Pilot-Scale Silicone Process for Low-Cost CO₂ Capture

GE Global Research



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2014 NETL CO₂ Capture Technology Meeting July 30, 2014

Overview

Program Team



GE Global Research

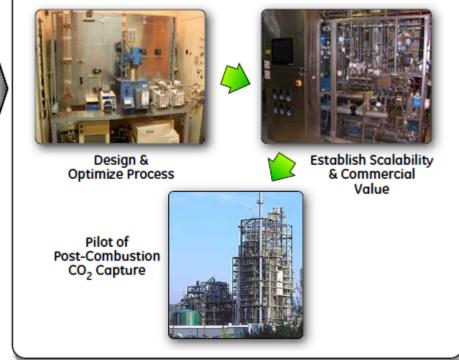
- Pilot-scale design
- Construction/Operation
 of Continuous System
- EH&S Assessment
- Techno-economic Assessment
- Plant Modeling



- Pilot-scale Operation
- Assessment of Data
- Integration of Components

24 Month, \$5.7MM Program to Advance the Amino-Silicone Solvent Process for CO₂ Capture to Pilot Scale

Program Objectives: Design and optimize a new process for a novel silicone CO₂ capture solvent and establish scalability and potential for commercialization of post-combustion capture of CO₂ from coal-fired power plants. A primary outcome will be a system capable of 90% capture efficiency with less than \$40/tonne CO₂ capture cost.



Technical Approach

- Design and construct pilot-scale unit and obtain parametric data to determine key scale-up parameters
- Perform an EH&S and technical and economic assessment to determine feasibility of commercial scale operation
- Develop scale-up strategy

Outcomes

- Strategy for future scale-up
- Technical and economic feasibility determined
- Environmental assessment

Anticipated Benefits of the Proposed Technology

- 90% CO₂ Capture
- \$40/tonne CO₂ capture cost

Scope

This two-year project is divided into two phases.

Phase I: 1/1/2014 - 12/31/2014

(\$1.5MM with 20% GE cost share)

- Develop preliminary process models and perform preliminary techno-economic analysis
- Perform preliminary EH&S risk assessment
- Design pilot-scale system and construct components

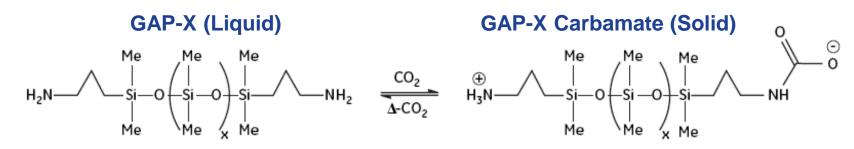
Phase II: 1/1/2015 - 12/31/2015

(\$4.2MM with 20% GE cost share)

- Integrate aminosilicone specific components with the NCCC pilot-scale system
- Obtain and analyze engineering data from pilot tests at 0.5 MW scale
- Perform techno-economic analysis and update cost of carbon capture
- Develop scale-up strategy
- Perform technology EH&S risk assessment
- Develop cost estimate for full-scale manufacture of solvent

