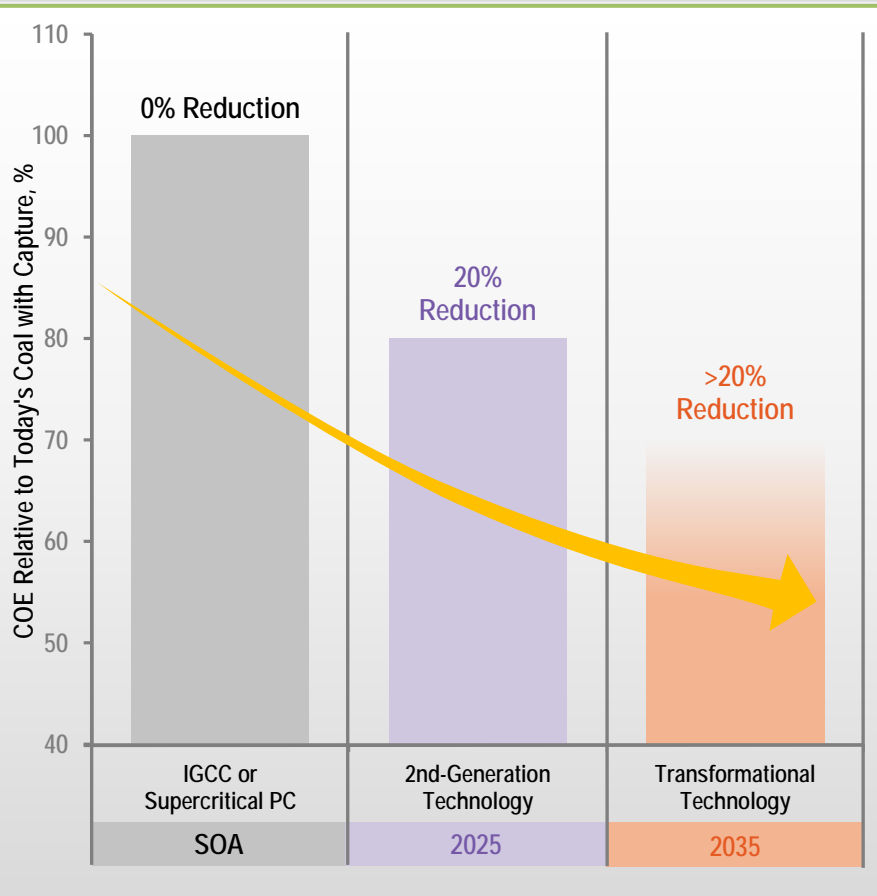




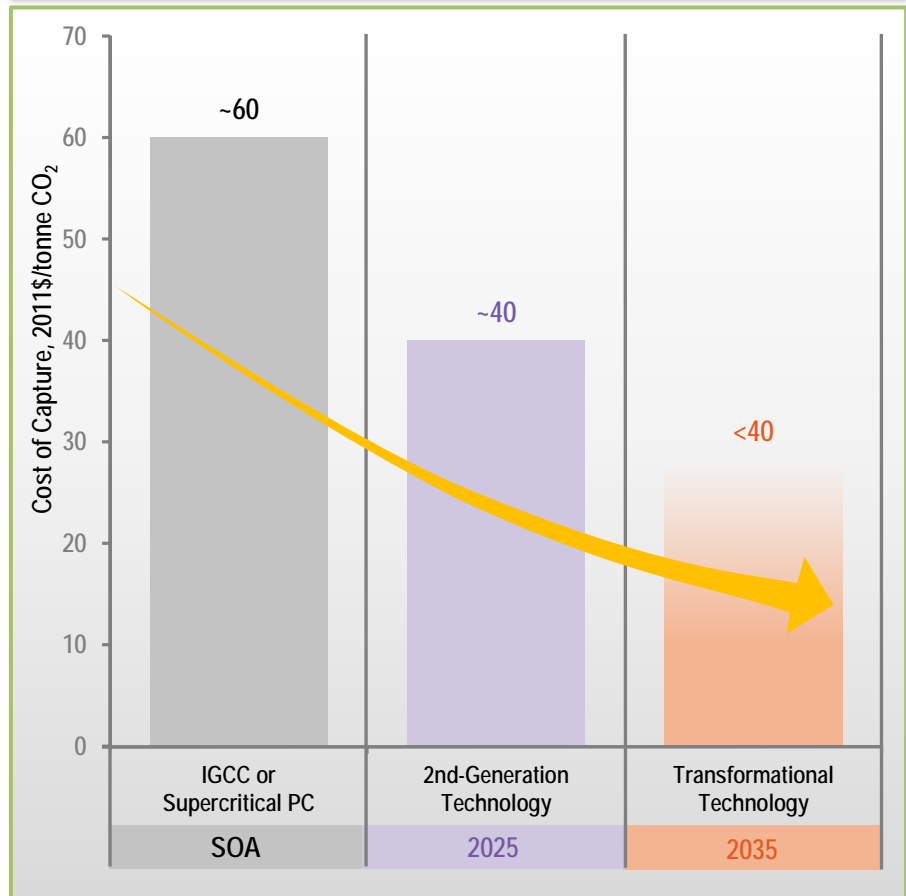
# Clean Coal Research Program Goals

*Driving Down the COE and Cost of CO<sub>2</sub> Capture of Coal Power with CCS*

*Cost of Electricity Reduction Targets*



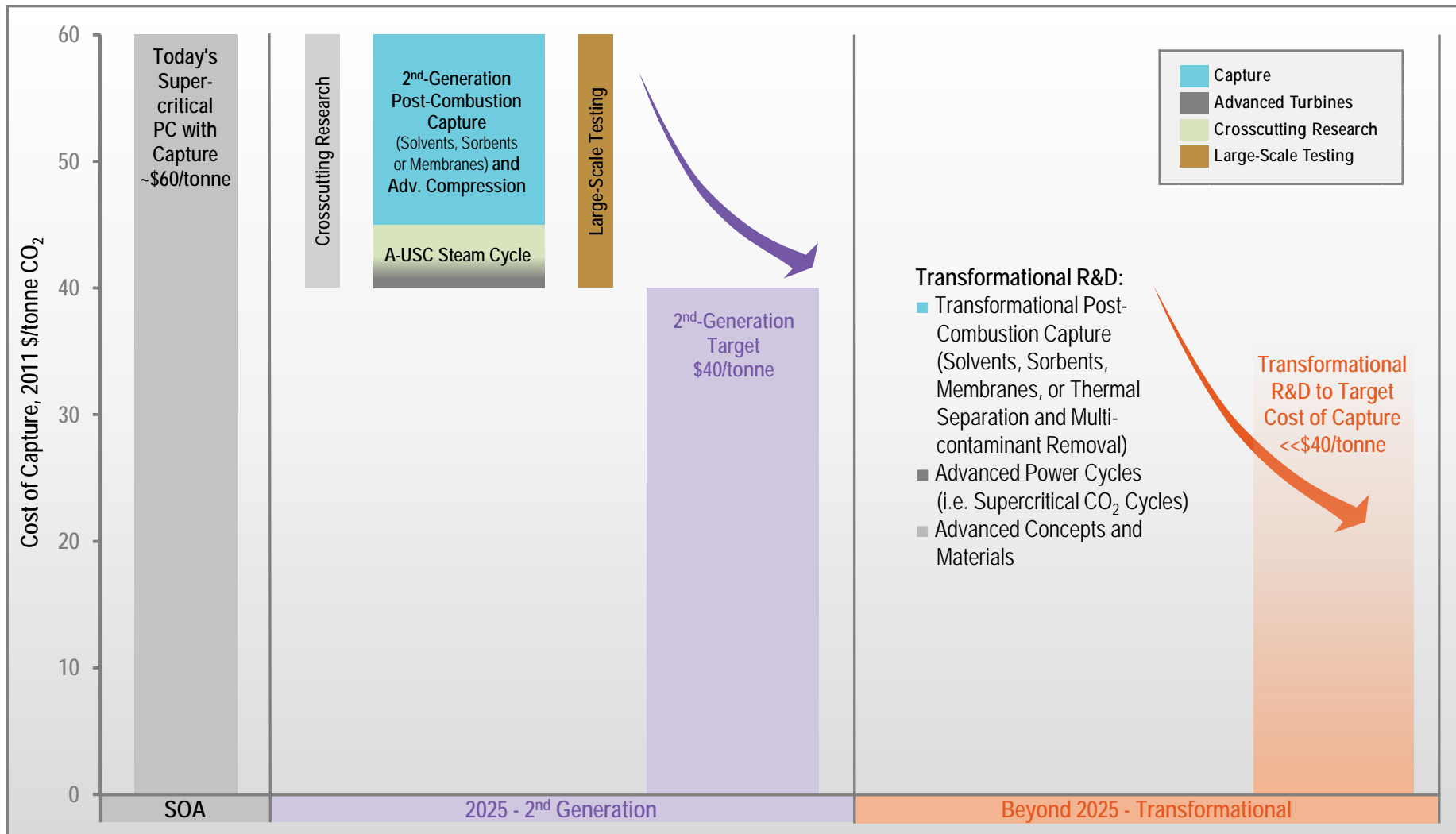
*Corresponding Cost of CO<sub>2</sub> Capture Targets*