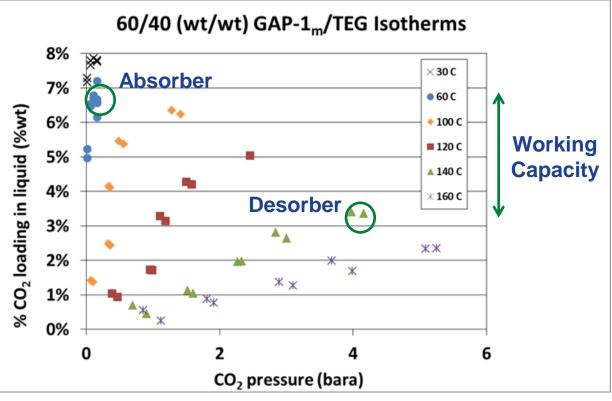


Aminosilicone Absorbent



GAP-1_m Absorbent Composition •40% GAP-0 •33% GAP-1 •19% GAP-2 •8% GAP-3

Carbamate does not precipitate in a 60/40 (wt/wt) GAP-1_m/TEG mixture





Summary of Aminosilicone Advantages

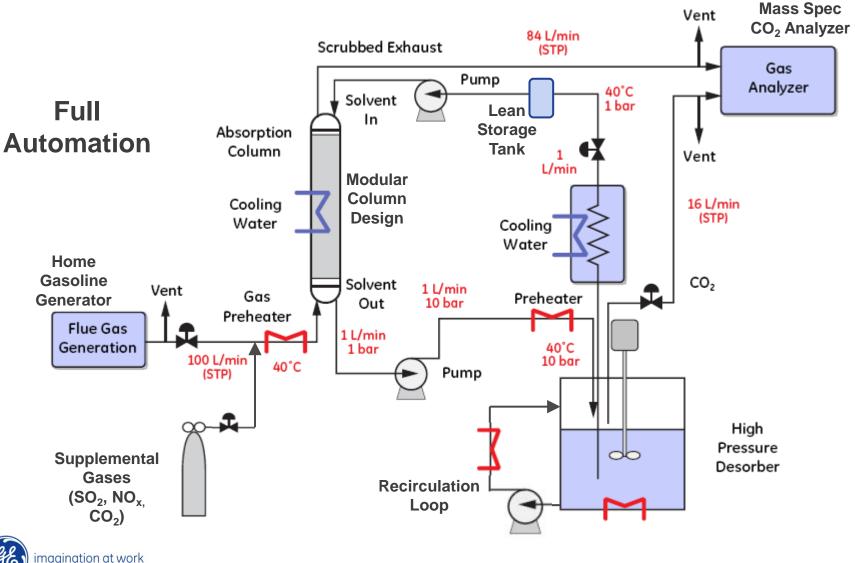
- Higher thermal stability (higher desorption T/greater capture capacity and/or pressure)
- Lower volatility
 - Simplified separations
 - Less energy wasted vaporizing solvent and/or water Lower airborne release rates
- Lower heat capacity
- Reduced corrosion
- Ability to remove water (useful in adjacent industries)
- Potentially decreased issues with aerosol formation

Challenges

- High viscosity (at low T and high loading)
- Higher heat of reaction
- Solvent cost



Bench-Scale Schematic

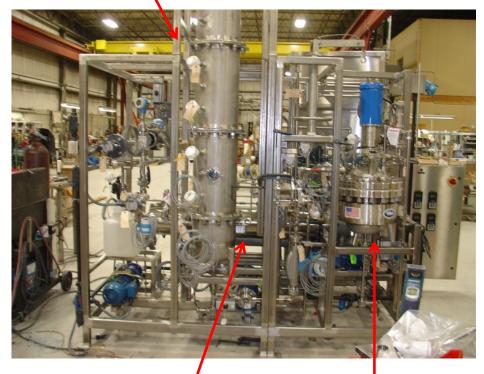


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Bench-Scale CO₂-Capture System



Absorber Column



Recycle Loop Heat Exchanger

Desorber

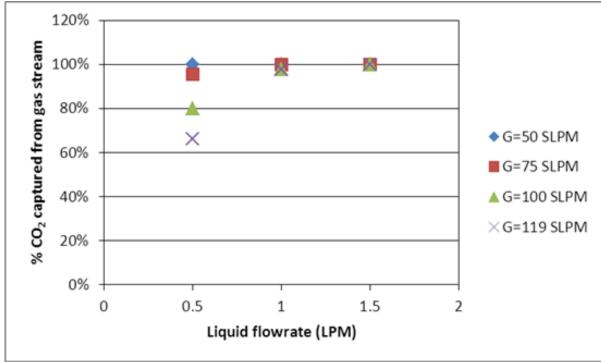
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Bench-Scale System Tests

The effect of varying liquid and gas flow rates on CO_2 capture were studied.