Goals shown are for greenfield plants. Costs are nth-of-a-kind, are for the first year of plant operation, and include compression to 2215 psia but exclude CO<sub>2</sub> transport and storage costs. Today's capture costs are relative to Today's SCPC without CO<sub>2</sub> capture. 2025 and 2035 capture costs are relative to an A-USC PC without CO<sub>2</sub> capture.

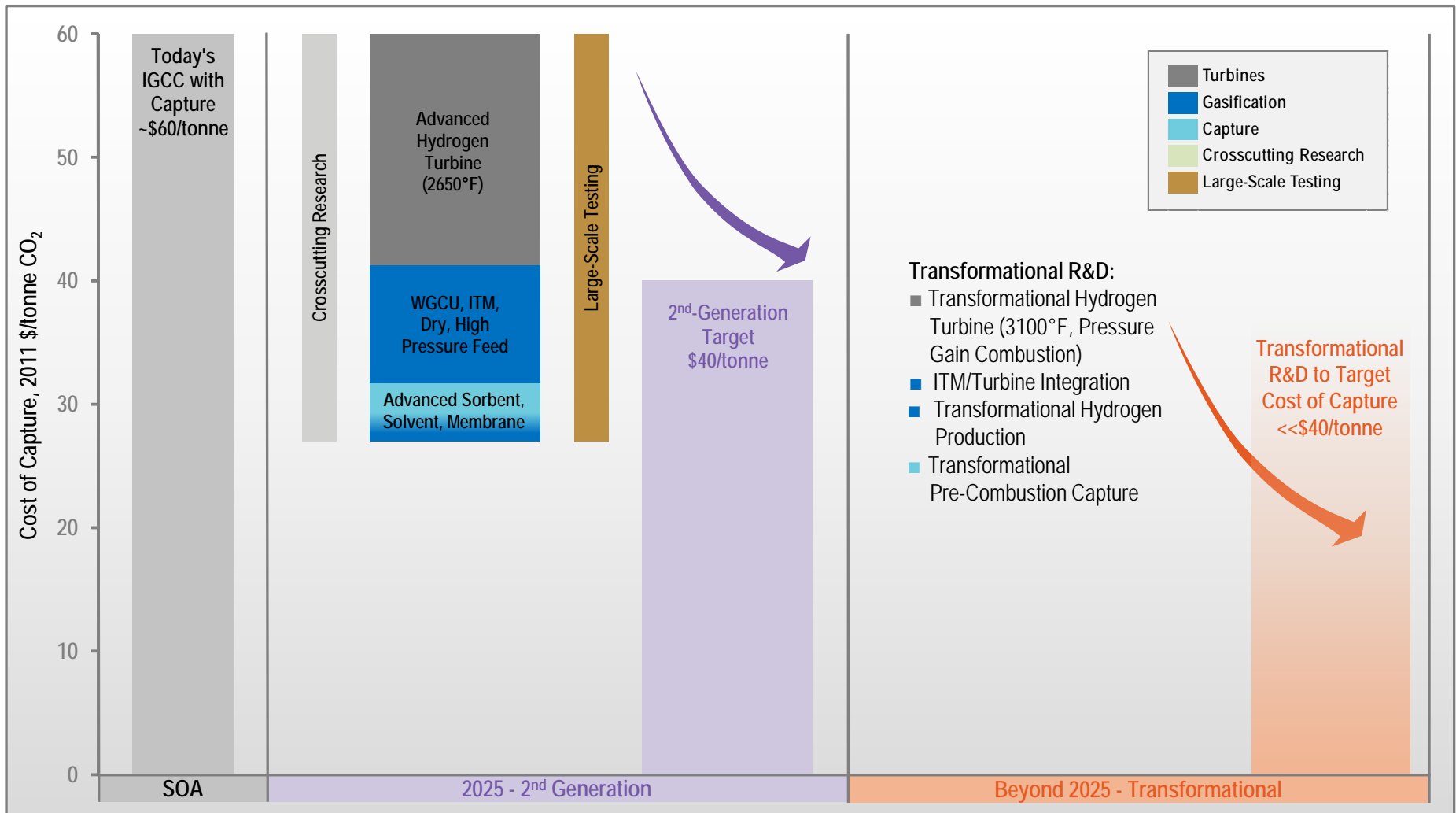
# R&D Driving Down the Cost of CO<sub>2</sub> Capture

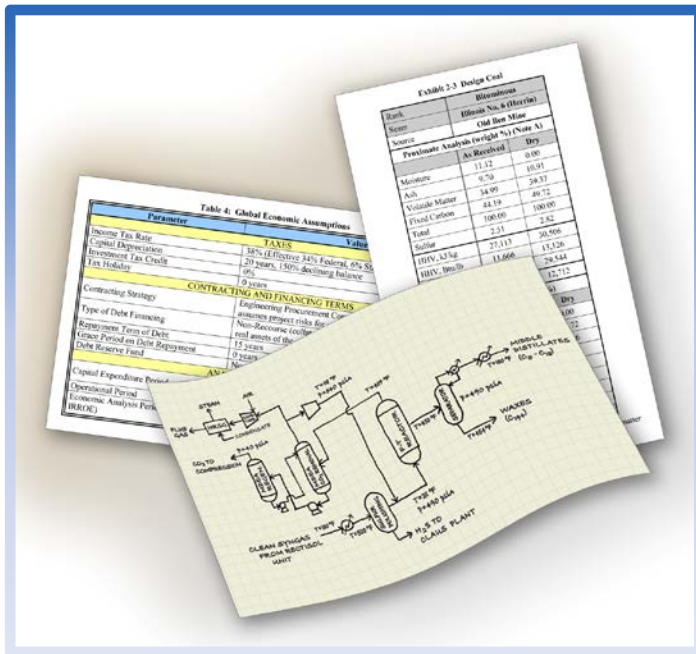
## Greenfield Post-Combustion Capture Plants



# R&D Driving Down the Cost of CO<sub>2</sub> Capture

## IGCC with Pre-Combustion Capture





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# ADVANCED CAPTURE TECHNOLOGY ASSESSMENTS

# NETL/OPPB Advanced Capture Ongoing Analyses

- **“Current and Future Technologies for Post-Combustion Capture” i.e. PCC Pathway Study**
  - Coal – Update to 2011 dollars; preliminary consideration of CO<sub>2</sub> purification
  - NGCC – In progress
- **Screening studies (pre- and post-combustion capture)**
  - Solvents
  - Sorbents
  - Membranes
  - Internal and external
- **R&D Guidance for Post-Combustion Capture Techno-Economic Evaluations**