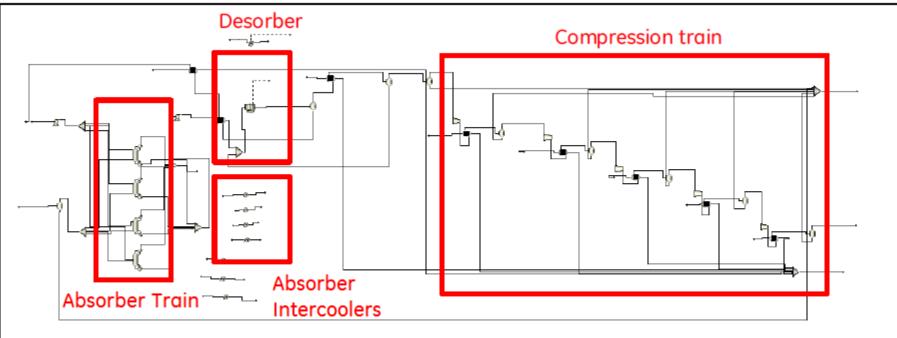
Parameter	Units	Value
Desorber temperature	°C	160
Desorber agitator speed	RPM	300
Desorber recirculation loop pump speed	% of max	50
Desorber level	in H ₂ O	7.5
Desorber pressure	psig	0
Inlet absorber temperature (gas and liquid)	°C	40
Absorber sump level	in H ₂ O	5.0
CO ₂ concentration in inlet gas to column	mol%	16
Gas source		bottled





Process Modeling

- Data from the bench-scale system were used to tune bench-scale carbon-capture model in ASPEN Plus
 - Model scaled up to pilot- and 550 MW commercial-scale
- Process modeling of the coal-fired power plant was performed in Thermoflow by GE Power and Water
 - Model without carbon capture was tuned to match Case 11 from Bituminous Baseline Study
- Power plant model and carbon capture model were integrated