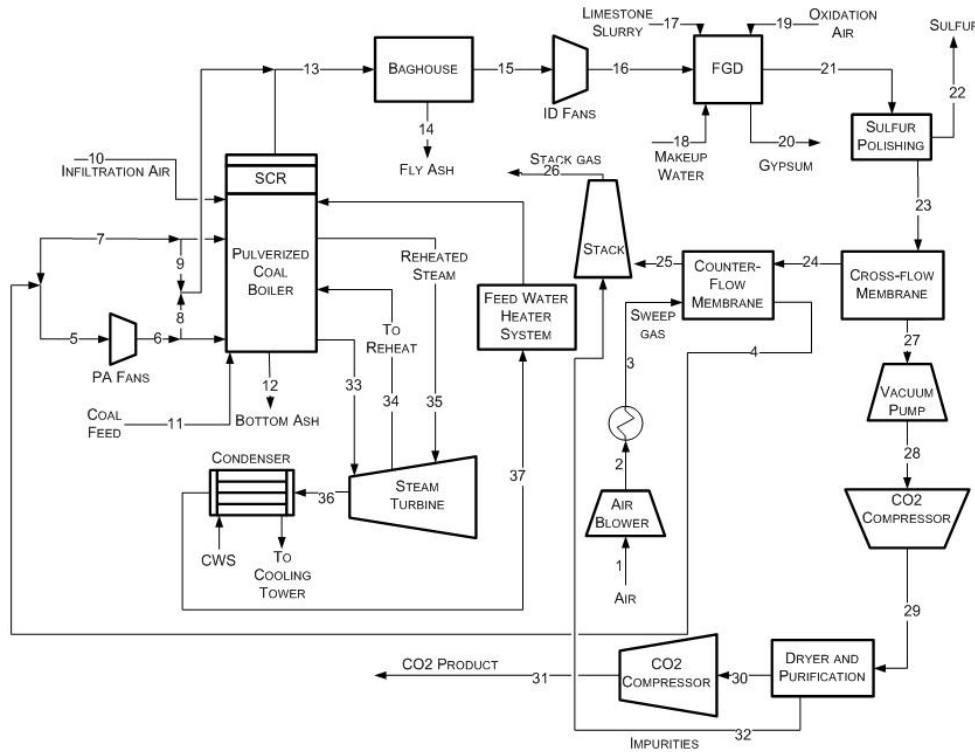


# PCC Pathway Study

## *Objectives & Scope*

- **Objectives:**
  - Develop technology pathways that feature post-combustion CCS-enabled PC plants that achieve DOE goals
  - Utilize the pathway studies to inform technology development through identification of performance and cost targets
- **Technologies included:**
  - 2<sup>nd</sup>-generation post-combustion CO<sub>2</sub> capture
  - Adv. Ultrasupercritical (A-USC steam) conditions (5000psig/1350F/1400F)
  - Advanced CO<sub>2</sub> compression
- **Scope:**
  - Pathway begins with 1<sup>st</sup> generation supercritical PC plant with today's post-combustion capture technology
  - Emerging technologies added based on mature stage of development, thus simulating “n<sup>th</sup>-of-a-kind” plant performance and cost
  - 2<sup>nd</sup>-generation post-combustion CO<sub>2</sub> capture and compression cost and performance adjusted to meet program goals

# PC with Adv. Membrane – Example to Meet Goals

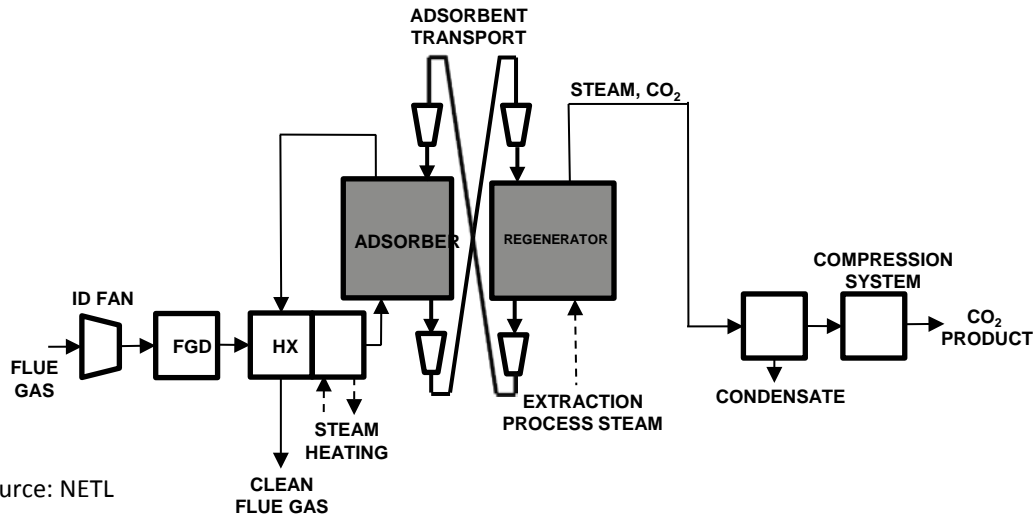


## Key Membrane Parameter Assumptions

- **CO<sub>2</sub> and SO<sub>2</sub> Permeance: 3,500 gpu**
- N<sub>2</sub>, O<sub>2</sub>, Ar Permeance: 100 gpu
- H<sub>2</sub>O Permeance: 5,000 gpu
- **Pressure drop: 1.0 psi (flue gas and sweep sides)**
- Vacuum pump achieves 0.2 bar pressure
- Membrane replacement time 5 years
- Membrane surface area: 1,500,000 m<sup>2</sup>
- **Membrane installed cost \$127/m<sup>2</sup>**
- Membrane replacement cost \$17/m<sup>2</sup>