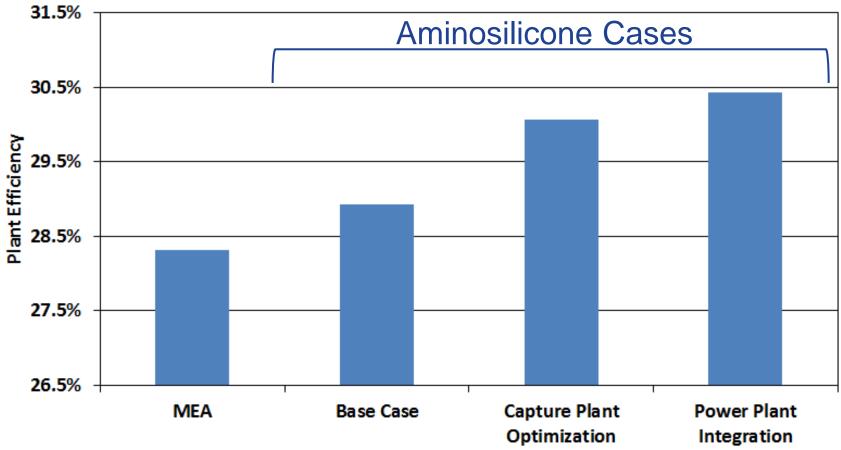


ASPEN Plus Model of Carbon-Capture System



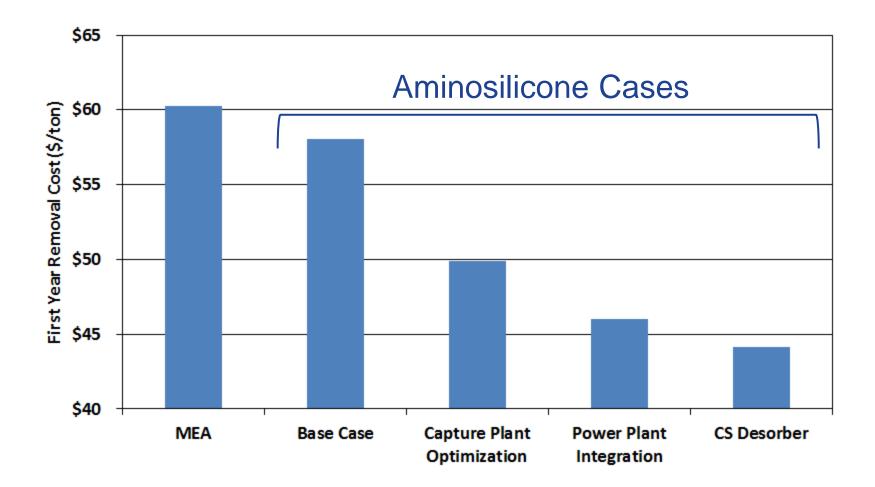
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Plant Efficiency



- Base Case Desorber at 140 °C and 4 bar(a)
- Capture Plant Optimization Optimization of desorber T, absorber column intercoolers, packing type, etc.
- Power Plant Integration Cooling water integration and waste heat recovery imagination at work

First Year Removal Cost of CO₂





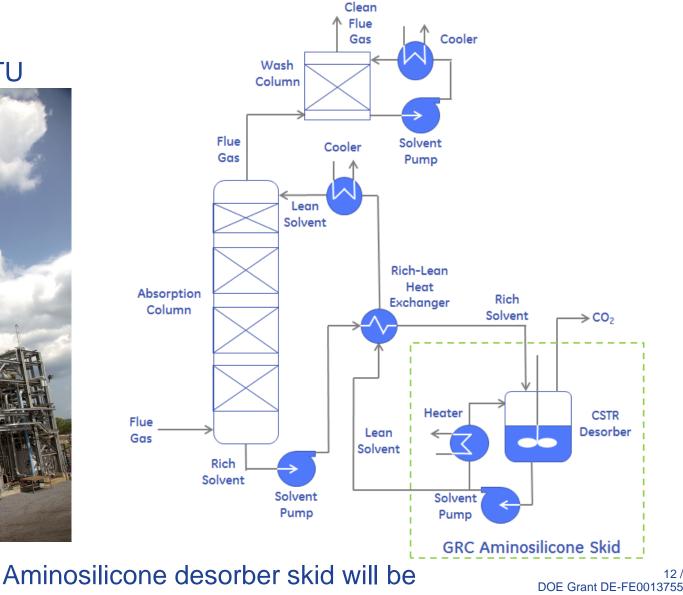
Pilot-Scale Process

CO₂-capture process for pilot-scale

The NCCC PSTU



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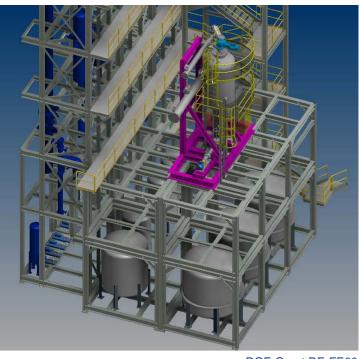
integrated with PSTU at the NCCC

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Skid Design

- Basic Engineering Package Completed
 - Detailed P&IDs
 - Initial designs/specs for major equipment
 - Material and energy balances
- Working with the NCCC
 - Kick-off meeting in first quarter of 2014
 - Transmitted Basic Engineering Package (Tier 1 information)
 - Conducted Preliminary Hazard Review







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Future Work

- Remainder of 2014
 - Complete detailed design of skid
 - Fabricate skid for delivery at the NCCC early next year
 - Perform preliminary EH&S Risk Assessment
- 2015
 - Integrate skid with PSTU at the NCCC
 - Perform tests (~3 months)
 - Use data to update process models
 - Update Techno-Economic Analysis and EH&S Risk Assessment
- Beyond
 - Determine next scale for testing
 - Consider adjacent applications with intermediate scale
 - Look for partners
 - Test site
 - Solvent manufactures
 - Need to grow solvent supply



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