Capture/Compression Impact Metric	Amine Quote Vintage		Adv. Membrane
	2005	2012	
Net Energy Penalty [kWh <sub>net</sub> /lb CO <sub>2</sub> Captured]	0.17	0.13	0.11
Reference Capital Cost [\$2011/tpd CO <sub>2</sub> Capt. @ full load]	\$45,000	\$47,900	\$39,100
CO <sub>2</sub> Capture Basis [tpd]	11,210	11,210	11,185

# PC with Adv. Adsorbent – Example to Meet Goals



Source: NETL

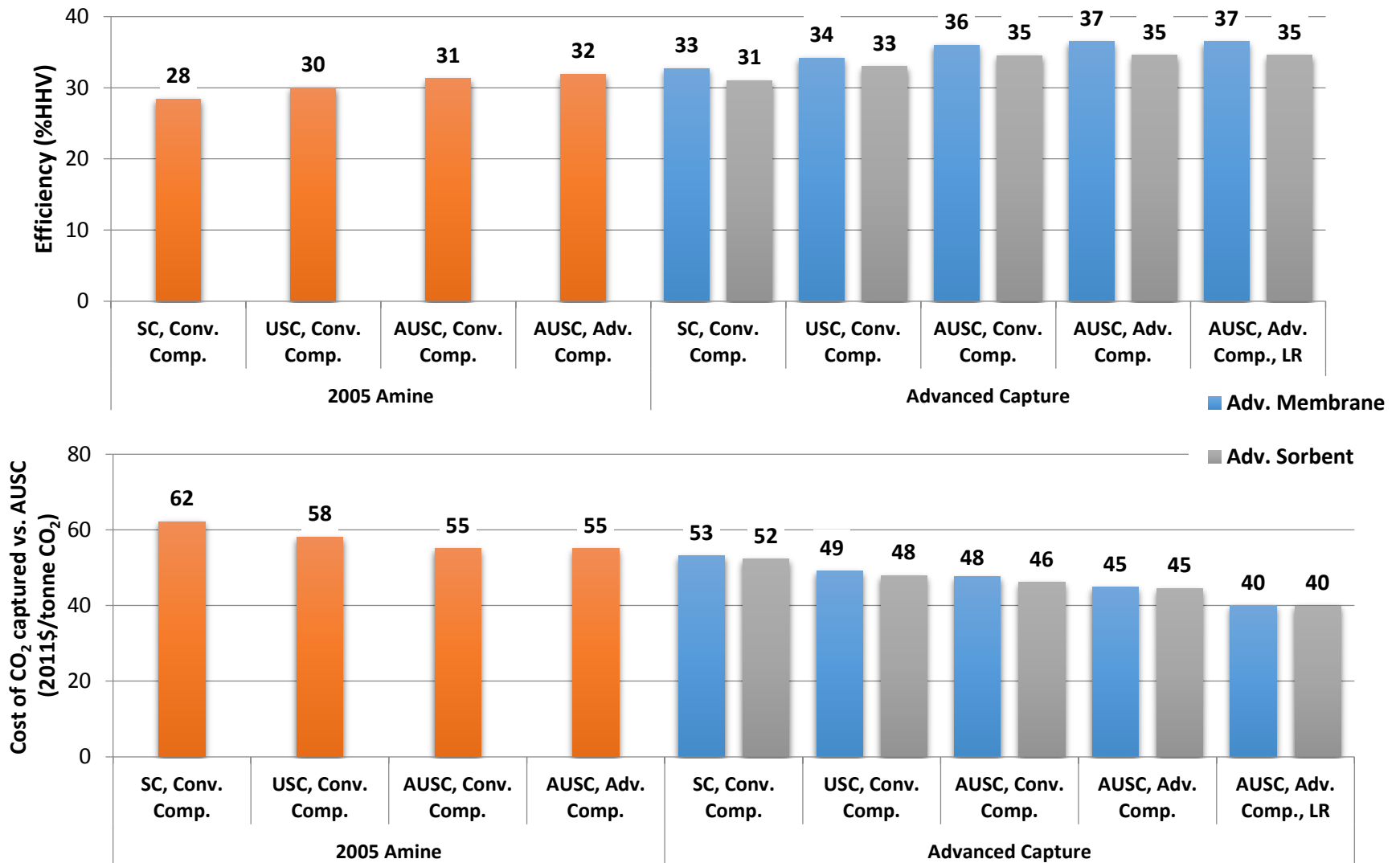
## Key Adsorbent Parameter Assumptions

- Adsorbent: alkalized alumina; 3/8 inch diameter spheres
- Adsorbent cost: \$5/lb
- **Sorbent CO<sub>2</sub> loading: 3.0%**
- Adsorber and regenerator temperature: 140°C
- Adsorber and regenerator pressure drop: 0.4 psi
- Adsorbent entrains 1.0 wt% of inlet N<sub>2</sub>, O<sub>2</sub> and water vapor to the regenerator
- **Regenerator off-gas: 50 mole % CO<sub>2</sub>**
- Adsorber-regenerator type: Moving bed
- Adsorbent transport: Bucket conveyor-elevators

- The adv. sorbent process requires considerable extraction steam consumption for flue gas heating and for adsorbent regeneration (> 1x10<sup>6</sup> lb/hr) and large BFW makeup treatment system
- The reaction vessels are very large and mechanical adsorbent circulation is used for the large adsorbent circulation rate required (> 31 x 10<sup>6</sup> lb/hr)

Capture/Compression Impact	Amine Quote Vintage		Adv. Sorbent
	2005	2012	
Net Energy Penalty [kWh <sub>net</sub> /lb CO <sub>2</sub> Captured]	0.17	0.13	0.13
Reference Capital Cost [\$2011/tpd CO <sub>2</sub> Capt. @ full load]	\$45,000	\$47,900	<b>\$37,700</b>
CO <sub>2</sub> Capture Basis [tpd]	11,210	11,210	11,349

# PCC Pathway Efficiency and Cost of Capture



**NOTES:**

- Amine-based cases are consistent with NETL Bituminous Baseline Rev. 2 Report
- All membrane and sorbent-based cases utilize enhanced performance and cost parameters

# CO<sub>2</sub> Purification

- Purification of the CO<sub>2</sub> product stream will likely be necessary for most end-uses
- Preliminary evaluation of refining CO<sub>2</sub> purification to PCC Pathway cases
  - CO<sub>2</sub> purity prior to purification: 92-97%
  - Impact using external refrigeration cycles
    - Efficiency reduction ~2% points
    - COE increase 8-10%
- Other potential purification options:
  - Auto-refrigeration cycles
  - Membranes
  - Other capture process optimizations

Purity Specifications	
CO <sub>2</sub>	≥ 95 vol%
O <sub>2</sub>	10 – 100 ppmv
H <sub>2</sub> O	500 ppm
N <sub>2</sub> , Ar, CH <sub>4</sub> , H <sub>2</sub>	1 – 4 vol%
CO	35 ppm
H <sub>2</sub> S	75 – 100 ppmv
SO <sub>2</sub>	50 – 100 ppmv
...etc.	

# Current and Future Technologies for Post-Combustion Capture: NGCC

- **Objective: Evaluate impact of advanced CO<sub>2</sub> capture technologies in an NGCC plant**
- **Preliminary conclusions:**
  - Sorbents and membranes more sensitive to lower CO<sub>2</sub> concentration of NGCC flue gas (~4% vs. ~14% for PC) than solvents
  - Exhaust gas recirculation (EGR) key to increase CO<sub>2</sub> concentration in flue gas for sorbents and membranes

# Advanced Capture Technology Screening Studies

- **Post-combustion capture solvents:**
  - Model/predict process improvements that are applicable to many capture technologies:
    - L/R exchanger temperature approach
    - CO<sub>2</sub> Stripper regen pressure
    - Advanced heat integration schemes
  - Forecast potential of combining advanced capture technologies with advanced processes
- **Pairing of post-combustion capture technologies**
  - e.g. solvents and membranes
- **Pre-combustion capture sorbents/membranes:**
  - Pairing with advanced gas cleanup systems and CO<sub>2</sub> purification systems
- **NETL may contact you with requests for details about your project (i.e., design and/or performance aspects)**

